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# A high-energy hybrid lithium-ion capacitor enabled by a mixed capacitive-battery storage $\text{LiFePO}_4$ – AC cathode and a $\text{SnP}_2\text{O}_7$ – rGO anode†

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In this work we present the development and optimization of a graphene-embedded Sn-based material and an activated carbon/lithium iron phosphate composite for a high-performing hybrid lithium-ion capacitor (LIC). For the negative electrode, we have synthesized and screened different tin and phosphorus-based graphene materials based on the chemical structure, morphology and particle size, selecting a composite consisting of nano-sized crystalline tin pyrophosphate ( $\text{SnP}_2\text{O}_7$ ) particles embedded in a graphenic matrix. For the positive electrode, a composite combining a high-loading (40 wt%) faradaic material lithium iron phosphate (LFP) with a graphene-activated carbon was developed whereas other bi-material cathodes are limited to about 20 wt% of faradaic material. The homogeneous distribution of nanosized carbon-coated LFP particles along the graphene-activated carbon has enabled energy storage *via* faradaic, pseudocapacitive, and capacitive mechanisms. The optimized-electrode LIC delivers high energy densities and overcomes the main power limitations of LICs using high-content battery-type materials (143 Wh  $\text{kg}^{-1}$  at 128 W  $\text{kg}^{-1}$  and 45 Wh  $\text{kg}^{-1}$  at 25 000 W  $\text{kg}^{-1}$ ).

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## 1. Introduction

In recent years, lithium-ion capacitors (LICs) have emerged as promising energy storage systems filling the gap between lithium-ion batteries and supercapacitors in terms of specific energy (10–100 Wh  $\text{kg}^{-1}$ ), power density (300–5000 W  $\text{kg}^{-1}$ ) and cyclability ( $10^3$ – $10^5$  cycles).<sup>1–5</sup> The excellent features of LICs are the result of the combination of a battery-type electrode along with a capacitive electrode in the same device. Within this configuration, a typical battery-type negative electrode stores energy *via* faradaic reactions, which enables the higher energy density of a LIC due to the higher charge storage capacity and the low redox potential, increasing the full LIC cell potential over that of non-faradaic supercapacitors. On the opposite side, a capacitor-type positive electrode stores energy electrostatically by the accumulation of charges at the electrode/electrolyte interface, which favors a fast response and long cycle life. However, due to the different charge storage mechanisms of each electrode, the multiparameter electrochemical

performance of a full LIC is usually limited by the imbalance between high capacity and fast kinetics.<sup>6,7</sup>

The optimization of negative electrodes would involve the use of active materials that exhibit high capacities at high rates. In this regard, tin-based compounds have attracted much attention in recent years.<sup>8</sup> Metallic tin (Sn) has advantages of high lithium storage capacity (994 mAh  $\text{g}^{-1}$ ), low price, and earth abundance. Nevertheless, due to the huge volume changes upon lithiation, tin particles can be pulverized and aggregated, which leads to structural fracture and a loss of electrical contact.<sup>9</sup> Consequently, the practical use of Sn poses serious challenges. To overcome them, strategies such as reduction in tin particle size<sup>10</sup> or Sn encapsulation in a conductive matrix buffering the volume changes have been applied.<sup>11–13</sup> Also, the use of tin oxides,<sup>14</sup> tin-based alloys,<sup>15</sup> tin phosphides,<sup>16</sup> or tin phosphates<sup>17</sup> has shown promising results. Especially, crystalline tin pyrophosphate ( $\text{SnP}_2\text{O}_7$ ) with a reversible specific capacity of >360 mAh  $\text{g}^{-1}$ , good capacity retention, and cycle stability has been widely studied.<sup>18–20</sup> Several studies pointed out that the excellent electrochemical performance is a consequence of the irreversible reduction of  $\text{SnP}_2\text{O}_7$  to metallic Sn and its further encapsulation into an inactive  $\text{Li}_4\text{P}_2\text{O}_7$  matrix that can buffer volume changes and promote fast electron transfer.<sup>21–23</sup> This material fulfills the requirements for a negative electrode in LICs.

On the opposite side, the optimization of a positive electrode is needed to increase its specific capacity while preserving a fast response. Activated carbons (ACs) are usually the common

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choice due to their large surface areas and tailored pore size distribution that allow them to accumulate more charge and work fast by physical storage. Nevertheless, the physical storage capacity is still much lower than that of redox-active battery-type materials. To raise the capacity of positive electrodes, the use of composites combining capacitive and faradaic (LTO, LVNP, and LFP) materials in a single electrode has been proposed.<sup>8,24,25</sup> Lithium iron phosphate (LFP) has been considered an attractive cathode material for lithium-ion batteries<sup>26</sup> and, more recently, also for lithium-ion capacitors<sup>27</sup> thanks to its low cost, low toxicity, high thermal stability, low volume change during lithiation/de-lithiation, the high specific capacity of 170 mAh g<sup>-1</sup>, a well-defined plateau at a high voltage (~3.5 V vs. Li/Li<sup>+</sup>), and reduced reactivity toward electrolytes. Nevertheless, its poor electronic conductivity ( $3.7 \times 10^{-9}$  S cm<sup>-1</sup>) and low Li-ion diffusion coefficient ( $1.8 \times 10^{-18}$  m<sup>2</sup> s<sup>-1</sup>) can limit the performance of LICs at high rates. Consequently, the extent to which LFP can be used in the positive electrode is not a trivial issue since the fast response and thus the power performance at high rates can be compromised, not to mention cycle stability.<sup>28</sup> The reduction in LFP particle size along with carbon coating are well-known strategies to overcome these limitations.<sup>29–31</sup> Also, smaller particle size, structural defects, and uniform distribution within the carbon matrix can induce extra pseudo-capacitive effects and improve diffusion, thus boosting the usable capacity even at high rates.<sup>32</sup>

In this study, we have developed and optimized different materials for both negative and positive electrodes for a highly performing hybrid lithium-ion capacitor. For the negative electrode, we have synthesized three different tin and phosphorus-based graphene electrodes. Using the same precursor and treating them thermally at 800, 900, and 1000 °C we obtained: (i) nano-sized crystalline tin pyrophosphate (SnP<sub>2</sub>O<sub>7</sub>) particles embedded in a graphenic matrix, (ii) an amorphous composite combining tin pyrophosphate (SnP<sub>2</sub>O<sub>7</sub>) within tin (Sn) all along graphene sheets, and (iii) micrometer-sized crystalline tin particles (Sn) embedded in a phosphorus-based graphenic matrix. The impact of different chemistries, structures, morphologies, and particle size on electrochemical performance was studied. Given the results, tin pyrophosphate (SnP<sub>2</sub>O<sub>7</sub>)-based material was chosen for the negative electrode of the final LIC thanks to its highest capacity even at high rates (420 mAh g<sup>-1</sup> at 0.5 A g<sup>-1</sup> and 110 mAh g<sup>-1</sup> at 5 A g<sup>-1</sup>). For the positive electrode, a composite comprising a high loading (40% wt) of lithium iron phosphate (LFP) and 60% of our previously reported graphene-activated carbon ResFaGO-A (RG) was developed. The nanosizing of our LFP particles, further carbon coating, and the homogeneous distribution of the carbon-coated LFP throughout the final composite enabled energy storage *via* faradaic, pseudocapacitive, and capacitive processes. As a result, this composite material demonstrated an outstanding capacity even at high rates (102 mAh g<sup>-1</sup> at 0.25 A g<sup>-1</sup> and 80 mAh g<sup>-1</sup> at 30 A g<sup>-1</sup>). Finally, the full optimization of the assembled LICs using mass balance 1:1 enabled high energy densities without compromising the power performance (143 Wh kg<sup>-1</sup> at 128 W kg<sup>-1</sup> and 45 Wh kg<sup>-1</sup> at 25 000 W kg<sup>-1</sup>).

## 2. Experimental

### 2.1. Synthesis of rGO800-P-Sn and LFP/RG

The LiFePO<sub>4</sub> (LFP)/RG composite was used as the positive electrode material. The two components of the composite were obtained as follows.

The activated carbon, RG, was prepared following our previously reported method.<sup>33</sup> Briefly, 440 mg of resorcinol (Sigma-Aldrich, 99%) were dissolved in 4.0 ml of water, 2.4 ml of ethanol, and 4.0 ml of graphene oxide (Graphenea, 4 mg ml<sup>-1</sup>). After complete dissolution of resorcinol, 600 μl of formaldehyde (Sigma-Aldrich, 37% w/w in H<sub>2</sub>O containing 10–15% methanol) and 100 μl of concentrated phosphoric acid (Sigma-Aldrich, ≥85% w/w in H<sub>2</sub>O) were added to the suspension. Then, the mixture was transferred into a closed container and thermally treated in an oven at 85 °C for 70 h. The resulting resins were pre-carbonized at 800 °C in a tubular oven for 1 h under a dynamic Ar atmosphere. The obtained carbon was grounded together with KOH (Sigma-Aldrich, ≥85%) using a C : KOH mass ratio of 1 : 6 and further carbonized in a tubular oven at 800 °C for 1 h under a dynamic Ar atmosphere. The resulting material was washed off once with diluted HCl, and then several times with hot deionized water to end up with the RG.

The LiFePO<sub>4</sub> (LFP) sub-micrometric size particles were synthesized by hydrothermal synthesis as follows: 7.5 ml of 1 M H<sub>3</sub>PO<sub>4</sub> solution (Sigma-Aldrich, ≥85% w/w in H<sub>2</sub>O) and 30 ml of ethylene glycol (EG) (FischerScientific, ≥99%) were homogenized using a magnetic stirrer to obtain the precursor solution. Then, 22.5 ml of 1 M LiOH aqueous solution was slowly introduced while stirring. Next, 15 ml of 0.5 M FeSO<sub>4</sub> aqueous solution was dropwise added. Finally, the solution was transferred into an autoclave and then thermally treated at 180 °C for 9 h. The resulting mixture was filtered and washed 3 times with hot deionized water. The LFP particles were carbon coated to increase their electrochemical performance. For this purpose, a mixture of the synthesized LFP powder with a 10% w/w of Super P C-65 conductive carbon was ball milled in a planetary ball mill (Pulverisette 5) with a 20 : 1 w/w ball to sample mass ratio for 3 hours at 250 rpm, resulting in LFP/C nanoparticles.

The negative electrode materials were obtained using a facile synthesis as follows: 100 mg of SnSO<sub>4</sub> (Sigma-Aldrich, ≥95%) were added to 50 ml of 4% w/w GO aqueous solution (Graphenea, 4 mg ml<sup>-1</sup>) that was gently stirred for 1 h. Then, 250 μl of H<sub>3</sub>PO<sub>4</sub> (Sigma-Aldrich, ≥85% w/w in H<sub>2</sub>O) were added to the solution and, after homogenization, the solution was transferred to a closed container and thermally treated at 80 °C for 18 h. The mixture was then freeze dried for 72 h. The resulting dry powder was subsequently treated in a tubular oven at 800 °C, 900 °C, or 1000 °C for 1 h under dynamic argon flow to obtain the final materials denoted as GOPR800\_Sn, GOPR900\_Sn, and GOPR1000\_Sn, respectively.

### 2.2. Physicochemical characterization

The morphology and chemical composition of the samples were characterized by scanning electron microscopy (SEM) and energy dispersive spectroscopy (EDS), respectively, using



a Quanta200 FEI (3 kV, 30 kV) microscope. The microstructure of the samples was analyzed by X-ray diffraction (XRD) using a Bruker D8 X-ray diffractometer. The data were collected using CuK $\alpha$  radiation over  $2\theta$  within the range from  $10^\circ$  to  $80^\circ$  for the GOPRX\_Sn and from  $15^\circ$  to  $65^\circ$  for the LFP samples, at steps of  $0.02^\circ$  and a residence time of 2 s in both cases. Nitrogen adsorption–desorption isotherms were registered at  $-196^\circ\text{C}$  using an ASAP 2460 instrument from Micromeritics. The samples were outgassed at  $150^\circ\text{C}$  for 12 h under a vacuum prior to the analysis. Specific surface area ( $S_{\text{BET}}$ ) values were calculated using the Brunauer–Emmett–Teller (BET) equation using the Rouquerol procedure for the monolayer capacity.<sup>34</sup> Pore size distributions were calculated with the 2D-NLDFT model applied to the data of the adsorption branches using the SAIEUS software.<sup>35</sup> Thermogravimetric analysis was performed using a TG 209 F1 Libra between 30 and  $1000^\circ\text{C}$  using a heating ramp of  $10^\circ\text{C min}^{-1}$ .

### 2.3. Electrochemical characterization

The negative electrode was processed by mixing the active materials (GOPR800\_Sn, GOPR900\_Sn, or GOPR1000\_Sn) with a Super P C-65 conductive carbon and a polyvinylidene fluoride (PVDF) binder in a 90:5:5 mass ratio using *N*-methyl-2-pyrrolidone (NMP) as the solvent. The positive electrode was processed by mixing the active materials, RG and LFP/C, with a Super P C-65 conductive carbon and a PVDF binder using a mass ratio of 54:36:5:5. The 60% w/w of the active materials corresponds to RG and the 40% w/w to the LFP/C, with the composite referred to as RG-LFP40. NMP was used as the solvent. The NMP-based inks of the negative and positive electrodes were coated on copper and aluminum foil, respectively. Laminates were dried overnight at  $80^\circ\text{C}$  under a vacuum. Electrode discs of 12 mm were furtherly punched out of the laminates and dried at  $120^\circ\text{C}$  overnight under a vacuum prior to cell assembly. For the sake of comparison, the RG and LFP/C electrodes were processed following the same procedure with a mass ratio of 90:5:5 and 80:10:10, respectively.

In the case of RG-LFP electrodes, the mass balance is  $1.6 \pm 0.2 \text{ mg}_{\text{AM}} \text{ cm}^{-2}$  while in the case of GOPR800-P-Sn, GOPR900-P-Sn, GOPR1000-P-Sn the mass loading is  $1.7 \pm 0.2 \text{ mg}_{\text{AM}} \text{ cm}^{-2}$ . Exceptionally,  $3.3 \pm 0.3 \text{ mg}_{\text{AM}} \text{ cm}^{-2}$  GOPR800-P-Sn electrodes were used for the 1:2 mass balance LIC.

The electrochemical measurements were conducted using a multichannel VMP3 generator (Biologic). Whatman D-type glass fibers discs of 13 mm in diameter and 1 M lithium hexafluorophosphate ( $\text{LiPF}_6$ ) in 1:1 v/v of ethylene carbonate (EC) and dimethyl carbonate (DMC) were used as a separator and an electrolyte, respectively, in all the measurements.

The electrochemical performance of the negative electrodes was first evaluated in two-electrode Swagelok-type cells using a half-cell configuration with a metallic lithium disc serving simultaneously as the counter and reference electrodes. Galvanostatic charge/discharge measurements were carried out at different current densities between 0.002 and 2.0 V vs.  $\text{Li/Li}^+$ .

Similarly, the electrochemical performance of the positive electrodes was evaluated using a half-cell configuration in

a three-electrode Swagelok-type cell using a metallic lithium disc as the reference electrode and an oversized Norit Activated Carbon (Kuraray) disc as the counter electrode. Galvanostatic charge/discharge measurements were carried out at different current densities with potentials between 2 and 4.2 V vs.  $\text{Li/Li}^+$ .

Before the assembly of LIC cells, the negative electrodes were pre-lithiated in a two-electrode Swagelok-type cell with a lithium metal disc simultaneously used as the counter and reference electrode. The pre-lithiation procedure consists of 5 charge/discharge cycles at C/10 between 0.002 and 2.0 V vs.  $\text{Li/Li}^+$  followed by a final discharge at C/40 to 0.2 V vs.  $\text{Li/Li}^+$ . After the pre-lithiation step, LICs were assembled within a three-electrode Swagelok-type cell using a pre-lithiated negative electrode, an LFP-containing positive electrode, and a lithium metal disc connected to the potentiostat as the counter, working, and reference electrodes, respectively. The negative electrode potential was set to 0.2 V vs.  $\text{Li/Li}^+$ , and the positive electrode potential to 4.2 V vs.  $\text{Li/Li}^+$  to maximize the cell potential and simultaneously prevent lithium plating and electrolyte decomposition. Galvanostatic charge/discharge measurements were performed within the 1.5–4.2 V vs.  $\text{Li/Li}^+$  voltage range at different current densities.

## 3. Results and discussion

### 3.1. Characterization of the negative electrode

As explained before in the experimental section, three different materials were synthesized as negative electrodes by an easy procedure consisting of mixing  $\text{SnSO}_4$  with a graphene oxide aqueous dispersion (GO) and  $\text{H}_3\text{PO}_4$ , heating, freeze drying, and subsequent pyrolysis at three different temperatures of  $800^\circ\text{C}$ ,  $900^\circ\text{C}$ , or  $1000^\circ\text{C}$ .

XRD patterns in Fig. 1 clearly show a huge impact of the temperature on the final structure of the materials. The material synthesized at  $800^\circ\text{C}$  (GOPR800\_Sn) exhibits very sharp peaks characteristic of tin pyrophosphate  $\text{SnP}_2\text{O}_7$  with a crystalline cubic structure, as previously reported.<sup>17,36</sup> Further increase in temperature to  $900^\circ\text{C}$  (GOPR900\_Sn) leads to crystallinity loss and amorphization. A high intensity and broad peak ascribed to the basal diffractions of graphene layers is registered in the  $15\text{--}35^\circ$  range.<sup>33</sup> This structure can be ascribed to the first stage



Fig. 1 XRD patterns of the as-synthesized materials.



where  $\text{SnP}_2\text{O}_7$  is partially reduced to metallic Sn along the randomly oriented graphene sheets. Finally, the temperature increase up to 1000 °C (GOPR1000\_Sn) leads to a successful reduction of tin pyrophosphate and the formation of crystalline metallic Sn particles deposited over the P-graphene sheets.<sup>37,38</sup> The TGA curve obtained for the precursor under the Ar atmosphere and using the same heating rate as that for the synthesis of the materials (Fig. S1†) is clearly in agreement with previous results. The first two steps of mass loss (20%) under 250 °C can be ascribed to the release of water molecules, weakly and strongly bonded, respectively. From 250 °C to 500 °C, the weight loss can be ascribed to the evolution of remaining oxygen and phosphorus-functional groups in graphene oxide. The crystallization of  $\text{SnP}_2\text{O}_7$  starts at 520 °C and goes through 880 °C. Further increase in the temperature promotes the carbothermal reduction of phosphorous-tin composites leading to the formation of metallic Sn while releasing phosphorous-containing gases.<sup>20,39</sup>

SEM images registered for the different thermal treated samples show the morphological differences between the three materials expected from the XRD results. Fig. 2a shows that GOPR1000\_Sn is composed of large Sn particles (7–14 μm) homogeneously embedded in the P-graphene matrix. Conversely, GOPR900\_Sn (Fig. 2b) shows a highly open 3D macroporous network made up of an amorphous phase of Sn and  $\text{SnP}_2\text{O}_7$  along the graphene sheets, confirming the beginning of the reduction of tin pyrophosphate to metallic tin. Finally, Fig. 2c and d illustrate that GOPR800\_Sn is shaped by small-sized crystalline particles of  $\text{SnP}_2\text{O}_7$  (~100 nm) homogeneously embedded in the graphenic matrix. This is expected to

enhance electrochemical properties since smaller particles make  $\text{Li}^+$  diffusion paths shorter, thus favoring faster kinetics. EDX results reported in Table 1 show that materials are mainly composed of carbon, tin, phosphorus, and oxygen in decreasing amounts. Also, as the temperature increases, the oxygen and phosphorus content decreases while that of tin increases, in good agreement with the further reduction of  $\text{SnP}_2\text{O}_7$  to metallic Sn.

The three materials were electrochemically tested using the half-cell configuration in the 0.002–2.0 V vs.  $\text{Li}/\text{Li}^+$  potential range to evaluate the impact of the chemical structure and morphology on the performance as negative electrodes for lithium storage. To this end, galvanostatic charge–discharge experiments at different current densities were performed. Fig. 3a–c and S2a† show the first four cycles registered at 0.05  $\text{A g}^{-1}$ . Clear differences can be distinguished among the three samples, especially in the first discharge where all irreversible processes occur. During the first discharge of GOPR800\_Sn (Fig. 3a), two main processes take place: (1) irreversible reduction of  $\text{Sn(IV)}$  to metallic  $\text{Sn(0)}$  and the formation of the amorphous  $\text{Li}_4\text{P}_2\text{O}_7$  matrix, where  $\text{Sn(0)}$  is

Table 1 Elemental composition of the as-synthesized materials obtained by EDX

	C (wt%)	O (wt%)	P (wt%)	Sn (wt%)
GOPR800_Sn	37.7	12.6	16.5	33.2
GOPR900_Sn	39.2	9.9	11.6	39.3
GOPR1000_Sn	47.0	7.9	10.8	34.3



Fig. 2 SEM images of the as-synthesized materials: GOPR1000\_Sn (a), GOPR900\_Sn (b), and GOPR800\_Sn (c and d). The scale is adapted to clearly show the morphological differences among the three materials.



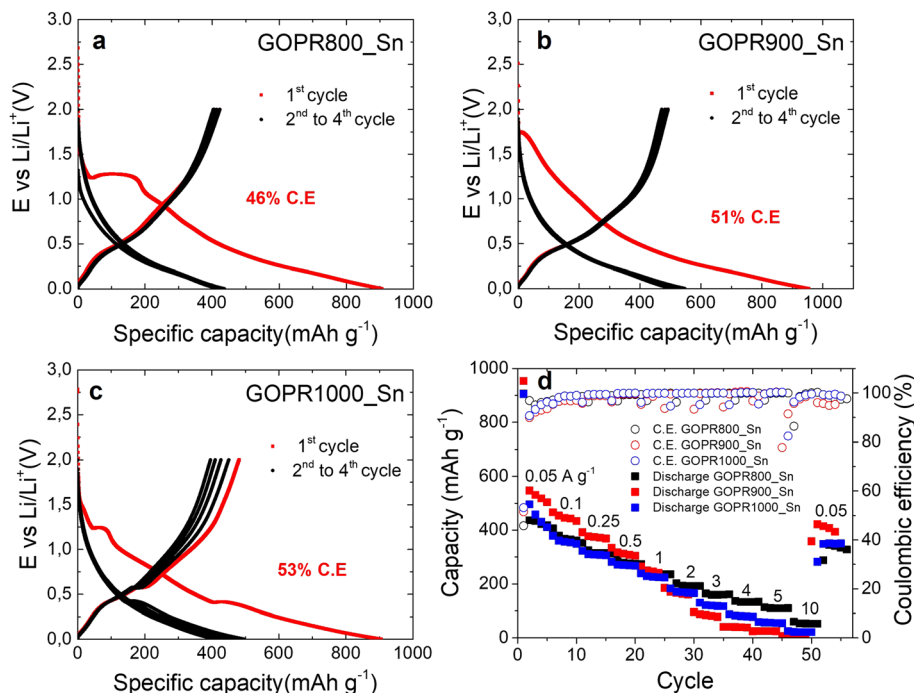


Fig. 3 Electrochemical characterization of the negative electrodes: galvanostatic charge/discharge of the first four cycles recorded at  $0.05 \text{ A g}^{-1}$  for GOPR800\_Sn (a), GOPR900\_Sn (b), GOPR1000\_Sn (c) and rate capability and their respective coulombic efficiency (d).

homogeneously dispersed (see eqn (1)) and (2) the formation of reversible lithium tin alloys (see eqn (2)).<sup>11,18,40</sup> The first irreversible process is evidenced at about 1.3 V, while the reversible alloying takes place at about 0.4 V.<sup>21,22</sup>



Fig. S3a and b† show the SEM images of the cycled GOPR800-Sn obtained using Everhart–Thornley (ETD) and backscattered electron (BSED) detectors, respectively, where one can observe the SEI and the  $\text{Li}_4\text{P}_2\text{O}_7$  matrix covering the reduced graphene oxide sheets, and the Sn(0) particles embedded in it.

The poor coulombic efficiency of 46% recorded for the first cycle accounts for all irreversible previously explained processes as well as the solid electrolyte interface (SEI) formation. The 3 subsequent cycles show sloping profiles with no marked plateaus, characteristic of  $\text{Li}^+$  insertion into non-graphitic materials, and the coulombic efficiency is close to 100%. By contrast, no defined plateaus are recorded for the first discharge of GOPR900\_Sn (Fig. 3b) due to its amorphous character where both  $\text{SnP}_2\text{O}_7$  and Sn(0) coexist along the graphene sheets. Also, the coulombic efficiency is slightly improved to 51%. Finally, the first discharge of GOPR1000\_Sn (Fig. 3c) shows a small plateau at 1.3 V and a prominent one at 0.4 V. The first small plateau accounts for the irreversible conversion of the remaining fraction of  $\text{SnP}_2\text{O}_7$  (undetectable by XRD) to Sn(0), while the second is for the Li/Sn alloying reaction, as previously explained. The coulombic efficiency is again enhanced to 53%

since less irreversible reactions take place. The subsequent 3 cycles still show marked plateaus at 0.4 V and worse coulombic efficiencies than the two previous materials due to the hindered lithiation of big Sn particles and their further breakup. Fig. S2a† clearly shows the different processes that take place during the first discharge for the three materials. Afterwards, galvanostatic charge–discharge curves at different current densities (Fig. S2b–d†) were recorded. Fig. 3d reveals that GOPR900\_Sn is the material best performing at low current densities ( $\sim 500 \text{ mAh g}^{-1}$ ), but its capacity drops drastically above  $2 \text{ A g}^{-1}$ . GOPR1000\_Sn and GOPR800\_Sn show similar capacities at low current densities ( $\sim 420 \text{ mAh g}^{-1}$ ), yet lower than that of GOPR900\_Sn, but the retention at high rates is highly improved. This is especially true for GOPR800\_Sn, which still retains  $110 \text{ mAh g}^{-1}$  at  $5 \text{ A g}^{-1}$ . This evidences that both morphology and microstructure clearly influence the electrochemical performance upon lithiation/de-lithiation. The submicrometer size of metallic Sn after the irreversible reduction of  $\text{SnP}_2\text{O}_7$  and its homogenous distribution over  $\text{Li}_4\text{P}_2\text{O}_7$ /graphene matrix enables the faster insertion of  $\text{Li}^+$  into the GOPR800\_Sn negative electrode. The better rate performance of the last material decides on its being the best choice as the negative electrode for our lithium-ion capacitor.

### 3.2. Characterization of the positive electrode

As stated above, a composite made of 40% of LFP/C and 60% RG was developed to be used as a positive electrode in LICs. Both components, LFP/C and RG, were synthesized and optimized separately. RG synthesis and electrochemical performance were already reported in our previous publication.<sup>33</sup> This material



was chosen as the most suitable activated carbon for the composite due to its large specific surface area, flat morphology, high specific capacitance, and excellent capacity retention.

On the other hand, and as described in the experimental section, LFP was hydrothermally synthesized from the  $\text{H}_3\text{PO}_4$ ,  $\text{LiOH}$ , and  $\text{FeSO}_4$  precursors using EG as a structure-directing agent to limit the particles' growth. Then, the LFP particles were coated with carbon to increase the conductivity and improve the contact between them. The carbon coating was performed by ball-milling a mixture of LFP with 10% w/w of Super P C65 conductive carbon using a 20 : 1 w/w ball-to-sample mass ratio for 3 hours at 250 rpm.

The SEM image of carbon-coated LFP (LFP/C) (Fig. 4a) shows irregular-shaped particles present on this sample and good connectivity between them. The analysis of SEM images with the ImageJ software allowed obtaining the particle size distribution (Fig. 4b) that ranges between 20 nm and 200 nm. Most of

the particles (78%) are smaller than 100 nm, with 31% between 60 and 100 nm, 33% between 40 and 60 nm, and 14% between 20 and 40 nm.

The XRD pattern in Fig. S4† shows characteristic peaks of the LFP olivine structure<sup>41</sup> ( $\alpha\text{-LiFePO}_4$ ). This confirms the successful synthesis procedure since, as previously reported, the olivine structure electrochemically outperforms other LFP structures. The XRD diffraction pattern registered for the LFP/C sample was treated using the FullProf software. After the carbon coating, the diffraction pattern still matches with the LFP olivine structure as shown in Fig. 4c, confirming that the structure is not damaged during the high-energy ball-milling. Further analysis of these patterns by FullProf software and the Scherrer equation allowed us to determine the average crystallite size of both the LFP and LFP/C samples. The average crystallite size was reduced during ball-milling from 39.5 nm for LFP to 19.7 nm for LFP/C. The crystallite size of LFP/C measured by XRD is smaller than the particle size obtained by SEM, meaning that this sample is formed by the aggregation of nanometric LFP/C crystals. Smaller particle sizes would be beneficial due to two reasons:<sup>29</sup> (i) the  $\text{Li}^+$  diffusion pathway along LFP/C particles is shortened, allowing a faster migration of  $\text{Li}^+$  from the bulk of  $\text{LiFePO}_4$  particles, which results in an improved performance at high current densities;<sup>42</sup> (ii) nano-sized LFP/C particles can be easily and homogeneously distributed along the activated carbon RG during the fabrication of the  $\text{R}_G\text{-LFP40}$  composite improving the electrical contact between the LFP/C particles and the RG matrix, and thus increasing the electrical conductivity of the electrode leading to higher capacity values and better capacity retention.

Summarizing, the carbon coating results in decreased particle size, better conductivity, and enhanced particle connectivity, which triggers improved electrochemical performance as evidenced in Fig. S5.†<sup>30</sup>

The SEM characterization results of the  $\text{R}_G\text{-LFP40}$  composite are shown in Fig. 5a and b. The composite is formed by the small-size particles of LFP/C and some agglomerates homogeneously integrated into the RG matrix. It is worth remarking that the good connectivity between the LFP/C and RG particles enhances the electronic conductivity of the composite. Also, there are some voids between particles that will enhance the electrode wettability and further improve ion adsorption.

Textural properties of  $\text{R}_G\text{-LFP40}$  composite were determined from nitrogen adsorption/desorption isotherms and included in Fig. 5c. For the sake of comparison, the textural properties of our previously reported RG are also included.<sup>33</sup> The isotherms of both RG and  $\text{R}_G\text{-LFP40}$  can be ascribed to type I according to the IUPAC classification, which corresponds to microporous samples. RG shows a BET specific surface area ( $S_{\text{BET}}$ ) of  $2318 \text{ m}^2 \text{ g}^{-1}$ . In the case of  $\text{R}_G\text{-LFP40}$ , the high loading of non-porous LFP/C particles and the partial pore clogging in the RG matrix result in a decrease in  $S_{\text{BET}}$  to only  $1151 \text{ m}^2 \text{ g}^{-1}$ . Pore size distributions calculated from the isotherms are depicted in Fig. 5d. Both materials are mainly composed of micropores (<2 nm), with a high volume of small micropores ( $\sim 0.85 \text{ nm}$ ). Also, as explained before, LFP/C particles obstruct the ultra-micropores (0.59 nm) of the RG matrix.



Fig. 4 SEM image of LFP/C (a), particle size distribution of LFP/C (b), and LFP/C XRD data refinement (c).





Fig. 5 EDT and BSD SEM images of RG-LFP40 electrodes (a and b),  $N_2$  adsorption/desorption isotherms (c), and pore size distribution of RG and RG-LFP40 (d).

The electrochemical performance of composite  $R_G$ -LFP40 was evaluated in the three-electrode cell configuration by cycling at several current densities between 2.0 and 4.2 V vs. Li/Li<sup>+</sup>. Also, to evaluate the impact of adding LFP/C to the activated carbon RG, both materials were also studied separately under the same conditions. The capacities obtained during the galvanostatic charge/discharge measurements are presented in Fig. 6a. Expectedly, at low current densities the faradaic LFP/C material (131 mAh g<sup>-1</sup>) outperforms composite  $R_G$ -LFP40 (102 mAh g<sup>-1</sup>) and capacitive material RG (91 mAh g<sup>-1</sup>). Nevertheless, from 0.5 A g<sup>-1</sup> on, the better capacity retention of  $R_G$ -LFP40 must be highlighted since it exceeds 80 mAh g<sup>-1</sup> at 30 A g<sup>-1</sup>.

To understand the better electrochemical performance of this material, a deeper analysis of the characteristic storage mechanisms was performed by differential capacity vs. voltage plot (Fig. 6b). On one hand, RG exhibits a typical rectangular profile ascribed to pure capacitive storage. On the other hand, two different storage mechanisms are observed for LFP/C: (i) the sharp peaks at 3.5 V and 3.4 V ascribed to the Li<sup>+</sup> insertion/deinsertion faradaic reaction of LFP represented by eqn (3),<sup>43</sup> and (ii) broad peaks in the 2.0–3.5 V potential window related to a pseudo-capacitive storage mechanism.



Finally, the  $R_G$ -LFP40 composite shows a combination of the three mechanisms: (i) capacitive, (ii) pseudo-capacitive, and (iii) faradaic. The pseudo-capacitive mechanism is worth mentioning since it enables the good performance of the  $R_G$ -LFP40 composite at high current densities.<sup>44</sup> While the

faradaic phase transition of LiFePO<sub>4</sub> to FePO<sub>4</sub> and *vice versa* is a slow process taking place in the bulk of the electrode, pseudo-capacitance is a fast mechanism caused by charge-transfer reactions at the electrode/electrolyte interphase enabling charge storage at high charge/discharge rates. The significant pseudo-capacitive feature present for the LFP/C nanoparticles is explained by two reasons: (i) nanosized particles with a high surface-to-volume ratio substantially increase the share of the surface-confined redox activity over that of the bulk redox process, boosting pseudo-capacitive contribution;<sup>45</sup> (ii) amorphous LFP was reported to exhibit pseudo-capacitive Li<sup>+</sup> insertion by a solid-solution reaction, the amorphization of LFP/C particles could be accomplished during the carbon coating process.<sup>32</sup> The contact with the amorphous carbon can distort the LFP lattice and, in addition, the contact with the environment during the high-energy ball-milling can induce the formation of Fe<sup>3+</sup> with a disordered structure.<sup>32,45</sup> In our experiments (Fig. S6†), the amorphization of LFP is confirmed using post-electrochemistry XRD analysis where most of the characteristic peaks for LFP are not discerned upon cycling whereas SEM shows no change in the shape and size of LFP.

The integration of the optimized LFP/C nanoparticles onto the RG matrix enables a higher percentage of the faradaic material in the hybrid cathode compared with most systems recently reported in the literature, increasing the specific capacity of the electrode while keeping excellent capacity retention values at high current densities.<sup>25</sup>

The charge/discharge profiles at 0.25 A g<sup>-1</sup> and 5 A g<sup>-1</sup> are shown in Fig. 6c and d. At low current densities, the Li<sup>+</sup> ions have enough time to move in and out of the bulk of the LFP/C





Fig. 6 Dependence of the specific capacitance on the current density (a), differential capacity vs. voltage plot (b), galvanostatic charge/discharge profiles registered at 0.25 A g<sup>-1</sup> (c), and 5 A g<sup>-1</sup> (d) for the studied samples.

particles. This fact is clearly shown in Fig. 6c, where LFP/C and RG-LFP40 outperform RG. As expected, high current densities have a detrimental effect on the LFP/C performance, which loses its insertion/de-insertion plateaus. In this scenario, RG-LFP40 still outperforms the bare RG. The composite successfully combines the high capacity of LFP/C and the excellent capacity retention of RG.

### 3.3. Characterization of the full-cell hybrid lithium-ion capacitor

As previously explained, R<sub>G</sub>-LFP40 and rGO800-P-Sn were selected as the positive and negative electrodes, respectively. Prior to LIC assembly, rGO800-P-Sn was pre-lithiated to form an SEI and supply enough lithium to counterbalance the irreversibility of the first cycles. The pre-lithiation step consists of 5 charge/discharge cycles at C/10 between 0.002 and 2 V vs. Li/Li<sup>+</sup>. Then, a cutoff potential of 0.2 V vs. Li/Li<sup>+</sup> was set to maximize the use of the negative electrode while preventing lithium plating. Also, the positive electrode potential was set to 4.2 V vs. Li/Li<sup>+</sup> to maximize its use at the time that electrolyte decomposition is avoided.

To maximize the output capacity, a mass balancing of the electrodes was performed. The charge stored on each electrode must be equal ( $Q_+ = Q_-$ ) and proportional to the capacitance ( $C_+$ ,  $C_-$ ), the active mass of the materials ( $m_+$ ,  $m_-$ ), and the working potential window ( $\Delta E_+$ ,  $\Delta E_-$ ) [eqn (4) and (5)].

$$Q_+ = m_+ C_+ \Delta E_+ \quad (4)$$

$$Q_- = m_- C_- \Delta E_- \quad (5)$$

The selection of a unique mass ratio that maximizes energy and power densities is difficult since the capacity of each electrode changes depending on the applied current density, and the working potential in the LIC differs from the one used to characterize each electrode individually. Thus, two different LIC configurations were evaluated: LIC1:1 and LIC1:2 (being LIC  $m_+ : m_-$ ). LICs were galvanostatically cycled at different current densities in the 1.5–4.2 V vs. Li/Li<sup>+</sup> cell voltage range. The profiles of the positive and negative electrodes as well as the full LIC at the current densities of 0.1 A g<sup>-1</sup> and 5 A g<sup>-1</sup> are depicted in Fig. 7. At 0.1 A g<sup>-1</sup>, capacitive and faradaic storage mechanisms are clearly visible for both LIC1:1 and LIC1:2. The LFP insertion/de-insertion plateaus at 3.4/3.5 V are combined with the linear profile characteristic of capacitive materials, with a minimum ohmic drop. The positive electrode of LIC1:1 swings from 4.46 V to 2.26 V (2.2 V) while the positive electrode of LIC1:2 goes from 4.39 V to 2.02 V (2.37 V). In the case of LIC1:1, the negative electrode fluctuates between 0.26 V and 0.76 V (0.5 V) while in the case of LIC1:2, the negative electrode moves between 0.19 V and 0.52 V (0.33 V). At 5 A g<sup>-1</sup>, the effect of the LFP/C is still visible in both LIC1:1 and LIC1:2 due to its pseudocapacitive characteristics, fast enough to store charges at high current densities. As expected, the ohmic drop increases, but is still low for both LIC1:1 and LIC1:2 at 5 A g<sup>-1</sup>. As the current density increases, there are greater differences between the voltage swing of the electrodes of the two LICs. The positive electrode of LIC1:1 fluctuates between 4.32 V and 2.43 V (1.89 V) while the positive electrode of LIC1:2 swings between 4.40 V and 2.05 V (2.35 V). The negative electrode of LIC1:1 goes from 0.12 V to 0.93 V (0.81 V) while the negative electrode of LIC1:2





Fig. 7 Galvanostatic charge/discharge profiles at  $0.1 \text{ A g}^{-1}$  and  $5 \text{ A g}^{-1}$  for LIC1:1 (a and b) and LIC1:2 (c and d): LIC (black), negative electrode (red), and positive electrode (blue).

moves between 0.20 V and 0.55 V (0.35 V). The overall difference between the electrode's potential ranges in the LICs is caused by the different mass ratios. This fact becomes increasingly important for the higher current densities. A heavier negative electrode is a conservative option with a shorter potential range that prevents lithium plating (the better safety option), this is easily recognizable in Fig. 7, especially at the high current density. Nevertheless, the full device will provide a lower energy density compared with a higher positive to negative electrode mass ratio.

The gravimetric energy and power densities of the LICs, calculated from the galvanostatic curves are included in Fig. 8. LIC1:1 outperforms LIC1:2 in terms of energy and power densities. LIC1:1 shows a remarkable energy density of

$143 \text{ Wh kg}^{-1}$  at  $128 \text{ W kg}^{-1}$  and retains  $100 \text{ Wh kg}^{-1}$  at  $2500 \text{ W kg}^{-1}$  and  $45 \text{ Wh kg}^{-1}$  at a maximum power density of  $25000 \text{ W kg}^{-1}$  without any evidence of lithium plating. As far as we know, this result surpasses most of the similar devices comprising composites that contain LFP in the positive electrode (see Table 2). Even considering the high loading of LFP in our composite (40%), the power performance has been preserved, which is usually the major challenge for this type of device. This can be explained by the proper optimization of both the positive and negative electrodes. In the positive electrode, nanosized LFP/C particles homogeneously dispersed into the graphene/activated carbon RG allow energy storage *via* faradaic, pseudo-capacitive, and capacitive mechanisms, maximizing the power performance. In the negative electrode, nanosized Sn particles homogeneously embedded into the conductive graphene/ $\text{Li}_4\text{P}_2\text{O}_7$  matrix can be rapidly lithiated/de-lithiated without suffering from huge volume changes and enabling an exceptional rate capability.

Owing to the better performance of LIC1:1, it was further subjected to a cycling stability test at  $2 \text{ A g}^{-1}$  ( $t_{\text{discharge}} = 1 \text{ min}$ ), showing 72% capacity retention after 2000 cycles. Although this value is somewhat lower than expected, it must be taken in the context of the high loading of faradaic materials (the full-faradaic negative electrode and 40% of LFP in the positive electrode) compared to other similar devices (Table 2 and Fig. S7†) and the limitations associated with the Swagelok-type cells used to perform the stability measurements. One approach to improve cycle life is to reduce the amount of faradaic materials, but energy delivery will be an obvious trade-off.<sup>28,46</sup>



Fig. 8 Ragone plot comparing gravimetric energy and power densities of LIC1:1 and LIC1:2.



Table 2 Electrochemical performance of relevant LFP-based LICs

Positive electrode	Negative electrode	LIC max. energy density (Wh kg <sup>-1</sup> )	LIC max. power density (W kg <sup>-1</sup> )	LIC power density at 100 Wh kg <sup>-1</sup> (W kg <sup>-1</sup> )	Number of cycles (% retention)	Ref.
LFP/AC 40/60% (6 layers)	Hard carbon	66	2000	—	14k (90%) 5 A g <sup>-1</sup>	28
LFP/expanded graphite	AC/graphite 90/10	15,1	2367	—	10k (70%) 2 A g <sup>-1</sup>	29
LFP/AC 20/80% multilayer	Hard carbon	—	—	—	1k (94%) 1 C	47
LFP/AC 20/80% pouch	Hard carbon	30	2000	—	30 k (90%) 60 C	48
LFP/AC 25/75%	Mesocarbon microbeads	30	1000	—	1k (100%) 0.05 A g <sup>-1</sup>	49
LFP/AC 20/80%	LTO	90	15 000	—	—	50
LFP/AC 20/80%	Hard carbon	—	—	—	5k (88.5%)	25
LFP/mesoporous carbon	Hard carbon	130	25 000	20 000	3k (92%)	32
LFP/AC 40%	GOPR800_Sn	158	26 600	4000	2.2k (70%) 2 A g <sup>-1</sup>	This work

## 4. Conclusions

We demonstrated a high-energy and power-performing lithium-ion capacitor comprising a tin and phosphorus-graphene-based composite as the negative electrode and a high-loading LFP/graphene-activated carbon as the positive electrode.

Particularly, it has been found that the incorporation of nano-sized crystalline tin pyrophosphate (SnP<sub>2</sub>O<sub>7</sub>) particles in a graphenic matrix can promote fast kinetics for Li<sup>+</sup> insertion/de-insertion, reaching high specific capacities even at fast rates (420 mAh g<sup>-1</sup> at 0.5 A g<sup>-1</sup> and 110 mAh g<sup>-1</sup> at 5 A g<sup>-1</sup>).

The incorporation of carbon-coated LFP particles (the battery-type material) with irregular shape and nanometer size in the graphene-activated-carbon positive electrode enables energy storage *via* faradaic, pseudo-capacitive, and capacitive mechanisms with an outstanding capacity even at high rates (102 mAh g<sup>-1</sup> at 0.25 A g<sup>-1</sup> and 80 mAh g<sup>-1</sup> at 30 A g<sup>-1</sup>).

The full optimization of the assembled LICs using mass balance 1:1 allowed high energy densities without compromising power performance (143 Wh kg<sup>-1</sup> at 128 W kg<sup>-1</sup> and 45 Wh kg<sup>-1</sup> at 25 000 W kg<sup>-1</sup>), overcoming the main power limitations of LFP-containing LICs.

## Conflicts of interest

There are no conflicts to declare.

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