TUTORIAL REVIEW

Check for updates

Electrochemical hydrogen production: sustainable hydrogen economy

Samina Aslam,[a] Sadia Rani, [ID] [a] Kiran Lal,[a] Miraj Fatima,[a] Tomas Hardwick,[b] Bahareh Shirinfar[c] and Nisar Ahmed [ID] *[b]

The development of sustainable energy technologies has received considerable attention to meet increasing global energy demands and to realise organisational goals (*e.g.*, United Nations, the Paris Agreement) of carbon neutrality. Hydrogen is a promising alternative energy source to replace fossil fuels and mitigate corresponding environmental issues. An aspiring method to produce hydrogen is to direct energy from intermittent renewable energy sources for water electrolysis. However, a major obstacle to practically achieving hydrogen storage is the future investment costs of water electrolysis due to the energy-intensive nature of the reaction. In this study, we present an overview of current research interests that produce hydrogen, including different types of water electrolysis such as high-temperature, low-temperature, nuclear-driven, solar-powered, wind-powered, and grid-connected water electrolysis. Electrolysis using organic fuels and hydrogen production as a by-product of various electrolytic methods are also briefly discussed. At the end, we demonstrate the economics, sustainability, and challenges of sustainable hydrogen production reporting since 2005 onwards.

[a]Department of Chemistry, The Women University Multan, Multan 60000, Pakistan
[b]School of Chemistry, Cardiff University, UK. E-mail: nisarhej@gmail.com, AhmedN14@cardiff.ac.uk
[c]Department of Chemistry, University of Bath, BA2 7AY Bath, UK

Nisar Ahmed

Nisar Ahmed obtained his PhD in organic chemistry with a Brain Korea BK21 fellowship from POSTECH, Korea. Then, he moved to the University of Zurich, Switzerland, for a post-doctoral stay with an Innovative Novartis Fellowship. Subsequently, he joined the University of Bristol as a senior research associate. Furthermore, from 2017 he started his independent academic career at the School of Chemistry, Cardiff University, United Kingdom. His fields of research include synthesis of value-added chemicals, fine chemicals, and pharmaceuticals with special focus on inert bonds' activations & cleavage using modern synthetic tools such as electrochemistry, photochemistry, sonochemistry, flow technology, digital & automation chemistry, and reaction engineering.

1. Introduction

It is well known that the continued burning of fossil fuels releases greenhouse gases into the atmosphere, which poses a major threat to the environment and leads to changes in climate.[1] Additionally, the infrastructure of a country that is dependent on the importation of foreign fuel sources will display vulnerability as a result of the increase in conventional fuel costs that have been forced by the rising energy demand. Future energy sources would ideally be carbon-free and renewable in order to combat climate change on a long-term basis and reduce our reliance on foreign oil.[2,3]

Hydrogen could be employed in future energy frameworks since it is a carbon-free alternative energy source with several benefits, such as environmental friendliness and high energy density. Clean and sustainable energy is produced from various energy sources all over the globe using hydrogen derived from renewable resources.[4]

H_2 has the highest specific energy of any fuel now in use, at 33.31 kW h kg^{-1}. By comparison, gasoline has a specific energy of 12.89 kW h kg^{-1} and lithium-ion batteries have a specific energy of 0.1–0.2 kW h kg^{-1}.[5,6] Due to the high energy density, 5 kg of H_2 is sufficient to propel a typical passenger vehicle 500 km in less than 5 minutes.[7] This is the key advantage over battery-powered cars, which require heavier and larger batteries to travel the same distance and require more refuelling intervals.[8]

To date there are a variety of sustainable and high-purity processes for electrolysis-based hydrogen production. There is much interest in, and funding for, this field of study, as seen by the increase in the number of scientific publications on the subject of hydrogen synthesis by the electrochemical splitting of water.[9] In addition to being manufactured as a fuel for transportation, hydrogen can also be produced as a feedstock for the chemical industry and as a solution to address the intermittent nature of renewable energy sources such as wind and solar energy. The existence of economically viable methods for sustainable hydrogen production is essential in making this vision a reality. Today, however, with around 96% of the world's hydrogen generation (mostly for ammonia production) relying on the steam reforming of fossil fuels, this is not the case.[10] Around 60 million tonnes of hydrogen are produced each year on a global scale.[11] Nearly half of this is created by the steam reforming of natural gas, 29% through the reforming of oil, and 17% through the gasification of coal, all of which emit significant amounts of greenhouse gases. Additionally, water electrolysis produces around 4% of the hydrogen.[12] At present, annual hydrogen consumption growth is 6%.[11]

There are numerous ways to make hydrogen which have traditionally relied upon electro- and thermochemical processes, in addition to biochemical methods that occur *via* fermentation, biophotolysis, or biological metabolic pathways. Electrochemistry involves the splitting of water into molecular hydrogen and oxygen, primarily through water electrolysis. Through reforming, pyrolysis, and gasification reactions of biomass and fossil fuels, hydrogen is produced thermochemically (carbonaceous fuels).[13] Notwithstanding this, thermochemical processes, photobiological water splitting, and biomass fermentation are a few of the potential methodologies that are being researched in order to produce hydrogen sustainably.[14] The need for sustainable energy sources is becoming increasingly important due to the rising global demand for energy and the need to reduce carbon emissions and ecological pollution. The current favourable (lower cost) generation of hydrogen from fossil fuels, in comparison with alternative technologies based on renewables, is the biggest obstacle to the introduction of renewable routes to hydrogen production. Other processing techniques, such as the gasification of biomass or the splitting of water using external energy sources like sunlight, have the potential to utilise more sustainable methods or feedstocks, despite the majority of hydrogen generation coming from unsustainable routes using carbon-based fuels. In light of this current less-than-optimal nature of hydrogen generation, more efficient alternative routes must be developed in conjunction with other energy supply channels. Many renewable-based technologies have efficiency restrictions, thus in practice a variety of technologies will need to be made commercially viable in order to meet the demand for a significant increase in sustainable hydrogen generation.[15] When compared with the usage of fossil fuels and biofuels, hydrogen offers some advantages that could be deemed favorable.[16] Table 1 demonstrates a brief summary of principles of various high-performance hydrogen production methods.

In this article, we give an overview of the several types of water electrolysis being researched today, including solar-powered, grid-connected, high-temperature, low-temperature, nuclear-assisted and wind-powered water electrolysis. Hydrogen production as a by-product of several electrolytic processes and electrolysis utilizing organic fuels are also slightly explored. We conclude by highlighting the cost, sustainability, and difficulties of sustainable hydrogen production.

2. Electrochemical production of hydrogen

As the most prevalent element in the universe, hydrogen is easily accessible in the form of biomass from plants, water, hydrocarbons, and other organic substances. Hydrogen is currently produced more for use as a chemical or reducing agent than as a fuel. As an energy carrier or energy vector rather than an energy source, hydrogen produced from renewable resources can offer an energy pathway that is both clean and sustainable.[18] Fig. 1 gives the recognised primary energy sources and their routes to hydrogen production.[10]

To fulfil its role in the future, hydrogen production must meet three key criteria:

i. It needs to follow sustainable routes;

ii. It ought to make use of plentiful and renewable feedstocks;

iii. High-purity hydrogen must be produced, because contaminants are hazardous in most fuel cell and other applications.

Hydrogen may only be regarded as sustainable if both the process's feedstock and the energy source for its electrical input are renewable.[28] The options for producing hydrogen sustainably are elaborated in this study. Fuel cells that use hydrogen to produce energy can be employed with ease. Additionally, hydrogen has a high energy yield of 122 kJ g^{-1}, which is 2.75 times higher than fuels derived from hydrocarbons.[29] As a technical and policy problem, the use of hydrogen as a fuel for mobile and stationary applications is getting a lot of positive attention.[30] The estimated total annual hydrogen consumption for the entire planet is 400–500 billion Nm^3.[31] The current use of hydrogen accounts for 3% of global energy consumption, with a growth rate of 5–10% each year.[32] There are numerous ways to manufacture hydrogen, and Table 2 lists them along with their benefits and drawbacks for producing hydrogen energy.[21,24–27] Electricity is used in electrolysis to divide water molecules into hydrogen and oxygen, and the price of electricity is a major factor in the cost of producing H$_2$ energy.[21,33,34]

In Table 3, the environmental effects of the various electrolysis procedures are described together with the current and projected costs of producing hydrogen through electrolysis utilising various electricity sources.[34,35] Table 3 shows that the most dependable and economically efficient way to currently produce hydrogen is through electrolysis utilising hydropower,

Table 1 Summary of principles of Green Hydrogen production methods[17]

Hydrogen production methods		Material resources	Process driving energy	Brief description
Thermolysis		Water	Thermal energy	Steam is heated to over 2500 K, where water molecules thermally disintegrate
Thermochemical processes	Gasification	Biomass		Syngas is produced from biomass, and H_2 is removed
	Water splitting	Water		Chemical reactions are carried out, whether or not they involve redox reactions
	H_2S splitting	H_2S		Cyclical processes to break the hydrogen sulfide molecule
	Reforming	Biofuels		Conversion of liquid biofuels into hydrogen
Thermocatalysis	Biomass conversion	Biomass		Conversion of biomass to hydrogen by thermocatalysis
	H_2S cracking	H_2S		Thermo-catalytic H_2S is broken down from seawater or other industrial processes
Coal gasification		Water	Electrical + thermal	Syngas is created from coal, and subsequently H_2 is removed and CO_2 is separated and sequestered (using electricity)
Fossil fuels reforming		Fossil fuels		With CO_2 capture and isolation, fossil hydrocarbons are transformed to H_2 (electricity used)
High-temperature electrolysis		Water		Splits water in solid oxide electrolyte cells using both an electrical and thermal source
Thermo-catalytic fossil fuels cracking		Fossil fuels		Fossil hydrocarbons are split into H_2 and CO_2 *via* a thermo-catalytic process, while CO_2 is separated or sequestered to make the method green
Hybrid thermochemical cycles		Water		Utilize thermal and electrical energy to cycle through chemical reactions, which will ultimately lead to the splitting of water
Plasma arc decomposition		Natural gas	Electrical energy	Hydrogen and carbon soot are formed when cleaned natural gas (methane) is pushed through an electrically generated plasma arc
Electrolysis		Water		An electrochemical process that generates a direct current leads water to decompose into oxygen and hydrogen gas
Dark fermentation		Biomass	Biochemical energy	Without light, anaerobic fermentation
Thermophilic digestion		Biomass	Biochemical + thermal	Uses thermal energy helped by biomass digestion to heat at low-grade temperature
Photoelectro-chemical method		Water	Photonic energy	The water electrolysis process is powered by photovoltaic electricity produced by a hybrid cell
PV-electrolysis		Water		Electricity from solar panels powers the electrolyzer
Bio-photolysis		Water		Utilizing cyanobacterial-based biological systems, hydrogen is produced under controlled conditions
Photocatalysis		Water		Hydrogen is produced from water using sophisticated homogeneous catalysts or molecules with photoinitiated electron collecting
Photofermentation		Biomass	Photonic + biochemical	By exposing the fermentation process to light, it is facilitated
Bio-photolysis		Biomass, water		Uses bacteria and other microorganisms to photogenerate hydrogen
Artificial photosynthesis		Biomass, water		To simulate photosynthesis and produce H_2, chemically modified molecules and related systems are used
Photoelectrolysis		Water	Electrical + photonic	Photoelectrodes and external source of electricity are required

Fig. 1 The primary energy sources considered and their routes to hydrogen. Reproduced from ref. 10 with permission from Elsevier, copyright 2005.

although in the future nuclear power may be utilised. Despite being a viable replacement for fossil fuels, hydrogen still faces several difficulties. Due to hydrogen's inability to liquefy at room temperature, these difficulties mostly relate to the high cost of production and the difficulty in storage.[16,35,36]

Using a strategy based on distinct colours, hydrogen-generating technologies are increasingly being stated.[37–39] Grey (or brown/black) hydrogen is created by fossil fuels (mostly coal and natural gas), which results in the release of carbon dioxide.[20] Blue hydrogen prevents the majority of the process's greenhouse gas (GHG) emissions by combining grey hydrogen and carbon capture and storage (CCS). Natural gas is converted into blue hydrogen by the steam reforming process. In this process, natural gas is broken down into hydrogen (H_2) and carbon dioxide (CO_2), with some of the generated CO_2 unable to be captured, while the remaining CO_2 is captured (85%–95%) and stored underground using commercial CCS tech-

Table 2 Hydrogen production from various sources and related mechanisms, efficiencies, costs as well as advantages/disadvantages[21,24–27]

Source	Mechanism	Benefits	Drawbacks	Hydrogen cost ($ per kg)	Efficiency (%)	Ref.
Water electrolysis	$2H_2O \rightarrow 2H_2 + O_2$	Proven technology Zero emission Only by-product is O_2 Existing infrastructure already developed	Storage problems Applicable only to special purposes Transportation issues	10–23	40–60	19 and 20
Hydrogen from biomass	Biomass + H_2O + Air $\rightarrow H_2 + CO_2$	Dependent on renewable sources Other useful products can be obtained such as adhesives, polymers, fertilizers Less expensive	Inefficient when compared with fossil fuels Not entirely a clean source because of methane gas produced as a by-product Potential contribution to deforestation	2.05	35–50	21
Steam methane reforming (SMR)	Biogas + steam $\rightarrow H_2$ + CO_2	Existing infrastructure. Most developed of these technologies	Unstable supply. Geopolitical tension. Pollution (CO, CO_2)	2.27	74–85	20
Nuclear energy	C_1H_2 (synthetic crude) + $2H_2O$ + nuclear heat $\rightarrow CO_2 + 3H_2$	Less carbon production	Disposal of radioactive waste Mining and processing of uranium Potential for accidents	4–7	45–50	22
Gasification of coal	$C_2H_4 + O_2 \rightarrow 2CO + 2H_2$	Less CO_2 emitted than conventional fossil fuel burning Syngas can be easily collected and used to produce carbon neutral fuels	Along with H_2, the production of heavy oils, petroleum and coke can occur Large amounts of CO_2 are still produced Energy and water intensive	1.48	60–75	22 and 23

Table 3 Comparison of various electricity sources for water electrolysis[34,35]

Electricity source	Present cost ($ per kg)	Future cost ($ per kg)	CO_2 emission (kg CO_2 per kg H_2)	Efficiency (%)
Hydro	1.4	3–4	0	25
Wind	7–11	3–4	0	21
Nuclear	4.15–7	2.45–2.63	0	45
Solar	10–30	3–4	0	20

niques. Leakage can still have a harmful impact on ecology and the climate, and the long-term effects of storage are undetermined.[40] Solid carbon in the form of carbon nanotubes or filamentous carbon is a by-product of the pyrolysis of methane to produce turquoise hydrogen.[41] Green hydrogen is manufactured by electrolysers powered by renewable electricity. It can also be generated *via* alternative bioenergy-based processes like biomethane reforming or solid biomass gasification.[42] Through atomic current electrolysis, purple hydrogen can be produced. Incorporating a hydrogen-producing facility could lessen the need to shut down nuclear power facilities.[43] The term "yellow hydrogen" is occasionally used in the literature to refer to purple/pink hydrogen. However, the more typical definition of yellow hydrogen for grid-powered electrolysis is employed. Finally, white hydrogen is hydrogen from its natural form or as a by-product of industrial processes.[37]

Since its invention in the late 1920s, electrolysis has been used to produce pure hydrogen commercially. In this case, water is separated into hydrogen and oxygen using external electricity. By the 1960s industrialised hydrogen production had switched to options fuelled by fossil fuels, which have continued to be the primary source of energy and raw materials for the manufacture of hydrogen.[11] Only 4% of the total hydrogen supply in the world is now produced by electrolysis.[44] Numerous hydrogen production techniques, including electrolysis, have been thoroughly researched from an economic, environmental, technological, and social standpoint in the literature.[9,27,42,45–58]

The electrolyser is the fundamental part of an electrolysis process for producing hydrogen (can be connected either in parallel or in series). The by-product gases, typically hydrogen and oxygen, are often cooled and compressed before being stored for multiple end uses. Since oxygen is typically not a desired result in electrolysis procedures, it is usually immediately released into the environment rather than entering storage. Additionally, the water supply to the electrolyser needs to be adequately treated to remove contaminants and, by extension, any possibility for unintended side reactions. Moreover, due to the absence of moving parts in most electrolysers, routine maintenance is not necessary. The silent operation and modular design of electrolysers make them suitable for distributing an energy supply to residential, commercial, and industrial units. To reduce the costs of electrolyser manufacture, distribution, and installation, considerable technological and material advancements are needed to coincide with efficient function under ambient conditions.[13] Different technologies have been compared for their energy efficacy in producing hydrogen (Fig. 2).[19]

Fig. 2 Different methods of hydrogen production. Reproduced from ref. 19 with permission from Elsevier, copyright 2022.

Currently, electrolysis creates pure hydrogen for use in the food, pharmaceutical, electronics, and other industries[59–62] and is being studied as a potential technique to create hydrogen for use as a fuel.[63] Potentially, electrolysis can offer a clean and sustainable supply of chemical energy when combined with a renewable energy source. In other cases, electrolysis can benefit from off-peak energy to lower the cost of electricity. Two commercial electrolyser technologies are alkaline and solid polymer electrolysers, while alkaline polymer, solid oxide, and molten carbonate are three technologies that are currently being researched and developed.[64]

Among other operating factors, electrolysers can be categorised based on their operating temperature. The most common systems use polymer electrolyte membrane (PEM) and alkaline technologies in low-temperature electrolysers, sometimes referred to as "water electrolysers", while molten carbonate electrolysis (MCE) cells and solid oxide electrolysis (SOE) cells are examples of high-temperature electrolysers, also referred to as "steam electrolysers".[65] Due to two primary factors, an increase in the electrolysis temperature is of tremendous interest. Firstly, this is because high-temperature technologies often require less energy than low-temperature ones. In fact, a portion of the electrical energy required to break down the water molecule can be replaced by heat as the temperature rises. Secondly, because of their internal fuel-processing capability, which is improved by higher operating temperatures and the presence of catalysts, they can process hydrocarbon fuels without experiencing severe degradation difficulties. Since losses, including ohmic losses, are reduced at higher temperatures.[66] Hydrogen may be produced with very low specific electrical consumption of 3–4 kW h Nm^{-3} by high-efficiency upgrading of hydrocarbon streams.[67]

2.1. Electrocatalysts for hydrogen production

Electrocatalysts are required for electrochemical energy conversion and storage techniques in order to create environmentally responsible and long-lasting energy systems. Systems that use electrochemistry for energy conversion and storage often employ a wide variety of electrochemical processes; they generate less carbon dioxide and have high energy densities. The effectiveness and affordability of the electrocatalyst are crucial for its broad application. The use of electrocatalysts increases the electrolysis system's energy efficiency. We selected a few examples to highlight many sorts of electrocatalysts from the many electrocatalyst examples that are accessible. Many compounds based on transition metals have proved to be effective electrocatalysts.[9,27,45,55,57,68–95]

Due to their powerful electrocatalytic activity, transition metal compounds (such as carbide, oxide, sulfide, phosphide, selenide, and others) are among the many electrocatalyst candidates being researched. The workings of different electrocatalysts differ. Because they facilitate the conversion of reaction intermediates and lower resistance, electrocatalysts are essential for increasing reaction speeds. Noble metals are the most complex electrocatalysts for OER (Ir/Ru oxide), HER (Pt), and ORR (Pt), but due to their high cost and scarcity, they are not frequently utilized in industry. Even at relatively low platinum loadings, a number of commercial electrodes constructed from Pt(Mo$_2$C)-produced catalysts exhibit significant catalytic activity for the hydrogen evolution reaction (HER) in 0.5 M sulfuric acid solution.[73] Commercial electrodes made of Ni and Ti mesh function well, offer superior cathode materials, and cost less than electrodes made of Pt.[74] Other materials offer the best electrode materials for general application since they are less expensive than Pt-based electrodes and have good performance. Of course, the cost of the electrodes must come next. They can be made of costly and affordable materials, corrosion-resistant metals, and alloys, including noble metals.

The components used for manufacturing the electrodes used in water in general, but particularly in seawater electrolysis, must adhere to precise specifications. Both the most extensively researched hydrogen evolution reaction (HER) and the less well-known oxygen evolution reaction (OER) must occur at the electrodes in seawater, hence the electrodes must have electrocatalytic qualities. On the electrolysis cell, this will lessen polarizations and explicit voltage losses. The findings of investigations on appropriate seawater electrocatalysts for HER recently employed in the electrolysis process are shown in Table 4.

Table 4 A few examples of electrocatalysts for hydrogen production[9]

Electrocatalysts	Stability, h	Ref.
Ni–N$_3$	14	72
Co–Se	12	96
CoP–WP/rGO	30	97
FeOOH/β-Ni–Co–OH	378	98
NiMoS	100	75
MFC-N,O doped C	76	86
Co/GCFs	10–20	78
MNiNS, Ni/Pt–C, Ni/Ir–C	12	99
FeCo–Ni$_2$P, MIL–FeCoNi	100	85
Pt–NiFe PBA	12	77
NiCo@C	60–140	100
MXene, carbide	225	94
Ni$_2$P–FeP	90	81

3. Water electrolysis

This approach makes reference to the earliest technique for creating hydrogen, which dates to the 19th century.[101] Although abundant, renewable energy is sometimes unreliable and intermittent. The need to store energy for times when the sun is not beaming and the wind is not blowing will increase as our reliance on renewable energy increases.[102] Utilising renewable energy (as and when it becomes available) to split water into hydrogen and oxygen in accordance with eqn (1) is one of the more interesting methods for storing this energy.[103]

A carbon-neutral fuel production and consumption cycle can be created by storing the hydrogen created by the reaction in eqn (1) and then oxidising it (by burning in air or in a fuel cell) to release energy and regenerate water. The overall reaction is shown below:

$$H_2O + electricity \rightarrow H_2 + \frac{1}{2}O_2 \qquad (1)$$

At room temperature and pressure, the reaction in eqn (1) is a thermodynamically upstream process and needs an energy input of 286 kJ mol^{-1}. This conversion is thought to be best accomplished *via* electrochemical methods, which just need inputs of water and voltage to make hydrogen.[104] According to eqn (2), water is oxidised at the anode when the environment is acidic.

$$2H_2O \rightarrow O_2 + 4e^- + 4H^+ \qquad (2)$$

These protons cross into the cathode compartment (to complete the electrochemical circuit), and the electrons move through the external circuit. The hydrogen evolution reaction (HER), which combines the protons and electrons at the cathode, follows:

$$4e^- + 4H^+ \rightarrow 2H_2 \qquad (3)$$

The minimal theoretical voltage needed to drive the OER and HER (to split water) is 1.23 V at ambient temperature. The reactions must have additional energy, or activation energy, in order to occur at noteworthy rates. The amount of activation energy required increases with the rate of water splitting (measured as charge flowing per unit area of electrode per unit time, or "current density"). The necessity for potential bias above the 1.23 V minimum results from the increased energy. The finest electrocatalysts for acidic environments (where protons serve as the electrochemical charge carriers, as shown in the figure below) are precious metals (platinum at the cathode and IrO_2 or RuO_2 at the anode). First-row transition metals (and their alloys) and oxides provide effective HER and OER catalysts, respectively, when the HER and OER proceed under the basic conditions stated in the equations below.[104]

$$\text{Basic HER}: \ 4H_2O + 4e^- \rightarrow 2H_2 + 4OH^- \qquad (4)$$

$$\text{Basic OER}: \ 4OH^- \rightarrow O_2 + 2H_2O + 4e^- \qquad (5)$$

The oxygen evolution reaction (OER) and hydrogen evolution reaction (HER) are the two main processes that make up overall water electrolysis. Both of these reactions require effective electrocatalysts[105-107] to speed up their slow kinetics for high energy efficiency.[104,108-110] Transition metal-based electrocatalysts play an important role in clean energy.[111,112] The development of non-precious OER/HER electrocatalysts as substitutes for Pt/C and Ir/Ru-based catalysts has made significant progress in recent years.[113,114] Fig. 3 depicts a typical electrolysis cell for splitting water.

About 1×10^{-6} S m^{-1} is the electrical conductivity of pure water, making it a poor conductor of electric currents. Under these conditions, hydrogen and oxygen production would require very high voltages. To make water more conductive, salts, acids, or bases are typically added. Acidic and alkaline solutions have higher electrical conductivities than neutral solutions because hydrogen ions (H^+) and hydroxyl ions (HO^-) have a greater degree of mobility in these environments. Despite the fact that acidic solutions are more conductive than alkaline solutions, the corrosion of steel-based metallic components leads to a rise in the material consumption of the electrodes, which results in process losses. Due to the formation of carbonates under the effect of carbon dioxide in the air, which results in a 75% reduction in initial conductivity, the electrical conductivity of alkaline electrolytes diminishes with time.[9]

As a sustainable approach, water electrolysis technology has been developed to produce high-purity hydrogen, called green hydrogen. A voltage is applied to the cells during water electrolysis, and a DC current travels between two electrodes while in contact with an ionic conducting medium, producing hydrogen and oxygen from the breakdown of water (Fig. 4).[20]

The best way for splitting water is electrolysis, which is a robust and well-understood process.[20] However, because of how endothermic the process is, electricity is used to supply the needed energy input.[115] In practice, the electrolysis of water achieves an energetic efficiency of 50–70% (chemical energy obtained per electrical energy provided).[4]

Since high-purity water supplies are necessary for all commercially available water electrolysers, a low system efficiency of 70% and high cost limit the applicability of water electrolysis.[116-118] In many places, especially in hot, arid locations, freshwater has historically been a rare resource.

Fig. 3 Electrolysis cell for splitting water. Reproduced from ref. 104 with permission from Nature Publishing Group UK London, copyright 2017.

Fig. 4 Flow diagram of the water electrolysis process. Reproduced from ref. 20 with permission from Elsevier, copyright 2017.

Table 5 Main renewable sources of energy that could be sustainably used for seawater electrolysis[9]

Type of renewable source	Ref.
Wave energy	122
Geothermal energy	122, 124 and 142
Wind energy	122, 124, 125, 128, 132, 135, 137 and 139
Hybrid renewable energy	121, 124, 126, 130 and 134–142
Solar energy	9, 59, 75, 121, 123–125, 127, 129–132, 134 and 136–139
Microhydropower	139

Equipment for water purification and desalination is required while building an electrolytic water system in order to pre-treat saline and low-grade water.[119,120] The flow of input-fluid and outflow-air streams, gas regulators, and thermal management devices are all complicated setups that distinguish practical electrolysers from basic laboratory systems. Even before factoring in related investments in transportation and maintenance, the deployment of more water purification devices will eventually come at a prohibitive cost. Direct use of saline seawater in water electrolysis systems can be a feasible and practical strategy for coastal dry zones and offshore large-scale hydrogen outputs when cost reduction is taken into account. The economic efficiency of purification/desalination can be significantly increased by removing pre-treatment systems. For the electrolysis of water and seawater to produce hydrogen, solar energy, geothermal energy, wind, micro-hydropower, and wave energy are all appropriate sources of energy (Fig. 5).

The market for hybrid renewable energy systems has grown significantly as a result of the year-round fluctuations in the availability of renewable energy sources like solar, wind, small hydro, geothermal, and ocean power. Numerous studies on the architecture, operation, dependability, and optimisation of hybrid renewable energy have been published recently in response to the rise in demand. The key renewable energy sources listed in Table 5 can be used to electrolyse seawater in a sustainable manner.[49,75,119–142]

Alkaline water electrolysis, proton exchange membrane (PEM) water electrolysis, and solid oxide water electrolysis (SOEC) can produce hydrogen when different electrolytes are used.[143] Key features of these techniques are described in Table 6.

3.1. High-temperature water electrolysis

This type of water electrolysis consists of following types:

3.1.1. Molten carbonate electrolysis (MCE). MCE and SOE are the most effective yet the least developed. Numerous researchers have examined electrolysis in molten carbonate salts, primarily concentrating on the electrolytic reduction of carbonate melts or carbon dioxide into solid carbon or gaseous carbon monoxide.[145–155] The molten carbonate electrolyte suspended in a porous and chemically inert ceramic matrix underlies the molten carbon fuel cell (MCFC) technology, from which MCEs are formed. The electrolyser's working principle is the opposite of that of the fuel cells, and the difference between the MCE cells and MCFC is in the direction of the redox reaction. The materials used to assemble the components of the MCE cells are the same as those used to assemble the MCFCs, with the exception that the cathode consists of porous nickel alloyed with Cr and/or Al, and the anode is of porous lithiated nickel oxide (NiO). The lithium, potassium, and/or sodium carbonate (Li_2CO_3, K_2CO_3, and Na_2CO_3) combination is used as electrolyte. Operating with a liquid carbonate electrolyte is possible when the temperature is between 620 and 680 °C. Only a few MCE-specific research studies are reported in the literature. However, despite being at a highly advanced level of research, MCFC technology is the only one of the fuel cell technologies to have produced power plants with several megawatts of output. The functional layout of a Molten Carbonate Electrolyser Cell (MCEC) is shown in Fig. 6.[156] Hydrogen electrode reactions are:

$$H_2O + CO_2 + 2e^- \rightarrow CO_3{}^{2-} + H_2 \tag{6}$$

$$2CO_2 + 2e^- \rightarrow CO_3{}^{2-} + CO \tag{7}$$

In reaction (6) steam is electrolysed in an MCE, while in reaction (7) carbon dioxide undergoes an electrochemical reaction to form carbon monoxide. The latter is slower and is not predicted to happen in the hydrogen electrode, according to literature reports.[157] It is anticipated that carbon monoxide will be produced through an equilibrium shift because of the

Fig. 5 Renewable sources of energy for hydrogen production from seawater electrolysis. Reproduced from ref. 9 with permission from MDPI, copyright 2022.

Table 6　Technical features of common water electrolysis methods[144]

Features	Alkaline	AEM	PEM	Solid oxide
Anode reaction	$2OH^- \rightarrow H_2O + \frac{1}{2}O_2 + 2e^-$	$2OH^- \rightarrow H_2O + \frac{1}{2}O_2 + 2e^-$	$H_2O \rightarrow 2H^+ + \frac{1}{2}O_2 + 2e^-$	$O^{2-} \rightarrow \frac{1}{2}O_2 + 2e^-$
Cathode reaction	$2H_2O + 2e^- \rightarrow H_2 + 2OH^-$	$2H_2O + 2e^- \rightarrow H_2 + 2OH^-$	$2H^+ + 2e^- \rightarrow H_2$	$H_2O + 2e^- \rightarrow H_2 + O^{2-}$
Overall cell	$H_2O \rightarrow H_2 + \frac{1}{2}O_2$	$H_2O \rightarrow H_2 + \frac{1}{2}O_2$	$H_2O \rightarrow H_2 + \frac{1}{2}O_2$	$H_2O \rightarrow H_2 + \frac{1}{2}O_2$
Operating temperature	70–90 °C	60–40 °C	50–80 °C	700–850 °C
Efficiency	50–78%	57–59%	50–83%	89% (laboratory)
Electrolyte	Electrolyte KOH/NaOH (5 M)	DVB polymer support with 1 M KOH/NaOH	Solid polymer electrolyte (PFSA)	Yttria-stabilized Zirconia (YSZ)
Electrode/catalyst (hydrogen side)	Nickel-coated perforated stainless steel	Nickel	Iridium oxide	Ni/YSZ
Electrode/catalyst (oxygen side)	Nickel-coated perforated stainless steel	Nickel or nickel alloys (NiFeCo)	Platinum carbon	Perovskites (LSCF, LSM) (La,Sr,Co,FE) (La,Sr,Mn)
Cell pressure	<30 bar	<35 bar	<70 bar	1 bar
Separator	Asbestos/Zirfon/Ni	Fumatech	Nafion®	Solid electrolyte YSZ
Electrode area	10 000–30 000 cm^2	<300 cm^2	1500 cm^2	200 cm^2
Lifetime (stack)	60 000 h	>30 000 h	50 000–80 000 h	20 000 h
Gas diffusion layer	Nickel mesh	Nickel foam/carbon cloth	Titanium mesh/carbon cloth	Nickel mesh/foam
Capital costs (stack) minimum 1 MW	US $270 per kW	Unknown	US $400 per kW	>US $2000 per kW
Capital costs (stack) minimum 10 MW	US $500–1000 per kW	Unknown	US $700–1400 per kW	Unknown
Bipolar plates	Stainless steel/nickel-coated stainless steel	Stainless steel/nickel-coated stainless steel	Platinum/gold-coated titanium or titanium	Cobalt-coated stainless steel
H$_2$ purity	99.5–99.9998%	99.9–99.9999%	99.9–99.9999%	99.9%
Development status	Mature	R & D	Commercialised	R&D
Nominal current density	0.2–0.8 A cm^{-2}	0.2–2 A cm^{-2}	1–2 A cm^{-2}	0.3–1 A cm^{-2}
Voltage range (limits)	1.4–3 V	1.4–2.0 V	1.4–2.5 V	1.0–1.5 V

Fig. 6 Working principle of a molten carbonate electrolysis (MCE) cell. Reproduced from ref. 156 with permission from Elsevier, copyright 2018.

operating temperature and the presence of nickel catalyst in the fuel electrode. Since steam and carbon dioxide are the only accessible reactants in this situation, the reaction is known as the reverse water–gas shift. The local condition indicates that all species are present and the reaction has reached thermodynamic equilibrium. The following is the reaction:

$$CO_2 + H_2 \leftrightarrow H_2O + CO \qquad (8)$$

Theoretically, both electrochemical (7) and chemical (8) reactions can result in the production of carbon monoxide. The interaction of reactions (7) and (8) results in reaction (6), which combines the reactions of carbon dioxide and steam. The following describes an oxygen electrode reaction:

$$CO_3^{2-} \rightarrow CO_2 + \frac{1}{2}O_2 + 2e^- \qquad (9)$$

As an intake reactant, oxygen gas is not needed. Carbon dioxide and oxygen are produced *via* the OER. The entire reaction between the two electrodes is the breakdown of water into hydrogen and oxygen:

$$H_2O \rightarrow H_2 + \frac{1}{2}O_2 \qquad (10)$$

Carbon dioxide moves from the hydrogen electrode to the oxygen electrode during the procedure. This indicates that both CO_2 and steam must be supplied to the electrode. A MCEC differs from a conventional electrolyser in that carbon dioxide is supplied to the hydrogen electrode and produced at the oxygen electrode. The hydrogen electrode contains carbon dioxide, which causes a chemical or electrochemical reaction that also produces carbon monoxide.[158]

In addition to transporting the carbonate ions between the electrodes and separating the fuel and oxidant gases, the electrolyte is retained in a porous matrix, typically constructed of γ-LiAlO$_2$.[67] However, because carbon dioxide is involved and the product stream from the electrolyser contains both hydrogen and carbon dioxide, there is a significant practical issue with the operation of an MCE cell, necessitating gas separation

for the production of pure hydrogen and recycling of carbon dioxide to the cell. In order to produce syngas (a combination of CO and H_2) through co-electrolysis of water and carbon dioxide, the MCE cell is probably a more advantageous alternative.[64]

One of the primary objectives of present scientific research is the investigation of novel technical methods to reduce CO_2 emission output into the atmosphere. The performance of MCECs for both H_2 production and CO_2 capture has been examined. Due to the combination of the steam reforming reaction, which can be supported inside the cell, and subsequent electrolysis, MCECs can work with CH_4 and H_2O feeding, enabling the syngas or hydrogen production. In this case, MCECs can function as a single, independent system for the generation of hydrogen as well as being retrofitted with reformer units to extend the scope of reforming, allowing for higher CH_4 conversion, production of H_2, and simultaneous storage of CO_2.[159]

3.1.2. Solid oxide electrolysis (SOE). Donitz and Erdle were the first to publish findings from a solid oxide electrolyser cell (SOEC), used in the HotElly project at Dornier System GmbH in the 1980s. The SOECs incorporated a supported tubular electrolyte.[160]

Recently, SOE cells have proved highly efficient for conversion of water and carbon dioxide to produce carbon fuel and hydrogen, with a high temperature necessary for their conversion and storage.[19] SOEs are divided into two groups in the literature: H^+ SOE and O^{2-} SOE. O^{2-} SOE is currently in the demonstration phase, whereas H^+ SOE is at the lab scale.[161] A dense electrolyte serves as the ionic conductor in SOECs, such as the oxygen ion-conducting SOEC (O-SOEC) and the proton-conducting SOEC (H-SOEC), in which reaction gases such as H_2O or CO_2 are fed into the cathode (or anode) and oxide ions (or protons) are conducted across the dense electrolyte to the cathode (or anode). The evolution of oxygen at the anode enables the cathode to produce fuel gases.[162] This method is very useful for obtaining these gases but requires a high production cost (80% of the energy comes from electricity).[163] Some technical issues are also involved because of the high temperature, such as leakage of gas-tight components, the requirement of tough materials and its limited application. Moreover, this method has high operational and maintenance costs. Different technological approaches may enhance durability and electro-catalytic performance under low temperature. In renewable energy conversion and storage systems SOE cells have been proved to be a useful and successful technology.[162] The working principle of an SOE cell is shown in Fig. 7.[162]

The endothermic reaction occurs in the SOE cell, while the oxidation reaction occurs at the anode, where oxygen ions move through the electrolyte.

$$\text{Anode}: \ O^{2-} \rightarrow \frac{1}{2}O_2 + 2e^- \tag{11}$$

$$\text{Cathode}: \ H_2O + 2e^- \rightarrow O^{2-} + H_2 \tag{12}$$

Fig. 7 Schematic of SOEC (O/H-SOEC). Red arrows represent the O-SOEC, and blue arrows represent the H-SOEC. Reproduced from ref. 162 with permission from Springer, copyright 2021.
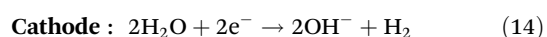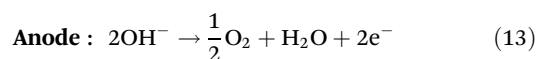
Moreover, based on the operating voltage, SOE cells can operate in one of three ways: endothermic, thermoneutral, or exothermic.[164] In endothermic mode, external heat must be applied because the operating voltage is below the thermoneutral voltage; in thermoneutral mode, the required heat is equal to the heat produced by the Joule effect; in exothermic mode, the operating voltage is above the thermoneutral voltage. In order to assure high efficiency and make heat management of SOE cell stacks and systems easier, the most ideal operation mode for an SOE system is the constant thermoneutral voltage (or slightly above in order to account for potential heat losses).[162]

3.2. Low-temperature water electrolysis

This type of electrolysis includes following methods:

3.2.1. Alkaline water electrolysis (AWE). Alkaline electrolysis has developed into a mature and well-researched technique for hydrogen production up to the megawatt range[165,166] since the electrolysis phenomenon was discovered by Troostwijk and Diemann in 1789,[167] and now represents the most extensive electrolytic technology at a commercial level worldwide.[168]

This type of electrolysis is operated between 30 and 80 °C with a concentrated alkaline solution of sodium hydroxide. Moreover, membranes with nickel-catalysed stainless steel and zirconium dioxide are used as a separator. Furthermore, there are various challenges associated with this system due to the use of corrosive electrolytes and medium mobility of the hydroxide ions. Due to salt formation of potassium carbonate and sensitivity of electrolyte, decreased ionic conductivity and hydroxyl ions is prominent. Therefore, alkaline water electrolysis produces lower purity hydrogen and oxygen gases since the membrane does not completely stop gases crossing over from one half of the cell to the other. Generally, the technique consists of two half-cell reactions, with oxygen evolution at the anode and hydrogen evolution at the cathode.[19]

$$\text{Anode}: \ 2OH^- \rightarrow \frac{1}{2}O_2 + H_2O + 2e^- \tag{13}$$

$$\text{Cathode}: \ 2H_2O + 2e^- \rightarrow 2OH^- + H_2 \tag{14}$$

In typical alkaline electrolysers, perovskites are frequently utilised as anodes and Ni-alloys as cathodes. According to reports, efficiency ranges from 59 to 70%.[169]

Gas bubbles containing oxygen and hydrogen, respectively, are created on the surfaces of the cathode and anode during the reaction. When the bubbles reach a particular size, they separate off the surface.[170] Several unfavourable events occur in the electrolysis system as a result of the creation of a gas phase. Gas bubbles cover the electrode surface, preventing the flow of electrons from the electrode to the electrolyte. The electrode surface is harmed and the electrolyte's resistance is increased by bubbles.[170,171]

The low maximum power density attained with liquid electrolytes is an issue with alkaline electrolysis. This restriction results from the detrimental impact of bubble formation. It is necessary to modify and improve materials and configurations since bubble generation in electrolysis cells is unavoidable. Numerous strategies have been used to counteract these consequences. Although they result in a more complicated system configuration, the use of centrifugal fields, magnetic fields, super gravity fields, ultrasound, and microwave treatments do not considerably increase efficiency. The application of an AEM and a zero-gap configuration, respectively, is a very promising technique to enhance the performance of the electrolysis cells. Additionally, operation with an AEM would prevent extra harmful effects of liquid electrolytes.[171] The working principle for an alkaline electrolysis cell is shown in Fig. 8.[170]

In-depth research has been conducted on numerous novel processes, and some of them have already achieved high efficiency. Anion-conducting membrane alkaline water electrolysers have a number of advantages over alternative technologies. One of the key benefits of alkaline systems over electrolysers utilising proton-conducting electrolytes is the relatively inexpensive cost of the electrode materials because less expensive, non-noble metals are stable in alkaline media.[28]

However, because of the modest OH^- mobility and use of corrosive (KOH) electrolytes, alkaline water electrolysis faces the major difficulty of limited current densities (0.1–0.5 A cm^{-2}).[172] To reduce gas crossing, commercial alkaline water electrolysers frequently employ 2–3 mm-thick porous layers.[173] Device performance is affected by limited ion transport through the layer. Numerous researchers in the past have attempted to create "zero gap" electrolysers, in which a 50–100 mm-thick anion exchange membrane is used in place of the 2–3 mm-thick porous layer.[28,173–177]

Some advancements are still needed to improve this technology to reduce the cross-over of gases and increase current density. Separators and electrode material need to be developed to achieve these challenges, while solar and wind energy sources will be most beneficial for cost reduction. One such avenue recently developed for water splitting is two-dimensional metal organic frameworks of nickel nano flakes in alkaline media.[178] Some research organisations/institutes are still actively working in this field to improve efficiency and lower the cost of hydrogen production.[179]

Alkaline water electrolysis mostly takes place by using a Ni-based electrolyte and 5 M KOH which reduces resistance between porous transport and catalyst layers. Current density should also be increased by *ca.* 2–3 A cm^{-2} using thinner separators with a high surface area of electrode material. For large-scale applications, the alkaline water electrolysis is a good system design. Alkaline water electrolysis now costs between \$500 and \$1000 per kW, and the system lasts for 90 000 h.[143,180]

3.2.2. Proton exchange membrane (PEM) water electrolysis.

PEM electrolysis is the most promising technology when compared with low-temperature electrolysis.[181] General Electric and Grubb initially developed PEM electrolysis in the 1950s and 1960s for space applications to produce oxygen for astronaut life support; submarines were then built using the technology, firstly by Hamilton Sundstrand (now Collins Aerospace).[182–185] Since then, a number of businesses have converted the same fundamental technology into goods for hydrogen production at varying scales. The main elements of a PEM electrolyser cell are shown in Fig. 9.[185]

In PEM water electrolysis, catalysts based on Pt/Pd are typically used as the cathode for the hydrogen evolution reaction (HER) and catalysts based on RuO_2/IrO_2 are typically used as the anode for the oxygen evolution reaction (OER).[186–189] An acidic membrane in the form of a solid electrolyte (Nafion, DuPont) and anode and cathode catalysts (mostly Ir and Pt, respectively) make up a PEM electrolyser.[190] The membrane separates the hydrogen and oxygen gases produced by the subsequent reaction while allowing the H^+ ions to pass from the anode to the cathode.[42]

$$\textbf{Anode}: \ H_2O \rightarrow \frac{1}{2}O_2 + 2H^+ + 2e^- \tag{15}$$

$$\textbf{Cathode}: \ 2H^+ + 2e^- \rightarrow H_2 \tag{16}$$

At the anode, hydrogen molecules break apart, which ionises the atoms and sends their electrons into an external circuit; through an ion-exchange membrane protons congregate at the cathode. Oxygen, protons from the ion-exchange

Fig. 8 Diagram of an alkaline electrolysis cell. Modified from ref. 170 with permission from Elsevier, copyright 2010.

Fig. 9 Core components of a PEM electrolyser cell; PTL = porous transport layer; GDL = gas diffusion layer. Modified from ref. 185 with permission from IOP Publishing, copyright 2021.

Fig. 11 (a) Overview of typical PEM water electrolyser, (b) PEM cell stack and, (c) cell components; 1-bipolar plate, 2-anode current collector, 3-MEA, 4-cathode current collector.[181]

membrane, and electrons all then come together to afford water or steam. We can get an energy conversion efficiency of 60% or more with this method.[191,192] The working principle of the PEM electrolysis cell is shown in Fig. 10.

Membrane electrode assemblies (MEAs), current collectors (gas diffusion layers), and separator plates make up the majority of the parts of a PEM water electrolysis cell. Fig. 11 depicts a typical overall view of a PEM water electrolysis cell assembly. However, MEA, which divides the cell into two half cells (anode and cathode), is at the centre of the electrolysis cell.[181]

These proton exchange membranes offer a number of benefits, including low gas permeability, robust proton conductivity (0.1 ± 0.02 S cm^{-1}), reduced thickness (20–300 µm), and high-pressure operation. PEM water electrolysis is one of the preferable technologies for converting renewable energy to highly pure hydrogen from a sustainability and environmental perspective. Other excellent attributes offered by the PEM water electrolysis method are a small carbon footprint, high current densities (over 2 A cm^{-2}), lower operating temperatures

(20–80 °C), ultrapure hydrogen production, and the production of oxygen as the by-product.[20,27,193–195] The purity of the gases produced is higher than that of alkaline electrolysis.[42] As a result, when compared with alkaline electrolysis, PEM electrolysis can achieve great efficiencies (50–75%) with a quick response.[17]

The PEM electrolyser is expected to cost between $1000 and $1400 per kW, with clear paths to be reduced to $400. The $1 per kg H$_2$ target set forward in the US Department of Energy's Hydrogen Energy Earth Shot campaign must be reached in order to reach its ultimate goal of $150 per kW. Due to the acidic nature of the electrolyte with strong proton conductivity and the structures that reduce ohmic losses, the water electrolysis kinetics in PEM cells is faster than in alkaline electrolysis. The capability of applying a high pressure on the cathode side while operating the side of the anode at atmospheric pressure is a beneficial aspect of PEM electrolysis.[185]

However, cost and durability continue to be obstacles preventing PEM electrolysers from being widely used. To research the deterioration of PEM electrolysers and further increase their durability, collaborative accelerated stress tests across many laboratories are extremely desirable.[185] The usage of expensive polymeric membranes and the need for noble metals due to the electrolyser's acidic liquid are current drawbacks. One of the main difficulties is reducing the amount of noble metals used in PEM electrolysers.[181] The adoption of platinum group metals as noble metal catalysts, Nafion-based membranes, and Ti-based stack materials are causes of PEM water electrolysis expenditure issues.[42]

3.2.3. Anion exchange membrane (AEM) water electrolysis. The AEM electrolysis cell consists of an electrode made of transition metals catalyst and a hydrocarbon anion exchange membrane. Purified water or a low-concentration alkaline solution can be used as the electrolyte in the AEM in place of a strong KOH solution (Fig. 12). Anion exchange membrane water electrolysis combines the advantages of alkaline electrolysis and proton exchange electrolysis.[177,196,197] AEM electrolysis techno-

Fig. 10 Illustration of a PEM electrolysis cell.

Fig. 12 Working principle of an AEM electrolysis cell.

logy, like alkaline and PEM electrolysis, uses low-cost catalysts and a solid polymer electrolyte.[198] It works in an alkaline environment, which allows for the use of low-cost electrocatalysts and a zero-gap architecture.[199] This method of electrolysis employs a polymeric membrane containing quaternary ammonium salts. It is relatively cheap and has little interaction with surrounding CO_2.[200,201]

AEM electrolysis is projected to outperform conventional electrolysis technologies in terms of performance and total cost.[202] Previous research with AEM electrolysis has yielded promising outcomes. One study found that a membrane electrode assembly (MEA) combination of polybenzimidazole (PBI) AEM and specific catalysts (Ni–Fe–Ox for oxygen evolution and Ni–Fe–Co for hydrogen evolution) performed best under specific conditions, with an AEM electrolysis efficiency of 74% at 1000 mA cm^2, 1.9 V, and 60 °C.[203]

Despite its satisfactory performance, the AEM electrolyser's performance is lower than that of traditional PEM electrolysers.[198,199] In AEM electrolysers, the voltage drives the electrolysis reaction, whilst the current reflects the rate of hydrogen generation. When a voltage is supplied between the anode and cathode, electrons travel *via* an external circuit and are balanced by the movement of hydroxide ions through the AEM.[204] The hydroxide ions strive to cross the AEM when more voltage is applied, while the electrons will travel *via* the external circuit. However, at lower voltages, electrons and OH⁻ cannot transfer due to internal barriers.[205]

A drop in voltage causes a decrease in hydrogen production, termed charge transfer resistance or activation overpotential. And if the applied voltage is low, the flow of electrons is restricted by internal components such as the catalyst layer, AEM, and gas diffusion electrode (GDL). The ohmic resistance (R_{ohm}) is the name given to this constraint.[206] However, the performance of an AEM electrolyser is determined by three variables: kinetic resistance, ohmic resistance, and mass transfer resistance.[207,208]

3.3. Solar-powered water electrolysis

Renewable energy electrolysis would produce an exceptionally clean hydrogen cycle (Fig. 13). Solar (and wind)-generated

Fig. 13 A renewable hydrogen cycle. Modified from ref. 209 with permission from Elsevier, copyright 2002.

hydrogen could meet the world's anticipated energy needs; however, delivering it may cost more than making hydrogen from natural gas.[209]

Solar-powered water-splitting for hydrogen production is a clean and viable energy solution; two promising technologies for this are photovoltaic-electrocatalysis (PV-EC) and photoelectrocatalysis (PEC). A photoelectrode harvests light and electrolyses water in the PEC process. PV-EC incorporates separate modules for solar-powered electricity generation and water splitting (Fig. 14), distinguishing PV-EC from a standard PEC configuration.[121]

3.3.1. Photoelectrochemical (PEC) cells. The process of PEC water-splitting produces hydrogen fuel from sunlight. Sunlight strikes the photoactive electrode, producing electron–hole pairs, which is the first of four steps. Water is oxidised by the photogenerated holes, and electrons are transferred to the photocathode. The proton (H⁺) undergoes reduction at the photocathode, creating hydrogen gas. It is possible to separate carriers effectively by employing an external power source. For electron generation, the photoactive material needs to have the appropriate band gap. The process is also impacted by semiconductor
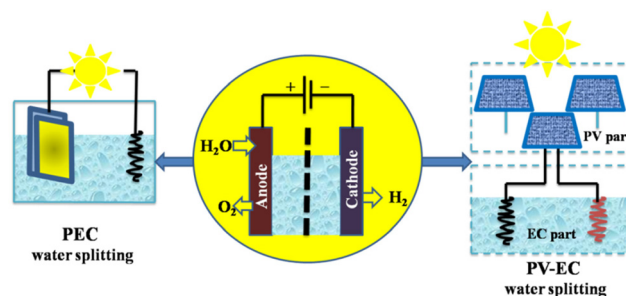

Fig. 14 Two pathways for solar hydrogen production by PEC and PV-EC water splitting. Modified from ref. 121 with permission from Springer, copyright 2021.

band locations. Due to its clean operation and direct conversion of sunlight, PEC-based hydrogen production is gaining popularity as a sustainable method of producing hydrogen.[210]

It is generally agreed that Brattain, Garret,[211] and Gerischer's[212] research established the groundwork for contemporary photoelectrochemistry. Numerous articles on photoelectrochemical cells emerged in the wake of the 1973 oil crisis, which prompted an increase of new study into renewable energy sources.[213] The focus was on two types of cells: regenerative cells and photosynthetic cells. Light is converted to electric power by regenerative cells without generating any net chemical change. Photon-generated electron–hole pairs are separated, with negative charge carriers passing through the semiconductor to the current collector and external circuit and positive holes being collected by a redox relaying molecule. Water is oxidised to oxygen at the semiconductor photoanode and reduced to hydrogen at the cathode in photosynthetic cells, which work similarly but include two redox systems, as shown in Fig. 15a.[212]

After the 1972 *Nature* paper by Fujishima and Honda showing photodriven water oxidation on TiO_2 with a small bias, the idea of a single-material PEC cell that could drive both photooxidation and photoreduction of water without an external bias was developed.[214] A single substance is immersed in water to make hydrogen and oxygen, making this idea interesting. However, there are several prerequisites, such as the material requiring a large band gap to generate energy but not one that is too large to absorb sunlight. Band edges must align with exact energy levels to enable water oxidation and reduction processes (Fig. 15b). The material should be able to separate and transport light-generated charge carriers without recombination. The interface of the material should also be catalytically active for water oxidation and reduction, as well as stable in water and light. The material should also be nontoxic and affordable.

Substantial effort has been put into discovering a suitable material for efficient PEC water-splitting.[215–217] Hundreds of compounds were investigated using combinatorial methods.[218–220] All

requirements, however, have not been met by any material. Using a plethora of materials to create a PEC device is more efficient since the stresses on each material are reduced. Instead of relying on each element to be efficient at everything, synergy of the materials can accomplish what is required. Putting distinct functionalities into a variety of materials has been beneficial for the development of useful technologies.

Different approaches to monolithic device design incorporating many materials are studied in the research literature. One way to do this is to make a group of monoliths that are suspended as nanoparticles.[217,221,222] This method is appealing because it is simple, and there is no need for wires, wiring, or separating the cells. It can also be made with sol–gel synthesis methods, which can be used on the large scale and possibly be less expensive.[223] Small particles are used in diffusion to split and move charges. Co-catalysts increase the activity of surface catalysts; two co-catalysts can be used; however, this increases the difficulty. This design makes oxygen and hydrogen at the same time, which raises worries about back reactions and so induces the additional requirement of gas separation in another second step. Because the particles are so small, it is hard to tell which ones do what. This limits the materials that can be used, but not as much as with single-material monoliths. Fig. 16c shows a monolithic cell with multiple layers. Pure PEC cells, underground PV junctions, and PV-electrolysis can employ this type of design. This design is larger than the nanoparticles-in-suspension approach, making material selection and combination easier. This design has yielded multiple functioning devices, including the 2.5% efficient "artificial leaf" and a 10% efficient CIGS (thin-film solar cell) device.[224]

Separating the cathode and anode spatially changes the perspective from a multi-layered PEC cell. Instead of passing through a back contact to a second electrode, the majority of carriers can be wired to the counter electrode; the only difference is charge distance. This method uses a macroscopic wire and a resistive element. The main benefit is greater freedom in geometrical arrangements, synthesis techniques, and material choice. This topological transition lets electrodes be developed, manufactured, and studied separately in an attempt to boost device performance.

There are numerous designs of this concept. One involves a photoactive electrode and a counter electrode performing a sole catalytic function, which constitutes the simplest configuration (Fig. 16a). Either a p-type semiconductor photocathode or an n-type semiconductor photoanode, as in Fig. 16a, can serve as the photoactive electrode. The devices produced by Khaselev et al.[225,226] and Recee et al.[227] show that the single photoactive electrode can be configured as a tandem cell. Fig. 16b illustrates a more sophisticated technique that employs two photoactive electrodes to create a spatially separated tandem cell. For instance, Abdi et al.[228] constructed a 4.9% efficient device using $BiVO_4$ and a tandem junction a-Si solar cell, while Brillet et al.[226] presented a 3.1% efficient device using WO_3 and a dye-sensitised solar cell as examples.

Fig. 15 Working principle of photoelectrochemical cells. (a) Regenerative-type cell producing electric current from sunlight; (b) a cell that generates a chemical fuel, hydrogen, through the photo-cleavage of water. Reproduced form ref. 212 with permission from Nature Publishing Group UK London, copyright 2001.

Fig. 16 (a) A single-material one-cell PEC-device. (b) Basic principle with suspended nanoparticles with two electrodes. (c) Monolithic design where the catalysts are not separated in space.

Researchers may improve each step and look into the fundamental functioning of the system by looking at the two half-reactions separately. Through photocurrents, the macroscopic charge transport makes it simple to gauge efficiency. Once the materials for both half-reactions have been determined as being effective, they can be joined to form a device for the full reaction. In the literature, a number of substances have been investigated for their potential to act as catalysts in these half-reactions.[215–217]

3.3.2. Photovoltaic cell (PVC). In a PEC, a configuration called PV-electrolysis involves spatially isolating the catalysts. The monolithic design in Fig. 17a serves as the starting point for the process. Separating one of the catalysts into a different electrode is one step toward PV-electrolysis, as shown in Fig. 17b. A three-electrode setup, as shown in Fig. 17c, can be created by separating the second catalyst from the photoabsorber to further improve the configuration.

PV-electrolysis is technologically mature because the PV (photovoltaic) part and the catalysts can be developed, improved, and tested separately. They can be connected directly, as shown in Fig. 18a, or through the power grid, as shown in Fig. 18b.

The transmission efficiency of electricity across power lines is approximately 93%, with loss of 7%.[229] Hydrogen electrolysers often make use of expensive resources and run at high levels to maximise efficiency and minimise costs. Unfortunately,

Fig. 18 (a) Photovoltaic electrolysis. (b) Grid-connected PV electrolysis.

this causes a loss of efficiency. However, other types of electrolysers can be even more efficient than alkaline ones. The biggest problem with these systems is the price, not how well they work. Creating hydrogen from natural gas is less expensive than using solar cells, but that could change in the future. Then, attention will turn to improving the process's catalysts.

Directly connecting the solar cell to the electrolysers, rather than going through the grid, avoids the need for inverters and decreases grid losses. Since this lowers solar cell and electrolyser prices, it can make the system more competitive in the market. But there is a disadvantage: since the electrolyser's power supply is less stable, its efficiency may suffer as a result. The benefit of disconnecting from the grid and inverters can be nullified if this happens.[230]

3.4. Grid-connected water electrolysis

Grid electrolysis involves connecting the electrolyser to an existing electrical network. For the transition to a prosperous hydrogen economy, this approach appears to be the shortest and least expensive. However, using this technique, hydrogen production is not practicable in isolated or rural areas lacking access to dependable electricity. Additionally, even though electrolysis does not directly release any harmful gases to the environment, it indirectly harms the environment by increasing the combustion of fossil fuels to produce electricity. Much research effort has focused on various elements of grid electrolysis, such as energy storage and grid balancing.[231] Currently,

Fig. 17 (a) Monolithic design where the catalysts are not separated by space. (b) Monolithic design with separated electrode. (c) A three-electrode setup in which the photoabsorber and both catalysts are separated by space.

it is believed that the most practical method for producing hydrogen for the switch to vehicles powered by hydrogen is grid electrolysis (*e.g.*, fuel cell vehicles).[232,233] There is more information available on grid electrolysis and its potential for producing sustainable hydrogen elsewhere.[234–236]

Various variables, such as the capital expenditure for controlling peak demands, the investments required for grid reliability, and the integration of renewable energy sources, might be linked to the rising interest in energy storage for the grid. There is acknowledgment that battery systems can offer a variety of high-value options, assuming that reduced costs can be reached, even if pumped hydropower is currently the dominant form of energy storage. The battery systems including redox-flow batteries, which are inexpensive, lithium-ion batteries, developed for commercial gadgets and electric vehicles, and sodium–sulfur batteries, which are commercially accessible for grid applications.[102]

Several electrolyser stacks, compressors, and gaseous hydrogen storage units make up a large-scale water electrolysis hydrogen production system (Fig. 19). We take into account hydrogen production from electrical grids with strong renewable energy penetration and usage in a variety of applications across various industries. This system layout was primarily chosen based on the input needs of feedstock hydrogen in the subsequent chemical processes related to the production of hydrocarbon fuels, industrial use, or fuel supplied in the production of electricity. A developed hydrogen value chain is necessary for centralised electrolytic hydrogen production, which is also applicable to the transportation industry. More significantly, the integration of renewable energy sources into the power grid through the use of water electrolysis and the production of hydrocarbon fuel (synfuel) creates a process that can decarbonize the energy supply chain. By turning electricity into hydrogen, the inclusion of large-scale water electrolysis into the power grid might reduce the volatility of renewable energy sources. The installed capacity of the water electrolysis facility is anticipated to vary from several MW to 100 MW, or possibly GW, for the case of synfuel production on a massive scale.[233]

The key distinction from typical chemical processes, such as Steam Methane Reforming (SMR), is the use of water and

electricity rather than coal or natural gas (NG) in an electrolyser that is connected to the grid to generate hydrogen. Additional sources of electricity include 26 MW and 54 MW solar and wind farms, respectively. The following possibilities are listed:

✓ An electrolyser that is grid-connected receives power from the exterior public electrical grid;

✓ Wind turbine (WT)/grid-connected electrolyser: The grid and wind turbine both provide energy to the electrolyser. A portion of the electricity generated by the WT is marketed to the electricity market because the wind turbine is greater than the electrolyser capacity;

✓ Photovoltaic (PV)/wind turbine (WT)/grid-connected electrolyser: The grid-connected electrolyser is powered by PV and WT, and some of the electricity is sold to the electricity market;

✓ PV/grid-connected electrolyser: The grid and PV work together to supply energy to the electrolyser. A portion of the electricity generated by PV is distributed to the electrical market since the PV capacity is greater than the electrolyser capacity.[237]

To create the techno-economic model for a grid-connected large-scale hydrogen production plant, three possibilities are taken into account (as illustrated in Fig. 20). This model also takes different power price structures, hydrogen generation and storage systems, and component sizes into account.

✓ In scenario 1, when electricity costs are defined as fixed-charge rates, the impact on a levelized cost of hydrogen is examined. Since the operation schedule reflects the output demand, hydrogen storage is not taken into consideration. For medium-scale implementation, the average outputs are set at 4000 kgH$_2$ per day, and for large-scale deployment, at 40 000 kgH$_2$ per day.

✓ In scenario 2, a metal tank at 200 bar is used to examine the impact on a levelized cost of hydrogen at wholesale energy markets with a 1-day storage capacity. The storage capacity (40 000 kgH$_2$) is viewed as being sufficient for one day. From 0.4 to 1.0 capacity factors are taken into account. The adaptability of areas where large-scale geological hydrogen storage is not practical is taken advantage of by this system arrangement.

✓ Scenario 3 investigates the impact of massive underground hydrogen storage on a levelized cost of hydrogen at wholesale energy markets. The production facilities anticipate that taking into account a 7-day storage capacity will allow them to further benefit from cost savings during non-peak times. The capacity factor is rated from 0.4 to 1.0, just like in scenario 2.[233]

3.5. Wind-powered water electrolysis

In wind electrolysis, the electrolyser is connected to the power generated by wind turbines. It is possible to create cleaner hydrogen using wind electrolysis, which also holds the potential to make greater use of the renewable energy sources that are already present in the area[238] and to increase the proportion of renewable energy in the electric grid while lowering greenhouse gas emissions.[239] However, hydrogen generation

Fig. 19 The water electrolysis technique for producing hydrogen (grid electrolysis process). Reproduced from ref. 233 with permission from Elsevier, copyright 2019.

Scenario 1

Scenario 2

Scenario 3

Fig. 20 Deployment scenarios for water electrolysis. (BC = British Columbia; MB = Manitoba; NL = Newfoundland and Labrador; ON = Ontario; QC = Quebec; YT = Yukon; CA = California; GE = Germany.) Modified from ref. 233 with permission from Elsevier, copyright 2019.

from wind electrolysis needs to be competitively priced to allow for a higher uptake of renewable energy sources, *e.g.* to compete with gasoline or other vehicle fuels as a vehicle fuel or be cost-competitive with other grid electricity technologies as a grid energy storage technology.[240,241] At some wind production sites, hydrogen production could be achieved at $4 per kg or less.[236] The capacity factor, which must be 44% or more together with reasonably high wind speeds, is a major problem.[242] Nevertheless, in addition to low production costs, delivery and storage costs will also affect the final pricing of hydrogen. For this reason, it is necessary to investigate a wider variety of wind sites, where geographical factors such as distance from the end usage should also be taken into account.[52]

The concept underlying the coupling system between non-grid connected wind power and water electrolysis holds that when "three fields"—temperature field, electric field, and flow field—are balanced, the large-scale fluctuations in wind power current density have little effect on water electrolysis efficiency in the electrolyser. Improvements should be made to cooling systems, power supplies, and water-electrolytic technologies to address the effects of wind power variation on production. The electrolyser utilizes an intelligent power controller to accomplish "seamless connection without disturbing each other" and to create "wind power-based, grid power-supplemented" systems. The intelligent power controller has two supply

models, referred to as wind/grid complementary power supply and wind power independent supply. Wind power will be completely used, regardless of wind speed. There are three scenarios:

✓ when wind power is greater than the rated power of the electrolyser, no grid power is used;

✓ when wind power is lower than the rated power of the electrolyser, grid power is complementary;

✓ and when there is no wind, grid power supplies all of the power. Grid electricity is used by the water circulation pump and other auxiliary devices.

In accordance with the wind conditions, the flow of cooling water is also adjusted. In order to improve the water electrolyser, "three-field" balancing was thus attained. Fig. 21 depicts the circuit diagram of a water electrolytic hydrogen generation system that uses wind energy without a grid connection.[243]

Electricity generation from wind energy illustrated minimum negative impacts on the environment compared with the other energy resources.[244] In 2012, about 282 275 MW electricity was generated by wind energy which was around 2% of total world electricity demand. The USA, China, Germany, Spain, and India generate more than 73% of annual worldwide wind electricity.[245] In order to utilise the maximum capacity of wind power, complex wind power plants should be managed wisely. For instance, in some wind power plants around the

Fig. 21 Circuit diagram of non-grid-connected wind power/water-electrolytic hydrogen production system. Modified from ref. 243 with permission from Elsevier, copyright 2012.

world, the transportation capacity of the electricity grid should be upgraded and additional power capacity should be installed to prepare a backup for the installed wind power system.

Wind energy can vary due to meteorological changes, which increases the demand for balancing power in load frequency regulation. Such issues might be resolved using a water electrolysis-based wind-to-hydrogen (WTH) technique. In times of low wind potential or after grid congestion has subsided, the excess electricity is stored as hydrogen and converted back into electricity.[246] For both grid-connected systems and isolated grid systems, electrolytic hydrogen's potential as a storage medium for wind energy in network balancing has been researched.[247,248] Hydrogen serves as a buffer for wind power facilities to control changes in wind power due to the synergy between the sectors of hydrogen energy and wind power.[249] Additionally, the WTH system has a great deal of potential for use in light-duty cars as a clean fuel to reduce rising GHG rates.[250] An integrated system for producing electricity from wind energy and using hydrogen is shown in Fig. 22.[251]

Based on the production of hydrogen from natural gas and gasoline as non-renewable fuels, Granovskii et al. completed a life cycle assessment (LCA) of hydrogen and power generation from wind and solar technologies as renewable resources. It was stated that the cost of hydrogen produced through the reforming of renewable sources is higher.[252] Additionally, it was noted that WTH for hydrogen vehicles fuel cells instead of gasoline can result in a cost-effective reduction of GHG emissions when the efficiency of an hydrogen vehicle is two times higher than an internal combustion vehicle.[253] Due to the
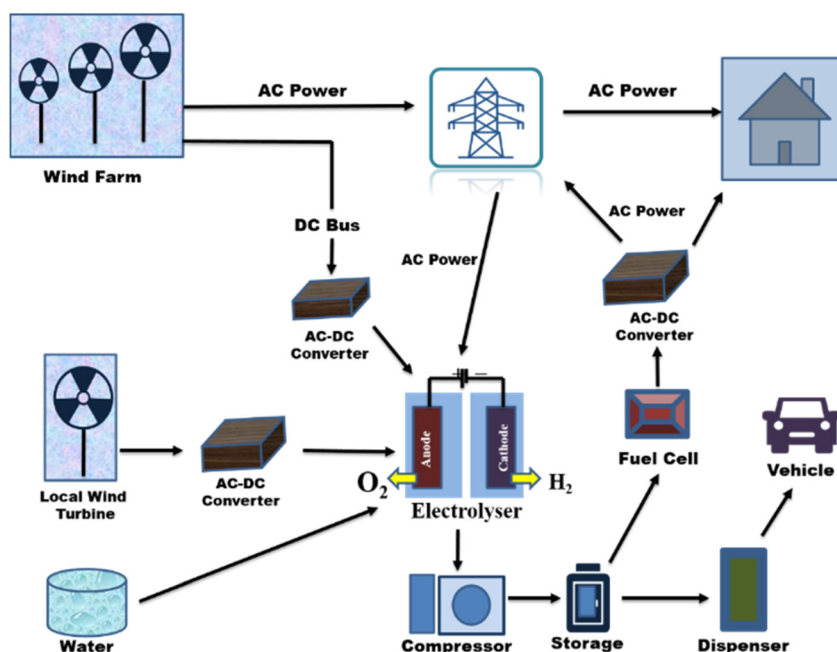

Fig. 22 Integrated wind energy system for producing electricity and hydrogen. Modified from ref. 34 with permission from Elsevier, copyright 2016.

high cost of newly installed equipment and energy loss from inefficient energy conversion processes, hydrogen produced from wind energy is expensive.[254]

According to Harrison *et al.*, the National Renewable Energy Laboratory (NREL) in the US oversaw the testing of a WTH pilot scale that connects 100 K wind turbines with polymer electrolyte membrane (PEM) and an air energy storage (AES) system that produces 20 kg of hydrogen per day. The price of the hydrogen produced by this technique is approximately $5.50 per kg; however, this price can be reduced by installing cutting-edge wind turbines, and the cost objective for 2017 was $2 per kg. It is significant that when the price of the WTH system falls to $0.015 per kW h, hydrogen production using the technology might be competitive with hydrogen generation using gasoline.[255]

3.6. Nuclear energy-powered water electrolysis

It is appealing to use nuclear energy as the main source of energy for hydrogen production because it is adaptable to large-scale hydrogen production and its greenhouse gas emissions are significantly lower than those associated with conventional fossil fuel combustion. Through numerous studies that were published in the open literature in recent years, advancements in nuclear-based hydrogen production have become apparent. Connecting an electrolyser to a nuclear power station is the easiest way to produce hydrogen from nuclear energy (Fig. 23). Such a system has the advantage of being able to run at design load without directly interfering with the grid, which can experience grid overload at times.

The fact that there is no need to modify the reactor is another significant benefit of nuclear/water electrolysis. Such systems were used on nuclear submarines to produce hydrogen and oxygen, which are both necessary for life. The system can be modified to use existing nuclear power reactors to produce off-peak electricity. Nuclear power facilities can operate at constant load with the maximum efficiency and lowest cost of electricity generation by producing hydrogen during off-peak hours. Additionally, potential grid congestion is avoided, enhancing the electrical grid's effectiveness and reliability. Remember that even though tested approaches only achieve less than 55%

efficiency, the maximum predicted efficiency of the water electrolysis process is 80%. The presented thermal-to-hydrogen efficiency when coupled to modern light water reactors or advanced light water reactors (ALWRs) is 27%; however, when coupled to modular helium reactors (MHRs) or advanced gas reactors (AGRs), the expected efficiency is 35%.

Nuclear reactors have typically been used to generate electricity using steam power plants. According to studies, if a sustainable fuel like hydrogen is created in addition to electricity, there will be more advantages. When using nuclear energy, higher temperatures and pressures are required for the reactor coolant since the efficiency of power generation typically increases as the working medium's temperature rises. However, the allowed temperatures in nuclear reactors and the corresponding temperatures and pressures of the coolants are what primarily restrict advancements in the power generation efficiency of nuclear power plants. The rates of material corrosion and safety restrictions on nuclear reactors set a limit on coolant parameters.

Numerous studies focus on the advancement of nuclear reactors, which must match certain criteria like providing inexpensive energy and high-temperature heat in order to effectively couple with a hydrogen manufacturing facility. The most promising hydrogen generation systems, in terms of the process heat temperature level they offer, are gas-cooled reactors, molten salt-cooled reactors, and heavy metal-cooled reactors. The various nuclear reactor technologies along with nuclear reactor-adaptable thermally driven hydrogen production processes will complement rather than compete in the development of nuclear-based hydrogen generation in the future.[17]

4. Electrolysis using organic fuels

Despite the fact that water or steam electrolysis is well recognised, its extensive application is constrained by high operational costs associated with energy use. Utilising an alternative anode reaction for O_2 evolution with a lower equilibrium potential can reduce the amount of electrical power needed for electrolysis. Several reactions can be employed to do this, but one that has the potential to be appealing is the use of an

Fig. 23 Approaches for integrating nuclear reactors and water electrolysis for (a) dedicated hydrogen production systems or (b) cogeneration systems of electricity and hydrogen. Modified from ref. 17 with permission from Elsevier, copyright 2012.

Green Chemistry

organic chemical fuel. Methane gas is one such method, which is used as an anode depolariser.[256]

$$\text{Anode}: \ CH_4 + 2H_2O \rightarrow CO_2 + 8H^+ + 8e^- \qquad (17)$$

$$\text{Cathode}: \ 8H^+ + 8e^- \rightarrow 4H_2 \qquad (18)$$
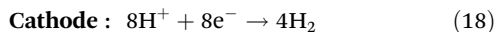
The traditional method of electrolysis is water electrolysis; however, because it uses so much energy, interest in producing hydrogen by methanol electrolysis has grown due to several benefits over traditional water electrolysis.[256–258]

By effectively substituting one unit of electricity with one equivalent energy unit of natural gas at a cheaper cost, this is analogous to electrochemical steam reforming. High system efficiency in terms of primary energy is made possible with the use of natural gas in the electrolyser; voltage reductions of up to 1.0 V in comparison with conventional electrolysers are feasible, and as a result, the electrolyser's electricity consumption can be as low as one-third of that of conventional electrolysers.[256–261] However, since it utilises natural gas, this method is not sustainable. Alcohol, which may be produced *via* fermentation technology, could be the basis of an alternative system. One such methanol-powered cell circulates an aqueous solution past the anode, where methanol and water combine to produce carbon dioxide, much like that in a direct methanol fuel cell:[256]

$$\text{Anode}: \ CH_3OH + H_2O \rightarrow CO_2 + 6H^+ + 6e^- \qquad (19)$$

$$\text{Cathode}: \ 6H^+ + 6e^- \rightarrow 3H_2 \qquad (20)$$

The electrolysis was carried out using a DC power supply to deliver a constant current to the electrolytic cell. A platinum resistance thermometer was positioned close to the anode surface to gauge the electrolytic cell's temperature. Water and the methanol–water solution were then given to the electrolytic cell's anode. A non-pulsation quantitative pump was used to regulate the flow rates, and the electrolytic cell's membrane electrolyte was a Nafion-117 membrane. Both the anode and the cathode catalyst were made of platinum.[256] Additionally, methanol crossover from an anode to a cathode in Nafion membrane methanol electrolysers increases fuel consumption and results in contaminants in the hydrogen produced; as a result, membranes have been further developed to solve this issue.[261–264] Fig. 24 indicates the electrolysis setup for organic fuel methanol.

A research study explained the exceptional performance of a CoS$_2$ nanoarray electrode on a titanium mesh substrate (CoS$_2$/TiM) as a highly efficient and durable catalyst for the oxidation of hydrazine in a 1.0 M KOH electrolyte containing 100 mM hydrazine. Achieving a current density of 100 mA cm^{-2} requires only a low potential of 125 mV. The impressive hydrogen-evolving activity exhibited by CoS$_2$/TiM positions it as a versatile bifunctional catalyst for energy-efficient hydrogen production through electrolysis, where it replaces the conventional water oxidation with hydrazine oxidation. In an electrolyser operating at 100 mA cm^{-2}, CoS$_2$/TiM demonstrates remarkable performance, with a minimal cell voltage requirement of just 0.81 V in a two-electrode setup. Furthermore, it

Fig. 24 Electrolysis using organic fuel methanol.

exhibits outstanding long-term electrochemical stability and achieves nearly 100% faradaic efficiency for the evolution of hydrogen gas.[265]

An effective strategy to substantially reduce the voltage required for water electrolysis is to substitute the anodic OER with the hydrazine oxidation reaction (HzOR) due to its lower thermodynamic oxidation potential. In a study, researchers designed a novel copper–nickel nitride (Cu$_1$Ni$_2$-N) catalyst with a well-defined Cu$_4$N/Ni$_3$N interface on a carbon fiber cloth substrate. This three-dimensional (3D) electrode demonstrates exceptional performance in HER, requiring only a minimal over-potential of 71.4 mV at a current density of 10 mA cm^{-2} in a 1.0 M KOH solution. Simultaneously, it exhibits an impressively low potential of 0.5 mV at 10 mA cm^{-2} for HzOR when used in a 1.0 M KOH/0.5 M hydrazine electrolyte. Furthermore, when this synthesized Cu$_1$Ni$_2$-N electrode is employed as both the cathode and anode in an electrolytic cell, it achieves a cell voltage of 0.24 V at 10 mA cm^{-2} and maintains excellent stability over a 75-hour duration. This research represented a significant step forward in the development of copper–nickel-based nitrides as bifunctional electrocatalysts, leveraging hydrazine assistance to enable energy-efficient hydrogen production through electrolysis (Fig. 25).[266]

A research study investigated an energy-efficient alkaline hydrogen production system by substituting the oxygen evolution reaction (OER) with the more oxidizable urea oxidation reaction (UOR). In this context, a bimetal heterostructure, CoMn/CoMn$_2$O$_4$, was engineered to serve as a bifunctional catalyst within an alkaline environment, facilitating both urea oxidation and the hydrogen evolution reaction (HER). The CoMn/CoMn$_2$O$_4$ heterostructure, characterized by a Schottky heterojunction structure, enables spontaneous charge transfer at the interface. This feature enhances the adsorption of reactant molecules and the breaking of chemical bonds, thereby initiating the decomposition of both water and urea. Consequently, the heterostructured electrode demonstrated remarkably low potentials of −0.069 V and 1.32 V (*versus* the reversible hydrogen electrode) to attain current densities of 10 mA cm^{-2} for HER and UOR, respectively, in an alkaline solution. Furthermore, the complete urea electrolysis driven by CoMn/CoMn$_2$O$_4$ achieves a current density of 10 mA cm^{-2} at a relatively modest potential of 1.51 V and maintains stable per-

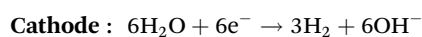**Fig. 25** Electrolysis using organic fuel hydrazine. Modified from ref. 266 with permission from Wiley Online Library, copyright 2019.

Fig. 27 Schematic illustration of HMFOR and HER. Modified from ref. 268 with permission from Elsevier, copyright 2022.

formance for over 15 hours. This innovative approach involving Mott–Schottky hybrids in electrocatalysts represents a promising avenue for sustainable energy conversion, merging hydrogen production with sewage treatment for environmentally responsible applications (Fig. 26).[267]

In another study researchers substituted the OER with the thermodynamically preferred 5-hydroxymethylfurfural (HMF) that gives 2,5 furan dicarboxylic acid (FDCA) on oxidation. They created three-dimensional (3D) hybrid electrocatalytic electrodes by layering nanosized graphene oxide as a building block. These electrodes were capable of aiding both HMF conversion and the hydrogen evolution process (HER) at the same time. The nanoarchitecture of the electrode, comprising the thickness and position of gold (Au) and palladium (Pd) nanoparticles (NPs), was found to have a substantial influence on electrocatalytic performance. Even when the same constituent NPs were used, the electrodes demonstrated highly adjustable performance *via* reaction kinetics and diffusion-controlled mechanisms. Furthermore, in a full-cell setting, a bifunctional two-electrode electrolyser optimised for HMF oxidation and HER had the highest overall electrocatalytic activity.

$$\text{Anode}: \text{HMF} + 6\text{OH}^- \rightarrow \text{FDCA} + 4\text{H}_2\text{O} + 6\text{e}^-$$

$$\text{Cathode}: 6\text{H}_2\text{O} + 6\text{e}^- \rightarrow 3\text{H}_2 + 6\text{OH}^-$$

$$\text{Overall} \quad \text{HMF} + 2\text{H}_2\text{O} \rightarrow \text{FDCA} + 3\text{H}_2$$

In a recent study, researchers introduced a novel integrated electrode composed of CoNiP nanosheets with a dual function-

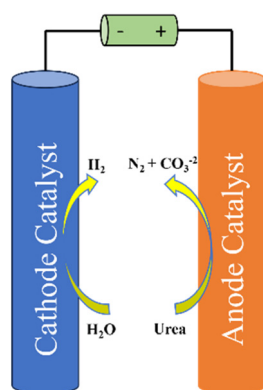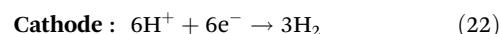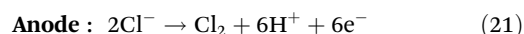**Fig. 26** Electrolysis using organic compound urea.

ality. The CoNiP-NIE serves to enhance the HER while also replacing the OER with the oxidation reaction of 5-hydroxymethylfurfural to produce the valuable compound 2,5-furandicarboxylic acid (FDCA). The newly designed electrode achieves a high faradaic efficiency exceeding 82% for HMFOR over a wide potential range, from 1.40 V to 1.70 V *vs.* RHE (reversible hydrogen electrode), which surpasses the performance of previously reported electrocatalysts. Furthermore, the low overpotential required for HER underscores its effectiveness in hydrogen (H_2) generation. Leveraging the bifunctional properties of CoNiP, researchers constructed an electrochemical device that combines hydrogen evolution with biomass oxidation. This device exhibits a lower voltage requirement (1.46 V) for anode oxidation compared with traditional water splitting (1.76 V) and achieves a higher H_2 evolution rate (41.2 L h^{-1} 1 m^{-2}) under the given conditions (Fig. 27).

5. Hydrogen as a by-product from electrolysis

Numerous electrolyses are based on anodic oxidation, which is accompanied at the cathode by hydrogen evolution. The electrolysis of the halides results in a variety of compounds, which is notable. The chemistry and electrochemistry of the halides (Br, Cl, and I) involve reactions that are quite similar, although the values of the kinetic and thermodynamic parameters vary. Chlorine electrochemistry is a significant field of industry. An important illustration is the electrolysis of sodium chloride to produce chlorine and sodium hydroxide (the chlor-alkali process). The desired reaction in the electrolysis of a sodium chloride solution is the production of chlorine at the anode, while in an alkali solution the cathode reaction results in the formatting of hydrogen gas and hydroxide ions.[269]

$$\text{Anode}: 2\text{Cl}^- \rightarrow \text{Cl}_2 + 6\text{H}^+ + 6\text{e}^- \quad (21)$$

$$\text{Cathode}: 6\text{H}^+ + 6\text{e}^- \rightarrow 3\text{H}_2 \quad (22)$$

It is possible to collect hydrogen gas by separating the anode and cathode reaction products so that they do not react. Other electrolyses of sodium chloride, depending on the circumstances, can generate substances such sodium hypochlor-

ite, chlorate, and perchlorate in addition to hydrogen (at the cathode):

$$NaCl + H_2O \rightarrow NaOCl + H_2 \text{ (Overall hypochlorite reaction)} \tag{23}$$

$$NaCl + H_2O + Cl_2 \rightarrow NaOCl_3 + H_2 \text{ (Overall chlorate reaction)} \tag{24}$$

$$NaCl + H_2O + 3/2Cl_2 \rightarrow NaOCl_4 + H_2 \text{(Overall perchlorate reaction)} \tag{25}$$

The counter electrode additionally produces hydrogen at the cathode as a result of other inorganic syntheses.[15]

6. Sustainability of hydrogen production

Methods for producing hydrogen are based on seven criteria for sustainability. The first two criteria that need to be looked into have to do with how effectively hydrogen can be produced in accordance with the first and second laws of thermodynamics. Energy efficiency is determined by the first law of thermodynamics, while the second law emphasizes energy efficiency. Since efficiency is typically defined as the desired output divided by the required input, the following equation represents energy efficiency:

$$\eta = \frac{m\text{LHV}}{E_{in}} \tag{26}$$

Here, "m" represents the rate of hydrogen generation in kg s^{-1}, "LHV" represents the lower heating value of hydrogen (calculated as 121 MJ kg^{-1}), and "E_{in}" denotes the rate of energy consumption in MJ kg^{-1}. It is possible to transform the energy efficiency equation into the exergy efficiency equation as follows:

$$\psi = \frac{m\text{Ex}_{H_2}^{ch}}{\text{Ex}_{in}} \tag{27}$$

Ex$_{H_2}^{ch}$ stands for the chemical exergy of hydrogen in the exergy efficiency equation, and "Ex$_{in}$" stands for the rate of exergy input into the process. The energy and exergy efficiencies of the chosen hydrogen production technologies are taken from the literature for this study.[270–272]

The cost of producing hydrogen is the third factor, and it is crucial, especially when scaling up and commercializing processes. Making sustainable hydrogen more accessible and extensively used on the market is a crucial first step. The least expensive methods for producing hydrogen right now are coal gasification and natural gas reforming, but they also produce the most pollutants. Technologies for carbon capture (CC) can lower the emissions. However, CC pushes up the price of producing hydrogen by 10% to 20%.[273]

The majority of renewable-based hydrogen production methods are still in their development as compared with conventional, fossil-based solutions. As a result, renewable hydro-

gen has a greater lifecycle cost than fossil-based hydrogen. However, the price of hydrogen derived from renewable sources has significantly reduced. Due to advancements in materials science and system designs, further cost reductions are anticipated for the majority of upcoming renewable hydrogen production techniques. While renewable hydrogen becomes more reasonably priced on a big scale, fossil-based hydrogen produced through carbon capture can be used as a bridge fuel. The cost information for the chosen hydrogen production technologies has been gathered.[20,271,274–276]

The probable effects of acidification and global warming according to the life cycle assessment (LCA) make up the fourth and fifth criteria. The LCA method is dependable for determining the true environmental effect.[277] Global warming potential (GWP) measures the amount of CO$_2$ emissions compared with the amount of H$_2$ produced. Acidification potential (AP) measures the amount of waste that is discharged into the land and water in grams of SO$_x$ per kilogram of H$_2$ generated. The two environmental impact metrics that are most frequently employed are GWP and AP.[278] According to the literature, renewable hydrogen has a distinct advantage over fossil-based hydrogen in terms of GWP and AP.[270,271,273,279]

Cost of carbon (CC) is the sixth criterion. According to the harm done to the environment and human health, CC calculates the marginal external cost of a unit of CO$_2$ emissions. The literature has detailed descriptions of the many models used in the calculation of CC.[280–284] The seventh criterion, known as the technology maturity level (TML), is rated on a modified, consolidated scale between 1 and 10. The TML facilitates the communication of a technology's maturity level. With regard to unique and small-scale alternatives, grade 1 denotes the extremely early stages of research, and the number 10 denotes complete market integration. Data on the state of technology maturity are taken from ref. 272.

All performance factors are standardized and ranked between 0 and 10 in the final step to carry out the comparison assessment. The optimal choice is 10, whereas the least desired scenario is 0. The technology maturity level is already on a 0–10 scale, where 0 and 10 represent the least and most preferable solutions, respectively, therefore there is no normalization added to it. The chosen hydrogen production techniques perform more sustainably across the board as their score rises from 0 to 10. Efficiency measures for energy and exergy are normalized by:

$$\text{Rank (i)} = \text{efficiency (i)} \times 10 \tag{28}$$

The remaining factors (cost of manufacturing, cost of carbon, and potentials for global warming and acidification) are normalized appropriately and ordered as

$$\text{Rank(i)} = \frac{\text{max value} - \text{performance (i)}}{\text{max value}} \times 10 \tag{29}$$

Here, the chosen approach is represented by (i). The highest value in the related performance category is indicated by the term "max value" in eqn (29). For example, if a method

has the greatest emissions among the options chosen, it receives a score of 0. As an alternative, the option with the highest rating would be the one with the lowest cost. It should be highlighted that zero cost and emissions receive rating 10. No method receives the highest ranking as a result. This strategy seeks to demonstrate that each alternative still has room for improvement across all chosen performance metrics. Each of the chosen hydrogen generation solutions is given a total sustainability score after all performance parameters have been normalized and graded between 0 and 10. The overall scores are compared with the ideal hypothetical case where hydrogen is produced with 100 percent energy and exergy efficiency, zero GWP, AP, and cost, and a TML of ten. The average scores are then determined. Table 7 illustrates detailed sustainability performance rankings of the selected hydrogen production methods. The eight cases used to determine average scores are as follows:[210]

EI: All factors are equally important.

EE: Energy efficiency is given a 40% weighting, and the remaining criteria are each given a 10% weighting.

ExE: Exergy efficiency is given a 40% weighting, and the remaining criteria are each given a 10% weighting.

CC: The weight for the cost of carbon is 40%, and the remaining criteria are each given a 10% weight.

Cost: Production cost is given a 40% weighting, while the remaining criteria are each given a 10% weighting.

AP: AP is given a 40% weighting, and the remaining criteria are each given a 10% weighting.

GWP: The weight for GWP is 40%, and the remaining criteria are each given a 10% weight.

TML: TML is given a 40% weighting, and the remaining criteria are each given a 10% weighting.

In the twenty-first century, sustainable energy systems are expected to play significant roles in the supply and demand aspects of the use of current sources. Identification of dependable, economical, plentiful, and clean sources for H_2 production is a necessity. There is much work being done to create and improve systems that manufacture H_2 more cheaply from renewable resources in order to further reduce emissions and energy use.

Hydrogen is widely regarded as an environmentally friendly secondary source of renewable energy and a viable replacement for fossil fuels because it is the only fuel that is carbon-free, and has the largest energy density of any fuel known.[285–287] Another benefit is that hydrogen can be used for domestic consumption and can be safely transported using conventional

transportation methods.[288–291] It can also be stored as compressed gas, cryogenic liquid, or solid hydride in order to be fed to stationary fuel cells.[292–294] A minor portion is utilisation in cars, and applications such as power generation and heating in the residential and industrial sectors are anticipated in the near future.[290,295,296]

The cost of alternative energy sources and novel H_2 generation techniques is falling, while the effectiveness of H_2-based energy conversion systems is rising. H_2 is therefore anticipated to achieve future sustainability objectives.[297] Options for electrolysis based on photovoltaics are also thought to be viable for producing hydrogen sustainably.[20] Unfortunately, the low conversion efficiency and the high investment costs are major barriers to the competitiveness of water-splitting technologies compared with conventional approaches. Integrating storage, transportation, and hydrogen generation based on renewable energy sources is essential for sustainable hydrogen production.[298] Hydrogen must be produced in clean, dependable, cost-effective, and safe ways that do not harm society or the environment in order for hydrogen systems to be acceptably sustainable. The following important factors should be taken into account:

• Technical performance (energy efficiencies, process control, raw material input),

• Social performance (impact on public health, employment and training opportunities, and public acceptance),

• Environmental performance (greenhouse gas emissions, land use, water discharge quality, and solid waste), and

• Availability/reliability (dependence on imported resources, predictability, and scalability).

Grid electrolysis (electricity from fossil fuels), wind electrolysis, solar electrolysis, nuclear thermochemical water-splitting cycles, solar thermochemical water-splitting cycles, and photoelectrochemical cells are some of the current and prospective hydrogen generation technologies. Grid electrolysis is anticipated to hold the key to more environmentally friendly hydrogen production in the near future as other technologies develop and their costs come down. In the long run, wind electrolysis and solar thermochemical water-splitting cycles will be promising methods for producing sustainable hydrogen.[299] Research into new, better-performing (ideally abundant) materials is necessary to enable all of these technologies to attain greater sustainability while aiming for cost reduction. A possible route to 100% sustainably produced hydrogen in the energy sector is shown in Fig. 28.

Table 7 Detailed sustainability performance rankings of the selected hydrogen production methods in different cases and the hypothetical ideal case[210]

	EI	EE	ExE	CC	Cost	AP	GWP	TML
Electrolysis (large scale)	7.7	7.7	6.5	8.3	7.1	8.1	8.3	8.1
PV electrolysis	4.6	3.6	3.4	5.6	3.5	5.5	5.6	4.7
High-temperature electrolysis	6.3	6.9	5.5	6.9	5.2	7.0	6.9	5.6
Photoelectrochemical cell	4.8	3.6	3.4	6.3	3.4	6.3	6.3	4.6
Ideal	10.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0

Fig. 28 A potential pathway to reach 100% sustainable hydrogen in the energy market. Modified from ref. 210 with permission from Elsevier, copyright 2022.

7. Hydrogen economy

The cost of feedstock, the efficiency of the technology used, the stage of development (*e.g.*, early stage or mature), and the physical proximity to end-use markets (centralized or distributed production) are just a few of the many factors that affect the economics of hydrogen production.[300] Investment costs play a large role in determining hydrogen production costs. The production strategy and plant size have an impact on the cost structure. For instance, the fuel cost share ranges from 50 to 68% in large-scale SMRs while it is only between 28 and 40% in small reformer units. Electricity costs account for between 75 and 80 percent of the cost of electrolytic hydrogen. Fuel costs for biomass gasification are roughly 40%. Regarding the evolution of feedstock prices, natural gas is forecast to cost more during the following ten years, while coal is anticipated to cost the same. Costs of electricity are significantly influenced by changes in the price of feedstocks, particularly fossil fuels.

A cheap and sustainable source of hydrogen is necessary for the Hydrogen Economy to succeed in the future. Presently, fossil fuels like coal and natural gas are mostly used to produce hydrogen. However, the availability of both of these fuels is constrained, and the creation of hydrogen results in the release of greenhouse gases. Therefore, in order to produce hydrogen in a hydrogen economy, alternative energy sources must be investigated for both environmental and economic reasons. The cost of operating fossil fuel facilities is rising, whereas the cost of alternative energy technology is falling as economies of scale are reached, even if historically the cost of hydrogen from fossil fuel plants has been less expensive than that from other energy sources. In the electrochemical production of hydrogen, the cost of producing hydrogen using the existing light water reactors with electrolysis is greater and is anticipated to range from 4.36 to 7.36 $ per kg, which would not be regarded as a low-cost energy source in light of current gasoline prices.[22] Costs for electrochemical methods of producing hydrogen are shown in Table 8.[15] The projected costs for PEM electrolysis and SOE to produce hydrogen are now $5.25 per kg and $4.7 per kg, respectively. According to future predic-

Table 8 Representative costs for electrochemical hydrogen production methods[15]

Electrochemical hydrogen production methods	Production costs $ per kg of H_2
SOE electrolysis	4.7–3.8 (forecast)
PEM electrolysis	5.25–4.5 (forecast)
Solar electrolysis	2.0

tions, using electricity generated from renewable resources, electrolysis-produced hydrogen will cost *ca.* $2 per kg. The cost of solar thermochemical hydrogen is approximately $2.5 per kg. Currently, there are roughly 0.1 GT of hydrogen produced annually, most of which is used locally to produce ammonia or to refine and treat metals.[286,295]

Compared with other methodologies, creating hydrogen gas with wind and solar energy is more expensive. This scenario is the result of a number of economic and technological variables, including the cost of maintenance work, the technology used in power systems, and the price of electricity generated by wind and solar systems. The high expenses of distributed and small-scale manufacturing in comparison with the industrial size of conventional power facilities is another factor. Unfortunately, carbon-based conversion is the most cost-effective way for producing hydrogen (steam methane reforming, coal and biomass gasification). Although many people believe that nuclear energy can produce hydrogen at a scale that is economically viable, there are still a number of restrictions and technical issues that need to be resolved.[301]

Table 9 Electrical and thermal efficiencies of conversion for different hydrogen production routes[303–306]

Conversion routes	Conversion efficiency (%)
Nuclear heat + electrolysis	28
Wind + electrolysis	70
Solar PV + electrolysis	10.5
Hydroelectric + electrolysis	70
Tidal + electrolysis	70

Table 10 Production cost and final cost for hydrogen from different processes[275,307–309]

Process hydrogen from	Production mode	Cost (€ per GJ)		
		Feedstock	Production	Final (incl. storage, delivery, dispensing)
Coal gasification	Centralized	1.2	13–16	32–37
Methane reforming	Centralized (3 M Nm^3 d^{-1})	3	5–8	22–30
Biomass gasification	Intermediate	2.4	17–22	33–40
Methane reforming	Decentralized	4–5	7–12	28–33
Gasoline	Refinery	2.5	6	7
Electrolysis	Decentralized	14	20–25	35–40

The overall system has a significant impact on the efficiency of the conversion from electricity to hydrogen and back to electricity. The efficiency of hydrogen production from low-temperature electrolysis will be no higher than 25%. However, by switching from low to high-temperature electrolysis, which produces steam at 800 °C, and by using advanced nuclear plants with higher thermal-to-electric conversion efficiencies, this conversion might be increased (Table 9).[302]

Examples of the technical, economic, and environmental aspects of systems for producing hydrogen using fossil and non-fossil fuels may be found widely in the literature.[270,271] For instance, Dawood *et al.*[272] have examined the function of hydrogen in future energy systems and suggested a pathway toward 100% renewable energy systems. The current situation of the hydrogen supply chain is depicted as an advancing energy vector in the techno-economic assessment of hydrogen production methods, which includes resources, generating and storage technologies, demand market, and economics. Ji and Wang have studied the state-of-the-art, most recent developments, and difficulties of both fossil- and renewable-based hydrogen production techniques. They have come to the conclusion that electrolysis and thermochemical cycles in combination with renewable energy sources exhibit significant economic and environmental promise (Table 10).[273]

8. Conclusion

Most of the hydrogen is produced (95%) from hydrocarbons after reacting with steam. In order to produce hydrogen from non-fossil natural resources in substantial amounts, a hydrogen-based energy system will need to rely on low-cost and effective methods. Using electrolysis, which primarily uses renewable energy sources and water, accounts for only 4% of global hydrogen production. The amounts of hydrogen needed are enormous and orders of magnitude more than what is now produced, according to estimates from different nations. Splitting water, which is a perfect hydrogen transporter, is the most sustainable method of obtaining hydrogen. Hydrogen and oxygen are split from water by electrolysis, a practical and proven process that today yields very pure hydrogen for usage in the electronics, pharmaceutical, and food sectors. Due to the fact that water electrolysis only necessitates a modest amount of storage, it is a safe choice for producing hydrogen at the point

of use in relatively small quantities. Around 80% of the cost of producing hydrogen comes from the electricity needed to electrolyse water and separate it into hydrogen and oxygen. Potentially, electrolysis can produce a clean and renewable energy supply when combined with a renewable energy source. However, electrolysis by itself would not be able to produce all the hydrogen anticipated to be required for upcoming energy demands. Although pilot systems are being investigated, the use of solar radiation for heating and/or photocatalysis shows considerable promise but still needs further research and development. This is currently being conducted on photoelectrochemical catalysts that create hydrogen when exposed to visible light in order to increase their robustness, efficiency, and material costs. There are many choices of methods for producing hydrogen that might be sustainable and prevent this consumption of fossil fuels. However, for them to develop there must be both significant capital investments in the infrastructure and political legislation-driven incentive. Different electrochemical methods have been discussed in detail in this study including wind, solar and nuclear-assisted water electrolysis, high and low-temperature water electrolysis, electrolysis using organic fuels and hydrogen production as a by-product of various electrolytic methods. This review makes an effort to do just that while also going detailing the economics and status of industrial and development electrolysis.

9. Future perspectives

In general, electrolysis is regarded as a well-known alternative technique for producing hydrogen that has already attained a significant market potential. Megawatt-scale units are already available, and problems with project production and supply chain development are also being addressed. Between the years 2020 and 2025 electrolysis is expected to become a marketable technology. The systems' durability is now a limitation of electrolysis technology; however, owing to intensive research, these issues should be solved in the upcoming decades. The viability will depend on the cost of the required renewable electricity. There are several future perspectives which are given below:

1. Resolving durability challenges

One of the primary challenges facing electrolysis technology is the durability of the systems. However, through extensive

research and development efforts, it is anticipated that these difficulties will be overcome in the coming decades. This improvement in durability is a critical step in making electrolysis a more reliable and long-lasting technology.

2. Cost-effective hydrogen production

The viability of electrolysis for hydrogen production is closely tied to the cost of renewable electricity. As renewable energy sources become more accessible and affordable, the cost-effectiveness of electrolysis is expected to increase. This shift is particularly significant as we strive to reduce carbon emissions and transition to a cleaner energy landscape.

3. Advancements in solid oxide electrolysis (SOE)

Solid Oxide Electrolysis (SOE) systems are poised to become more economical and durable in the next decade. They are expected to catch up with traditional alkaline and PEM electrolysis technologies by 2030. This advancement in SOE technology will contribute to a more diverse and competitive hydrogen production landscape.[164]

4. Nuclear-powered hydrogen production

A prospective approach involves utilizing electrolytically produced hydrogen derived from nuclear power sources. This method enables the generation and storage of hydrogen during periods of low electrical demand, which can then be converted back into energy during peak demand. As natural gas prices rise, the stability of nuclear power steam generation becomes increasingly attractive, offering a reliable alternative for hydrogen production.[310]

5. Carbon-neutral hydrogen production

The quest for cost-effective hydrogen production without emitting carbon dioxide remains a top priority. As technology continues to advance, there is a strong possibility that we will achieve the goal of producing hydrogen in an environmentally friendly and economically viable manner. The recent developments in this area are highlighted.[210]

6. Underground seasonal hydrogen storage (USHS)

To secure the energy supply chain for a hydrogen-based future, large-scale energy storage technologies are essential. Underground Seasonal Hydrogen Storage (USHS) is emerging as a viable method to address the temporal fluctuations in renewable energy output. Geological research, including assessments of geochemical and biological reactions, is critical to its success. The connection between hydrogen demand and various applications, such as ammonia generation and integration into power systems, will shape the future energy landscape.[311]

7. Collaboration and diverse production technologies

Collaboration between government agencies, industry leaders, and educational institutions is crucial for driving advancements in hydrogen production. Both centralized and decentralized methods of hydrogen production are under investigation. Prioritizing the improvement of existing commercial methods, while also exploring cutting-edge technologies such as direct photon-to-hydrogen energy-based water-splitting, will lead to diverse and efficient production configurations.

8. Policy adjustments and technological advancements

To achieve these goals, several steps and policy adjustments are recommended:[14]

i. **Foster technology and market development:** Government support should prioritize the development of carbon dioxide capture and absorption technologies and the advancement of renewable and low-carbon-emitting methods.

ii. **Improve gas separation and purification techniques:** Research into high-efficiency hydrogen purification technologies suitable for distributed reformers is essential.

iii. **Invest in small reformers:** Utilizing small reformers powered by various fuels can reduce the cost of hydrogen supply, with a focus on reliability and compatibility with fuel cells.

iv. **Reduce electrolyser expenses and maximize efficiency:** Continuous improvement in electrolyzer efficiency and cost reduction is vital, especially for decentralized power generation.

v. **Explore innovative photolytic processes:** Advancements in photolytic processes that use light energy for hydrogen production should be a research priority, with a focus on efficiency and corrosion resistance.

vi. **Nuclear-powered hydrogen:** Develop cost-effective and environmentally friendly methods for producing hydrogen from nuclear energy, leveraging advanced nuclear reactor technology.

vii. **Carbon dioxide collection and sequestration:** Integrate carbon dioxide capture systems into hydrogen production plants to minimize carbon emissions.

viii. **Demonstrations and technology integration:** Showcase hydrogen production technology alongside practical examples to generate market interest and promote safety.

ix. **Large-scale testing sites:** Establish dedicated sites for large-scale testing and technology display to address logistical challenges.

In conclusion, the future of hydrogen production through electrolysis is bright, with a range of advancements on the horizon. Through collaborative efforts, technological innovation, and policy support, we can build a reliable and efficient hydrogen production system that plays a pivotal role in a sustainable energy future.

Conflicts of interest

The authors declare no conflict of interest.

Acknowledgements

References

1 R. A. Hites, *Persistent organic pollutants in the Great Lakes*, 2005, pp. 1–12.
2 H. Lund, *Energy*, 2007, **32**, 912–919.

3 K. Blok, *Energy Policy*, 2005, **33**, 1635–1641.

4 J. Turner, G. Sverdrup, M. K. Mann, P. C. Maness, B. Kroposki, M. Ghirardi, R. J. Evans and D. Blake, *Int. J. Energy Res.*, 2008, **32**, 379–407.

5 K. T. Møller, T. R. Jensen, E. Akiba and H.-w. Li, *Prog. Nat. Sci.: Mater. Int.*, 2017, **27**, 34–40.

6 J.-S. Kim, D.-C. Lee, J.-J. Lee and C.-W. Kim, *Sci. Rep.*, 2020, **10**, 15586.

7 M. Ball and M. Weeda, *Int. J. Hydrogen Energy*, 2015, **40**, 7903–7919.

8 I. Staffell, D. Scamman, A. V. Abad, P. Balcombe, P. E. Dodds, P. Ekins, N. Shah and K. R. Ward, *Energy Environ. Sci.*, 2019, **12**, 463–491.

9 G. E. Badea, C. Hora, I. Maior, A. Cojocaru, C. Secui, S. M. Filip and F. C. Dan, *Energies*, 2022, **15**, 8560.

10 B. Ewan and R. Allen, *Int. J. Hydrogen Energy*, 2005, **30**, 809–819.

11 C. M. Kalamaras and A. M. Efstathiou, Conference Papers in Energy, 2013, DOI: 10.1155/2013/690627.

12 M. H. Islam, O. S. Burheim and B. Pollet, *Ultrason. Sonochem.*, 2019, **51**, 533–555.

13 J. J. Lamb, M. Hillestad, E. Rytter, R. Bock, A. S. Nordgård, K. M. Lien, O. S. Burheim and B. G. Pollet, in *Hydrogen, biomass and bioenergy*, Elsevier, 2020, pp. 21–53.

14 C. Acar and I. Dincer, *Compr. Energy Syst.*, 2018, **3**, 1–40.

15 K. Scott, *Electrochemical Methods for Hydrogen Production*, 2019, vol. 25, p. 392.

16 F. H. Sobrino, C. R. Monroy and J. L. H. Pérez, *Renewable Sustainable Energy Rev.*, 2010, **14**, 772–780.

17 I. Dincer, *Int. J. Hydrogen Energy*, 2012, **37**, 1954–1971.

18 J. Turner, G. Sverdrup and M. Mann, *J. Energy Res.*, 2008, **32**, 379.

19 S. S. Kumar and H. Lim, *Energy Rep.*, 2022, **8**, 13793–13813.

20 P. Nikolaidis and A. Poullikkas, *Renewable Sustainable Energy Rev.*, 2017, **67**, 597–611.

21 M. Balat and M. Balat, *Int. J. Hydrogen Energy*, 2009, **34**, 3589–3603.

22 J. R. Bartels, M. B. Pate and N. K. Olson, *Int. J. Hydrogen Energy*, 2010, **35**, 8371–8384.

23 A. Midilli, H. Kucuk, M. E. Topal, U. Akbulut and I. Dincer, *Int. J. Hydrogen Energy*, 2021, **46**, 25385–25412.

24 F. Barbir, *Energy*, 2009, **34**, 308–312.

25 A. Ahmed, A. Q. Al-Amin, A. F. Ambrose and R. Saidur, *Int. J. Hydrogen Energy*, 2016, **41**, 1369–1380.

26 M. F. Milazzo, F. Spina, P. Primerano and J. Bart, *Renewable Sustainable Energy Rev.*, 2013, **26**, 579–624.

27 M. A. Khan, H. Zhao, W. Zou, Z. Chen, W. Cao, J. Fang, J. Xu, L. Zhang and J. Zhang, *Electrochem. Energy Rev.*, 2018, **1**, 483–530.

28 M. Bodner, A. Hofer and V. Hacker, *Wiley Interdiscip. Rev.: Energy Environ.*, 2015, **4**, 365–381.

29 I. K. Kapdan and F. Kargi, *Enzyme Microb. Technol.*, 2006, **38**, 569–582.

30 M. Ricci, G. Newsholme, P. Bellaby and R. Flynn, *Int. J. Energy Sect. Manag.*, 2007, **1**, 34–50.

31 A. Demirbas, *Energy Sources, Part B*, 2017, **12**, 172–181.

32 S. V. Mohan, Y. V. Bhaskar and P. Sarma, *Water Res.*, 2007, **41**, 2652–2664.

33 A. L. Ortiz, M. M. Zaragoza and V. Collins-Martínez, *Int. J. Hydrogen Energy*, 2016, **41**, 23363–23379.

34 S. E. Hosseini and M. A. Wahid, *Renewable Sustainable Energy Rev.*, 2016, **57**, 850–866.

35 M. Balat, *Energy Sources, Part B*, 2007, **2**, 49–61.

36 N. Z. Muradov and T. N. Veziroğlu, *Int. J. Hydrogen Energy*, 2005, **30**, 225–237.

37 A. Ajanovic, M. Sayer and R. Haas, *Int. J. Hydrogen Energy*, 2022, **47**, 24136–24154.

38 M. Newborough and G. Cooley, *Fuel Cells Bull.*, 2020, **2020**, 16–22.

39 M. Noussan, P. P. Raimondi, R. Scita and M. Hafner, *Sustainability*, 2020, **13**, 298.

40 Z. Navas-Anguita, D. García-Gusano, J. Dufour and D. Iribarren, *Sci. Total Environ.*, 2021, **771**, 145432.

41 A. M. Amin, E. Croiset and W. Epling, *Int. J. Hydrogen Energy*, 2011, **36**, 2904–2935.

42 M. Carmo, D. L. Fritz, J. Mergel and D. Stolten, *Int. J. Hydrogen Energy*, 2013, **38**, 4901–4934.

43 S. Zhiznin, V. Timokhov and A. Gusev, *Int. J. Hydrogen Energy*, 2020, **45**, 31353–31366.

44 A. Konieczny, K. Mondal, T. Wiltowski and P. Dydo, *Int. J. Hydrogen Energy*, 2008, **33**, 264–272.

45 S. Wang, A. Lu and C.-J. Zhong, *Nano Convergence*, 2021, **8**, 1–23.

46 M. Rashid, M. K. Al Mesfer, H. Naseem and M. Danish, *Int. J. Eng. Adv. Technol.*, 2015, **4**, 80–93.

47 C. Hora, F. C. Dan, N. Rancov, G. E. Badea and C. Secui, *Energies*, 2022, **15**, 6076.

48 L. Pérez Orosa, E. Chinarro, D. Guinea and M. C. García-Alegre, *Energies*, 2022, **15**, 5888.

49 B. Jenkins, D. Squires, J. Barton, D. Strickland, K. Wijayantha, J. Carroll, J. Wilson, M. Brenton and M. Thomson, *Energies*, 2022, **15**, 5796.

50 A. Saravanan, S. Karishma, P. S. Kumar, P. Yaashikaa, S. Jeevanantham and B. Gayathri, *Biomass Convers. Biorefin.*, 2020, 1–21.

51 A. M. Elgarahy, M. Eloffy, A. Hammad, A. N. Saber, D. M. El-Sherif, A. Mohsen, M. Abouzid and K. Z. Elwakeel, *Environ. Chem. Lett.*, 2022, **20**, 3453–3504.

52 S. M. Saba, M. Müller, M. Robinius and D. Stolten, *Int. J. Hydrogen Energy*, 2018, **43**, 1209–1223.

53 Y. Liu, F. Wang, Z. Jiao, S. Bai, H. Qiu and L. Guo, *Electrochem. Energy Rev.*, 2022, **5**, 5.

54 J. Wang, Z. Zhang, J. Ding, C. Zhong, Y. Deng, X. Han and W. Hu, *Sci. China Mater.*, 2021, **64**, 1–26.

55 H.-Y. Wang, C.-C. Weng, J.-T. Ren and Z.-Y. Yuan, *Front. Chem. Sci. Eng.*, 2021, 1–19.

56 D. V. Esposito, *Joule*, 2017, **1**, 651–658.

57 M. Gong, D.-Y. Wang, C.-C. Chen, B.-J. Hwang and H. Dai, *Nano Res.*, 2016, **9**, 28–46.

58 X. Li, L. Zhao, J. Yu, X. Liu, X. Zhang, H. Liu and W. Zhou, *Nano-Micro Lett.*, 2020, **12**, 1–29.

59 S. Atilhan, S. Park, M. M. El-Halwagi, M. Atilhan, M. Moore and R. B. Nielsen, *Curr. Opin. Chem. Eng.*, 2021, **31**, 100668.

60 F. Mödinger, *InterCeram: Int. Ceram. Rev.*, 2021, **70**, 32–37.

61 B. S. Thapa and B. Thapa, *J. Phys.: Conf. Ser.*, 2020, **1608**, 012020.

62 Y. Zhao, V. McDonell and S. Samuelsen, *Int. J. Hydrogen Energy*, 2020, **45**, 11368–11379.

63 H. Balat and E. Kırtay, *Int. J. Hydrogen Energy*, 2010, **35**, 7416–7426.

64 L. Hu, G. r. Lindbergh and C. Lagergren, *J. Phys. Chem. C*, 2016, **120**, 13427–13433.

65 L. Barelli, G. Bidini, G. Cinti and J. Milewski, *Int. J. Hydrogen Energy*, 2021, **46**, 14922–14931.

66 D. Penchini, G. Cinti, G. Discepoli and U. Desideri, *Int. J. Hydrogen Energy*, 2014, **39**, 9457–9466.

67 A. Monforti Ferrario, F. Santoni, M. Della Pietra, M. Rossi, N. Piacente, G. Comodi and L. Simonetti, *Front. Energy Res.*, 2021, **9**, 655915.

68 S. Dresp, T. N. Thanh, M. Klingenhof, S. Brückner, P. Hauke and P. Strasser, *Energy Environ. Sci.*, 2020, **13**, 1725–1729.

69 G. E. Badea, I. Maior, A. Cojocaru and I. Corbu, *Rev. Roum. Chim.*, 2007, **52**, 1123–1130.

70 A. Cojocaru, G. E. Badea, I. Maior, P. Creț and T. Badea, *Rev. Roum. Chim.*, 2009, **54**, 49–54.

71 G. E. Badea, I. Maior, A. Cojocaru, I. Pantea and T. Badea, *Rev. Roum. Chim.*, 2009, **54**, 55–61.

72 W. Zang, T. Sun, T. Yang, S. Xi, M. Waqar, Z. Kou, Z. Lyu, Y. P. Feng, J. Wang and S. J. Pennycook, *Adv. Mater.*, 2021, **33**, 2003846.

73 V. V. Kuznetsov, B. I. Podlovchenko, K. V. Frolov, M. A. Volkov and D. A. Khanin, *J. Solid State Electrochem.*, 2022, **26**, 2183–2193.

74 S. Farhangi, S. Ebrahimi and M. S. Niasar, *Biotechnol. Lett.*, 2014, **36**, 1987–1992.

75 S. H. Hsu, J. Miao, L. Zhang, J. Gao, H. Wang, H. Tao, S. F. Hung, A. Vasileff, S. Z. Qiao and B. Liu, *Adv. Mater.*, 2018, **30**, 1707261.

76 C. Zhang, D. Li and Y. Xu, *J. Mater. Res.*, 2022, **37**, 807–817.

77 Z. Chen, D. Liu, Y. Gao, Y. Zhao, W. Xiao, G. Xu, T. Ma, Z. Wu and L. Wang, *Sci. China Mater.*, 2022, **65**, 1217–1224.

78 Q. Xiong, X. Zhang, Q. Cheng, G. Liu, G. Xu, J. Li, X. Ye and H. Gao, *Nano Res.*, 2021, **14**, 1443–1449.

79 H. Xie, C. Lan, B. Chen, F. Wang and T. Liu, *Nano Res.*, 2020, **13**, 3321–3329.

80 L. Dong, G.-R. Chang, Y. Feng, X.-Z. Yao and X.-Y. Yu, *Rare Met.*, 2022, 1–12.

81 J. Li, M. Song, Y. Hu, C. Zhang, W. Liu, X. Huang, J. Zhang, Y. Zhu, J. Zhang and D. Wang, *Nano Res.*, 2023, **16**, 3658–3664.

82 G. Wang, Y. Sun, Y. Zhao, Y. Zhang, X. Li, L. Fan and Y. Li, *Nano Res.*, 2022, **15**, 8771–8782.

83 Y. Chen, P. Sun and W. Xing, *J. Chem. Sci.*, 2019, **131**, 1–8.

84 D. Liang, Y. Liu, S. Peng, F. Lan, S. Lu and Y. Xiang, *Front. Environ. Sci. Eng.*, 2014, **8**, 624–630.

85 Q. Yu, J. Chi, G. Liu, X. Wang, X. Liu, Z. Li, Y. Deng, X. Wang and L. Wang, *Sci. China Mater.*, 2022, **65**, 1539–1549.

86 Q. Liu, S. Sun, L. Zhang, Y. Luo, Q. Yang, K. Dong, X. Fang, D. Zheng, A. A. Alshehri and X. Sun, *Nano Res.*, 2022, **15**, 8922–8927.

87 C. González-Buch, I. Herraiz-Cardona, E. Ortega, J. García-Antón and V. Pérez-Herranz, *J. Appl. Electrochem.*, 2016, **46**, 791–803.

88 A. Laszczyńska and I. Szczygieł, *Int. J. Hydrogen Energy*, 2020, **45**, 508–520.

89 S. Wang, M. Wang, Z. Liu, S. Liu, Y. Chen, M. Li, H. Zhang, Q. Wu, J. Guo and X. Feng, *ACS Appl. Mater. Interfaces*, 2022, **14**, 15250–15258.

90 L. Yu, L. Wu, S. Song, B. McElhenny, F. Zhang, S. Chen and Z. Ren, *ACS Energy Lett.*, 2020, **5**, 2681–2689.

91 H. Li, Q. Tang, B. He and P. Yang, *J. Mater. Chem. A*, 2016, **4**, 6513–6520.

92 J. Zheng, Y. Zhao, H. Xi and C. Li, *RSC Adv.*, 2018, **8**, 9423–9429.

93 S. Gao, G.-D. Li, Y. Liu, H. Chen, L.-L. Feng, Y. Wang, M. Yang, D. Wang, S. Wang and X. Zou, *Nanoscale*, 2015, **7**, 2306–2316.

94 X. Wu, S. Zhou, Z. Wang, J. Liu, W. Pei, P. Yang, J. Zhao and J. Qiu, *Adv. Energy Mater.*, 2019, **9**, 1901333.

95 J. Miao, Z. Lang, X. Zhang, W. Kong, O. Peng, Y. Yang, S. Wang, J. Cheng, T. He and A. Amini, *Adv. Funct. Mater.*, 2019, **29**, 1805893.

96 Y. Zhao, B. Jin, Y. Zheng, H. Jin, Y. Jiao and S. Z. Qiao, *Adv. Energy Mater.*, 2018, **8**, 1801926.

97 Y. Jiao, H. Yan, D. Wang, X. Wang, S. Xu, Y. Xie, A. Wu, L. Jiang, C. Tian and R. Wang, *Sci. China Mater.*, 2022, **65**, 1225–1236.

98 A. R. Jadhav, A. Kumar, J. Lee, T. Yang, S. Na, J. Lee, Y. Luo, X. Liu, Y. Hwang and Y. Liu, *J. Mater. Chem. A*, 2020, **8**, 24501–24514.

99 Y. Zhao, B. Jin, A. Vasileff, Y. Jiao and S.-Z. Qiao, *J. Mater. Chem. A*, 2019, **7**, 8117–8121.

100 L. Chen and J. Shi, *Sci. China Mater.*, 2022, **65**, 1–9.

101 J. Hnát, M. Paidar and K. Bouzek, in *Current Trends and Future Developments on (Bio-) Membranes*, Elsevier, 2020, pp. 91–117.

102 B. Dunn, H. Kamath and J.-M. Tarascon, *Science*, 2011, **334**, 928–935.

103 N. S. Lewis and D. G. Nocera, *Proc. Natl. Acad. Sci. U. S. A.*, 2006, **103**, 15729–15735.

104 I. Roger, M. A. Shipman and M. D. Symes, *Nat. Rev. Chem.*, 2017, **1**, 0003.

105 R. Gao and D. Yan, *Adv. Energy Mater.*, 2020, **10**, 1900954.

106 R. Gao, J. Zhu and D. Yan, *Nanoscale*, 2021, **13**, 13593–13603.

107 Z. Guo, W. Ye, X. Fang, J. Wan, Y. Ye, Y. Dong, D. Cao and D. Yan, *Inorg. Chem. Front.*, 2019, **6**, 687–693.

108 X.-W. Lv, Z.-P. Hu, L. Chen, J.-T. Ren, Y.-P. Liu and Z.-Y. Yuan, *ACS Sustainable Chem. Eng.*, 2019, **7**, 12770–12778.

109 Y. Zheng, Y. Jiao, A. Vasileff and S. Z. Qiao, *Angew. Chem., Int. Ed.*, 2018, **57**, 7568–7579.

110 J.-T. Ren, Y. Yao and Z.-Y. Yuan, *Green Energy Environ.*, 2021, **6**, 620–643.

111 M. A. Mushtaq, M. Arif, G. Yasin, M. Tabish, A. Kumar, S. Ibraheem, W. Ye, S. Ajmal, J. Zhao and P. Li, *Renewable Sustainable Energy Rev.*, 2023, **176**, 113197.

112 M. A. Mushtaq, A. Kumar, G. Yasin, M. Arif, M. Tabish, S. Ibraheem, X. Cai, W. Ye, X. Fang and A. Saad, *Appl. Catal., B*, 2022, **317**, 121711.

113 J.-W. Zhang, H. Zhang, T.-Z. Ren, Z.-Y. Yuan and T. J. Bandosz, *Front. Chem. Sci. Eng.*, 2021, **15**, 279–287.

114 J. Wang, S.-J. Kim, J. Liu, Y. Gao, S. Choi, J. Han, H. Shin, S. Jo, J. Kim and F. Ciucci, *Nat. Catal.*, 2021, **4**, 212–222.

115 J. Rossmeisl, A. Logadottir and J. K. Nørskov, *Chem. Phys.*, 2005, **319**, 178–184.

116 C. C. Weng, J. T. Ren and Z. Y. Yuan, *ChemSusChem*, 2020, **13**, 3357–3375.

117 J.-T. Ren, Y.-J. Song and Z.-Y. Yuan, *J. Energy Chem.*, 2019, **32**, 78–84.

118 J. A. Turner, *Science*, 2004, **305**, 972–974.

119 C. Xiang, K. M. Papadantonakis and N. S. Lewis, *Mater. Horiz.*, 2016, **3**, 169–173.

120 M. Cuartero, G. Crespo, T. Cherubini, N. Pankratova, F. Confalonieri, F. Massa, M.-L. Tercier-Waeber, M. Abdou, J. r. Schäfer and E. Bakker, *Anal. Chem.*, 2018, **90**, 4702–4710.

121 Z. Wang, Y. Gu and L. Wang, *Front. Energy*, 2021, **15**, 596–599.

122 F. Esmaeilion, *Appl. Water Sci.*, 2020, **10**, 84.

123 Y. Kuang, M. J. Kenney, Y. Meng, W.-H. Hung, Y. Liu, J. E. Huang, R. Prasanna, P. Li, Y. Li and L. Wang, *Proc. Natl. Acad. Sci. U. S. A.*, 2019, **116**, 6624–6629.

124 R. A. Evrin and I. Dincer, *Energy Storage*, 2020, **2**, e195.

125 A. Headley, G. Randolf, M. Virji and M. Ewan, *MRS Energy Sustainability*, 2020, **7**, E26.

126 F. Musharavati, P. Ahmadi and S. Khanmohammadi, *J. Therm. Anal. Calorim.*, 2021, **145**, 1673–1689.

127 S. Serag and A. Echchelh, *Technol. Econ. Smart Grids Sustain. Energy*, 2022, **7**, 30.

128 K. Meier, *Int. J. Energy Environ. Eng.*, 2014, **5**, 1–12.

129 Y. Gao, W. Yao, J. Wang and Z. Cui, *J. Therm. Sci.*, 2023, **32**, 93–108.

130 S. Rarotra, T. K. Mandal and D. Bandyopadhyay, *Energy Technol.*, 2017, **5**, 1208–1217.

131 M. R. Omidvar, A. H. Meghdadi Isfahani, R. Kumar, A. Mohammadidoust and A. Bewoor, *Biomass Convers. Biorefin.*, 2021, 1–19.

132 M. Rezaei, A. Mostafaeipour, M. Qolipour and M. Momeni, *Front. Energy*, 2019, **13**, 539–550.

133 P. D. Cavaliere, A. Perrone and A. Silvello, *Metals*, 2021, **11**, 1816.

134 R. Banik and P. Das, *J. Inst. Eng. (India): Ser. B*, 2020, **101**, 527–539.

135 S. Furfari and A. Clerici, *Eur. Phys. J. Plus*, 2021, **136**, 509.

136 S. Chai, G. Zhang, G. Li and Y. Zhang, *Clean Technol. Environ. Policy*, 2021, **23**, 1931–1946.

137 K. Jing, C. Liu, X. Cao, H. Sun and Y. Dong, *J. Electr. Eng. Technol.*, 2021, **16**, 2355–2365.

138 H. Niaz, M. M. Lakouraj and J. Liu, *Korean J. Chem. Eng.*, 2021, **38**, 1617–1630.

139 S. Rawat, B. Jha and M. K. Panda, *Iran. J. Sci. Technol., Trans. Electr. Eng.*, 2018, **42**, 403–417.

140 M. G. Shirkoohi, R. D. Tyagi, P. A. Vanrolleghem and P. Drogui, *J. Environ. Health Sci. Eng.*, 2022, **20**, 1089–1109.

141 J. Brauns and T. Turek, *Processes*, 2020, **8**, 248.

142 L. Vidas and R. Castro, *Appl. Sci.*, 2021, **11**, 11363.

143 O. Schmidt, A. Gambhir, I. Staffell, A. Hawkes, J. Nelson and S. Few, *Int. J. Hydrogen Energy*, 2017, **42**, 30470–30492.

144 R. Vakulchuk, I. Overland and D. Scholten, *Renewable Sustainable Energy Rev.*, 2020, **122**, 109547.

145 M. Ingram, B. Baron and G. Janz, *Electrochim. Acta*, 1966, **11**, 1629–1639.

146 H. Bartlett and K. Johnson, *J. Electrochem. Soc.*, 1967, **114**, 457.

147 B. Kaplan, H. Groult, A. Barhoun, F. Lantelme, T. Nakajima, V. Gupta, S. Komaba and N. Kumagai, *J. Electrochem. Soc.*, 2002, **149**, D72.

148 V. Kaplan, E. Wachtel, K. Gartsman, Y. Feldman and I. Lubomirsky, *J. Electrochem. Soc.*, 2010, **157**, B552.

149 H. V. Ijije, C. Sun and G. Z. Chen, *Carbon*, 2014, **73**, 163–174.

150 H. V. Ijije, R. C. Lawrence, N. J. Siambun, S. M. Jeong, D. A. Jewell, D. Hu and G. Z. Chen, *Faraday Discuss.*, 2014, **172**, 105–116.

151 H. V. Ijije, R. C. Lawrence and G. Z. Chen, *RSC Adv.*, 2014, **4**, 35808–35817.

152 D. Chery, V. Albin, V. Lair and M. Cassir, *Int. J. Hydrogen Energy*, 2014, **39**, 12330–12339.

153 D. Chery, V. Lair and M. Cassir, *Electrochim. Acta*, 2015, **160**, 74–81.

154 J. Ren, F.-F. Li, J. Lau, L. González-Urbina and S. Licht, *Nano Lett.*, 2015, **15**, 6142–6148.

155 J. Ren, J. Lau, M. Lefler and S. Licht, *J. Phys. Chem. C*, 2015, **119**, 23342–23349.

156 J. P. Perez-Trujillo, F. Elizalde-Blancas, M. Della Pietra and S. J. McPhail, *Appl. Energy*, 2018, **226**, 1037–1055.

157 J. P. Pérez-Trujillo, F. Elizalde-Blancas, S. J. McPhail, M. Della Pietra and B. Bosio, *Appl. Energy*, 2020, **263**, 114630.

158 L. Hu, I. Rexed, G. Lindbergh and C. Lagergren, *Int. J. Hydrogen Energy*, 2014, **39**, 12323–12329.

159 E. Audasso, K. I. Kim, G. Accardo, H. S. Kim and S. P. Yoon, *J. Power Sources*, 2022, **523**, 231039.

160 W. Dönitz and E. Erdle, *Int. J. Hydrogen Energy*, 1985, **10**, 291–295.

161 A. Nechache and S. Hody, *Renewable Sustainable Energy Rev.*, 2021, **149**, 111322.

162 Y. Zheng, Z. Chen and J. Zhang, *Electrochem. Energy Rev.*, 2021, **4**, 508–517.

163 Y. Li, L. Zhang, B. Yu, J. Zhu and C. Wu, *Engineering*, 2023, **21**, 101–114.

164 D. Guban, I. K. Muritala, M. Roeb and C. Sattler, *Int. J. Hydrogen Energy*, 2020, **45**, 26156–26165.

165 M. Schalenbach, A. R. Zeradjanin, O. Kasian, S. Cherevko and K. J. Mayrhofer, *Int. J. Electrochem. Sci.*, 2018, **13**, 1173–1226.

166 M. Wang, G. Wang, Z. Sun, Y. Zhang and D. Xu, *Global Energy Interconnect.*, 2019, **2**, 436–443.

167 V. Romano, G. D'Angelo, S. Perathoner and G. Centi, *Energy Environ. Sci.*, 2021, **14**, 5760–5787.

168 A. Ursúa Rubio, L. Gandía Pascual and P. Sanchis Gúrpide, *Proc. IEEE*, 2012, **100**(2), 2012.

169 Z. Liu, S. D. Sajjad, Y. Gao, H. Yang, J. J. Kaczur and R. I. Masel, *Int. J. Hydrogen Energy*, 2017, **42**, 29661–29665.

170 K. Zeng and D. Zhang, *Prog. Energy Combust. Sci.*, 2010, **36**, 307–326.

171 S. Marini, P. Salvi, P. Nelli, R. Pesenti, M. Villa, M. Berrettoni, G. Zangari and Y. Kiros, *Electrochim. Acta*, 2012, **82**, 384–391.

172 IRENA, International Renewable Energy Agency, Abu Dhabi, 2020, https://www.irena.org/-/media/Files/IRENA/Agency/Publication/2020/Dec/IRENA_Green_hydrogen_cost_2020.pdf.

173 D. Jones and C. W. Dunnill, *ChemRxiv*, 2021, preprint, DOI: 10.26434/chemrxiv.13547813.v1.

174 D. Pletcher and X. Li, *Int. J. Hydrogen Energy*, 2011, **36**, 15089–15104.

175 M. R. Kraglund, D. Aili, K. Jankova, E. Christensen, Q. Li and J. O. Jensen, *J. Electrochem. Soc.*, 2016, **163**, F3125.

176 S. H. Ahn, S. J. Yoo, H.-J. Kim, D. Henkensmeier, S. W. Nam, S.-K. Kim and J. H. Jang, *Appl. Catal., B*, 2016, **180**, 674–679.

177 Y. Leng, G. Chen, A. J. Mendoza, T. B. Tighe, M. A. Hickner and C.-Y. Wang, *J. Am. Chem. Soc.*, 2012, **134**, 9054–9057.

178 Z. Xu, C.-L. Yeh, J.-L. Chen, J. T. Lin, K.-C. Ho and R. Y.-Y. Lin, *ACS Sustainable Chem. Eng.*, 2022, **10**, 11577–11586.

179 S. Liu, B. Li, S. V. Mohite, P. Devaraji, L. Mao and R. Xing, *Int. J. Hydrogen Energy*, 2020, **45**, 29929–29937.

180 L. Bertuccioli, A. Chan, D. Hart, F. Lehner, B. Madden and E. Standen, *Development of water electrolysis in the European Union*, Element Energy, E4tech Sarl, Cambridge (UK), Lausanne (CH), 2014.

181 S. S. Kumar and V. Himabindu, *Mater. Sci. Energy Technol.*, 2019, **2**, 442–454.

182 L. Nuttall, A. Fickett and W. Titterington, *Hydrogen Energy: Part A*, 1975, 441–455.

183 W. Grubb, *J. Electrochem. Soc.*, 1959, **106**, 275.

184 W. Grubb and L. Niedrach, *J. Electrochem. Soc.*, 1960, **107**, 131.

185 K. Ayers, N. Danilovic, K. Harrison and H. Xu, *Electrochem. Soc. Interface*, 2021, **30**, 67.

186 W. Xu and K. Scott, *Int. J. Hydrogen Energy*, 2010, **35**, 12029–12037.

187 M. T. Giacomini, M. Balasubramanian, S. Khalid, J. McBreen and E. Ticianellia, *J. Electrochem. Soc.*, 2003, **150**, A588.

188 C. Rozain, E. Mayousse, N. Guillet and P. Millet, *Appl. Catal., B*, 2016, **182**, 153–160.

189 L. Yin, T. Yang, X. Ding, M. He, W. Wei, T. Yu and H. Zhao, *Electrochem. Commun.*, 2018, **94**, 59–63.

190 M. Bühler, P. Holzapfel, D. McLaughlin and S. Thiele, *J. Electrochem. Soc.*, 2019, **166**, F1070.

191 E. V. dos Santos and O. Scialdone, in *Electrochemical Water and Wastewater Treatment*, Elsevier, 2018, pp. 239–266.

192 M. Sillanpaa and M. Shestakova, *Electrochemical water treatment methods: Fundamentals, methods and full scale applications*, Butterworth-Heinemann, 2017.

193 S. Z. Baykara, *Int. J. Hydrogen Energy*, 2018, **43**, 10605–10614.

194 H. Ju, S. Badwal and S. Giddey, *Appl. Energy*, 2018, **231**, 502–533.

195 S. Grigoriev, P. Millet and V. Fateev, *J. Power Sources*, 2008, **177**, 281–285.

196 J. B. Benziger, M. B. Satterfield, W. H. Hogarth, J. P. Nehlsen and I. G. Kevrekidis, *J. Power Sources*, 2006, **155**, 272–285.

197 D. Li, E. J. Park, W. Zhu, Q. Shi, Y. Zhou, H. Tian, Y. Lin, A. Serov, B. Zulevi and E. D. Baca, *Nat. Energy*, 2020, **5**, 378–385.

198 G.-F. Li, M. Divinagracia, M. F. Labata, J. D. Ocon and P.-Y. Abel Chuang, *ACS Appl. Mater. Interfaces*, 2019, **11**, 33748–33758.

199 M. Manolova, C. Schoeberl, R. Freudenberger, C. Ellwein, J. Kerres, S. Stypka and B. Oberschachtsiek, *Int. J. Hydrogen Energy*, 2015, **40**, 11362–11369.

200 A. Miller, L. Singh, L. Wang and H. Liu, *Environ. Int.*, 2019, **126**, 611–618.

201 J. Parrondo, C. G. Arges, M. Niedzwiecki, E. B. Anderson, K. E. Ayers and V. Ramani, *RSC Adv.*, 2014, **4**, 9875–9879.

202 J. E. Park, S. Y. Kang, S.-H. Oh, J. K. Kim, M. S. Lim, C.-Y. Ahn, Y.-H. Cho and Y.-E. Sung, *Electrochim. Acta*, 2019, **295**, 99–106.

203 C. C. Pavel, F. Cecconi, C. Emiliani, S. Santiccioli, A. Scaffidi, S. Catanorchi and M. Comotti, *Angew. Chem., Int. Ed.*, 2014, **53**, 1378–1381.

204 I. Vincent, A. Kruger and D. Bessarabov, *Int. J. Hydrogen Energy*, 2017, **42**, 10752–10761.

205 I. Vincent, E.-C. Lee and H.-M. Kim, *RSC Adv.*, 2020, **10**, 37429–37438.

206 I. Vincent and D. Bessarabov, *Renewable Sustainable Energy Rev.*, 2018, **81**, 1690–1704.

207 D. Zhang and K. Zeng, *Ind. Eng. Chem. Res.*, 2012, **51**, 13825–13832.

208 L. Wang, T. Weissbach, R. Reissner, A. Ansar, A. S. Gago, S. Holdcroft and K. A. Friedrich, *ACS Appl. Energy Mater.*, 2019, **2**, 7903–7912.

209 S. Dunn, *Int. J. Hydrogen Energy*, 2002, **27**, 235–264.

210 C. Acar and I. Dincer, *Int. J. Hydrogen Energy*, 2022, **47**, 40118–40137.

211 W. Brattain and C. Garrett, *Bell Syst. Tech. J.*, 1955, **34**, 129–176.

212 M. Grätzel, *Nature*, 2001, **414**, 338–344.

213 K. Kalyanasundaram, *Sol. Cells*, 1985, **15**, 93–156.

214 A. Fujishima and K. Honda, *Nature*, 1972, **238**, 37–38.

215 F. A. Frame, E. C. Carroll, D. S. Larsen, M. Sarahan, N. D. Browning and F. E. Osterloh, *Chem. Commun.*, 2008, 2206–2208.

216 X. Chen, S. Shen, L. Guo and S. S. Mao, *Chem. Rev.*, 2010, **110**, 6503–6570.

217 A. Iwase, S. Yoshino, T. Takayama, Y. H. Ng, R. Amal and A. Kudo, *J. Am. Chem. Soc.*, 2016, **138**, 10260–10264.

218 M. Woodhouse, G. Herman and B. Parkinson, *Chem. Mater.*, 2005, **17**, 4318–4324.

219 S. Baeck, T. Jaramillo, C. Brändli and E. McFarland, *J. Comb. Chem.*, 2002, **4**, 563–568.

220 B. Parkinson, *Energy Environ. Sci.*, 2010, **3**, 509–511.

221 X. Chen, L. Liu, P. Y. Yu and S. S. Mao, *Science*, 2011, **331**, 746–750.

222 K. Maeda and K. Domen, *J. Phys. Chem. Lett.*, 2010, **1**, 2655–2661.

223 D. Bokov, A. Turki Jalil, S. Chupradit, W. Suksatan, M. Javed Ansari, I. H. Shewael, G. H. Valiev and E. Kianfar, *Adv. Mater. Sci. Eng.*, 2021, **2021**, 1–21.

224 T. J. Jacobsson, V. Fjällström, M. Sahlberg, M. Edoff and T. Edvinsson, *Energy Environ. Sci.*, 2013, **6**, 3676–3683.

225 O. Khaselev, A. Bansal and J. Turner, *Int. J. Hydrogen Energy*, 2001, **26**, 127–132.

226 J. Brillet, J.-H. Yum, M. Cornuz, T. Hisatomi, R. Solarska, J. Augustynski, M. Graetzel and K. Sivula, *Nat. Photonics*, 2012, **6**, 824–828.

227 S. Y. Reece, J. A. Hamel, K. Sung, T. D. Jarvi, A. J. Esswein, J. J. Pijpers and D. G. Nocera, *science*, 2011, **334**, 645–648.

228 F. F. Abdi, L. Han, A. H. Smets, M. Zeman, B. Dam and R. Van De Krol, *Nat. Commun.*, 2013, **4**, 2195.

229 F. H. Saadi, N. S. Lewis and E. W. McFarland, *Energy Environ. Sci.*, 2018, **11**, 469–475.

230 J. T. Hinkley, J. A. O'Brien, C. J. Fell and S.-E. Lindquist, *Int. J. Hydrogen Energy*, 2011, **36**, 11596–11603.

231 A. Buttler and H. Spliethoff, *Renewable Sustainable Energy Rev.*, 2018, **82**, 2440–2454.

232 A. T-Raissi and D. L. Block, *IEEE Power Energy Mag.*, 2004, **2**, 40–45.

233 T. Nguyen, Z. Abdin, T. Holm and W. Mérida, *Energy Convers. Manage.*, 2019, **200**, 112108.

234 C. C. Elam, C. E. G. Padró, G. Sandrock, A. Luzzi, P. Lindblad and E. F. Hagen, *Int. J. Hydrogen Energy*, 2003, **28**, 601–607.

235 J. Romm, *Energy Policy*, 2006, **34**, 2609–2614.

236 R. Bhandari, C. A. Trudewind and P. Zapp, *J. Cleaner Prod.*, 2014, **85**, 151–163.

237 I. Sorrenti, Y. Zheng, A. Singlitico and S. You, *Renewable Sustainable Energy Rev.*, 2023, **171**, 113033.

238 M. Z. Jacobson, W. Colella and D. Golden, *Science*, 2005, **308**, 1901–1905.

239 C. Acar and I. Dincer, *Int. J. Glob. Warm.*, 2017, **13**, 260–277.

240 C. Jørgensen and S. Ropenus, *Int. J. Hydrogen Energy*, 2008, **33**, 5335–5344.

241 Ø. Ulleberg, T. Nakken and A. Ete, *Int. J. Hydrogen Energy*, 2010, **35**, 1841–1852.

242 H. De Battista, R. J. Mantz and F. Garelli, *J. Power Sources*, 2006, **155**, 478–486.

243 G. Weidong, *Int. J. Hydrogen Energy*, 2011, **37**, 737–740.

244 P. Denholm, G. L. Kulcinski and T. Holloway, *Environ. Sci. Technol.*, 2005, **39**, 1903–1911.

245 J. Sarkar and S. Bhattacharyya, *Arch. Thermodyn.*, 2012, **33**, 23–40.

246 J. Linnemann and R. Steinberger-Wilckens, *Int. J. Hydrogen Energy*, 2007, **32**, 1492–1499.

247 A. González, E. McKeogh and B. Gallachoir, *Renewable Energy*, 2004, **29**, 471–489.

248 R. Gazey, S. Salman and D. Aklil-D'Halluin, *J. Power Sources*, 2006, **157**, 841–847.

249 S. Shaw and E. Peteves, *Int. J. Hydrogen Energy*, 2008, **33**, 3249–3263.

250 T. J. Wallington, M. Grahn, J. E. Anderson, S. A. Mueller, M. Williander and K. Lindgren, *Environ. Sci. Technol.*, 2010, **44**, 2702–2708.

251 K. B. Martin and S. E. Grasman, *Int. J. Hydrogen Energy*, 2009, **34**, 6581–6588.

252 M. Granovskii, I. Dincer and M. A. Rosen, *J. Power Sources*, 2006, **157**, 411–421.

253 M. Granovskii, I. Dincer and M. A. Rosen, *Int. J. Hydrogen Energy*, 2007, **32**, 927–931.

254 M. Aguado, E. Ayerbe, C. Azcárate, R. Blanco, R. Garde, F. Mallor and D. M. Rivas, *Int. J. Hydrogen Energy*, 2009, **34**, 2845–2854.

255 K. Harrison, G. Martin, T. Ramsden, W. Kramer and F. Novachek, *Wind-to-Hydrogen Project: Operational Experience, Performance Testing, and Systems Integration*, National Renewable Energy Lab. (NREL), Golden, CO, United States, 2009.

256 T. Take, K. Tsurutani and M. Umeda, *J. Power Sources*, 2007, **164**, 9–16.

257 X.-W. Fang, L. Wang, W.-F. Cai, D.-W. Jing, Q.-Y. Chen and Y.-H. Wang, *Int. J. Hydrogen Energy*, 2019, **44**, 15766–15770.

258 Z. Hu, M. Wu, Z. Wei, S. Song and P. K. Shen, *J. Power Sources*, 2007, **166**, 458–461.

259 E. Rasten, G. Hagen and R. Tunold, *Electrochim. Acta*, 2003, **48**, 3945–3952.

260 D. L. Stojić, M. P. Marčeta, S. P. Sovilj and Š. S. Miljanić, *J. Power Sources*, 2003, **118**, 315–319.

261 S. Grigor'ev, V. Porembskii and V. Fateev, *Chem. Pet. Eng.*, 2004, **40**, 606–610.

262 H. Deligöz, S. Yılmaztürk, T. Karaca, H. Özdemir, S. N. Koc, F. Öksüzömer, A. Durmuş and M. A. Gürkaynak, *J. Membr. Sci.*, 2009, **326**, 643–649.

263 W. C. Choi, J. D. Kim and S. I. Woo, *J. Power Sources*, 2001, **96**, 411–414.

264 L. Jörissen, V. Gogel, J. Kerres and J. Garche, *J. Power Sources*, 2002, **105**, 267–273.

265 X. Ma, J. Wang, D. Liu, R. Kong, S. Hao, G. Du, A. M. Asiri and X. Sun, *New J. Chem.*, 2017, **41**, 4754–4757.

266 Z. Wang, L. Xu, F. Huang, L. Qu, J. Li, K. A. Owusu, Z. Liu, Z. Lin, B. Xiang and X. Liu, *Adv. Energy Mater.*, 2019, **9**, 1900390.

267 C. Wang, H. Lu, Z. Mao, C. Yan, G. Shen and X. Wang, *Adv. Funct. Mater.*, 2020, **30**, 2000556.

268 Y. Song, W. Xie, Y. Song, H. Li, S. Li, S. Jiang, J. Y. Lee and M. Shao, *Appl. Catal., B*, 2022, **312**, 121400.

269 Y. Wang, Y. Liu, D. Wiley, S. Zhao and Z. Tang, *J. Mater. Chem. A*, 2021, **9**, 18974–18993.

270 I. Dincer and C. Acar, *Int. J. Hydrogen Energy*, 2018, **43**, 8579–8599.

271 I. Dincer and C. Acar, *Int. J. Hydrogen Energy*, 2015, **40**, 11094–11111.

272 F. Dawood, M. Anda and G. Shafiullah, *Int. J. Hydrogen Energy*, 2020, **45**, 3847–3869.

273 M. Ji and J. Wang, *Int. J. Hydrogen Energy*, 2021, **46**, 38612–38635.

274 M. McPherson, N. Johnson and M. Strubegger, *Appl. Energy*, 2018, **216**, 649–661.

275 R. S. El-Emam and H. Özcan, *J. Cleaner Prod.*, 2019, **220**, 593–609.

276 T. Sinigaglia, F. Lewiski, M. E. S. Martins and J. C. M. Siluk, *Int. J. Hydrogen Energy*, 2017, **42**, 24597–24611.

277 A. Mehmeti, A. Angelis-Dimakis, G. Arampatzis, S. J. McPhail and S. Ulgiati, *Environments*, 2018, **5**, 24.

278 O. Siddiqui and I. Dincer, *Int. J. Hydrogen Energy*, 2019, **44**, 5773–5786.

279 C. Acar and I. Dincer, *J. Cleaner Prod.*, 2019, **218**, 835–849.

280 R. E. Kopp and B. K. Mignone, *Economics*, 2012, **6**, 20120015.

281 F. C. Moore, U. Baldos, T. Hertel and D. Diaz, *Nat. Commun.*, 2017, **8**, 1607.

282 Y. Cai and T. S. Lontzek, *J. Pol. Econ.*, 2019, **127**, 2684–2734.

283 R. S. Pindyck, *J. Environ. Econ. Manag.*, 2019, **94**, 140–160.

284 M. Adler, D. Anthoff, V. Bosetti, G. Garner, K. Keller and N. Treich, *Nat. Clim. Change*, 2017, **7**, 443–449.

285 M. A. DeLuchi, *Int. J. Hydrogen Energy*, 1989, **14**, 81–130.

286 M. Momirlan and T. N. Veziroglu, *Int. J. Hydrogen Energy*, 2005, **30**, 795–802.

287 M. Momirlan and T. Veziroglu, *Renewable Sustainable Energy Rev.*, 2002, **6**, 141–179.

288 J. Hord, *Int. J. Hydrogen Energy*, 1980, **5**, 579–584.

289 L. Zhou, *Renewable Sustainable Energy Rev.*, 2005, **9**, 395–408.

290 H. J. Pasman and W. J. Rogers, *J. Loss Prev. Process Ind.*, 2010, **23**, 697–704.

291 D. Das and T. N. Veziroglu, *Int. J. Hydrogen Energy*, 2008, **33**, 6046–6057.

292 J. Zheng, X. Liu, P. Xu, P. Liu, Y. Zhao and J. Yang, *Int. J. Hydrogen Energy*, 2012, **37**, 1048–1057.

293 A. Züttel, *Mater. Today*, 2003, **6**, 24–33.

294 B. Sakintuna, F. Lamari-Darkrim and M. Hirscher, *Int. J. Hydrogen Energy*, 2007, **32**, 1121–1140.

295 G. Marbán and T. Valdés-Solís, *Int. J. Hydrogen Energy*, 2007, **32**, 1625–1637.

296 J. Van Mierlo, G. Maggetto and P. Lataire, *Energy Convers. Manage.*, 2006, **47**, 2748–2760.

297 I. Dincer and C. Acar, *Int. J. Hydrogen Energy*, 2017, **42**, 14843–14864.

298 M. Fereidooni, A. Mostafaeipour, V. Kalantar and H. Goudarzi, *Renewable Sustainable Energy Rev.*, 2018, **82**, 415–423.

299 C. Acar, A. Beskese and G. T. Temur, *Int. J. Hydrogen Energy*, 2018, **43**, 18059–18076.

300 Y. Lim, C.-J. Lee, Y. S. Jeong, I. H. Song, C. J. Lee and C. Han, *Ind. Eng. Chem. Res.*, 2012, **51**, 4982–4989.

301 C. Acar and I. Dincer, *Causes, impacts and solutions to global warming*, 2013, pp. 493–514.

302 R. S. El-Emam, H. Ozcan and C. Zamfirescu, *J. Cleaner Prod.*, 2020, **262**, 121424.

303 B. Ewan, D. Graf, N. Monnerie, C. Sattler, F. Le Naour, W. Stein and J. Hinkley, *INNOHYP CA final report*, INNOHYP CA-FR-CEA/07-05, 2007.

304 T. Pregger, D. Graf, W. Krewitt, C. Sattler, M. Roeb and S. Möller, *Int. J. Hydrogen Energy*, 2009, **34**, 4256–4267.

305 R. Elder and R. Allen, *Prog. Nucl. Energy*, 2009, **51**, 500–525.

306 E. Solomin, Z. Salah, K. Osintsev, S. Aliukov, S. Kuskarbekova, V. Konchakov, A. Olinichenko, A. Karelin and T. Tarasova, *Energies*, 2023, **16**, 6118.

307 R. S. El-Emam, H. Ozcan and I. Dincer, *Int. J. Hydrogen Energy*, 2015, **40**, 11168–11177.

308 A. Godula-Jopek, *Hydrogen production: by electrolysis*, John Wiley & Sons, 2015.

309 M. Conte, F. Di Mario, A. Iacobazzi, A. Mattucci, A. Moreno and M. Ronchetti, *Energies*, 2009, **2**, 150–179.

310 C. Forsberg and M. Kazimi, *Nucl. Prod. Hydrogen*, 2010, 155–164, DOI: 10.1787/9789264087156-17-en.

311 A. I. Osman, N. Mehta, A. M. Elgarahy, M. Hefny, A. Al-Hinai, A. a. H. Al-Muhtaseb and D. W. Rooney, *Environ. Chem. Lett.*, 2022, 1–36.