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Fluoroalkyl phosphonic acid radical scavengers for proton exchange membrane fuel cells

Radical attack on perfluorosulfonic acid membranes is detrimental to the long-term durability of proton-exchange membrane fuel cells. The radical scavenging efficiency of state-of-the-art cerium antioxidants is limited by their high mobility. Here, we found that fluoroalkyl phosphonic acids can surpass the radical scavenging activity of cerium without the migration issue. Computational studies confirm the radical scavenging mechanism of fluoroalkyl phosphonic acids in an acidic environment. This study implies that fluoroalkyl phosphonic acid incorporation can improve fuel cell durability for heavy-duty applications.

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Fluoroalkyl phosphonic acid radical scavengers for proton exchange membrane fuel cells†

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Radical-induced degradation of proton exchange membranes limits the durability of proton-exchange membrane fuel cells. Cerium is widely used as a radical scavenger, but the migration of cerium ions to the catalyst layer has been an unresolved issue, reducing its effectiveness over time. Here, we report phosphonic acids as a promising class of radical scavengers, showing competent radical scavenging activity compared to cerium without the migration issue. The *ex situ* Fenton test shows that the fluoride emission rate for Nafion membrane incorporated with fluoroalkyl phosphonic acid ranged from 0.22 to 0.37 $\mu\text{g F cm}^{-2} \text{ h}^{-1}$, lower than that of the cerium-incorporated NafionTM membrane (0.39 $\mu\text{g F cm}^{-2} \text{ h}^{-1}$). The *in situ* open circuit voltage hold test confirmed that a phosphonic acid-incorporated NafionTM membrane has a 58% lower fluoride emission rate compared to the baseline. Density functional theory calculations indicate that the activation energy of the hydroxyl radical scavenging reaction of an alkyl phosphonic acid is only 0.68 eV, suggesting an effective radical scavenging pathway.

Proton exchange membranes (PEMs) transport protons while preventing the diffusion of hydrogen and oxygen between the anode and cathode electrodes. However, the small amounts of gases that cross over through the PEM cause the generation of hydrogen peroxide at the catalyst layers. This peroxide breaks down into radicals that degrade PEMs, leading to the eventual failure of the fuel cell devices.¹ The prominent sites for the attack in perfluorosulfonic acid (PFSA) membranes like that

discussed in this paper include the terminal carboxylic acid groups, ether groups in the side chains, tertiary carbon atoms, and the sulfonic acid C–S bonds.^{2,3} Usually, a radical attack causes the polymer chain to fragment, referred to as the unzipping reaction. Unreacted carboxylic groups in PFSA react with hydroxyl radicals forming CO₂ and HF. This causes the formation of the terminal CF₂ unit. This unzipping proceeds ultimately reaching a side chain which causes loss of the overall side chain.

Attack on the side chain C–S is one of the most important mechanisms of PFSA degradation. Attack of hydroxyl radicals on the terminal R_F–CF₃–SO₃H results in the formation of the R_F–CF₂ radical. This terminal radical then reacts with the hydroxyl radical forming R_F–CF₂–OH. R_F–CF₂–OH reacts with water and results in the subsequent release of HF which causes the formation of –COOH acid groups. Attack on the ether bonds close to the sulfonic acid is perhaps the dominant mechanism of side chain degradation followed by the attack on the tertiary carbon atoms. Attack on the ether bond results in the formation of side group R_F–CF₂–O radicals which react with water causing HF release and carboxylic acid end group. This further unzips the PFSA chain by the mechanism discussed above.

Cerium is widely used as a radical scavenger because of its ability to switch rapidly between oxidation states. Cerium below 0.6 wt% in the PEM reduces voltage degradation by a factor of 20 while reducing the fluoride emission rate (FER) by orders of magnitude over non-modified NafionTM.^{4,5} Because of the highly efficient radical scavenging activity, Toyota Motors implemented the cerium technology into their MIRAI fuel cell vehicles to improve fuel cell durability. Although they are effective radical scavengers, cerium ions tend to migrate through the PEM under fuel cell operating conditions,^{6,7} which reduces the radical scavenging activity over time,⁸ depriving the PEM of the benefits of cerium incorporation.⁹ There are several approaches to stabilizing cerium in the membrane. Zirconium doping reduces the dissolution rate of cerium oxide to enhance cerium stability.^{10,11} Graphene oxides¹² and carbon nanotubes^{13,14} have been used for the durability enhancement of membranes

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samples were subjected to a 0.4 V potential gradient till a total of 2C charge transfer was achieved. This *ex situ* test well simulates the *in situ* migration of cerium during fuel cell operation.²³ For the Ce-NafionTM membrane, the concentration of cerium drastically increased toward the counter electrode (CE) after the migration test (Fig. 2a). The migration of cerium under potential conditions is also evident from the X-ray fluorescence (XRF) line scan (Fig. S4[†]), where the concentration of cerium towards the counter electrode is approximately 3 times higher than that in the part toward the working electrode (WE) at the end of the test. As opposed to cerium, C8 and PFOPA showed uniform distribution before and after the test (Fig. 2b and c). Slight redistribution occurred likely due to an initial non-uniform distribution of phosphonic acid in the as-cast membrane. This could also be due to the relatively high swelling for these membranes and the non-flat nature of the membrane when performing EDX analysis. This test was designed to study the migration of radical scavengers driven by potential gradients and mobility under high humidities and temperatures. Therefore, the minimal migration of phosphonic acids does not mean that they are resistant to migration under all conditions, such as pressure gradients and water fluxes. Nevertheless, the test shows the increased resistance of these non-water-soluble radical scavengers to migration when compared to cerium.

After validating the radical scavenging activity and migration resistance of the phosphonic acids, we examined the *in situ* performance of the PFOPA-incorporated NafionTM using the US Department of Energy (DOE) protocols. The H₂/air fuel cell performance was measured with 5 cm² differential cells after conditioning the membranes in humidified conditions over two days. The performance of the cell using the PFOPA-incorporated

membrane was lower than that of the cell using the Baseline and Ce-NafionTM membranes (Fig. 3a). High-frequency resistance (HFR) is similar for all three membranes ($\sim 0.054 \Omega \text{ cm}^2$) (Fig. S5[†]). Cyclic voltammogram (CV) data suggests that the active sites on Pt(100) were reduced for the cell using the PFOPA-incorporated membrane (Fig. 3b), causing the lower performance of the PFOPA cell.²⁴ It is also to be noted that the capacitance for the PFOPA cell is lower. The observations from CV data are supported by the high Tafel slope and lower mass activity for the cell using the PFOPA-incorporated NafionTM (Fig. 3c). This result indicates that phosphonic acid leaching from the membrane can affect catalyst activity, although the impact on overall performance is not substantial. It is to be noted that our conditioning protocol incorporates break-in of the cell under flooded conditions for large periods of time. This situation can aggravate the migration of immobile species. This is not the situation we simulated in the migration test and is unlikely to be experienced in an operating fuel cell.

Next, we validated the radical scavenging activity of phosphonic acids using the US DOE membrane durability AST protocol which consists of holding the fuel cell at 90 °C at 30% RH under OCV conditions.²⁵ The Baseline cell started to fail after 175 hours in the OCV hold test, but the cells using Ce-NafionTM and PFOPA-NafionTM were stable for more than 200 hours without signs of failure evident (Fig. 3d). The initial H₂ crossover current density of the MEAs using Ce-NafionTM and PFOPA-NafionTM was $\sim 5 \text{ mA cm}^{-2}$, notably higher than that using the baseline MEA ($\sim 1.75 \text{ mA cm}^{-2}$) (Fig. 3e). The higher crossover for the PFOPA membrane could be due to the higher water uptake, unoptimized fabrication process of the MEAs and non-uniformities in the membrane casting process. Fig. 3f

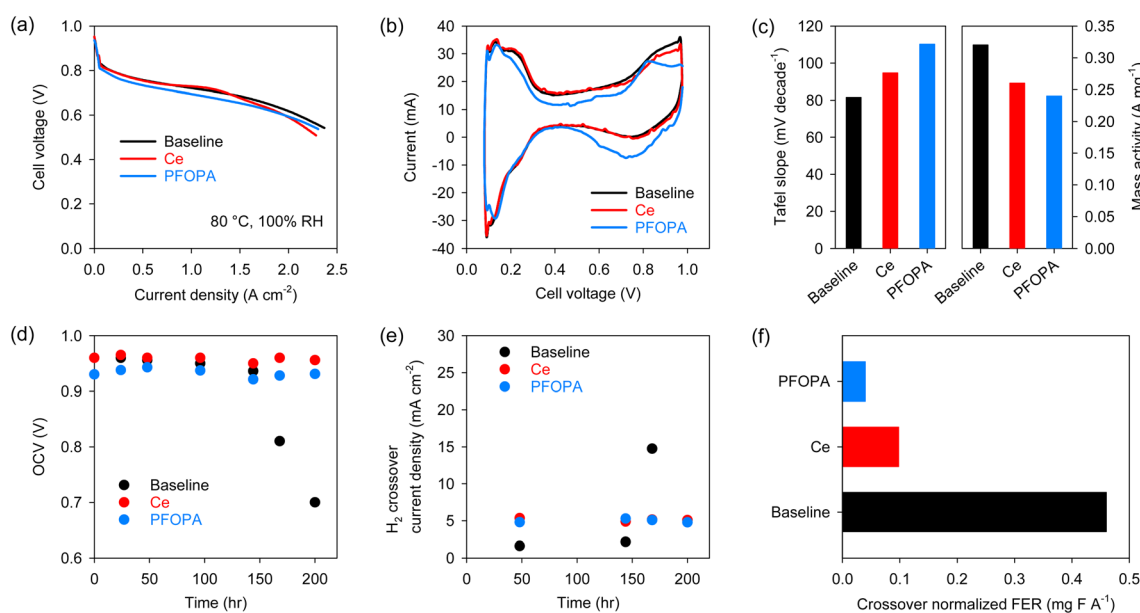


Fig. 3 *In situ* performance of radical scavenger incorporating MEAs: (a) *iR*-corrected polarization curves of the MEAs under H₂/air, at flow rates of 1000 and 3000 sccm on the anode and cathode, respectively, (b) CVs of the MEAs for the Ce and PFOPA incorporating membranes, (c) Tafel slope and mass activity at 0.9 V under H₂/air conditions, (d) OCV and (e) H₂ crossover current density for the MEAs for the Ce and PFOPA incorporating membranes during the chemical durability test, and (f) crossover normalized FER for the MEAs using the Ce and PFOPA incorporating membranes during the chemical durability test.



shows the H_2 crossover normalized FER calculated from the non-normalized total FER emissions during the stable OCV operation of different membranes. The H_2 crossover normalized FER of the PFOPA-NafionTM membrane was 0.04 mg F A^{-1} , which is 58% lower than that of the Ce-NafionTM membrane for the same duration, confirming the stronger radical scavenging activity of phosphonic acids compared to cerium. Even with

a higher crossover, the total FER for the PFOPA membrane is lower than for the Ce membrane (Fig. S6[†]). The FER trend from Fenton's test and OCV hold test differ considerably, corroborating the long-held belief that Fenton's test may not be an accurate predictor for membrane degradation under fuel cell operating conditions.

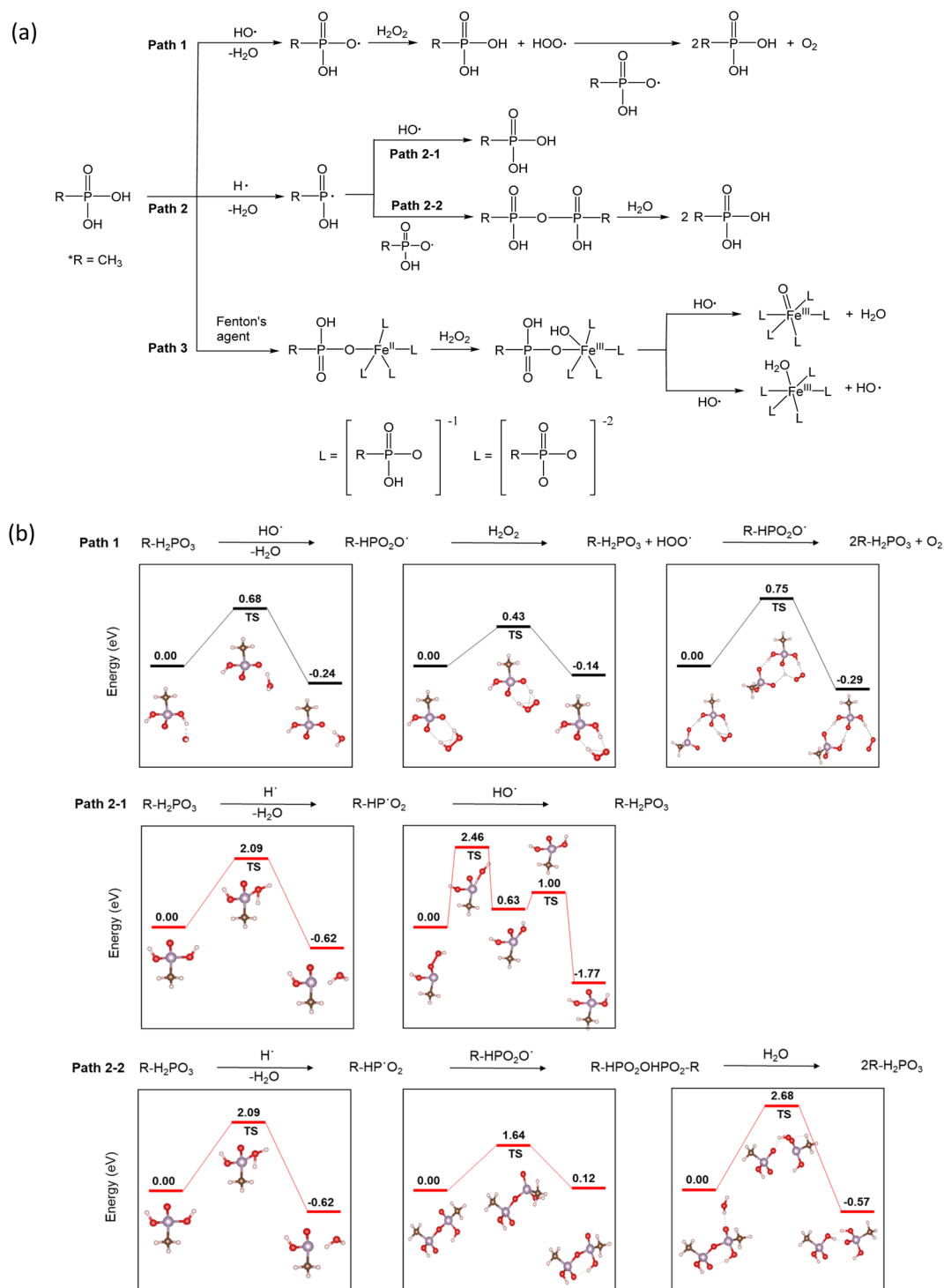


Fig. 4 Proposed radical scavenging mechanisms of phosphonic acids: (a) three reaction pathways, (b) reaction activation energy of Path 1 and Path 2.



