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# Tailoring Lewis/Brønsted acid properties of MOF nodes *via* hydrothermal and solvothermal synthesis: simple approach with exceptional catalytic implications†

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The Lewis/Brønsted catalytic properties of the Metal–Organic Framework (MOF) nodes can be tuned by simply controlling the solvent employed in the synthetic procedure. In this work, we demonstrate that Hf-MOF-808 can be prepared from a material with a higher amount of Brønsted acid sites, *via* modulated hydrothermal synthesis, to a material with a higher proportion of unsaturated Hf Lewis acid sites, *via* modulated solvothermal synthesis. The Lewis/Brønsted acid properties of the resultant metallic clusters have been studied by different characterization techniques, including XAS, FTIR and NMR spectroscopies, combined with a DFT study. The different nature of the Hf-MOF-808 materials allows their application as selective catalysts in different target reactions requiring Lewis, Brønsted or Lewis–Brønsted acid pairs.

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## 1. Introduction

Metal–Organic Frameworks (MOFs) are microporous crystalline materials, whose framework is formed by inorganic metallic nodes connected through organic ligands.<sup>1</sup> The high chemical tunability of both components enables the rational design of these materials for selective catalytic applications based on unique structure–activity relationships.<sup>2,3</sup> Fine-tuning of the electronic properties of the metal nodes is a well-established design pathway to modulate the catalytic properties of MOF-type materials, which can usually be achieved by modifying the nature of the organic linkers,<sup>4</sup> introducing other metals in the metallic nodes<sup>5,6</sup> or creating coordinatively unsaturated open metal sites.<sup>7,8</sup>

Coordinatively unsaturated open metal sites, either naturally present in MOFs with low connectivity on the metal cluster or associated with missing organic linkers in the MOF framework, can act as selective Lewis acid sites for a wide range of organic

transformations.<sup>7,9,10</sup> The generation of these defective sites can be efficiently controlled during the solvothermal synthesis of MOFs using modulators, such as monocarboxylic acids or inorganic acids that compete with the organic linkers in bonding to the metallic nodes,<sup>11,12</sup> or following post-synthetic treatments into preformed MOFs, such as acid/base treatments.<sup>8,13</sup> Interestingly, it has been recently reported that the post-incorporation in these defective sites of water molecules *via* hydration processes could facilitate the creation of Brønsted acid sites.<sup>14,15</sup>

Zr- and Hf-MOFs have attracted great attention for their inherent chemical, mechanical and hydrothermal stabilities, offering excellent properties for their wide application in different relevant catalytic processes.<sup>16–20</sup> Despite Hf and Zr should have similar physicochemical properties, the higher oxophilicity of Hf with respect to Zr, should imply a stronger Brønsted acidic character of the  $\mu$ 3-OH groups present on the metallic node.<sup>21,22</sup> However, traditional solvothermal synthesis of Hf-MOFs usually ends up with amorphous materials or requires several weeks to crystallize.<sup>23</sup> For this reason, an alternative modulated hydrothermal approach has been recently applied to successfully synthesize the 12-connected UiO-66 material and the 6-connected MOF-808, both with Zr- and Hf-composition.<sup>24–27</sup> It is worth noting that traditional solvothermal processes require the use of large amounts of organic solvents, preferentially *N,N*-dimethylformamide (DMF), which is toxic, flammable and carcinogenic. Thus, these hydrothermally-mediated synthesis methods can be considered

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**2.2.5. XAS spectroscopy study.** X-ray absorption spectroscopy experiments were carried out at the Hf L<sub>3</sub>-edge (9561 eV) using the 20 BM beamline of Argonne National Laboratory (Lemont, IL, USA).<sup>31</sup> The samples were pelletized and the spectra were collected at room temperature in transmission mode using ionization chambers as detectors. Zn foil placed between I1 and I2 ionization chambers was used for energy calibration. Several scans per sample were acquired to ensure spectral reproducibility and good signal-to-noise ratio. Data reduction and extraction of the  $\chi(k)$  functions were performed using Athena software while EXAFS data analysis was done with Artemis software, as implemented in the Demeter package.<sup>32</sup> A core-refinement approach of data fitting was adopted, using two Debye–Waller factors ( $\sigma^2$ ) per spectrum and the same energy threshold ( $E_0$ ) for both samples. The  $\sigma^2$  and  $E_0$  values were let to vary during the fit but common between the spectra. Phase and amplitudes have been calculated by FEFF6 code using orthorhombic hafnia crystallographic file as input. Additional information will be displayed as a note below the table of EXAFS results.

### 2.3. DFT simulations

All density functional theory (DFT) calculations were carried out using the M062X functional,<sup>33</sup> the 6-31g(d,p) basis set for O, C, P and H atoms,<sup>34,35</sup> and the LANL2DZ basis set and pseudopotential for Hf<sup>36,37</sup> as implemented in the Gaussian 09 software.<sup>38</sup> For the simulation of NMR parameters, the isotropic absolute chemical shielding constants ( $\sigma$ ) were obtained using the gauge including atomic orbitals (GIAO) approach<sup>39,40</sup> and the <sup>31</sup>P chemical shifts were calculated as  $\delta_{\text{iso}}(^{31}\text{P}) = \sigma_{\text{ref}} - \sigma$ , using phosphoric acid as reference. To improve accuracy, all values were corrected with an equation obtained by fitting  $\delta_{\text{iso}}(^{31}\text{P})$  values at 6-31G(d,p) level against  $\delta_{\text{iso}}(^{31}\text{P})$  values at 6-311++G(d,p) level for a series of acid–base TMPO adducts, described in reference <sup>41</sup>.

The active sites present in the Hf-MOF-808 were simulated by cluster models containing one [Hf<sub>6</sub>O<sub>4</sub>(OH)<sub>4</sub>]<sup>12+</sup> node, the first shell of six organic linkers surrounding it, extracted from the experimental structure MOF-808,<sup>29</sup> and the six hydroxyl groups necessary to compensate the excess positive charge (see Fig. S1†). The organic linkers were simulated by benzoate anions in which the carboxylic groups of the linkers not bonded to the [Hf<sub>6</sub>O<sub>4</sub>(OH)<sub>4</sub>]<sup>12+</sup> node were replaced by hydrogen atoms. In a first step, all C–H distances were optimized while keeping the positions of all other atoms in the model fixed, and in the subsequent geometry optimizations the five hydrogen atoms of each benzoate group were kept fixed at these optimized positions in order to maintain the structure of the MOF while all other atoms in the system were allowed to move without restrictions. Models A and B in Fig. S1† include a first shell of water molecules strongly coordinated to the Hf atoms and hydrogen bonded to the hydroxyl groups, while in models C and D this shell of stabilizing water was removed to simulate the possible desorption of some of these water molecules due to the pre-treatment of the samples prior to the <sup>31</sup>P MAS NMR experiments. Models B and D are generated by proton transfer from

a  $\mu$ -3-OH Brønsted acid site (dotted circles in Fig. S1†) to a neighboring carboxylic group. The network of water molecules in B stabilize this proton, making this migration 10 kcal mol<sup>−1</sup> more favorable than the same process in the dehydrated D system. Additional water molecules are included in models E to H to simulate possible structures favored in the hydrothermal synthesis, including the partial displacement of one carboxylate linker in structure F.

## 2.4. Catalytic test reactions

**2.4.1. Meerwein–Ponndorf–Verley reduction of acetophenone with isopropanol.** The Meerwein–Ponndorf–Verley reactions were performed in 2 mL glass-vessel reactors equipped with a magnetic bar. Acetophenone (0.45 mmol, 54 mg), dodecane (0.22 mmol, 37.40 mg) as external standard and isopropanol (1.6 mL) were added to each reactor containing the corresponding amount of Hf-MOF-808 (10 mol% Hf). The mixtures were placed in an aluminum heating block at 100 °C with magnetic stirring. Approximately 50  $\mu$ L aliquots were taken at different times, diluted with ethyl acetate and centrifuged. The supernatant obtained from batch reactions were analyzed using gas chromatography in an instrument equipped with a 25 m capillary column of 5% phenylmethylsilicone.

**2.4.2. Styrene oxide ring-opening with isopropanol.** The epoxide ring-opening reactions were performed in 2 mL glass-vessel reactors equipped with a magnetic bar. Styrene oxide (0.75 mmol, 90.10 mg), *o*-xylene (0.21 mmol, 22.50 mg) as external standard and isopropanol (2 mL) were added to each reactor containing the corresponding amount of Hf-MOF-808 (2.5 mol% Hf). The mixtures were placed in an aluminum heating block at 55 °C with magnetic stirring. Approximately 50  $\mu$ L aliquots were taken at different times, diluted with ethyl acetate and centrifuged. The supernatant obtained from batch reactions were analyzed using gas chromatography in an instrument equipped with a 25 m capillary column of 5% phenylmethylsilicone.

**2.4.3.  $\alpha$ -Pinene oxide isomerization.** The isomerization reactions were performed in 2 mL glass-vessel reactors equipped with a magnetic bar.  $\alpha$ -Pinene oxide (0.34 mmol, 52 mg), dodecane (0.30 mmol, 51.10 mg) as external standard and toluene (2 mL) were added to each reactor containing the corresponding amount of Hf-MOF-808 (10 mol% Hf). The mixtures were placed in an aluminum heating block at 70 °C with magnetic stirring. Approximately 50  $\mu$ L aliquots were taken at different times, diluted with ethyl acetate and centrifuged. The supernatant obtained from batch reactions were analyzed using gas chromatography in an instrument equipped with a 25 m capillary column of 5% phenylmethylsilicone.

## 3. Results and discussion

### 3.1. Synthesis and characterization of materials

The Hf-MOF-808 material prepared *via* modulated hydrothermal synthesis, denoted as Hf-MOF-808\_H<sub>2</sub>O, requires less time to crystallize than the Hf-MOF-808 prepared *via* modulated solvothermal synthesis, denoted Hf-MOF-808\_DMF (see

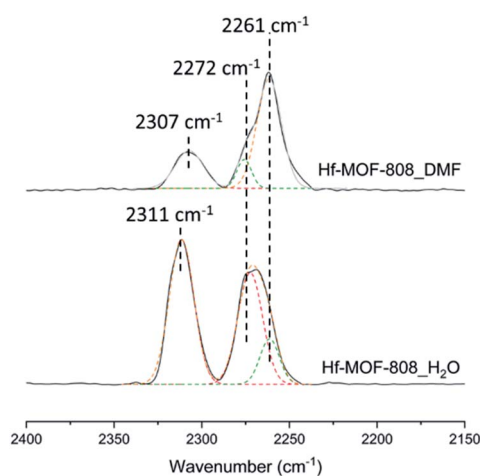




**Table 1** Data characterizing the MOF-808 materials: chemical composition, N<sub>2</sub> adsorption isotherms and catalytic performance for the Meerwein–Ponndorf–Verley (MPV) and the epoxide ring-opening (ERO) reactions

Sample	Chemical composition				N <sub>2</sub> adsorption isotherms			Catalytic performance <sup>c</sup>	
	Hf <sup>a</sup> (% wt)	C <sup>b</sup> (% wt)	H <sup>b</sup> (% wt)	N <sup>b</sup> (% wt)	BET surf. area (m <sup>2</sup> g <sup>-1</sup> )	Microp. area (m <sup>2</sup> g <sup>-1</sup> )	Microp. vol. (cm <sup>3</sup> g <sup>-1</sup> )	MPV <sup>d</sup>	ERO <sup>e</sup>
Hf-MOF-808 H <sub>2</sub> O	33.6	11.2	2.7	—	1123	1065	0.52	1.23	5.42
Hf-MOF-808 DMF	36.2	17.9	2.1	2.1	1135	1094	0.54	6.05	2.55

<sup>a</sup> Measured by ICP analysis. <sup>b</sup> Measured by elemental analysis. <sup>c</sup> Determined by TOF values (h<sup>-1</sup>). Reaction conditions. <sup>d</sup> Acetophenone (0.45 mmol), isopropanol (1.6 mL), and MOF catalyst (10 mol% Hf), temperature 100 °C. <sup>e</sup> Styrene oxide (0.75 mmol), isopropanol (2 mL), and MOF catalyst (2.5 mol% Hf), temperature 55 °C.

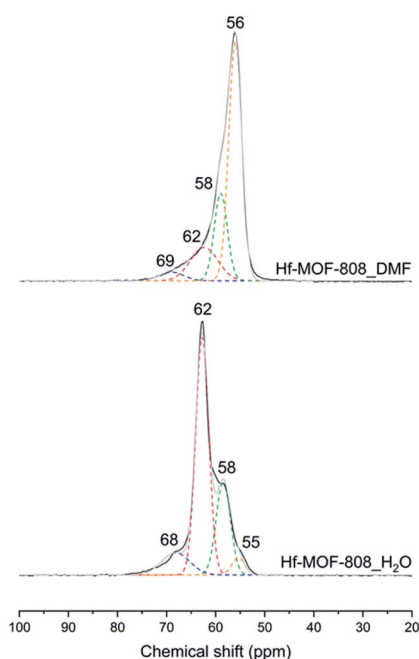


**Fig. 3** FTIR spectra of 2 mbar CD<sub>3</sub>CN adsorbed at 25 °C on Hf-MOF-808-H<sub>2</sub>O (down) and Hf-MOF-808-DMF (top). The IR bands at 2311 and 2307 cm<sup>-1</sup> are associated with CD<sub>3</sub>CN coordinated to Hf sites, and the IR bands at 2272 cm<sup>-1</sup> to OH groups in the Hf cluster. The band at 2261 cm<sup>-1</sup> is associated with physisorbed CD<sub>3</sub>CN molecules.

samples. In both Hf-MOFs, the Hf4f core line in the XPS spectra contains two peaks at 17.6 and 19.2 binding energy, corresponding to the Hf4f<sub>5/2</sub> and Hf4f<sub>7/2</sub> components of hafnium in the oxidation state Hf<sup>4+</sup> (see Fig. S5†).<sup>48,49</sup> On the other hand, the normalized XANES spectra at Hf L<sub>3</sub>-edge of the Hf-MOF-808-DMF, Hf-MOF-808-H<sub>2</sub>O and Hf-based standards are shown in Fig. 6. In both MOF samples, Hf<sup>4+</sup> is the main oxidation state due to the position of the first derivative at ~9563 eV,<sup>50,51</sup> corroborating the results obtained in the XPS analysis. The intense whiteline (related to the 2p<sub>3/2</sub> → 5d electronic transition) of the MOFs is similar to that of other Hf-based materials,<sup>50</sup> which is stronger in the Hf-MOF-808-DMF followed by the Hf-MOF-808-H<sub>2</sub>O sample. EXAFS data (see Table S3 and Fig. S6†) indicate a similar local environment around Hf atoms in both samples, with each Hf atom interacting with approximately six nearest neighbours (averaging of oxygen atoms in the metal cluster and/or solvent molecules). The obtained Hf–O and Hf–Hf distances lie between those obtained by Gianolio *et al.*<sup>52</sup> for hydroxylated/dehydroxylated Hf-MOFs.

### 3.3. Catalytic activity: Lewis and Brønsted acid-sites

After unraveling the different nature of the metallic nodes of the above described Hf-MOF-808 materials, two different catalytic processes requiring Lewis and Brønsted acid sites, such as the Meerwein–Ponndorf–Verley (MPV) and the epoxide ring-opening (ERO) reactions, respectively, have been tested to evaluate their catalytic performance. The Meerwein–Ponndorf–Verley reduction of carbonyl compounds with alcohols has been described as a model reaction to study the Lewis acidity in Hf-MOFs (see Scheme 1).<sup>53–55</sup> For this reason, the Hf-MOF-808 materials synthesized in this work are first tested for the MPV reaction of acetophenone and isopropanol (see the Experimental section for details). While the acetophenone conversion reaches ~90% after 6 h when Hf-MOF-808-DMF is used as catalyst, the acetophenone conversion only achieves ~64% after 6 h with Hf-MOF-808-H<sub>2</sub>O (see Fig. 7). The calculated turnover



**Fig. 4** <sup>31</sup>P MAS NMR spectra of TMPO loaded on Hf-MOF-808-H<sub>2</sub>O (down) and Hf-MOF-808-DMF (top). Experimental spectra are shown in black and the sum of the deconvoluted peaks in gray.



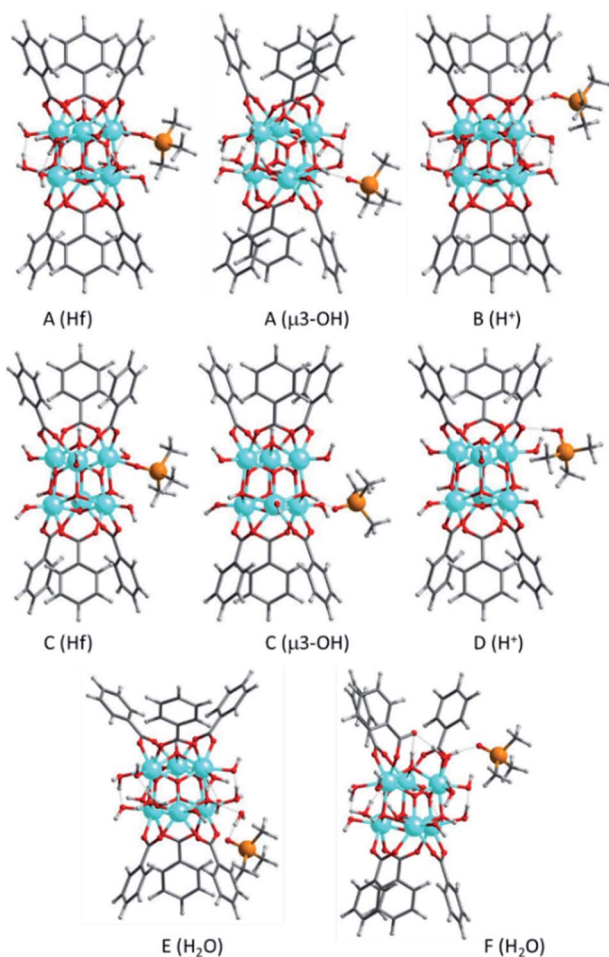
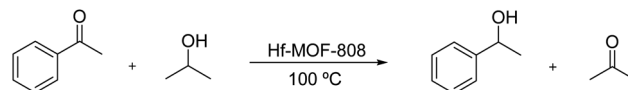


Fig. 5 Optimized geometries of TMPO interacting with Hf Lewis sites,  $\mu_3$ -OH Brønsted acid sites, or additional  $\text{H}_2\text{O}$  molecules, and of protonated  $\text{TMPOH}^+$  in Hf-MOF-808 models. The labels A to F identify the MOF-808 model used, as described in Fig. S1,† and the type of interaction between TMPO and MOF-808 is given in parenthesis. C and O atoms are depicted as gray and red sticks, Hf, P and H as cyan, yellow and white balls.



Scheme 1 Meerwein-Ponndorf-Verley reduction of acetophenone with isopropanol catalyzed by Hf-MOF-808.

frequency (TOF) with Hf-MOF-808\_DMF is  $\sim 5.0$  times higher than the calculated TOF when using Hf-MOF-808\_ $\text{H}_2\text{O}$  for the MPV transformation (see Table 1). This result is consistent with the previous characterization. The higher amount of 5d orbitals in the MOF-808 sample synthesized in DMF media and, therefore, the more accessible Lewis acid sites, would corroborate its higher activity for the Lewis acid-demanding MPV catalytic reaction.

On the other hand, the oxide ring-opening reaction (see Scheme 2) has been employed as a model catalytic test to distinguish catalytic Brønsted acid sites.<sup>16,56,57</sup> Considering this, Hf-MOF-808\_ $\text{H}_2\text{O}$  and Hf-MOF-808\_DMF have been tested for the styrene oxide ring-opening reaction with isopropanol (see the experimental section for details).

The styrene oxide conversion is almost completed after 21 h when using Hf-MOF-808\_ $\text{H}_2\text{O}$  as catalyst, whereas Hf-MOF-808\_DMF material only achieves  $\sim 43\%$  conversion at this point (see Fig. 8). Moreover, the calculated TOF ( $\text{h}^{-1}$ ) with Hf-MOF-808\_ $\text{H}_2\text{O}$  catalyst is  $\sim 2.0$  higher than Hf-MOF-808\_DMF for this transformation (see Table 1). The improved Brønsted acidity introduced into the metallic nodes of the Hf-MOF-808 during the hydrothermal synthesis would explain the remarkable catalytic differences for the styrene ring-opening reaction.

If both reactions are considered, the relative catalytic activities, measured as  $\text{TOF}_{\text{ERO}}/\text{TOF}_{\text{MPV}}$ , for Hf-MOF-808\_ $\text{H}_2\text{O}$  and Hf-MOF-808\_DMF are 4.41 and 0.42, respectively (see Table S1,†). The different relative catalytic activity by a factor of  $\sim 10$  for the two Hf-MOF-808 catalysts, could be tentatively connected to the different relative amount of Brønsted to Lewis acid sites obtained from the  $^{31}\text{P}$  MAS NMR spectra after TMPO

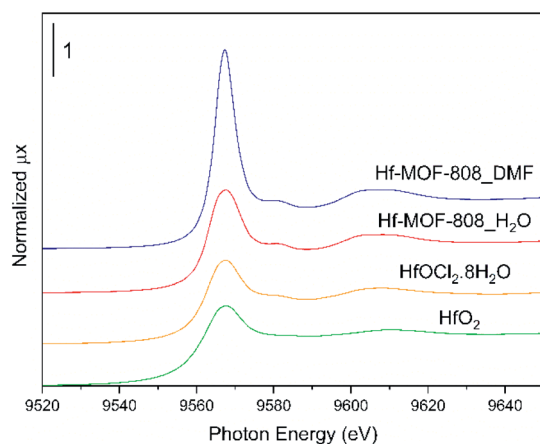


Fig. 6 Normalized XANES spectra at Hf  $L_3$ -edge of Hf-MOF-808 samples and Hf-based standards.

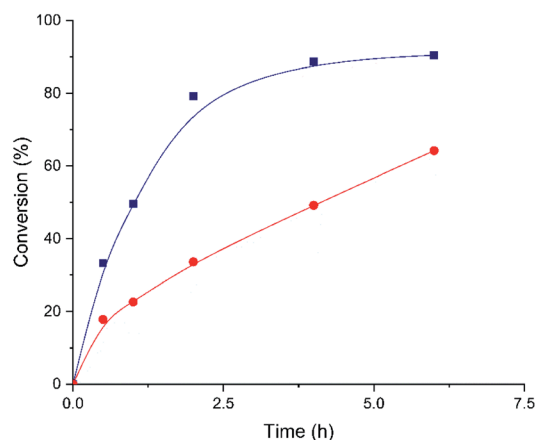
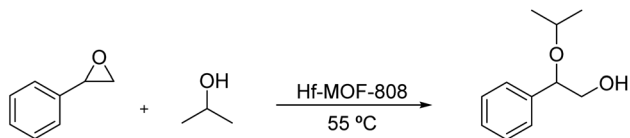


Fig. 7 Kinetic profiles for acetophenone conversion employing Hf-MOF-808\_ $\text{H}_2\text{O}$  (red circles) and Hf-MOF-808\_DMF (blue squares) as catalysts.





Scheme 2 Styrene oxide ring-opening with isopropanol catalyzed by Hf-MOF-808.

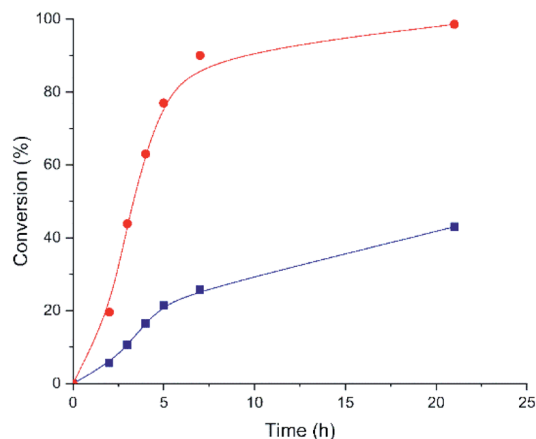
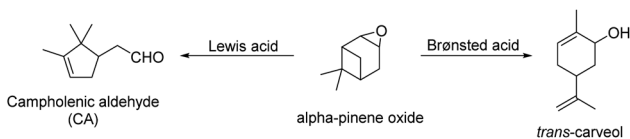


Fig. 8 Kinetic profiles for styrene oxide conversion employing Hf-MOF-808\_H<sub>2</sub>O (red circles) and Hf-MOF-808\_DMF (blue squares) as catalysts.

adsorption, which is  $\sim 9$  times higher for Hf-MOF-808\_H<sub>2</sub>O than for Hf-MOF-808\_DMF (see Table S1†). These evidences may indicate good structure–activity relationships for both Hf-containing MOF-808 catalysts.

Finally, the  $\alpha$ -pinene oxide isomerization has been employed to evaluate the catalytic performance of the prepared Hf-MOF-808, since this reaction is very sensitive to the presence of Lewis and Brønsted acid sites. Indeed, the product distribution of this reaction unavoidably depends on the nature of the acid sites (see Scheme 3): (1) the selectivity toward campholenic aldehyde (CA) is usually lower than 55% with Brønsted acids, whereas the CA selectivity is considerably higher with Lewis acid sites ( $>85\%$ );<sup>58,59</sup> (2) a significant amount of *trans*-carveol is formed with Brønsted acid sites.<sup>60–62</sup>

As seen in Fig. 9 and S7,† both Hf-MOF-808 materials show a similar  $\alpha$ -pinene oxide conversion after 5 h ( $\sim 75$ – $80\%$ ), but the product distribution is considerably different. Hf-MOF-808 obtained *via* hydrothermal synthesis shows  $\sim 45\%$  selectivity toward CA, in good agreement with descriptions in the literature where Brønsted acid catalysts present CA selectivities below 55% (see Fig. 9 and S8†), whereas Lewis-acid containing Hf-



Scheme 3 Isomerization of  $\alpha$ -pinene oxide.

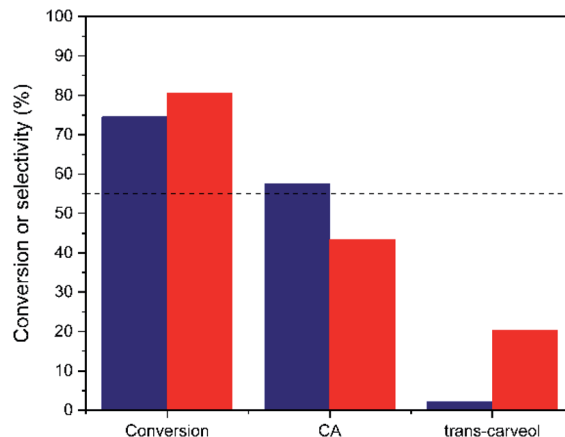


Fig. 9 Conversion and different product selectivities obtained for the  $\alpha$ -pinene oxide isomerization when using Hf-MOF-808\_H<sub>2</sub>O (red bar) and Hf-MOF-808\_DMF (blue bar) as catalysts.

MOF-808\_DMF approaches  $\sim 60\%$  CA selectivity (see blue bar in Fig. 9). Moreover, a remarkably higher amount of *trans*-carveol has been obtained when using the Hf-MOF-808\_H<sub>2</sub>O as catalyst ( $\sim 20\%$ , see Fig. 9) compared to Hf-MOF-808\_DMF, where only traces of *trans*-carveol are observed (see Fig. 9).

The heterogeneous catalytic nature and the cycle performance of the Hf-MOFs for the  $\alpha$ -pinene oxide isomerization have been studied. To do this, hot filtration and recyclability tests have been carried out, respectively (see Fig. S9†). On the one hand, the  $\alpha$ -pinene oxide conversions remain unaltered after filtering the solid catalysts in both cases (see Fig. S9A†). On the other hand, the Hf-MOF-808 samples can be reused at least two consecutive runs with only a minor decrease in the catalytic activity (see Fig. S9B†). These evidences corroborate the heterogeneous catalytic nature and the stability of the Hf-MOF-808 catalysts for the  $\alpha$ -pinene oxide isomerization reaction.

## 4. Conclusions

In this work, it has been shown how the Lewis/Brønsted catalytic properties of the Hf-MOF-808 material can be simply and efficiently adjusted by controlling the solvent employed in the synthetic procedure. The modulated hydrothermal synthesis maximizes the presence of Brønsted acid sites, whereas solvothermal synthesis allows increasing the proportion of unsaturated Hf Lewis acid sites. These different Lewis/Brønsted acidities, which have been adequately characterized by different techniques, in Hf-MOF-808 materials have a direct impact on their catalytic activity and selectivity, in particular when very sensitive and complex target reactions are studied. The ability to design and control the different nature of the metallic active sites by simple, direct and green synthesis methods, as those presented here for the Hf-MOF-808 material, could be extended to other MOF-type structures and even to the design of multifunctional MOF-based catalysts where different metals or organic linkers can be combined to incorporate other chemical functionalities.



## Author contributions

The manuscript was written through the contributions of all authors. All authors have given approval to the final version of the manuscript.

## Conflicts of interest

There are no conflicts to declare.

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