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In situ construction of hetero-structured perovskite composites with exsolved Fe and Cu metallic nanoparticles as efficient CO₂ reduction electrocatalysts for high performance solid oxide electrolysis cells†

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Solid oxide electrolysis cells (SOECs) have been widely used for efficient conversion of CO₂ into valuable fuels and chemicals utilizing clean and renewable alternative energy sources. However, the scarcity of highly active cathode materials prevents their use in real-world applications. Herein, hetero-structured double perovskite/Ruddlesden–Popper perovskite (DP/RP-P) composites with exsolved Fe–Cu bimetallic nanoparticles are developed *via in situ* reduction treatment of the Sr₂Fe_{1.25}Cu_{0.25}Mo_{0.5}O_{6–σ} (SFCuM) perovskite at high temperatures. The LSGM-electrolyte-supported SOEC with the composite perovskites as the cathode demonstrates excellent electrochemical performance in CO₂ electrolysis. At an operating temperature of 800 °C and an applied potential of 1.4 V, the current density towards CO₂ electrolysis was as high as 1.7 A cm^{–2}, while the CO production and faradaic efficiency achieved were about 12.8 ml min^{–1} cm^{–2} and 95.2%, respectively. These results indicate that the hetero-structured DP/RP-SFCuM composites with exsolved Fe–Cu bimetallic nanoparticles are promising CO₂ electrolysis electrocatalysts for high-performance SOECs. Our research therefore highlights the potential for developing extremely efficient electrocatalysts for CO₂ electrolysis and utilization.

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1 Introduction

Owing to uncontrolled fossil fuel consumption, CO₂ emissions have increased dramatically in recent decades, resulting in a severe environmental crisis.¹ Therefore, lowering CO₂ concentrations and emissions in the atmosphere is critical. In addition to the use of renewable energy sources as replacement for fossil fuels, CO₂ capture and utilization has become another promising alternative.^{2–4} Solid oxide electrolysis cells (SOECs) are ideal for this because they are the most efficient devices for converting CO₂ into usable compounds, such as CO with theoretically energy conversion efficiencies close to 100% utilizing clean and sustainable alternative energy sources.^{5–8}

Conventionally, Ni-YSZ has been explored and employed as the cathode in SOECs, owing to its operating reliability, considerable electrocatalytic performance, and reasonable cost. Unfortunately, long-term stability concerns such as Ni particle agglomeration, carbon deposition, and Ni oxidation in the

testing environment greatly hinder further applications.⁵ Perovskite-related oxides,^{9–12} such as Sr₂Fe_{1.5}Mo_{0.5}O_{6–σ}, have attracted considerable interest as novel options for cathode materials in SOECs owing to their enhanced impurity tolerance, high redox stability, outstanding coking resistance, and acceptable ionic and electronic conductivity.^{11,13} However, weak high-temperature chemical adsorption of CO₂ molecules and poor electrocatalytic activity limit their efficacy in CO₂ reduction operations.

In situ exsolving of metal nanoparticles on the perovskite surface has been explored as a promising approach for improving catalytic activity.^{14–17} Under the testing conditions, fine and equally dispersed catalyst nanoparticles can be obtained on the surface of porous electrodes. Subsequently, the exsolved metal nanoparticles and abundant oxygen vacancies at the metal–oxide interfaces can supply more active reaction sites for the adsorption and activation of CO₂ molecules.¹⁵ Furthermore, owing to a stronger metal–oxide interface arising from the binding effect with the parent perovskite, the exsolved metal nanoparticles have improved high-temperature anti-sintering stability.^{10,18} Among the various metal catalysts, Fe- or Cu-based metals/alloys are widely used as catalysts in the CO₂ reduction reaction,^{19–21} as Fe has the highest catalytic activity for CO₂ reduction and a low energy barrier,^{22,23} whereas Cu has excellent CO₂ adsorption properties and coking resistance.²¹

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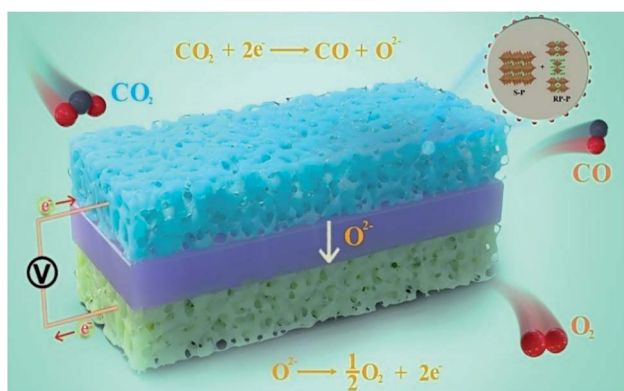
In addition to these *in situ* exsolution strategies, another potential technique that can result in favorable properties is the fabrication of oxide heterostructures,^{24,25} especially simple perovskite/Ruddlesden–Popper perovskites (S-P/RP-P).^{26–29} For example, partially painting the surface of a single perovskite oxide (La_{0.6}Sr_{0.4})CoO₃ with a Ruddlesden–Popper (RP) K₂NiF₄-type layered perovskite (La,Sr)₂CoO_{4.27} can result in a 1000 times increase in the surface oxygen exchange coefficient.²⁸ The electrical surface exchange coefficient of hetero-structured Nd_{0.5}Sr_{0.5}CoO_{3–δ}/Nd_{0.8}Sr_{1.2}CoO_{4±δ} composites is 100–1000 times greater than that of a single-phase sample.²⁶ Thus, hetero-structured composites can potentially also be introduced into SOECs for efficient catalytic reactions during the CO₂ electrolysis process.

Herein, the *in situ* construction of hetero-structured DP/RP-SFCuM composites with exsolved Fe–Cu bimetallic nanoparticles was proposed with one-step treatment of the Sr₂Fe_{1.25}Cu_{0.25}Mo_{0.5}O_{6–σ} perovskite under reducing conditions at high temperatures. Subsequently, the effects of the phase evolution on the crystal and the physical and chemical properties were thoroughly analyzed, and the catalytic performances of the resultant electrode in CO₂ electrolysis reactions were systematically evaluated. A schematic illustration of the cell configurations of the SOECs for CO₂ electrolysis is shown in Scheme 1. The hetero-structured DP/RP-SFCuM perovskite composites with exsolved Fe–Cu bimetallic nanoparticles exhibit excellent electrochemical performance in CO₂ electrolysis reactions. At 800 °C, the CO₂ electrolysis current density is equal to approximately 1.7 and 2.5 A cm^{–2} at an applied potential of 1.4 and 1.5 V, respectively, which is superior to that of single cells with DP-SFCuM as the cathode and other promising electrodes, demonstrating that it is an efficient CO₂ electrolysis electrocatalyst for high-performance SOECs.

2 Experimental section

2.1 Material preparation

Sr₂Fe_{1.5}Mo_{0.5}O_{6–δ} (SFM) and Sr₂Fe_{1.25}Cu_{0.25}Mo_{0.5}O_{6–δ} (SFCuM) powders were prepared by the combustion method.³⁰ During the preparation, the starting materials were H₂₄Mo₇N₆O₂₄,



Scheme 1 Schematic illustration of the cell configurations of SOECs for CO₂ electrolysis.

Cu(NO₃)₂·9H₂O and Fe(NO₃)₃·9H₂O (all more than 99.9% pure) as well as Sr(NO₃)₂ (99.5% pure). The chelating agents were citric and ethylene diamine tetra-acetic acids. After synthesis, the powders were obtained by firing at 1000 °C for 10 h. Similar preparation procedures were applied for the synthesis of La_{0.4}Ce_{0.6}O_{2–δ}, Sm_{0.2}Ce_{0.8}O_{1.9} and La_{0.58}Sr_{0.4}Co_{0.2}Fe_{0.8}O_{3–δ} powders.

2.2 Cell preparation and electrochemical testing

La_{0.8}Sr_{0.2}Ga_{0.8}Mg_{0.2}O_{3–δ} (LSGM)-based electrolyte, which supported a single SOEC, was used to evaluate the performance of the catalyst during the CO₂ electrolysis. Firstly, the LSGM electrolytes (the powders were bought from Wuxi city Kaistar Electro-Optic Materials Co., Ltd., and the average particle size is about 3 μm with a purity of about 99.9%) were dry-pressed and heated at 1500 °C for 6 h, followed by polishing to ~250 μm. Then, La_{0.4}Ce_{0.6}O_{2–σ} (LDC) was applied to one side of the electrolyte and heated at 1400 °C for 2 h. Next, the cathode pastes were coated on the LDC layer and heated at 1150 °C for 2 h. Subsequently, LSCF-SDC anode paste was applied to another solid electrolyte side and sintered at 1100 °C for 2 h. To evaluate the catalytic activities of the obtained electrodes in terms of the CO₂ reduction reaction, LSGM electrolyte-supported symmetrical cells in a 1 : 1 CO–CO₂ atmosphere are applied. Ag paste (covering 0.215 cm² area) served as a current collector.

Then, the single SOEC was sealed in an Al₂O₃ tube using a Cerama-bond 552-VFG sealant (Aremco) and heated to 850 °C. Prior to the tests, the cathodes were conditioned in H₂ containing 3% of H₂O for 2 h. The cell performance towards CO₂ electrolysis was then evaluated when the cathode was changed to a pure CO₂ environment. During testing, the LSV and EIS data (10⁵ to 0.01 Hz) were collected at 700–850 °C. After testing, an equivalent circuit was decided by using RelaxIS3.0 software (Germany). The electrical surface exchange coefficient (*k^{el}*) was then calculated using eqn (1):^{26,27,31}

$$k^{\text{el}} = RT/4F^2 R A_{\text{electrode}} \times c_0 \quad (1)$$

where *R* and *F* are the universal gas and the Faraday constants, respectively, *T* is the temperature (in K), *R* is the polarization resistance of the low frequencies, *A_{electrode}* is the effective area of electrode and *c₀* is the concentration of lattice O in the resultant electrode (calculated from XPS analysis).

The gas product was determined by gas chromatography (performed using a GC2060 instrument manufactured in China). The gas flow rate was determined using a flowmeter. The Faraday efficiency was calculated as follows:³²

$$\text{FE}_{\text{CO}} = \frac{0.1315 \times V (\text{mL min}^{-1}) \times \nu (\text{vol}\%) }{I_{\text{total}} (\text{A})} \times 100\% \quad (2)$$

where *V* is the gas flow rate, *ν* (vol%) is the concentration of CO, and *I_{total(A)}* is the cell current.

2.3 Material characterization

The materials synthesized in this work were characterized by XRD (Miniflex600, Japan), HR-TEM (performed using a JEM-

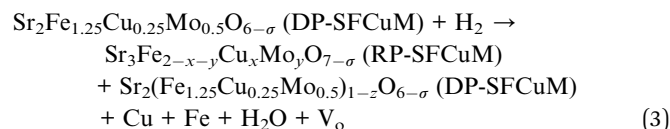
F200 instrument manufactured in Japan), and SEM (performed using an APREOS instrument, manufactured in the Netherlands). The O vacancy concentration was analyzed by EPR (EMXmicro-6/1/P/L, Germany). The chemical states of the Sr, Fe, Mo, Cu and O elements were analyzed by XPS (ESCALAB 250Xi). Relaxis3.0 software (Germany) was used to analyze the EIS data, and the detailed parameters about the DRT analysis are as follows: (basic function: Gaussian; lambda: 0.0001; shape factor: 0.5).

3 Results and discussion

3.1 Crystal structure and morphology of the catalysts

As shown in Fig. 1(a) and (c), the as-synthesized $\text{Sr}_2\text{Fe}_{1.25}\text{Cu}_{0.25}\text{Mo}_{0.5}\text{O}_{6-\sigma}$ (SFCuM) powders in the oxidation state exhibit a pure perovskite phase (DP-SFCuM), which crystallizes in a cubic $Fm\bar{3}m$ space group with a lattice constant of $a = b = c = 0.782$ nm. However, after reduction under a H_2 atmosphere at 850°C for 2 h, phase evolution occurs. In addition to the DP-SFCuM phase (43.4%), the Ruddlesden–Popper layered perovskite of $\text{Sr}_3\text{Fe}_{2-x-y}\text{Cu}_x\text{Mo}_y\text{O}_{7-\sigma}$ (RP-SFCuM, 49.79%) and Cu–Fe bimetal phases (Fe: 2.72% and Cu: 4.09%) could also be clearly detected (Fig. 1(b) and (d)); this result is slightly different from that of the sample without Cu doping (Fig. S1†), where only exsolved Fe metal is clearly detected.

It is worth noting that the peak positions corresponding to the exsolved Cu and Fe metals are clearly separated (Fig. 1(b)), indicating that the Cu and Fe elements exsolved from the parent SFCuM matrix are not in alloy form, which differs significantly from the previous reports such as the exsolved Fe–Ni,¹⁹ Fe–Co³³ and Cu–Ni alloys.³⁴ This could be because that Cu and Fe atoms are less likely to come together on an atomic basis, resulting in significant fluctuations and phase separation in Fe–Cu alloys.^{35,36} According to the detected phases in the XRD results, the exsolution process can be expressed using eqn (3):



where $\text{Sr}_2(\text{Fe}_{1.25}\text{Cu}_{0.25}\text{Mo}_{0.5})_{1-z}\text{O}_{6-\sigma}$ (DP-SFCuM) represents a B-site-deficient perovskite after reduction and before phase transformation, and V_O represents the O vacancy during the phase evolution process.

HR-TEM analysis is applied to observe the structural variations in the DP-SFCuM phase induced by the reduction treatment. As shown in Fig. 2, before reduction, only a single phase is observed; the interplanar spacing is approximately 0.39 nm in each direction (see Fig. 2(b)), which is consistent with the [001] zone axis of the cubic SP-SFCuM phase. However, after

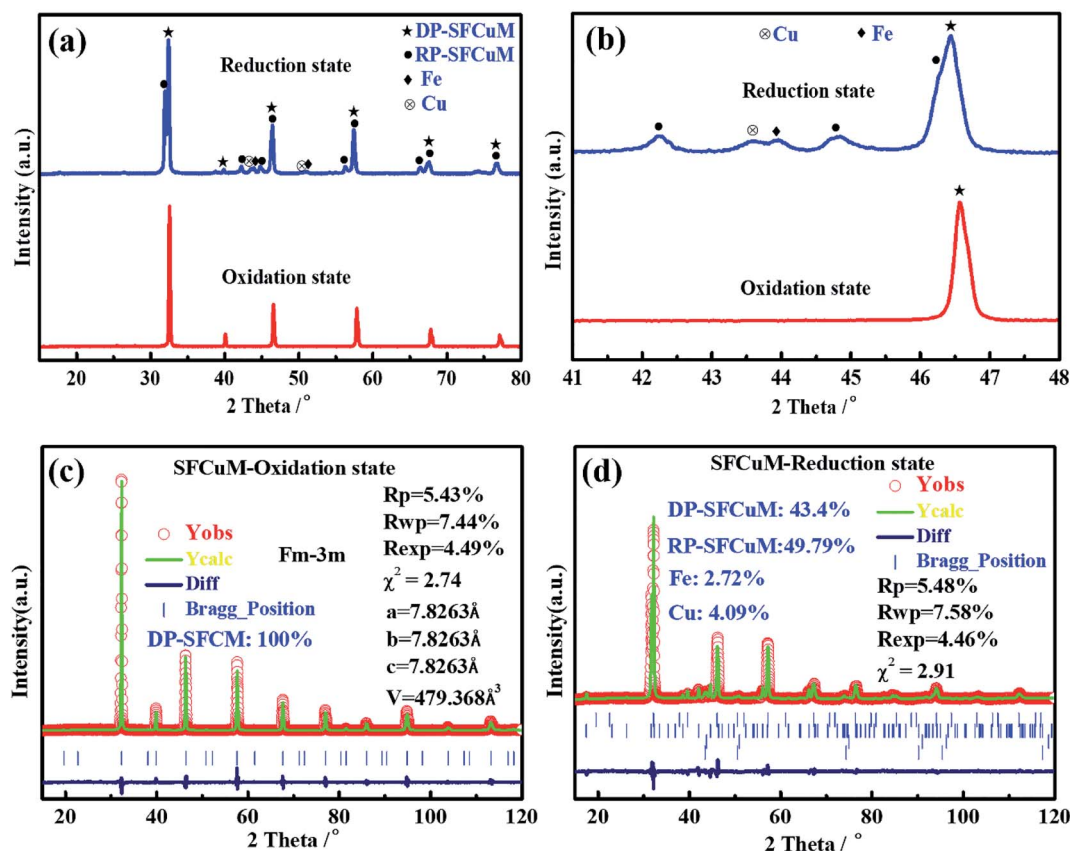


Fig. 1 (a) As-synthesized and reduced $\text{Sr}_2\text{Fe}_{1.25}\text{Cu}_{0.25}\text{Mo}_{0.5}\text{O}_{6-\sigma}$ (SFCuM) powders, (b) magnification of (a), and (c) and (d) Rietveld refinement performed for the as-synthesized and reduced SFCuM powders, respectively.

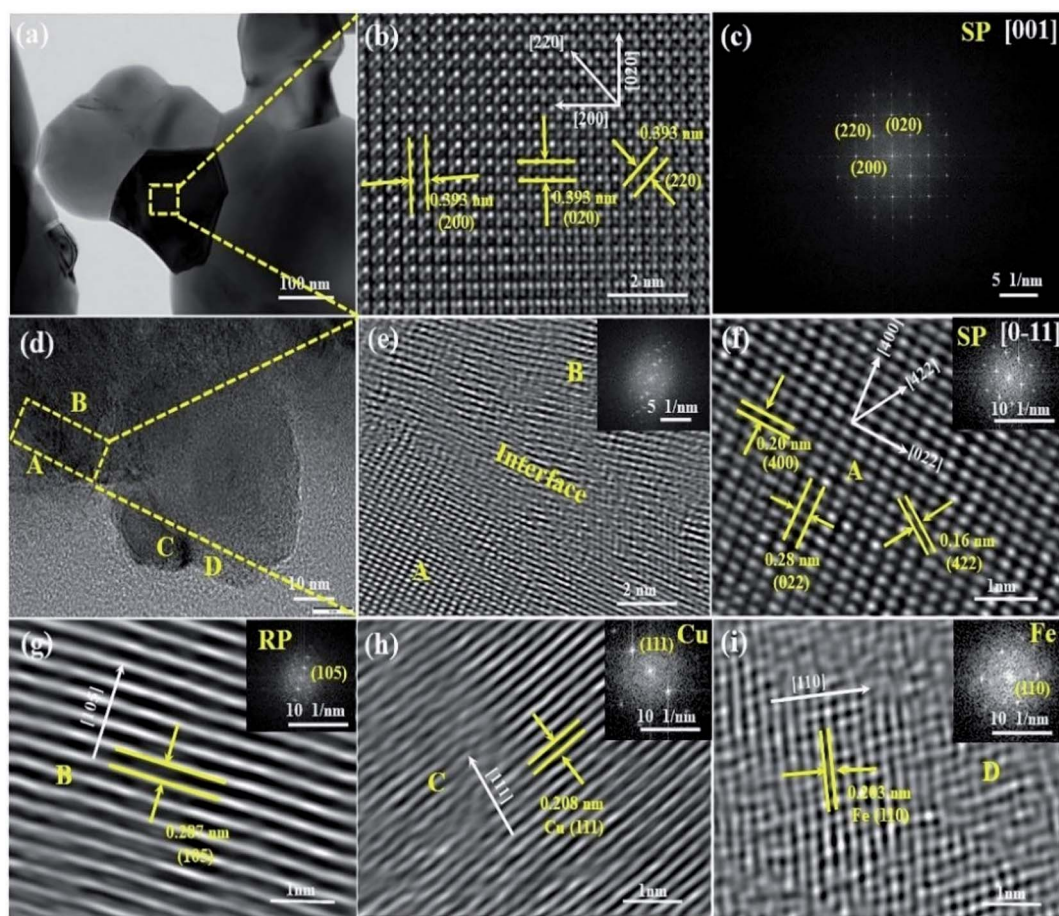


Fig. 2 (a) Morphology of the as-synthesized SFCuM powders, (b) HR-TEM images of the powders shown in (a), and (c) corresponding fast Fourier transform (FFT) spectra. (d) Morphology of the reduced SFCuM powders, (e) magnification of the interface between parts A and B, and (f–i) magnification of parts A, B, C and D, respectively.

reduction, the morphology and crystalline structure are obviously changed, as shown in (d–i). Not only are the crystalline structures of DP-SFCuM (part A, indexed as the [0–11] zone axis of the DP-SFCuM phase) and RP-SFCuM (part B, indexed as the (105) lattice plane of the RP-SFCuM phase) observed, but Cu and Fe nanoparticles could also be clearly confirmed (the lattice spacing was 0.208 and 0.203 nm in parts C and D, which corresponds to the (111) plane of Cu and the (110) plane of Fe, respectively). The XRD results shown in Fig. 1 are in good agreement with these results.

Furthermore, the HR-TEM images reveal that the exsolved Cu and Fe bimetal nanoparticles were both effectively fixed in the matrix of the perovskite, showing that the exsolved Cu–Fe bimetal nanoparticles and the perovskite matrix interact strongly. This anchoring effect is critical for improving the stability of metal nanocatalysts under SOEC testing conditions, as it mostly prevents metal nanoparticles from sintering and agglomerating by the perovskite ceramic matrix at higher operating temperatures.^{14,18}

To further determine the distribution of the exsolved nanoparticles in the reduced SFCuM matrix, TEM-EDS elemental mapping was carried out and the results are shown in Fig. 3. On

the surface of the matrix particles, a large number of nanosized particles with particle sizes in the range of 10–30 nm are uniformly dispersed. Furthermore, the exsolved nanoparticles include exclusively Cu or Fe metals, whereas other elements are equally distributed in the matrix particles, indicating that these nanoparticles are composed of Fe or Cu metal. Further, TEM-EDS line scanning is performed to determine the atomic fraction of each element in the exsolved nanoparticles. Fig. 3(h) and (i) further confirm that the exsolved nanoparticles are not in alloy form but mainly comprise separated Cu and Fe elements, which is consistent with a previous report.²⁹

As shown in Fig. S2,† when only Fe exsolves from the matrix, the exsolved nanoparticles grow easily and are mainly in the range 50–70 nm. By contrast, in the presence of Fe–Cu bimetal, the average size of the exsolved particles is obviously decreased, and is mainly in the range of approximately 10–30 nm. This suggests that the separated Fe–Cu bimetal is also effective for preventing the metal nanoparticles from sintering and agglomerating at the high temperatures. The separated Fe–Cu bimetal may be due to the fact that Cu and Fe metals are difficult to form alloys, which could be separated each other during the exsolution process, effectively preventing them from

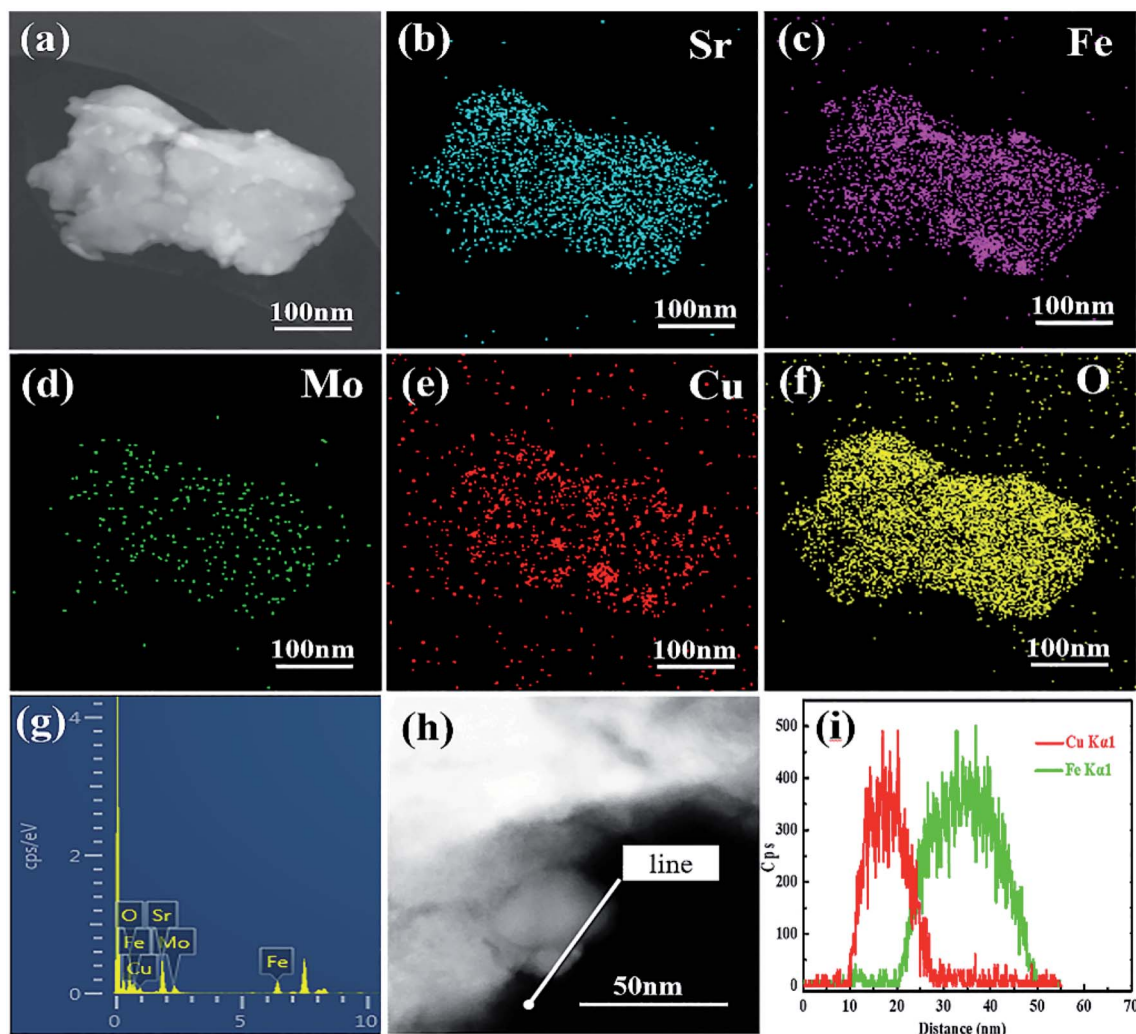


Fig. 3 (a) TEM micrographs of the reduced SFCuM particles, (b–f) TEM-EDS elemental mappings of the reduced SFCuM particles, (g) amount of each element, and (h) and (i) TEM-EDS line scanning of the exsolved nanoparticles.

agglomerating and sintering at high temperatures. This structural feature is not only beneficial for stability enhancement of the exsolved nano catalysts, but could also provide more metal–oxide interfaces for the adsorption and activation of CO_2 molecules in the resultant electrode.¹⁵

3.2 Surface chemical states of the catalysts

In addition to crystal morphology and structure, the surface chemical states change substantially during reduction. As shown in Fig. 4, the XPS spectra of the Mo cations in the as-synthesized SFCuM sample demonstrate two symmetric peaks at 235.3 and 232.15 eV (Fig. 4(a)), which correspond to Mo^{6+} electrons $3d_{3/2}$ and $3d_{5/2}$,³⁷ respectively. The Fe 2p spectrum (Fig. 4(b)) shows two asymmetric peaks, each of which could be deconvoluted into three peaks, each corresponding to the mixed oxidation state of $\text{Fe}^{2+/3+/4+}$.³⁷ The oxidation states corresponding to Mo, Fe, and Cu are all clearly reduced after reduction at 850 °C for 2 h under a H_2 atmosphere, especially Fe^0 and Cu^0 are clearly observed.

During reduction, the creation of additional oxygen vacancy defects in the final sample is followed by the formation of lower oxidation state metals (Fig. 5), which is also in good agreement with the variations in the O_{latt} and O_{ads} shown in Fig. 4(d). After reduction treatment, the amount of O_{latt} is obviously decreased, whereas that of O_{ads} is greatly increased. Accordingly, the ratio of the $\text{O}_{\text{ads}}/\text{O}_{\text{latt}}$ significantly increases from 2.40 to about 4.54. The high $\text{O}_{\text{ads}}/\text{O}_{\text{latt}}$ peak ratio demonstrates an increased concentration of adsorbed species of oxygen (such as carbonate, O_2^{2-} , OH^- , and O^-) at the reduced SFCuM surface. At higher temperatures and in a reducing atmosphere, such weakly adsorbed oxygen species can be easily released,³⁸ leaving a large number of active sites, which would promote full contact between CO_2 molecules and active B-site transition metals. Furthermore, the presence of mixed-valent $\text{Mo}^{5+}/\text{Mo}^{6+}$ and $\text{Fe}^{2+}/\text{Fe}^{3+}$ and large concentrations of oxygen vacancy defects, can result in the ionic and electrical conductivity and catalytic activity necessary for the CO_2 electrolysis processes.

According to the XPS analysis, phase evolution also has a significant impact on the surface composition of the resulting

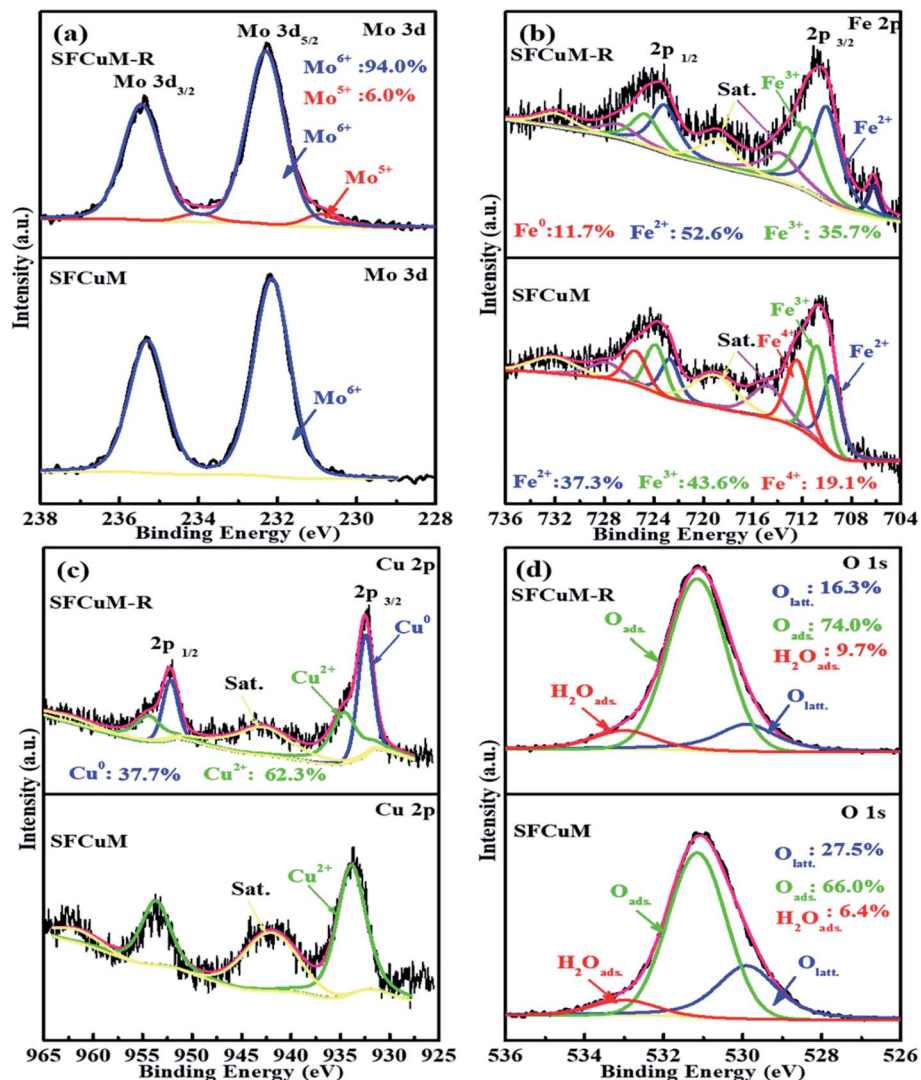


Fig. 4 XPS spectra of the as-synthesized and reduced SFCuM: (a) Mo 3d, (b) Fe 2p, (c) Cu 2p and (d) O 1s (PS: all the SFCuM-R samples stand for the DP-SFCuM/RP-SFCuM composite phase with the exsolved nanoparticles after reduction).

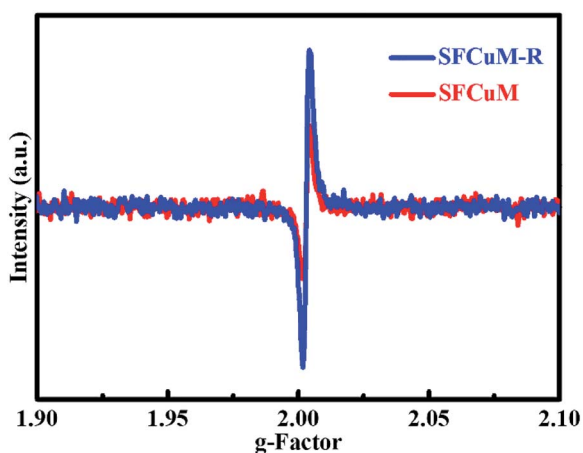


Fig. 5 Electron paramagnetic resonance (EPR) measurements of the SFCuM and SFCuM-R samples.

perovskite. As illustrated in Fig. 6(a), the ratio of $Sr_{\text{surface}}/Sr_{\text{latt}}$ is greatly increased after reduction, wherein Sr_{latt} indicates Sr in the SFCuM lattice, whereas Sr_{surface} comprises mainly surface-bound Sr, such as Sr-OH or Sr-CO₃. Because the binding energies for the O 1s core levels in the species CO₃²⁻ and OH⁻ are almost identical, photoelectron spectroscopy alone is insufficient to distinguish between the hydroxyl and carbonate groups on the surface. Quantitative data, notably the atomic ratio between the C 1s component (only CO₃²⁻) at 289.3–289.6 eV and the O-component (OH⁻ + CO₃²⁻) at 531.5 eV are utilized to elucidate the aforementioned issue. According to Table S1,[†] the ratio of O/C is about 3.75 for the reduced SFCuM sample, which is slightly higher than the theoretical value estimated from the stoichiometry of carbonate (O/C in carbonate is 3). This simple assessment shows that the Sr_{surface} comprises both Sr-OH and Sr-CO₃, which is consistent with the result shown in Table S2,[†] where the ratio of CO₃²⁻/Sr is about 0.84 on the surface of the reduced SFCuM.

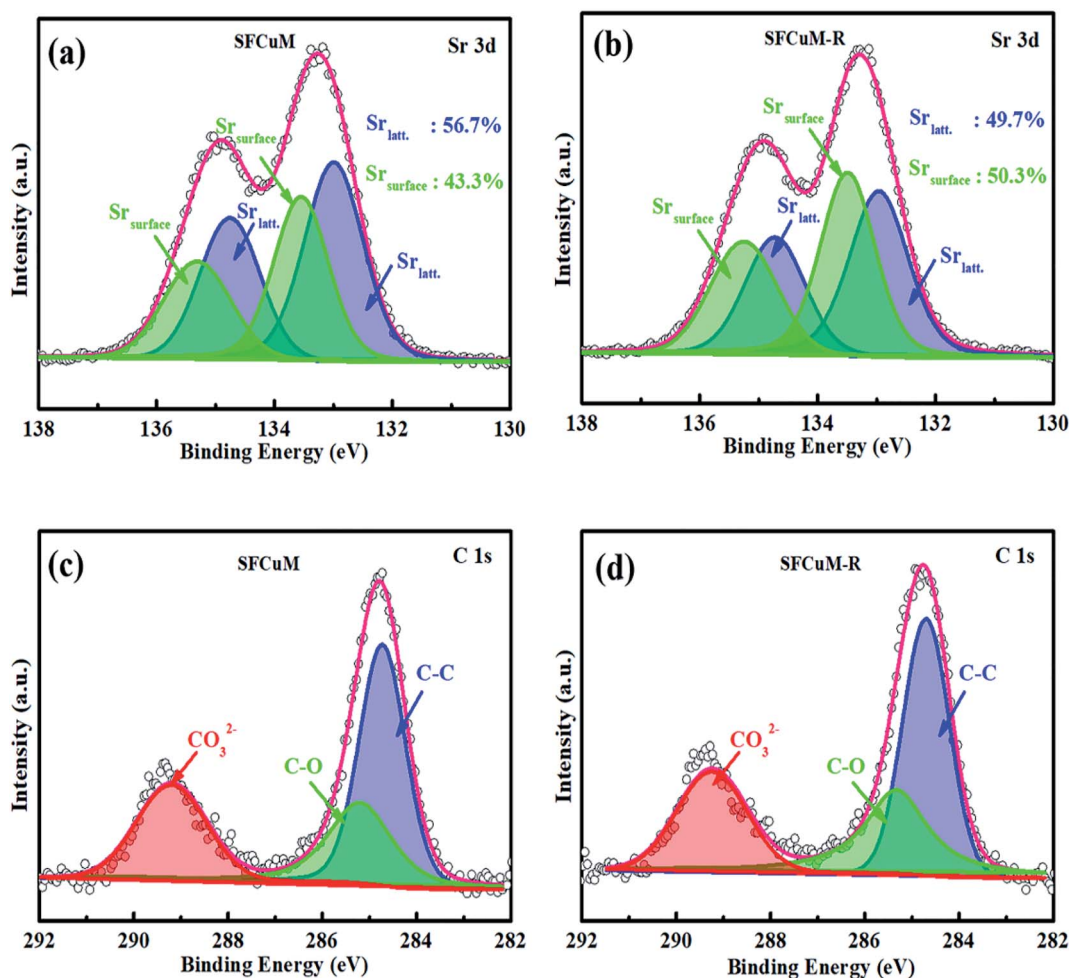


Fig. 6 XPS spectra of the as-synthesized and reduced SFCuM: (a) and (b) Sr 3d, (c) and (d) C 1s.

It is probable that the adsorbed carbonate ions should be caused by the enriched alkaline earth element Sr on the surface. According to the surface composition (Table S2[†]), before reduction, the Sr/(Fe + Mo + Cu) ratio in the SFCuM sample is approximately 1.54, whereas that of the reduced sample increases to approximately 1.93. The increased amount of Sr segregation is closely related to the formation of the RP-SFCuM ($\text{Sr}_3\text{Fe}_{2-x-y}\text{Cu}_x\text{Mo}_y\text{O}_{7-\sigma}$) phase after reduction, in which the larger A-site Sr cations preferentially dominate the perovskite surface.^{39,40} The segregated Sr cations on the perovskite surface are also important for the chemical adsorption of CO_2 molecules.^{41,42} A-site alkali and/or alkaline earth oxides such as SrO ⁴¹ or CaO ⁴³ on the perovskite surface has been revealed to improve CO_2 adsorption at elevated temperatures, as these metal oxides are alkaline in nature and can adsorb CO_2 ,⁴⁴ resulting in a highly active surface for CO_2 reduction.

3.3 Electrochemical performances of a single SOEC for CO_2 electrolysis

To evaluate the catalytic activities of the SFCuM and SFCuM-R electrodes in terms of the CO_2 reduction reaction, their electrochemical impedance spectra (EIS) are obtained using LSGM

electrolyte-supported symmetrical cells in a 1 : 1 $\text{CO}-\text{CO}_2$ atmosphere at different operating temperatures. The discrepancy between the intercepts of the low- and high-frequency arcs with the real axis is regarded as the polarization resistance (R_p) in the EIS, which is defined as a leading parameter for the assessment of electrode electrochemical performance; a smaller R_p value indicates more desirable catalytic activities in electrochemical systems. As shown in Fig. 7, the R_p values of the SFCuM-R electrode are 0.46, 0.81, 2.15 and $7.2 \Omega \text{ cm}^{-2}$ at the operating temperatures of 850, 800, 750 and 700°C , respectively (Fig. 7(a)). This is obviously lower than the R_p values of the SFCuM electrode under the same testing conditions (Fig. S3[†]), indicating that the catalytic activity for the CO_2 reduction reaction in the SFCuM electrode is likely to be enhanced by the reduction treatment.

To clarify the origin of the enhancement in catalytic activity, the EIS data are further evaluated according to the distribution of relaxation times (DRTs), as demonstrated in Fig. 7(c). Clearly, the area of the low-frequency peak P3 process is significantly reduced by the reduction treatment, whereas that of the P1 and P2 processes do not change significantly. In addition, in a previous study, it is found that P1 is linked to oxygen ion

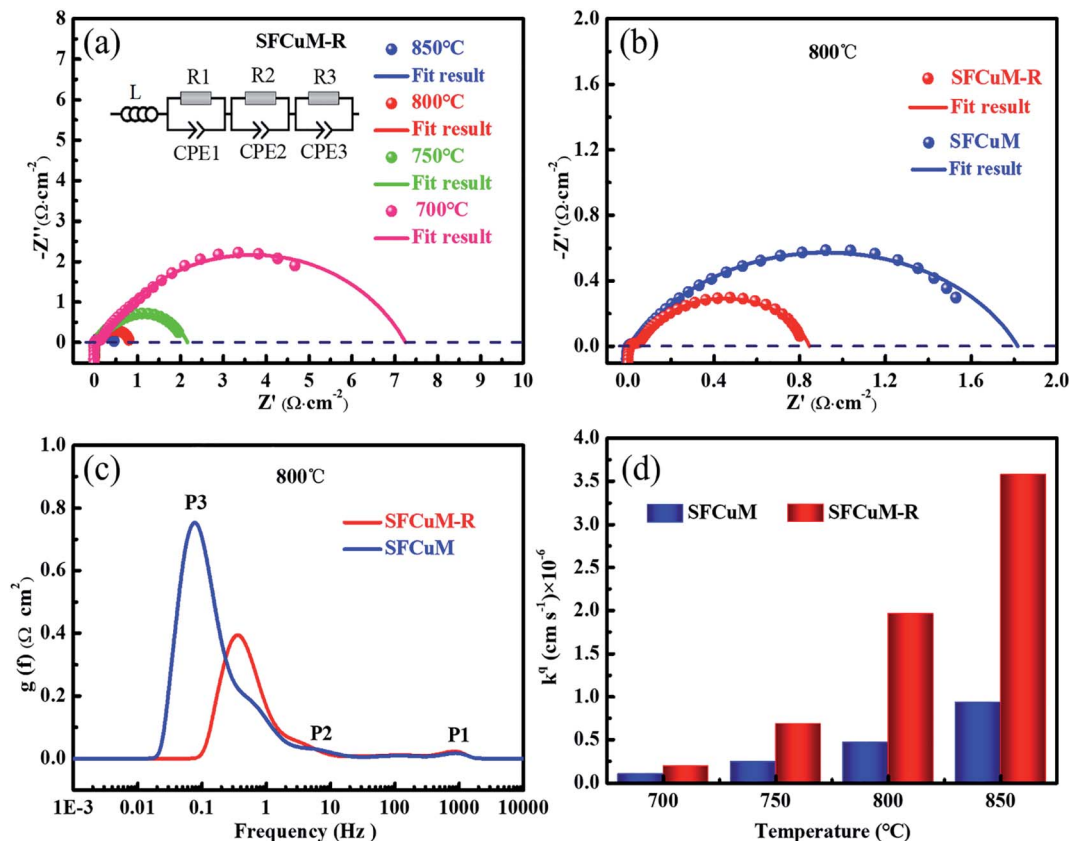


Fig. 7 (a) EIS of LSGM electrolyte-supported symmetrical cells with the configuration SFCuM-R/LDC/LSGM/LDC/SFCuM-R under a 1 : 1 CO₂-CO₂ atmosphere at different operating temperatures; (b) comparison of the EIS spectra using different electrodes at 800 °C; (c) assessment of the DRT spectrum at 800 °C; (d) calculated k^q of the different electrodes.

transportation at the interface between the electrodes and the LSGM electrolyte, whereas P2 is linked to the transfer of O²⁻ in the electrodes, and P3 represents gas convention processes, which include adsorption, activation, and dissociation reactions.^{11,12,19,45} CO₂ adsorption and activation processes are considerably improved by the reduction treatment, as evidenced by the decreased P3 in the SFCuM-R electrode. Besides, it is also obvious that the peak position corresponding to the P3 process greatly shifts toward the high frequency range for the reduced SFCuM-R electrode, suggesting that the electrochemical surface exchange reactions of the gas convention process should also be accelerated by the reduction treatment. The improved gas convention process is not only related to the formation of more metal-oxide interfaces and oxygen vacancy defects during reduction, which supply more active reaction sites for the activation and adsorption of CO₂ molecules,^{15,16} but also to the formation of hetero-structured DP/RP-SFCuM composites by reduction, which exhibit superior electrical surface exchange coefficient (k^q , Fig. 7(d)) for enhanced electrochemical surface exchange reactions.^{26-28,31}

Consequently, the LSGM-electrolyte-supported single cell with SFCuM-R as the cathode and LSCF-SDC as the anode exhibits excellent current density for CO₂ electrolysis under a 100% CO₂ atmosphere (see Fig. 8(a)). At 800 °C, the CO₂ electrolysis current density of the SFCuM-R-containing SOEC is

equal to 0.45, 0.75, 1.15, 1.7 and 2.5 A cm⁻² at an applied potential of 1.1, 1.2, 1.3, 1.4 and 1.5 V, respectively, which is superior to that of the single cell with SFCuM and SFM-R as the cathodes (see Fig. 8(b), S4 and S5[†]). Furthermore, these values are also comparable to those of other prospective perovskite electrodes (see Table S3[†]). Additionally, the single cell with the SFCuM-R electrode also exhibits high current efficiency for CO₂ to CO conversion at different potentials. As shown in Fig. 8(c), the CO production gradually increases with increasing applied potential, whereas the corresponding faradaic efficiency decreases slightly. However, even at an applied potential of 1.4 V, the CO production and faradaic efficiency are still as high as 12.8 ml min⁻¹ cm⁻² and 95.2%, respectively. Besides, the obtained SFCuM-R electrode exhibits excellent long-term stability during CO₂ electrolysis. As shown in Fig. 8(d), the current density stabilizes at around 0.43 A cm⁻² under a pure CO₂ atmosphere at 800 °C and shows no prominent degradation following 100 h of examination. After the long-term stability testing, no obvious carbon formation and delamination are observed (Fig. S6 and S7[†]), suggesting that the hetero-structured DP/RP-SFCuM composite with exsolved Fe-Cu bimetal nanoparticles is a promising CO₂ electrolysis electrocatalyst for high performance SOECs.

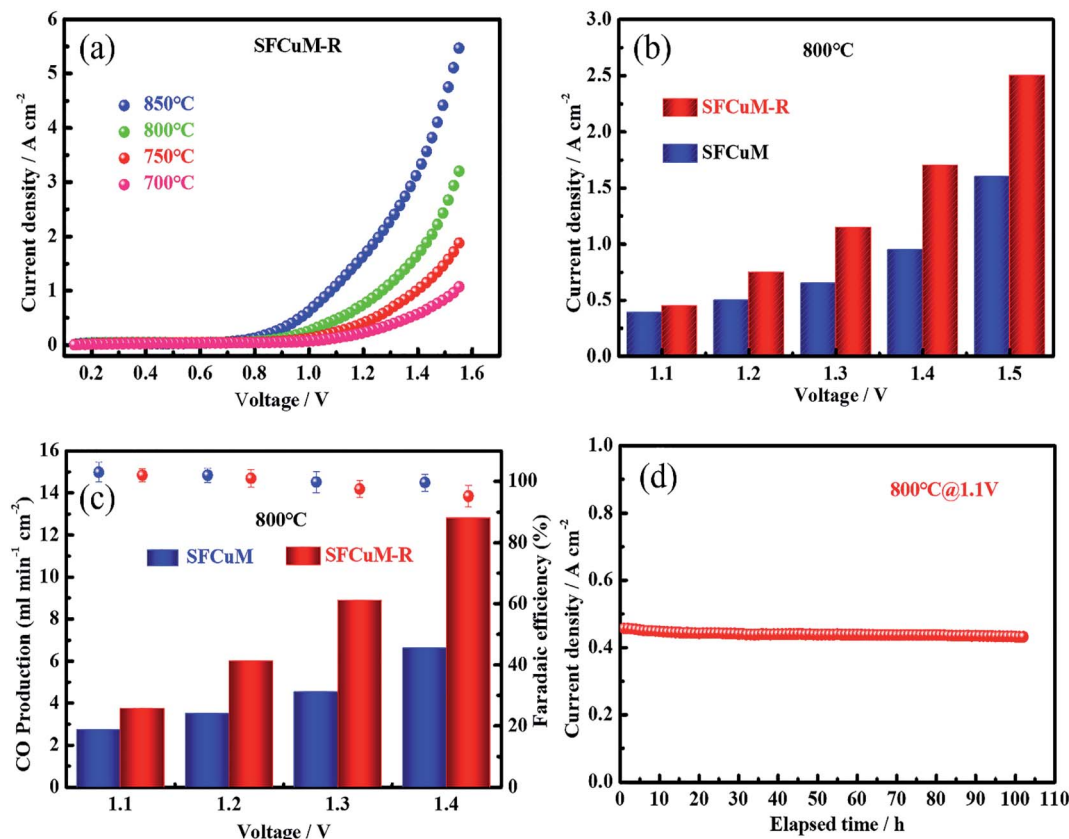


Fig. 8 (a) Single-cell current density with SFCuM-R as the fuel electrode; (b) current density comparison of the cell with various fuel electrodes; (c) production of CO and faradaic efficiency; (d) long-term electrochemical stability during CO₂ electrolysis.

4 Conclusions

The *in situ* construction of hetero-structured DP/RP-SFCuM composites with exsolved Cu–Fe bimetal nanoparticles is successfully achieved by one-step reduction treatment of the Sr₂Fe_{1.25}Cu_{0.25}Mo_{0.5}O_{6-σ} (SFCuM) perovskite at a temperature of 850 °C for 2 h. The LSGM-electrolyte-supported single cell with the obtained composite as the cathode exhibits excellent electrochemical performance for CO₂ electrolysis. At an operating temperature of 800 °C, the CO₂ electrolysis current density is as high as 1.7 and 2.5 A cm⁻² at the applied potentials of 1.4 and 1.5 V, respectively, which is superior to that of a single cell with DP-SFCuM as the cathode. The improved electrochemical performance is directly related to the formation of abundant metal–oxide interfaces and oxygen vacancy defects, as well as the combination of oxide heterostructures. These results demonstrate that hetero-structured DP/RP-SFCuM composites with exsolved Cu–Fe bimetal nanoparticles are very efficient CO₂ electrolysis electrocatalysts for high-performance SOECs.

Conflicts of interest

There are no conflicts of interest to declare.

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References

- W. Li and J.-L. Luo, *Electrochem. Energy Rev.*, 2021, **4**, 518–544.
- Y. Song, X. Zhang, K. Xie, G. Wang and X. Bao, *Adv. Mater.*, 2019, **31**, e1902033.
- F. Cheng, X. Duan and K. Xie, *Angew. Chem.*, 2021, **133**, 18940–18947.

- 4 M. Zheng, S. Wang, Y. Yang and C. Xia, *J. Mater. Chem. A*, 2018, **6**, 2721–2729.
- 5 Y. Song, Z. Zhou, X. Zhang, Y. Zhou, H. Gong, H. Lv, Q. Liu, G. Wang and X. Bao, *J. Mater. Chem. A*, 2018, **6**, 13661–13667.
- 6 J. Zhu, W. Zhang, Y. Li, W. Yue, G. Geng and B. Yu, *Appl. Catal., B*, 2020, **268**, 118389.
- 7 H. Li, T. Liu, P. Wei, L. Lin, D. Gao, G. Wang and X. Bao, *Angew. Chem., Int. Ed.*, 2021, **60**, 14329–14333.
- 8 D. Huan, L. Zhang, S. Zhang, N. Shi, X. Li, K. Zhu, C. Xia, R. Peng and Y. Lu, *J. Mater. Chem. A*, 2021, **9**, 2706–2713.
- 9 Y. Zhou, Z. Zhou, Y. Song, X. Zhang, F. Guan, H. Lv, Q. Liu, S. Miao, G. Wang and X. Bao, *Nano Energy*, 2018, **50**, 43–51.
- 10 L. Ye, M. Zhang, P. Huang, G. Guo, M. Hong, C. Li, J. T. Irvine and K. Xie, *Nat. Commun.*, 2017, **8**, 14785.
- 11 Y. Li, Y. Li, Y. Wan, Y. Xie, J. Zhu, H. Pan, X. Zheng and C. Xia, *Adv. Energy Mater.*, 2019, **9**, 1–10.
- 12 Y. Jiang, Y. Yang, C. Xia and H. J. M. Bouwmeester, *J. Mater. Chem. A*, 2019, **7**, 22939–22949.
- 13 C. Zhu, S. Hou, X. Hu, J. Lu, F. Chen and K. Xie, *Nat. Commun.*, 2019, **10**, 1173.
- 14 J. T. S. Irvine, D. Neagu, M. C. Verbraeken, C. Chatzichristodoulou, C. Graves and M. B. Mogensen, *Nat. Energy*, 2016, **1**, 1–13.
- 15 H. Lv, L. Lin, X. Zhang, Y. Song, H. Matsumoto, C. Zeng, N. Ta, W. Liu, D. Gao, G. Wang and X. Bao, *Adv. Mater.*, 2020, **32**, 1–9.
- 16 H. Lv, T. Liu, X. Zhang, Y. Song, H. Matsumoto, N. Ta, C. Zeng, G. Wang and X. Bao, *Angew. Chem., Int. Ed.*, 2020, **59**, 15968–15973.
- 17 D. J. Deka, J. Kim, S. Gunduz, M. Aouine, J.-M. M. Millet, A. C. Co and U. S. Ozkan, *Appl. Catal., B*, 2021, **286**, 119917.
- 18 J. H. Myung, D. Neagu, D. N. Miller and J. T. Irvine, *Nature*, 2016, **537**, 528–531.
- 19 H. Lv, L. Lin, X. Zhang, D. Gao, Y. Song, Y. Zhou, Q. Liu, G. Wang and X. Bao, *J. Mater. Chem. A*, 2019, **7**, 11967–11975.
- 20 Y. Li, B. Hu, C. Xia, W. Q. Xu, J. P. Lemmon and F. Chen, *J. Mater. Chem. A*, 2017, **5**, 20833–20842.
- 21 J. Lu, C. Zhu, C. Pan, W. Lin, J. P. Lemmon, F. Chen, C. Li and K. Xie, *Sci. Adv.*, 2018, **4**, 1–8.
- 22 Y. Jiang, F. Chen and C. Xia, *J. Power Sources*, 2021, **493**, 229713.
- 23 J. Ko, B.-K. Kim and J. W. Han, *J. Phys. Chem. C*, 2016, **120**, 3438–3447.
- 24 C. Zhao, Y. Li, W. Zhang, Y. Zheng, X. Lou, B. Yu, J. Chen, Y. Chen, M. Liu and J. Wang, *Energy Environ. Sci.*, 2020, **13**, 53–85.
- 25 Y. Zheng, Z. Chen and J. Zhang, *Electrochem. Energy Rev.*, 2021, **4**, 508–517.
- 26 Y. Zheng, Y. Li, T. Wu, W. Zhang, J. Zhu, Z. Li, J. Chen, B. Yu, J. Wang and J. Zhang, *Nano Energy*, 2018, **51**, 711–720.
- 27 Y. Zheng, C. Zhao, Y. Li, W. Zhang, T. Wu, Z. Wang, Z. Li, J. Chen, J. Wang, B. Yu and J. Zhang, *Nano Energy*, 2020, **78**, 105236.
- 28 M. Sase, F. Hermes, K. Yashiro, K. Sato, J. Mizusaki, T. Kawada, N. Sakai and H. Yokokawa, *J. Electrochem. Soc.*, 2008, **155**, B793.
- 29 Y. Song, Y. M. Yin, L. Li, Z. Chen and Z. F. Ma, *Chem. Commun.*, 2018, **54**, 12341–12344.
- 30 X. Xi, J. Liu, Y. Fan, L. Wang, J. Li, M. Li, J.-L. Luo and X.-Z. Fu, *Nano Energy*, 2021, **82**, 105707.
- 31 Y. Zheng, Y. Li, T. Wu, C. Zhao, W. Zhang, J. Zhu, Z. Li, J. Chen, J. Wang, B. Yu and J. Zhang, *Nano Energy*, 2019, **62**, 521–529.
- 32 S. Liu, Q. Liu and J.-L. Luo, *J. Mater. Chem. A*, 2016, **4**, 17521–17528.
- 33 X. Xi, X.-W. Wang, Y. Fan, Q. Wang, Y. Lu, J. Li, L. Shao, J.-L. Luo and X.-Z. Fu, *J. Power Sources*, 2021, **482**, 228981.
- 34 D. Li, M. Lu, K. Aragaki, M. Koike, Y. Nakagawa and K. Tomishige, *Appl. Catal., B*, 2016, **192**, 171–181.
- 35 H. Wang and B. Wei, *Chin. Sci. Bull.*, 2011, **56**, 3416–3419.
- 36 K. Yuge, A. Seko, I. Tanaka and S. R. Nishitani, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 2005, **72**, 174201.
- 37 Z. Du, H. Zhao, S. Li, Y. Zhang, X. Chang, Q. Xia, N. Chen, L. Gu, K. Świerczek, Y. Li, T. Yang and K. An, *Adv. Energy Mater.*, 2018, **8**, 1800062.
- 38 M. Zhi, G. Zhou, Z. Hong, J. Wang, R. Gemmen, K. Gerdes, A. Manivannan, D. Ma and N. Wu, *Energy Environ. Sci.*, 2011, **4**, 139–144.
- 39 F. Sher, A. J. Williams, A. Venimadhev, M. G. Blamire and J. P. Attfield, *Chem. Mater.*, 2005, **17**, 1792–1796.
- 40 T. Chakraborty, C. Meneghini, A. Nag and S. Ray, *J. Mater. Chem. C*, 2015, **3**, 8127–8131.
- 41 L. Ye, C. Pan, M. Zhang, C. Li, F. Chen, L. Gan and K. Xie, *ACS Appl. Mater. Interfaces*, 2017, **9**, 25350–25357.
- 42 H. Falcon, *Appl. Catal., B*, 2004, **53**, 37–45.
- 43 Y. Tian, L. Zhang, Y. Liu, L. Jia, J. Yang, B. Chi, J. Pu and J. Li, *J. Mater. Chem. A*, 2019, **7**, 6395–6400.
- 44 J. D. Kirtley, S. N. Qadri, D. A. Steinhurst and J. C. Owrutsky, *J. Power Sources*, 2016, **336**, 54–62.
- 45 X. Zhang, Y. Song, F. Guan, Y. Zhou, H. Lv, Q. Liu, G. Wang and X. Bao, *J. Power Sources*, 2018, **400**, 104–113.