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## Decarbonizing potential of global container shipping with hydrogen-based fuels

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Hydrogen-based fuels are expected to support maritime shipping in reaching net-zero climate targets. However, the complexity of hydrogen-based fuel supply, propulsion system deployment, and fleet composition make their full life cycle decarbonization potential unclear. A comprehensive fleet-level assessment of their decarbonization potential is thus essential. Here, we evaluate the life cycle climate change impact of global container shipping using hydrogen-based fuels from 2020 to 2050, considering fuel mix, propulsion system, ship size and transport demand. By integrating energy scenarios from the International Energy Agency with socio-economic scenarios from the Shared Socioeconomic Pathways and the Organization for Economic Co-operation and Development, we explore three scenarios that represent different levels of ambition for the future hydrogen production transition, hydrogen-based fuel use, and corresponding transport demand: the Less Ambitious, Ambitious and Very Ambitious scenarios. Our findings indicate that container shipping's greenhouse gas (GHG) emissions per tonne-nautical mile could decrease from 22 g CO<sub>2</sub>-eq in 2020 to 21 g, 9 g, and 3 g CO<sub>2</sub>-eq by 2050 under the Less Ambitious, Ambitious, and Very Ambitious scenarios, respectively. Cumulative GHG emissions from global container shipping could reach 9–12 Gt, 7–10 Gt, and 4–5 Gt CO<sub>2</sub>-eq between 2020 and 2050 across these scenarios, accounting for 1–3% of the global carbon budget required to achieve the worldwide net-zero target. The substitution of heavy fuel oil with hydrogen-based fuels does not always lead to a reduction in GHG emissions: in the Less Ambitious scenario, cumulative emissions increase by 0.4–0.6 Gt CO<sub>2</sub>-eq due to the slow decarbonization in hydrogen production, whereas in the Ambitious and Very Ambitious scenarios, they decline by 1–2 Gt and 3–5 Gt CO<sub>2</sub>-eq, respectively. Deep decarbonization of maritime shipping requires overcoming key bottlenecks in renovating the fleet, scaling up ammonia production and electrolyzer capacity, and ensuring sufficient renewable electricity supply. This highlights the need for coherent policies to foster multi-sectoral coordination among maritime shipping, hydrogen-based fuel production, and power generation to maximize their decarbonizing potential.

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### Broader context

Hydrogen-based fuels are gaining attention as a key solution for decarbonizing the maritime shipping sector. Yet, the full life-cycle decarbonization potential of these fuels remains uncertain, primarily due to the complexity of the sector. A comprehensive assessment framework is necessary to quantify this potential. The prospective life cycle assessment that integrates technological details with broader socioeconomic developments can provide a clearer understanding of hydrogen-based fuels' role in maritime shipping. Such an approach can also help guide the International Maritime Organization and policymakers in shaping effective decarbonization roadmaps. This paper also highlights the potential challenges of relying on hydrogen-based fuels for deep decarbonization in the shipping sector.

## 1. Introduction

Maritime shipping enables more than 80% of global merchandise trade by volume and accounted for 2% of annual global

greenhouse gas (GHG) emissions, totaling 1.01 Gt carbon dioxide equivalent (CO<sub>2</sub>-eq) in 2022, primarily due to its reliance on fossil fuels such as heavy fuel oil (HFO) and marine gas oil (MGO).<sup>1,2</sup> If left unregulated, these emissions could rise to as much as 1.5 Gt CO<sub>2</sub>-eq by 2050.<sup>3</sup> The International Maritime Organization (IMO) has set a strategic and guidance-based target to achieve net-zero GHG emissions from international shipping by 2050.<sup>4</sup> The maritime shipping sector faces an urgent need for decarbonization, but the transition path is

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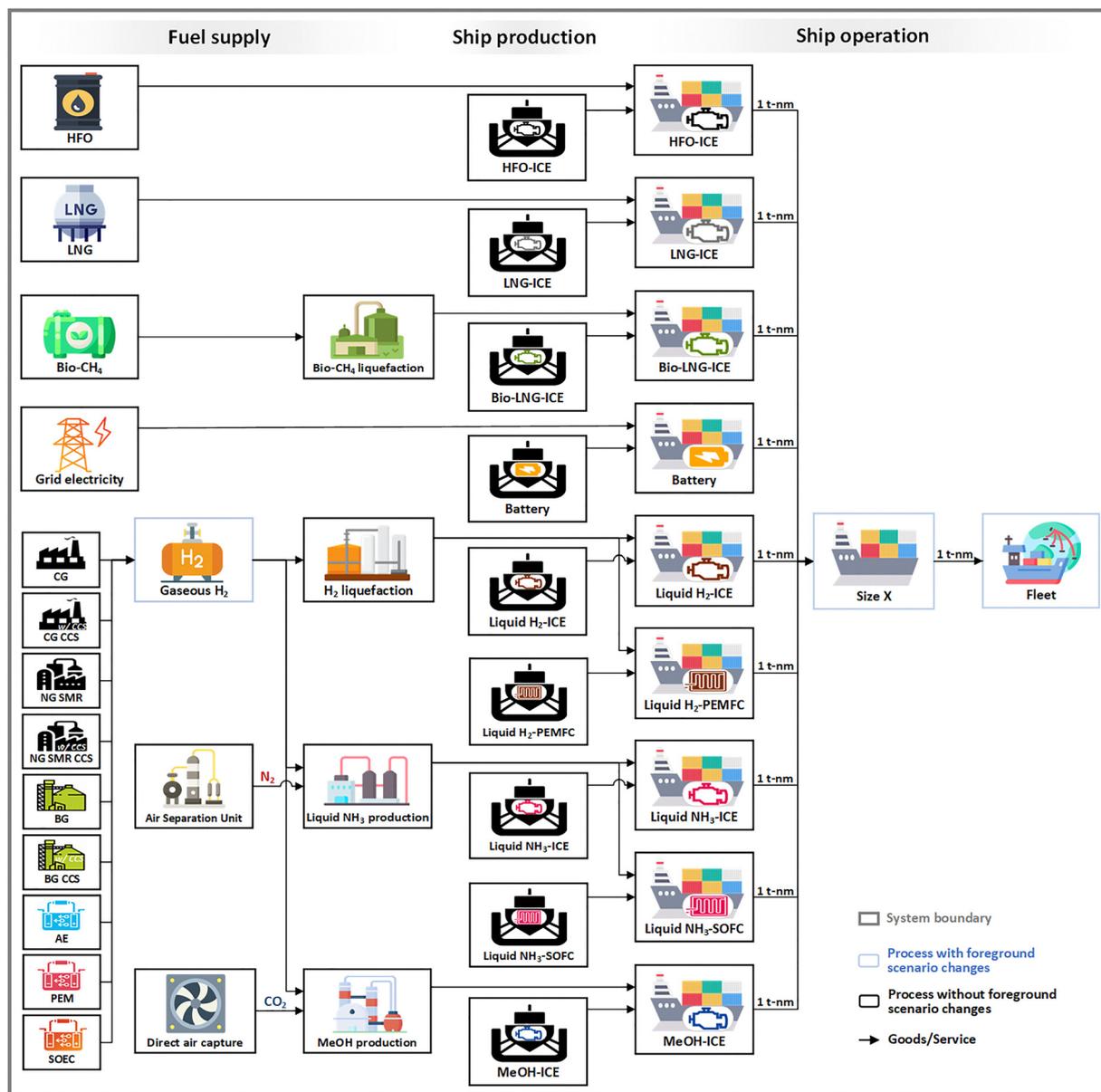


Fig. 1 The LCA model of container shipping.<sup>†</sup> In this figure, CG = coal gasification, NG SMR = steam methane reforming of natural gas, BG = biomass gasification, CCS = carbon capture and storage, AE = alkaline electrolyzers, PEM = proton exchange membrane electrolyzers, SOEC = solid oxide electrolysis cells, ICE = internal combustion engines, PEMFC = proton-exchange membrane fuel cells, SOFC = solid oxide fuel cells, HFO = heavy fuel oil, LNG = liquefied natural gas, and Bio-LNG = liquefied biomethane. Nine ship size categories are considered. For LNG-ICE, Bio-LNG-ICE, liquid H<sub>2</sub>-ICE, liquid NH<sub>3</sub>-ICE, and MeOH-ICE, a small amount of marine gas oil is required as pilot fuel. Size X represents nine container ship categories with capacities ranging from 0–999 TEU, 1000–1999 TEU, 2000–2999 TEU, 3000–4999 TEU, 5000–7999 TEU, 8000–11 999 TEU, 12 000–14 499 TEU, 14 500–19 999 TEU, and 20 000+ TEU. TEU (twenty-foot equivalent unit) refers to a standard 20-foot-long shipping container. Battery-powered ships are only applicable to the 0–999 TEU category.

### 2.2.1. Ship production

**Hull production.** For different sizes of container ships, the material requirements for hull production are determined by the lightweight mass, as calculated in eqn (1),<sup>28</sup> and the material composition share from Jain *et al.*<sup>29</sup> and Notten *et al.*<sup>28</sup> Welding, electricity use, heat consumption, and emissions during hull production are calculated according to

Notten *et al.*<sup>28</sup> The hull weight remains the same for each ship size while the propulsion systems are different.

$$\text{LWT} = (1 - 0.7) \times \frac{\text{DWT}}{0.7} \quad (1)$$

where LWT represents the weight of the empty vessel, including hull material, machinery, and outfitting;<sup>28</sup> deadweight tonnage (DWT) is the load capacity of the ship, including the cargo, fuel,

<sup>†</sup> This figure has been designed using images from Flaticon.com.



water, crew and effects;<sup>30</sup> and 0.7 is the ratio of the DWT to the total weight of the ship.<sup>31</sup>

**Propulsion system.** For each ship size, nine propulsion systems are modeled. Conventional diesel engines are used for the HFO-ICE propulsion system, while dual-fuel engines are used for ICEs fueled by LNG and H<sub>2</sub>-based fuels due to their ease of scaling up.<sup>3</sup> For ICE-based ships, the two-stroke slow-speed main engine drives the propeller directly *via* shafting, while a four-stroke medium-speed auxiliary engine is coupled with a generator to provide electricity. For dual-fuel LNG engines, there are two types: high-pressure engines with higher pilot fuel demand and low-pressure engines with lower pilot fuel demand but higher emissions of unburned methane.<sup>32</sup> In this study, the low-pressure type is chosen as it is the most widely adopted solution at present.<sup>33</sup> A small amount of diesel pilot fuel is required for these dual-fuel ICEs. For ICEs fueled by LNG and H<sub>2</sub>-based fuels, 1% and 5% of the energy content, respectively, is assumed to come from MGO.<sup>20,34</sup> To comply with the IMO Tier III NO<sub>x</sub> regulations, selective catalytic reduction (SCR) is assumed to be equipped for both the main and auxiliary engines in HFO-ICE, liquid NH<sub>3</sub>-ICE, and MeOH-ICE propulsion systems, while only the main engine is equipped with SCR in LNG-ICE, bio-LNG-ICE and liquid H<sub>2</sub>-ICE propulsion systems.<sup>20</sup> For fuel cells, PEMFC and SOFC are considered for the direct use of H<sub>2</sub> and NH<sub>3</sub>. The generated electricity powers the propeller *via* an electric motor and meets the auxiliary electrical and heating demands. Options such as cracking H<sub>2</sub>-based fuels to use H<sub>2</sub> in PEMFC are not considered due to

the additional onboard components required for cracking and purification, which would reduce overall system efficiency. The battery energy storage system is required to supply energy for the fuel cell's cold start-up, allowing the system to reach its operating temperature. For fuel cell-powered ships, the battery is sized to support 10 minutes of operation at 20% load for PEMFCs and 30 minutes at the same load for SOFCs.<sup>21</sup> This is because PEMFCs operate at a lower temperature than SOFCs, allowing for faster start-up and quicker response.<sup>35</sup> In this study, the battery depth of discharge is assumed to be 80%, with a 20% safety margin accounted for to consider battery degradation over its lifetime (11 years, requiring two replacements over a ship's 25-year lifespan). For the battery ship, Li-ion batteries are used to store grid electricity and power the ship in a manner similar to fuel cell ships. However, batteries are not suitable for long trips and are primarily used for short-sea shipping due to their lower energy density compared to other liquid fuels (*e.g.*, about 2% and 3% HFO's gravimetric and volumetric energy density, respectively).<sup>7</sup> The specific configurations of different propulsion systems are shown in Fig. S1 in the SI. For each ship size, alternative propulsion systems are sized to match the propeller and auxiliary system output power of the HFO-ICE propulsion system. For components with a lifespan shorter than the ship's service life, their replacement is taken into account. The key parameters and data sources for different components used in the propulsion systems are summarized in Table 1.

### 2.2.2. Fuel supply

**Fossil fuels and biofuels.** The HFO and MGO are sourced from the global market as modeled in the ecoinvent database.<sup>39</sup>

**Table 1** The main technical parameters of propulsion systems. In this table, 2S = two stroke, and 4S = four stroke, ICE = internal combustion engine, PEMFC = proton-exchange membrane fuel cells, SOFC = solid oxide fuel cells, DF = Dual fuel, and SCR = selective catalytic reduction

Components	Efficiency (%)	Lifespan (years)	Mass factor (t MW <sup>-1</sup> )	Volume factor (m <sup>3</sup> MW <sup>-1</sup> )	Key parameters source	LCI source
2S Diesel ICE	50	25	29.2	27.5	21 and 36	21
2S LNG DFICE	50	25	29.2	27.5	32 and 36	21
2S H <sub>2</sub> /MeOH DFICE	48	25	29.2	27.5	20 and 36	21
2S NH <sub>3</sub> DFICE <sup>a</sup>	46	25	29.2	27.5	20 and 36	21
PEMFC	55	6	3.3	5.7	21 and 37	38
SOFC	60	5	45.3	97.2	21 and 37	21
Li-ion battery	96	11	—	—	37	39
4S Diesel ICE	48	25	29.2	27.5	21 and 36	21
4S LNG DFICE	48	25	29.2	27.5	32 and 36	21
4S H <sub>2</sub> /MeOH DFICE	46	25	29.2	27.5	20 and 36	21
4S NH <sub>3</sub> DFICE <sup>a</sup>	44	25	29.2	27.5	20 and 36	21
Alternator	96	25	2.5	5	21 and 36	39
Converter (main engine) <sup>b</sup>	98	25	2.3	5.1	37 and 40	39
Inverter	98	6	3.7	9	41–43	39
Motor drive	97	25	1.1	4.4	44–46	47 and 48
Electric motor	98	25	2.7	4.2	21, 49 and 50	39
Switchboard	99.8	11	0.7	1.4	51–53	39
Converter (energy storage)	98	25	3	6.7	37 and 40	39
Shafting	99	25	—	—	54 and 55	28
Exhaust gas/Oil composite boiler	85	25	3	8.8	56 and 57	39
Exhaust gas/Gas composite boiler	85	25	3	8.8	56 and 57	39
Exhaust gas/Electric composite boiler <sup>c</sup>	99	25	3	8.8	57 and 58	59
SCR	—	25	0.9	5	60 and 61	16

<sup>a</sup> In H<sub>2</sub>-based DFICE, NH<sub>3</sub> DFICE has a 2% lesser efficiency due to high heat of vaporization.<sup>21</sup> <sup>b</sup> This refers to fuel cells and Li-ion battery. <sup>c</sup> This type of boiler is installed on ICE ships powered by H<sub>2</sub>-based fuels. For fuel cell- and battery-powered ships, where a large flow of exhaust gas is unavailable, an electric boiler is required.



In this study, we further add a desulfurization process according to the study of Silva<sup>62</sup> to adapt the sulfur content in HFO and MGO from 1.03%<sup>39</sup> to 0.5% (very low sulphur fuel oil, or VLSFO) to satisfy the upper limit of sulfur content in fuel oil worldwide outside Sulphur Emission Control Areas (SECAs) under the IMO 2020 regulation.<sup>63</sup> Although a stricter sulfur content of 0.1% is regulated in SECAs,<sup>64</sup> and fuel oil switching may be required when ships are entering these areas, this process is not considered in this study, as the fuel used in SECAs is marginal compared to the total fuel consumption in container shipping. The regulation on sulfur content in marine fuels aims to reduce SO<sub>x</sub> emissions, as these emissions are solely determined by the sulfur content of the fuel used in ship operation, whereas NO<sub>x</sub> emissions are not only related to the nitrogen content in the fuel but can also be formed thermally from nitrogen and oxygen in the intake air at high engine temperatures.<sup>65,66</sup> The LNG is sourced from the global market as modelled in the ecoinvent database.<sup>39</sup> For bio-LNG production, gaseous synthetic biomethane with a pressure of 60 bar, derived from wood chips gasification using fluidized bed technology modeled in the ecoinvent database,<sup>39</sup> is further liquefied through a pressure reduction liquefaction facility.<sup>67</sup> Wood chips are sourced from sustainably managed forests.<sup>39</sup> The source and technology of biofuels used in maritime shipping are not specified in the IEA report.<sup>10,17</sup> Although there are other drop-in biofuels, such as Fischer-Tropsch biodiesel,<sup>10,68</sup> bio-LNG is used to represent biofuels due to its higher technology readiness.<sup>69</sup>

**H<sub>2</sub>-based fuels.** The supply of H<sub>2</sub>-based fuels is based on the global gaseous H<sub>2</sub> production model developed in our previous study Wei *et al.*,<sup>12</sup> which incorporates two H<sub>2</sub> production scenarios developed by the International Energy Agency (IEA): the Stated Policies (STEPS) Scenario and Net Zero Emissions by 2050 (NZE) Scenario.<sup>12</sup> These models cover nine leading H<sub>2</sub> production technologies, including coal gasification, natural gas steam reforming, and biomass gasification, both with and without carbon capture and storage (CCS), as well as grid-coupled water electrolysis using alkaline electrolyzers, proton exchange membrane electrolyzers, and solid oxide electrolysis cells. Additionally, the models account for electricity decarbonization, efficiency improvements, advancements in electrolyzer technology, and shifts in the H<sub>2</sub> production mix.

The gaseous H<sub>2</sub> from the global market<sup>12</sup> is used as the feedstock for the liquid H<sub>2</sub>, liquid NH<sub>3</sub> and MeOH production. The H<sub>2</sub> is liquefied in a liquefaction plant, consuming 10.5 kWh of electricity per kg of liquefied H<sub>2</sub>.<sup>70</sup> H<sub>2</sub> losses of 16.2 g per kg of liquid H<sub>2</sub> occur during this process.<sup>71</sup> The LCI is based on the research of Wulf and Zapp.<sup>71</sup> Liquid NH<sub>3</sub> is produced *via* the Haber-Bosch process by reacting gaseous H<sub>2</sub> with nitrogen obtained from cryogenic distillation. The LCI is derived from the research of D'Angelo, *et al.*<sup>14</sup> MeOH is synthesized from gaseous H<sub>2</sub> and captured CO<sub>2</sub> *via* direct air capture (DAC). DAC is currently operated in a few demonstration plants (TRL 6–7), with full commercialization expected by the late 2030s.<sup>24,72,73</sup> The LCI for MeOH production is based on the research of

González-Garay *et al.*<sup>74</sup> and Keith *et al.*<sup>75</sup> Although synthetic methane produced *via* the Sabatier reaction is also a type of synthetic H<sub>2</sub>-based fuel,<sup>76</sup> MeOH is used in this study as the representative since it is mainly covered in IEA reports.<sup>10,17,77</sup> Despite being at a similar TRL (9), synthetic methane may face commercial challenges given the low-cost availability of fossil gas and the growing production of biomethane.<sup>24</sup> Moreover, since synthetic H<sub>2</sub>-based fuels will account for only 0.5% of maritime fuel use by 2050 in the IEA's NZE scenario,<sup>10</sup> a more detailed differentiation between MeOH and synthetic methane would have only marginal impacts on the overall results.

### 2.2.3. Ship operation

**Energy demand for ship operation.** The energy demand for ship operation comes from the main engine power system, the auxiliary engine system, and the auxiliary boiler, which respectively satisfy propeller power, electricity use, and heating demand.<sup>3</sup> The energy demand for ship operation during a voyage is determined by the average output power and energy efficiency of the three systems, as well as by the operating time and fuel margin. It is calculated using eqn (2)–(4). The parameters required for each ship size are provided in Table S1 of the SI. A validation of our model has been conducted by comparing modelled direct CO<sub>2</sub> emissions of HFO ships with CO<sub>2</sub> emissions for each ship size category reported under the EU Monitoring, Reporting and Verification (EU-MRV) Maritime Regulation<sup>78</sup> and with calculated results presented in the IMO report.<sup>3</sup> Overall, both sets of measured values confirm the validity of our model for present-day ship emissions (see Section 3.1 of the SI for the detailed comparison).

$$E_{Oi} = \left( \frac{P_{OMi}}{\lambda_{MEi}} + \frac{P_{OAI}}{\lambda_{AEi}} + \frac{P_{OBI}}{\lambda_{ABSi}} \right) \times T \times FM \quad (2)$$

where  $E_{Oi}$  is the energy demand for the ship operation powered by propulsion system  $i$ , in MWh;  $P_{OMi}$  is the average output power of main engine in propulsion system  $i$ , calculated by the Admiralty formula (eqn (3));<sup>3</sup>  $\lambda_{MEi}$  is the energy efficiency for main engine in propulsion system  $i$ ;  $P_{OAI}$  is the average output power of the auxiliary engine in propulsion system  $i$ , calculated by eqn (4);<sup>79</sup>  $\lambda_{AEi}$  is the energy efficiency for auxiliary engine in propulsion system  $i$ ;  $P_{OBI}$  is the output power of the auxiliary boiler in propulsion system  $i$ , assumed equal to its installed power;  $\lambda_{ABSi}$  is the energy efficiency for auxiliary boiler system in propulsion system  $i$ . It should be noted that when the ship is at sea, the auxiliary boiler can utilize exhaust gas in ICE-based propulsion systems, while in fuel-cell-based propulsion systems, it requires electricity consumption.<sup>80</sup>  $T$  is the operation time for one voyage, determined by the voyage length and the average speed;  $FM$  is the fuel margin, which ensures voyage completion even in the event of potential detours, unexpected adverse weather conditions, or similar factors,<sup>7</sup> and is set to 1.2.<sup>81</sup>

$$P_{OMi} = \frac{P_{IMi} \times \left( \frac{d_{ave}}{d_{max}} \right)^{\left( \frac{2}{3} \right)} \times \left( \frac{v_{ave}}{v_{max}} \right)^3}{\eta_w \times \eta_f} \quad (3)$$



where  $P_{IMi}$  is the installed power of the main engine in propulsion system  $i$ ;  $d_{ave}$  and  $d_{max}$  represent the average and max draught of a ship in a specific voyage;  $v_{ave}$  and  $v_{max}$  represent the average and max speed of a ship in a specific voyage;  $\eta_w$  and  $\eta_f$  are correction factors for weather and fouling, indicating the power increase affected by weather conditions and hull fouling.

$$P_{Oai} = P_{Iai} \times l_{AE} \quad (4)$$

where  $P_{Iai}$  is the installed power of the auxiliary engine in propulsion system  $i$ ;  $l_{AE}$  is the load factor of the auxiliary engine, which is 0.5.<sup>79</sup>

**Energy demand for fuel storage.** For propulsion systems using LNG, liquid H<sub>2</sub> and liquid NH<sub>3</sub>, which are stored in cryogenic tanks on board, heat penetration can cause fuel evaporation, leading to the formation of boil-off gas (BOG).<sup>82</sup> The BOG can be managed by either directing it to the engine for propulsion or reliquefying it. However, the first method offers less control over the fuel consumption rate.<sup>82</sup> Therefore, in this study, BOG is conservatively assumed to be managed through a reliquefaction plant. As BOG decreases with fuel consumption, the reliquefaction capacity is designed based on the maximum BOG volume per hour. The mass and volumetric factors of the reliquefaction plant are 0.04 t and 0.11 m<sup>3</sup> per kilogram of liquefaction capacity per hour, respectively.<sup>83,84</sup> The additional energy required for this process is calculated using eqn (5):

$$E_{Ri} = \frac{k_{Ri}}{\lambda_{AESi}} \times \sum_{t=0}^{T-1} \left[ \left( \frac{E_{Oi}}{D_i} - \frac{E_{Oi} \times t}{D_i \times FM \times T} \right) \times BOG_i \right] \quad (5)$$

where  $E_{Ri}$  is the energy demand for reliquefying BOG, in MWh;  $k_{Ri}$  is the electricity demand for reliquefying BOG of propulsion system  $i$ , 1.23 kWh kg<sup>-1</sup> LNG,<sup>83</sup> 3.3 kWh kg<sup>-1</sup> liquid H<sub>2</sub><sup>85</sup> and 0.224 kWh kg<sup>-1</sup> liquid NH<sub>3</sub>;<sup>86</sup>  $\lambda_{AESi}$  is the efficiency of the auxiliary engine system for propulsion system  $i$ ;  $t$  is time point of ship operation in one voyage, in hours;  $D_i$  is the energy density for fuel used in propulsion system  $i$ ;  $BOG_i$  is the hourly evaporation rate of the fuel used in propulsion system  $i$ , 0.0054% per hour for LNG, 0.0167% per hour for liquid H<sub>2</sub> and 0.0017% per hour for liquid NH<sub>3</sub>.<sup>87</sup>

**Fuel storage.** Based on the energy demand for the trip, the tank size is further determined. HFO and MGO are stored in the diesel tank. MeOH, being liquid at atmospheric temperature, is stored in a carbon steel tank with epoxy coatings to prevent

corrosion. LNG, liquid H<sub>2</sub>, and liquid NH<sub>3</sub> are stored in cryogenic tanks, each with specific material requirements due to their differing storage temperatures. The related parameters for fuel storage and LCI data sources are shown in Table 2.

**Emissions of ship operation.** For each ship size, the gravimetric and volumetric changes of alternative propulsion systems and their corresponding fuel storage, compared to the conventional HFO-ICE system, are also quantified. The results are provided in the Section 1.3 of the SI. It should be noted that the gravimetric constraint directly affects cargo weight, while volumetric constraints, though significant, can be mitigated by mounting additional energy storage volume on deck.<sup>80,94,95</sup> Finally, fuel consumption per t-nm is determined based on energy demand, ship range, and resulting cargo weight. The fuel consumption and corresponding emissions for different propulsion systems are detailed in Table 3.

**2.2.4. Future transport demand for global container shipping.** Three scenarios, reflecting different ambitions for future containerized transport demand and the penetration of H<sub>2</sub>-based fuels, are explored in this study, as shown in Table 4. In setting these scenarios, consistency between socioeconomic development and energy scenarios is considered. The Less Ambitious scenario reflects current trends, where transport demand continues along historic trajectories, the penetration rate of H<sub>2</sub>-based fuels is extrapolated from the existing strategy, and H<sub>2</sub> production is modeled based on current policies. The Ambitious scenario envisions a society pursuing green growth, characterized by higher transport demand growth, with both the energy mix for container shipping and H<sub>2</sub> production aligned with net-zero CO<sub>2</sub> emissions targets. The Very Ambitious scenario explores a post-growth society placing greater emphasis on environmental sustainability and human well-being,<sup>100</sup> where transport demand grows more slowly, and container ship fleets transition more rapidly to fully renewable H<sub>2</sub>-based fuels. A detailed description is provided below.

In 2020, the transport demand of global container shipping was approximately 8.9 trillion t-nm.<sup>102</sup> Considering socioeconomic development across different pathways, future container shipping transport demand will follow varying patterns. Three social-economic development pathways are considered based on the Shared Socioeconomic Pathways (SSPs) and the Organization for Economic Co-operation and Development (OECD)'s long-term projections, as presented in the Fourth IMO GHG Study 2020:<sup>3</sup> SSP2, SSP1, and OECD. In SSP2, the

Table 2 The key technical parameters and data source of various fuels and their storage

Fuel/energy storage	Tank type	Lower heating value (MWh t <sup>-1</sup> )	Gravimetric energy density including tank (MWh t <sup>-1</sup> )	Volumetric energy density including tank (MWh m <sup>-3</sup> )	Data source	LCI of tanks
HFO	Diesel tank	11.2	9.7	11.1	19 and 88	89
MGO	Diesel tank	11.9	10.1	10.1	19	89
LNG/Bio-LNG	Cryogenic LNG tank	13.6	8.3	3.1	19	90
Li-ion battery	—	—	0.17	0.3	7	—
Liquid H <sub>2</sub>	Cryogenic H <sub>2</sub> tank	33.3	5.6	1.3	19	91
Liquid NH <sub>3</sub>	Cryogenic NH <sub>3</sub> tank	5.2	4.2	2.9	19	90 and 92
MeOH	MeOH tank	5.6	4.6	4.4	19	89 and 93



**Table 3** Fuel consumption and emissions for different propulsion systems. Battery and liquid H<sub>2</sub>-PEMFC systems produce no emissions and are therefore not listed here

Propulsion system	HFO-ICE <sup>20,96–98</sup>		LNG/Bio-LNG-ICE <sup>20,34,96–98</sup>		Liquid H <sub>2</sub> -ICE <sup>16,20,96–98</sup>		Liquid NH <sub>3</sub> -ICE <sup>16,20,96–98</sup>		MeOH-ICE <sup>20,96–99</sup>		Liquid NH <sub>3</sub> -SOFC <sup>16</sup>
	2S	4S	2S	4S	2S	4S	2S	4S	2S	4S	—
Engine type	2S	4S	2S	4S	2S	4S	2S	4S	2S	4S	—
Main fuel (g kWh <sup>-1</sup> )	178.6	186.0	145.6	151.7	59.4	62.0	397.2	415.2	353.4	368.8	320.5
Pilot fuel (g kWh <sup>-1</sup> )	—	—	1.7	1.8	8.8	9.1	9.1	9.5	8.8	9.1	—
Urea/NH <sub>3</sub> (g kWh <sup>-1</sup> ) <sup>a</sup>	14.4	9.6	14.4	—	14.4	—	8.2	6.6	14.4	3.7	—
CH <sub>4</sub> (g kWh <sup>-1</sup> ) <sup>b</sup>	0.009	0.009	4.4	4.5	0.0004	0.0004	0.0004	0.0004	0.0004	0.0004	—
CO (g kWh <sup>-1</sup> )	0.9	1.0	1.2	1.2	0.2	0.2	0.2	0.2	4.1	4.3	—
CO <sub>2</sub> (g kWh <sup>-1</sup> )	585	605	401	407	38	29	29	30	536	551	—
NO <sub>x</sub> (g kWh <sup>-1</sup> )	3.4	2.6	3.4	0.7	3.4	0.7	3.4	2.6	3.4	2.6	0.003
N <sub>2</sub> O (g kWh <sup>-1</sup> )	0.029	0.030	0.014	0.014	0.001	0.002	0.013	0.014	0.001	0.002	—
NH <sub>3</sub> (g kWh <sup>-1</sup> )	0.026	0.026	0.024	0.00002	0.024	0.0001	0.037	0.038	0.024	0.024	—
NMVOG (g kWh <sup>-1</sup> )	0.424	0.441	0.446	0.465	0.024	0.025	0.025	0.026	0.021	0.022	—
PM10 (g kWh <sup>-1</sup> )	0.051	0.053	0.003	0.003	0.003	0.003	0.003	0.003	0.011	0.011	—
PM2.5 (g kWh <sup>-1</sup> )	0.581	0.605	0.035	0.037	0.029	0.031	0.031	0.032	0.123	0.128	—
SO <sub>2</sub> (g kWh <sup>-1</sup> )	1.795	1.869	0.017	0.017	0.086	0.090	0.090	0.094	0.086	0.090	—
CH <sub>2</sub> O (g kWh <sup>-1</sup> )	—	—	—	—	—	—	—	—	0.192	0.200	—

<sup>a</sup> In most propulsion systems, a 40 wt% urea solution (the urea amount is shown in the table) is used in the SCR to generate NH<sub>3</sub> for NO<sub>x</sub> reduction.<sup>34</sup> Excessive urea injection can lead to NH<sub>3</sub> slip, which is assumed to be 0.024 g per kWh.<sup>97</sup> However, in the liquid NH<sub>3</sub>-ICE system, the leaked NH<sub>3</sub> can be utilized as a reducing agent.<sup>20</sup> <sup>b</sup> For the LNG/Bio-LNG-ICE systems, a methane slip of 3 wt% is assumed during combustion.<sup>34</sup>

**Table 4** Scenarios for future container shipping demand and the propulsion system mix. In this table, non-fossil H<sub>2</sub> in the IEA's STEPS and NZE scenarios includes H<sub>2</sub> from water electrolysis and biomass gasification, with biomass gasification contributing only 0.09% and 0.27% of total gaseous H<sub>2</sub> production by 2050, respectively<sup>10,101</sup>

Variables	Less ambitious scenario <sup>3,4,12</sup>	Ambitious scenario <sup>3,10,12</sup>	Very ambitious scenario <sup>3,12</sup>
Global container shipping demand	SSP2 pathway • Higher: logistic model • Lower: gravity model	SSP1 pathway • Higher: logistic model • Lower: gravity model	OECD pathway • Higher: logistic model • Lower: gravity model
Fuel transition	IMO's 2023 strategy	IEA's NZE scenario	Own assumption
Penetration rate of H <sub>2</sub> -based fuels	• 2030-7.5% • 2040-15% • 2050-22.5%	• 2030-10% • 2040-37% • 2050-63%	• 2030-33% • 2040-67% • 2050-100%
Gaseous H <sub>2</sub> production mix	IEA's STEPS scenario	IEA's NZE scenario	100% renewable electrolytic H <sub>2</sub> sourced from PEM with onshore wind power
Propulsion systems	• Non-fossil H <sub>2</sub> in 2020-0.04% • Non-fossil H <sub>2</sub> in 2050-13.8% • HFO-ICE • LNG-ICE • Liquid H <sub>2</sub> -ICE • Liquid H <sub>2</sub> -PEMFC • Liquid NH <sub>3</sub> -ICE • Liquid NH <sub>3</sub> -SOFC • MeOH-ICE	• Non-fossil H <sub>2</sub> in 2020-0.04% • Non-fossil H <sub>2</sub> in 2050-61% • HFO-ICE • LNG-ICE • Bio-LNG-ICE • Battery • Liquid H <sub>2</sub> -ICE • Liquid H <sub>2</sub> -PEMFC • Liquid NH <sub>3</sub> -ICE • Liquid NH <sub>3</sub> -SOFC • MeOH-ICE	• Non-fossil H <sub>2</sub> in 2020-100% • Non-fossil H <sub>2</sub> in 2050-100% • HFO-ICE • LNG-ICE • Liquid H <sub>2</sub> -PEMFC • Liquid NH <sub>3</sub> -SOFC • MeOH-ICE

Middle of the Road narrative, socio-economic factors follow historical trends without significant shifts.<sup>103</sup> SSP1 envisions a world focused on green growth and sustainable development.<sup>104</sup> The OECD narrative has a lower gross domestic product (GDP) projection, leading to slower growth in transport demand.<sup>3</sup> At the same time, different prediction models, such as logistic and gravity models, estimate transport demand based on the elasticity of transport demand concerning per capita GDP and population. Projections using the logistic model typically show higher elasticity with respect to GDP compared to those based on the gravity model. Consequently, transport demand projections from the logistic model are about 45–83% higher in 2050 than those from the gravity

model.<sup>3</sup> This study presents both sets of results from the IMO's report,<sup>3</sup> with the difference between them representing the uncertainty inherent in projecting future developments. By 2050, container transport demand is projected to reach 16.9–25.6, 17.5–31.9, and 14.8–21.4 trillion t-nm in the Less Ambitious, Ambitious, and Very Ambitious scenarios, respectively. The transport demand by ship size from 2020 to 2050 is calculated based on the distribution of container ships across size categories, along with their cargo capacity and annual travel distance for each ship size. The distribution of ship numbers by size remains the same across different pathways.<sup>3</sup> In this analyses, we decided to build upon the existing, well elaborated scenarios discussed above. It is beyond the scope of this paper to work out our own, detailed





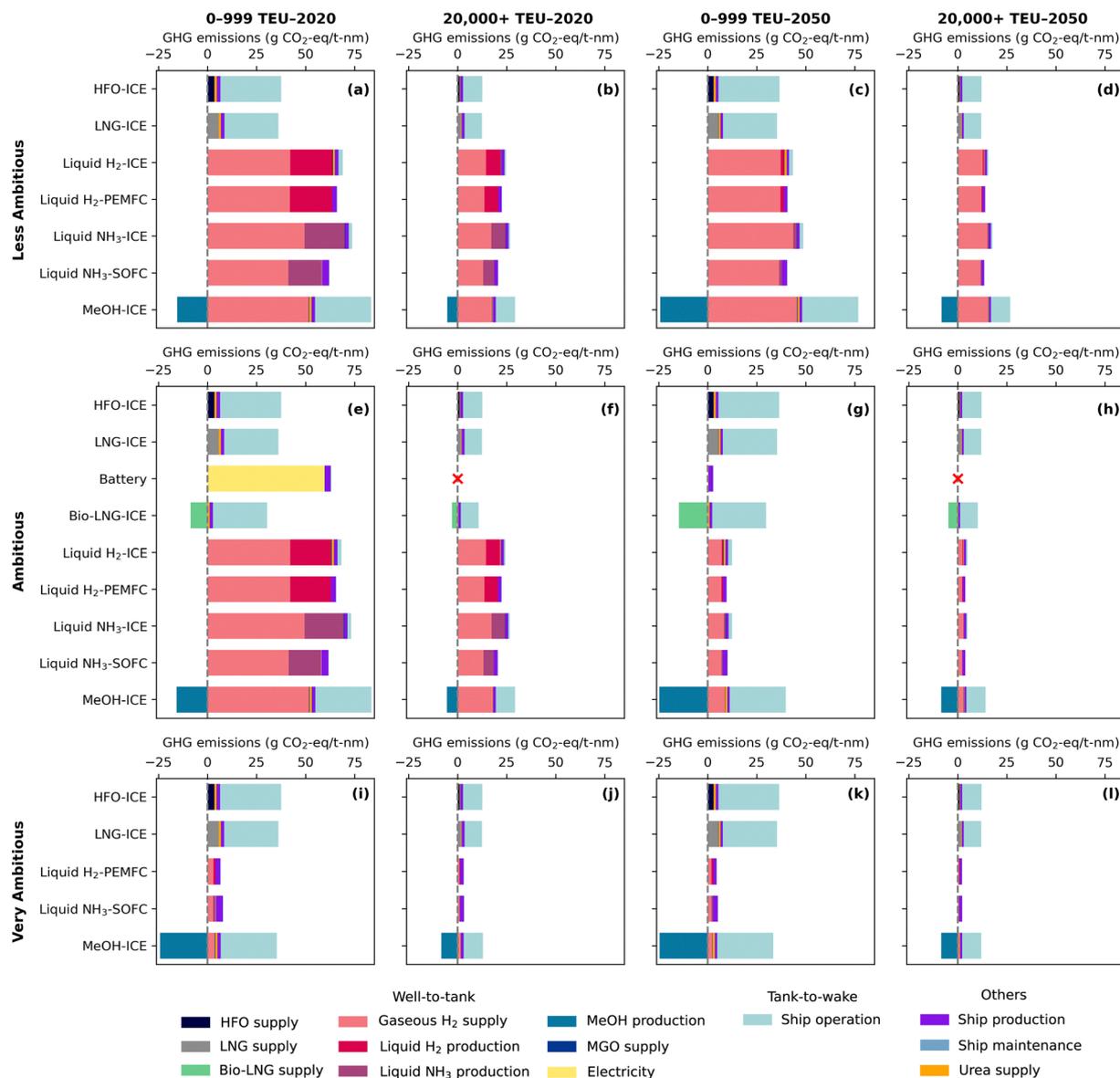


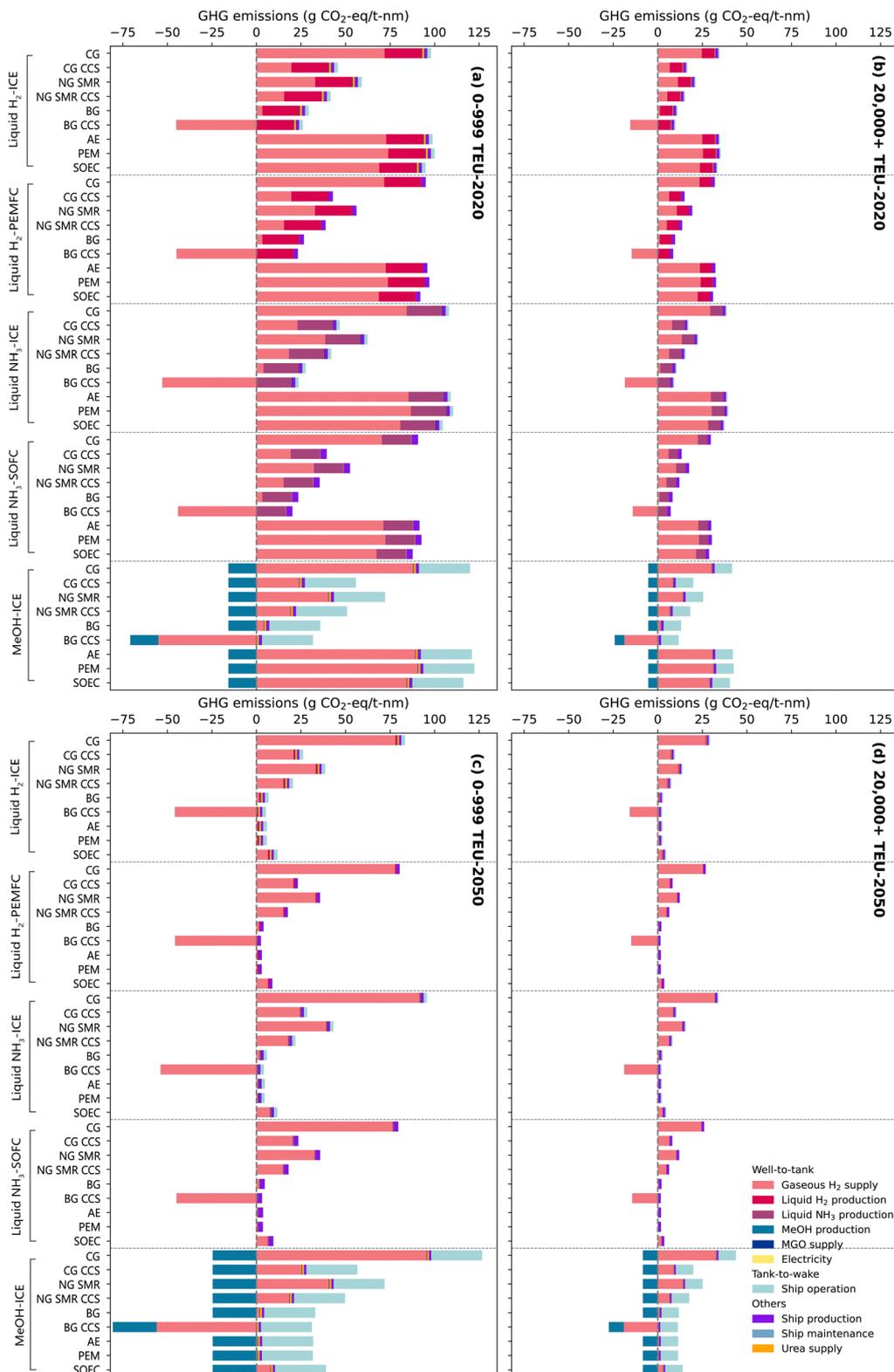
Fig. 2 Prospective GHG emissions of different propulsion systems across various scenarios, by ship size and time. (a)–(d), (e)–(h), and (i)–(l) show the results for the Less Ambitious, Ambitious, and Very Ambitious scenarios, respectively. In these figures, H<sub>2</sub>-based fuels are sourced from the gaseous H<sub>2</sub> market. The red cross marker for battery mains is not applicable to ships with a capacity of 20 000+ TEU. Bio-LNG production and CO<sub>2</sub> capture through direct air capture can all contribute to negative emissions. The GHG emissions of different propulsion systems across various scenarios, by ship size from 2020 to 2050 in five-year intervals, are provided in Tables S293–S295 in the SI.

efficiency, offer lower GHG emissions: liquid H<sub>2</sub>-PEMFC and liquid NH<sub>3</sub>-SOFC emit 22–66 and 21–62 g CO<sub>2</sub>-eq per t-nm, respectively. For ships powered by liquid H<sub>2</sub> and NH<sub>3</sub>, in addition to the gaseous H<sub>2</sub> supply, the processes of H<sub>2</sub> liquefaction and NH<sub>3</sub> synthesis are significant contributors to GHG emissions due to their high electricity consumption. In the Less Ambitious scenario, despite electricity being decarbonized, the fossil-fuel-dominated H<sub>2</sub> market results in H<sub>2</sub>-based fuels having higher GHG emissions than HFO by 2050. In the Ambitious scenario, as the H<sub>2</sub> market adopts more CCS and water electrolysis, and electricity decarbonizes, H<sub>2</sub>-based fuels can reduce GHG emissions compared to HFO by 2050. The GHG emissions

of liquid H<sub>2</sub>-ICE, liquid H<sub>2</sub>-PEMFC, liquid NH<sub>3</sub>-ICE, liquid NH<sub>3</sub>-SOFC, and MeOH-ICE are expected to be 5–12, 4–10, 5–12, 4–10, and 6–15 g CO<sub>2</sub>-eq per t-nm, respectively. Compared to HFO in 2050, H<sub>2</sub>-based fuels sourced from the H<sub>2</sub> market can reduce GHG emissions by 52–68% for ULCVs and 58–73% for feeder ships. In the Very Ambitious scenario, where H<sub>2</sub>-based fuels are entirely produced using additional renewable electricity—including for gaseous H<sub>2</sub> production, liquefaction, NH<sub>3</sub> synthesis, direct air capture, and MeOH synthesis—the GHG emissions drop substantially. In 2020, liquid H<sub>2</sub>-PEMFC, liquid NH<sub>3</sub>-SOFC, and MeOH-ICE emit only 3–7, 3–8, and 5–11 g CO<sub>2</sub>-eq per t-nm, respectively, depending on ship size. This corresponds to a



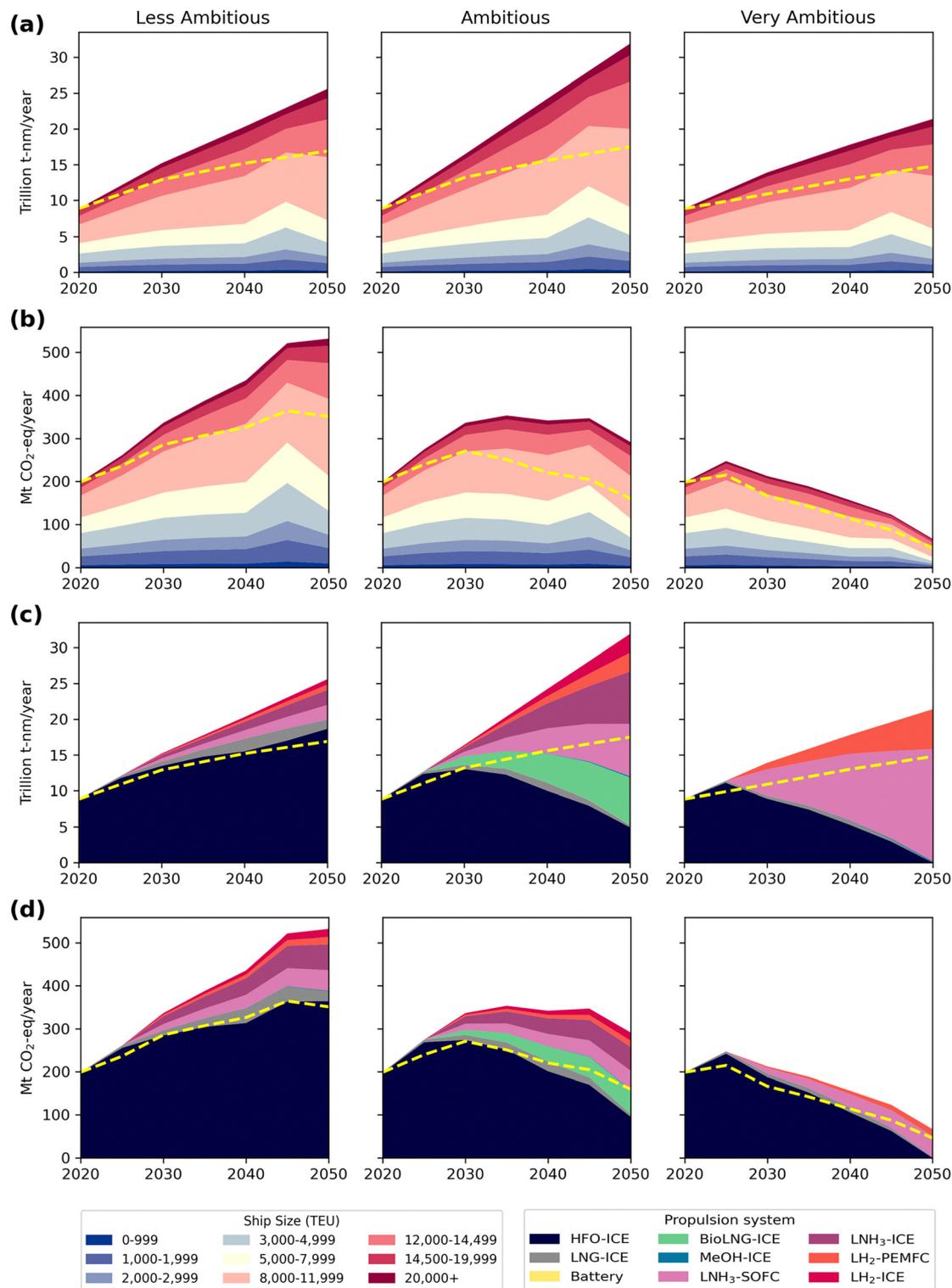




**Fig. 3** Prospective GHG emissions from H<sub>2</sub>-based propulsion systems for container ships in 2020 and 2050 by H<sub>2</sub> source in the Ambitious scenario. In this figure, CG = coal gasification, NG SMR = steam methane reforming of natural gas, BG = biomass gasification, CCS = carbon capture and storage, AE = alkaline electrolyzer, PEM = proton exchange membrane electrolyzer, and SOEC = solid oxide electrolysis cell. Gaseous H<sub>2</sub> production via biomass gasification with carbon capture and storage, and CO<sub>2</sub> capture through direct air capture can contribute to negative emissions. Prospective GHG emissions from H<sub>2</sub>-based ships by H<sub>2</sub> source under the Less Ambitious scenario are shown in Fig. S7 of the SI. In the Very Ambitious scenario, the H<sub>2</sub> market consists exclusively of 100% renewable electrolytic H<sub>2</sub> from PEM using newly built onshore wind power, without contributions from other technologies. Prospective GHG emissions from H<sub>2</sub>-based ships by H<sub>2</sub> source under the Very Ambitious scenario are the same as those shown in Fig. 2. To convey the information effectively, only the results for the smallest and largest ship categories in 2020 and 2050 are shown, as the outcomes for other ship categories and years fall within these ranges.



crops may be insufficient to meet ambitious carbon sequestration targets.<sup>113,114</sup> Moreover, large-scale deployment of BECCS entails significant social, economic, and environmental risks,<sup>115</sup> as bioenergy crop cultivation requires extensive land use, potentially affecting food security, water resources, and biodiversity.<sup>116–119</sup>



**Fig. 4** Annual global container shipping transport demand and GHG emissions by ship size (a) and (b) and propulsion systems (c) and (d). In this figure, the stacked values are based on predictions from the logistic model. The yellow dashed lines represent the total annual transport demand and GHG emissions estimated by the gravity model for comparison.



In terms of ship size, vessels with capacities of 7999 TEU or less accounted for 46% of total transport demand and 59% of GHG emissions in 2020. By 2050, they would account for 28% of transport demand while contributing 36–40% of the sector's emissions across the three scenarios. At the same time, ships below 7999 TEU represent the largest share (>90%) of vessels older than 20 years by 2024.<sup>120</sup> Given these factors, this segment should be prioritized for the adoption of alternative propulsion technologies to maximize emission reduction potential if H<sub>2</sub>-based fuels can be produced in a low-carbon manner, as in the Ambitious and Very Ambitious scenarios. Retrofitting these older ships with alternative propulsion systems could provide a solution that extends their economic life and ensures competitiveness by complying with well-to-wake GHG emissions regulations (*e.g.*, the IMO Net-Zero Framework and FuelEU Maritime, taking effect from 2028—possibly later due to the delay in formal adoption in October 2025—and 2025, respectively) and avoiding penalties.<sup>121–123</sup> Fig. 5 further shows the temporal change in weighted average GHG emissions per t-nm of ship fleets by size across three scenarios. Depending on the penetration rate of H<sub>2</sub>-based fuel use, the decarbonization extent of H<sub>2</sub> production, and propulsion system choices, the weighted average GHG emissions per t-nm for the entire container shipping fleet decreases from 22 g CO<sub>2</sub>-eq in 2020 to 21, 9, and 3 g CO<sub>2</sub>-eq by 2050 under the Less Ambitious, Ambitious, and Very Ambitious scenarios, respectively. In 2020, the average GHG emissions per t-nm for different ship sizes ranged from 13 to

38 g CO<sub>2</sub>-eq. In the Less Ambitious scenario, the use of H<sub>2</sub>-based fuels can increase GHG emissions for each ship size, as H<sub>2</sub>-based fuels cannot be produced more cleanly than HFO. In the Ambitious scenario, the average GHG emissions per t-nm across different ship sizes in 2050 ranges from 6 to 15 g CO<sub>2</sub>-eq, representing a 53–59% decrease compared to 2020. In the Very Ambitious scenario, the gap in average GHG emissions per t-nm across different ship sizes narrows by 2050, with emissions decreasing by 81–86%, to a range of 2–5 g CO<sub>2</sub>-eq per t-nm.

### 3.3. Cumulative GHG emissions of global container shipping

To assess the role of the container shipping sector in achieving net-zero targets for the global economy, we further quantify its cumulative GHG emissions between 2020 and 2050. As shown in Fig. 6, the cumulative emissions are estimated to be 9–12, 7–10, and 4–5 Gt CO<sub>2</sub>-eq under the Less Ambitious, Ambitious, and Very Ambitious scenarios, respectively. In the Less Ambitious scenario, replacing HFO with H<sub>2</sub>-based fuels could increase cumulative emissions by 0.4–0.6 Gt CO<sub>2</sub>-eq. In contrast, in the Ambitious and Very Ambitious scenarios, H<sub>2</sub>-based fuels could reduce emissions by 1–2 and 3–5 Gt CO<sub>2</sub>-eq, respectively. Previous research estimates that the remaining global carbon budget for limiting warming to 1.5 °C with 67% certainty between 2020 and 2050 is approximately 400 (± 220) Gt CO<sub>2</sub>-eq.<sup>124</sup> Based on a 400 Gt CO<sub>2</sub>-eq budget, emissions from global container shipping could consume 1–3% of the total remaining carbon budget. In 2022, container shipping accounted

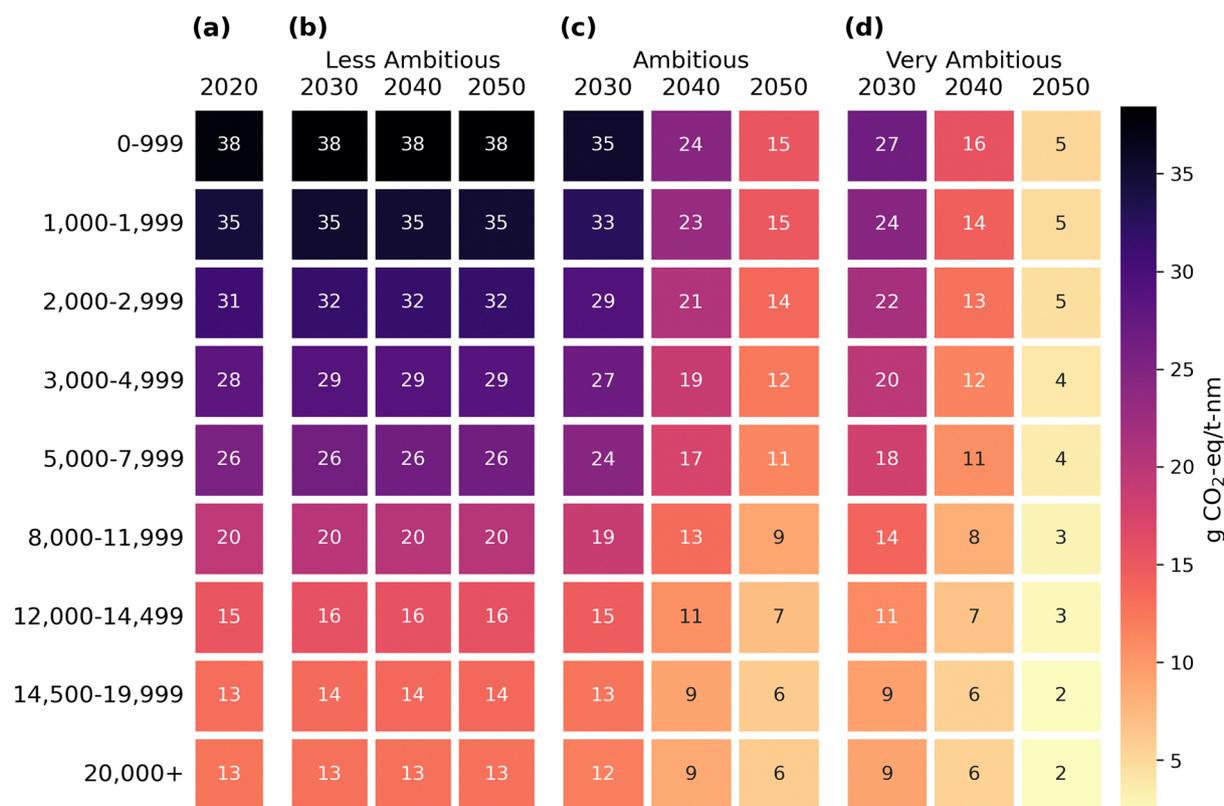


Fig. 5 Weighted average GHG emissions of ship fleet by size (TEU). In the figure, (a) represents the value in 2020, (b), (c), and (d) present the values for 2030, 2040, and 2050 in the Less Ambitious, Ambitious, and Very Ambitious scenarios, respectively.





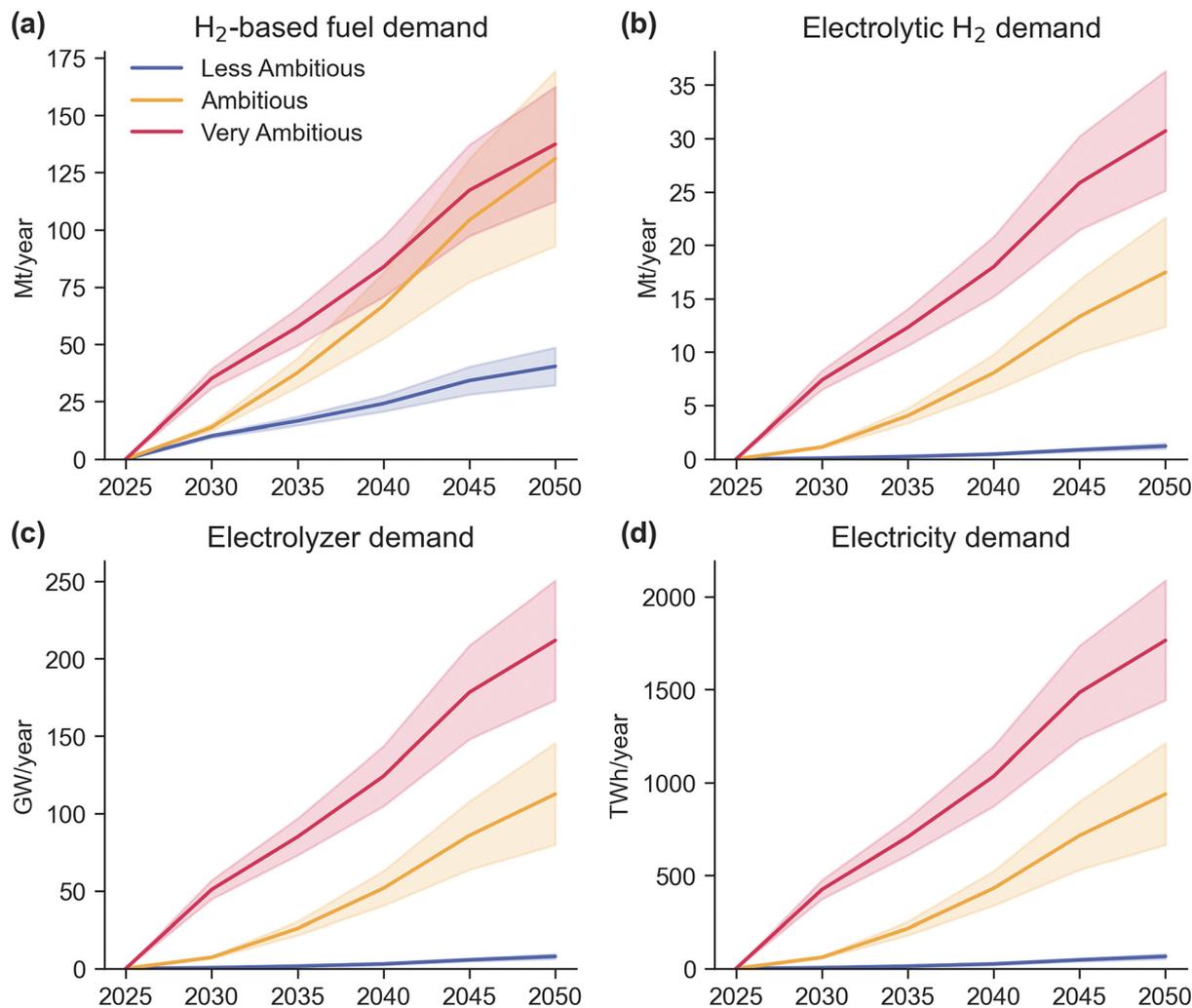


Fig. 7 Demand for (a) H<sub>2</sub>-based fuels, (b) electrolytic gaseous H<sub>2</sub>, (c) electrolyzer capacity, and (d) electricity required for electrolytic H<sub>2</sub> production in global container shipping under the Less Ambitious, Ambitious, and Very Ambitious scenarios. In this figure, the higher and lower boundaries represent the values corresponding to the transport demand estimated by the logistic and gravity models, respectively, while the line is the average value.

of electrolytic H<sub>2</sub>. In the Ambitious and Very Ambitious scenarios, electrolyzer capacity would reach 6–8 GW and 45–57 GW by 2030, and 80–146 GW and 173–250 GW by 2050, respectively. While the announced global electrolyzer capacity is expected to increase from 1.4 GW in 2023 to 230 GW by 2030,<sup>131</sup> not all of the announced electrolyzer projects may be installed and operational on time, creating a risk of a significant implementation gap.<sup>132</sup> For example, by the end of 2023, only 7% of the new capacity expected for installation in 2023 had been achieved.<sup>132</sup> Based on this, it is estimated that only 16 GW of electrolyzer capacity may be deployed by 2030. In the Ambitious scenario, the electrolyzer capacity required to decarbonize global container shipping will occupy half of this capacity, while in the Very Ambitious scenario, it will occupy three times as much. It is important to note that electrolyzer demand extends beyond maritime shipping, as it is also critical for decarbonizing other hard-to-abate sectors such as steel and chemicals. This presents a major obstacle to meeting the electrification and decarbonization targets for the maritime shipping sector.

In the Very Ambitious scenario, the large-scale production of renewable electrolytic H<sub>2</sub> could trigger an additional renewable electricity demand of around 1765 TWh by 2050. In total, including the electricity required for H<sub>2</sub>-based fuel production, approximately 2032 TWh of renewable electricity will be needed by 2050. Under current policy settings, low-emission electricity generation from sources such as solar PV, wind, hydropower, and nuclear is projected to increase by approximately 35 433 TWh between 2023 and 2050.<sup>133</sup> In this context, the renewable electricity demand for H<sub>2</sub>-based fuels would represent around 6% of the expected growth in low-emission electricity over this period. Given that renewable electricity is a competitive resource essential for decarbonizing the global economic sectors, sufficient capacity expansion is required.

## 4. Conclusions

In this study, we systematically assess the potential future climate change impact of global container shipping at both



the individual ship and fleet levels from 2020 to 2050. This assessment considers key drivers such as fuel mixes, propulsion systems, ship sizes, and future transport demand. The Less Ambitious, Ambitious, and Very Ambitious scenarios illustrate the varying roles of H<sub>2</sub>-based fuels in different maritime decarbonization roadmaps, integrating comparable energy transition and socio-economic development pathways. It should be noted that our scenarios are assessments of possible futures and ranges for emissions and not to be confused with predictions. Our findings provide insights for policymakers on the climate implications of adopting H<sub>2</sub>-based fuels in maritime shipping and highlight key challenges in realizing their decarbonizing potential. The main conclusions are as follows:

**H<sub>2</sub>-based fuels can substantially decarbonize maritime shipping, but clear policies are needed to prioritize those from low-carbon electrolysis over fossil-derived alternatives with CCS**

Currently, the immediate adoption of H<sub>2</sub>-based fuels fully sourced from renewables can enable rapid and deep decarbonization, reducing GHG emissions by over 80% per t-nm compared to HFO. This, however, requires additional renewable electricity capacity. Although H<sub>2</sub>-based fuels from biomass gasification with CCS also offer substantial GHG reduction potential, their limited scalability makes them a less promising option. As the power sector decarbonizes, H<sub>2</sub>-based fuels produced from grid electricity could achieve GHG reductions comparable to those from fully renewable sources by 2050. By then, H<sub>2</sub>-based fuels derived from fossil sources with CCS could offer at most a 50% reduction compared to HFO, primarily because the electricity used in their production would also be decarbonized, while the emissions from fossil-based gaseous H<sub>2</sub> with CCS would remain largely unchanged.

**The maritime shipping sector needs stronger policies to adopt renewable H<sub>2</sub>-based fuels, yet BECCS remains essential to achieving the net-zero target**

For global container shipping, transport demand is expected to increase two- to four-fold by 2050 compared to 2020. The sector still emits substantial amounts of GHG under all scenarios in 2050, with annual GHG emissions in 2050 ranging from one-quarter to three times the 2020 levels. Even if transport demand increases more slowly and is fully powered by renewable H<sub>2</sub>-based fuels, annual GHG emissions will still reach 56 Mt CO<sub>2</sub>-eq by 2050. It is estimated that the maritime shipping sector can still consume 4% of the global carbon budget remaining until 2050 to meet the worldwide net-zero target. Achieving net-zero emissions in the sector requires BECCS, but this approach is constrained by scalability limitations.

**Decarbonizing maritime shipping with H<sub>2</sub>-based fuels requires resolving major bottlenecks in fleet renovation, NH<sub>3</sub> production and electrolyzer capacity expansion, and renewable electricity supply**

As the current fleet still relies on conventional HFO-ICE propulsion systems, decarbonizing with H<sub>2</sub>-based fuels largely requires

retrofitting existing ships or inducing the entry of new ones. In the early stages, container ships with a capacity below 7999 TEU can be prioritized for adopting H<sub>2</sub>-based fuels, as they contribute a disproportionately high share of GHG emissions relative to their transport work and are relatively old, allowing for greater potential emissions reductions. As H<sub>2</sub>-based fuels are increasingly used to decarbonize maritime shipping, timely development and deployment of new NH<sub>3</sub> production and electrolyzer capacity are essential to ensure stable fuel supply and enable a smooth fleet transition. More importantly, sufficient renewable electricity is fundamental to maximizing the decarbonization potential of H<sub>2</sub>-based fuels in maritime shipping.

## Abbreviations

AE	Alkaline electrolyzers
AIS	Automatic Identification System
BECCS	Bioenergy with carbon capture and storage
BG	Biomass gasification
Bio-LNG	Liquefied biomethane
BOG	Boil-off gas
CCS	Carbon capture and storage
CG	Coal gasification
GHG	Greenhouse gas
H <sub>2</sub>	Hydrogen
HFO	Heavy fuel oil
ICE	Internal combustion engines
IEA	International energy agency
IMO	International maritime organization
LCA	Life cycle assessment
LCI	Life cycle inventory
LNG	Liquefied natural gas
LOHC	Liquid organic H <sub>2</sub> carrier
MeOH	Methanol
MGO	Marine gas oil
NG SMR	Steam methane reforming of natural gas
NH <sub>3</sub>	Ammonia
NZE	Net Zero Emissions by 2050 Scenario
OECD	Organization for Economic Co-operation and Development
PEM	Proton exchange membrane electrolyzers
PEMFC	Proton-exchange membrane fuel cells
SCR	Selective catalytic reduction
SOEC	Solid oxide electrolysis cells
SOFC	Solid oxide fuel cells
SSPs	Shared Socioeconomic Pathways
STEPS	Stated Policies Scenario
ULCVs	Ultra Large Container Vessels

## Conflicts of interest

There are no conflicts to declare.



## Data availability

The data supporting this article have been included as part of the supplementary information (SI). Supplementary information is available. See DOI: <https://doi.org/10.1039/d5ee03477a>.

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