



Cite this: *Lab Chip*, 2016, 16, 208

## Digital droplet PCR on disk†

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Existing systems for digital droplet PCR (ddPCR) either suffer from low integration or are difficult to introduce to mass fabrication. Here we present an integrated system that is compatible to mass fabrication and combines emulsification, PCR, and fluorescence readout in a single chamber within a disposable cartridge (disk). Droplets are generated by injecting the sample into fluorinated oil *via* centrifugal step emulsification. The resulting emulsion is aligned in the PCR and readout zone by capillary action. During thermocycling, gas bubbles generated by degassing are removed by capillary driven transport through tapered regions in the PCR chamber. Thereby, the positioning of the emulsion within the readout zone of the PCR chamber is ensured at any time and no bubbles are present during readout. Manual handling of the disk solely requires pipetting of oil and PCR mix into the inlet structures, placing the disk into the thermocycler and subsequently into a microarray scanner. The functionality of the ddPCR process chain is demonstrated by quantitative detection of the cystic fibrosis causing mutation p.Phe508del, which is of interest for non-invasive prenatal testing (NIPT). The mutation was detected in a concentration range spanning four orders of magnitude. We envision that this work will lay the base for the development of highly integrated sample-to-digital-answer PCR systems that can be employed in routine clinical diagnosis.

Received 8th September 2015,  
Accepted 3rd November 2015

DOI: 10.1039/c5lc01068c

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## Introduction

Digital droplet polymerase chain reaction (ddPCR) is a versatile tool that enables absolute quantification of nucleic acids without the need for any calibrants. It features single molecule sensitivity and is relatively tolerant towards inhibitors.<sup>1</sup> To perform a ddPCR, the sample containing PCR mix and target DNA must first be emulsified. Other dPCR systems use physical compartments on stationary<sup>2</sup> or centrifugal systems<sup>3</sup> for digital PCR. In particular for centrifugal systems, it is difficult to integrate a sufficient number (>1000) of physical compartments, to ensure evenly sized, sufficiently small aliquots.

In droplet digital PCR, typically more than 10 000 droplets in the nano- to picoliter range are produced, submerged in fluorinated oil.<sup>4</sup> This emulsion is then thermocycled to perform a PCR in the droplets. Afterwards, the droplets are read out by fluorescence measurements. Commercialization of ddPCR<sup>5</sup> drastically increased the use of the technique. However, the current methods require many handling steps and

multiple pieces of specialized machinery and disposables (e.g. 4 machines and 2 disposables are needed when using one of the currently commercially available systems<sup>6</sup>). This in turn comes with relatively high costs and the need for specially trained personnel. To simplify this process, a higher integration of emulsification, thermocycling and readout is needed. Systems have been proposed to introduce the produced droplets into a shallow chamber instead of a tube, so that a monolayer of droplets forms.<sup>7,8</sup> This monolayer is then thermocycled with subsequent readout in the same chamber. A major problem for microfluidic PCR in general<sup>9</sup> and specifically when performed in shallow chambers is the development of bubbles, mainly caused by degassing of dissolved gas within the oil phase. This also leads to unfavourable evaporation of oil. Emerging bubbles may displace the emulsion from the reaction chamber, or exert shear forces on the droplets that can lead to merging of the same, posing problems during readout.<sup>8</sup> It is therefore important to employ methods which either avoid bubble formation entirely or guide the bubbles away from the PCR and readout zone. Fully closed systems<sup>7</sup> generate an internal pressure when bubbles are produced. This pressure prevents the generation of further bubbles. Such a fully closed system is more difficult to handle while still not eliminating bubble formation entirely. To counter this problem, pressurized systems with an active external pressure generation have been demonstrated to completely avoid bubble generation.<sup>9,10</sup> However, these solutions

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† Electronic supplementary information (ESI) available. See DOI: 10.1039/c5lc01068c



need a bulky pressure source and interfaces that connect the chamber to a pressure source. Hatch *et al.*<sup>8</sup> used mineral oil in PDMS/glass composite chips to avoid bubbles in most cases. Flushing the chip with oil was required as a pre-treatment to reduce bubbles. Still in about 5% of the reported experiments, bubble formation inhibited the experiment. In addition, the use of PDMS for microfluidic structures in general and specifically for droplet microfluidics has a number of disadvantages<sup>12</sup> with the major one being the difficulty to scale up production.<sup>13</sup> Compared to fluorinated oil, the use of mineral oils is inferior with regard to droplet stability. Thus, ddPCR systems should be compatible with fluorinated oils. However, the high gas solubility of fluorinated oils<sup>14</sup> may lead to severe bubble problems. As a possible solution, degassing of the oil prior to use needs specialized equipment and requires the oil to be used directly afterwards since the uptake of gas from the surrounding air is relatively fast.

The above mentioned shortcomings highlight the need for an integrated and low cost ddPCR system that reliably removes bubbles from shallow chambers, is compatible with mass production and fluorinated oils and easy to handle for the end user. Here, we present such a cartridge (disk) that integrates a centrifugal microfluidic process chain for ddPCR analysis comprising the unit operations emulsification, capillary driven self-alignment and capillary driven bubble removal during PCR amplification and subsequent readout in one single chamber of a disposable disk. In this context, as introduced recently,<sup>15</sup> the term process chain is used to provide standardized implementations of a complete laboratory workflow (here ddPCR) on a higher level of integration as compared to using unit operations. The integrated ddPCR system is applied for a proof-of-principle ddPCR for non-invasive prenatal testing (NIPT).

### System description

The chip (a disk shaped disposable) is made from a thermoplast (COC) and is compatible to scalable manufacturing techniques such as injection moulding. The ddPCR process chain comprises centrifugal step emulsification<sup>11</sup> to produce aqueous microdroplets in fluorinated oil. The emulsion is then positioned in the PCR chamber by capillary driven self-alignment. The tapered shape of the PCR chamber is also used to completely remove any bubbles formed during thermocycling, again by capillary driven bubble transport.<sup>16</sup> Since droplets remain in a stable monolayer throughout the PCR, the subsequent fluorescence readout can be performed in the same chamber. User interaction is limited to 3 pipetting steps and one transfer of the disk. Automated emulsification and PCR are performed by the same centrifugal processing device. A post-PCR fluorescence scan is done in a commercial microarray scanner.

### Working principle

The centrifugal microfluidic disk comprises one minimalistic structure for emulsification, capillary driven self-alignment of the emulsions in the PCR and readout zone, and capillary driven bubble removal. The latter two are both new unit operations with respect to the implementation of ddPCR. A sketch with explanations is depicted in Fig. 1.

### Centrifugal step emulsification

Droplets are generated by centrifugal step emulsification as shown recently.<sup>11</sup> The process of droplet generation is illustrated in Fig. 2. In brief, an inlet is connected to a PCR chamber by a microfluidic channel. A backward facing step is located at the junction of the channel and the PCR chamber (*i.e.* the line between the red and green region in Fig. 1C) is the backward facing step). First, the disk is loaded with oil; afterwards PCR mix is introduced to the inlet and spun down the channel by centrifugal forces. Monodisperse droplets form at the backward facing step. The droplet production is exclusively determined by surface tension and the size of the channel. The droplets rise in the fluorinated oil towards the centre of rotation, since the droplets (composed of PCR mix,  $\rho = 1.0 \text{ g ml}^{-1}$ ) are less dense than the surrounding fluorinated oil ( $\rho = 1.6 \text{ g ml}^{-1}$ ).

### Capillary driven self-alignment

During centrifugation, the emulsion is located in the radially outer part of the chamber touching the radially outer side of the pyramid. Two counteracting forces act on the emulsion (see Fig. 3). First, the centrifugal force that pushes the emulsion radially outward. Second, the capillary force acting on the oil/gas interface located in the shallow area between the sealing foil and the side of the pyramid. The capillary force pulls the emulsion radially inward onto the shallow region.

When spinning the disk at relatively high rotational frequencies, the centrifugal force dominates and a meniscus almost concentric to the center of rotation is formed. A small deviation from concentric shape is due to a slightly higher capillary force in the shallow region of the pyramid. Decreasing the speed of rotation leads to a decreased centrifugal force. The capillary force starts to take over and pulls the emulsion onto the shallow areas until it completely detaches from the radially outer part of the chamber and is located in the shallow area.

### Capillary driven bubble removal

In order to remove any disturbing bubbles, capillary driven bubble transport is employed which has been used previously for removal of bubbles in methanol fuel cells.<sup>17,18</sup> While this principle can be used to support the formation of droplets,<sup>19</sup> here it is applied to the capillary driven bubble movement. The transport of bubbles away from the PCR zone is achieved by tilting the bottom of the chamber relative to the ceiling. The bottom of the PCR chamber thus forms a pyramid with its tip located in the centre (compare Fig. 1). The angle between the pyramid sides (*i.e.* the bottom of the chamber) and the ceiling ( $\alpha$ ) enables the transport of bubbles away from the centre of the pyramid to its sides as described in the following. Bubbles trapped between the bottom and ceiling of a shallow chamber are deformed as soon as the bubble diameter exceeds the chamber height (Fig. 4). Since bottom and ceiling are tilted with respect to each other at an angle  $\alpha$  (compare Fig. 1B), different curvatures of the interfaces of the bubble form with the higher curvature located in the more shallow region, as schematically depicted in Fig. 4B).





**Fig. 1** Schematic outline of the all-in-one digital droplet PCR disk. A) Section of a circular disk with embedded microfluidic structures (top view), the centre of rotation is on the top. An inlet (red) is connected to the PCR chamber (green) by a channel (red). The channel leads to a centrifugal step emulsification nozzle (see inset C)). The emulsification chamber is connected to the inlet by an air vent. The PCR chamber features two zones, the PCR and readout zone (light green) and the surrounding bubble drains (dark green). Both, the inlet and the PCR chamber have inlets (black) to allow the loading of liquids to the disk. B) A cross section of the tapered PCR chamber. The largest part of the chamber is occupied by a pyramid with inclination angle  $\alpha$ . The chamber is sealed with a sealing foil (blue) so that the chamber has a varying depth  $d$ .  $d_0$  should be larger than the droplet size, while the maximum depth should be less than twice the droplet size, so that a continuous monolayer forms. C) Centrifugal step emulsification nozzle (top view) as reported in our previous work.<sup>11</sup> The feed channel (red) opens to a terrace (red) that has the same depth as the feed channel. The dark green area north of the red terrace is significantly deeper than the terrace.

According to the Young-Laplace equation, the pressure at the interface in non-spherical bubbles is defined as:

$$p_{\text{cap}} = \sigma \left( \frac{1}{r_1} + \frac{1}{r_2} \right)$$

where  $r_1$  and  $r_2$  are the two mean radii of the interface. Since the bubble has a circular cross section when seen from the top, the mean radius  $r_2$  is the same for every point on the interface. The cross section through the bubble perpendicular to the chamber (compare Fig. 4B)) however, is not circular with two different radii at the positions A and B. Therefore, different capillary pressures emerge at the different curvatures of the interface. These different capillary pressures cause a pressure difference across the bubble as schematically depicted in Fig. 4B). In order to illustrate the driving forces of bubble transport, the propelling pressure difference across the bubble can be derived from the Young-Laplace equation:

$$\begin{aligned} \Delta p_{\text{bub}} &= p_{\text{cap}}(r_{1A}) - p_{\text{cap}}(r_{1B}) = \sigma \left( \frac{1}{r_{1A}} - \frac{1}{r_{1B}} \right) \\ &= \sigma \left( \frac{2 \cos(\theta_{\text{ad}})}{d_A} - \frac{2 \cos(\theta_{\text{rec}})}{d_B} \right) \end{aligned}$$

where  $p_{\text{cap}}$  is the capillary pressure at the interface of the bubble in the shallow region (A) and the deeper region (B), respectively.  $r_{1A}$  and  $r_{1B}$  are the mean curvature radii in the

cross-section plane of the bubble and  $d_A$  and  $d_B$  are the chamber depth at the two interface positions A and B.  $\theta_{\text{ad}}$  and  $\theta_{\text{rec}}$  are the advancing and receding contact angles of the oil at the interface to gas, respectively.

The pressure difference across the bubble causes a pressure increase in the continuous liquid phase (oil) from shallow to the deep (Fig. 4B, bottom). Consequently, an oil flow sets on from deep to shallow regions around the bubble. This pushes the bubble in the opposite direction of the oil flow towards the opening of the tilted bottom and ceiling, until equilibrium is reached. This equilibrium is achieved when the bubble is of perfectly spherical shape. In a perfect spherical shape, all three radii  $r_{1A}$ ,  $r_{1B}$ , and  $r_2$  are the same and no pressure differences remain.

## Experimental

### Production of disks

The microfluidic disks were fabricated by Hahn-Schickard Lab-on-a-Chip Design & Foundry Service.<sup>20</sup> First, a master mold was produced by micro milling in polymethyl methacrylate (PMMA) (Maertin, Freiburg, Germany) using a Kern Evo (Kern Micro- und Feinwerktechnik GmbH & Co. KG, Eschenlohe, Germany). Quality control was performed by using a Zeiss AX10 microscope equipped with an AxioCam ICc1 and an Imager M2m (Zeiss, Jena, Germany). Afterwards, a PDMS master was produced by pouring a mixture of Elastosil 607 and Elastosil 675 (1:1, with monomer/





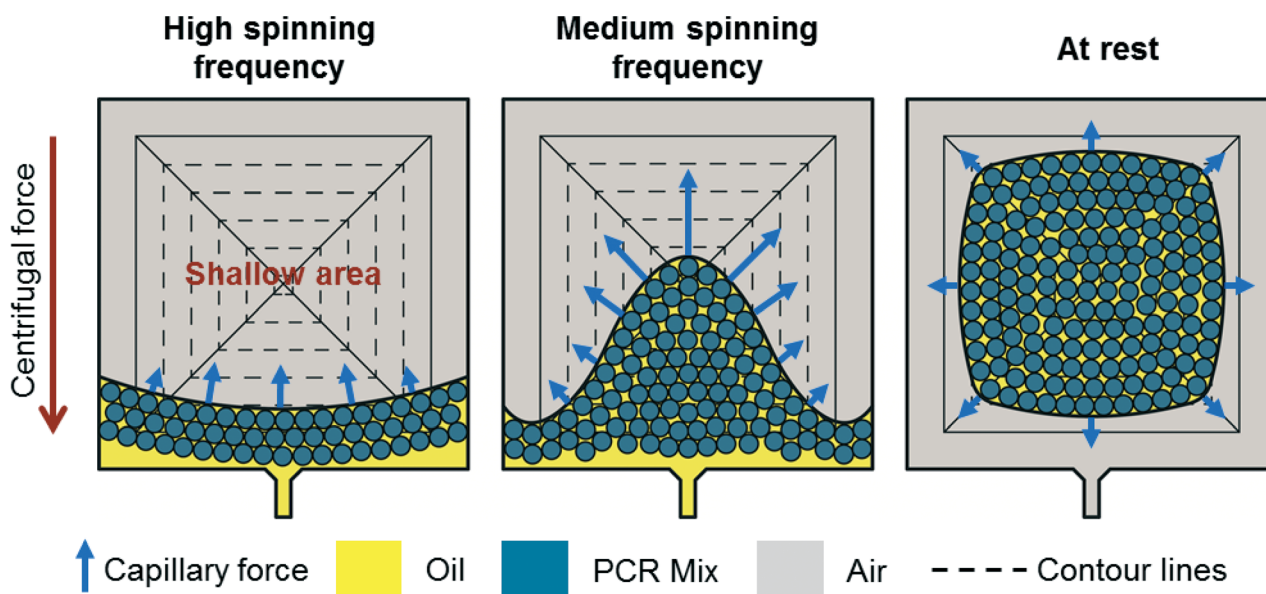
**Fig. 2** Principle of centrifugal step emulsification amended from.<sup>11</sup> The top view shows the step emulsification nozzle. The inlet channel coming from below opens to both sides forming a terrace. After that a sudden change in depth (step, dashed line) occurs that leads to the PCR and readout chamber. The PCR mix gets pushed through the inlet channel by centrifugal pressure. When it reaches the step a droplet is formed by capillary forces. The droplet rises in the surrounding oil due to buoyancy.

crosslinker ratios of 9:1 and 1:1 respectively) into the milled substrate and applying centrifugal force (Hettich Zentrifuge Rotanta 460 R). A hot stamp (Wickert WMP-30) was used to produce replicates of the master mold in COC (Topas 5013). Inlet holes were opened with a drill and the thickness

reduced to 1 mm with the Kern Evo. Pressure sensitive adhesive (PSA) foil (#900 320, HJ Bioanalytik, Erkelenz, Germany) was used to seal the structures with aid of a PCS 30 lamination tool (Jakob Weiß & Söhne, Sinsheim, Germany). The channel was 90  $\mu\text{m}$  wide and 60  $\mu\text{m}$  deep, the terrace was 100  $\mu\text{m}$  wide. The slope angle  $\alpha$  was varied from 1–6°, the width and length of the pyramidal structures was varied between 12.6 mm and 4.2 mm. The tip of the pyramid was located 180  $\mu\text{m}$  beneath the sealing foil.

### PCR

The disk was processed in a LabDisk player prototype (Qiagen Lake Constance, Stockach, Germany) that allows for rotation of the disks while heating and cooling with ambient air. For PCR, the inlet was filled with 15  $\mu\text{l}$  of Novec7500 with 5 wt% of Picosurf-1 (Dolomite, Royston, UK). The fluorinated oil was transferred to the PCR chamber by centrifugal force (15 Hz for 1 min). Reaction mix was prepared using Qiagen HotStar TaqPlus polymerase with 3 mM  $\text{Mg}^{2+}$  final concentration in the reaction mix and dNTPs used according to manufacturer's protocol (Qiagen, Hilde, Germany). Primer (300 nM final concentration), probes (200 nM final concentration) and target DNA (for sequences see below) were added to the mix and 20  $\mu\text{l}$  were then introduced in the inlet chamber. Emulsification took place by centrifugation (10 Hz for 8 min). Then, 20  $\mu\text{l}$  of FC-40 with 5 wt% of Picosurf-1 (Dolomite, Royston, UK) was introduced in the PCR chamber directly. FC-40 was introduced since the higher boiling point reduces the evaporation of oil during PCR. However, the disk needs to be filled with Novec7500 initially since droplet production is more



**Fig. 3** Schematic top views of the PCR chamber illustrating the static positions of the emulsion at different spinning frequencies. At high spinning frequencies, the emulsion is located on the radially outer part of the chamber since the centrifugal force outweighs the capillary force. The area above the emulsion is filled with air. At medium spinning frequencies, the emulsion covers the center of the pyramid (*i.e.* the most shallow area). Here, the capillary force is higher than on the sides where the structure is deeper. With the disk at rest, no centrifugal force is applied and the capillary forces prevail. The emulsion spreads on the shallow area until equilibrium is reached. In equilibrium, the capillary force is equal along the oil interface at any position. It should be noted that the total volume of emulsion remains unchanged throughout the process.







Fig. 4 Schematic of capillary driven bubble removal. A) Top view of an air bubble (grey) amidst PCR droplets (blue) in oil (yellow). From top, the bubble has a circular shape. B) Cross section through the bubble. The bubble is trapped between ceiling and bottom of the chamber. The ceiling and bottom are tilted with respect to each other at an angle  $\alpha$ . The pressure in the oil/air is depicted below. The pressure is constant in the oil, increases sharply at the interface and is static in the air volume again (otherwise there would be air flow to equate the pressure differences). The second pressure jump across the interface is smaller since the radius  $r_{1B}$  is larger than  $r_{1A}$ . C) Cross section through the chamber (compare Fig. 1B)). Sequence from 1 to 6: an air bubble is forming and transported away to the bubble drain on the right. The emulsion flows around the bubble.

reliable in this oil. The upper inlet holes were sealed with an air permeable filter (PTFE Pet Backed 0.2  $\mu\text{m}$ , Millipore, Tullagreen, Ireland), while the lower was sealed with PSA foil. The thermal protocol for the PCR was 5 min at 95  $^{\circ}\text{C}$ , followed by 45 cycles of 15 s at 95  $^{\circ}\text{C}$  and 60 s at 58  $^{\circ}\text{C}$ . The disk was rotated at 0.5 Hz. Sequences of primers, probes and DNA all in 5'  $\rightarrow$  3' direction (Life Technologies, Darmstadt, Germany):

Forward primer: GATTATGCCTGGCACCATTAAAG

Backward primer: GCATAATCAAAAAGTTTTCAC

Probe: FAM- CACCAATGATATTTT- MGB

Amplicon sequence: TGCCTGGCACCATTAAAGAAAATATCA-TTGGTGTTCCTATGATGAATATAGATACAGAAGCGTCATCAAAG-CATGCCAACTAGAAGAGGTAAGAACTATGTGAAAACTTTTG-ATTATGC (CFTR gene, OMIM 602421)

A dilution series of target DNA was prepared using LoBind tubes (Eppendorf, Hamburg, Germany) and dilution buffer containing 0.2 $\times$  TE buffer and 10 ng  $\mu\text{L}^{-1}$  herring sperm DNA. DNase/RNase free water (Thermo Fisher Scientific, Waltham, US) was used for the preparation of the buffers.

### Imaging

For imaging of the bubble generation during PCR conditions, a modified LabDisk player with a stroboscopic setup<sup>21</sup> was used. Fluorescence imaging was performed using a LaVision Bioanalyzer (4/4S, LaVision BioTec GmbH, Bielefeld,

Germany) with a custom made holder at 475 nm emission and 530 nm emission wavelength and 800 ms integration time. ImageJ<sup>22</sup> was used for evaluation of the images. Circular regions of interests were placed over the droplets manually and the grey value was measured. A threshold was defined manually. More than 500 droplets were evaluated per sample. To increase the sensitivity, more droplets would need to be counted which could be accomplished in future using an automated image recognition routine.

## Results and discussion

### Centrifugal step emulsification

The droplets have a diameter of 147  $\mu\text{m}$  with a CV of 1.4% (for details see Fig. S1<sup>†</sup>). A sample of 20  $\mu\text{L}$  DNA-solution yields approximately 11 000 droplets of 1.8 nL, each. A dead volume of <1% of the sample remains trapped in the channel. If needed, it can be removed by flushing the channel with oil to reduce the dead volume to zero.

### Capillary driven self-alignment

The process of capillary driven self-alignment of the emulsion in the PCR and readout zone is shown in Fig. 5 and in Movie S1<sup>†</sup>. The self-alignment process of the emulsion transports >99% of the emulsion to the PCR and readout zone



### A) Capillary driven self-alignment of emulsion

Spinning frequency decreases:

10 mm



### B) Capillary driven bubble transport



### C) Fluorescence image after PCR



**Fig. 5** Microscopic images of self-alignment of emulsion and bubble removal. Angle of slope:  $\alpha = 2^\circ$ . A) Microscopic images of the emulsion at different spinning frequencies. At 10 Hz, the emulsion is in the radially outer part of the chamber since the centrifugal force dominates the capillary force. The radially inner part is filled with air. As the spinning frequency decreases, the emulsion spreads onto the shallow area of the pyramid (square with 9 circular pillars that support the sealing foil). At 0.5 Hz, the emulsion is completely detached from the radially outer chamber wall. B) Capillary driven bubble removal. The bubbles are transported along the slope by capillary action. C) False color fluorescent image of droplets after PCR. Some edge effects can be observed, but most droplets remain stable and can be evaluated. Differences in illumination (vertical “lines”) are artefacts from stitching of multiple pictures to one large picture.

with only very few droplets remaining in the edges of the chamber. Moreover, no merging or coalescence of droplets due to shear forces could be observed. The total time needed for the alignment of the emulsion can be as low as 8 s. Since the disk surface is not perfectly smooth but features some grooves from micro milling, some pinning of the emulsion can be observed. It can be seen in Movie S1† that the pinning leads to a somewhat uneven propagation of the interface onto the shallow region. An inhibition of positioning by pinning however, has never been observed in more than 50 experiments. The emulsion is now perfectly aligned in the PCR zone for cycling and readout.

#### Capillary driven bubble removal

The gas solubility of liquids decreases with increasing temperature. Since the gas solubilities of FC-40 and HFE7500 are very high (0.27 and 0.48 ml air/ml oil, respectively),<sup>14</sup> the absolute amount of gas set free during heating from 25 °C to 95 °C is high as well. Some of this gas volume can be

released by diffusion at the oil/air interface, while a large part will be released in form of bubbles which need to be transported away. The amount of gas set free in form of bubbles was estimated to be no lower than 18% of the emulsion volume.

With respect to the geometry of the pyramid for capillary driven bubble transport, different configurations were studied with inclination angles  $\alpha$  of 1°, 2°, 4°, and 6°. All of these configurations removed all bubbles without any problems and allowed for precise positioning of the emulsion. This is likely due to the fact that the air bubbles in the emulsion have no direct contact to either bottom or ceiling. The fact that bubble transport is independent of inclination angle  $\alpha$  supports the assumption that the advancing and receding contact angles  $\theta_{ad}$  and  $\theta_{rec}$  at the left and right border of the moving bubble, respectively (compare Fig. 4B)) are zero or very close to it. This is due to the fact that a thin film of (highly wetting) fluorinated oil remains between the air and the polymer. The air bubble therefore never touches the polymer wall. This is also in line with the theory.<sup>19,23</sup>



The bubble transport works for all bubbles that are larger than the height of the chamber (see Movie S2†). This is important since the size of the bubbles varies. Very small bubbles that do not touch bottom and ceiling dissolve completely in the oil when the temperature is reduced (*e.g.* during the annealing step of a PCR) and the gas uptake capacity of the oil increases. It can be concluded that no bubble remains in the emulsion after PCR since all bubbles are either transported away by the capillary action or small enough to dissolve in the oil. In all cases, no matter if small or large bubbles (largest observed bubbles were up to 10% of the total surface of PCR zone) are transported, the emulsion was not affected. This means that no merging of droplets with each other or unwanted transport of droplets to the air vents was observed. The bubbles were transported with an average speed of at least  $8 \text{ mm s}^{-1}$  (for  $\alpha = 2^\circ$ ). Bubble speed was measured by comparing the location of bubbles in pictures taken at defined time intervals with a stroboscopic setup in the LabDisk Player under rotation. Since the spinning frequency was low (0.5 Hz), time intervals were large (2 s). Therefore, the number can only give a lower limit.

The size and number of pyramids situated in one chamber was varied as well, with up to 3 pyramids in one chamber and pyramid sizes of 4.2 mm to 12.6 mm in length (for detailed measurements compare Table S1†). All of them worked without any problems. Smaller pyramids led to a decrease in overall bubble production. This can be attributed to the higher surface to volume ratio with a much larger oil/gas interface and a smaller distance from the centre of the pyramid to the next interface. As a consequence, for smaller pyramids, diffusion of dissolved gas to the oil/air interface is enhanced. Therefore, the contribution of diffusion as a mean of dissolved gas removal increases compared to convective transport in the form of bubbles.

It should be noted that some evaporation of oil and droplets takes place during PCR. This leads to an increasing concentration of salt in the shrinking droplets. The increase in salt concentration might lead to changes or even breaks in the structure of the probe. A break of the probe leads to an increase of fluorescence which lead to edge effects at the emulsion/air interface. In these regions, droplets cannot be evaluated (<10% of all droplets). The edge effects are illustrated in Fig. 5C). In order to keep these regions small, the emulsion/air interface should be reduced as far as possible. Consequently, the larger pyramids are beneficial. However, care must be taken that distance between sealing foil and bottom of the chamber does not allow the droplets to form a double layer of droplets. The larger the pyramid is, the deeper the chamber gets (at a given angle  $\alpha$ ). As a compromise, a structure with 2 parallel pyramids was chosen (Fig. 5C) and structure 3 in Table S1†) to accommodate a high number of droplets, while keeping edge effects at a comparatively low level.

### Digital droplet PCR

To show the feasibility of the system, a digital droplet PCR targeting the mutation p.Phe508del was performed in the

disk. p.Phe508del is a mutation present in more than 70% of patients suffering from cystic fibrosis.<sup>24</sup> A serial dilution of four 1 : 10-dilutions of target DNA was tested in four different chambers on one disk. The number of positive reactions (*i.e.* of positive droplets) was counted and the number of target molecules initially present in the sample calculated by using Poisson statistics.<sup>25</sup> The results are shown in Fig. 6. The number of expected copies was estimated from qPCR

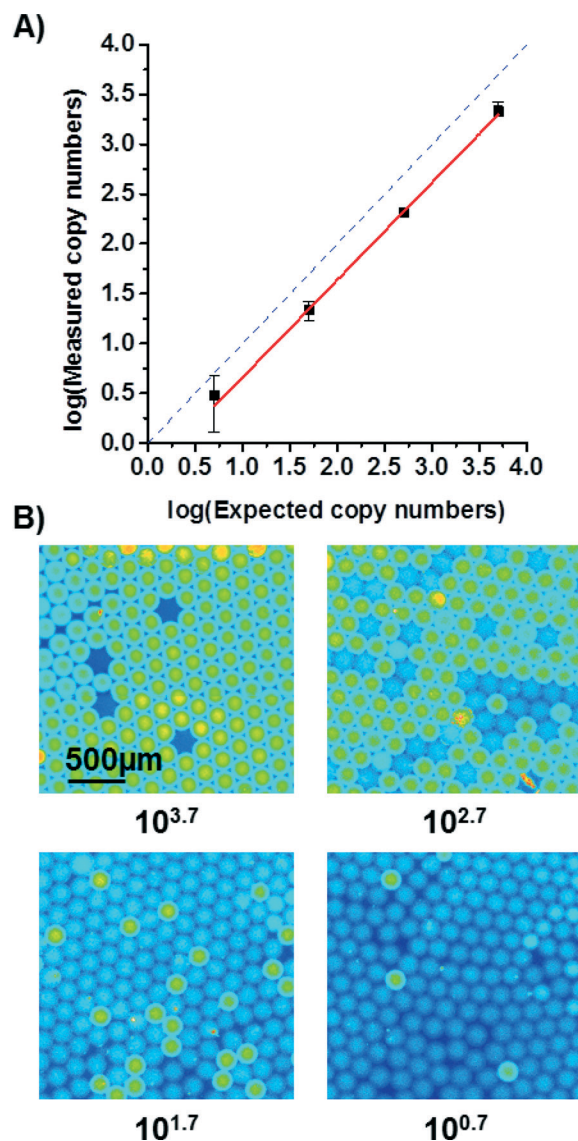


Fig. 6 A) Measured copy numbers corrected by Poisson statistics are depicted on the y-axis. The expected copy numbers were estimated from qPCR measurements (see ESI†) and plotted on the x-axis. The solid red line is a linear fit ( $R^2 > 99.7\%$ ) while the dashed blue line represents the ideal curve. The deviation between them is most likely due to an uncertainty when estimating copy numbers with qPCR and due to some DNA degradation during transport of the studied sample. The errors are  $1\sigma$ -errors including sample and Poisson errors. B) False colour fluorescent images of droplets after ddPCR. The subcaptions of the images give the expected copy numbers as derived from the qPCR measurement. For an expected copy number of  $10^{0.7}$ , an area was chosen to show at least 3 positive droplets. The real droplet count for a larger area was relatively lower.





which requires additional steps, before the ddPCR. For that purpose, upstream sample preparation could be integrated using established centrifugal microfluidic unit operations.<sup>15,27</sup>

We gratefully acknowledge financial support from EU Framework 7 project “ANGELab” #317635. We want to thank Michael Lehnert for helpful discussions. We furthermore want to thank the Lab-on-a-Chip Design & Foundry Service of Hahn-Schickard for manufacturing of disks and the custom made disk holder for the LaVision Bioanalyzer, as well as Oliver Barth and Benjamin Rutschinski for helpful discussions.

In future, we envision that the development of the single chamber droplet digital PCR process chain will facilitate the development of fully integrated and highly automated sample-to-digital-answer systems. Reagents could be pre-stored lyophilized or in liquid form in stick packs<sup>26</sup> on the disposable disk. For an application in a clinical setting, the DNA would need to be extracted from the sample matrix

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