

Electrocatalysis of hydrogen peroxide reactions on perovskite oxides: experiment *versus* kinetic modeling†

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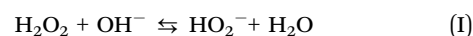
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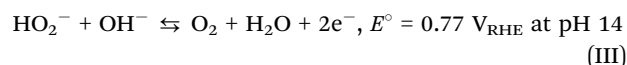
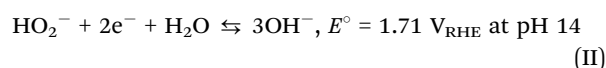
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Hydrogen peroxide has been identified as a stable intermediate of the electrochemical oxygen reduction reaction on various electrodes including metal, metal oxide and carbon materials. In this article we study the hydrogen peroxide oxidation and reduction reactions in alkaline medium using a rotating disc electrode (RDE) method on oxides of the perovskite family (LaCoO₃, LaMnO₃ and La_{0.8}Sr_{0.2}MnO₃) which are considered as promising electrocatalytic materials for the cathode of liquid and solid alkaline fuel cells. The experimental findings, such as the higher activity of Mn-compared to that of Co-perovskites, the shape of RDE curves, and the influence of the H₂O₂ concentration, are rationalized with the help of a microkinetic model.

Considering the value of pK_a of H₂O₂ (11.7⁴), in alkaline media it transforms into HO₂[−]:



Four electrode reactions can theoretically occur in the presence of HO₂[−]: HO₂[−] reduction into OH[−] (II), HO₂[−] oxidation into O₂ (III), and the inverse reactions, OH[−] oxidation into HO₂[−] (−II) and O₂ reduction into HO₂[−] (−III).



1. Introduction

Hydrogen peroxide has been identified as a stable intermediate of the electrochemical oxygen reduction reaction (ORR) on various electrodes including metal, metal oxide and carbon materials. In this article we study the hydrogen peroxide oxidation and reduction reactions (HPOR/HPRR) in alkaline medium on oxides of the perovskite family which are considered as promising electrocatalytic materials for the cathode of liquid and solid alkaline fuel cells. While several researchers studied the catalytic hydrogen peroxide decomposition kinetics on perovskite oxides, very few published results can be found for the study of the electrochemical HPOR/HPRR on perovskite oxides,^{1–3} and these are unfortunately not sufficiently detailed.

Given the standard potential of the HO₂[−]/OH[−] couple, the OH[−] oxidation into HO₂[−] (step −II) is unlikely in the potential range of interest for a cathode of an alkaline fuel cell, and will be neglected in this work. Thus, the current–potential curve over a perovskite electrode in a H₂O₂ containing electrolyte is essentially determined by reactions II, III, and −III.

In this work, the HPOR and HPRR are studied using the rotating disc electrode (RDE) method on two oxides of the perovskite family, LaCoO₃ and La_{0.8}Sr_{0.2}MnO₃, which demonstrated distinct behavior in the ORR (see our recent work in ref. 5), as well as on LaMnO₃. The activity of the oxide materials is compared with that of Pt/C, a reference material in fuel cell electrocatalysis, and with carbon. The latter is an essential component of transition metal oxide-based cathodes improving their electronic conductivity, and thus the degree of the catalyst utilization. To better understand the mechanism of the HPOR and HPRR, and the ORR, on perovskite oxides, a kinetic model is proposed, and the experimental RDE curves are compared with the simulated ones. The study of the influence of the H₂O₂ concentration on the HPOR and HPRR allows one to shed light on the reaction kinetics and helps to validate the model assumptions.

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2. Experimental

LaCoO₃, LaMnO₃ and La_{0.8}Sr_{0.2}MnO₃ were synthesized at the Moscow State University using polyacrylamide gel by a soft chemistry method, which offers materials with higher surface areas than conventional high temperature approaches. For the synthesis procedure the reader is referred to ref. 5. Specific surface areas of LaCoO₃, LaMnO₃ and La_{0.8}Sr_{0.2}MnO₃ measured by BET were 10, 14 and 17 m² g⁻¹, respectively. Oxides were mixed with carbon and deposited on a glassy carbon RDE (0.07 cm² geometric area, Autolab) in the form of a thin layer.⁵ Carbon of the Sibunit family with a BET surface area of 65.7 m² g⁻¹ was chosen due to its high purity and high electron conductivity.⁶ In order to improve the adhesion of the perovskite and carbon particles onto the GC support, an alkaline ionomer (AS-4 from Tokuyama Company) was deposited on top of the dry catalyst layer to form a thin film (the ionomer loading was 2.4 μg cm⁻²). For further details on the electrode preparation the reader is referred to ref. 5. For all oxide/carbon loadings utilized in this work the catalytic layer thickness was smaller than the diffusion layer thickness.

Pt/C electrodes were prepared by drop-casting a suspension containing Pt/C (40 wt% Pt on carbon black, Alfa Aesar) to obtain 20 μg cm⁻² Pt loading. The roughness factor of Pt on the electrode estimated using the coulometry of the hydrogen underpotential deposition was equal to 6.

Electrochemical measurements were performed at 25 °C in a three electrode cell whose parts in contact with the electrolyte were made out of Teflon. The electrolyte was 1 M NaOH prepared from extra pure NaOH solution (50 wt% solution in water, Acros Organics) and ultrapure water (Purcelab: 18.2 MΩ cm, < 3 ppb TOC). The counter electrode was a platinum wire and the reference electrode was a Hg/HgO/1 M NaOH electrode (IJ Cambria Scientific). In what follows the electrode potentials are given in the RHE (reversible hydrogen electrode) scale. RDE curves were IR-corrected by using the value of the electrolyte resistance (15 Ohm) determined from the high frequency part of the electrochemical impedance spectra (measured in the 1 Hz to 100 kHz range). Electrochemical measurements were performed using an Autolab potentiostat with an analog scan generator at a scan rate of 10 mV s⁻¹. H₂O₂ solutions were prepared from 30 wt% solution in water (SupraPur, Merck) titrated with standardized KMnO₄.

3. Results and discussion

Fig. 1a shows positive scans of RDE voltammograms in N₂-purged 1 M NaOH containing 0.84 mM H₂O₂ for LaCoO₃/carbon, LaMnO₃/carbon and La_{0.8}Sr_{0.2}MnO₃/carbon composite electrodes, as well as for Pt/C and Sibunit carbon. Such H₂O₂ concentration was chosen since it corresponds to the O₂ concentration in the O₂ saturated electrolyte. For Pt/C in agreement with the literature data^{7–10} the voltammogram is reversible, suggesting fast hydrogen peroxide oxidation and reduction reactions, and the anodic and cathodic current plateaus correspond to the diffusion limited HPOR and HPRR,

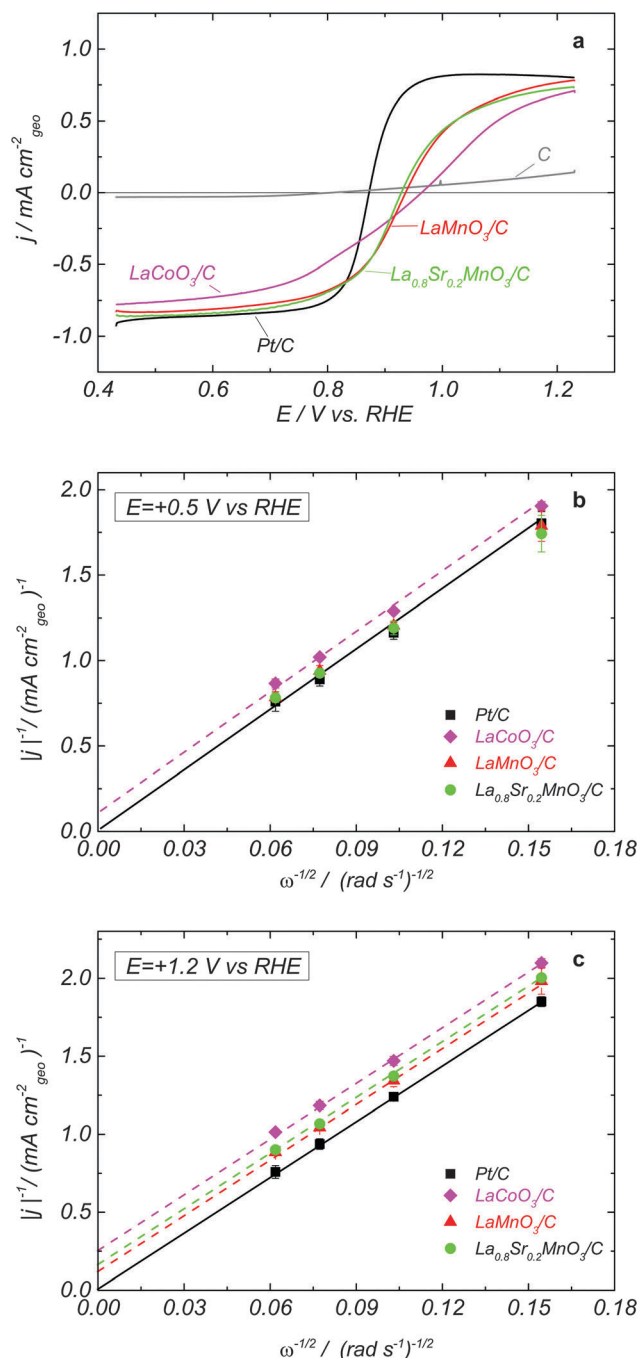


Fig. 1 (a) Positive scans of the RDE voltammograms in N₂-purged 1 M NaOH + 0.84 mM H₂O₂ at 900 rpm and 10 mV s⁻¹ and corresponding Levich–Koutecky plots at +0.5 V_{RHE} (b) and at +1.2 V_{RHE} (c) for GC-supported thin films of LaCoO₃ + C (magenta), LaMnO₃ + C (red), La_{0.8}Sr_{0.2}MnO₃ + C (green), C (grey) and Pt/C (black). Catalyst loadings are 91 μg cm⁻² perovskite + 37 μg cm⁻² carbon for oxide electrodes, 37 μg cm⁻² for carbon electrodes, and 50 μg cm⁻² for Pt/C electrodes. Currents are normalized to the electrode geometric area and corrected to the background currents measured in a N₂ atmosphere. Error bars in panels (b) and (c) represent standard deviations from at least two independent repeated measurements.

as confirmed by the Levich–Koutecky (LK) plots shown in Fig. 1b and c. For Sibunit carbon, the voltammogram is strongly irreversible, pointing to a very slow HPOR and an even slower



HPRR (Fig. 1, grey curve). For oxide/carbon composites, both the anodic and the cathodic waves have smaller slopes compared to Pt, pointing out at slower electrocatalysis of hydrogen peroxide reactions on studied perovskite oxides. Furthermore, the mixed potential values, where the sum of currents of all electrode reactions (reactions II/–II and III/–III) is equal to zero, for perovskite oxides are shifted positive compared to those of Pt/C, suggesting a slower HO_2^- oxidation, notably for LaCoO_3 . In the absence of carbon, perovskite oxides show slower hydrogen peroxide oxidation/reduction kinetics (Fig. S1, ESI†). However, contrary to what has recently been demonstrated for the ORR on oxides of the perovskite family, where carbon plays a dual role, (i) improving the interparticle contact, and also (ii) participating in the ORR electrocatalysis, the enhancement of the rates of HPOR and HPRR is predominantly due to the first factor (improvement of the electronic conductivity of the catalytic layer). This is due to the low catalytic activity of carbon in HO_2^- reactions (*cf.* Fig. 1a, grey curve). Note also that for LaMnO_3 the effect of addition of carbon on the RDE curves is stronger compared to that for the $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$. This can be attributed to a higher intrinsic electron conductivity of the doped compared for the undoped Mn-based perovskite (for further details see ESI†).

The Mn-based LaMnO_3 and $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$ perovskites display close mixed potentials (similar trends can be found in the

literature for $\text{La}_{1-x}\text{Sr}_x\text{MnO}_3$ ¹), and very similar activities for HO_2^- reduction/oxidation, once sufficient amount of carbon is present in the catalytic layer (Fig. 1a). Moreover, their HO_2^- reduction and oxidation currents approach the diffusion plateau reached by the Pt/C electrode at low and high potentials, respectively (note however that at 1.2 V the intercepts of the LK plots are non-zero). This suggests that on Mn perovskite oxides at high overpotentials the HPOR and HPRR are diffusion-limited. For LaCoO_3 electrodes, the currents do not reach the plateaus of Pt/C, due to a slower HO_2^- reduction and oxidation kinetics. The comparison of the current slope near the mixed potential for various perovskites (Fig. 1a) confirms that LaCoO_3 is less catalytically active in HO_2^- reactions than either LaMnO_3 or $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$. Since the mixed potential of LaCoO_3 is positively shifted compared to that of Mn perovskite oxides, we conclude that the HPOR is slower than the HPRR on the cobalt perovskite. The cathodic branch of the RDE voltammograms for LaCoO_3 shows two slopes (Fig. 1a) suggesting that at least two steps are involved in the HO_2^- reduction reaction. In what follows this hypothesis will be corroborated with the help of a mathematical model.

The influence of the H_2O_2 concentration on the HPOR and HPRR kinetics is shown in Fig. 2a for $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$. While the absolute values of the limiting anodic and cathodic currents increase proportionally to the H_2O_2 concentration, the mixed

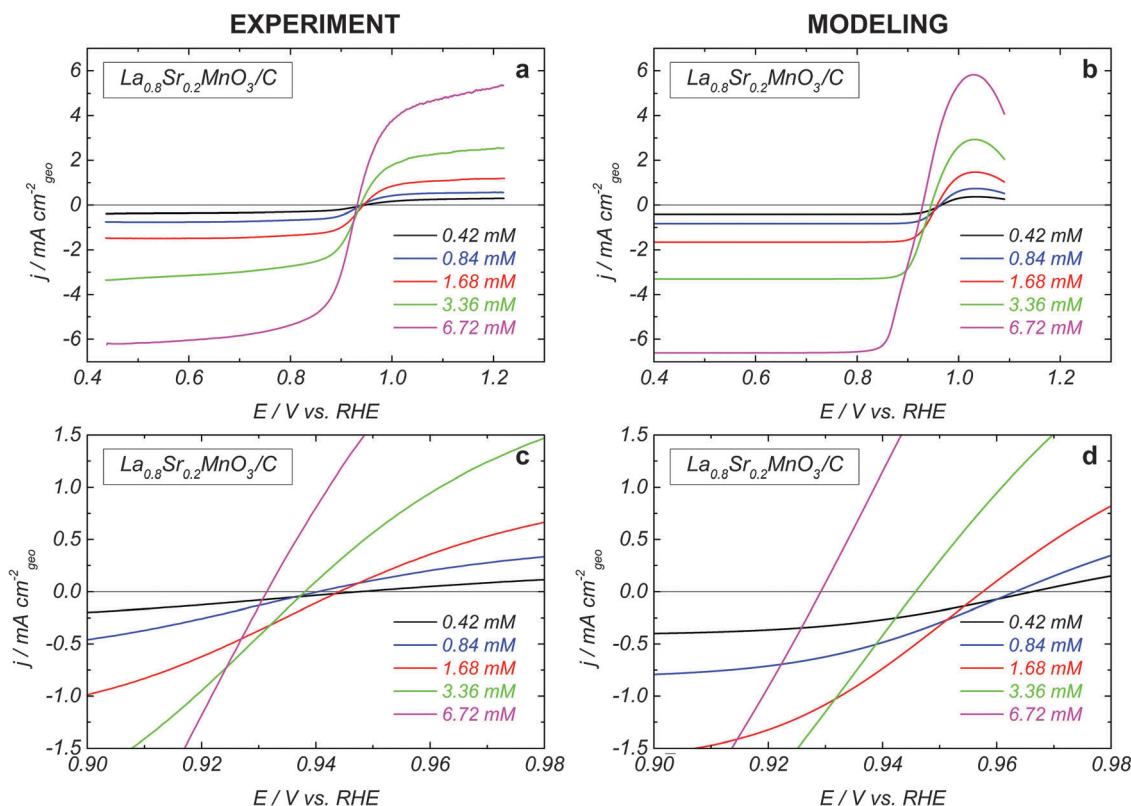


Fig. 2 (a) Experimental positive scans of the RDE voltammograms in N_2 -purged solutions of 1 M NaOH and various H_2O_2 concentrations at 900 rpm and 10 mV s^{-1} for GC-supported thin films of $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$ ($91 \mu\text{g cm}^{-2}$) + carbon ($74 \mu\text{g cm}^{-2}$). Currents are normalized to the geometric area of the electrode and corrected to the background currents measured in a N_2 atmosphere. (b) Simulated RDE voltammograms. (c) and (d) show close-ups for experimental (c) and simulated (d) voltammograms. For details see the text.



potential is displaced towards the negative values (see close-up in Fig. 2c). The same behavior was observed for LaCoO₃ (not shown). This indicates that the perovskite oxide-catalyzed HO₂[−] reduction and the HO₂[−] oxidation reactions have different concentration dependences.

In order to better understand the experimental findings, a microkinetic model was developed. Note that the mathematical model serves to understand the influence of the experimental parameters (potential and concentration), the differences between Mn and Co perovskites, and to verify the consistency of the proposed reaction mechanism with the experimental data, rather than to accurately determine the values of the rate constants. The elementary steps for the HO₂[−] and O₂ adsorption and reaction on perovskite oxides were inspired by the experimental studies of Goodenough¹¹ and Suntivich *et al.*¹² and the density functional theory (DFT) calculations of Wang and Cheng,¹³ and adapted in order to reproduce the experimental findings of this work.

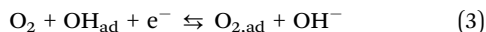
Since the oxide surface in an alkaline electrolyte is supposed to be covered by OH_{ad},^{11,14} displacement of OH_{ad} by either O₂ or HO₂[−] is likely to be the first step in the electrocatalysis of O₂¹¹ and H₂O₂ reactions.



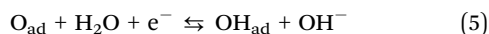
The adsorbed HO_{2,ad} may be oxidized into oxygen in the reverse step of reaction (2):



The adsorbed oxygen molecule resulting from the backward step of reaction (2) may desorb in the reverse step of reaction (3). In agreement with the literature,^{11,13} we suppose that upon adsorption oxygen molecules displace hydroxo species on the oxide surface:



The adsorbed HO_{2,ad} can also undergo reduction. To account for the negative shift of the mixed potential with the increase of the H₂O₂ concentration, the HPOR and the HPRR must have different concentration dependence. In order to reproduce this, we assume that the HO_{2,ad} reduction occurs in a sequence of chemical and electrochemical steps:



Note that steps (1)–(5) also account for the catalytic decomposition of H₂O₂ occurring under open circuit conditions.

Considering both the experimental and the literature data we suppose that O_{ad} species are adsorbed on transition metal (B) cations in the high oxidation state B^{(m+1)+} (B=O), while OH_{ad} species – on B-cations in the low oxidation state B^{m+} (B–OH). According to the DFT calculations of Wang and Cheng,¹³ these intermediates (OH_{ad} and O_{ad}) are indeed strongly adsorbed on the surface of perovskite oxides.

Assuming Langmuir-type adsorption isotherms and Butler–Volmer type of the electrochemical kinetics, the reaction rates may be expressed as follows:

$$v_1 = k_1 c_{\text{HO}_2^-}^{\text{S}} (1 - \theta_{\text{O}_2} - \theta_{\text{HO}_2} - \theta_{\text{O}}) - k_{-1} \theta_{\text{HO}_2} \quad (6)$$

$$v_2 = k_2 \theta_{\text{O}_2} \exp\left(\frac{-(1-\alpha)FE}{RT}\right) - k_{-2} \theta_{\text{HO}_2} \exp\left(\frac{\alpha FE}{RT}\right) \quad (7)$$

$$v_3 = k_3 c_{\text{O}_2}^{\text{S}} (1 - \theta_{\text{O}_2} - \theta_{\text{HO}_2} - \theta_{\text{O}}) \exp\left(\frac{-(1-\alpha)FE}{RT}\right) - k_{-3} \theta_{\text{O}_2} \exp\left(\frac{\alpha FE}{RT}\right) \quad (8)$$

$$v_4 = k_4 \theta_{\text{HO}_2} (1 - \theta_{\text{O}_2} - \theta_{\text{HO}_2} - \theta_{\text{O}}) \quad (9)$$

$$v_5 = k_5 \theta_{\text{O}} \exp\left(\frac{-(1-\alpha)FE}{RT}\right) - k_{-5} (1 - \theta_{\text{O}_2} - \theta_{\text{HO}_2} - \theta_{\text{O}}) \exp\left(\frac{\alpha FE}{RT}\right) \quad (10)$$

where $c_{\text{HO}_2^-}^{\text{S}}$, $c_{\text{O}_2}^{\text{S}}$ are the concentrations in front of the electrode at $x = 0$ (x is the distance along the normal to the electrode surface) and θ_{HO_2} , θ_{O_2} , θ_{O} the coverages of adsorbed intermediates, with $\theta_{\text{OH}} = 1 - \theta_{\text{O}_2} - \theta_{\text{HO}_2} - \theta_{\text{O}}$. α is the charge transfer coefficient, $F = 96486 \text{ C mol}^{-1}$ is the Faraday constant, $R = 8.314 \text{ J K}^{-1} \text{ mol}^{-1}$ the ideal gas constant and $T = 300 \text{ K}$ the absolute temperature.

Under stationary conditions, this reaction scheme can be cast into a set of equations determining the concentrations of HO₂[−] and O₂ in front of the electrode surface, and the coverages of adsorbed intermediates, HO_{2,ad}[−], O_{2,ad}, O_{ad}, and OH_{ad} on perovskite sites:

$$D_{\text{O}_2} \left(\frac{\partial c_{\text{O}_2}}{\partial x} \right) = - \frac{D_{\text{O}_2} c_{\text{O}_2}^{\text{S}}}{\delta_{\text{O}_2}} = \Gamma_{\text{geo}} v_3 \quad (11)$$

$$D_{\text{HO}_2^-} \left(\frac{\partial c_{\text{HO}_2^-}}{\partial x} \right) = \frac{D_{\text{HO}_2^-} (c_{\text{HO}_2^-}^{\text{b}} - c_{\text{HO}_2^-}^{\text{S}})}{\delta_{\text{HO}_2^-}} = \Gamma_{\text{geo}} v_1 \quad (12)$$

$$\frac{d\theta_{\text{O}_2}}{dt} = v_3 - v_2 = 0 \quad (13)$$

$$\frac{d\theta_{\text{HO}_2}}{dt} = v_1 + v_2 - v_4 = 0 \quad (14)$$

$$\frac{d\theta_{\text{O}}}{dt} = 2v_4 - v_5 = 0 \quad (15)$$

where δ_i is the diffusion layer thickness, $c_{\text{HO}_2^-}^{\text{b}}$, the concentration of HO₂[−] in the bulk of the electrolyte, and Γ_{geo} stands for the number of active sites per geometric area of the electrode. The overall current density is given by eqn (16).

$$j = -F\Gamma_{\text{geo}}(v_2 + v_3 + v_5) \quad (16)$$

A linear concentration profile for O₂ and HO₂[−] is assumed in front of the electrode surface. The electrode thickness is assumed to be sufficiently small to keep this linear



Table 1 Rate constants used in the mathematical model to simulate the experimental curves of LaCoO₃ and La_{0.8}Sr_{0.2}MnO₃ electrodes

Rate constant	Units	Value	
		LaCoO ₃	La _{0.8} Sr _{0.2} MnO ₃
k_1	$\text{cm}^3 \text{mol}^{-1} \text{s}^{-1}$	5×10^7	5×10^7
k_{-1}	s^{-1}	50	50
k_2	s^{-1}	5.1×10^8	5.1×10^9
k_{-2}	s^{-1}	4.9×10^{-8}	4.9×10^{-7}
k_3	$\text{cm}^3 \text{mol}^{-1} \text{s}^{-1}$	1.6×10^{11}	1.6×10^{12}
k_{-3}	s^{-1}	1.6×10^{-8}	1.6×10^{-7}
k_4	s^{-1}	40	40
k_5	s^{-1}	6×10^7	1.2×10^8
k_{-5}	s^{-1}	2.9×10^{-9}	5.8×10^{-9}

concentration profile. The diffusion coefficients of O₂ and HO₂[−] in 1 M NaOH were determined as $D_{\text{O}_2} = 1.5 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ and $D_{\text{HO}_2^-} = 0.8 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$, respectively, from the corresponding diffusion limited current plateaus for Pt/C electrodes. Thus, the diffusion layer thickness at 900 rpm is $\delta_{\text{O}_2} = 19 \mu\text{m}$ for O₂ and $\delta_{\text{HO}_2^-} = 15 \mu\text{m}$ for HO₂[−].

Assuming that B cations act as active sites, the number of active sites per geometric surface area Γ_{geo} was calculated from the catalyst loading and the number of B sites per unit of the real surface area, which was estimated from the crystalline structure of perovskite oxides as $4.14 \times 10^{-10} \text{ mol cm}^{-2}_{\text{oxide}}$. The values of the reaction rate constants were adjusted in order to reproduce the main features of the experimental RDE voltammograms for HPOR and HPRR, as well as for the ORR,⁵ and are given in Table 1. Symmetry factors were all considered to be equal to 0.5, which is realistic for low and moderate overvoltages considered in this work. The adsorption-desorption rates of HO₂[−] on perovskite sites directly depend on the values of k_1 and k_{-1} which have to be considered sufficiently high for adsorption and low for desorption to account for the significant activity of perovskites in the HPRR. k_2 and k_3 were adjusted to reproduce both the onset potential and the Tafel slopes for the ORR on perovskite oxides,⁵ while the rate constants of the reverse reactions k_{-2} , k_{-3} were chosen to account for the standard potential of the O₂/HO₂[−] at 0.77 V vs. RHE.

Finally, the values of the mixed potential for the HPRR/HPOR and the potential of the B^{(m+1)+}/B^{(m)+} redox peaks (see CVs in ref. 5) were used to adjust the values of k_4 , k_5 and k_{-5} .

Fig. 3 shows simulated RDE voltammograms for LaCoO₃ and La_{0.8}Sr_{0.2}MnO₃ oxides. The rate constants are listed in Table 1, and an almost reversible voltammogram is obtained for La_{0.8}Sr_{0.2}MnO₃ (Fig. 3b). By choosing smaller rate constants for steps 2, 3 and 5, we are able to reproduce a slower HPOR on LaCoO₃ (cf. Fig. 3a and b) and a positive shift of the mixed potential compared to La_{0.8}Sr_{0.2}MnO₃. Furthermore, the assumption of the HO_{2,ad} reduction as a sequence of two elementary steps allows us to reproduce the observed change of the slope of the HPRR on LaCoO₃. Fig. 3 also shows the splitting of the RDE voltammograms into a sum of three main contributions for two HO₂[−] concentrations. The anodic branch corresponds to the HO₂[−] oxidation into O₂ (step III), while the cathodic branch consists of two contributions: the HO₂[−] reduction into OH[−] (step II) and the O₂ reduction (this oxygen is formed in the anodic branch) into HO₂[−] (step −III). One may note that the differences between LaCoO₃ and La_{0.8}Sr_{0.2}MnO₃ are partly due to the lower ORR activity of LaCoO₃ (cf. blue curves in Fig. 3a and b). For experimental ORR data on LaCoO₃ and La_{0.8}Sr_{0.2}MnO₃ the reader is referred to our earlier publication.⁵

The influence of the H₂O₂ concentration can be traced from simulated voltammograms shown in Fig. 2b, d and 3b. Increasing the concentration directly affects the reaction rate of the adsorption-desorption of HO₂ (reaction (1)) and therefore the site coverage by HO_{2,ad} species (θ_{HO_2}). In the anodic direction, an increase of θ_{HO_2} causes an increase in the rate (step −2) of formation of O_{2,ad} from HO_{2,ad} (cf. dashed over solid green lines in Fig. 3b). On the other hand, in the cathodic branch, an increase of the HO₂[−] concentration does not lead to a strong acceleration of reaction (4), since its rate depends on both θ_{HO_2} and $\theta_{\text{OH}} = (1 - \theta_{\text{O}_2} - \theta_{\text{HO}_2} - \theta_{\text{O}})$ (cf. dashed over solid magenta lines in Fig. 3b). A stronger concentration dependence of the HO₂[−] oxidation compared to the reduction counterpart, and the potential dependence of the former result in the negative shift of the mixed potential with the HO₂[−] concentration (Fig. 3b, black curves, and Fig. 2b and d).

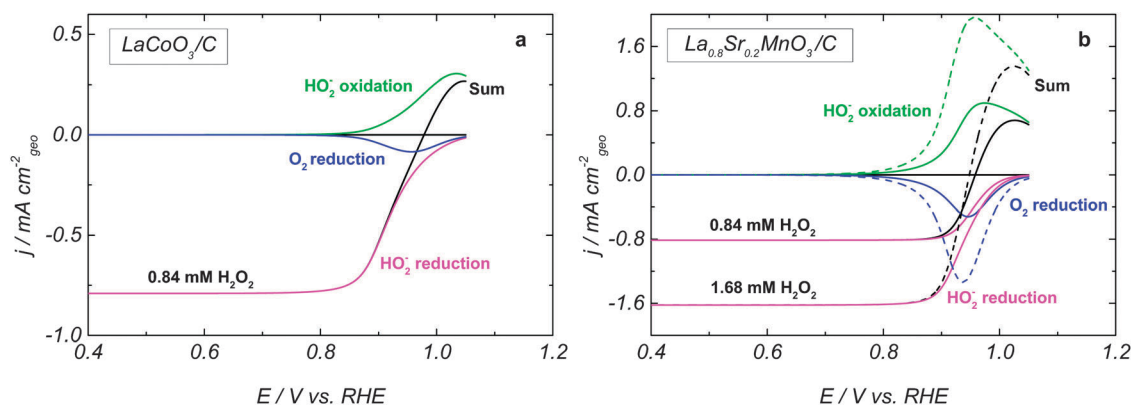


Fig. 3 Simulated RDE voltammograms for (a) LaCoO₃ and (b) La_{0.8}Sr_{0.2}MnO₃ in 0.84 mM H₂O₂ (solid lines) and 1.68 mM H₂O₂ (dashed lines) at 900 rpm. The number of sites per geometric surface area is $3.8 \times 10^{-9} \text{ mol cm}^{-2}_{\text{geo}}$ for LaCoO₃ and $6.4 \times 10^{-9} \text{ mol cm}^{-2}_{\text{geo}}$ for La_{0.8}Sr_{0.2}MnO₃. Color codes for the individual contributions: HO₂[−] reduction (magenta), O₂ reduction (blue), HO₂[−] oxidation (green), and total current obtained by the addition of the previously mentioned contributions (black). Currents are calculated per geometric area of the electrode.



The deconvolution of the whole current into individual contributions shows that the kinetic currents of the HO_2^- reduction/oxidation cannot be directly obtained from the total currents, contrary to what has been suggested in the literature.¹⁵

The main difference between the simulated and the experimental curves is the decrease of the HO_2^- oxidation current at high potentials for the former. It is caused by the oxidation of B^{m+} cations (which in our model are required for the adsorption of HO_2^-) into $\text{B}^{(m+1)+}$ cations at high potentials. Various possible explanations may be offered in order to account for the absence of such a current drop in the experiment, among these (i) surface heterogeneity resulting in a wide potential distribution of the $\text{B}^{m+}/\text{B}^{(m+1)+}$ red-ox transitions, (ii) adsorption of HO_2^- on $\text{B}^{(m+1)+}$ sites as well, (iii) carbon contribution to the HPOR at high electrode potentials (see grey curve in Fig. 1).

4. Conclusions

In this work, it is demonstrated that the LaCoO_3 , LaMnO_3 and $\text{La}_{0.8}\text{Sr}_{0.2}\text{MnO}_3$ perovskite oxides, when mixed with carbon, show significant activity towards hydrogen peroxide reduction/oxidation reactions, with LaCoO_3 being less active than Mn perovskites. The kinetics of the hydrogen peroxide oxidation/reduction reactions on perovskite oxides can be reasonably described with a simple kinetic model. Modeling helps to rationalize the observed differences between Co and Mn perovskite oxides in H_2O_2 electrocatalysis, which are largely due to the lower electrocatalytic activity of Co perovskite for the H_2O_2 oxidation and O_2 reduction. Furthermore, it allows one to explain the H_2O_2 concentration dependence (including the displacement of the mixed potential with the concentration) by the multistep mechanism of the hydrogen peroxide reduction. The conclusions obtained have far-reaching consequences for the understanding of the ORR electrocatalysis on oxides of the perovskite family and will be further corroborated in our forthcoming publication.

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