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Zirconium-metal–organic framework@activated carbon composites for prevention of secondary emission of nerve agents†

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We have studied the formation of core–shell hybrid metal–organic framework@activated carbon sphere (MOF@AC) adsorbents, by means of a layer-by-layer (LBL) growth method of MOFs on shaped AC materials. The hybrid MOF@AC materials are useful for preventing the secondary emission problems of chemical warfare agent protective filters. Mesopores on AC materials facilitate carbon surface oxidation and a subsequent MOF growth, allowing $Zr_6O_4(OH)_4(\text{benzene-1,4-dicarboxylate-2-X})_6$ ($X = \text{H}$, UiO-66; $X = \text{NH}_2$, UiO-66-NH₂) thin film formation. By contrast, microporous spheres do not allow a significant MOF layer growth. The MOF@AC hybrids are able to capture the G-type nerve agent surrogate, diisopropylfluorophosphate (DIFP), and quantitatively hydrolyse a P–F bond, within 24 h at room temperature, to yield non-toxic diisopropylphosphate (DIP) in unbuffered moist media. Neither the MOF nor the carbon spheres alone can hydrolyse the model toxic compound to that extent. The enhanced performance of the MOF@AC composites is attributed to a synergistic interplay of the hydrolytic degradation of DIFP at the MOF layer and the physisorption of DIP at the carbon pore structure, allowing the regeneration of the MOF catalytic sites.

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Introduction

Organophosphorus-based pesticides and chemical warfare nerve agents (CWAs) are extremely toxic compounds^{1,2} due to their ease to penetrate tissues and the labile nature of P–X bonds ($X = \text{O}, \text{F}, \text{S}$). They irreversibly bind to the active site of acetylcholinesterase (AChE) inhibiting its function and causing concomitant damage to the central nervous system.^{3–5} The thread of destabilizing groups using nerve agents^{6–8} has created the need for efficient technologies to detoxify this kind of harmful compounds. One of the most widespread approaches to avoid CWA exposure is the use of adsorbents to build filtering systems able to selectively capture these toxic molecules.⁹ The adsorbents of choice are activated carbon (AC) based adsorbents because of their large surface area, hydrophobicity and tunable porosity and surface area.^{10,11} Thanks to their easy-shaping as spheres and textile fibers, they are extensively used as chemical barrier masks and clothing for military and civilian purposes.¹² However, the physisorptive nature of AC-based

protective adsorbents leads to contaminated filter materials that can potentially leak the contaminant (secondary emission) and consequently need to be destroyed after exposure to toxic molecules.^{13–16}

In this regard, zirconium metal–organic frameworks (MOFs) combine Lewis acidic metal centers and basic/nucleophilic sites which render them hydrolytic catalysts for the decontamination of chemical warfare agents.^{17–22} However, as MOF materials are usually obtained in a powder form, they need to be shaped to allow their integration into protective systems.^{23–26} Moreover, many MOF catalysts become poisoned by organophosphate degradation products, needing the addition of amine basic buffered media to allow detoxification to progress^{27–30} and therefore have a low real applicability. In a previous study, we investigated the thin film growth of prototypical zirconium MOF UiO-66 on H₂O₂ oxidized shaped activated carbon.¹³ However, the resulting materials exhibited a poor ability to hydrolyse the G-type nerve agent model diisopropylfluorophosphate (DIFP), as a consequence of the strong competition with the physisorption process at the hydrophobic activated carbon pore structure.

In this work, we have carried out a comprehensive study on the impact of the pore structure of activated carbon spheres (microporous vs. mesoporous) and surface oxidants (H₂O₂, HNO₃, and (NH₄)₂S₂O₈) on the growth of $Zr_6O_4(OH)_4(\text{benzene-1,4-dicarboxylate-2-X})_6$ ($X = \text{H}$, UiO-66; $X = \text{NH}_2$,

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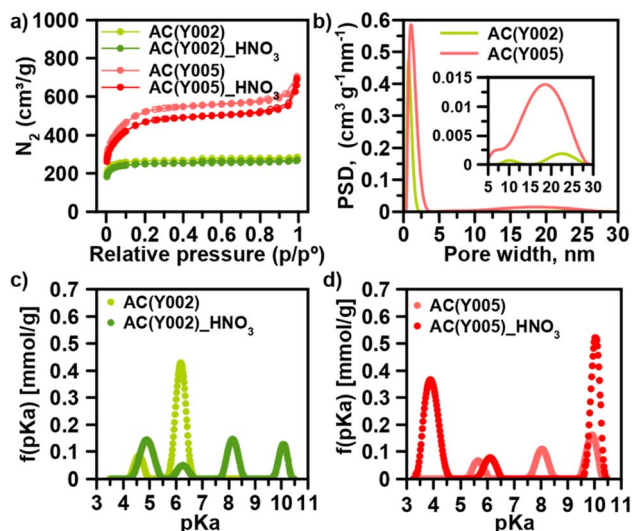


Fig. 1 Impact of HNO₃ oxidation on the pore surface of two representative microporous AC(Y002) and mesoporous AC(Y005) activated carbon spheres. (a) N₂ adsorption isotherms at 77 K. (b) Pore size distribution (inset: range extension between 5 and 30 nm). Distribution of acidity constants for (c) AC(Y002) and (d) AC(Y005) spheres before and after HNO₃ oxidation.

UiO-66-NH₂) thin films to yield core-shell hybrid metal-organic framework@activated carbon spheres (MOF@AC). This was performed to assess the suitability of the hybrid adsorbents to prevent secondary emission problems of chemical warfare agent protective filters. The results show a synergistic interplay between physisorption at the mesoporous carbon spheres and hydrolytic catalysis at the MOF

thin layer advancing the CWA detoxification process in unbuffered moist media.

Results and discussion

Oxidation and functionalization of activated carbon spheres

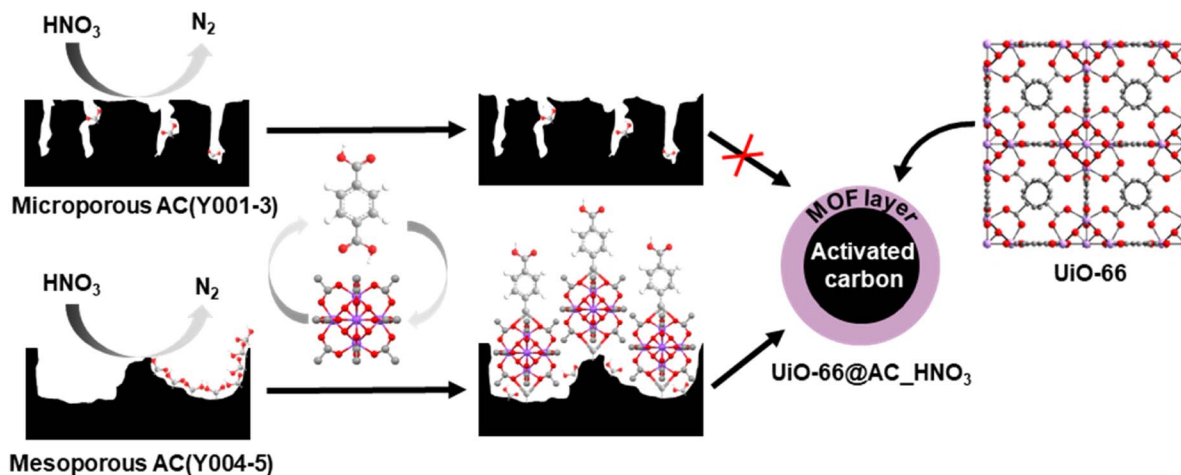
We have selected a set of activated carbon spheres, provided by Blücher company, ranging from microporous AC(Y001–Y003) to micro-/mesoporous AC(Y004 and Y005) (Fig. 1a, b, S1, S2† and Table 1) in order to study the impact of the pore structure on their functionalization and ulterior growth of MOF thin films. In the first step, we selected the micro-/mesoporous activated carbon spheres AC(Y005) to screen optimal surface functionalization conditions with different oxidants (H₂O₂, HNO₃ and (NH₄)₂S₂O₈) to provide oxygenated anchoring sites for the MOF thin film layer growth (Scheme 1).¹³ N₂ adsorption was indicative of a diminution of the surface area after oxidation following the trend H₂O₂ (3.5%) < HNO₃ (9.6%) < (NH₄)₂S₂O₈ (15.4%) (Fig. 1a, S3 and Table S1†). The X-ray photoelectron spectroscopy (XPS) analysis confirmed an increase in the oxygen concentration on the sphere surface, being more noticeable after the HNO₃ and (NH₄)₂S₂O₈ treatment (Fig. S4†). In the second step, we carried out an ulterior treatment of the oxidized activated carbon spheres with urea and thiourea, at 450 °C for 30 min under a N₂ atmosphere, to explore the impact of the introduction of nitrogen and sulphur groups onto the oxidized carbon surface. XPS analysis demonstrated a clear increase in the surface nitrogen content as well as a decrease in the surface oxygen content (Fig. S5†). Moreover, for the thiourea treated AC spheres, N₂ adsorption was indicative of a marked decrease in pore accessibility with a 40% loss of the specific BET surface area (Fig. S3 and Table S1†).

Table 1 Summary of properties of carbon spheres, UiO-66(-NH₂) and UiO-66(-NH₂)@AC composites

Material	Particle size (μm)	S _{BET} (m ² g ⁻¹)	Pore size (nm)	pK _a ^a (mmol g ⁻¹)	% DIFP degradation (24 h)
AC(Y001)	170	1460	0.9	5.03 (0.210), 8.65 (0.050), and 9.80 (0.005)	18.7
AC(Y001)_HNO ₃	170	1100	0.7	4.55 (0.224), 6.20 (0.012), 7.62 (0.032), and 10.13 (0.130)	24.1
AC(Y002)	470	790	0.7	4.60 (0.030) and 6.18 (0.200)	17.1
AC(Y002)_HNO ₃	470	770	0.7	4.90 (0.089), 6.21 (0.025), 8.14 (0.071), and 10.11 (0.050)	48.5
AC(Y003)	470	1260	0.9	5.09 (0.114), 8.06 (0.045), and 9.72 (0.050)	1.2
AC(Y003)_HNO ₃	470	1180	0.8, 1.3	4.90 (0.089), 6.3 (0.022), 8.14 (0.075), and 10.11 (0.050)	9.6
AC(Y004)	390	1740	1.1, 16	6.05 (0.055), 8.40 (0.080), and 9.92 (0.074)	30.9
AC(Y004)_HNO ₃	390	1485	0.8, 1.3, 17	4.91 (0.089), 6.30 (0.022), 8.18 (0.075), and 10.11 (0.050)	23.9
AC(Y005)	475	1720	1.1, 18	5.65 (0.030), 8.05 (0.058), and 9.90 (0.068)	15.6
AC(Y005)_HNO ₃	475	1555	1.0, 17	3.89 (0.238), 6.16 (0.041), and 10.08 (0.214)	9.2
UiO-66 LBL	0.2	1155	1, 1.9, 2.3, 4–15	4.02 (0.157) and 8.57 (3.56)	25.5
UiO-66-NH ₂ LBL	0.3	910	1, 1.9, 2.3, 4–15	4.3 (0.609) and 8.79 (2.27)	24.1
UiO-66@AC(Y004)_HNO ₃	390	1400	1.0, 21.1	4.84 (0.023), 8.25 (0.0225), and 10.14 (0.900)	80.7
UiO-66-NH ₂ @AC(Y004)_HNO ₃	390	1320	1.0, 18.0	4.2 (0.072), 8.3 (0.364), and 10.10 (0.390)	93.9
UiO-66@AC(Y005)_HNO ₃	475	1240	1.0, 19.0	5.74 (0.015), 7.93 (0.050), and 10.10 (0.163)	89.1
UiO-66-NH ₂ @AC(Y005)_HNO ₃	475	1295	1.0, 21	4.06 (0.095), 6.87 (0.012), and 9.81 (0.070)	97.5

^a Amounts of groups associated with each pK_a value.





Scheme 1 Surface oxidation of microporous (top) and mesoporous (bottom) activated carbon spheres followed by layer-by-layer growth of UiO-66 thin films. Color code: oxygen, red; hydrogen, white; zirconium, purple; and carbon, grey.

Based on this initial screening, HNO_3 oxidation was selected as the optimal treatment for surface functionalization of the microporous AC(Y001–003) and micro-/mesoporous AC(Y004–005) carbon spheres (Table 1). N_2 adsorption isotherms indicate that the overall porosity is only slightly modified after the oxidation process (Fig. S6†). Microporous AC(Y002) $_{\text{HNO}_3}$ and AC(Y003) $_{\text{HNO}_3}$ carbon spheres (diameter 470 μm) exhibit a minor surface area loss of 3–6% while the smaller sphere AC(Y001) $_{\text{HNO}_3}$ (diameter 170 μm), with a 25% loss of the surface area, seems to be more sensitive to the oxidative treatment (Tables 1, S2 and Fig. S6†). The mesoporous spheres AC(Y004) $_{\text{HNO}_3}$ (390 μm) and AC(Y005) $_{\text{HNO}_3}$ (475 μm) exhibit a larger surface area loss (10–16%) upon the HNO_3 treatment than microporous spheres of a similar size AC(Y002–3) $_{\text{HNO}_3}$ indicating a higher reactivity of the mesopores. The acid–base titration results (Fig. S7–S10†) clearly show an increase in acidity upon the HNO_3 treatment, as expected (Tables 1 and S5†). Oxidized mesoporous AC(Y004) $_{\text{HNO}_3}$ and AC(Y005) $_{\text{HNO}_3}$ are more acidic than their microporous counterparts. This is especially seen in the acidic pH region of the acid–base titration curve of AC(Y005) $_{\text{HNO}_3}$, which exhibits a high amount of carboxylic groups ($\text{p}K_{\text{a}} < 4$), compared to oxidized microporous AC(Y002) $_{\text{HNO}_3}$ (Fig. 1c and d). These carboxylic groups are very important as seeds for the MOF crystal growth (see below).

Layer by layer growth of MOF on activated carbon spheres

Upon detailed characterization of the functionalised activated carbon spheres, we have studied the impact of their surface functionalities on the growth of thin films of the prototypical UiO-66($-\text{NH}_2$) MOFs by means of the layer-by-layer (LBL) synthesis.¹³ The LBL MOF growth consisted of the successive immersion of the AC(Y00*n*) $_{\text{HNO}_3}$ ($n = 1$ –5) spheres in dimethylformamide (DMF)/acetic acid (AcOH) solutions of the oxyhydroxide metal cluster $[\text{Zr}_6\text{O}_4(\text{OH})_4(\text{AcO})_{12}]$ for 15 minutes at 130 $^\circ\text{C}$ followed by washing with DMF and immersion in a DMF

solution of the organic linker benzene-1,4-dicarboxylic acid (H_2bdc) or benzene-2-amino-1,4-dicarboxylic acid ($\text{H}_2\text{bdc}-\text{NH}_2$) for 15 minutes at 130 $^\circ\text{C}$. The general process for UiO-66($-\text{NH}_2$)@AC(Y00*n*) $_{\text{HNO}_3}$ ($n = 1$ –5) hybrid materials ends after 12 synthetic immersion cycles according to Scheme 1

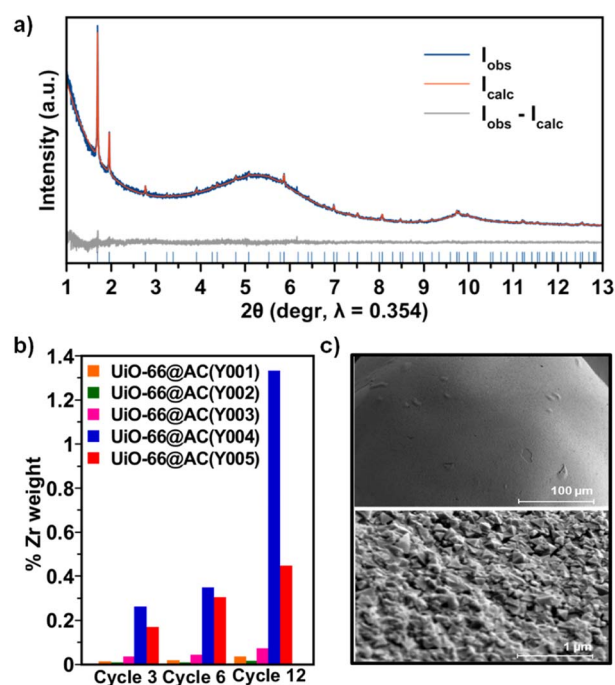


Fig. 2 (a) Graphical result of the whole powder pattern refinement carried out with the Le Bail method ($R_{\text{p}} = 0.022$; $R_{\text{wp}} = 0.019$) on the HR-PXRD of as-synthesized UiO-66@AC(Y004) $_{\text{HNO}_3}$ in terms of observed, calculated and difference traces (blue, red and grey, respectively). The positions of the Bragg reflection are indicated by blue ticks. Cell parameters: $a = b = c$ 20.8288 (3) \AA , $V = 9036.4$ (3) \AA^3 ; (b) inductively coupled plasma analysis of Zr percentage in UiO-66@AC(Y00*n*) $_{\text{HNO}_3}$ ($n = 1$ –5) composites throughout different synthetic cycles; (c) SEM images of UiO-66@AC(Y004) $_{\text{HNO}_3}$.



(experimental details in the ESI†). The LBL growth process was followed by a powder X-ray diffraction (PXRD), Fourier transform infrared spectroscopy (FTIR), inductively coupled plasma-mass spectrometry (ICP-MS), acid–base titration, thermogravimetric analysis (TGA) and N_2 adsorption–desorption experiments at 77 K (Fig. 2a, b, S11–S16, Tables 1, S2 and S3†). High resolution-powder X-ray diffraction (HR-PXRD) measurements on $UiO-66(-NH_2)@AC(Y00n)_HNO_3$ ($n = 4, 5$) acquired at European Synchrotron Radiation Facility Beam line ID-22^{31,32} of hybrid materials unequivocally confirm the formation of crystalline pure phase $UiO-66(-NH_2)$ thin films (Fig. 2a and S17–S20†). Structureless Le Bail refinement indicates that positions and intensity of the Bragg reflection peaks and cell parameters: $a = b = c$ 20.8288 (3) Å and $V = 9036.4$ (3) Å³ are in agreement with the formation of crystalline pure phase $UiO-66(-NH_2)$ thin films on the surface of the activated carbon spheres. The high background of the pattern is characteristic of the amorphous nature of the activated carbon spheres. ICP-MS analysis clearly shows an appreciable increase in a % Zr weight (and therefore of $UiO-66$) in $AC(Y004-5)_HNO_3$ throughout different synthetic cycles (Fig. 2b). In fact, a total amount of 3.96 wt% and 1.04 wt% of $UiO-66$ was introduced to $UiO-66@AC(Y004)_HNO_3$ and $UiO-66@AC(Y005)_HNO_3$ composites, respectively (Table S3†). In addition, we also managed to synthesize $UiO-66-NH_2@AC$ composites reaching around 3 wt% of MOF on mesoporous $AC(Y004)_HNO_3$ and $AC(Y005)_HNO_3$ spheres (Fig. S21–27, Tables S3 and S4†). Neither microporous $AC(Y00n)_HNO_3$ ($n = 1-3$) nor pristine $AC(Y004)$ and $AC(Y005)$ give rise to the formation of a $UiO-66(-NH_2)$ thin layer (Fig. S38†). These results indicate that only the oxidized mesoporous spheres $AC(Y004-5)_HNO_3$ give rise to the formation of a MOF crystalline thin layer. We attribute this behaviour to the formation of carboxylic residues at the accessible mesoporous surface (see above) that allows zirconiumoxyhydroxide metal cluster anchoring and resulting a MOF thin layer in $UiO-66(-NH_2)@AC(Y004-5)_HNO_3$ hybrid materials. Scanning electron microscopy (SEM-EDX) images of the $UiO-66(-NH_2)@AC(Y004-5)_HNO_3$ hybrid materials proved the formation of a rather homogeneous MOF layer of octahedral microcrystals covering the AC spheres' surface (Fig. 2c, and S28–S31†). Moreover, the growth of the $UiO-66$ or $UiO-66-NH_2$ thin film layer does not hamper access to the carbon sphere pore structure, although a slight decrease in the N_2 uptake upon MOF growth is noticed (Tables 1, S2, S4, Fig. S12 and S22, †). This result is in agreement with the smaller surface area of $UiO-66$ ($1155\text{ m}^2\text{ g}^{-1}$) and $UiO-66-NH_2$ ($910\text{ m}^2\text{ g}^{-1}$) in comparison to that of the mesoporous carbon spheres, as well as with the possible incorporation of organic linkers (H_2bdc or $H_2bdc-NH_2$) into the pores of the hybrid material. The latter hypothesis was demonstrated by performing a vigorous DMF wash of the $UiO-66@AC(Y005)_HNO_3$ composite (see the ESI†), with the BET surface area of the hybrid material increasing from $1240\text{ m}^2\text{ g}^{-1}$ to $1525\text{ m}^2\text{ g}^{-1}$, similar to that of the oxidized carbon spheres ($1555\text{ m}^2\text{ g}^{-1}$) (Fig. S32†). For comparative reasons, we also synthesized and characterized $UiO-66(-NH_2)$ materials using the same conditions as for LBL synthesis terming these materials $UiO-66(-NH_2)$ LBL (see ESI, Fig. S33–S37†). The results confirm the formation of 200 nm

$UiO-66$ framework type materials particles. Still, the higher surface area, broader diffraction peaks, larger mesopore contribution and lower organic linker content (TGA traces) of $UiO-66(-NH_2)$ LBL in comparison to $UiO-66(-NH_2)$ prepared by conventional solvothermal synthesis point to defective structures (see ESI, Fig. S33–37†).

Self-detoxification towards a nerve agent model compound

Once we characterized the different AC spheres and MOF@AC composites, we proceeded to evaluate their functional properties as self-detoxifying adsorbents of nerve agents. With this aim, we have screened the activity of the MOF@AC hybrids and their individual components (AC spheres and Zr-MOFs) towards the adsorption and degradation of a G-type nerve agent model, diisopropylfluorophosphate (DIFP). The activated carbon

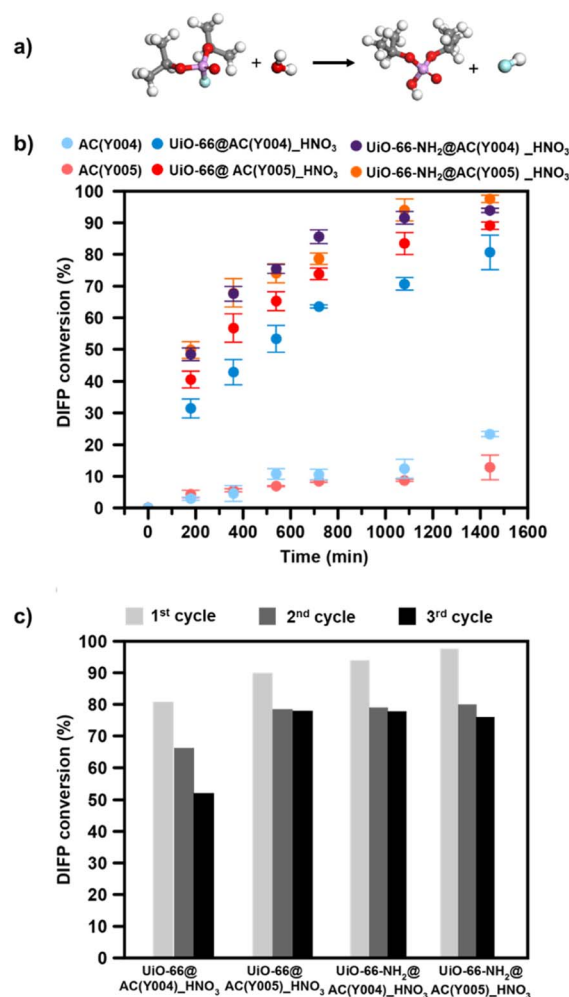


Fig. 3 (a) Diisopropylfluorophosphate (DIFP) hydrolytic degradation to yield non-toxic diisopropylphosphate (DIP). (b) Profiles of the DIFP (0.865 M) hydrolytic degradation process on the activated carbon sphere $AC(Y00n)_HNO_3$, $UiO-66@AC(Y00n)_HNO_3$ and $UiO-66-NH_2@AC(Y00n)_HNO_3$ ($n = 4, 5$) composites using a MOF : DIFP ratio, 1 MOF formula unit: 4 DIFP molecules. (c) Catalyst recyclability tests on DIFP hydrolysis (every 24 h) by $UiO-66(-NH_2)@AC(Y00n)_HNO_3$ composites ($n = 4, 5$).



spheres (AC(Y00n)_HNO₃ ($n = 1-5$)), MOFs (UiO-66(-NH₂) LBL) and hybrid MOF@AC materials were spiked with 2 μ L of water and 0.3 μ L of DIFP (0.865 M, MOF : DIFP ratio, 1 MOF formula unit: 4 DIFP molecules) and incubated at room temperature in a closed vial. The progress of the detoxification process was assessed by the extraction of unreacted DIFP and its detoxification product, diisopropylphosphate (DIP), with 2 mL of CDCl₃ and 0.5 mL of 0.1 M NaDCO₃ deuterium oxide solution, respectively. Afterwards, the CDCl₃ and D₂O extracts were analysed by GC-FID and ¹H and ³¹P NMR (Fig. S39–S45†). The results indicate that only the MOF@AC composites based on HNO₃-oxidized mesoporous activated carbon spheres, UiO-66(-NH₂)@AC(Y00n)_HNO₃ ($n = 4, 5$), led to a significant DIFP degradation (>90%), yielding non-toxic diisopropylphosphate (DIP) (Fig. 3a, b, S39† and Table 1).

The observed half-life times for DIFP degradation follow the trend UiO-66-NH₂@AC(Y004)_HNO₃ (1.8 h) < UiO-66-NH₂@AC(Y005)_HNO₃ (3.8 h) < UiO-66@AC(Y005)_HNO₃ (4.5 h) and UiO-66@AC(Y004)_HNO₃ (7.8 h) (Table S6†). Noteworthy, neither UiO-66(-NH₂) systems nor the carbon spheres (AC(Y00n)_HNO₃, $n = 1-5$) were able to hydrolyse the P-F bond to that extent (Fig. S40† and Table 1). In the case of the carbon spheres, the poor performance can be related to the typical physisorption of the toxic compound in a hydrophobic pore environment.¹³ The poor efficiency of UiO-66 and UiO-66-NH₂ is linked to the strong interaction of nerve agent degradation products with the oxyhydroxide metal cluster catalytically active sites in unbuffered aqueous media as already reported in the literature.^{17,34,35} Moreover, we have also tested the performance of a highly dispersed UiO-66(NH₂)/AC(Y00n)_HNO₃ ($n = 4, 5$) physical mixture of the same composition of MOF@AC composites (see Section S3.1 of the ESI†). The results show a 20–30% degradation of DIFP after 24 h (Fig. S49†). The low activity of the MOF/AC physical mixtures points to a lack of synergy between the two components in contrast to MOF@AC composites.

Considering these results, the observed synergistic interplay between UiO-66(-NH₂) systems and the carbon spheres can be

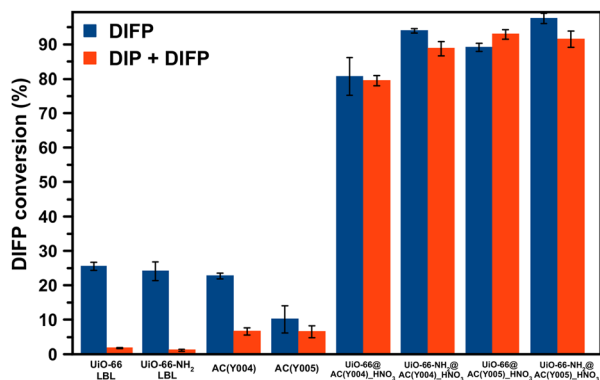


Fig. 4 Inhibitory effect of diisopropylphosphate (DIP) on diisopropylfluorophosphate (DIFP) hydrolytic degradation. Hydrolytic degradation of DIFP without the presence of DIP (blue) and in a 1 : 1 DIFP : DIP mixture (red) after 24 hours by the different materials.

explained by a strong affinity of the carbon pores for DIP, thereby preventing the poisoning of the catalytically active sites at metal clusters of the MOF framework. This mechanism is plausible given the amphiphilic nature of the DIP molecular structure featuring two hydrocarbon moieties and one phosphate fragment. To confirm this hypothesis, we have measured solid-liquid adsorption isotherms of DIP on the UiO-66(NH₂) LBL synthesized materials and AC(Y004)_HNO₃, AC(Y005)_HNO₃ activated carbon spheres at room temperature. Isotherms fitting to the Langmuir model (Fig. S46†) have allowed the calculation of an α partition coefficient for DIP between the AC and MOF phases according to the following equation: $\alpha = (K_1 \times m_2) / (K_2 \times m_1)$, where K_1 and K_2 correspond to the Langmuir equilibrium constant of DIP with the activated carbon sphere and MOF material, respectively and m_1 and m_2 correspond to the respective mass of activated carbon and the MOF in the composite material. The results show the α partition coefficient values in the range 10–30 (Table S7†) which indicate the favourable transfer of DIP from the MOF thin layer to the activated carbon sphere. Afterwards, we studied the inhibitory effect of DIP on DIFP degradation. The results show the total inhibition of the UiO-66(-NH₂) catalytic activity for DIFP degradation upon the addition of DIP (Fig. 4). Likewise, the moderate DIFP degradation activity of AC(Y004)_HNO₃ and AC(Y005)_HNO₃ is also affected by the DIP addition. By contrast, the presence of DIP does not affect the MOF@AC composite catalytic activity (Fig. 4). These observations support the synergistic behaviour of the MOF and AC in the MOF@AC hybrid systems for the degradation of the G-type nerve agent model.

The better performance of the UiO-66-NH₂@AC composites than those of UiO-66@AC can be attributed to the nucleophilic nature of the amino residue.^{34,36} Finally, to extend the application potential of these hybrid materials, we carried out reusability tests (see the ESI† for experimental details). With this aim, we have evaluated the continuous hydrolysis performance of DIFP (0.865 M, 1 MOF formula unit: 4 DIFP molecules) throughout 3 injection cycles (one DIFP injection every 24 h). The results indicate that UiO-66(-NH₂)@AC(Y00n)_HNO₃ ($n = 4, 5$) composites are able to detoxify the toxic model compound in the next two cycles, although a slight decrease in percentage degradation (10–30%) (Fig. 3c and Table S8†) is noticed. MOF integrity after each recyclability test was evaluated by PXRD showing that the UiO-66(-NH₂)@AC(Y00n)_HNO₃ ($n = 4, 5$) systems were unaffected (Fig. S48†).

Conclusions

We have found that the nature of the pore surface in a series of activated carbon spheres determines its oxidation process as well as the concomitant growth of a MOF thin film layer. The resulting UiO-66(-NH₂)@AC composites are able to prevent the secondary emission problem found in classical activated carbon adsorbents. This self-cleaning property positions them as advanced protective filters. The observed synergistic interplay between UiO-66(-NH₂) and the carbon spheres can be justified on the basis of a strong affinity of the carbon pores for the nerve



agent degradation product DIP, thereby preventing the poisoning of the catalytically active sites at metal clusters of the MOF framework after the P–F bond hydrolysis.

Conflicts of interest

There are no conflicts to declare.

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