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The solid-state physicochemical properties and biogas production of the anaerobic digestion of corn straw pretreated by microwave irradiation

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The effect of different temperatures used in microwave pretreatment on enhancing methane production of corn straw was comparatively studied in this paper through the analysis of the physicochemical properties of the pretreated materials and the methane yield during anaerobic digestion. Analytic methods such as scanning electron microscopy, Fourier transform infrared spectroscopy, and X-ray diffraction were performed to detect the surface chemistry of the pretreated corn straw. The results indicated that microwave pretreatment could effectively disrupt the lignocellulosic structure to release cellulose, hemicellulose, and related derivatives and make them available for the process of anaerobic digestion. The outcome of the methanogenic assay demonstrated that methane production could be significantly improved by 73.08% concerning the variation of the temperatures in microwave pretreatment. This study provides technical support for pretreatment methods of lignocellulose materials and deems that microwave pretreatment boosts methane yield efficiently during the process of anaerobic digestion of lignocellulosic materials.

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1. Introduction

It is well known that the exorbitant and inappropriate use of fossil resources and the continuing increase in energy security concerns have driven researchers to seek renewable and environmentally friendly energy resources that could play a crucial role in the replacement of fossil fuels.^{1,2} As a promising means of production for second-generation biofuels from lower-value and abundant substrates such as lignocellulosic materials, there are high hopes resting on biogas to not only mitigate the undesirable impacts of fossil fuels and solve the challenge of replacing them, but also to significantly enhance ecological effects on a global scale.³ Anaerobic digestion technology is one of the most efficient and environmentally friendly approaches to obtain biogas with a rich content of methane produced by lignocellulosic substrates, which will be widely employed to take the place of fossil fuels.⁴ 280 million tons of corn straw (CS), an agricultural residue, are produced in China yearly.⁵ Due to its high availability, CS is the most abundant biomass energy resource of lignocellulosic waste that can be used as a substrate for bioenergy production *via* anaerobic digestion.⁶

It is generally accepted that four major steps based on the differences in the microorganism are used to describe the sequential process in the anaerobic digestion of particulate materials and macromolecules, which include hydrolysis, acidogenesis, acetogenesis, and methanogenesis.⁷ Hydrolytic bacteria decompose complex organic matter into soluble monomers through their secreted extracellular enzymes. Acidogenic and acetogenic bacteria take advantage of monomers to generate acetic acid, hydrogen, and carbon dioxide, which are then used as substrates for methanogenic bacteria to yield biogas.⁸ On the other hand, hydrolysis is the most critical and rate-limiting of these different steps.⁹

Typically, CS is mainly composed of cellulose, hemicellulose, and lignin, shaping a complicated organic polymer crystal structure.¹⁰ Unlike starch and sucrose, which can be easily broken down into carbohydrates, the lignin and hemicellulose in CS are tightly embedded in the cellulose, resulting in crystallization and lignification, which expresses the low accessibility of cellulose to microorganisms and makes the cell wall more recalcitrant towards hydrolysis in the anaerobic digestion process. Meanwhile, the wax layer on the surface of CS is not beneficial to the adhesion of microorganisms, which leads to it being difficult for the microorganisms to utilize CS to produce biogas. According to a previous report, only a 20% maximum sugar yield, in theory, could be gained from hydrolysis of lignocellulosic biomass without any of the pretreated approaches.^{11,12} Therefore, appropriate pretreatment methods should be introduced to disrupt the heterogeneous matrix and

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then partially remove the lignin to increase the specific surface area and porosity of the cellulosic materials, which favors the degradation and conversion of lignocellulose materials.¹³

As a rule, there are numerous kinds of pretreatment methods that can enhance biogas production from lignocellulosic biomass, which have been classified into several categories: physical (*i.e.*, microwave irradiation, extrusion, and hot water), chemical (*i.e.*, alkaline and acidic), and biological (*i.e.*, a fungal thermophilic microbial consortium) or a combination of two or more of these methods.^{14,15} Among these technologies, the microwave pretreatment method is an efficient heating treatment which can shorten the processing time and consume less energy because of the thermal and non-thermal effects elicited by the radiation in the presence of water.¹⁶ Thermal effects embody the generation of internal heat by radiation due to the local temperature rise, which results in so-called rapid local heating.¹⁷ Conversely, non-thermal effects include the oscillation of polar bonds, which further leads to the fracture of bonds and the acceleration of chemical and physical processes.¹⁸ Microwave pretreatment can change the biomass structure, increase the specific surface area, and reduce the polymerization crystallinity of lignocellulose. It was reported previously in the literature that the lignin removal rate could reach 6% in microwave pretreatment of 700 W (30 min), which meant that the hydrolysis rate of the enzyme during the anaerobic digestion process was improved.¹⁹ Beszédes *et al.* observed that microwave pretreatment enhances the COD solubilization of dairy-industry and meat-processing sludge. Besides, the total biogas yield considerably improved and the initial lag-phase of anaerobic digestion decreased.²⁰ A 28% increase in methane yield compared with the control group after microwave pretreatment of CS was found by Jackowiak.²¹ Accordingly, the physicochemical properties of lignocellulosic biomass after pretreatment were analyzed by SEM, FTIR, XRD, *etc.* Kupryaniuk *et al.* found that during the degradation process, the selection of appropriate agents could significantly accelerate the degradation of the main structures of lignocellulose through FTIR.²² Similarly, SEM and FTIR results revealed the surface disruption and lignin removal impacts of pretreatment.²³ Nevertheless, there are few reports in the literature on the solid-state characteristics of CS pretreated by different microwave temperatures and the biogas production of the pretreated solid-phase as a substrate in anaerobic fermentation.

In this paper, the microwave pretreatment method was introduced for the sake of considerable methane production. The physicochemical properties of CS pretreated at different temperatures of microwave pretreatment and the methane yield produced in the subsequent anaerobic digestion were investigated. Moreover, the optimal temperature was selected by comparing methane yield in the anaerobic fermentation of the CS solid-phase under various temperature of microwave pretreatment, which offers efficient technical support for the pretreatment techniques to enhance anaerobic fermentation from CS.

2. Materials and methods

2.1. Substrate

The CS used in this study was collected from an experimental field of the Northwest Agriculture and Forestry University in

Yangling in the Shaanxi Province. After drying at 65 °C to a constant weight, it was milled to pieces in an 18 mesh using a laboratory-scale grinder. The ground CS was sealed in a plastic bag and stored at 4 °C before use. The total solid (TS) content, volatile solid (VS) content, and carbon/nitrogen ratio (C/N) of CS in this paper were 96.15%, 88.26% (based on the dry matter), and 42.35, respectively.

The inocula for anaerobic digestion were derived from domestication in the laboratory at 35 °C, a substrate with a TS of 1% (pig manure : bovine powder = 1 : 1) and 5 g L⁻¹ sodium acetate was added. The domestication was considered to be finished when the daily gas production was lower than 1% of the cumulative gas production. The pH value, TS content, and VS content of the inocula were 7.6, 6.53%, and 3.47% (based on the dry matter), respectively.

2.2. Experimental setup

2.2.1. Microwave pretreatment. Microwave pretreatment was conducted in a microwave hydrothermal synthesizer (XH-800SE, Xianghu Science Co., Ltd; China; 0–1600 W power output; 2.45 GHz frequency; pressure range, 0–6 MPa; temperature range, 0–260 °C). A vessel with a volume of 100 mL in the cavity was equipped with pressure and temperature sensors on the top. The five pretreatment groups in the experiment, which consisted of the different pretreatment temperatures of 120 °C, 150 °C, 180 °C, and 210 °C with the corresponding input power and untreated straw and the duration of the microwave pretreatment set at 10 minutes, were labeled as M120-10, M150-10, M180-10, M210-10, and CK, respectively. The heating time was recorded when the temperature of the vessel reached the setup level. The 5 g dry matter and 50 mL deionized water (with a solid to liquid ratio of 1 : 10) were thoroughly stirred and then poured into the vessel for microwave heating. The slurry in this vessel started cooling down to ambient temperature after 10 minutes of heating and then the solid and fluid fractions were separated by filtration with a funnel. The pretreated particles were washed repeatedly with deionized water and dried in a constant temperature oven at 105 °C for 24 hours. Then the resultant solid fraction was further subjected to analysis of the physicochemical properties and the anaerobic digestion experiment was carried out.

2.2.2. Biochemical methane potential (BMP) assays. The experiment in batches was carried out in a 500 mL wide-mouthed bottle with a 400 mL working volume. A 400 mL digested solution consisting of 24 g (relating to the dry matter) pretreated or raw materials to satisfy the 6% TS concentration and 120 mL inoculums as well as a certain amount of distilled water. The pH value and C/N of the digestive solution were adjusted to be about 7.0 and 30.0 with sodium hydroxide and ammonium chloride, respectively. The headspace of the wide-mouthed bottle was flushed with pure N₂ gas for 2 minutes to remove the oxygen. Subsequently, those bottles were sealed with rubber stoppers at once and a biochemical methane potential experiment was performed in an incubator with a constant temperature of 37 °C. Besides, each assay was set up with three parallel groups to determine the reproducibility of the experiments, and the average value of the three groups was



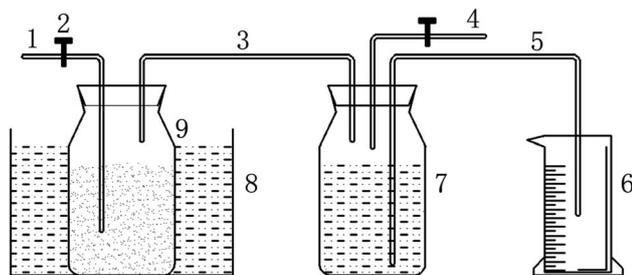


Fig. 1 A schematic figure of the anaerobic fermentation equipment. (1) Sampling vent; (2) valve; (3) airway; (4) gas-sampling vent; (5) aqueduct; (6) graduated cylinder; (7) biogas-collecting flask; (8) constant temperature trough; (9) fermentation flask.

used in the analysis. During the experiment, all the digesters were manually shaken twice a day for 20 seconds. The volume of biogas produced was measured by the water displacement method,²⁴ which is elucidated in Fig. 1, and the biogas composition was analyzed using gas chromatography (GC-2014C; Shimadzu, Japan).

2.3. Analysis and calculations

2.3.1. Physicochemical analysis. The TS and VS contents of the CS and inoculum were determined according to the standard methods, in which TS and VS were measured by the change of quality dried at 105 °C for 24 h and 550 °C for 4 h, respectively.²⁵ The solid recovery was determined by weighing the samples before and after pretreatments, after drying in a hot air oven at 105 °C for 24 h. A portable pH meter (DZS-706; INESA Scientific Instrument Co., Ltd, China) was used for measuring the pH during the anaerobic digestion process. The elemental composition of CS was determined by using an elemental analyzer (EA3000; Euro Vector, Italy). The chemical constitution of cellulose, hemicellulose, and lignin was quantified *via* Van Soest's method.²⁶ The methane concentration was determined by gas chromatography (GC-2014C; Shimadzu, Japan).²⁷

2.3.2. The properties of corn straw. A scanning electron microscope (TM3030; Shimadzu, Japan) was applied to observe the microstructural changes of the pretreated and untreated samples for the CS. During SEM analysis, the dehydrated samples were bonded to the stub with carbon-tape, and then images were formed after sputter-coating with metal nanoparticles.²⁸ The pretreated and untreated CS samples used for Fourier transform infrared spectrophotometry (Nicolet iS10; Thermo Fisher Scientific, USA) analysis were ground into a powder and then ground with KBr in the ratio of 1 : 100, which were pressed at approximately 10 MPa pressure to form a uniform 13 mm diameter sample disc for further analysis. The spectra were detected in the wavelength ranging from 4000 cm⁻¹ to 400 cm⁻¹ at the resolution of 0.5 cm⁻¹. The background spectrum of pure potassium bromide was subtracted from the sample spectrum. All the spectra were measured at ambient temperature.²⁹ The crystallinity index (CrI) of the untreated and pretreated CS samples was determined by X-ray diffraction (XRD) analysis (D8 ADVANCE A25; Bruker, Germany) operated at 40 kV and a tube current of 40

mA. Samples were recorded over the range of $2\theta = 10\text{--}50^\circ$ at a scan speed of 5° min^{-1} with a step size of 0.02° . The CrI was calculated according to the following eqn (1)³⁰

$$\text{CrI} = [(I_{002} - I_{\text{am}})/I_{002}] \times 100 \quad (1)$$

where I_{002} (crystallinity fraction) is the intensity from the 002 planes at $2\theta = 22.2^\circ$ and I_{am} (amorphous fraction) is the intensity of the background measured at $2\theta = 18.7^\circ$ (ref. 31 and 32) without considering the influence of lattice distortion, the microcrystalline size can be calculated according to Scherrer's formula

$$D = KL/(\beta \cos \theta) \quad (2)$$

where D represents the size of the microcrystal perpendicular to the direction of the reflector (nm), L denotes the X-ray wavelength (0.154 nm), K is Scherrer's constant (0.9), θ characterizes the diffraction angle ($^\circ$), and β delegates the corresponding half-height width of the diffraction peak.

2.3.3. Data analysis. The method which was described by Van Soest³³ was used to determine the cellulose, hemicellulose, and lignin content in CS. Acid detergent fiber (ADF), neutral detergent fiber (NDF), the residue after 72% H₂SO₄ treatment, and acid detergent lignin (ADL) were determined to calculate the contents of cellulose, hemicellulose, and lignin. The calculation equations are as follows:

$$\text{Hemicellulose (\%)} = \text{NDF (\%)} - \text{ADF (\%)} \quad (3)$$

$$\text{Lignin (\%)} = \text{ADL (\%)} \quad (4)$$

$$\text{Cellulose (\%)} = \text{ADF (\%)} - \text{residue after 72\% H}_2\text{SO}_4 \text{ (\%)} \quad (5)$$

The modified Gompertzian model³⁴ was employed to fit the cumulative methane yield curves for each pretreatment group during batch anaerobic digestion to obtain the maximum CH₄ production potential (P), CH₄ production rate (R), and lag phase (λ) as shown in eqn (5)

$$M = P \times \exp\{-\exp[(R \times e)/P \times (\lambda - t) + 1]\} \quad (6)$$

where M is the cumulative CH₄ production (mL per gVS_{added}) over time t (day), P is the maximum CH₄ potential (mL per gVS_{added}), R is the maximum CH₄ production rate (mL per gVS_{added} per d), λ is the lag phase (day) and 'e' is $\exp(1) = 2.71828$. The three parameters P , R , and λ were obtained by the nonlinear fit program in Origin 2021. The regression value (adj- R^2) and root mean square error (RMSE) were used to measure the degree that the kinetic model fitted the methane production curve.

All the data in this paper were analyzed by SPSS 22.0, and the corresponding figures were drawn by Origin 2021 for Windows.

3. Result and discussion

3.1. Effects of microwave pretreatment on the chemical properties of corn straw

3.1.1. The difference in chemical constitution. The compact structure of lignocellulosic biomass is attributed to the



Table 1 The effect on the chemical compositions of corn straw before and after microwave pretreatment under different temperatures^a

Temperature	Composition (%)			Removal percentage		
	Cellulose	Hemicellulose	Lignin	Cellulose	Hemicellulose	Lignin
CK	29.57 ± 0.18	22.15 ± 0.99	13.73 ± 3.20	—	—	—
M120-10	37.71 ± 0.46C	28.33 ± 0.34Aa	10.79 ± 2.13Aa	3.48 ± 0.13	3.20 ± 0.04	40.53 ± 0.18
M150-10	38.07 ± 0.32C	26.79 ± 0.97Ab	7.69 ± 2.00Ab	6.20 ± 0.01	11.87 ± 0.05	59.19 ± 0.14
M180-10	41.03 ± 0.29B	16.59 ± 0.92B	6.84 ± 0.00Abc	11.23 ± 0.01	49.61 ± 0.04	66.48 ± 0.08
M210-10	45.44 ± 0.56A	11.72 ± 0.67C	4.68 ± 0.62Ac	15.27 ± 0.01	70.82 ± 0.01	81.20 ± 0.05

^a Different capital and small letters in the same line show a significant difference in $p < 0.01$ and $p < 0.05$, respectively.

cell wall polysaccharide link with lignin through the covalent bonds that form a lignin carbohydrate complex, in which both cellulose and hemicellulose are apt to decompose and conversely, lignin is difficult to degrade.³⁵ Consequently, it is

necessary to study the change of chemical composition before and after pretreatment.

Table 1 displays the change of the chemical components of lignocellulose before and after pretreatment at different

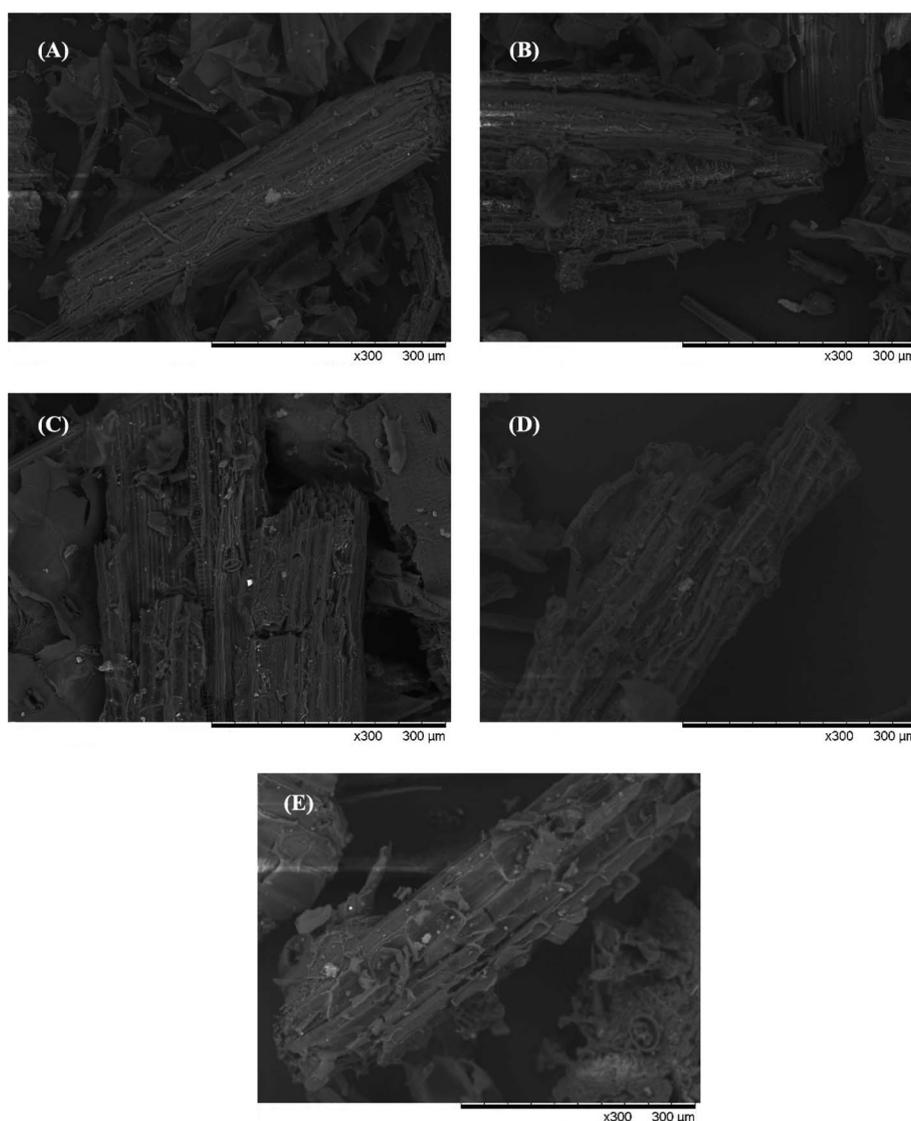


Fig. 2 Scanning electron microscope images of the microwave pretreated corn straw and the control. CK (A); 120 °C, 10 min (B); 150 °C, 10 min (C), 180 °C, 10 min (D), and 210 °C, 10 min (E).



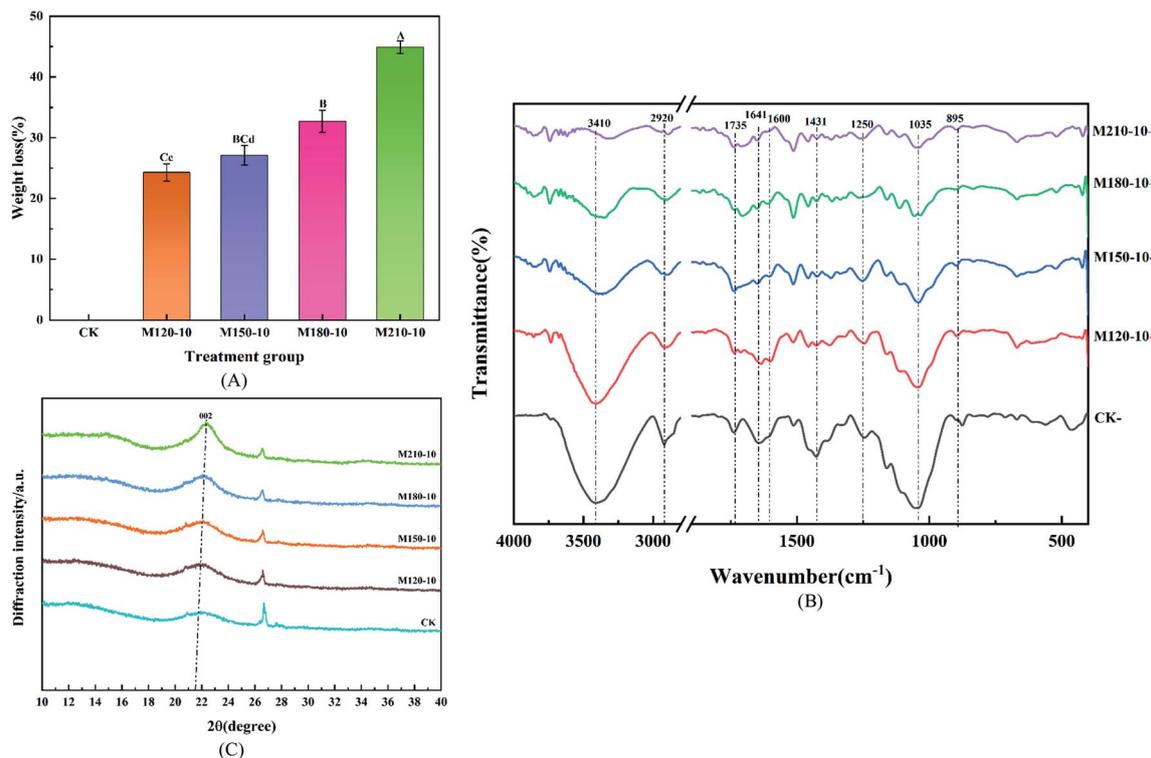


Fig. 3 The difference of weight loss (A), FTIR spectra (B), and XRD patterns (C) of corn straw before and after microwave pretreatment with various temperatures.

temperatures for CS. An ideal pretreatment method not only makes substrates biodegradable but also retains the maximum available carbohydrates for further production of biofuels.³⁶ It can be seen from Table 1 that the cellulose and hemicellulose contents based on dry matter increased, accompanied by a reduction in lignin content. This is due to the fact that lignin became adjoined to the carbohydrate structures (cellulose and hemicellulose) through certain chemical bonds such as α -ether bonds, phenyl glycosidic bonds, acetal bonds, and ester bonds.³⁷ The remaining cellulose and hemicellulose were released and hydrolyzed into small molecules, which are then available for hydrolytic enzymes to improve the quality of biogas during anaerobic digestion. In contrast to the lignin removal rate of 40.53–81.20%, the percentage of cellulose and

hemicellulose removed was 3.48–15.27% and 3.2–70.82% compared with CK, respectively. The maximum cellulose content of 45.44% was obtained in the M210-10 group, this comes at the expense of a lot of cellulose and hemicellulose. Conversely, the M120-10 group retained most of the cellulose and hemicellulose content, but the lignin removal percentage was very low. According to the analysis of the significant difference, all pretreatment groups expressed significant or extremely significant differences. There was an extremely significant difference between the M180-10 group and M210-10 group for components of hemicellulose and cellulose ($p < 0.01$).

All in all, this pretreatment method has satisfied the requirement to remove lignin and preserve cellulose and

Table 2 The peak assignments of the FT-IR spectrum of 850–3450 cm^{-1} of corn straw before and after microwave pretreatment under different temperatures

Number	Wavenumber (cm^{-1})	Functional group	Assignment
1	3410	–OH stretching vibration	—
2	2920	–CH and –CH ₂ up stretching vibration	Cellulose
3	1735	C=O asymmetric bending vibration of xylan	Hemicellulose and lignin
4	1641	C=C stretching vibration of the aromatic ring	Lignin
5	1600	C=C vibrating of the aromatic skeleton	Lignin
6	1431	–CH ₂ bending vibration	Lignin
7	1250	C–O–C stretching vibration	Lignin
8	1035	C–O stretching vibration	Cellulose and hemicellulose
9	895	–CH bending vibration in the plane	Cellulose



hemicellulose and can be proposed as a promising method for pretreatment in the anaerobic digestion process.

3.1.2. The difference in microstructure. A scanning electron microscope was employed to observe the surface morphology of the samples after microwave pretreatment under various temperatures concerning that of the control group. Fig. 2 exhibits the changes in surface morphology before and after pretreatment. The raw material shows a condensed and smooth bundle surface structure with many fiber layers that plays a defensive role in microbial degradation. A significant change was that the cell walls of untreated CS were somewhat destroyed and the initial smooth and rigid structure became loose and separated, which could be seen in the CS surface morphology after microwave pretreatment. Coarseness and defibrillation of the CS surface increased as the temperature increased. Especially, the micrographs in Fig. 2(E) were found to be more swollen and have more fiber fragments appearing on the surface. It is also worth mentioning that although the M120-10 treatment group showed some damage to the structure of CS, its internal tissue exposure was less and thus it was difficult for microorganisms to use it directly. Relatively, the rest of the treated group show an outstanding result. These performances also illustrated the partial lignin removal and the increase in cellulose and hemicellulose exposed to the surface, which is consistent with the results regarding the chemical composition changes of pretreated CS.

3.1.3. The difference in corn straw degradation. Fig. 3(A) exhibits the weight loss of the CS after microwave pretreatment under different temperatures, which implies that microwave pretreatment has a significant effect on the degradation of the lignocellulosic structure. The degradation rate ranged from 24.32 to 44.86% of the weight loss for CS with the temperature increasing from 120 to 210 °C. Obviously, the maximum weight loss of 44.86% could be found in the M210-10 group compared with other groups. Especially, weight loss leads to partial lignin removal for biomass during the pretreatment process from the standpoint of Wyman.³⁸ According to a one-way analysis of variance, all microwave treated CS showed extremely significant differences ($p < 0.01$) except for the sample M120-10 group and M150-10 group ($p < 0.05$). Meanwhile, there was no significant difference between the M150-10 group and the M180-10 group ($p > 0.05$). Hence, the results above suggested that the microwave pretreatment was substantially conducive to break the lignocellulosic structure and remove lignin from CS.

3.1.4. The difference in functional groups. FTIR can be employed to qualitatively analyze the change of chemical composition in lignocellulose structures after pretreatment.³⁹ For a more detailed characterization, the FTIR spectra for raw materials and pretreated samples are shown in Fig. 3(B), while the spectrum peak assignments are listed in Table 2 according to the literature.^{40–42} The intensity of the vibration located at 3410 cm^{-1} attributed to O–H stretching that exists in the raw samples became weaker as the pretreatment temperature increased, indicating that the intermolecular and extra molecular hydrogen bonds of the cellulose were broken down, which was conducive to the degradation of cellulose because the destruction of hydrogen bonding can change the cellulose

structure of CS and increase the accessibility of cellulose during anaerobic digestion. Similarly, the vibration detected at 2920 cm^{-1} represented the –CH and –CH₂ stretching vibration, indicating that partial carbon chains were destroyed resulting in a partial loss of cellulose after microwave pretreatment. Additionally, the carbonyl bands in the region 1735 cm^{-1} were attributed to the hydroxyl C=O stretching vibration, which belonged to the ester functional groups with the function of linking celluloses and hemicelluloses related to carboxylic compounds and ketones.⁴³ This feature was easy to observe in raw CS, but it gradually vanished in all the pretreated samples, which proved that the removal of a large portion of lignin was ascribed to the destruction of the carbonyl. The intensity of the vibrations at 1641 cm^{-1} and 1600 cm^{-1} is ascribed to C=C stretching of the aromatic ring and the C=C aromatic skeleton vibration from lignin. The intensity decreased at different levels among those samples after microwave pretreatment. Similarly, the intensity at 1431 cm^{-1} could be detected in treated samples, which also implied the effective removal of lignin. The intensity of the vibration at 1250 cm^{-1} , representing the C–O–C stretching vibration, appeared evidently in raw samples and correspondingly decreased as pretreatment temperature increased, which corroborated the removal of lignin. However, the intensity of the vibration at 1035 cm^{-1} is representative of the C–O stretching vibration in cellulose and hemicellulose. The intensity was slowly reduced, which implied that the contents of cellulose and hemicellulose were degraded by microwave pretreatment. There was no significant difference to observe in the intensity of the peak at 895 cm^{-1} which represents the C–H bending vibration in the plane of cellulose.

Besides, the lateral order index (LOI) based on the absorbance ratios at wavenumbers 1431 cm^{-1} and 900 cm^{-1} was used to semi-quantitatively analyze the changes in the physico-chemical character of lignocellulosic biomass after pretreatment. The LOI values of the 5 experimental groups were 4.78, 1.82, 1.70, 2.17, and 1.89, respectively, whereas they significantly decreased after microwave pretreatment, which indicated that the highly ordered cellulosic network was transformed into a more amorphous state.⁴⁴

3.1.5. The difference in cellulose crystallinity. For lignocellulosic biomass including the crystalline structure and non-crystalline structure, cellulose is considered to be crystalline, while hemicellulose and lignin are regarded as an amorphous substrate.^{31,45} The X-ray diffraction pattern was performed to measure the relative amount of cellulose crystallinity of

Table 3 The crystallinity index and crystallite size of untreated and microwave pretreated corn straw with various temperatures

Treatment	CrI (%)	2θ (°)	β (°)	D (nm)
CK	23.58	21.71	2.94	2.74
M120-10	30.17	21.83	2.14	3.76
M150-10	27.59	22.02	1.98	4.06
M180-10	36.01	21.83	2.47	3.27
M210-10	43.25	22.39	1.51	5.35



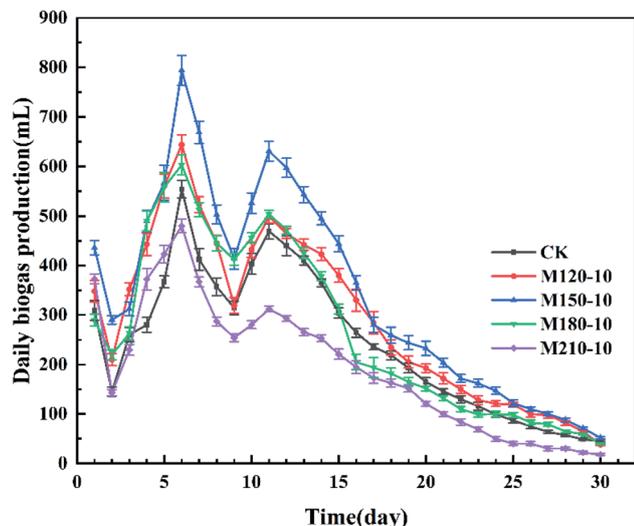


Fig. 4 Daily biogas production from untreated and microwave pretreated corn straw under diverse temperatures.

untreated and pretreated samples as displayed in Fig. 3(C). It can be seen from Fig. 3(C) that the X-ray diffraction peaks of the cellulose of pretreated samples were sharper than that in untreated CS and the diffraction intensity was improved after pretreatment. Besides, the primary peak of each sample was clearly shown at 22.2° for 2 theta, respectively. The major peak from the 002 planes represents the diffraction intensity in the crystal region.

Table 3 lists all the CrI results of all the samples. The CrI values of the pretreatment groups M120-10, M150-10, M180-10, and M210-10 were 30.17%, 27.59%, 36.01% and 43.25%, respectively, which implied a 17–83.42% increase compared with 23.58% of the untreated samples. The maximum CrI value of the M210-10 group was 43.25% which is 1.83 times as much

as the CK group. The increasing CrI values indicated an increase in cellulose content, which confirmed the similar development observed in the chemical composition of CS. The phenomenon whereby the crystallinity index of the raw materials was improved by pretreatment has also been reported previously in the literature.⁴⁶ This is because the reduction of lignin cladding exposes the complete crystal structure of the defective crystal region, which makes the crystal region clearer and thus increases the crystallinity index. Furthermore, the decrease of diffraction intensity in the amorphous region and the increase of diffraction intensity in the crystalline region may also be attributed to the recrystallization in the cellulose crystalline region.⁴⁷ Table 3 also shows the crystallite size and the position of the 002 planes in the CS after microwave pretreatment. As can be seen from Table 3, the position of the 002 plane microcrystal in cellulose remained unchanged, but the size (D) of the vertical 002 plane microcrystal increased, which indicated that microwave pretreatment did not change the original crystal shape of cellulose, but only affected the microcrystalline size. Therefore, the X-ray diffraction analysis also confirmed the partial removal of amorphous structures such as hemicellulose and lignin *via* microwave pretreatment.

3.2. Effect of microwave pretreatment on anaerobic digestibility

3.2.1. Daily biogas production. The amount of daily biogas produced by anaerobic digestion from untreated and pretreated CS is shown in Fig. 4. The daily biogas yield of all the pretreated groups was almost similar. The daily biogas production from anaerobic digestion of pretreated CS for treatment groups CK, M120-10, M150-10, M180-10, and M210-10 increased on the second day, which made a first biogas production peak of 554, 644, 794, 603, and 480 mL, respectively. After a certain degree of decline, it reached the secondary biogas production peaks of 469, 499, 631, 504, and 312 mL respectively. Finally, the daily

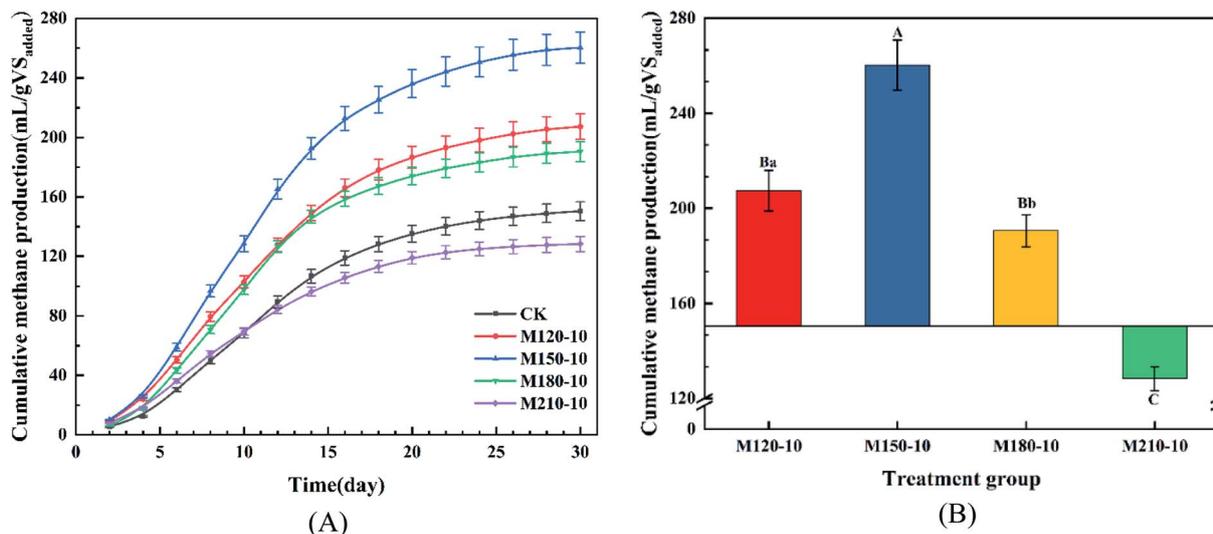


Fig. 5 The yield of cumulative methane production (A) and total methane production (B) from untreated and microwave pretreated corn straw with various temperatures.

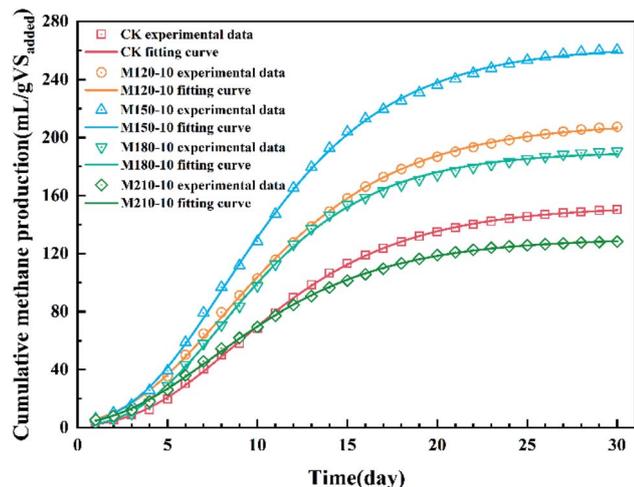


Fig. 6 Curve fitting of the Gompertz model to the methane production data of corn straw before and after microwave pretreatment under different temperatures.

biogas production continued to decline with small fluctuations until almost no biogas was produced from anaerobic digestion. For the maximum daily biogas production, the pretreatment group M150-10 was significantly higher than the other groups, while the pretreatment group M210-10 was the worst among all the groups. This was also attributed to the higher temperature of the microwave pretreatment, which destroyed the lignocellulosic structure, accompanying the consumption of partial fermentation substrates such as hemicellulose. It is inferred that microwave pretreatment can increase the daily biogas yield from these observations.

Finally, one-way ANOVA showed that there were extremely significant differences among all the experimental groups except for the significant differences among the CK, M180-10, and M120-10 groups for the maximum production of daily biogas.

3.2.2. Cumulative methane production. The change in the cumulative methane production from the anaerobic digestion of raw and pretreated CS is shown in Fig. 5(A). As can be seen from Fig. 5(A), each group showed the trend of a slow increase in the preliminary stage, a significant increase in the mid-stage, and a gradual decrease in the late-stage until it tended to be gentle for cumulative methane production during anaerobic fermentation. There was no obvious difference between the M120-10 group and the M180-10 group for the tendency of

cumulative methane yield, while the M150-10, M180-10 and M210-10 groups had a discrepancy after 4 days based on the CK group. Especially, the M150-10 group was observed with a notable gap compared with the CK group. Fig. 5(B) shows that the total methane production for CK, M120-10, M150-10, M180-10, and M210-10 groups are 150.36, 207.37, 260.25, 190.53, and 128.24 mL per gVS_{added}, respectively. The M150-10 group showed the highest maximum cumulative methane yield, followed by the M120-10 and M180-10 groups. The M150-10 group reached the maximum cumulative methane yield, which is 73.08% higher than the CK group. Additionally, the cumulative methane production of the M120-10 group increased by 37.92%, but the M210-10 group actually decreased on account of some removal of cellulose and hemicellulose as substrates for anaerobic digestion in the pretreatment process.

There was an extremely significant difference ($p < 0.01$) between the M150-10 group and other groups determined through the analysis of significant difference, while the M180-10 group and M120-10 group showed a significant difference ($p < 0.05$). It was concluded that microwave pretreatment could enhance the cumulative methane yield from the anaerobic digestion of CS. Additionally, the degree of improvement was closely related to the temperature of microwave pretreatment.

3.2.3. Kinetic analysis. The results which were applied to fit the cumulative methane production from the anaerobic digestion of five substrates with the Gompertz model are presented in Fig. 6. The evaluation of model parameters obtained by kinetic analysis is shown in Table 4. According to Table 4, all the coefficients of determination ($\text{adj-}R^2$) were above 0.99, which indicated that the selected model fitted the cumulative methane production well. The root mean square error (RMSE) was observed to be 0.786–1.75%, which is less than 25%, implying that the model error was within the acceptable range.⁴⁸ The predicted maximum methane production (P) values from the model corresponding to anaerobic digestion of five substrates were 152.78, 210.25, 262.78, 190.32, and 130.61 mL per gVS_{added}, respectively. The value of P also expressed a 24.57–71.99% increase compared with that in the CK group. However, a slight decrease appeared in the M210-10 group, which indicated that a higher temperature was not conducive to increasing methane production. The lag-phase time (λ) values defined the time required for anaerobic microorganisms to adapt to the fermentation system. The values of λ from 2.06 to 3.22 days showed a 3.30–38.14% shortening of the period in comparison to the 3.33 days in the CK group, which corresponds to previous literature.⁴⁹ The value of λ also confirmed the significant

Table 4 Kinetic parameters and goodness of fit to methane production from corn straw under different microwave pretreated temperatures obtained from the modified Gompertz model evaluation

Parameter	CK	M120-10	M150-10	M180-10	M210-10
P (mL per gVS _{added})	152.78	210.25	262.78	190.32	130.61
R (mL per gVS _{added} per d)	10.51	14.02	18.83	14.84	8.90
λ (day)	3.33	2.56	2.99	3.22	2.06
Adj- R^2	0.999	0.999	0.999	0.999	0.999
RMSE (%)	0.862	1.28	1.75	1.59	0.786



advance after microwave pretreatment of the methane production efficiency.

4. Conclusions

Microwave pretreatment in a certain temperature range was beneficial to the decomposition of the lignocellulose structure, improving coarseness and defibrillation in the surface morphology, reducing the mass fraction of lignin, and increasing cellulose and hemicellulose contents. Besides, the specific degradation of the chemical composition of corn straw was detected at marker bands in the performed FTIR studies. An augmentation of the cellulose crystallinity and crystallite size for corn straw was observed in the XRD studies. The above analysis showed that microwave pretreatment enhanced the degradation degree of corn straw, which was beneficial to boosting utilization during anaerobic digestion. By comparing it to the CK group, the best results based on the methanogenic tests were obtained in the M150-10 group for a methane production yield with a 73.08% improvement. The values of λ from the fitting parameters in the modified Gompertz equation were reduced, which also helped to prove that microwave pretreatment is an effective way of improving the efficiency of the anaerobic digestion of biomass.

Conflicts of interest

There are no conflicts to declare.

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References

- 1 S. A. Jambo, R. Abdulla, S. H. Mohd Azhar, H. Marbawi, J. A. Gansau and P. Ravindra, *Renewable Sustainable Energy Rev.*, 2016, **65**, 756–769.
- 2 B. Sen, Y.-P. Chou, S.-Y. Wu and C.-M. Liu, *Int. J. Hydrogen Energy*, 2016, **41**, 4421–4428.
- 3 D. S. Ganesh, *Afr. J. Biotechnol.*, 2012, **11**(5), 1002–1013.
- 4 W. M. Budzianowski, *Renewable Sustainable Energy Rev.*, 2016, **54**, 1148–1171.
- 5 X. Wang, S. Cheng, Z. Li, Y. Men and J. Wu, *Sustainability*, 2020, **12**, 5453.
- 6 K. Li, R. Liu and C. Sun, *Renewable Sustainable Energy Rev.*, 2016, **54**, 857–865.
- 7 Y. Wu, S. Wang, D. Liang and N. Li, *Bioresour. Technol.*, 2020, **298**, 122403.
- 8 R. Chandra, H. Takeuchi and T. Hasegawa, *Renewable Sustainable Energy Rev.*, 2012, **16**, 1462–1476.
- 9 M. Elsayed, E. F. Abomohra, P. Ai, K. Jin, Q. Fan and Y. Zhang, *Energy Convers. Manage.*, 2019, **195**, 447–456.
- 10 C. Sawatdeenarunat, K. C. Surendra, D. Takara, H. Oechsner and S. K. Khanal, *Bioresour. Technol.*, 2015, **178**, 178–186.
- 11 L. Zhao, G. L. Cao, A. J. Wang, H. Y. Ren, D. Dong, Z. N. Liu, X. Y. Guan, C. J. Xu and N. Q. Ren, *Bioresour. Technol.*, 2012, **114**, 365–369.
- 12 L. Dong, G. Cao, J. Wu, B. Liu, D. Xing, L. Zhao, C. Zhou, L. Feng and N. Ren, *Bioresour. Technol.*, 2019, **287**, 121399.
- 13 D. N. Barman, M. A. Haque, T. H. Kang, G. H. Kim, T. Y. Kim, K. K. Min and D. Y. Han, *Environ. Technol.*, 2014, **35**, 232–241.
- 14 S. Croce, Q. Wei, G. D'Imporzano, R. Dong and F. Adani, *Biotechnol. Adv.*, 2016, **34**, 1289–1304.
- 15 Q. Yu, R. Liu, K. Li and R. Ma, *Renewable Sustainable Energy Rev.*, 2019, **107**, 51–58.
- 16 A. Bichot, M. Lerosty, M. Radoiu, V. Mechin and D. Garcia-Bernet, *Energy Convers. Manage.*, 2020, **203**, 112220.
- 17 X. Kan, J. Zhang, Y. W. Tong and C. H. Wang, *Energy Convers. Manage.*, 2018, **158**, 315–326.
- 18 L. Peng, L. Appels and H. Su, *J. Environ. Manage.*, 2018, **213**, 271–278.
- 19 J. Kainthola, A. S. Kalamdhad and V. V. Goud, *Process Biochem.*, 2019, **84**, 81–90.
- 20 B. Sándor, L. Zsuzsanna, K. Szabolcs, S. G. György and H. Cecilia, *Hung. Agric. Eng.*, 2008, **21**, 27–29.
- 21 D. Jackowiak, D. Bassard, A. Pauss and T. Ribeiro, *Bioresour. Technol.*, 2011, **102**, 6750–6756.
- 22 K. Kupryaniuk, T. Oniszczyk, M. Combrzynski, W. Czekala and A. Matwijczuk, *Materials*, 2020, **13**, 3003.
- 23 F. Yilmaz, E. K. Unsar and N. A. Perendeci, *Waste Biomass Valorization*, 2019, **10**, 3071–3087.
- 24 Y. Deng, L. Qiu, Y. Yao and M. Qin, *RSC Adv.*, 2018, **8**, 22643–22651.
- 25 C. Sun, W. Cao, C. J. Banks, S. Heaven and R. Liu, *Bioresour. Technol.*, 2016, **218**, 1215–1223.
- 26 L. Dong, G. Cao, L. Zhao, B. Liu and N. Ren, *Bioresour. Technol.*, 2018, **267**, 71–76.
- 27 W. Cao, C. Sun, X. Li, J. Qiu and R. Liu, *RSC Adv.*, 2017, **7**, 5701–5707.
- 28 A. M. Mustafa, H. Li, A. A. Radwan, K. Sheng and X. Chen, *Bioresour. Technol.*, 2018, **259**, 54–60.
- 29 Y. Gu, Y. Zhang and X. Zhou, *Bioresour. Technol.*, 2015, **196**, 116–122.
- 30 T. Liu, X. Zhou, Z. Li, X. Wang and J. Sun, *Bioresour. Technol.*, 2019, **280**, 345–351.
- 31 S. Kim and M. T. Holtzapfel, *Bioresour. Technol.*, 2006, **97**, 583–591.
- 32 X. Liu, S. M. Zicari, G. Liu, Y. Li and R. Zhang, *Bioresour. Technol.*, 2015, **185**, 150–157.
- 33 A. Nowicka, M. Zielinski, M. Debowski, M. Dudek and P. Rusanowska, *Biomass Bioenergy*, 2019, **126**, 174–180.
- 34 H. Wang, Z. Li, X. Zhou, X. Wang and S. Zuo, *Water*, 2020, **12**, 2556.



- 35 M. Watanabe, H. Inomata, M. Osada, T. Sato, T. Adschiri and K. Arai, *Fuel*, 2003, **82**, 545–552.
- 36 H. Lou, Q. Hu, X. Qiu, X. Li and X. Lin, *BioEnergy Res.*, 2015, **9**, 335–343.
- 37 A. T. Hendriks and G. Zeeman, *Bioresour. Technol.*, 2009, **100**, 10–18.
- 38 K. Kaur and U. G. Phutela, *Renewable Energy*, 2016, **92**, 178–184.
- 39 D. N. Barman, M. A. Haque, M. M. Hossain, S. K. Paul and H. D. Yun, *Waste Biomass Valorization*, 2020, **11**, 1755–1764.
- 40 N. Poornejad, K. Karimi and T. Behzad, *J. Biomass Biofuel*, 2014, **1**, 8–15.
- 41 T. Raj, M. Kapoor, R. Gaur, J. Christopher, B. Lamba, D. K. Tuli and R. Kumar, *Energy Fuels*, 2015, **29**, 3111–3118.
- 42 M. Taherdanak and H. Zilouei, *Fuel*, 2014, **115**, 714–719.
- 43 J. A. Heredia-Guerrero, J. J. Benitez, E. Dominguez, I. S. Bayer, R. Cingolani, A. Athanassiou and A. Heredia, *Front. Plant Sci.*, 2014, **5**, 305.
- 44 S. Sarbishei, A. Goshadrou and M. S. Hatamipour, *Biomass Convers. Biorefin.*, 2020, In press.
- 45 T. Jeoh, C. I. Ishizawa, M. F. Davis, M. E. Himmel, W. S. Adney and D. K. Johnson, *Biotechnol. Bioeng.*, 2007, **98**, 112–122.
- 46 W. Zhang, N. Sathitsuksanoh, J. R. Barone and S. Renneckar, *Bioresour. Technol.*, 2016, **199**, 148–154.
- 47 S. Wang, G. Dai, B. Ru, Y. Zhao, X. Wang, G. Xiao and Z. Luo, *Energy*, 2017, **120**, 864–871.
- 48 B. Deepanraj, V. Sivasubramanian and S. Jayaraj, *Ecotoxicol. Environ. Saf.*, 2015, **121**, 100–104.
- 49 J. Kainthola, A. S. Kalamdhad, V. V. Goud and R. Goel, *Bioresour. Technol.*, 2019, **286**, 121368.

