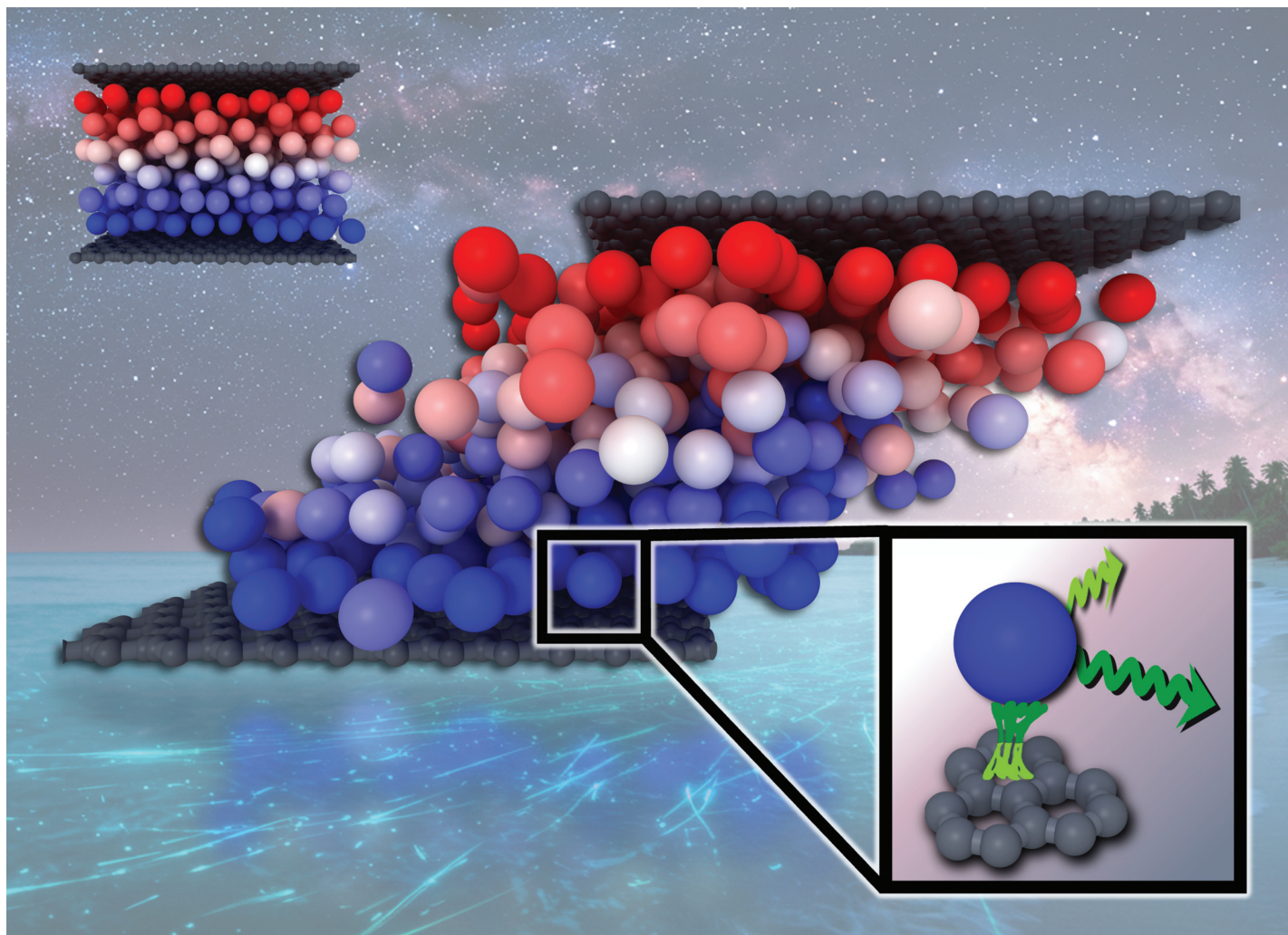




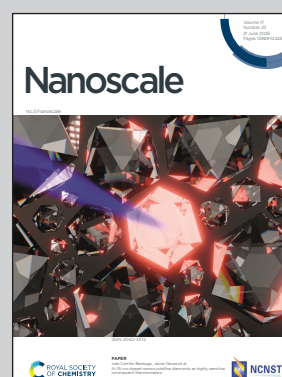
Showcasing research from Prof. Gerald J. Wang's group,
Department of Civil and Environmental Engineering,
Carnegie Mellon University, Pittsburgh, United States.

Revealing nanoscale slip within Taylor-Aris dispersion

A method to estimate interfacial slip velocity from Taylor-Aris dispersion in a plane-Couette flow has been developed. This method leverages the anisotropic fluid self-diffusion in streamwise and spanwise directions due to shear, and has been validated through extensive molecular simulations.

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Revealing nanoscale slip within Taylor–Aris dispersion†

Mehul Bapat and Gerald J. Wang *

Hydrodynamic slip at fluid–solid interfaces plays an important role in a range of transport phenomena, especially in fluids under small-scale confinement. Much work has studied the microscopic origins of slip. In this work, we explore the connection between the microscopic slip velocity and the macroscopic (slip-adjusted) Taylor–Aris dispersion in the fluid, which enables the former to be written in terms of the latter. Through extensive molecular-dynamics simulations of simple and polymeric fluids under a wide range of thermodynamic and geometric conditions, we show that the continuum treatment of Taylor–Aris dispersion can be readily extended to systems where the confining length-scale is comparable to the slip length. We further demonstrate that slip velocity can be accurately inferred through measurements of equilibrium and shear-augmented molecular self-diffusivities.

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1 Introduction

The continuum treatment of fluids frequently presumes zero hydrodynamic slip at a fluid–solid interface (the no-slip

boundary condition). However, non-zero slip at fluid–solid interfaces can play an important role in transport phenomena at interfaces^{1,2} and under confinement, especially in systems where a confining length-scale is comparable to the slip length.³

Owing to the fact that slip is intrinsically a microscopic phenomenon, a significant body of work using both experiments and molecular-dynamics (MD) simulations has sought to characterize the microscopic mechanisms underlying slip, as reviewed in previous work.^{4,5} Many studies have investigated the microscopic kinetics of slip within the broad (and inter-related) frameworks of thermally activated rate processes,^{6,7} molecular-kinetic theory,^{8–11} and biased Brownian motion.¹² Slip has been studied in relation to microscopic friction at the fluid–solid interface^{13–16} and also as a function of microscopic roughness and surface texture.^{17,18} All of the aforementioned work focuses on relating the slip phenomenon with microscopic aspects of the system, with no explicit connection to macroscopic fluid mechanics.

In contrast, a distinct body of work on slip explores its connections with continuum-scale descriptions of a fluid. Several studies have explored slip within the framework of continuum fluid mechanics; these studies infuse microscopic details into a fundamentally macroscopic picture *via*, *e.g.*, a corrugated potential energy landscape representative of the boundary.^{19,20} Hsu and Patankar²¹ demonstrated that the relationship between slip and fluid shear rate (supported both by molecular-scale simulations and experiments) can be qualitatively recovered using a continuum treatment of a compressible fluid in the presence of a wall that imposes a potential on the fluid.

The present work follows in the spirit of the latter by studying the validity of (appropriately interpreted) continuum

Department of Civil and Environmental Engineering, Carnegie Mellon University, Pittsburgh, PA 15213, USA. E-mail: gjwang@cmu.edu

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Gerald J. Wang

Gerald “Jerry” Wang is an Assistant Professor of Civil and Environmental Engineering, and Chemical Engineering (by courtesy) and Mechanical Engineering (by courtesy), at Carnegie Mellon University. He received his BS from Yale University (Mechanical Engineering, Mathematics and Physics), SM from MIT (Mechanical Engineering), and PhD from MIT (Mechanical Engineering and Computation).

He was a postdoctoral researcher at MIT in Chemical Engineering and is an EIT in Electrical and Computer Engineering. At CMU, Jerry directs the M5 Lab, which focuses on computational small-scale mechanics of fluids, soft matter, and active matter, with applications across energy, food, sustainable materials, and urban livability.



theory in the limit of small confining length-scales. In particular, we address the following question: “Does the continuum theory of Taylor–Aris dispersion describe the relationship between shear rate and shear-enhanced diffusivity in a nanoscale channel with non-negligible hydrodynamic slip?” We answer this question in the affirmative, and show as a consequence that the classical theory can be inverted to infer details about slip using only measurements of diffusivity. The closest related work²² to that carried out here presents purely classical results (both analytical and numerical, *via* finite volumes) for the relationship between dispersion and slip; our focus here is on seamlessly extending the classical theory to channels of nanoscale dimension, validated using molecular simulations.

In the following section, we model slip velocity in terms of equilibrium and shear-augmented diffusivities in plane-Couette flow. We describe our numerical experiments in section 3 (and Appendix A), with results discussed in section 4, followed by concluding remarks and future directions in section 5.

2 Theory: Taylor–Aris dispersion in the presence of hydrodynamic slip at the fluid–solid interface

Consider the schematic for plane-Couette flow shown in Fig. 1a, with fluid sheared by two solid walls moving opposite to each other along the x -direction (the streamwise direction) with equal speeds u_w . The walls, separated by a gap height H in the z -direction (the wall-normal direction) and of infinite extent in the y -direction (the spanwise direction) and the x -direction, are identical in microstructure, yielding equal slip

velocity u_s at both interfaces. The steady and fully-developed streamwise fluid velocity with slip boundary conditions is:

$$u(z) = (u_w - u_s) \left(\frac{2z}{H} - 1 \right). \quad (1)$$

Following the classic arguments by Aris and Taylor,^{23,24} and assuming no slip, the ratio of the shear-augmented (effective) diffusivity D_{eff} to the equilibrium diffusivity D_{eq} (diffusivity in a non-sheared direction) is:

$$\frac{D_{\text{eff}}}{D_{\text{eq}}} = 1 + \frac{u_w^2 H^2}{30 D_{\text{eq}}^2}. \quad (2)$$

In the slip case, since the fluid velocity at the boundaries has magnitude $u_w - u_s$, this ratio is:

$$\frac{D_{\text{eff}}}{D_{\text{eq}}} = 1 + \frac{(u_w - u_s)^2 H^2}{30 D_{\text{eq}}^2}. \quad (3)$$

An extended discussion of eqn (2) and (3) is presented in the ESI.†

The core premise of this work is the observation that eqn (3) establishes a connection between the slip velocity and the extent to which the diffusivity is enhanced by shear. In particular, eqn (3) can be inverted to obtain slip velocity in terms of the equilibrium and shear-augmented diffusivities:

$$u_s = u_w - u_D, \quad (4)$$

where

$$u_D \equiv \sqrt{\frac{30 D_{\text{eq}}^2 (D_{\text{eff}}/D_{\text{eq}} - 1)}{H^2}}. \quad (5)$$

Here, u_D can be physically interpreted as the interfacial fluid velocity, *i.e.*, $u_D = |u(z=0)| = |u(z=H)|$. It is worth emphasizing that eqn (5) constructs a velocity-scale using only diffu-

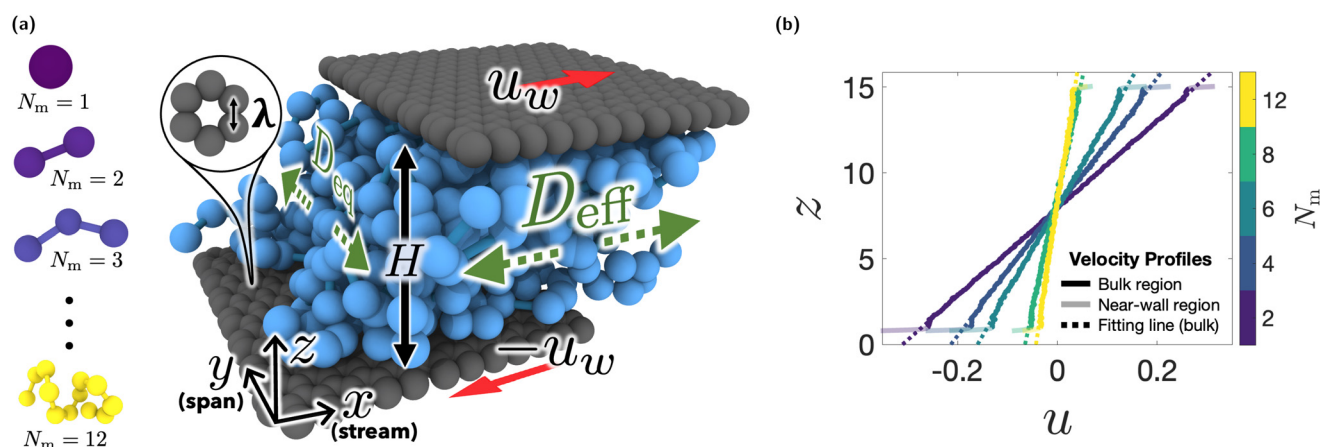
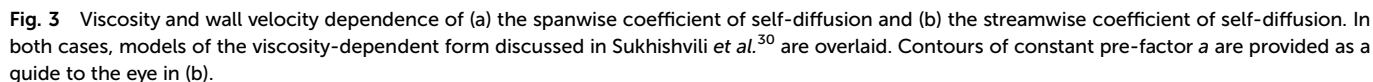
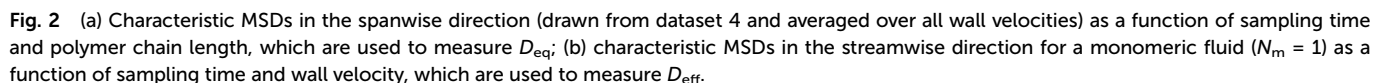


Fig. 1 (a) Schematic of simulated plane-Couette flow for a fluid (LJ chains with $N_m = 5$) confined by two identical graphene walls with nearest-neighbor distance λ and gap height H and fluid self-diffusion coefficient in the streamwise direction D_{eff} and spanwise direction D_{eq} . Fluids with different chain lengths simulated in this study are shown on the left. (b) Steady-state fluid velocity profiles at $u_w = 0.74$ for LJ chains drawn from dataset 4 (Table 1). Linear fits to velocity profiles are performed in the bulk region and are extrapolated to the wall locations to calculate slip velocity. All quantities are non-dimensionalized as discussed in section 3.





velocity profile to the wall location. We find agreement within 2.3% mean absolute error, with no systematic discrepancies as a function of any of the parameters varied. These results confirm the hypothesis that the slip velocity can in fact be inferred from the streamwise-spanwise diffusivity difference *via* inversion of (slip-adjusted) Taylor–Aris dispersion.

This is an intriguing result for several reasons. Despite Taylor–Aris dispersion following from a continuum description of a fluid, this theory – when applied to molecular self-diffusivities – extends seamlessly to channels of nanoscale dimension, provided that the relevant shear rates are adjusted for slip; this result follows a pattern of macroscopic fluid-mechanical phenomena that can be observed in systems of nanoscale dimension, despite the continuum laws not being obviously applicable in such systems.⁴ Moreover, this result provides a new route by which one can determine the boundary condition

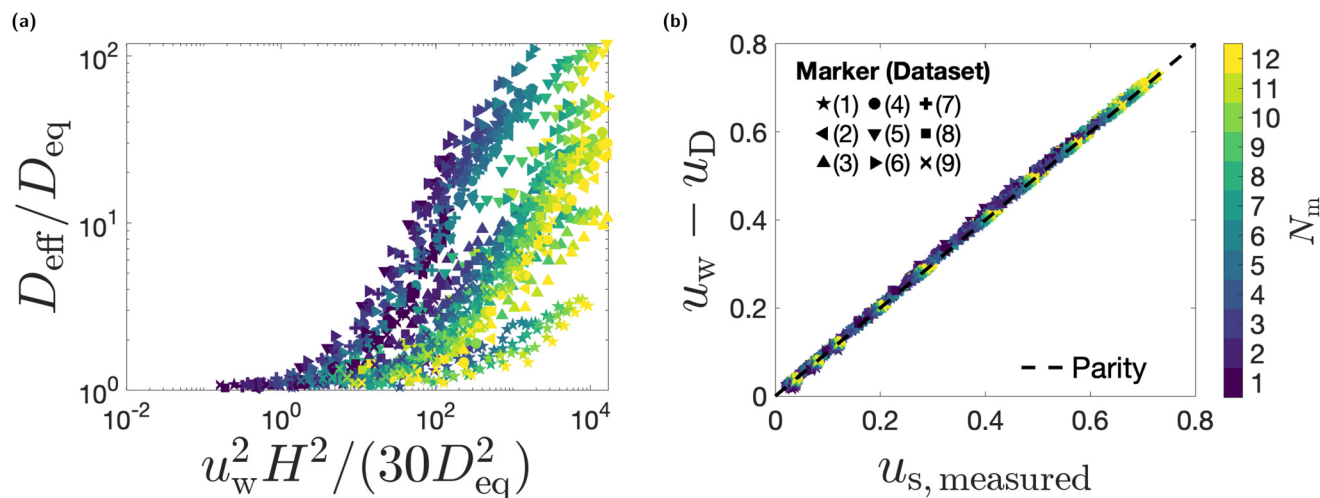


Fig. 4 (a) Normalized shear-augmented coefficient of self-diffusion vs. linear term in eqn (2); (b) slip velocity inferred via Taylor-Aris dispersion eqn (4) vs. slip velocity measured by extrapolation of fluid velocity profile to boundary (dashed line of parity overlaid).

(slip velocity) that is consistent with the bulk flow, which makes exclusive use of measurements of fluid diffusivity.

5 Conclusions

In this work, we investigated the connection between hydrodynamic slip at a fluid-solid boundary and Taylor-Aris dispersion in a confined fluid, leading to the relationship in eqn (4) and (5), between the slip velocity, the spanwise diffusivity, and the streamwise diffusivity. We performed MD simulations of plane-Couette flow for a wide range of fluids (simple fluids and polymers of varying length) under a wide range of thermodynamic and geometric conditions, and we observed that (slip-adjusted) Taylor-Aris dispersion accurately captures shear-augmented diffusivity in fluids under small-scale confinement. We further found excellent agreement between the slip velocity inferred from dispersion (using the streamwise-spanwise diffusivity difference) and the slip velocity measured using an approach traditional in MD simulations (using the fluid velocity profile extrapolated to the boundaries).

These results motivate several natural extensions. One such extension would be to assess the accuracy of this theory for a fluid mixture (comparing against, *e.g.*, Zhou *et al.*³¹) or for fluid bounded by rough or patchy walls.¹⁷ The smallest channel studied in this work still has a majority of fluid in its bulk region, in which interfacial effects – especially fluid layering^{32,33} – are negligible. The question of whether the present dispersion model can be adapted to yet-smaller channels, in which surface-driven effects play a significant role in diffusion in all directions,³⁴ remains open. Fig. 4b establishes strong agreement between two distinct approaches for measuring slip velocity, at the level of means; an intriguing direction of further study would be comparison at higher moments and for the full distributions of measured slip velocities (*e.g.*, at the level of variances in the slip velocity). Such work could have

important implications for the uncertainty quantification of slip in small-scale channels within MD simulations. Finally, we note that eqn (4) is but one example of using Taylor-Aris dispersion to formulate a nanoscale hydrodynamic quantity in terms of anisotropic diffusivities. It would be especially interesting to see whether this treatment extends to other related quantities (*e.g.*, the fluid-solid friction coefficient).

Data availability

Data for this article, including scripts to generate the MD simulations described in section 3, are available at <https://github.com/M5-Lab/NanoscaleTaylorAris>.

Conflicts of interest

The authors report no conflict of interest.

Appendix A: details of MD simulations

Each system consists of a homogeneous fluid with number density $\rho = 0.85$ (based upon number of monomers), confined by two identical graphene walls that are squares with a side length of 9.52. A cutoff radius of 3.17 was used for all simulations. Apart from the non-bonded LJ interactions in eqn (9), intra-chain interactions in polymeric fluids are governed by: (a) a harmonic potential $U_{\text{bond}}(r)$ for particles directly bonded to each other and separated by a distance r , given by $U_{\text{bond}}(r) = (k_{\text{bond}}/2)(r - r_0)^2$, with bond constant $k_{\text{bond}} = 72.0$ and equilibrium bond length $r_0 = 2^{1/6}$ (same as equilibrium distance between two non-bonded fluid particles); (b) a harmonic potential for two consecutive bonds forming an angle θ , given by $U_{\text{angle}}(\theta) = (k_{\text{angle}}/2)(\theta - \theta_0)^2$, with angle constant $k_{\text{angle}} =$



66.7 and equilibrium bond angle $\theta_0 = 110^\circ$; and (c) CHARMM-style dihedral interactions³⁵ for sets of four contiguously bonded particles in the same chain with dihedral angle ϕ , given by $U_{\text{dihedral}}(\phi) = k_{\text{dh}}(1 + \cos(\phi + \alpha_{\text{dh}}))$, with dihedral coefficients $k_{\text{dh}} = -18.67$ and $\alpha_{\text{dh}} = 7^\circ$. The structures of different fluids and solids were generated using the software Moltemplate³⁶ and visualizations were rendered using the Open Visualization Tool (OVITO).³⁷ To counter the effects of viscous heating due to shear, the temperature of the fluid was maintained *via* a Nosé–Hoover (NH) thermostat,^{38,39} we verified that the core Taylor–Aris dispersion result (Fig. 4b) is unaffected by choice of thermostat or choice of thermostat damping timescale (see ESI†). We measure viscosity of the fluid using $\mu = \tau_{xz}/\dot{\gamma}$, where τ_{xz} is the magnitude of the shear stress imposed by the walls on the fluid in the streamwise direction and $\dot{\gamma}$ is the fluid shear rate. τ_{xz} is obtained by evaluating the time-average of the difference of forces applied by the top and bottom walls on the fluid in the streamwise direction, normalized by the wall area.

Appendix B: limits of validity for system-center-of-mass-corrected diffusivity

For the purpose of evaluating eqn (6), mean-squared displacements are computed in a single reference frame with no net center-of-mass motion. In an MD simulation, this reference frame can be established by computing the average velocity for all particles in the system. For a plane-Couette flow (with the origin of velocity at the channel midline, as shown in Fig. 1a), this frame should simply be the laboratory frame, by symmetry.

It is worth emphasizing that there are limits of validity to choosing a single reference frame. In particular, this choice is only justified if particles are tracked over a sampling time sufficiently long that all particles may sample velocities throughout the channel ($t_{\text{sample}} \sim \mathcal{O}(H^2/D_{\text{eq}})$), a critical assumption of the Taylor–Aris theory. On this timescale, for a plane-Couette flow, each individual particle has an expected velocity of the channel midline velocity, *i.e.*, the velocity of the single reference frame described above.

Since any fluid particle not at the channel midline locally has a non-zero expected velocity (given by eqn (1)), it is important to note that when $t_{\text{sample}} \ll \mathcal{O}(H^2/D_{\text{eq}})$, many individual particles will have only sampled a subset of velocities. If the MSD of these particles is tracked with the single choice of reference frame described above, then this MSD will grow quadratically with time, as would be expected for ballistic transport; indeed, a slight quadratic “knee” can be observed to the far left of Fig. 2b. In all MD simulations reported, sampling is performed through at least $\mathcal{O}(H^2/D_{\text{eq}})$.

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