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## Perspectives regarding metal/mineral-incorporating materials for water purification: with special focus on Cr(vi) removal

Khalid Z. Elwakeel,<sup>id</sup>\*<sup>ab</sup> Ahmed M. Elgarahy,<sup>c</sup> Ziya A. Khan,<sup>a</sup> Muath S. Almughamisi<sup>a</sup> and Abdullah S. Al-Bogami<sup>a</sup>

Metal/mineral-incorporating materials have received significant attention over the last decades given the outstanding adsorption behavior towards various pollutants, especially Cr(vi), in aqueous solutions. Here, the pattern of sorption of some pollutants with special focus on Cr(vi) removal over metal/mineral-incorporating materials has been compiled. Furthermore, the key influencing adsorption variables, *i.e.*, pH, concentration at the beginning, contact time, and dosage of sorbent, were discussed while considering different material classifications. Different isothermal and kinetic models were elaborated. Langmuir and Freundlich's models are adopted as the main sorption isotherms, while the pseudo-second-order kinetic model is the most fitted heavy metal ion and Cr(vi) kinetic model in aqueous systems. The results revealed that metal/mineral-incorporating materials are quite effective for heavy metal (especially Cr(vi)) recovery from water and confirmed that these materials are affordable and reliable for contaminated water remediation. Also, several methods are available for the modification of these materials in order to increase their sorption efficiency. However, to establish the use of metal/mineral-incorporating materials for water purification compared with other established methods, more investigations are required to determine the best modification method and investigate the release of metals from these materials during sorption.

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### 1. Introduction

Pollution refers to the contamination of water by foreign matter such as microorganisms, chemicals, and industrial or other waste or sewage.<sup>1</sup> Among essentials for human beings, water is vital. Water contamination renders it undrinkable and not suitable for human consumption. The foremost consequence of water pollution is severe damage to the ecosystem. Changes in natural water's chemical or physical properties affect aquatic biodiversity and the usability of water. There are ecological, social, and economic identifiers.<sup>2</sup> Pollution of water occasioned by different toxic contaminants, mostly including heavy metals, organics, and oil, has steadfastly become one of the most impactful environmental challenges globally.<sup>3</sup> Water is usually taken for granted when produce safety is taken into consideration. Not only it is vital for crop growth but also in their processing as well. Water usage spans multiple functions: produce cooling,

decontamination, debris removal, personal hygiene, and equipment washing.<sup>4</sup> Water contamination takes place within and outside of cities. Although in-city contamination impacts fewer water tables, it can severely affect not only water procurement and quality but also public health.<sup>5</sup> Water pollution is the presence of chemical, physical, or biological components or factors affecting water's integrity, although certain natural events can cause water pollution.<sup>6</sup> Water pollution is becoming increasingly serious in coastal waters. To make full use of marine resources and develop the marine economy, national authorities are paying increasing attention to this issue.<sup>7</sup> The release of residential and modern waste spillage from water tanks, marine dumping, radioactive waste, and climactic effects are significant causes of water contamination. Water pollutants are categorized as point or nonpoint sources.<sup>8</sup> The type of contaminant depends on the nature of the business. Lethal metals enter into water and decrease the drinkability of water.

In environmental pollution, heavy metals mainly refer to mercury, cadmium, chromium, lead, and arsenic, which have significant biological toxicity. Usually, the natural background concentrations of heavy metals do not reach harmful levels. Poisonous and harmful metals get into the atmosphere, water, and soil and cause serious environmental pollution because of

<sup>a</sup> University of Jeddah, College of Science, Department of Chemistry, Jeddah, Saudi Arabia. E-mail: kelwakeel@uj.edu.sa, khalid\_elwakeel@sci.psu.edu.eg

<sup>b</sup> Environmental Science Department, Faculty of Science, Port-Said University, Port-Said, Egypt

<sup>c</sup> Zoology Department, Faculty of Science, Port-Said University, Port-Said, Egypt



human activities such as heavy metal mining. As major toxicants, heavy metals are found in industrial wastewater and possess severe effects on wastewater biological treatment. Heavy metals' sources in wastewater treatment plants are from industrial discharge and urban stormwater runoff. Some of the heavy metals, *e.g.*, Cd, Cr, Pb, Hg, and Ag, are priority pollutants. Heavy metal toxicity is caused by the fact that they are soluble metals. The toxicity is managed by various factors such as pH and the type and concentration of complexing agents in wastewater.<sup>9</sup> Due to their discharge into the environment, heavy metal concentrations in sediments and suspended solids in water have increased sharply and major water pollution problems have occurred.<sup>10</sup> Many heavy metals, especially at high concentrations, are deadly to even the most resistant species of bacteria, algae, and fungi. Therefore, in many cases of highly contaminated industrial wastewater, biological treatment would be impractical or even impossible.<sup>11</sup> High concentrations of trace metals can also be found in groundwater near contaminated sources; however, these may pose potential health threats. Some trace constituents are associated with industrial pollution, such as As(v) and Cr(vi).<sup>12,13</sup> Chromium is present in the zerovalent state, while in the environment, trivalent and hexavalent chromium species are the most thermodynamically stable. Hexavalent chromium usually occurs as  $\text{CrO}_4^{2-}$  or  $\text{HCrO}_4^-$ , whereas Cr(III) as  $\text{Cr}(\text{OH})_3$ . Chromium(III) is an essential nutrient while Cr(vi) is strongly carcinogenic.<sup>14</sup> It has long been recognized that Cr(III) occurs naturally in most environmental media, while Cr(vi) only naturally in groundwater.

The World Health Organization recommended the total value of chromium in drinking water to be  $0.05 \text{ mg L}^{-1}$ .<sup>15</sup> The European Union has also recommended the same value in its council directive 98/83/EC on drinkable water quality.<sup>16</sup> However, the United States Environmental Protection Agency has established  $0.1 \text{ mg L}^{-1}$  as the maximum allowed contaminant level for total chromium.<sup>17</sup>

Chromium(vi) is one of the most toxic heavy metals existing in wastewater. Until now, various adsorbents were broadly tested for the displacement of Cr(vi) from contaminated water, but the results illustrate a low and hindered adsorption capacity. Chromium, as well as its compounds, is usually used in steel production and metallurgy, the chemical industry, leather tanning, protection and decorative coatings, the automotive industry, pigment manufacture, and wood treatment. Due to such an extensive range of use, large amounts of chromium are released into the atmosphere and terrestrial and aquatic environments. As a result of developed industrial activities, huge amounts of chromium-rich waste materials are generated.<sup>18</sup> Waste from the steelmaking industry may often be reused in civil engineering, while other chromium-containing waste materials are in general disposed of.<sup>19</sup> In nature, under environmental conditions, Cr(III) species prevail, while Cr(vi) compounds are mainly of anthropogenic origin. The essentiality and toxic nature of Cr depend primarily on its chemical forms. Generally, Cr(III) compounds are of lower toxicity compared with Cr(vi). Cr(III) is a crucial micronutrient present in glucose and lipid metabolism. For minimizing the health

hazards of Cr(vi) to occupationally exposed workers, the Occupational Safety and Health Administration standardized the limits of exposure to Cr(vi) compounds in the workplace. Chromium(vi) usage is limited by different regulative acts, and measures are also taken to diminish the environmental impacts of disposed of and reused chromium waste materials.<sup>20</sup> The soluble Cr(vi) species are readily released into soil solution and ground- and surface water and can be taken up by plants. To prevent harmful effects of Cr(vi) on terrestrial and aquatic environments and safely dispose of or reuse chromium-rich waste materials, reliable determination of Cr(vi) is of paramount importance.<sup>21</sup> Accurately determining Cr(vi) is also crucial in the investigations of the oxidation–reduction processes of Cr in soil and the evaluation of the efficiencies of the remediation processes of Cr-contaminated soil. Chromium(vi) exists in aqueous solution in the form of dichromate ( $\text{Cr}_2\text{O}_7^{2-}$ ), hydrochlorate ( $\text{HCrO}_4^-$ ), or chromate ( $\text{CrO}_4^{2-}$ ).<sup>22</sup> These anionic species are usually not adequately adsorbed by negatively charged soil particles due to the nonrepulsive electrostatic interaction. Therefore, Cr(vi) is capable of mobility and prevails only in aqueous solutions. Most chromite mine discharge water contains higher Cr(vi) concentration and electroplating effluent and ferrochrome, and leather tanning industries contain even higher Cr(vi) concentrations than the permissible limit.<sup>23</sup> Chromium compounds, of some significance considering human intake of the metal, can be used as an additive in water to prevent corrosion in industrial and various cooling systems. Opinions suggest that this utilization could cause a significant amount of environmental contamination from industrial emissions. As we will elaborate later, chromium salt utilization as a passivation agent on tin plate sometimes causes high levels of contamination in tinned foodstuffs. Although water may contain chromium, especially if it is affected by industrial emissions, it is not likely to account for impactful contributions to dietary intake of the element. Chromium's common form in drinking water is Cr(vi) and it is more soluble than hydrated Cr(III) oxide.<sup>22</sup>

Conditions have been documented in which residents in the vicinity of a chromium-contaminated site were potentially exposed to Cr(vi) in their drinking water at levels up to 10 ppm.<sup>24</sup> Whether prolonged exposure to low concentrations of Cr(vi) in drinking water can lead to cancer is directly related to the current concern about the dangers of environmental exposure to Cr(vi). Subsequent poor disposal practices, such as dumping of Cr(vi) into unlined ponds, have led to Cr seepage into waterways and consequent contamination of irrigation and drinking water.<sup>25</sup> Chromium compounds' emissions in water and air are mainly caused by chemical manufacturing industries (rubber, dyes, pharmaceuticals, and plastic products). In humans, sufficient evidence exists for the carcinogenicity of Cr(vi) compounds which are found in chromate production, chromate pigment production, and chromium plating industries.<sup>26</sup> Extremely toxic contaminants like As(v), Cr(vi), and Pb(II) were found in the chrome-tanning process of animal skin to produce leather; these industries were located in Riyadh and Jeddah, in Saudi Arabia, industrial cities.<sup>27</sup> Chromium enters the oceans in two-way riverine discharge



and atmospheric deposition. Almost no rivers flow into the Red Sea; hence, the major likely source of higher concentrations of Cr near Al Wahj and Jazan could be atmospheric deposition, activities of the Al Wajh Port, or wastewater streams from the local community.<sup>28</sup> Chromium abundantly exists in the Earth's crust; its level in groundwater depends on the nature of the crust and the rocks in any given area. Accordingly, relatively high concentrations were detected in Makkah wells, though still below international and local standards.<sup>29</sup> Different studies illustrated that Cr(VI) compounds can increase lung cancer risk, and that ingesting large amounts can cause ulcers, upset stomach, convulsions, and liver and kidney damage, and could even cause death.

## 2. Traditional wastewater treatment technologies

The main vulnerability of surface water is its ability to be contaminated by industrial and municipal emissions and runoff and soil erosion. Excessive turbidity and pollution cause numerous unwanted tastes, odors, and colors of water.<sup>30</sup> Industries not only cause physical damage to river systems through direct water withdrawal and water infrastructure but also pollute the river qualitatively.<sup>31</sup> Surface water is contaminated from industrial, agricultural, and domestic chemicals that enter from the surface

by inorganic chemicals that are water soluble, such as acids, salts, and toxic metal compounds such as lead and mercury. These dissolved solids can render water undrinkable, affect fish and other aquatic life, diminish crop yields, and expedite corrosion of equipment that uses water.<sup>32</sup> Many of these industries' factories are situated along the banks of rivers, such as steel and pulp and paper industries' factories, due to their requirement for huge amounts of water in their manufacturing processes. Their waste contains acid and alkali derivatives, dyestuffs, and other chemicals that are dumped into rivers as effluents. Chromium salts are used in industrial processes for the production of sodium dichromate and other compounds containing Cr(VI).<sup>33</sup>

Because of the undesirable inhibitory properties in terms of water pollution caused by dyes and heavy metals, elimination of these pollutants from wastewater is key. Several methods including physical, mechanical, chemical, thermal, and biological methodologies are applied to remove these pollutants from water systems. Ion exchange,<sup>34</sup> precipitation,<sup>35</sup> flocculation/coagulation,<sup>36</sup> photo oxidation,<sup>37</sup> phytoextraction,<sup>38</sup> electrocoagulation,<sup>39</sup> electrodialysis,<sup>40</sup> irradiation,<sup>41</sup> membrane separation,<sup>42</sup> ultrafiltration,<sup>43</sup> forward osmosis,<sup>44</sup> and microorganisms and plants<sup>45–47</sup> are applied to remove dyes and heavy metals from water bodies. Generally, wastewater treatment scenarios can be categorized into mechanical, chemical, physical, thermal, and biological methods as displayed in Fig. 1.



Fig. 1 Different strategies for water and wastewater treatment.



### 3. Adsorption

Nowadays, the treatment of wastewater from different pollutants, such as heavy metals, is a worldwide necessity. Challenges related to pollution caused by heavy metals necessitate effective methods for their decontamination. Adsorption is an eco-friendly method to ameliorate this problem. It possesses a lot of potential in wastewater treatment as it is efficient and not costly. Yet, the majority of these complicated processes could introduce some challenges, *e.g.*, high costs, inefficiency in low-concentration pollutants, huge time consumption, reagents and energy, and formation of chemical sewage sludge.<sup>48,49</sup> Based on the famous comment of Albert Einstein, “We can’t solve our problems by using the same kind of thinking we used when we created them.”, it is time to come up with alternative, greener, and cheaper technology for eliminating contaminants from water efficiently. The advantages of adsorption over other technologies can be summarized as:

- Extract a large number of pollutants over a wide pH range
- Fast kinetics
- Easy handling and low space
- Regenerability
- Low cost
- No chemical sludge

#### 3.1. Adsorption fundamentals

Adsorption, as a practical application of sustainable development, is applied and considered as an economically efficient and ecofriendly technique for reducing various contaminant

concentrations in different water resources, *e.g.*, drinking water, to the optimal limits advised by various federal regulations all over the world.<sup>50–52</sup> The green protocol conforms with green chemistry principles. The fundamentals involved in the adsorption process are related to its ingredients. Briefly, adsorption is a metabolism-independent process (passive uptake) utilizing non-living biomass to get rid of various water pollutants. In general, this process yields many benefits because of recycling biomass (biowaste). Application in the original and/or altered forms minimizes waste, rectifying various environmental and ecological issues.<sup>51</sup> It also is characterized by exemplary merits, *e.g.*, low operating and manufacturing costs, availability, flexibility, minimal energy requirements, easy operation, and high efficiency. Fig. 2 presents different water pollutants’ sorption on various low-cost biosorbents.

#### 3.2. Adsorption strategy

Recently, the concept of adsorption as a multidimensional effective process has been evolving. It is considered as an admirable alternative to other orthodox technologies for wastewater decontamination. Sorption is a physicochemical phenomenon where gas or liquid molecules (the sorbate) concentrate on the surface of another substance (the sorbent). A sorbate is a material that gathers at the sorbent surface, while a sorbent is the substance whose surface hosts sorption, yielding high-quality purified effluents. Despite the presence of “bio” as a prefix, adsorption simply defined is a physicochemical process where target sorbate molecules are captured from aqueous

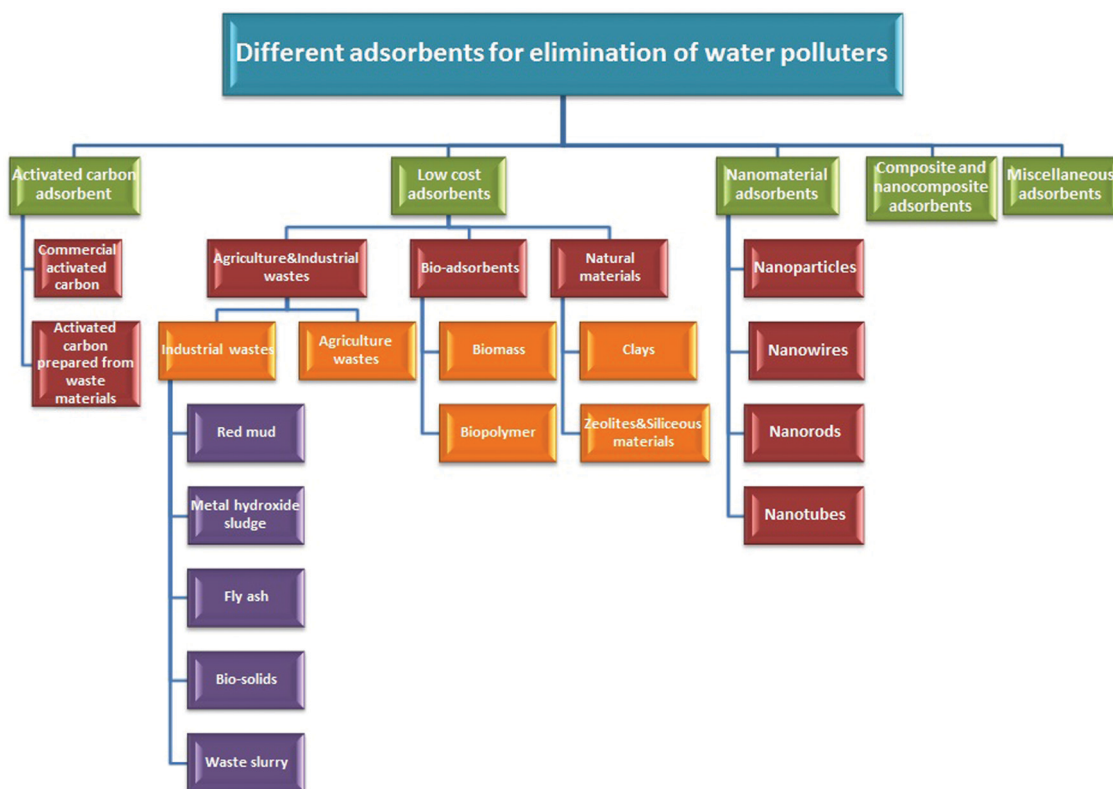


Fig. 2 Various types of water pollutant adsorbents.





solutions *via* a biological matrix. Absorption is the incorporation of a substance from one state into another substance with a different state, *i.e.*, gases absorbed by water or liquids absorbed by a solid, into a three-dimension matrix. Adsorption, on the other hand, is a physical attachment in which a sorbate, *i.e.* molecules and/or ions, interacts with a solid surface of another molecule (the sorbent), resulting in a sorbent–sorbate interface, *i.e.*, into a two-dimensional surface.<sup>53</sup>

Adsorption can be described as a metabolically independent and passive process that covers all interactions between any sorbate and biological matrix (biosorbent). It is crucial to many naturally occurring processes in different scientific disciplines, *e.g.*, biotechnology, life sciences, and medical approaches.

### 3.3. Selection of adsorbents

The adsorbent adequacy is known to be the most vital factor dictating the selection and preparation of a biosorbent. Considering cost and biomass origin as vital requirements as well, these two factors represent crucial criteria affecting the selection of the biosorbent. Dead biomass seizing priority over viable biomass stands out as a preferable technology applied for contending with various water pollutants. Utilizing dead biomass possesses many advantages such as the following: (1) there is no need for nurture, *i.e.*, nutrients and media, to be contained in the feed solution. (2) Toxicity is not a factor. (3) Saturated biosorbents and sorbed pollutants can be reused and recovered, respectively. (4) It is easier to model, mathematically and statistically, the pollutant uptake. To ensure the potential for a biosorbent to detoxify water pollutants, the biosorbent should possess various parameters such as being ecofriendly, biocompatibility, availability, and cost efficiency. Other merits of biosorbents are high sorptive performance towards target pollutants under different physicochemical parameters, *i.e.*, temperature, pH, *etc.*, and good stability under acidic/alkaline conditions with capacity for sequential sorption of various pollutants. Economically and environmentally, recyclability and adaptability to various designs, *i.e.*, fixed-bed systems, batch, are crucial features for the established biosorbents.<sup>54</sup> Some believe in waste as wealth—to be treated as a valuable resource; accordingly, this available waste should be treated with the utmost attention and care since utilizing it offers promising subject with a lot of benefits due to its environmentally benign nature. Reusing this waste is economically beneficial because it eliminates disposal problems while generating revenue for various industries. In reality, the plentiful biological materials structurally differ with the presence of various ligands such as amino, alcohol, aldehyde, hydroxyl, carboxylic, thiol, phosphate, ketone, phenolic and ether groups to different degrees with the capacity of interacting with target pollutants through various mechanisms, hence enhancing their sorption processes. The adsorption capacities of different biosorbents towards multiple pollutants were investigated and reported in thousands of articles researching their extent.

### 3.4. Adsorption mechanism

Adsorption mechanism studies of multiple water pollutants allow the appraisal of their manipulation efficiency, which is

crucial to and beneficial for optimization of the conditions of the removal process. Until now, a lot of studies have focused on assessing the possible interaction mechanism of different water pollutants on as-used biosorbents. Efficiency in terms of high adsorption plays a vital role in characterizing a biosorbent for the elimination of different water pollutants effectively. In general, the process of adsorption actualizes the physico-chemical features of the biosorbent, *i.e.*, molecular size, solubility, chemical composition, surface charge, reactivity, and hydrophobicity. The structural components' variable characters are attributed to the presence of many functional groups, with varying degrees, on its surface, *i.e.*, amino, hydroxyl, carboxyl, thiol, phosphate, *etc.*, which facilitates water pollutant sorption onto the biosorbent *via* various sorption mechanisms. The interaction between contaminants and biosorbent surfaces, commonly, may occur through complexation/coordination, aggregation, electrostatic interaction, microprecipitation, ion exchange, oxidation, and reduction. Fig. 3 illustrates various mechanisms involved in the process of adsorption. The occurrence of precipitation, as well as crystallization, is possible and it cannot be ignored; thus, this complicates sorption and/or desorption processes.

To explore the main mechanism of adsorption, many strategies of characterization and theoretical calculation related to various models' assumptions in terms of kinetics, thermodynamics, and isotherms were carried out. The adsorption interaction between water contaminants and different biosorbents takes place in two different scenarios: surface and interstitial sorption. In surface sorption, sorbate molecules displace from the aqueous solution to the biosorbent surface. Once pollutants (molecules and/or ions) pass the biosorbent's surrounding boundary layer, they attach to the active sites present on its surface, displacing themselves from aqueous solutions. Dipole interactions, hydrogen bonding, or van der Waals forces are usually the cause of this type of sorption.<sup>55</sup> On the other hand, the interstitial sorption mechanism differs, where pollutants (molecules and/or ions) diffuse towards the biosorbents, entering the biosorbent pores (macro, meso, and/or micropores),

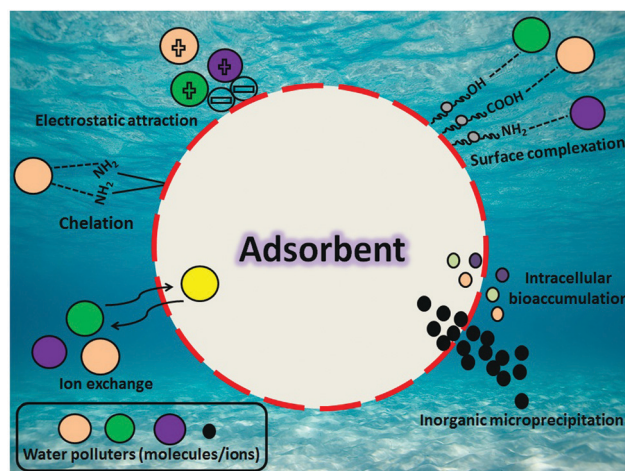


Fig. 3 Various mechanisms occurring in the adsorption process.



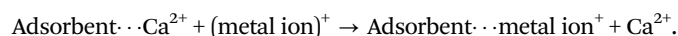
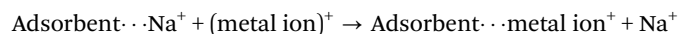
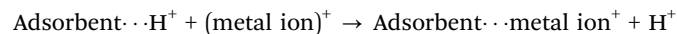
and becoming biosorbed to the interior surface of the biosorbent.<sup>56</sup>

Using biosorbents to tackle different pollutants from water and wastewater can be explained *via* electrostatic interactions. They have been established as major contributors to water contaminant adsorption. The presence of a plethora of functional groups (active sites) on the surface of the biosorbent elects them for efficiently capturing pollutants from various water systems. The capacity of these functional groups is significantly affected by the medium's pH. The biosorbent surface charge and pollutant's speciation are heavily reliant on the environmental pH. Lower pH values lead to protonation of various functional groups, which results in maintaining a positive charge on the surface of the biosorbent. As a consequence, electrostatic repulsion takes place, diminishing and/or inhibiting positively charged pollutant sorption, *i.e.*, metal cations. Conversely, electrostatic repulsion diminishes with increasing the pH of the medium, causing an increase in their adsorption in terms of electrostatic attraction phenomena. For example, negative-function moieties such as carboxylate ( $-\text{COO}^-$ ) and hydroxyl ( $-\text{OH}^-$ ) on the biosorbent surface maintain its negative charge, hence facilitating the binding of positive-charge pollutants (molecules and/or ions). Contrarily, the holding of positive functional groups such as amine sites ( $-\text{NH}_2$ ) is considered as the main cause of the sorption of negative-charge water pollutants.

The dissociation constant values ( $\text{p}K_a$ ) of biosorbent functional groups and their  $\text{pH}_{\text{PZC}}$  values are relative to the solution's pH, hence influencing the capacity of biosorbent sorption. The  $\text{p}K_a$  values of various functional groups such as carboxylic and phenol groups range from 3.5 to 5.5. This implies that the majority of these groups deprotonate in this pH working range and that avails enhancement of negatively charged sorption sites for the adsorption process.<sup>57</sup> Additionally, the biosorbent ( $\text{pH}_{\text{PZC}}$ ) value greatly affects the adsorption process. The charge of the surface of the biosorbent is positive ( $\text{pH}$  of solution  $<$   $\text{pH}_{\text{PZC}}$ ), while its surface charge is negative ( $\text{pH}$  of solution  $>$   $\text{pH}_{\text{PZC}}$ ). Therefore, the elimination of pollutants (molecules and/or ions), particularly those possessing positive charges, *i.e.*, metal cations, is decreased when their pH is lower than  $\text{pH}_{\text{PZC}}$  and increases when their pH is greater than  $\text{pH}_{\text{PZC}}$ . This suggests the significant role of electrostatic forces during the process of adsorption.<sup>58</sup>

The adsorption process can be fathomed based on the ion exchange mechanism between the biosorbent and the studied pollutants. Its contribution is illustrated through the replacement of protons from the exchangeable sites on the biosorbent surface with pollutants, *i.e.*, metal ions. Hydroxyl, carboxyl, and phenol groups facilitate the mechanism's operation, which can be attached to by pollutant ions, *i.e.*, divalent heavy metal ions, *via* two pairs of electrons and subsequently the release of two  $\text{H}^+$  and/or  $\text{Na}^+$  into the solution.<sup>59</sup> The pH of the solution affects the ion exchange mechanism: in an acidic medium, the increase in the  $\text{H}^+$  ions leads to a competition with positively charged pollutants (molecules and/or ions) leading to them being sorbed onto the biosorbent. Meanwhile in a basic medium,

$\text{OH}^-$  ions' increase compels negatively charged pollutants (molecules and/or ions) to be sorbed on the sorption sites. For example, the possible ion exchange mechanism between pollutants such as metal cations and exchangeable protons from the adsorbent surface can be illustrated as shown in the following equations:



Formation of surface complexes (complexation) involves the interaction of pollutants, *i.e.*, metal ions, with oxygen donor atoms from oxygen-containing functional groups (coordination) associated with the release of protons and formation of surface complexes. The ligand tendency for forming metal complexes significantly depends on the metal classification according to their chemical characters including the Hard-Soft-Acid-Base principle (HSAB). Metal ions (cations) can bind with the biosorbent surface through inner- or outer-sphere complex mechanisms by the covalent bond chemically established between the metal and the oxygen atom (electron donor) or by cations nearing the negative groups present on the surface (critical distance) linked to the presence of at least one water molecule between the cation and base, respectively.<sup>53</sup>

### 3.5. Batch adsorption

A batch adsorption scenario is a primitive step to assess the capability of the biosorbent of eliminating pollutants from their matrices. The influence of several operational parameters can be estimated during this strategy (Fig. 4).

### 3.6. Adsorption isotherm modeling

An adsorption isotherm is a curve relating the equilibrium concentration of a solute on the surface of an adsorbent,  $q_e$ , to the concentration of the solute in the liquid,  $C_e$ , with which it is in contact. The relationship between these  $q_e$  and  $C_e$  can normally be fitted to one or more equilibrium isotherm models. There are several isotherm equations available for analyzing experimental sorption equilibrium parameters. The most commonly used isotherms are reported in Table 1. The availability of various models on the basis of parameter number whether two, three, four and five parameters are shown in Fig. 5.

**3.6.1 Modeling of adsorptions kinetics.** Kinetic studies grant insightful outcome data necessary for modeling and devising an adsorption operation system with high efficiency. Commonly, the time-dependent adsorption data are cross-checked with several kinetic models such as the Pseudo-First-Order Rate Equation (PFORE),<sup>78</sup> Pseudo-Second Order Rate Equation (PSORE),<sup>79</sup> Weber and Morris model (W&M),<sup>80</sup> and Elovich model.<sup>81</sup> Usually, linearized forms of the various previously mentioned models illustrate the sorption process, exhibited in Table 2.



Table 1 Linearized and nonlinearized forms of some common isotherm models

Isotherm	Nonlinear form	Linear form	Theoretical assumption	Ref.
Langmuir	$q_m = \frac{q_{m,L} K_L C_e}{1 + K_L C_e}$	$\frac{C_e}{q_e} = \frac{C_e}{q_{m,L}} + \frac{1}{K_L q_{m,L}}$	Assumes monolayer adsorption on a homogeneous surface with a definite number of adsorption sites	60
Freundlich	$q_e = K_F C_e^{1/n}$	$\ln q_e = \ln K_f + \frac{1}{n} \ln C_e$	Suitable for a heterogeneous surface and can be applied to multilayer adsorption	61
Dubinin–Radushkevich	$q_e = Q_{DR} e^{-K_{DR} \varepsilon^2}$	$\ln q_e = \ln Q_{DR} - K_{DR} \varepsilon^2$	Mainly used to determine the adsorption mechanism (physical or chemical adsorption) with the mean free energy on a heterogeneous surface	62
Temkin	$q_e = \frac{RT}{b_T} [\ln(A_T C_e)]$	$q_e = \left(\frac{RT}{b_T}\right) \ln A_T + \left(\frac{RT}{b_T}\right) \ln C_e$	Assumes that there is a linear decrease in the heat of adsorption	63
Flory–Huggins	$\frac{\theta}{C_0} = K_{FH} - (1 - \theta)^{n_{FH}}$	$\log\left(\frac{\theta}{C_0}\right) = \log K_{FH} - n_{FH} \log(1 - \theta)$	Indicates the spontaneous nature and feasibility of the adsorption process	64 and 65
Hill	$q_e = \frac{q^s H C_e^n}{K_D + C_e^n}$	$\log\left(\frac{q_e}{q^s H - q_e}\right) = nH \log(C_e) - \log K_D$	Follows the hypothesis that ligand binding sites of a macromolecule can affect other binding sites of the same macromolecule	66
Redlich–Peterson	$q_e = \frac{K_R C_e}{1 + a_R C_e^g}$	$\ln\left(K_R \frac{C_e}{Q_e} - 1\right) = g \ln(C_e) + \ln(a_g)$	A combination of the Langmuir and Freundlich models. It can be used over a vast range of concentrations and can be used in both homogeneous and heterogeneous systems	67
Sips	$q_e = \frac{K_S C_e^{\beta_s}}{1 + a_S C_e^{\beta_s}}$	$\beta_s \ln C_e = -\ln\left(\frac{K_S}{q_e}\right) + \ln(a_S)$	Used for predicting heterogeneous adsorption systems in a wide range of adsorbate concentration. It approaches the Freundlich isotherm at low concentration and the Langmuir isotherm at high concentration	68
Toth	$q_e = \frac{K_T C_e}{(a_T + C_e)^{1/t}}$	$\ln\left(\frac{q_e}{K_T}\right) = \ln(C_e) - \frac{1}{t} \ln(a_T + C_e)$	Widely used for inhomogeneous solid surfaces. It incorporates the effect of the interaction between the adsorbed substances as well	69
Koble–Corrigan	$q_e = \frac{A C_e^n}{1 + B C_e^n}$	$\frac{1}{q_e} = \frac{1}{A C_e^n} + \frac{B}{A}$	Incorporated both the Langmuir and Freundlich isotherm models for representing the equilibrium adsorption data. It has an exponential dependence on concentration in the numerator and denominator. It is usually used with heterogeneous adsorption surfaces	70
Khan	$q_e = \frac{q_s b_k C_e}{(1 + b_k C_e) a_k}$	–	A general model for adsorption of a biadsorbate from pure dilute equation solutions.	71
Radke–Prausnitz	$q_e = \frac{a_{RP} r_e C_e^{\beta_R}}{a_{RP} + r_e C_e^{\beta_R - 1}}$	–	More preferred in most adsorption systems at low adsorbate concentration. At low adsorbate concentration, this isotherm model reduces to a linear isotherm, while at high adsorbate concentration it becomes the Freundlich isotherm	72
Frenkel–Halsey–hill	$\ln\left(\frac{C_e}{C_s}\right) = -\frac{\alpha}{RT} \left(\frac{q_s}{q_e d}\right)^r$	–	Mainly depending on the fractal dimension of the surface and on whether the dominant force is the substrate potential (van der Waals wetting, low coverage) or the film-vapor surface tension (capillary wetting, high coverage)	73–76
MacMillan–Teller	$q_e = q_s \left(\frac{k}{\ln\left(\frac{C_s}{C_e}\right)}\right)^{1/3}$	–	Derived from the BET model including the effects of surface tension in layers formed in the adsorbent	77

### 3.7. The goodness of model fitting

The goodness of fit of the used mathematical models to the experimental data can be evaluated *via* different statistical function errors as presented in Table 3. The following equations normally help to estimate the variances between the predicted and experimental data. The smaller the values of SSE,  $X^2$ , and CFEF, ARE, MPSD, and HYBRID, the closer the experimental data to the estimated data.

## 4. Metals and adsorbents

### 4.1. Copper-incorporating adsorbents

CuO nanostructures' various morphologies (leaves, clusters, ovals, small rods, and porous nano sheets) have been synthesized

by a novel simple method applying microwave radiation.<sup>82</sup> The produced CuO nanostructures were characterized by the X-ray diffraction analysis technique (XRD), transmission electron microscopy (TEM), surface area analysis (BET), and energy-dispersive spectroscopy (EDS). CuO nanostructures' capacity as adsorbents was investigated for adsorptive removal of Pb(II) ions from aqueous solutions. Different physico-chemical parameters such as the initial metal ion concentration, pH, and equilibrium contact time were evaluated. The optimum pH value of the solution made for adsorption of Pb(II) from aqueous solutions was found to be 6.5, while the optimum contact time was found to be four hours. The maximum capacity of oval, cluster, leaf, small rod, and porous nanosheet CuO nanostructures for Pb(II) was 125, 116, 117, 120, and 115 mg g<sup>-1</sup>.



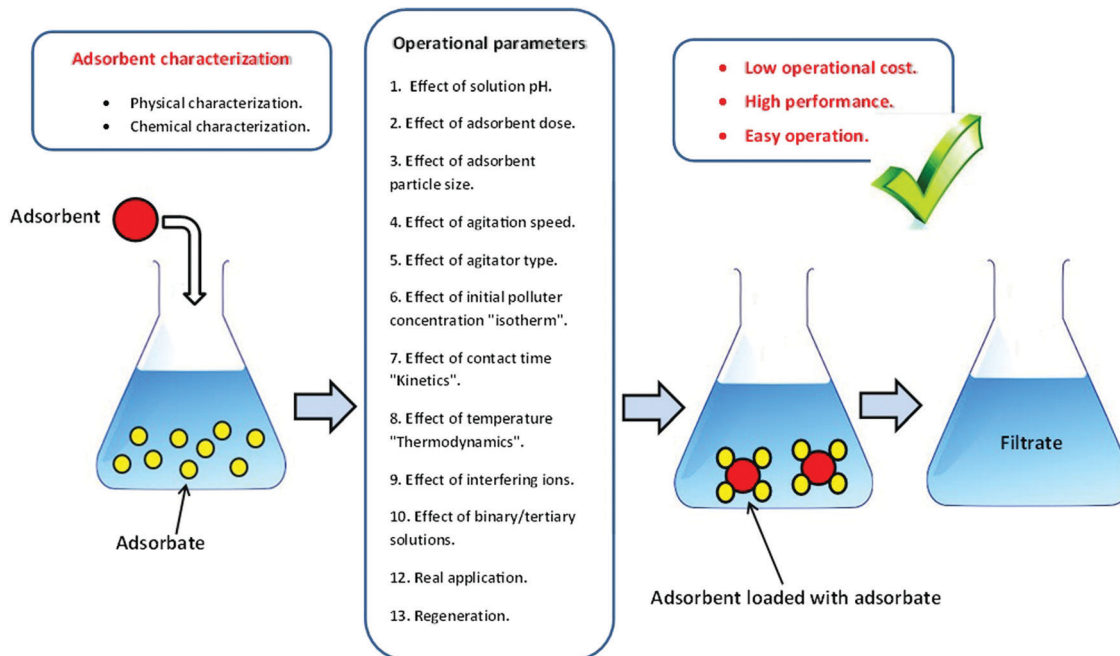


Fig. 4 Schematic diagram of batch adsorption.

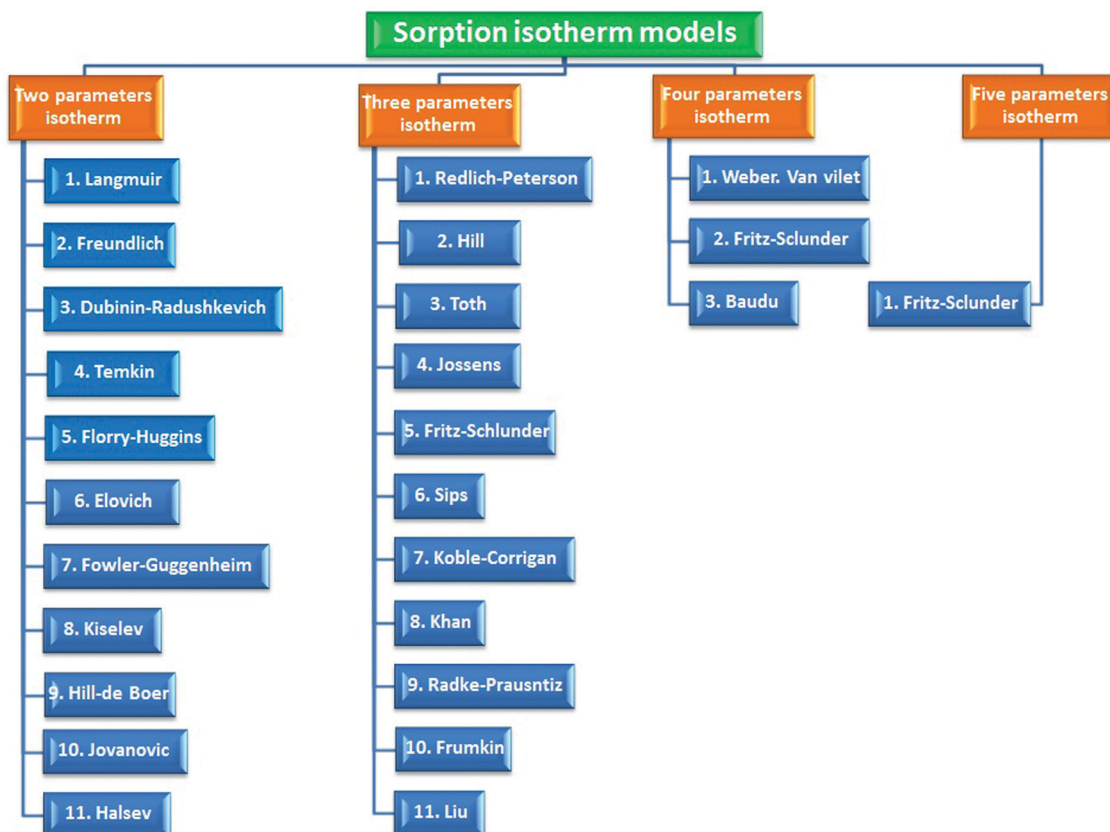


Fig. 5 Different isotherm models based on the number of parameters used.

To acquire a high-efficiency and low-cost adsorbent for arsenic removal from water, a nanostructured Fe(III)-Cu(II) binary oxide was devised *via* the facile coprecipitation method.<sup>83</sup> Various techniques including BET surface area measurement,





Table 2 Linearized forms of some different kinetic models

Kinetic model	Nonlinear form	Linear form	Theoretical assumption	Ref.
Pseudo-first order	$q_t = \frac{q_e}{1 + e^{-k_1 t}}$	$\log(q_e - q_t) = \log q_e - \left(\frac{k_1}{2.303}\right)t$	Based on the sorption capacity and removal rate change with time being directly proportional to the difference in saturation concentrations (physical sorption)	78
Pseudo-second order	$q_t = \frac{q_e^2 k_2 t}{1 + k_2 q_e t}$	$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \left(\frac{1}{q_e}\right)t$	Investigates kinetic behavior in the case of a chemical reaction being the rate controlling step (chemical sorption)	79
Intraparticle diffusion	—	$q_t = k_i t^{0.5} + X$	Determines the rate controlling step of the sorption process (film diffusion and/or intraparticle diffusion)	80
Elovich equation	$\frac{dq_t}{dt} = \alpha e^{-\beta q}$	$q_t = \frac{1}{\beta} \ln \alpha \beta + \frac{1}{\beta} \ln t$	Based on the difference in the sorption energies of sorbent active sites which resulted from the heterogeneous nature of the binding sites	81

Table 3 Statistical functions used to investigate error deviation between experimental and calculated values

Functions	Equation
An error analysis of the sum of squared errors of prediction (SSE)	$SSE = \sum_{n=1}^n (q_{cal} - q_{exp})^2$
Chi-square statistic ( $X^2$ )	$X^2 = \sum_{n=1}^n \left[ \frac{(q_{e,exp} - q_{e,cal})^2}{q_{e,cal}} \right]$
The composite fraction error function (CFEF)	$CFEF = \sum_{n=1}^n \left[ \frac{(q_{e,exp} - q_{e,cal})^2}{q_{e,exp}} \right]$
Average relative error (ARE)	$ARE = \frac{1}{n} \sum \left( \frac{q_{e,cal} - q_{e,exp}}{q_{exp}} \right) \times 100$
Marquardt's percentage standard deviation (MPSD)	$MPSD = \sqrt{\frac{\sum (q_{e,exp} - q_{e,cal})^2}{n - P}}$
Hybrid fractional error function (HYBRID)	$HYBRID = \frac{1}{n - p} \sum \left( \frac{q_{e,exp} - q_{e,cal}}{q_{e,exp}} \right) \times 100$

Here  $q_{e,exp}$  and  $q_{e,cal}$  are the experimental and model calculated (predicted) sorption capacity values, respectively, and  $n$  is the experimental sample number.  $P$  is the number of parameters in each isotherm model.

powder XRD, SEM, and XPS were used to characterize the synthetic Fe(III)–Cu(II) binary oxide. Adsorption experiments took place to assess the adsorption kinetics, isotherms, and pH edge and regeneration of spent adsorbent. The results indicated that the Fe(III)–Cu(II) binary oxide with a Cu:Fe molar ratio of 1:2 performed excellently in displacing As(V) and As(III) from water, and the maximal adsorption capacities for As(V) and As(III) were 82.7 and 122.3 mg g<sup>-1</sup> at pH 7.0, respectively.

It was attempted to synthesize cupric oxide nanoparticles (CuONPs) in a green effective way through utilizing lemon juice extract as a bioreductant.<sup>84</sup> The CuONPs were applied for Cr(VI) displacement from water through the method of adsorption. The experimental parameters were optimized through the Box–Behnken Design (BBD) of response surface methodology for the optimum response. The adsorption equilibrium data were well fitted using the Freundlich isotherm model and the kinetics was explained through a pseudo-second-order kinetic model. The entire process proved to be cost effective, spontaneous, and exothermic. The linear approach for analyzing the isotherm as well as kinetic parameters was found to be more appropriate than the nonlinear approach. The experimental results showed that CuO nanoparticles can be good alternatives for the removal of Cr(VI) from aqueous solutions.

Another type of CuONPs has been effectively created *via* a green-effective route through employing lemon juice as a bioreductant.<sup>85</sup> The green method for the synthesis of nanoparticles was cost effective, safe, and eco-friendly. The synthesized CuONPs were characterized by different analytical techniques, *e.g.*, UV-visible, XRD, FTIR, SEM, and TEM analyses. This study revealed that the synthesized CuONPs were excellent solutions for detoxifying water of Cr(VI) through adsorption. The process of adsorption was found to be spontaneous and endothermic; the equilibrium during adsorption was well explained through pseudo-second-order kinetics.

Synthesizing copper oxide nanoparticles through the reactive magnetron sputtering technique and their adsorptive removal properties for Pb(II) ions from aqueous solution were investigated.<sup>86</sup> Various adsorption parameters, *e.g.*, the solution pH, adsorbent dose, initial metal ion concentration, equilibrium contact time and temperature were evaluated for removing maximum Pb(II) ions. The optimal prerequisites were found to be, respectively, 6, three hours, and 2 g L<sup>-1</sup> for a 50 mg L<sup>-1</sup> Pb(II) ion concentration. The adsorption kinetics followed the pseudo-second-order kinetic model, indicating that the adsorption was controlled through the chemisorption process. The adsorption isotherm follows a Langmuir isotherm with a maximum adsorption capacity of 37.03 mg g<sup>-1</sup>. The  $\Delta S$  and



$\Delta H$  values were found to be positive, indicating the endothermic nature of the adsorption process, while the negative value of the Gibbs free energy ( $\Delta G$ ) denotes that Pb(II) adsorption was spontaneous. The study revealed that the synthesized CuO nanoparticles may be a lucrative solution for removing Pb(II) ions from aqueous solutions.

A simple one-step approach for devising copper ferrocyanide-embedded magnetic hydrogel beads (CuFC-MHBs) was designed,<sup>87</sup> and the beads were applied to effectively remove Cs and then magnetically separate it from water. The resulting CuFC-MHBs illustrated the effectiveness of Cs removal performance with a high  $K_d$  value of 66 780 mL g<sup>-1</sup> and exemplary structural stability without the release of CuFC for at least one month; it was effectively separated from water by an external magnet. Additionally, the CuFC-MHBs selectively adsorbed Cs with high  $K_d$  values in the presence of different competing ions, such as in simulated groundwater (24 500 mL g<sup>-1</sup>) and seawater (8290 mL g<sup>-1</sup>). Also, they maintained their Cs adsorption capacity in a wide pH spectrum, from 3 to 11. The convenient fabrication method and effective removal of Cs from various aqueous media showed that CuFC-MHBs show massive potential for practical application in the decontamination of Cs-contaminated water sources resulting from radioactive liquid waste and nuclear accidents in different nuclear industry fields.

#### 4.2. Zinc-incorporating adsorbents

Efficient adsorbents made from Mg–Al–Zn-mingled oxides were prepared by the coprecipitation method.<sup>88</sup> The structure, composition, morphology, and thermal stability of the created Mg–Al–Zn-mingled oxides were assessed by powder X-ray diffraction, Fourier-transform infrared spectrometry, N<sub>2</sub> physisorption, scanning electron microscopy, differential scanning calorimetry, and thermogravimetry. The prepared Mg–Al–Zn-mingled oxides can be used as a viable adsorbent for the removal of Co(II) and Ni(II) from their aqueous solutions. The maximum adsorption capacity was 116.7 mg g<sup>-1</sup> and 70.4 mg g<sup>-1</sup> for Co(II) and Ni(II), respectively. The adsorbed metal ion amount was found to differ with increasing the initial pH value of the solution up to a point where metal ions are precipitated out in the alkaline solution. The optimum pH was found to be 6 and 5.5 for Co(II) and Ni(II), respectively. The experimental data remained per the equation of the PSO rate. The equilibrium data of the metals were fitted optimally using the Langmuir isotherm and Freundlich isotherm models, and the maximum adsorption capacity values were 113.8 mg g<sup>-1</sup> and 79.4 mg g<sup>-1</sup> for Co(II) and Ni(II), respectively. The outcome denotes that the adsorbent provides a cost-effective method for removing heavy metal ions from contaminated wastewater.

The potential uses of ZnO and its microparticles and TiO<sub>2</sub> nanoparticles to rid groundwater of arsenic were evaluated.<sup>89</sup> The outcomes showed that the arsenic adsorption efficiency surged in proportion with the reduction of the adsorbents' particle size. Upon using ZnO and TiO<sub>2</sub> nanoparticles, their adsorption capacities were 0.85 and 0.99 mg g<sup>-1</sup>, respectively. TiO<sub>2</sub> nanoparticles showed better adsorption ability for arsenic

than that of ZnO since the first had a smaller average particle size and larger surface area. In aqueous solution, metal oxide nanoparticles have a hydroxyl surface that allowed the physisorption of incoming HAsO<sub>4</sub><sup>2-</sup> ions *via* hydrogen bonding; this resulted in a better arsenic adsorptive capacity.

Meng *et al.* (2018)<sup>90</sup> developed a one-pot method to remove CrO<sub>4</sub><sup>2-</sup> from wastewater by forming Zn Al-Layered Double Hydroxides (ZnAl-LDH). By this process, the efficiency of Cr(VI) removal was nearly 100% and reached the theoretical maximum of the ZnAl-LDH removal capacity. In addition, mixed contaminants of Cr(VI) and dyes in wastewater can be separated from each other by controlling the addition of Zn/Al solution using this one-pot method.

A ZnO-tetrapod-activated carbon (ZnO-T/AC) nanocomposite was synthesized as an adsorbent for efficient decontamination of Cr(VI) from an aqueous medium.<sup>91</sup> The reduction of Cr(VI) using the ZnO-AC adsorbent was influenced by the pH value, contact time and dose of the adsorbent. The maximum reduction efficiency of Cr(VI) to Cr(III) by AC, ZnO, and ZnO-AC adsorbents occurred at pH 2.0. At optimum pH 2, AC, ZnO-T, and ZnO-T/AC showed 43%, 55%, and 97% Cr(VI) reduction, respectively. The pseudo-second-order model and intraparticle diffusion and Elovich models were used to determine the adsorption capacity and the kinetic rate constant, and fitted well for all the adsorbents.

#### 4.3. Iron-incorporating adsorbents

Nonmagnetic iron oxide–hydroxide nanoparticles of a spherical morphology and their application for defluorination of drinking water were reported.<sup>92</sup> XRD, BET surface area, FTIR, Field Emission Scanning Electron Microscopy (FESEM), and Transmission Electron Microscopy (TEM) images were utilized to detect nanoscale iron oxide–hydroxide. TEM imagery revealed that the iron oxide–hydroxide nanoparticles were formed in a spherical morphology. These nanoparticles exhibited an exemplary capacity to displace fluoride from contaminated water within a wide range of pH. The effects of temperature, pH, stirring speed, the dose of adsorbent, and contact time were evaluated. The equilibrium data were verified with different isotherm models. Eventually, a calculation procedure was devised to determine the adsorbent requirement. The nanoparticles with adsorbed fluoride were regenerated up to 70% using sodium hydroxide or hydrochloric acid solution. The iron oxide–hydroxide nanoparticles can be employed as an effective and replicable adsorbent media for defluorination of water in the presence of competing anions like chloride, iodate, iodide, and sulfate.

Sulfidated zerovalent iron (S-ZVI) is garnering more attention owing to its easy-to-prepare and highly-reactive nature with contaminants.<sup>93</sup> The results showed that sulfidation of zerovalent iron (ZVI) could significantly increase the Cr(VI) and Sb(III) sequestration simultaneously. During the sequestration of these pollutants, Cr(VI) was diminished into Cr(III) and Sb(III) was oxidized into Sb(V); both processes occurred simultaneously in this system. The sequestration rate of Cr(VI) and Sb(III) increased with the pH surging from 4.0 to 6.0 but diminished when the pH continued to rise to 8.0. More



surface Fe(II) regenerated at pH 6.0, which significantly contributes to Cr(VI) sequestration.

Mubarak *et al.* (2018)<sup>94</sup> prepared Mg/Fe-layered double hydroxide (MF-LDH) hollow nanospheres by a simple thermal method. After calcination at 400 °C, the MF-LDH hollow nanospheres were converted into the corresponding oxide. The nanospheres showed remarkable efficiency in removing As(V) and Cr(VI) ions, with maximum adsorption capacities of 178.6 mg g<sup>-1</sup> for As(V) and 148.7 mg g<sup>-1</sup> for Cr(VI). Complete heavy metal removal (~99.9%) from wastewater up to the drinking water level (WHO standards) was achieved in 20 min and 10 min for As(V) and Cr(VI), respectively. This material should facilitate practical applications in cost-effective wastewater purification.

Siderite (FeCO<sub>3</sub>), an iron(II)-containing mineral, exists in many anaerobic sediments and groundwater systems. Siderite is an effective material for removing Cr(VI) in aqueous conditions with a maximum sorption of 81 mg g<sup>-1</sup> at pH 5.<sup>95</sup> The outcomes denote that within anoxic aqueous parameters, Cr(VI) can be detoxified by siderite provided that these coupled sorptions and redox reactions are being controlled by the initial Cr(VI) concentrations and pH.

Graphene-coated iron oxide nanoparticles (GCIO) were devised *via* the microemulsion method for removing Cr(VI) ions from aqueous solutions.<sup>96</sup> A swift and remarkable Cr(III) and Cr(VI) ion removal efficiency is exhibited by aqueous solution-prepared GCIO, which is 99.13% with 0.06 g GCIO in 100 ppm adsorbate solution as confirmed by EDX analysis. The adsorption process follows pseudo-second-order kinetics with an *R*<sup>2</sup> value of 0.97 and the Freundlich model isotherm with a high adsorption capacity. The Cr(VI) removal surges with the increase in temperature, revealing the endothermic nature of the process of adsorption. GCIO also shows a high intraparticle diffusion value with an *R*<sup>2</sup> value of 0.98. GCIO maintains remarkable stability in an extremely acidic environment when treated with concentrated acid for 24 hours as well as a reusable nature to the same extent for adsorption of Cr(VI).

A multifunctional adsorbent was developed by preparing a composite of Fe<sub>2</sub>O<sub>3</sub> and ZnO.<sup>97</sup> The prepared composite removed Cr(VI) efficiently. The data of adsorption corroborated well with the Freundlich isotherm model and pseudo-second-order kinetic model with *R*<sup>2</sup> values close to 1. The 1:1 ratio of Fe<sub>2</sub>O<sub>3</sub> and ZnO provided the optimum sorption properties to the sorbent. At this ratio, the maximum adsorption capacity of the adsorbent was 36.50 mg g<sup>-1</sup>.

Mechano-chemically sulfidated microscale zerovalent iron (S-mZVIbm) is a potential remedy for groundwater for the removal of Cr(VI).<sup>98</sup> Removing Cr(VI) by S-mZVIbm is mainly a process of a chemisorption nature and its kinetics was well fitted by a pseudo-second-order model. Alkaline pH halted the removal of Cr(VI) while dissolved oxygen slightly depressed the removal of Cr(VI). The high extent of removal of Cr(VI) by S-mZVIbm compared to its unsulfidated contemporary mZVIbm is a result of its enhanced surface area.

Another nanoscale zerovalent iron (nZVI) sorbent with a considerably high surface area (182.97 m<sup>2</sup> g<sup>-1</sup>) with chain-structure

morphology was synthesized and well characterized.<sup>99</sup> The as-prepared nZVI can entirely displace Cr(VI) under anoxic conditions after a reaction of 20 min; on the other hand, only 43% of Cr(VI) was removed after a reaction of 60 min under oxic conditions. Notably, nZVI demonstrates a remarkable removal capacity of Cr(VI) (123.85 mg g<sup>-1</sup>) as well as a quick removal rate (0.017 g mg<sup>-1</sup> min<sup>-1</sup>). Moreover, the as-prepared nZVI exhibited swift displacement of traced Cr(VI) from Cr-spiked drinking water or actual Cr-contaminated lake water. Cr(VI) removal experimental results from simulated Cr-contaminated tap, drinking, and actual lake water show the effectiveness of the as-prepared nZVI as a potential material for the quick removal of traced Cr(VI) from Cr-spiked drinking water or actual Cr-contaminated lake water.

After being analyzed and characterized, nanoadsorbents of core-shell bimagnetic nanoparticles (CoFe<sub>2</sub>O<sub>4</sub>@ $\gamma$ -Fe<sub>2</sub>O<sub>3</sub>) with two different mean sizes were applied as potential sorbents for removing Cr(VI) from aqueous solutions *via* magnetic-assisted chemical separation.<sup>100</sup> The adsorption data checked out with the Freundlich model, denoting that the Cr(VI) species create multilayers surrounding the nanoadsorbent surface. The utmost removal percentage was gauged at pH = 2.5 with an orbital shaking rate of 400 rpm, and the maximum adsorption capacities obtained were higher or close to those of other magnetic adsorbents dedicated to removing Cr(VI). The improved adsorption capacity of the sample according to smaller nanoparticles was related to its higher BET surfaces. The adsorption rapidly achieved equilibrium and the kinetic data adhered to the pseudo-second-order model, implying that the rate-controlling step of the process revolved around ionic interactions between the surface sites and the Cr(VI) species. The thermodynamic analysis yielded that the adsorption is endothermic and spontaneous. The process was found to be enhanced at higher temperatures and presented increased randomness at the surface/solution interface. The magnetic nanoadsorbents also demonstrated a high selectivity towards Cr(VI) and good renewability for reuse, establishing them as a greener material. The adsorption capability remained high in simulated wastewater. This process can be efficiently applied to other related heavy metals such as molybdenum and arsenic.

Jain *et al.* (2018)<sup>101</sup> fabricated magnetite (Fe<sub>3</sub>O<sub>4</sub>) and magnetite/activated-carbon (Fe<sub>3</sub>O<sub>4</sub>/AC) through the coprecipitation method for removing Cr(VI), Cu(II), and Cd(II) ions from aqueous solution in batch mode. The optimal conditions for the removal of ions were as follows: pH = 2 for Cr(VI) desorption studies with 0.1 M HCl. It is stated that these nanoparticles can be regenerated effectively, allowing them to be reused for up to four adsorption-desorption cycles without any loss in mass.

A highly selective Fe<sub>3</sub>O<sub>4</sub>@Arg-PPy adsorbent was effectively synthesized by a one-pot chemical polymerization of pyrrole with arginine and was made commercially available as Fe<sub>3</sub>O<sub>4</sub> NPs. The FTIR, VSM, XRD, and TEM analyses of the Fe<sub>3</sub>O<sub>4</sub>@Arg-PPy nanocomposite imply the successful implementation of arginine and Fe<sub>3</sub>O<sub>4</sub> into PPy.<sup>102</sup> The batch experimental results showed a highly pH-dependent removal of Cr(VI) at the optimum pH value of 2. The process of adsorption was



Langmuir modeled with adsorption capacities of 294.11, 322.58, 370.37, and 416.67 mg g<sup>-1</sup> at 15, 25, 35, and 45 °C, respectively. The Cr(vi) removal kinetics *via* Fe<sub>3</sub>O<sub>4</sub>@Arg-PPy conformed to the pseudo-second-order model, and the determined rate constant was 6.67 × 10<sup>-3</sup> g m<sup>-1</sup> min<sup>-1</sup> at room temperature for a solution of an initial Cr(vi) concentration of 50 mg L<sup>-1</sup> and pH 2. The thermodynamic parameters that were calculated were as follows: ΔG° -4.76 kJ mol<sup>-1</sup> at 25 °C, ΔH° +76.16 kJ mol<sup>-1</sup>, ΔS° + 0.27 kJ mol<sup>-1</sup> K<sup>-1</sup> and E<sub>a</sub> 49.91 kJ mol<sup>-1</sup>, showing an endothermic, spontaneous, and chemisorption process.

A Microsized Granular Ferric Hydroxide (mGFH) adsorbent for chromate removal in competition with ions present in drinking water was elaborated.<sup>103</sup> The results show a high dependency on the pH value with increasing adsorption in correspondence to decreasing pH values. Competing ions present in drinking water were tested for interfering effects on chromate adsorption. Bicarbonate was identified as the main inhibitor of chromate adsorption. Sulfate, silicate, and phosphate also decreased chromate loadings, while calcium enhanced chromate adsorption. The adsorption equilibrium was reached after 60 min for particles smaller than 63 nm, while 240 min was required for particles from 125 nm to 300 nm. The adsorption kinetics in single-solute systems could be modeled using the Homogeneous Surface Diffusion Model (HSDM) with a surface diffusion coefficient of 4 × 10<sup>-14</sup> m<sup>2</sup> s<sup>-1</sup>.

Wen *et al.* (2019)<sup>104</sup> successfully synthesized nanosized ordered Magnetic Mesoporous Fe-Ce bimetal oxides (nanosized-MMIC) with a highly well-ordered interconnected mesostructure. This nanosized-MMIC exhibited remarkable adsorption capabilities for As(v), Cr(vi), and acid orange 7 (AO<sub>7</sub>) and the corresponding calculated maximum adsorption capacities of the materials were 111.17, 125.28, and 156.52 mg g<sup>-1</sup>, respectively. The removal of As(v) and Cr(vi) by nanosized-MMIC was slightly dependent on the ionic strength, yet it was highly solution-pH dependent; the coexistent silicate and phosphate ions competed excellently with As(v) and Cr(vi) for the adsorption active sites. The mechanisms implied that As(v) and Cr(vi) formed inner-sphere complexes on the nanosized-MMIC interface through surface complexation and electrostatic interaction. Nanosized-MMIC is anticipated to be a potential excellent nano-adsorbent with high potential for application for removing coexisting organic dyes and toxic heavy metals in specific wastewater treatment. The adsorption capacity of some selected iron incorporating adsorbents are reported in Table 4.

#### 4.4. Other metallic adsorbents

The aluminum oxide hydroxide efficiency to displace trivalent chromium from aqueous solutions through batch mode experiments was assessed.<sup>163</sup> The effects of the contact time, pH, initial concentration, and dosage on Cr(III) adsorption were evaluated. This study divulged that more than 99% of Cr(III) was removed over a wide range of initial pH (3–10). The optimal parameters for removing Cr(III) were established to be at pH 4–6 with a 40 g L<sup>-1</sup> adsorbent dose within a contact time of 60 min. The capacity of adsorption was evaluated *via* Langmuir and

Freundlich isotherms. The equilibrium data at varying adsorbent dosage crosscheck with the two isotherms. The adsorbent was found to be optimal for removing Cr(III) from waste effluent from a tannery.

Mikhaylov *et al.* (2018)<sup>164</sup> synthesized Al/Fe oxide-oxyhydroxide composite powders through a hydrothermal method applying metal sulfate solutions and urea as precursors. The maximum specific surface area (190 m<sup>2</sup> g<sup>-1</sup>) is reached for the synthesized samples synthesized from solutions with [Al<sup>3+</sup>]:[Fe<sup>3+</sup>] = 1:0 and 1:1. However, sulfate ions present on the surface of Al-containing samples inhibit the adsorption of Cr(vi). The maximum capacity for adsorption in the batch regime (3.66 mg g<sup>-1</sup>) was for a sample synthesized from solutions with [Al<sup>3+</sup>]:[Fe<sup>3+</sup>] = 1:6, which had a high (though not maximal) surface area (102 m<sup>2</sup> g<sup>-1</sup>), a low-sulfate content, and maximum zeta potential. Sorption experiments illustrated that the mean free adsorption energy was lower than 8 kJ mol<sup>-1</sup> for the entirety of the samples; this indicates that the process of adsorption was physical and the possibility of Cr(vi) desorption and adsorbent regeneration.

Another type of metallic adsorbent based on Apatitic Tricalcium Phosphate powder (ATrPh-105) was devised and analyzed by different techniques of characterization.<sup>165</sup> At 60 °C and under acidic conditions, a higher adsorption capacity (527.19 mg g<sup>-1</sup>) towards Cr(vi) was recorded. The kinetic data of the adsorption of Cr(vi) onto ATrPh-105 adhered to pseudo-second-order kinetics. The results of isotherms and thermodynamics studies affirmed that Cr(vi) adsorption onto ATrPh-105 is endothermic, which happens to fit the Langmuir isotherm as well. According to the thermodynamic results of the sorption of Cr(vi) onto ATrPh-105, the process was controlled by a chemical reaction. Additionally, ATrPh-105 illustrated Cr(vi) high sorption efficiency (90.22%) following three cycles of adsorption-regeneration. This finding confirms the potential of ATrPh-105 as an efficient adsorbent with room for utilization in various environmental applications.

#### 4.5. Silica-based adsorbents

Corn cob silica-supported nanoscale zerovalent iron (MCCS) is a nano biocomposite that was developed by a facile technique, and its efficiency for removal of Cr(vi) from aqueous solution was evaluated.<sup>166</sup> The adsorption data illustrated that the extent of fitting with models is higher in the pseudo-second-order kinetics as compared with the pseudo-first-order kinetics model. Corn cob silica is a cost-effective material. From the studied results, it is divulged that the efficiency of the removal is correlated to the pH value of the solution and temperature and the sorption kinetics. Moreover, thanks to its magnetic property, this material is potent in overcoming the separation problems concerning adsorption-based treatment techniques, alongside other advantages such as being environmentally friendly and highly efficient, and its high capacity. Thus, MCCS can also be utilized for removing other toxic elements present in wastewater.

Dutta and Nath (2018)<sup>167</sup> synthesized a SiO<sub>2</sub>/carbon nanocomposite (SiO<sub>2</sub>/CCNC) and nanoporous carbon (CCNC) from a simple, low-cost, and industry-scalable method from corn cob





Table 4 Adsorption capacity of some selected iron incorporating adsorbents

No.	Magnetic adsorbents	Adsorbate	Adsorption capacity (mg g <sup>-1</sup> ) or removal efficiency (%)	Ref.
1	Fe <sub>3</sub> O <sub>4</sub> @thiourea-formaldehyde polymer	Cr(vi), As(v)	Cr(vi) (4.28 mmol g <sup>-1</sup> ), As(v) (1.97 mmol g <sup>-1</sup> )	105
2	MgFe <sub>2</sub> O <sub>4</sub>	Co(II), Mn(II), Ni(II), Cu(II)	Co(II) (2.30 mmol g <sup>-1</sup> ), Mn(II) (1.56 mmol g <sup>-1</sup> ), Ni(II) (0.89 mmol g <sup>-1</sup> ), Cu(II) (0.46 mmol g <sup>-1</sup> )	106
3	Dried ZVI NPs	Pb(II)	807.23 mg g <sup>-1</sup> at pH 6	107
4	ZnFe <sub>2</sub> O <sub>4</sub> @NH <sub>2</sub> -SiO <sub>2</sub> @polydiphenylmethane diisocyanate@dithizone	Pb(II)	267.2 mg g <sup>-1</sup>	108
5	ZVI/activated carbon nanotubes	Te(II)	800 mg g <sup>-1</sup> at pH 4.7	109
6	Ammonium-pillared montmorillonite/CoFe <sub>2</sub> O <sub>4</sub> /calcium alginate	Cs <sup>+</sup>	86.46 mg g <sup>-1</sup>	110
7	ZVI-Coffee grounds	Pb(II), Cd(II), As(III), As(V)	Pb(II) 164.1 mg g <sup>-1</sup> (1 h), Cd(II) 112.5 mg g <sup>-1</sup> (24 h), As(V) 9.3 mg g <sup>-1</sup> (1 h) As(III) 23.5 mg g <sup>-1</sup> (1 h)	111
8	Clinoptilolite/CoFe <sub>2</sub> O <sub>4</sub>	Sr(II)	20.58 mg g <sup>-1</sup>	112
9	ZVI/chitosan	U(VI)	591.72 mg g <sup>-1</sup> at pH 6	113
10	MnFe <sub>2</sub> O <sub>4</sub>	U(VI), Eu(III)	U(VI) 119.90 mg g <sup>-1</sup> , pH 5 Eu(III) 473.93 mg g <sup>-1</sup> , pH 7	114
11	ZVI NPs	Cu(II)	343 mg g <sup>-1</sup>	115
12	Hydroxyapatite/NiFe <sub>2</sub> O <sub>4</sub>	<sup>152+154</sup> Eu <sup>160</sup> Tb	Eu(III) (137.35 mg g <sup>-1</sup> ) Tb(III) (130.43 mg g <sup>-1</sup> )	116
13	ZVI/alginate	Pb(II)	581.7 mg g <sup>-1</sup> (15 min)	117
14	Ni <sub>0.6</sub> Fe <sub>2.4</sub> O <sub>4</sub>	U(VI)	189.04 mg g <sup>-1</sup> (2 h)	118
15	ZVI/biochar	Cr(VI)	35.30 mg g <sup>-1</sup>	119
16	NiFe <sub>2</sub> O <sub>4</sub> /MnO <sub>2</sub>	Pb(II)	85.78 mg g <sup>-1</sup>	120
17	ZVI/polyaniline/attapulgit	Cr(VI)	86.56 mg g <sup>-1</sup>	121
18	MgFe <sub>2</sub> O <sub>4</sub> /biochar	PO <sub>4</sub> <sup>3-</sup>	163.02 mg g <sup>-1</sup> , pH 3	122
19	ZVI/ZVAL	Cr(VI), Cd(II), Ni(II), Cu(II), Zn(II)	99.5% (300 h)	123
20	Poly( <i>m</i> -phenylenediamine)/GO/NiFe <sub>2</sub> O <sub>4</sub>	Cr(VI)	502.5 mg g <sup>-1</sup> at pH 3	124
21	ZVI NPs	Cd(II), Cu(II), Ni(II), Pb(II)	Cd(II) (79.33–102.00) mg g <sup>-1</sup> Cu(II) (111.11–142.85) mg g <sup>-1</sup> , Ni(II) (107.30–137.96) mg g <sup>-1</sup> , Pb(II) (110.97–142.68) mg g <sup>-1</sup>	125
22	NiFe <sub>2</sub> O <sub>4</sub> -nitrogen-doped mesoporous carbon	Hg(II)	476.2 mg g <sup>-1</sup>	126
23	ZVI/fly ash	Pb(II), Cr(VI)	Pb(II) 78.13 mg g <sup>-1</sup> , Cr(VI) 15.70 mg g <sup>-1</sup>	127
24	Ni <sub>0.5</sub> Zn <sub>0.5</sub> Fe <sub>2</sub> O <sub>4</sub>	Ag(I)	243.90 mg g <sup>-1</sup>	128
25	Bentonite/ZVI	Pb(II), Cu(II), Zn(II), Ni(II)	Pb(II) (3.1 mg g <sup>-1</sup> ), Cu(II) (0.6 mg g <sup>-1</sup> ), Zn(II) (2.8 mg g <sup>-1</sup> ), Ni(II) (2.4 mg g <sup>-1</sup> )	129
26	Bacterial cells/sawdust/MnFe <sub>2</sub> O <sub>4</sub>	As(III) As(V)	As(III) (87.573 mg g <sup>-1</sup> ), As(V) (88.990 mg g <sup>-1</sup> )	130
27	ZVI/magnetite carbon	U(VI)	203.94 mg g <sup>-1</sup>	131
28	GO/NiFe <sub>2</sub> O <sub>4</sub>	Pb(II) Cr(III)	Pb(II) (25.0 mg g <sup>-1</sup> ), Cr(III) (45.50 mg g <sup>-1</sup> )	132
29	ZVI/polyaniline-graphene aerogel	U(VI)	350.47 mg g <sup>-1</sup> at pH 5.5	133
30	CoFe <sub>2</sub> O <sub>4</sub> -G & NiFe <sub>2</sub> O <sub>4</sub> -G	Pb(II), Cd(II)	Pb(II) is 142.8 and 111.1 mg g <sup>-1</sup> at pH 5 and 310 K for CoFe <sub>2</sub> O <sub>4</sub> -G & NiFe <sub>2</sub> O <sub>4</sub> -G; while for Cd(II) it was 105.26 and 74.62 mg g <sup>-1</sup> at pH 7 and 310 K	134
31	ZVI/activated carbon	As(V)	100% after 2.5 h	135
32	α-Fe <sub>2</sub> O <sub>3</sub>	Hg(II)	1.16 mg g <sup>-1</sup>	136
33	Fe <sub>3</sub> O <sub>4</sub> /bone char/chitosan	As(V)	112 μg g <sup>-1</sup>	137
34	γ-Fe <sub>2</sub> O <sub>3</sub>	Cd(II), Ni(II), Co(II)	Cd(II) (94.33 mg g <sup>-1</sup> ), Ni(II) (86.206 mg g <sup>-1</sup> ), Co(II) (60.60 mg g <sup>-1</sup> )	138
35	Fe <sub>2</sub> O <sub>3</sub> -Al <sub>2</sub> O <sub>3</sub>	Cu(II), Pb(II), Ni(II), Hg(II)	Cu(II) (4.98 mg g <sup>-1</sup> ), Pb(II) (23.75 mg g <sup>-1</sup> ), Ni(II) (32.36 mg g <sup>-1</sup> ), Hg(II) (63.69 mg g <sup>-1</sup> )	139
36	γ-Fe <sub>2</sub> O <sub>3</sub>	Pb(II), Zn(II), Cd(II)	Pb(II) (10.55 mg g <sup>-1</sup> ), Zn(II) (4.79 mg g <sup>-1</sup> ), Cd(II) (1.75 mg g <sup>-1</sup> )	140
37	ZVI/zeolite	Cd(II), Pb(II)	Cd <sup>2+</sup> (63.14 mg g <sup>-1</sup> ), Pb <sup>2+</sup> (154.61 mg g <sup>-1</sup> )	141
38	Fe <sub>3</sub> O <sub>4</sub> /PANI	Cr(VI)	200 mg g <sup>-1</sup>	142
39	Fe <sub>2</sub> O <sub>3</sub> @GO	Pb(II)	303.0 mg g <sup>-1</sup>	143
40	γ-Fe <sub>2</sub> O <sub>3</sub> /TiO <sub>2</sub> /PVA/alginate beads	Ba(II)	99% in 150 min at pH 8	144
41	γ-Fe <sub>2</sub> O <sub>3</sub> @chitosan	Cd(II)	15.2 mg g <sup>-1</sup>	145
42	Chitosan/Cu(OH) <sub>2</sub> , chitosan/CuO	Cr(VI)	1.4 mmol g <sup>-1</sup> , 2.6 mmol g <sup>-1</sup>	146
43	Polyacrylonitrile/α-Fe <sub>2</sub> O <sub>3</sub>	As(V)	82.2 mg g <sup>-1</sup> at 25 °C	147
44	Fe <sub>3</sub> O <sub>4</sub> /MgAl-layered double hydroxide	Co(II)	95.8% at pH 8	148
45	Chitosan/PVA/ZVI	As(V)	200 mg g <sup>-1</sup>	149
46	ZVI/diethylenetriamine/2-pyridinecarboxaldehyde	Co(II), Cu(II), Zn(II), Cd(II), Hg(II), Pb(II)	Co(II) 2600 μmol g <sup>-1</sup> , Cu(II) 4750 μmol g <sup>-1</sup> , Zn(II) 5600 μmol g <sup>-1</sup> , Cd(II) 4000 μmol g <sup>-1</sup> , Hg(II) 5200 μmol g <sup>-1</sup> , Pb(II) 5050 μmol g <sup>-1</sup>	150
47	ZVI/MnO <sub>2</sub>	As(V)	16.4 mg g <sup>-1</sup>	151
48	Fe <sub>3</sub> O <sub>4</sub> /alginate beads	La(III)	1.8 mmol g <sup>-1</sup>	152
49	γ-ALOOH/α-Fe <sub>2</sub> O <sub>3</sub>	Cr(VI)	4.17 mg g <sup>-1</sup>	153
50	Chitosan/clay/Fe <sub>3</sub> O <sub>4</sub>	Cu(II), As(V)	Cu(II) (17.2 mg g <sup>-1</sup> ), As(V) (5.9 mg g <sup>-1</sup> )	154
51	Fe <sub>3</sub> O <sub>4</sub> /poly- <i>p</i> -phenylenediamine-thiourea-formaldehyde	As(V)	99.04 mg g <sup>-1</sup>	12
52	Fe <sub>3</sub> O <sub>4</sub> /GO/beads	Cr(VI), As(V)	Cr(VI) (80%), As(V) (99%)	155
53	Fe <sub>3</sub> O <sub>4</sub> @cyclodextrin	Eu(III)	95% at pH 8	156



Table 4 (continued)

No.	Magnetic adsorbents	Adsorbate	Adsorption capacity (mg g <sup>-1</sup> ) or removal efficiency (%)	Ref.
54	Fe <sub>3</sub> O <sub>4</sub> /chitosan	Cr(vi)	231.77 mg g <sup>-1</sup>	13
55	Functionalized nanosilica	Cu(II)	386.4 mg g <sup>-1</sup>	157
56	Diethylenetriamine/GO/Fe <sub>3</sub> O <sub>4</sub>	Cr(vi)	123.4 mg g <sup>-1</sup> (40 s)	158
57	Chitosan-based magnetic composite	Diclofenac sodium tetracycline hydrochloride	164 mg g <sup>-1</sup> , 40.2 mg g <sup>-1</sup>	159
58	Zeolitic imidazolate frameworks confined in polystyrene	Benzotriazole	210.4 mg g <sup>-1</sup>	160
59	Poly( <i>N</i> -isopropyl acrylamide) grafted chitosan/Fe <sub>3</sub> O <sub>4</sub> composite particles, [CN-MCP]	Nonylphenol	166.7 mg g <sup>-1</sup>	161
60	Aromatic ring-functionalized chitosan magnetic composite	Norfloxacin, tylosin, diclofenac sodium	327.5 mg g <sup>-1</sup> , 843.5 mg g <sup>-1</sup> , 438.6 mg g <sup>-1</sup>	162

biowaste. The higher BET specific surface area of SiO<sub>2</sub>/CCNC (715.22 m<sup>2</sup> g<sup>-1</sup>) compared with CCNC (430.17 m<sup>2</sup> g<sup>-1</sup>) allows for enhanced adsorption efficiency. The uptake of Cr(vi) ions was also tested in the presence of interfering salts such as NaCl/Na<sub>2</sub>SO<sub>4</sub>. The effects of temperature, pH, and concentration of the dye on the efficiency of sorption of the SiO<sub>2</sub>/CCNC nanocomposite and CCNC for MB dye were evaluated. The adsorption process kinetics adhered to the pseudo-first-order model for CCNC and a pseudo-second-order model for the SiO<sub>2</sub>/CCNC nanocomposite. The experimental data acquired for SiO<sub>2</sub>/CCNC and CCNC adhere to Bangham's pore diffusion model, indicating pore diffusion as the rate-controlling step during MB adsorption. The isotherm data match the Freundlich model for SiO<sub>2</sub>/CCNC and CCNC, which is a telltale of multilayer sorption. Hence, it can be deduced that SiO<sub>2</sub>/CCNC is a potential low-cost adsorbent compared with commercial activated carbon for removing pollutants like MB dye and U(vi)/Cr(vi) ions from water and wastewater.

Carboxyl-group-functionalized mesoporous silica (CFMS) prepared by a one-pot cocondensation method was employed for the Solid Phase Extraction (SPE) of chromium species.<sup>168</sup> The captured Cr(III) can be eluted by using HNO<sub>3</sub> and detected by ICP-MS, and the concentration of Cr(vi) was the difference between the total chromium and Cr(III). This protocol has been successfully applied to detect inorganic chromium species in environmental water (rain and lake and river water) with recoveries between 91.9% and 103%. Therefore, this developed method exhibited good potential for the speciation of chromium in environmental water samples.

#### 4.6. Zeolite-based adsorbents

Adsorptive Cr(vi) removal from an aqueous solution was evaluated using a natural zeolite, clinoptilolite, in the shape of a Hollow Fiber Ceramic Membrane (HFCM).<sup>169</sup> The performance of the HFCM in adsorption/filtration was 44% Cr(vi) removal at a concentration of 40 mg L<sup>-1</sup> and pH 4. The natural zeolite-based HFCM has potential as a single-step removal-by-adsorption process for Cr(vi) for treating wastewater. The slightly low removal could be a result of the high feed concentration and the HFCM's morphology. This performance can be further increased by maintaining the particle size of the natural

zeolite and the sintering temperature and preconditioning the feed before the adsorption and filtration processes. The HFCM also exhibited self-accelerating adsorption behavior, which was translated from some mechanisms and models. The membrane can be potentially developed in different separation systems such as membrane contact and membrane distillation.

Elwakeel *et al.* (2018)<sup>170</sup> prepared a composite material (PAN-Na-Y-zeolite) through the polymerization of acrylonitrile in the presence of Na-Y-zeolite. The composite was made usable through amidoximation as a result of the reaction of hydroxylamine on nitrile groups of the composite. The adsorbent (APNa-Y-zeolite) was characterized by FTIR spectrometry, XRD diffraction, SEM, TGA, zetametry, and BET analysis. The adsorption properties of APNa-Y-zeolite were evaluated for the recovery of Cu(II), Cd(II), and Pb(II) from synthetic solutions prior to being tested for purity standards of drinking water. The properties of adsorption were profiled through the study of the effect of pH, adsorption isotherms, and uptake kinetics. The PSORE adhered to the kinetic profiles. Langmuir, Freundlich, and Sips equations were used to model adsorption. Variation of temperature was used as a benchmark to evaluate thermodynamic parameters. While the adsorption of Cu(II) and Cd(II) was endothermic, Pb(II) recovery was exothermic. Metal ions were effectively desorbed using 5 M HCl solutions. High concentrations of NaCl scarcely affect the sorption performance.

## 5. Biosorbents

The utility of a bacteria (*Nitrosomonas*)-modified zirconium Metal–Organic Framework (MOF) was tested for the remediation of toxic Cr(vi).<sup>171</sup> The proposed MOF-*Nitrosomonas* combination emphasized the crucial impact and convergence of biotechnology and porous materials to detoxify Cr(vi). Supported by composite analytical characterization techniques, chromium interaction with the biosorbent was well established. The porosity of the metal–organic framework in conjunction with the functional groups (NH<sub>2</sub>, COOH, and OH) on the bacterial cell surface enhances the affinity between the hydrochlorate anion and the biosorbent through an electrostatic interaction mechanism. With a Langmuir adsorption capacity of 23.69 mg g<sup>-1</sup>, facile



adsorption–desorption kinetics and favorable thermodynamics, a removal efficiency exceeding 95% was attained with this biosorbent. The proof of concept was verified in removing chromium in a certified rock phosphate sample with utmost efficiency. The biosorbent reusability was confirmed *via* facile desorption employing NaOH for three adsorption–desorption cycles. In principle, the microbe-modified MOF represents an interesting confluence of biotechnology and materials science towards the development of sustainable methods for removing various pollutants from the environment.

Spent *C. monacanthastem* (CS) is a copiously available agro-waste material that was experimented upon for adsorbing noxious pollutants from water systems. Toxic Cr(vi) adsorption has been verified by EDX and FTIR techniques. The adsorption behavior of the adsorbates was highly correlated with the pH of the solution.<sup>172</sup> The maximum adsorption of Cr(vi) was recorded at 2.0, and the maximum monolayer adsorption capacity ( $Q_m$ : mg g<sup>-1</sup>) of Cr(vi) was recorded to be 67.88 mg g<sup>-1</sup>. The thermodynamic evaluation confirmed the endothermic and spontaneous displacement of adsorbate ions from the aqueous phase. On the other hand, the desorption assessment showed that the adsorbate was efficiently removed from the adsorbent's surface with greater adsorption uptake (%) after five cycles. The use of CS-AC as an adsorbent for Cr(vi) was highly economic and competent, indicating potential use for detoxification of water.

The utilization of magnetic activated carbon modified with Poly Amidoxime (PAMC) as a potent methodology for chromium and thallium adsorption was studied.<sup>173</sup> Activated carbon was devised from waste rubber tires, subsequently altered with

magnetic properties, and then changed with poly amidoxime to provide more functional groups and thus improve the sorption efficiency. Tests were also carried out on real wastewater. With easy separation and high efficiency of removing chromium and thallium from water, besides reliable regeneration without significant loss in the capacity of adsorption, even after multiple cycles, the material exhibited encouraging potential as an adsorbent for treating water. The obtained result showed that the adsorbent works in a broad spectrum of pH from 3 to 11 and at an initial concentration of 1 to 20 ppm with an optimal shaking speed of 200 rpm. Adsorbents were easily displaced from the liquid after adsorption of the toxic pollutants from water; this indicates that PAMC has a promising method as an adsorbent for treating water.

Electrospinning allowed the facile synthesis of a mechanically stable nanofiber network, while hydrothermal treatment attained an  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanostructure surface coating that expanded the reactive surface area allocated for the uptake of dissolved metals.<sup>174</sup> Composite nanofibers of polyacrylonitrile (PAN) with embedded hematite ( $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>) nanoparticles were synthesized *via* a single-pot electrospinning synthesis. A core-shell nanofiber composite was also prepared through the subsequent hydrothermal growth of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanostructures on embedded hematite composites. These materials were tested for Cu(II), Pb(II), Cr(vi), and As(v) sorption. Although the uptake of Cu(II), Pb(II), Cr(vi), and As(v) was largely independent of the core-shell variables explored, metal uptake on embedded nanofibers was increased with  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> loading. Fig. 6 summarizes the incorporation of different metals into biosorbents.

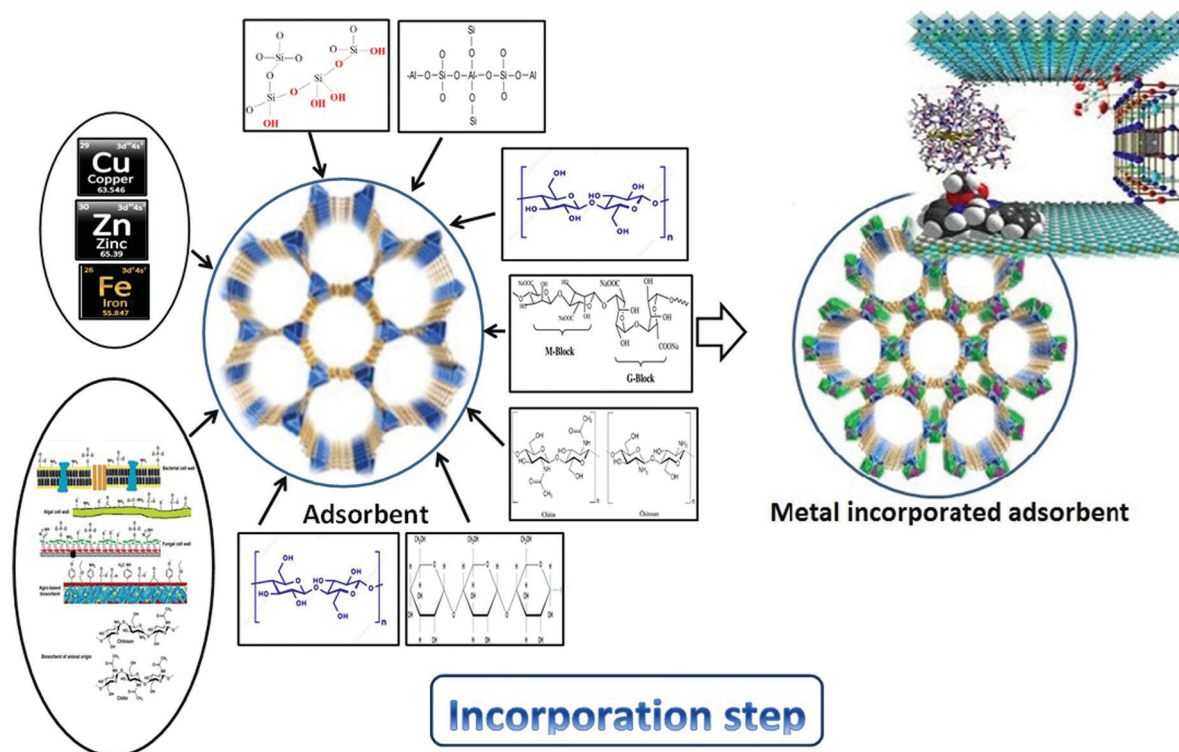


Fig. 6 Incorporation process using different adsorbents.







well-developed porous structure, proved to be beneficial for removing Cr(VI). The experiments of adsorption show that the hierarchical porous carbon is an exemplary Cr(VI) adsorbent with an adsorption aptitude of 463 mg g<sup>-1</sup> at pH 1. The developed porous carbon monolith maintains high selectivity for Cr(VI) ions in a coexisting system of Ni(II), Zn(II), and Cu(II). Therefore, this novel hierarchical porous carbon with controllable hierarchical porosity possesses good potential for water treatment application. Monolith strength improvement, adjustment of the carbon surface chemistry, and the performance in a more realistic water treatment system will be studied in our future work.

### 5.2. Cellulose-incorporating metals

Merging the advantages of both cellulose and an ionic liquid, Ionic Liquid-Functionalized Cellulose (ILFC) acting as an adsorbent was devised through radiation-grafting glycidyl methacrylate onto cellulose microspheres followed by reaction with ionic liquid 1-aminopropyl-3-methyl imidazolium nitrate.<sup>183</sup> The adsorption characteristics of removing Cr(VI) were evaluated in batch and column experiments. Taking other adsorbents into consideration, ILFC maintained quick and efficient adsorption properties with an adsorption capacity of 181.0 mg g<sup>-1</sup>. The test in simulated chrome-plating wastewater revealed that ILFC can selectively remove and separate Cr(VI) from the solution even when the concentrations of Cu(II), Zn(II), and Ni(II) are higher than that of Cr(VI) by ten times. Moreover, ILFC can be regenerated and reused six times without any apparent decrease in the adsorbed amount. Therefore, ILFC has reusability, practicality, and selectivity for the removal of Cr(VI), and is set to be a potential adsorbent for actual environmental wastewater.

Hydroxyethyl cellulose and CuO nanoparticles making up a clay-alumina ceramic composite membrane (CuO/HEC) were fabricated for separation of Cr(VI) and Pb(II) from contaminated water.<sup>184</sup> They were prepared by a slurry-casting method over a low-cost clay alumina ceramic substrate. It is believed that these CuO nanoparticle-containing clay-alumina ceramic composite membranes will be an effective solution for removing heavy metals from contaminated water. The prepared composite represents a reasonably high-performance novel ceramic UF membrane for the separation of toxic metal ions from mixed-salt solution. However, future study related to the use of the developed membrane for the treatment of real wastewater is necessary before implementation on a pilot scale.

Cellulose Aerogels (CA) and Zeolitic Imidazolate Framework-8 (ZIF-8) are combined into one highly functional aerogel for removing Cr(VI) from water through adsorptive means as a facile method of combining two emerging materials, by entrapping ZIF-8 particles into a flexible and porous CA (ZIF-8@CA).<sup>185</sup> The adsorption capacity of the cellulose aerogel for Cr(VI) was significantly increased when ZIF-8 was added, and the Langmuir maximum adsorption capacity reaches up to 41.84 mg g<sup>-1</sup>. This kind of material may also be extended to be used as air filters and sensors, and for substrate-supported catalysis.

An efficient adsorbent of bacterial cellulose/poly(*m*-phenylenediamine) (BC/PmPD) was prepared for removing Cr(VI) through

merging the merits of PmPD's high adsorption capacity and BC's ease of reclamation.<sup>186</sup> The Cr(VI) BC/PmPD adsorption was ascribed to the Cr(VI) adsorption on protonated -NH- and -NH<sub>2</sub> groups and the redox reaction of Cr(VI) to Cr(III) by the reduction of amine. Afterward, Cr(III) chelation on imino groups of PmPD took place. The calculated adsorption capacity of BC/PmPD for Cr(VI) was as high as 434.78 mg g<sup>-1</sup>. The Cr(VI) adsorption kinetics on BC/PmPD can be properly modeled by the pseudo-second-order kinetic model, placing the rate-controlling step as the chemical reaction. The findings in that study showed that BC/PmPD can be deemed as a potential adsorbent for removing Cr(VI) thanks to its efficient reclamation, high adsorption capacity, and good regeneration aptitude.

A composite adsorbent (PCA@AC) was successfully devised *via* cellulose (AC) as a substrate and poly(catechol tetraethylenepentamine-*p*-phenylenediamine) as a coating layer under a multitude of technical conditions.<sup>187</sup> This composite maintains a remarkable performance for removing Cr(VI) from aqueous solutions, surpassing pure AC. The PCA@AC maximum adsorption capacity for Cr(VI) is obtained as 507.61 mg g<sup>-1</sup> at 30 °C using the Langmuir model, surpassing pure AC. The removal ability of PCA@AC is attributed to the electrostatic interaction and reduction reaction of Cr(VI) to Cr(III) within the adsorption process. The composite adsorbent (PCA@AC) has great potential for Cr(VI)-wastewater purification with excellent chelating ability.

### 5.3. Starch-incorporating metals

The adsorption capacity of chemically modified potato starch (CPS) for Cr(VI) from an aqueous solution was simulated.<sup>188</sup> The material at hand is biodegradable and considered environmentally acceptable and safe. The hydroxyl, carbonyl, and carboxyl groups are responsible for the process of adsorption. The influence of different vital criteria, *e.g.*, time, pH, dose, and Cr(VI)'s initial concentration, on the adsorption capacity was evaluated. The Freundlich and the Redlich-Peterson isotherms well fitted the adsorption of Cr(VI) with chemically modified potato starch. The Cr(VI) removal kinetics using chemically modified potato starch were well explained by the second-order kinetic model. The thermodynamic prerequisites were also evaluated from the adsorption measurements. Among the different desorbing agents tested, 98.2% chromium recovery was achieved with 0.1 mol L<sup>-1</sup> NaOH.

Singh *et al.* (2014)<sup>189</sup> evaluated the effect of starch functionalization of iron oxide nanoparticles on their adsorption of Cr(VI) from aqueous solutions. Starch-Functionalized (SIONPs) as well as nonfunctionalized Iron Oxide Nanoparticles (IONPs) have been synthesized under different rates of addition of the base NaOH. The efficiency of SIONPs and IONPs for removal of hexavalent chromium from aqueous medium has been studied. The variation of the adsorption capacity with pH depends on the nanoparticle phase composition as well as its starch functionalization. Cr(VI) removal by SIONPs and IONPs follows a Langmuir adsorption isotherm. The highest monolayer saturation adsorption capacity as obtained from the Langmuir adsorption isotherm for SIONPs is 9.02 mg g<sup>-1</sup>.





other reported adsorptive materials, this core-shell/bead-like composite promises advantages of low cost, ultra-high adsorption capacity, environmental friendliness, and exemplary recycling performance.

Alginate can be made into various usable forms like membranes, beads, and candles for water remediation. To prepare alginate in a usable bead form, magnetic nano-hydroxyapatite encapsulated alginate beads ( $\text{Fe}_3\text{O}_4@\text{n-HApAlg}$ ) were devised by a hydrothermal method for selective removal of chromium.<sup>196</sup> The thermodynamic studies imply the spontaneous and endothermic nature of the sorption of  $\text{Cr}(\text{VI})$ .  $\text{Fe}_3\text{O}_4@\text{n-HApAlg}$  beads were made usable by using NaOH eluent, up to five cycles. The magnetic alginate hybrid beads showed promising results against chromium-contaminated groundwater by removing  $\text{Cr}(\text{VI})$  ions below the tolerance limit. Regeneration and reusability assessments were successfully conducted, and the hybrid beads can be reused for up to five successive cycles. The synthesized  $\text{Fe}_3\text{O}_4@\text{n-HApAlg}$  beads were an optimal material for the treatment of  $\text{Cr}(\text{VI})$ -contaminated field water.

Removing  $\text{Cr}(\text{VI})$  using NZVI immobilized in alginate beads (NZVI beads) and a bacterial consortium immobilized in alginate beads (bio beads) in a sequence process was performed.<sup>197</sup> The process utilizing the NZVI beads and bio beads was successfully analyzed with a  $\text{Cr}(\text{VI})$ -spiked groundwater sample. The efficiency of removing  $\text{Cr}(\text{VI})$  was observed to upscale (more than  $90 \pm 5.96\%$  at  $381 \pm 17.1 \text{ mg g}^{-1}$  capacity for a  $10 \text{ mg L}^{-1}$  influent concentration) using NZVI beads and microbial consortium immobilized beads in sequence. The system was successfully assessed with real water systems, having direct field applicability for that process.

The suitability of the Ca-alginate immobilized consortium SFC 500-1 for simultaneous removal of  $\text{Cr}(\text{VI})$  and phenol was demonstrated.<sup>198</sup> Immobilization was a successful strategy to enhance the removal of  $\text{Cr}(\text{VI})$ , mostly associated with enzymatic reduction through the synthesis of  $\text{Cr}(\text{III})$ . The immobilized SFC 500-1 showed great prowess in degrading phenol in a short time, probably due to the protective impact of the alginate matrix against the toxicity of phenol concentrations over  $1000 \text{ mg L}^{-1}$ . Complete phenol oxidation to catechol and *cis*-muconate was verified through the detection of these intermediates in the reaction medium during the co-remediation process. The optimum long-term storage, removal potential, and reusability make SFC 500-1 entrapped cells an interesting system for the removal of  $\text{Cr}(\text{VI})$  and phenol in media of low-concentration organic matter. The low-cost and high-resistance alginate matrix exhibits more merits when possible applications for the decontamination of real effluents are considered.

### 5.5. Chitin and chitosan incorporating metals

Sargin *et al.* (2019)<sup>199</sup> produced three-dimensional chitinous microcages and their iron-based magnetic particle loaded counterparts from ephippial resting eggs of a cladoceran species (*D. longispina*). FTIR spectra analysis revealed that the microcages produced from ephippial resting eggs consisted of  $\alpha$ -chitin. SEM-EDX analysis confirmed the incorporation of the magnetic particles into the chitinous microcages. The findings of heavy

metal sorption experiments demonstrated that the magnetic particles enhanced the affinity of the chitinous-microcages for  $\text{Cd}(\text{II})$ ,  $\text{Cu}(\text{II})$ , and  $\text{Ni}(\text{II})$  ions. In conclusion, it was revealed that these biological materials are optimal sorbents for heavy metal ions. These newly produced materials also can possess the potential for biotechnological applications in various areas in further studies.

Ali (2018)<sup>200</sup> prepared chitosan-1,2-cyclohexylenedinitrilotetraacetic acid/graphene oxide (chitosan/CDTA/GO) nanocomposite in the presence of glutaraldehyde as a cross-linker. The removal efficiency and adsorption of  $\text{Cr}(\text{VI})$  utilizing the chitosan/CDTA/GO adsorbent were investigated at various adsorption conditions. The prepared adsorbent at hand was characterized by SEM and FTIR. The effects of the adsorbent chemical composition, CDTA/GO concentration, adsorbent dose, pH, temperature, time of contact, and initial metal ion concentration on  $\text{Cr}(\text{VI})$  sorption were investigated. The results showed that the optimum adsorbent dose was  $2 \text{ g L}^{-1}$  at a pH value of 3.5 and an equilibrium time of 60 min. Besides, the temperature and pH immensely influenced the adsorption process. The  $\text{Cr}(\text{VI})$  adsorption kinetics onto Cs/CDTA/GO followed the pseudo-second-order model and the adsorption isotherm adhered to the Langmuir model. The maximum adsorption capacity of the adsorbent was  $166.98 \text{ mg g}^{-1}$ , and the equilibrium parameter ( $R_L$ ) at different concentrations was less than unity, indicating that  $\text{Cr}(\text{VI})$  ion adsorption onto chitosan/CDTA/GO is favorable. The chitosan/CDTA/GO adsorbent could be regenerated more than three times according to its adsorption-desorption cycles.

Chitosan and alginate nanocomposites were evaluated for chromium(VI) removal from wastewater.<sup>201</sup> The sorbent was characterized by XRD, FT-IR, SEM, DLS, and DSC. Batch adsorption experiments were carried out to evaluate the removal process under various factors like the effects of the initial concentration, dose of adsorbent, pH value, and agitation time. The pH-dependent metal ion removal reached the optimum at pH 5.0. The experimental data were analyzed by the Freundlich and Langmuir isotherms. The isotherm study revealed that the adsorption equilibrium is adherent to the Freundlich isotherm and the sorption extent of alginate and chitosan nanocomposites is very high, and the adsorbent favors multilayer adsorption. Pseudo-first and second-order kinetics models were used to illustrate the kinetic data. It was determined that removing  $\text{Cr}(\text{VI})$  adhered to second-order reaction kinetics. It is concluded that alginate and chitosan nanocomposites are exemplary biosorbents material for adsorbing  $\text{Cr}(\text{VI})$  from wastewater.

Zirconium(IV) cross-linked chitosan magnetic microspheres ( $\text{Fe}_3\text{O}_4@\text{Zr-chitosan}$ ) as a recoverable adsorbent were fabricated through the coordination reaction between zirconium oxychloride and a chitosan biopolymeric matrix for efficient adsorption and simultaneous detoxification of  $\text{Cr}(\text{VI})$  in aqueous solutions.<sup>202</sup> XRD and SEM verified the formation of core@shell magnetite microspheres. XPS and FT-IR confirmed Zr(IV)'s cross-linking with chitosan on the microspheres. The batch  $\text{Cr}(\text{VI})$  adsorption performances of the resultant  $\text{Fe}_3\text{O}_4@\text{Zr-chitosan}$  microspheres



showed that a maximum adsorption capacity of 280.97 mg g<sup>-1</sup> was achieved under pH 4.0 at 298 K. The XPS analyses indicated that 61.1% of the adsorbed Cr(vi) was reduced to Cr(III) because of the oxidization of alcoholic groups on C-6 in chitosan serving as electron donors to carbonyl groups. The adsorbent showed preferential Cr(vi) adsorption with the existence of coexisting cations (K<sup>+</sup>, Na<sup>+</sup>, Cu<sup>2+</sup>, Zn<sup>2+</sup>, Ca<sup>2+</sup>, and Mg<sup>2+</sup>) and anions (NO<sub>3</sub><sup>-</sup>, Cl<sup>-</sup>, SO<sub>4</sub><sup>-2</sup>, and CO<sub>3</sub><sup>-2</sup>). The adsorbent maintained excellent reusability and lowered the effluent Cr(vi) contents down to the ppb level, reaching the drinking water standard recommended by the World Health Organization, and was a potential option for water purification.

Chitosan-Fe(OH)<sub>3</sub> beads were one-step synthesized without using acid solvents, which could be used as effective adsorbents for anionic dye removal. The preparation process was simple and green.<sup>203</sup> The prepared beads were characterized by morphological and structural analyses in detail using several techniques, e.g., SRD, SEM, XRD, TGA, and XPS. The Fe(OH)<sub>3</sub> content in the chitosan-Fe(OH)<sub>3</sub> beads was 54.64 wt%. The removal efficiencies towards anionic dyes, Congo Red (CR) and Methyl Orange (MO), by the chitosan-Fe(OH)<sub>3</sub> beads surpassed the pure chitosan beads. Moreover, incorporating Fe(OH)<sub>3</sub> into chitosan beads could overcome the shortcoming that powdery Fe(OH)<sub>3</sub> particles are not easy to separate from adsorption solutions. The maximum adsorption capacities from the Langmuir model for CR and MO by the chitosan-Fe(OH)<sub>3</sub> beads were 445.32 and 314.45 mg g<sup>-1</sup>, respectively. The calculated thermodynamic parameters, namely  $\Delta G^\circ$ ,  $\Delta H^\circ$ , and  $\Delta S^\circ$ , suggest that adsorption of CR and MO was endothermic and spontaneous in the temperature range 293–353 K. More importantly, the chitosan-Fe(OH)<sub>3</sub> beads can be regenerated and the adsorption properties reset after NaOH treatment. The desorption results showed that the adsorption capacity can remain up to 95% after being used five times. Moreover, the chitosan-Fe(OH)<sub>3</sub> beads additionally exhibited good reusability and the efficiencies for the removal of both dyes surpassed 95% after five cycles. From this work, it is suggested that chitosan-Fe(OH)<sub>3</sub> beads have great potential as effective and low-cost adsorbents for removing anionic dyes.

Bimetallic Fe/Cu nanoparticles were successfully stabilized by chitosan and then used for remediating Cr(vi)-contaminated wastewater.<sup>204</sup> However, the overloaded chitosan on the surface of Fe/Cu particles limited the reduction of Cr(vi) due to the occupation of the surface reactive sites. Most importantly, the contribution of chitosan and Cu in the removal mechanism was studied by reduction experiments and XPS analysis. On one hand, chitosan could effectively combine with Cr(vi) due to chelation; on the other hand, Cu played an important role in the precipitation and coprecipitation phenomena. These findings dictate that CS-Fe/Cu has the potential to be a promising material for wastewater treatment.

The preparation of Cu<sub>2</sub>S-chitosan nanocomposites for removing Cr(vi) ions from wastewater samples was achieved.<sup>205</sup> Structural studies of the particles were carried out using TEM and XRD. The XRD patterns presented the cubic Cu<sub>1.8</sub>S phase for all the synthesized copper sulfide nanoparticles. TEM images showed spherical

shape particles which became agglomerated when the stabilizers were introduced into the nanomaterial. The adsorption studies proved that the pH value, dosage, and time of contact play an important part during the water treatment.

Guo *et al.* (2018)<sup>206</sup> synthesized polydopamine-modified-chitosan (CS-PDA) aerogels through dopamine self-polymerization and glutaraldehyde cross-linking reactions to increase the capacity of adsorption and acid resistance of chitosan. CS-PDA were applied in the adsorption of Cr(vi) and Pb(II). CS-PDA exhibited superior adsorption performances in removing Cr(vi) and Pb(II). The adsorption isotherms and kinetic data were adherent to the Langmuir and pseudo-second-order kinetic models. The maximum adsorption capacities of CS-PDA for Cr(vi) and Pb(II) were 374.4 and 441.2 mg g<sup>-1</sup>, respectively. After eight cycles, the CS-PDA adsorption capacity showed no obvious decline. These superiorities make CS-PDA a promising multifunctional adsorbent for the purification of metal ions and dyes.

A chitosan-grafted graphene oxide (CS-GO) nanocomposite was tested for the adsorption of Cr(vi) in batch mode.<sup>207</sup> The CS-GO nanocomposite material was prepared by the ultrasonic irradiation technique. The CS-GO adsorbent was characterized by XRD, FTIR spectroscopy, SEM, and TEM. An adsorption capacity of 104.16 mg g<sup>-1</sup> was achieved at pH 2.0, at a contact time of 420 min. The adsorption process was confirmed by the pseudo-second-order kinetic and Langmuir isotherm models. The nano-microstructural investigation validates the successful Cr(vi) adsorption on the CS-GO nanocomposite. The CS-GO material is recyclable for up to ten cycles with a minimum loss in adsorption capacity.

Thiosemicarbazide-modified chitosan (TSFCS) was fabricated and characterized by SEM, FTIR, and TGA techniques and its application as an adsorbent for the displacement of Pb(II) and methyl red (MR) was evaluated.<sup>208</sup> Some adsorption parameters, e.g., the dose of sorbent, pH value, and initial concentration of solutions, were evaluated alongside their effects. The maximum removal percentages for MR and Pb(II) were found to be about 91% and 85.6% at pH values 8 and 5 and sorbent dosages of 3.33 g L<sup>-1</sup> and 1.33 g L<sup>-1</sup>, respectively. Langmuir, Freundlich, and Temkin isotherms were evaluated and the maximum adsorption extents for Pb(II) and MR were found to be 56.89 mg g<sup>-1</sup> and 17.31 mg g<sup>-1</sup> at 55 °C and 25 °C, respectively. Isotherm studies indicate that Pb(II) and MR adsorption adhere to the Freundlich and Langmuir models, respectively. The kinetics of adsorption was more accurately adherent to the PSORE. Thermodynamic parameters including  $\Delta G^\circ$ ,  $\Delta H^\circ$ , and  $\Delta S^\circ$  were gauged over the temperature range of 25–55 °C. The sorption process was endothermic and spontaneous.

Neto *et al.* (2019)<sup>209</sup> prepared an adsorbent in the form of an iron oxide/carbon nanotube/chitosan magnetic composite film (CLCh/MWCNT/Fe). CLCh/MWCNT/Fe was characterized by Inductively Coupled Plasma Mass Spectrometry (ICP-MS), nitrogen adsorption/desorption, SEM, XRD, Energy-Dispersive Spectrometry (EDS), Raman spectroscopy, and IR. The CLCh/MWCNT/Fe film presented a maximum adsorption capacity of 449.30 mg g<sup>-1</sup> for Cr(vi) (60 min) at 25 °C. In ten consecutive reutilization adsorption





cycles, the CLCh/MWCNT/Fe film suffered efficiency losses of only 12% and 6% for the removal of Cr(III) and Cr(VI), respectively.

## 6. Adsorbent regeneration

A suitable adsorbent for metal ion removal should not only have high sorption capacity and feasibility but should also be amenable to easy desorption of the sorbed metal ion as well, to be efficiently regenerated and reusable for a long time. Desorption of metal ions is done by leaching of sorbed metal ions using bases, acids, and salts and chelating agents. In some cases, desorption may be done using a combination of salts and bases. High concentrations of bases and acids do not suit certain sorbents (oxides such as Si, Fe, and Al and carbonates of Ca and Mg) because they can dissolve or corrode parts of the sorbents, structurally changing or damaging them; this negatively affects regeneration and reuse of the sorbents. The search for a suitable eluent for the new prepared materials needs further investigation; the eluent type, volume, concentration, and regeneration kinetics needs further investigations. The stability of the adsorbent incorporating metal or mineral should be investigated using FTIR, SEM, TEM and XRD during successive desorption cycles along with the analysis of the released metals during desorption cycles.

## 7. Prospects for future research

Incorporation of metals/minerals can enhance their sorption behavior compared with metal/mineral free materials; however, the risk of release of the incorporated metals under different adsorption conditions such as pH and time needs further investigation. Also the release of these metals during successive adsorption/desorption cycles is an important issue. Also the authors propose a detailed desorption study to optimize the desorption conditions (*i.e.* optimum pH, eluent concentration, desorption kinetics, equilibrium parameters, desorption temperature and thermodynamics). Moreover the effect of several industrial factors such as microwave radiation and ultrasonic power on the sorption/desorption behavior of these materials needs to be investigated. Eventually, a multiply reused sorbent resin can no longer be regenerated and will require disposal. It is very important to dispose of the spent sorbents in an environmentally friendly way. If this waste is not managed and destroyed in a proper manner it can create health and environmental risks. Only limited studies are available in the literature about the safe disposal of the spent sorbents. The disposal options and costs of the spent material will generally depend on whether or not the materials are hazardous. Several options are available such as (i) converting the adsorbent to energy – this is the process of generating energy in the form of electricity and/or heat from the primary treatment of the exhausted sorbent. (ii) Incineration of the adsorbent, converting it to a char based adsorbent, and then reuse. (iii) Landfill – for landfilling, the toxicity characteristic leaching procedure determines the toxic hazards of a spent adsorbent. Additional studies may be

needed to adequately predict any environmental or health threat from landfilling for the spent adsorbent.

## 8. Conclusion

The current immobilization methods of metals/minerals onto sorbents mainly include adsorption, crosslinking, and embedding methods. Among them, embedding is the most used method. The cross-linking method is usually used in combination with the sorption and embedding methods. This review investigates the use of metal/mineral-incorporating sorbents and biosorbents for water pollutant removal with a special focus on Cr(VI). It was illustrated from this article that the incorporation of metals/minerals with several sorbents and biosorbents elevates the sorption potential of these materials alongside the separation ease of suspending adsorbents in the case of magnetite incorporation. Moreover, the sorption process kinetics depends on several factors such as the surface properties and operational factors such as pH, sorbent dose, temperature, and the initial concentration of pollutants. Secondly, biosorbents have an advantage over other sorbents in being naturally available with high abundance and renewability. Incorporation of metals/minerals can enhance their sorption behavior compared with metal/mineral free materials; however, this may increase the remediation expenses and introduce new materials into the environment. Furthermore, the risk of release of the incorporated metals during sorption needs further investigation. Finally, it is very important to dispose of the spent sorbents in an environmentally friendly way. Only limited studies are available in the literature about the safe disposal of the spent sorbents. Eventually, a multiply reused sorbent resin can no longer be regenerated and will require disposal. The disposal options and costs of the spent material will generally depend on whether or not the materials are hazardous.

## Nomenclature

$C_0$	Sorbate initial concentration ( $\text{mol L}^{-1}$ )
$C_e$	The equilibrium concentration ( $\text{mol L}^{-1}$ )
$q_e$	The amount of sorbate sorbed in the adsorbent at equilibrium ( $\text{mol g}^{-1}$ )
$q_{m,L}$	The capacity of maximum monolayer ( $\text{mol g}^{-1}$ )
$K_L$	Langmuir isotherm constant ( $\text{L mol}^{-1}$ )
$K_F$	Freundlich constant relative sorption capacity ( $\text{mol g}^{-1}$ ) ( $\text{L mol}^{-1}$ ) <sup>1/n</sup>
$n$	Sorption intensity
$R$	Universal gas constant ( $8.314 \text{ J mol}^{-1} \text{ K}^{-1}$ )
$T$	Temperature (K)
$A_T$	Temkin isotherm equilibrium constant ( $\text{L g}^{-1}$ )
$b_T$	Temkin isotherm constant ( $\text{J mol}^{-1}$ )
$\varepsilon$	The Polanyi potential ( $\text{J}^2 \text{ mol}^{-2}$ )
$q_s$	Theoretical isotherm saturation capacity ( $\text{mol g}^{-1}$ )



$\beta$	Dubinin–Radushkevich isotherm constant ( $\text{mol}^2 \text{kJ}^{-2}$ )
$\theta$	Degree of surface coverage
$K_{\text{FH}}$	Flory–Huggins isotherm equilibrium constant ( $\text{L g}^{-1}$ )
$K_{\text{D}}$	Hill constant
$n_{\text{H}}$	Hill cooperativity coefficient of the binding interaction
$q_{\text{sH}}$	Hill isotherm maximum uptake saturation ( $\text{mol L}^{-1}$ )
$K_{\text{R}}$	Redlich–Peterson isotherm constant ( $\text{L g}^{-1}$ )
$a_{\text{R}}$	Redlich–Peterson isotherm constant ( $\text{L mol}^{-1}$ )
$g$	Redlich–Peterson isotherm exponent
$K_{\text{S}}$	Sips isotherm model constant ( $\text{L mg}^{-1}$ )
$\beta_{\text{S}}$	Sips isotherm model exponent
$K_{\text{T}}$	Toth isotherm constant ( $\text{mol g}^{-1}$ )
$B$	Koble–Corrigan isotherm constant ( $\text{L mol}^{-1}$ ) <sup><math>n</math></sup>
$A$	Koble–Corrigan isotherm constant ( $\text{L}^n \text{mol}^{1-n} \text{g}^{-1}$ )
$b_{\text{k}}$	Khan isotherm model constant
$\alpha_{\text{k}}$	Khan isotherm model exponent
$\alpha_{\text{RP}}$	Radke–Prausnitz isotherm model constant
$\beta_{\text{R}}$	Radke–Prausnitz isotherm model exponent
$\gamma_{\text{R}}$	Radke–Prausnitz isotherm model constant
$\alpha$	Frenkel–Halsey–Hill isotherm constant ( $\text{J mol}^{-1}$ )
$r$	Sign of inverse power of distance from the surface
$d$	Interlayer spacing (m)
$k$	MacMillan–Teller (MET) isotherm constant
$q_t$	Amount of metal ions sorbed at time $t$ ( $\text{mmol g}^{-1}$ )
$K_1$	Pseudo-first-order rate constant of adsorption ( $\text{min}^{-1}$ )
$K_2$	Pseudo-second-order rate constant of adsorption ( $\text{g mmol}^{-1} \text{min}^{-1}$ )
$K_i$	The intra-particle diffusion rate ( $\text{mmol g}^{-1} \text{min}^{-0.5}$ )
$X$	The boundary layer diffusion effects ( $\text{mmol g}^{-1}$ )
$\alpha$	The initial sorption rate ( $\text{mmol g}^{-1} \text{min}^{-1}$ )
$\beta$	The desorption constant ( $\text{g mmol}^{-1}$ )

## Conflicts of interest

The authors declare that they have no known competing financial interests or personal relationships that could have influenced the work reported in this paper.

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