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Construction of single-atom copper sites with low coordination number for efficient CO₂ electroreduction to CH₄†

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Generally speaking, the preparation of single-atom catalysts always requires harsh conditions such as high-temperature pyrolysis or strong acid etching. In this manuscript, a simple and effective plasma-activated strategy is employed to synthesize a MOF-based single-atom copper catalyst. The bombardment of plasma forms abundant oxygen vacancies and significantly increases the number of low-coordinated catalytically active copper sites. Moreover, plasma treatment also creates a hierarchically porous structure, which can effectively adsorb the reactant molecules. The synergistic effect of the porous structure and low-coordinated copper sites dramatically improves the activity of CO₂ electroreduction to CH₄ with a maximum faradaic efficiency of 75.3%. Furthermore, the total faradaic efficiency of carbon-containing products (CO, CH₄ and C₂H₄) can reach as high as 96.5% with a partial current density of 47.8 mA cm⁻². Density functional theory (DFT) calculations confirm that the low-coordinated copper sites can be beneficial for the formation and further reduction of the key intermediate to CH₄. This strategy provides a successful example for the preparation of single-atom catalysts under mild conditions.

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Due to the advantage of high energy density, fossil fuels are still the leading choices in the global energy supply system. Unfortunately, the consumption of fossil fuels over several centuries is inevitably accompanied by serious direct environmental damage and massive CO₂ emission.¹ The growing atmospheric CO₂ levels bring forth irreversible environmental changes, global warming, ocean acidification and other issues, thereby threatening the sustainable development of mankind.² Therefore, energy conversion and storage technology based on electrochemical technology have received widespread attention.

Specifically, the electrocatalytic CO₂ reduction technology can utilize the greenhouse gas CO₂ and the surplus electricity from renewable energy to produce carbon-based fuels (such as C₂H₅OH, CH₄) and bulk chemicals (such as CO).^{3–5} The electrochemical reduction of CO₂ provides an effective technique for the development of renewable and environment-friendly energy utilization systems. However, the special linear structure of CO₂ endows it with high chemical inertia and stability.⁶ Hence, one of the key research fields of CO₂ electroreduction technology is to design and prepare efficient and stable electrocatalysts to activate CO₂ molecules.⁷ According to the

different active components, CO₂ electroreduction catalysts can be divided into noble metal catalysts^{8–14} (e.g., Au, Ag, Pd), non-noble metal catalysts^{15–21} (e.g., Fe, Co, Ni, Cu, Zn, Sn) and metal-free catalysts.^{22–27} Based on the size and dispersion of catalytically active species, they can also be divided into nano-structure catalysts and atom-scale catalysts.

In recent years, single-atom catalysts have shown great prospects in CO₂ electroreduction.^{28–34} Single-atom catalysts usually contain isolated metal atoms, which are highly dispersed on certain supports, including metal oxides, two-dimensional layered crystals and carbon materials. The distance between the isolated metal atoms is long enough to prevent the formation of a significant metal lattice.³⁰ This unique structure can maximally improve the utilization rate of metal atoms and greatly increase the selectivity of target products (e.g., CO, CH₄) in CO₂ electroreduction. The preparation of single-atom catalysts usually involves high-temperature heat treatment of specific precursors, e.g., metal-organic frameworks (MOFs) and crosslinked polymers.³¹ The pyrolysis of MOFs or polymer precursors could easily cause the generation of metal single atoms as well as metal nanoparticles. These nanoparticles always need to be removed by acid etching to obtain a single-atom catalyst, which is not in accordance with the basic principle of atom economy.³⁵

Based on the above reasons, we employed a kind of conjugated copper(II) catecholate MOFs (denoted as CuDBC) as

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potential catalysts for CO₂ electroreduction. After simple plasma gas bombardment, this Cu-DBC material can be utilized as a high-efficiency electrocatalyst for CO₂ reduction, involving no high-temperature pyrolysis. In the plasma-activated procedure, Cu-DBC retained the abundant pores, which could adsorb CO₂ molecules and accelerate the transfer of reactants to the active sites. In addition, the high energy plasma creates a large number of low-coordinated Cu sites, which could efficiently convert CO₂ into CH₄.

As described in Scheme 1, the CuDBC precursor was firstly synthesized from DBC ligand and Cu(OAc)₂ in a mixed solvent of deionized water and *N,N*-dimethylformamide (DMF) at 85 °C in a nitrogen atmosphere. In the CuDBC precursor, Cu²⁺ could coordinate with four O atoms to form the Cu–O₄–C moiety (Fig. S1†).³⁶ However, ligand doped copper sites with high coordination number can hardly be directly utilized as efficient catalytic sites for CO₂ reduction, due to the steric hindrance effect that blocks the adsorption of CO₂ molecules and intermediates on the inner Cu sites.³⁷ Consequently, the Cu-DBC precursor was further activated using high energy plasma treatments with 100 W O₂ for 20 minutes. The as-synthesized powder was named plasma activated CuDBC (PA-CuDBC-1). The microstructures of the CuDBC precursor and PA-CuDBC-1 were characterized *via* scanning electron microscopy (SEM) and transmission electron microscopy (TEM). As revealed in Fig. 1a, b and S2,† CuDBC shows long and crystallized nanorods with approximately several micrometres length and around 100 nanometers width. In addition, CuDBC has a flat and smooth surface, and no obvious holes are found on the crystal surface.

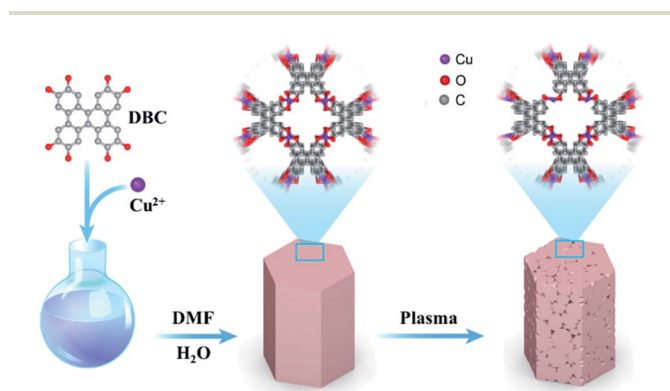
After the plasma treatment, PA-CuDBC-1 retains the overall structure of long and crystallized nanorods (Fig. 1c) of CuDBC. Compared with the flat and smooth surface of CuDBC, the surface of PA-CuDBC-1 tends to be chapped and rough after plasma treatment (Fig. 1c, d and S3†). It is notable that plasma bombardment did not cause fundamental damage to the crystal structure of the CuDBC, which could be proved by the obvious lattice stripes in high resolution TEM images (Fig. 1e). Furthermore, energy dispersive spectroscopy mapping (EDS, Fig. 1f) exhibits the uniform dispersion of C, O and Cu elements on the PA-CuDBC-1 skeleton. Therefore, the 20 minute plasma



Fig. 1 (a) SEM and (b) TEM images of pristine CuDBC; (c) SEM and (d and e) HR-TEM images of PA-CuDBC-1, respectively; (f) EDS mapping images for C, O, and Cu of PA-CuDBC-1.

treatment of PA-CuDBC-1 did not lead to the aggregation of copper single sites into copper nanoparticles.

X-ray diffraction (XRD) was also employed to uncover the potential structural change of PA-CuDBC-1. XRD patterns (Fig. 2a) of CuDBC and PA-CuDBC-1 show similar sharp peaks, indicating the high crystallinity of both samples. No obvious diffraction peaks of metallic Cu are observed, ruling out the generation of Cu nanoparticles in plasma activation. PA-CuDBC-1 was further treated with 100 W O₂ plasma for another 20 minutes, and named PA-CuDBC-2. Compared to CuDBC and PA-CuDBC-1, the XRD pattern of PA-CuDBC-2 (Fig. 2a, inside the dashed frame) presents significant weakness in the diffraction peaks between 25° and 30°.³⁶ Besides, some small Cu nanoparticles can be seen in the TEM images of PA-CuDBC-2, implying the disintegration of the metal organic frameworks and aggregation of Cu ions using 40 minute O₂ plasma bombardment (Fig. S4†). In the Fourier transform infrared spectroscopy (FT-IR, Fig. 2b) of the three samples, two major peaks around 1580 and 1395 cm⁻¹ are observed, indicating the C–O asymmetric and symmetric stretching vibrations in the CuDBC structure.³⁸ Moreover, the N₂ sorption isotherms of PA-CuDBC-1 manifest an apparent hysteresis loop at high relative pressures, which is attributed to the type-IV or mesoporous structure. The curve of pore size distribution also reveals the abundant mesopores in PA-CuDBC-1 (Fig. 2c). In contrast, CuDBC displays typical type I adsorption and desorption isotherms (Fig. S5†). The Brunauer–Emmett–Teller (BET) surface area is 86.0 and 265.1 m² g⁻¹ for CuDBC and PA-CuDBC-1, respectively. It is worth noting that PA-CuDBC-2 (Fig. S6†) only has a specific surface area of 137.0 m² g⁻¹, because of the



Scheme 1 Schematic illustration of the preparation method of PA-CuDBC-1.

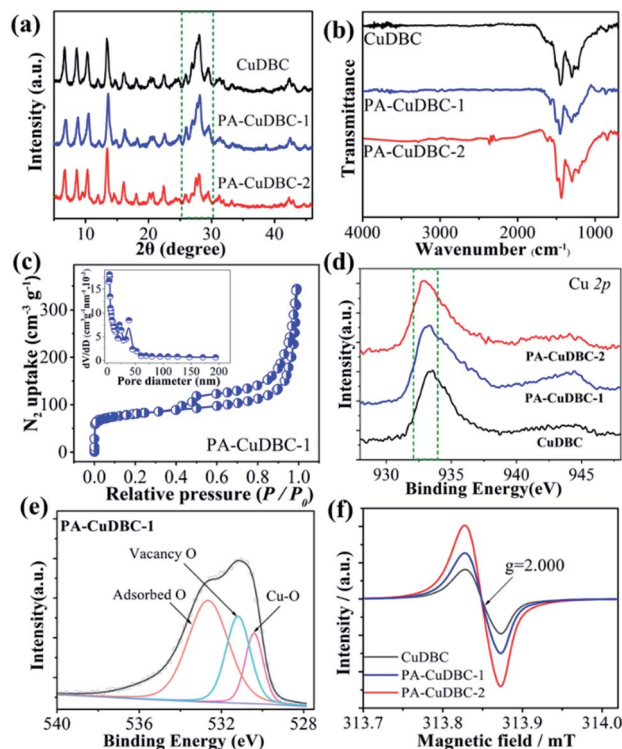


Fig. 2 (a) XRD patterns and (b) FT-IR spectra of the three samples; (c) N_2 sorption isotherms of PA-CuDBC-1, inset shows the pore size distribution; (d) Cu 2p XPS spectra of the three samples; (e) O 1s XPS spectra of PA-CuDBC-1; (f) EPR profiles of the three samples.

destruction of micropores under continuous plasma bombardment.

To explore the chemical composition and coordination environment, all three samples were characterized by X-ray photoelectron spectroscopy (XPS). The XPS survey spectra of the three samples prove the coexistence of Cu, O and C (Fig. S7†). The Cu 2p fine spectra (Fig. 2d and S8†) of the three samples display a characteristic peak at around 933 eV, corresponding to Cu 2p_{3/2} for Cu²⁺ species. Compared to the values of CuDBC, a slight binding energy shift can be detected in PA-CuDBC-1, which could be attributed to the lower oxygen coordination number around copper sites. The high-resolution O 1s spectra of the three samples (Fig. 2e) can be deconvoluted into three subpeaks of Cu–O, vacancy O and adsorbed O, respectively. Specifically, PA-CuDBC-1 shows a larger peak area of vacancy O than CuDBC and PA-CuDBC-2 (Fig. S9–S11†). This binding energy shift and vacancy O peaks in XPS spectra manifest the improvement of oxygen vacancies in plasma activated CuDBC samples.³⁹ Electron paramagnetic resonance (EPR) spectra (Fig. 2f) were also obtained to further study the oxygen vacancy. PA-CuDBC-1 and PA-CuDBC-2 exhibit very strong signals at $g = 2.000$ induced by the oxygen vacancy.^{37,39} These abundant oxygen vacancies and low coordinated copper sites (Fig. S12†) were caused by the bombarding of high energy O₂ plasma, which have great potential in CO₂ electro-reduction.

As mentioned above, PA-CuDBC-1 not only has a hierarchically porous structure, but also possesses a large number of low



Fig. 3 (a) LSVs of PA-CuDBC-1 in N_2 or CO_2 -saturated 0.5 M $KHCO_3$ electrolyte; (b) LSVs of the three samples in CO_2 -saturated 0.5 M $KHCO_3$ electrolyte; product distribution and Faraday efficiencies with error bars of (c) PA-CuDBC-1, (d) CuDBC and (e) PA-CuDBC-2, and error bars correspond to the standard deviation of three independent measurements; (f) partial current densities of carbon-containing products.

coordination copper single-atom sites, which might have great potential in CO₂ electroreduction. To evaluate and compare the CO₂ reduction activities, all the three samples are powdered and drop-cast on a piece of carbon paper *via* polymer binders to obtain a useful working electrode in a two-chamber electrolytic cell. Linear sweep voltammetry (LSV) of all samples was conducted in a N_2 - or CO_2 -saturated 0.5 M $KHCO_3$ solution with a scan rate of 0.01 V s⁻¹. As displayed in Fig. 3a, the LSV curve of PA-CuDBC-1 increases significantly around $-0.5 V_{RHE}$ cathode potential in the N_2 -saturated electrolyte, due to hydrogen evolution, while the current density increases sharply at approximately $-0.35 V_{RHE}$ potential in the CO_2 -saturated electrolyte. Furthermore, much higher current density could be observed in the CO_2 -saturated solution from $-0.35 V_{RHE}$ to $-1.15 V_{RHE}$ cathode potential, due to the additional CO₂ reduction currents of the PA-CuDBC-1 catalyst.³⁰ Notably, PA-CuDBC-1 shows much higher current densities in CO_2 -saturated 0.5 M $KHCO_3$ solution than CuDBC and PA-CuDBC-2, e.g., 22.2 mA cm⁻² (CuDBC), 30.1 mA cm⁻² (PA-CuDBC-2) and 36.5 mA cm⁻² (PA-CuDBC-1) at $-0.9 V_{RHE}$ (Fig. 3b). The current densities indicate the enhanced catalytic activities of PA-CuDBC-1 in CO₂ reduction.

In LSV curves, the current densities were all increased in CO_2 -saturated $KHCO_3$ solution, demonstrating the existence of the CO₂ reduction procedure. To determine the product

distribution in CO₂ electroreduction, potentiostatic electrolysis using CuDBC, PA-CuDBC-1 and PA-CuDBC-2 catalysts with cathode potentials from $-0.5 V_{\text{RHE}}$ to $-1.3 V_{\text{RHE}}$ was conducted in 0.5 M KHCO₃ electrolyte. The reduction products were qualitatively and quantitatively detected by nuclear magnetic resonance (NMR) and gas chromatography (GC). In this research, no (or only trace) liquid products were observed throughout the applied potentials. For all three samples, H₂, CO, CH₄ and C₂H₄ are the main reduction products with $\sim 100\%$ total faradaic efficiencies (FE, Fig. 3c–e). For PA-CuDBC-1 (Fig. 3c), H₂ and CO are the dominant reduction products at applied potentials before $-0.7 V_{\text{RHE}}$. PA-CuDBC-1 brings forth the highest CO FE (52.6%) at $-0.5 V_{\text{RHE}}$ and a H₂ FE of 33.5%, along with a CH₄ FE of 12.4% and a little amount of C₂H₄ (1.5%). When the potentials increased to $-0.8 V_{\text{RHE}}$ and $-0.9 V_{\text{RHE}}$ applied potential, the H₂ FE declined to 30.8% and 28.4%, and the CO FE decreased to 37.2% and 27.0%, respectively. In contrast, the faradaic efficiencies of CH₄ and C₂H₄ improve from 2.9% to 26.5% and 0% to 5.5%, when the potentials increase from $-0.6 V_{\text{RHE}}$ to $-0.8 V_{\text{RHE}}$. If the applied potentials are higher than $-0.9 V_{\text{RHE}}$, the main reduction product turns out to be CH₄. PA-CuDBC-1 produces the highest CH₄ FE of 75.3% at $-1.1 V_{\text{RHE}}$ along with a C₂H₄ FE of 7.1%, and the CO FE and H₂ FE reduce to 14.1% and 3.5%, respectively. Under the same reaction conditions using CuDBC catalyst, the corresponding faradaic efficiencies of H₂, CO, CH₄ and C₂H₄ are also summarized in Fig. 3d. H₂ and CO are the major products in the whole range of applied potentials, with a small amount of CH₄ and C₂H₄. The highest faradaic efficiency of CO is 44.9% at $-1.0 V_{\text{RHE}}$, and the highest faradaic efficiency of CH₄ is 12.1% at $-1.2 V_{\text{RHE}}$ cathode potential. PA-CuDBC-2 exhibits similar product distribution and tendency to PA-CuDBC-1 (Fig. 3e). The CH₄ FE reaches the maximum value (37.3%) at $-1.2 V_{\text{RHE}}$, with a CO FE of 20.6%, a C₂H₄ FE of 10.1% and a H₂ FE of 32.0%. Although PA-CuDBC-2 achieved significantly lower CH₄ FE than CuDBC-1, it also achieved the highest C₂H₄ FE (12.0%) among the three catalysts.

Intriguingly, both PA-CuDBC-1 and PA-CuDBC-2 engender obviously higher faradaic efficiencies of carbon-containing products than CuDBC. As demonstrated above, the high energy plasma created a plenty of oxygen vacancies and low coordinated copper sites in PA-CuDBC-1 and PA-CuDBC-2. These low coordinated metal sites have more vacant coordination sites and less steric hindrance, which might favour the CO₂ adsorption and activation.^{40,41} Besides, the current densities are presented against the corresponding overpotentials to obtain a Tafel plot (Fig. 4a). A 163 mV dec⁻¹ Tafel slope is observed for PA-CuDBC-1, which is related to the first electron transfer to CO₂ molecule.^{25,26} In addition, the Tafel slope for PA-CuDBC-1 (163 mV dec⁻¹) is much lower than those of PA-CuDBC-2 (262 mV dec⁻¹) and CuDBC (388 mV dec⁻¹), indicating the faster initial electron transfer to CO₂ molecules and higher activity in CO₂ reduction. Electrochemical impedance spectroscopy (EIS) characterizations are also conducted to explore the electrical conductivity of the three catalysts.¹¹ The resistance value is calculated according to the EIS (Fig. 4b), which proves the lowest charge-transfer resistance of PA-CuDBC-1 compared

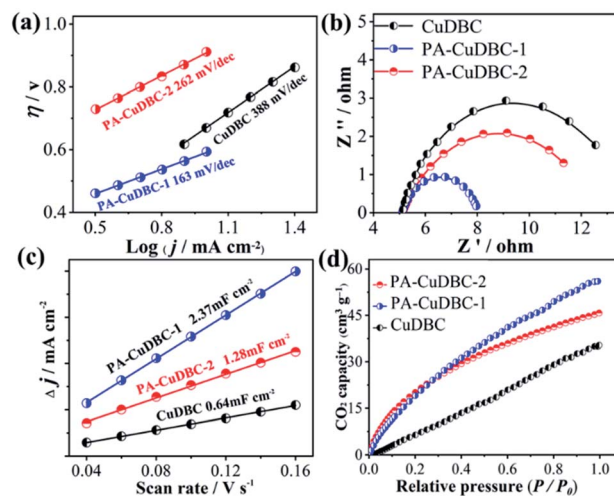


Fig. 4 (a) Tafel plots, (b) EIS and (c) ECSA of the three samples; (d) CO₂ adsorption capacity of the three samples.

to PA-CuDBC-2 and CuDBC, further proving that PA-CuDBC-1 is beneficial for the electron transfer in CO₂ reduction.

Besides the higher faradaic efficiencies, the partial current densities of all carbon-containing products (CO, CH₄ and C₂H₄) for PA-CuDBC-1 are also significantly larger than those of CuDBC and PA-CuDBC-2 (Fig. 3f). For example, 26.5, 36.8 and 47.8 mA cm⁻² partial current densities were obtained using CuDBC, PA-CuDBC-1 and PA-CuDBC-2, respectively, at $-1.1 V_{\text{RHE}}$ applied potential. As characterized above, PA-CuDBC-1 has a larger specific surface area and hierarchically porous structure, because of the plasma bombardment (Fig. 1c and 2c). This superior structure can bring about much higher electrochemical active area (ECSA, Fig. 4c and S13[†]), where the CO₂ reduction procedure occurs. The hierarchically porous structure also increases the adsorption capacity of CO₂ molecules (Fig. 4d) and enhances the CO₂ content around the copper sites for CO₂ reduction reaction,²⁶ eventually leading to the higher partial current densities of PA-CuDBC-1. Since the durability is also an important specification for CO₂ electro-reduction,^{6–8} the long-term electrolysis of PA-CuDBC-1 was carried out at $-1.1 V_{\text{RHE}}$ applied potential for 50 hours (Fig. S14[†]). The total current density can retain a stable value of $\sim 52 \text{ mA cm}^{-2}$ with slight decrease, indicating the excellent stability. After all the electrolysis experiments, SEM, TEM, XRD and FTIR analysis of the PA-CuDBC-1 sample were conducted. As shown in Fig. S15,[†] PA-CuDBC-1 still retained the structure of long and crystallized nanorods. There are no obvious metallic clusters or nanoparticles in the SEM or TEM images, and no diffraction peaks of metallic Cu are observed in XRD patterns, excluding the accumulation of single-atom Cu sites during electrolysis. Moreover, the characteristic peaks of C–O stretching vibration are still observed in the FTIR, proving the good stability of PA-CuDBC-1 during CO₂ reduction. Therefore, PA-CuDBC-1 is indeed a stable and high-performance catalyst for CO₂ electro-reduction.

According to Fig. 3c–e, CO and CH₄ are the main products with only a small fraction of C₂H₄ from CO₂ reduction using all

the three samples. Since copper single atoms are the dominant active sites in CuDBC, PA-CuDBC-1 and PA-CuDBC-2, the large distance between copper atoms in these catalysts can hardly facilitate effective C–C bond coupling to produce C^{2+} products.^{16,17} PA-CuDBC-2 can generate the highest C_2H_4 FE (12.0%) among the three catalysts, attributed to the aggregation of Cu ions into Cu nanoparticles during long-time plasma bombardment. As for the production of CH_4 , adsorbed CO on active sites ($*CO$) has been reported to be a crucial reaction intermediate. The adsorbed $*CO$ intermediate would then go through an electro-hydrogenation procedure to $*CHO$, eventually leading to the generation of CH_4 .^{41–43} Density functional calculation (DFT) based computational methods are introduced to understand the high selectivity of CH_4 on PA-CuDBC-1. The Cu active sites of CuDBC were simplified and simulated as a $Cu-O_4-C$ (Fig. S16†) structure within a single-layer, while the low-coordinated Cu sites in PA-CuDBC-1 and PA-CuDBC-2 were modelled as $Cu-O_3-C$ (Fig. S17†) and $Cu-O_2-C$ (Fig. S18†) structure within a single-layer. According to our calculations, the transformation from CO_2 into $*COOH$ with the three structures are all uphill type in the free energy profiles, indicating the rate determining step.^{19–21} $Cu-O_2-C$ presents the lowest free-energy (ΔG , 0.31 eV) for this procedure, followed by $Cu-O_3-C$ (0.43 eV), and $Cu-O_4-C$ (1.02 eV). The $*COOH$ intermediate would be further reduced to a $*CO$ and $*CHO$ species with a coupled proton and a transferred electron. $Cu-O_2-C$ and $Cu-O_3-C$ both exhibit much lower energy barriers than $Cu-O_4-C$. Therefore, the lower energy barriers of $Cu-O_2-C$ and $Cu-O_3-C$ are well consistent with the low-coordinated copper sites in PA-CuDBC-1, leading to the highest CH_4 selectivity in CO_2 electro-reduction (Fig. 5).

In conclusion, a MOF-derived single-atom Cu catalyst, PA-CuDBC-1, was prepared *via* simple and effective plasma

treatment under mild conditions. PA-CuDBC-1 possesses abundant low-coordinated copper sites and a hierarchically porous structure, which was utilized as an efficient catalyst for electrochemical reduction of CO_2 . PA-CuDBC-1 could produce the highest CH_4 FE of 75.3% at $-1.1 V_{RHE}$ applied potential along with a C_2H_4 FE of 7.1%, a CO FE of 14.1% and a H_2 FE of 3.5%, respectively. The total faradaic efficiency of carbon-containing products (CO, CH_4 and C_2H_4) can reach 96.5% with a partial current density of 47.8 mA cm^{-2} , which are significantly better than that of pristine CuDBC without plasma activation. DFT calculations demonstrate that the low-coordinated copper sites, $Cu-O_3-C$ and $Cu-O_2-C$, can decrease the energy barrier for the formation of the key intermediate, and accelerate the kinetic process for the reduction of CO_2 to CH_4 . This strategy provides a good example of efficient catalysts for CO_2 reduction and also shows feasibility for the preparation of other single-atom catalysts.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

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Fig. 5 (a) Optimized structures of $Cu-O_2-C$, $Cu-O_3-C$ and $Cu-O_4-C$ moieties; (b) free energy diagram of CO_2 to $*COOH$, $*CO$ and $*CHO$ intermediates on $Cu-O_2-C$, $Cu-O_3-C$ and $Cu-O_4-C$ structures.

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