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# Creating hydrophobic nanopockets in metal–organic frameworks to promote hydrodeoxygenation of lignin derivatives under ambient conditions†

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The construction of homogeneous-like reaction environments in the vicinity of heterogeneous active sites is an effective artificial method for replicating the catalytic activity of natural enzymes. In this work, we fabricated hydrophobic nanopockets in metal–organic frameworks (MOFs) and confined Pd nanoclusters in them to mimic the joint action of metal centers and proximal cofactors in enzyme catalysis. The hydrophobic microenvironment of the MOF pore was introduced by the functional group (–CH<sub>3</sub>) modification on the organic linkers, which provide noncovalent interactions for substrate enrichment and ultimately create homogeneous-like conditions for the catalyst to exert its intrinsic activity. The obtained Pd@UIO-66-CH<sub>3</sub> composite with enhanced hydrophobic interaction exhibited high catalytic performance for the hydrodeoxygenation of lignin-derived aromatic alcohols/aldehydes under ambient conditions. This work elucidates the importance of the microenvironment around the active site in catalysis and provides new ideas for designing artificial enzyme catalytic systems with substrate-specific recognition.

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## Introduction

Hydrodeoxygenation (HDO) reactions for the cleavage of C–O/C=O bonds in aromatic alcohols and aldehydes are of crucial importance in coal and petrochemical processing, biomass feedstock transformation and the pharmaceutical industry.<sup>1–5</sup> However, harsh catalytic conditions such as high H<sub>2</sub> pressure or temperature are often required when hydrogen is used as the reducing agent.<sup>6–10</sup> To achieve hydrodeoxygenation (HDO) under ambient conditions, and to avoid over-reduction of other unsaturated bonds or damage to special functional groups, precise catalyst design is required to obtain target products in high yields.

Palladium, with its high ability to activate H<sub>2</sub> and strong adsorption of C=O/C–O, is expected to enable HDO reactions under ambient conditions. Current studies of HDO catalysts mainly focus on the modulation of metal active sites, including their composition,<sup>11–15</sup> electronic structure,<sup>16</sup> and particle size.<sup>17</sup> Inspired by the ideal enzyme catalysis, which relies on necessary metal sites and suitable adjacent environments, where

noncovalent interactions between substrates and cofactors within the binding pocket play a crucial role in substrate enrichment, organization, and activation,<sup>18,19</sup> microenvironmental modulation around catalytic sites may be an effective way to regulate catalytic behavior. Considering the hydrophobic nature of aromatic compounds, the creation of hydrophobic microenvironments to alter the binding affinity of substrates within the pocket would increase the local concentration of reactants and accordingly the HDO activity.<sup>20–22</sup> However, the introduction of such noncovalent interactions in the vicinity of the active site is difficult to achieve in traditional porous supports due to the challenges in precisely tailoring their structure. In this context, it is of great importance to find a suitable support to construct an artificial hydrophobic nanopocket with heterogeneous active sites.

Different from the traditional porous materials, metal–organic frameworks (MOFs) have cavities or channels with tuneable geometry, which provide a confined environment akin to enzymes.<sup>23–30</sup> In addition, active metal sites can be dispersed in the pore, the functional groups for the noncovalent interaction can be furnished on the organic linkers in the pore walls, and the group type is also adjustable,<sup>31,32</sup> which fulfils all the conditions for building nanopockets.

In this work, we successfully constructed hydrophobic nanopockets with Pd nanoclusters confined. The noncovalent interaction was introduced by the functional group

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modification of the MOF pore wall, effectively recognizing hydrophobic aromatic substrates and accumulating them around the Pd clusters, thus mimicking a homogeneous environment for the catalyst to exert its intrinsic activity. The Pd@UIO-66-CH<sub>3</sub> with enhanced hydrophobic interaction exhibits much higher catalytic activity and reaction kinetics in the HDO of aromatic alcohols/aldehydes under ambient conditions than that of Pd@UIO-66-NH<sub>2</sub> with hydrophilic properties.

## Results and discussion

UIO-66 with three-dimensional cavities that consist of Zr<sub>6</sub>O<sub>8</sub> cluster nodes and terephthalate linkers was selected for the construction of substrate-binding nanopockets. Due to the polarity difference between functional groups,<sup>33</sup> the wettability of the MOF pore wall environment can be systematically regulated by switching the functional groups dangling on the linkers (Fig. 1A). To prevent the formation of Pd nanoparticles on the MOF external surface, a double-solvent method was employed, in which a small amount of aqueous palladium chloride solution was added to the highly hydrophobic *n*-hexane, and the capillary force effect allowed it to go inside the pore,<sup>34</sup> affording encapsulated Pd nanocluster composites Pd@UIO-66-X (X = -CH<sub>3</sub>, -H, -NH<sub>2</sub>). Powder X-ray diffraction (PXRD) patterns

suggest that the whole MOF scaffold structure is maintained well upon modification and metal loading (Fig. 1B and S1†). The absence of identifiable Pd diffraction peaks possibly indicates low Pd content and/or small Pd size. The successful introduction of the functional groups was confirmed by Fourier-transform infrared (FT-IR) spectroscopy (Fig. S2†). As shown in Fig. 1C, we observed absorption peaks related to the C-N (1340 cm<sup>-1</sup>, 1257 cm<sup>-1</sup>) and -CH<sub>3</sub> (1455 cm<sup>-1</sup>) in Pd@UIO-66-NH<sub>2</sub> and Pd@UIO-66-CH<sub>3</sub>, respectively.<sup>35,36</sup> The water contact angle of UIO-66-NH<sub>2</sub> is 32°, which increases to 41° for UIO-66 and 74° for UIO-66-CH<sub>3</sub> (Fig. 1D). Similarly, the contact angle still follows the above pattern after the introduction of Pd nanoclusters. In a mixed benzyl alcohol and water solvent, UIO-66-NH<sub>2</sub> and Pd@UIO-66-NH<sub>2</sub> are dispersed in the upper water phase, while UIO-66-CH<sub>3</sub> and Pd@UIO-66-CH<sub>3</sub> are selectively suspended in the lower benzyl alcohol phase, which clearly demonstrates that the -CH<sub>3</sub> modification enhances the hydrophobicity of the material. Alcohols and aldehydes tend to adsorb onto Pd@UIO-66-CH<sub>3</sub> rather than Pd@UIO-66-NH<sub>2</sub>. In the catalysis of natural enzymes, the active metal centers usually incorporate the proximal amino acids or cofactors. To replicate enzyme pockets vividly, the Pd cluster needs to be bound in the constructed hydrophobic microenvironment. The decrease in the Brunauer-Emmett-Teller (BET) surface area of Pd@UIO-66-X suggests that Pd was successfully introduced into the MOF



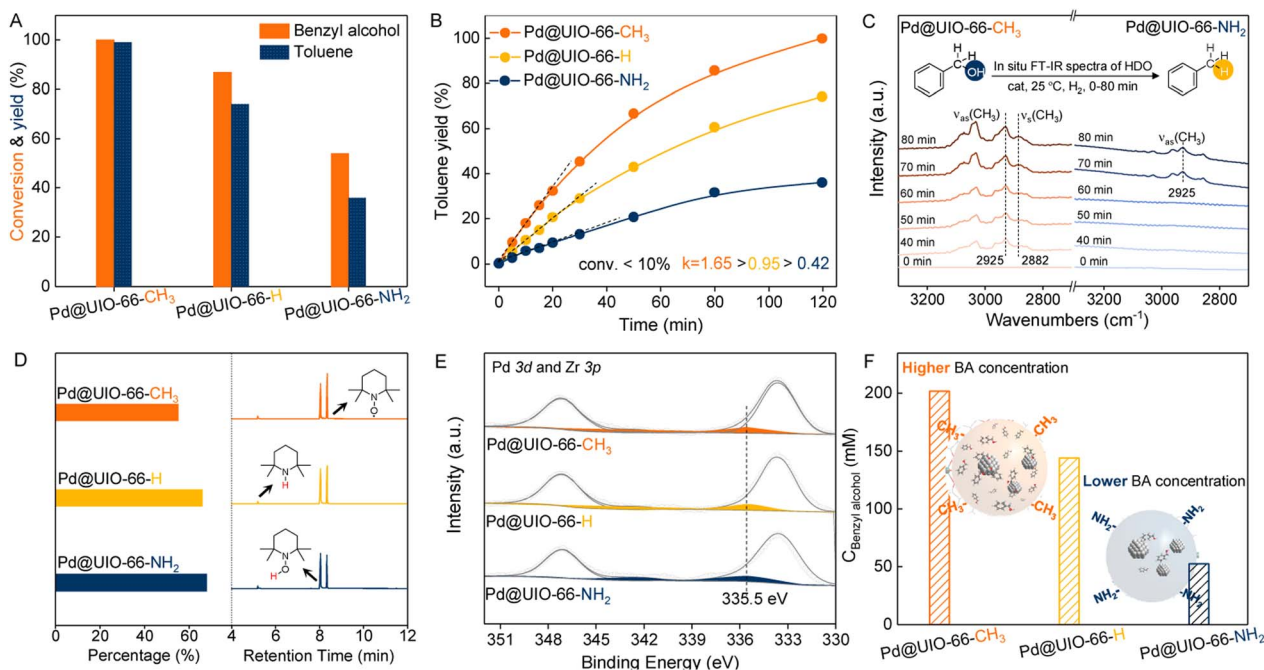
**Fig. 1** (A) Schematic illustration of the fabrication of hydrophobic nanopocket Pd@UIO-66-CH<sub>3</sub>. (B) The PXRD patterns for Pd@UIO-66-CH<sub>3</sub>, Pd@UIO-66-H, and Pd@UIO-66-NH<sub>2</sub>. (C) FT-IR spectra for Pd@UIO-66-CH<sub>3</sub>, Pd@UIO-66-H, and Pd@UIO-66-NH<sub>2</sub>. (D) The water contact angle and dispersion of (1) UIO-66-CH<sub>3</sub>, (2) Pd@UIO-66-CH<sub>3</sub>, (3) UIO-66-NH<sub>2</sub>, and (4) Pd@UIO-66-NH<sub>2</sub> in water (upper phase) and benzyl alcohol (lower phase) mixture. (E–G) N<sub>2</sub> adsorption–desorption isotherms for UIO-66-X and Pd@UIO-66-X. (H) TEM images of Pd@UIO-66-CH<sub>3</sub>, Pd@UIO-66-H, and Pd@UIO-66-NH<sub>2</sub>. (I) The elemental mapping profiles for Pd@UIO-66-CH<sub>3</sub>.



pores (Table S1†). Furthermore, the nitrogen adsorption isotherms of Pd@UIO-66-X display a Type I curve like that of the pristine MOF (Fig. 1E–G), suggesting the existence of micropores for the enrichment of substrates, which is a key element in the fabrication of artificial nanopockets. Transmission electron microscopy (TEM) revealed an octahedral morphology of Pd@UIO-66-X with a particle size of *ca.* 200 nm (Fig. 1H). Due to the small size of the Pd clusters ( $\sim 5$  Å), it is difficult to obtain an accurate lattice spacing. However, this is rather an evidence that the clusters are confined within the MOF cavities (cages with  $\sim 8$  and  $\sim 11$  Å diameter dimensions, Fig. S3–S4†). The energy dispersive X-ray spectrometer (EDX) elemental mapping clearly shows the presence of Pd, Zr, and O, indicating the presence of uniformly distributed Pd clusters within Pd@UIO-66-CH<sub>3</sub>. All the above results suggest that we successfully constructed hydrophobic nanopockets with confined Pd clusters, aiming to mimic enzyme catalysis for substrate enrichment *via* multiple weak interactions and thereby improving the catalytic performance of the ambient-condition HDO reaction.

Benzyl alcohol (BA) ambient-condition hydrodeoxygenation (normal temperature and pressure) is employed as the model reaction to evaluate the performance of the constructed artificial hydrophobic nanopockets. Prior to the reaction, thermogravimetric analysis (TGA) was carried out, and it was found that all three samples exhibited high thermal stability up to 350 °C (Fig. S5†), which is favorable for them to maintain stability

under catalytic conditions. The catalytic performance is shown in Fig. 2A; Pd@UIO-66-CH<sub>3</sub> was able to achieve complete conversion of benzyl alcohol, and the yield of toluene was above 99% (Fig. S6†). Moreover, the Pd@UIO-66-CH<sub>3</sub> maintained a high toluene yield and structural stability (Fig. S7 and S8†) for 10 consecutive cycles. However, compared to Pd@UIO-66-CH<sub>3</sub>, the toluene yields on Pd@UIO-66-H and Pd@UIO-66-NH<sub>2</sub> were only 74% and 35%, respectively, under the same reaction conditions and Pd content (the Pd contents of Pd@UIO-66-CH<sub>3</sub>, Pd@UIO-66-H and Pd@UIO-66-NH<sub>2</sub> in Table S2† were 1.81 wt%, 1.74 wt%, and 1.87 wt%, respectively). Although the recyclability of Pd@UIO-66-H and Pd@UIO-66-NH<sub>2</sub> reaches that of Pd@UIO-66-CH<sub>3</sub>, the activity is still lower than that of Pd@UIO-66-CH<sub>3</sub> (Fig. S9 and S10†). To understand the kinetics of catalysis, we drew a tangent to the reaction time curve (conv. < 10%) and calculated the corresponding reaction rate. As reflected in Fig. 2B, we can see that Pd@UIO-66-CH<sub>3</sub> has the highest initial reaction kinetic rate with a *k* of 1.65. Although the reaction rate of Pd@UIO-66-CH<sub>3</sub> slows down as the reaction proceeds, it is still higher than that of Pd@UIO-66-H and Pd@UIO-66-NH<sub>2</sub>. Furthermore, *in situ* FT-IR spectroscopy was performed to further confirm the high HDO reaction rate on the Pd@UIO-66-CH<sub>3</sub> surface (Fig. 2C). We used the same dose of benzyl alcohol and H<sub>2</sub>, vibrational peaks associated with toluene appeared for Pd@UIO-66-CH<sub>3</sub> after 40 min of reaction, but were not found for Pd@UIO-66-NH<sub>2</sub>. Continuing the



**Fig. 2** (A) The conversion of benzyl alcohol and yield of toluene over Pd@UIO-66-CH<sub>3</sub>, Pd@UIO-66-H, and Pd@UIO-66-NH<sub>2</sub> under ambient conditions. Reaction conditions: 5 mg of catalyst, 1 mL of substrate solution (10 mM), 1 atm of H<sub>2</sub>, 25 °C, 2 h. (B) The reaction time curve and the reaction rate for Pd@UIO-66-CH<sub>3</sub> (*k* = 1.65), Pd@UIO-66-H (*k* = 0.95) and Pd@UIO-66-NH<sub>2</sub> (*k* = 0.42). (C) *In situ* FT-IR spectra for the benzyl alcohol HDO progress over Pd@UIO-66-CH<sub>3</sub> and Pd@UIO-66-NH<sub>2</sub>. The inset shows the reaction conditions for the benzyl alcohol HDO. (D) The percentage of active H in the hydrogen radical capture experiment and the corresponding GC-MS spectra. Conditions: 5 mg of catalyst, 1 mL of acetonitrile, 30 mg of TEMPO, 1 atm of H<sub>2</sub>, 25 °C, 2 h. (E) The Pd 3d XPS spectra for Pd@UIO-66-CH<sub>3</sub>, Pd@UIO-66-H, and Pd@UIO-66-NH<sub>2</sub>. (F) The pre-concentration effect of Pd@UIO-66-CH<sub>3</sub>, Pd@UIO-66-H, and Pd@UIO-66-NH<sub>2</sub> on benzyl alcohol in 2 h. The inset is a schematic representation of the enrichment of benzyl alcohol by materials modified with different functional groups.



reaction for 80 min, the  $\nu_{\text{as}}(\text{CH}_3)$  band appeared for Pd@UIO-66-NH<sub>2</sub> and its intensity was much lower than that of Pd@UIO-66-CH<sub>3</sub>, while the  $\nu_{\text{s}}(\text{CH}_3)$  was still not obvious. This performance disparity may stem from the Pd cluster or the different microenvironments.

To clarify the key influencing factors, we first performed control and CO poisoning experiments, and the results show that the Pd cluster is responsive for H<sub>2</sub> activation (Fig. S11<sup>†</sup>). Then, we used 2,2,6,6-tetramethyl-piperidine 1-oxide (TEMPO) as the <sup>1</sup>H acceptor to investigate the amount of active H generated within three nanopockets (Fig. S12<sup>†</sup>). TEMPO can be reduced to 1-hydroxy-2,2,6,6-tetramethyl-piperidine (TEMPO-H) or 2,2,6,6-tetramethylpiperidine (TMA) so that the percentages of TEMPO-H and TMA in solution give the relative amount of active H.<sup>37</sup> As shown in Fig. 2D, the amount of <sup>1</sup>H was almost the same for all three samples at the same reaction time and TEMPO dose, suggesting that Pd clusters have a similar ability to cleave H<sub>2</sub>. The hydrodeoxygenation of alcohols involves the steps of direct C–O bond cleavage and reactive H generation, which are carried out on the active Pd site. Therefore, the electronic environment of the Pd cluster will also influence its ability to activate the C–O bond. To understand it, X-ray photoelectron spectroscopy (XPS) was performed on Pd@UIO-66-X (Fig. 2E and S13<sup>†</sup>). The Pd 3d<sub>5/2</sub> binding energy of ca. 335.5 eV verifies the metallic palladium. Due to the small size of the Pd cluster in our sample, the peak shifts to a higher binding energy compared to bulk Pd (335 eV),<sup>38</sup> but there is no significant difference in the electronic state of the Pd cluster between the three samples. Similarly, there was no change in the binding energy of Zr 3d<sub>5/2</sub> (Fig. S14<sup>†</sup>). *In situ* FT-IR analysis of CO adsorption on Pd@UIO-66-X was carried out to further confirm the electron state of the Pd cluster. As shown in Fig. S15,<sup>†</sup> the adsorption mode of CO is the same for all three samples, with a broad peak at 2118 cm<sup>-1</sup> attributed to the linear adsorbed CO on Pd clusters,<sup>39</sup> indicating that the Pd in these samples is of a similar structure and situation. The above result suggests that the three functional groups have the same effect on the electronic states of Pd clusters in our system, and therefore the differential activity of these materials for benzyl alcohol HDO may stem from the microenvironment of the MOF framework itself.

Given that the Pd catalytic active sites are located within the porous skeleton, and the reaction substrates must enter the skeleton to access these sites, the hydrophobic microenvironment of Pd@UIO-66-CH<sub>3</sub> may play an important role in substrate enrichment. To confirm it, we first examined the binding ability of the nanopockets to the substrate. As reflected in Fig. 2F (Fig. S16<sup>†</sup>), all of the Pd@UIO-66-X materials can extract benzyl alcohol and their enrichment is consistent with the previously mentioned trend in hydrophobic strength (Pd@UIO-66-CH<sub>3</sub> > Pd@UIO-66-H > Pd@UIO-66-NH<sub>2</sub>). Although some reports have suggested that differences in adsorption capacity can be triggered by changes in the electronic state of the metal,<sup>40–42</sup> the similarity of the electronic state of palladium in our material precludes this possibility. Then, we focused on the delicate host–guest interactions between the hydrophobic framework and the substrate. As shown in Fig. S17,<sup>†</sup> after reaching adsorption equilibrium, UIO-66-CH<sub>3</sub> exhibited a conspicuous pre-concentration ability for benzyl

alcohol, and the calculated concentrations of the reactants inside UIO-66-CH<sub>3</sub> were higher than those in UIO-66-H and UIO-66-NH<sub>2</sub>. The time-dependent adsorption data were collected on UIO-66-X to gain insight into the adsorption kinetics and efficiency, and this process was monitored by gas chromatography (Fig. 3A–C). It takes only 10 min to reach adsorption–desorption equilibrium in the extremely diluted solution (10, 20, 30 mM). Among them, UIO-66-CH<sub>3</sub> showed close to 10% benzyl alcohol capture ratios (ratio of saturated adsorption to initial substrate amount) at all three concentrations, which is 2 and 5 times higher than those of UIO-66-H and UIO-66-NH<sub>2</sub>, respectively. Generally, the adsorption capacity is closely related to the porosity of the material.<sup>43</sup> Therefore, theoretically, UIO-66-H, with the highest surface area and pore size (the lowest steric hindrance of –H), should have the highest adsorption capacity and the fastest adsorption kinetics. However, there is a nonlinear relationship between the saturated adsorption capacity of UIO-66-X with the surface area and the functional group's steric hindrance. This result suggests that there are additional interactions between benzyl alcohol and the framework that influence the enrichment capacity of the material.

Hence, the saturation uptake per surface area (SUPS) was used to assess the noncovalent interaction of three nanopockets, and it was found that UIO-66-CH<sub>3</sub> exhibited the highest SUPS (Fig. 3D). To further understand this noncovalent interaction, cyclohexane adsorption isotherms were obtained for UIO-66-X (Fig. 3E). All isotherms showed characteristic Type I profiles. The cyclohexane uptake of UIO-66-CH<sub>3</sub> exhibited obvious superiority to those of UIO-66-H and UIO-66-NH<sub>2</sub>, suggesting that –CH<sub>3</sub> sites display, not unexpectedly, good affinity for cyclohexane. Especially noteworthy in UIO-66-CH<sub>3</sub> is the sharp increase in the uptake of cyclohexane at low pressure, demonstrating the importance of the enhanced noncovalent interactions in UIO-66-CH<sub>3</sub> for capturing trace cyclohexane. This point will directly affect the kinetic rate of the reaction in the later stage (the substrate concentration decreases as the reaction progresses), as verified by the fact that the rate of UIO-66-CH<sub>3</sub> is consistently higher than that of UIO-66-NH<sub>2</sub> throughout the course of the reaction. In addition, the strength of the interactions with benzyl alcohol was further investigated by *in situ* FT-IR spectroscopy. After introducing the same dose of benzyl alcohol on UIO-66-CH<sub>3</sub> and UIO-66-NH<sub>2</sub>, peaks at 1491, 1495, and 1377 cm<sup>-1</sup> attributed to C–C and O–H stretching were observed, respectively (Fig. 3F–G and S18<sup>†</sup>).<sup>44</sup> Then, the materials were evacuated to desorb benzyl alcohol for the same time. Results showed that these peaks almost disappeared on UIO-66-NH<sub>2</sub> after 8 min. Contrastingly, these peaks were still maintained on UIO-66-CH<sub>3</sub> even after 12 min, which suggests that the noncovalent interaction provided by –CH<sub>3</sub> is the driving force for benzyl alcohol adsorption. Armed with the above analysis, we conclude that noncovalent interactions provided by the hydrophobic microenvironment can enhance the macroscopic enrichment capacity of the nanopockets for substrates, thus increasing the local concentration of reactants and mimicking enzyme catalysis to exert its intrinsic activity for





Fig. 3 (A–C) Kinetic adsorption curves for UIO-66-CH<sub>3</sub>, UIO-66-H, and UIO-66-NH<sub>2</sub> in a wide concentration range of benzyl alcohol solution (10 mM, 20 mM, 30 mM). (D) Comparison of the SUPS between UIO-66-CH<sub>3</sub>, UIO-66-H, and UIO-66-NH<sub>2</sub>. (E) Cyclohexane adsorption isotherms on UIO-66-CH<sub>3</sub>, UIO-66-H, and UIO-66-NH<sub>2</sub> at 298.15 K. (F and G) *In situ* FT-IR spectra for benzyl alcohol adsorption and desorption on UIO-66-CH<sub>3</sub> and UIO-66-NH<sub>2</sub>, respectively.



Fig. 4 The catalytic activities of Pd@UIO-66-CH<sub>3</sub> in the hydrodeoxygenation of a broad range of aromatic alcohol/aldehyde substrates. Yield in percent is given next to each compound. Condition: 5 mg of catalyst (Pd 1.81 wt%), 0.01 mmol of substrate, 1 atm of H<sub>2</sub>, 25 °C, 24 h. The solvents are ethanol, except for 2 and 4, which are methanol.



a broad range of lignin-derived aromatic alcohol/aldehyde HDO with product yield of 69–99% (Fig. 4, S19 and S20†).

## Conclusions

In summary, we fabricated an artificial enzyme-mimicking nanopocket by integrating active metal centers and hydrophobic microenvironments in MOFs, which exhibits highly efficient ambient-condition hydrodeoxygenation capacity for various aromatic alcohols/aldehydes. Differing from the consensus on the electron effect on the altered activity of metal centers, this enhanced activity mainly stems from the strong enrichment of the substrate by the noncovalent interactions of the functional group on the MOF pore wall. Viewed in perspective, the judicious creation of a noncovalent interaction microenvironment around metal active sites in confined spaces will significantly improve the capacity of artificial mimetic enzymes for specific substrate recognition and accumulation.

## Data availability

The data that support the findings of this study are available in the ESI† of this article.

## Author contributions

Y. L. conducted most of the experiments of the project and data analysis and wrote the manuscript. H. Z. directed the research and analyzed the data. Z. Y., X. L. and Z. C. directed the *in situ* FT-IR characterization. M. W. and M. J. designed the project, supervised the research, and revised the manuscript.

## Conflicts of interest

The authors declare no conflict of interest.

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