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**EDGE ARTICLE**

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# Direct CO<sub>2</sub> capture and conversion to fuels on magnesium nanoparticles under ambient conditions simply using water†

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Converting CO<sub>2</sub> directly from the air to fuel under ambient conditions is a huge challenge. Thus, there is an urgent need for CO<sub>2</sub> conversion protocols working at room temperature and atmospheric pressure, preferentially without any external energy input. Herein, we employ magnesium (nanoparticles and bulk), an inexpensive and the eighth-most abundant element, to convert CO<sub>2</sub> to methane, methanol and formic acid, using water as the sole hydrogen source. The conversion of CO<sub>2</sub> (pure, as well as directly from the air) took place within a few minutes at 300 K and 1 bar, and no external (thermal, photo, or electric) energy was required. Hydrogen was, however, the predominant product as the reaction of water with magnesium was favored over the reaction of CO<sub>2</sub> and water with magnesium. A unique cooperative action of Mg, basic magnesium carbonate, CO<sub>2</sub>, and water enabled this CO<sub>2</sub> transformation. If any of the four components was missing, no CO<sub>2</sub> conversion took place. The reaction intermediates and the reaction pathway were identified by <sup>13</sup>CO<sub>2</sub> isotopic labeling, powder X-ray diffraction (PXRD), nuclear magnetic resonance (NMR) and *in situ* attenuated total reflectance-Fourier transform infrared spectroscopy (ATR-FTIR), and rationalized by density-functional theory (DFT) calculations. During CO<sub>2</sub> conversion, Mg was converted to magnesium hydroxide and carbonate, which may be regenerated. Our low-temperature experiments also indicate the future prospect of using this CO<sub>2</sub>-to-fuel conversion process on the surface of Mars, where CO<sub>2</sub>, water (ice), and magnesium are abundant. Thus, even though the overall process is non-catalytic, it could serve as a step towards a sustainable CO<sub>2</sub> utilization strategy as well as potentially being a first step towards a magnesium-driven civilization on Mars.

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## Introduction

Excessive CO<sub>2</sub> emissions are a major cause of climate change, and hence reducing the CO<sub>2</sub> levels in the Earth's atmosphere is key to limit adverse environmental effects. Rather than just capturing and storing CO<sub>2</sub>, it would be desirable to use it as carbon feedstock for fuel production, to achieve the target of "net-zero-emissions energy systems".<sup>1–3</sup> Some efficient protocols have been reported for CO<sub>2</sub> conversion,<sup>2–8</sup> but they required external energy by photo-, electro- or thermal activation (which also requires gaseous hydrogen). Thus, any process that could use water as a hydrogen source at room temperature and

atmospheric pressure would be highly sustainable, but no such processes have been reported in the literature to date.

Herein, based on our work in heterogeneous catalysis,<sup>9–13</sup> we report the use of Mg nanoparticles (and bulk) to directly react CO<sub>2</sub> with water at room temperature and atmospheric pressure, forming methane, methanol, and formic acid without requiring external energy sources. Magnesium is the 8<sup>th</sup> most abundant element in the Earth's crust and 4<sup>th</sup> most common element in the Earth (after iron, oxygen and silicon).

Both pure CO<sub>2</sub> and CO<sub>2</sub> in the air were used, while water acted as a hydrogen source. Nanoparticles of Mg are air-stable and can be handled in an open environment. Mg-based catalysts/materials are widely used for organic transformations,<sup>14–20</sup> hydrogen generation, and thermal and electric energy production,<sup>21–23</sup> and there have been few studies of CO<sub>2</sub> and Mg metal/metal oxide interactions.<sup>24–32</sup> However, so far, there are no reports employing Mg for CO<sub>2</sub> conversion to methane, methanol, and formic acid. Herein, we present the first report of how Mg can convert CO<sub>2</sub> to fuel [CO<sub>2</sub> + H<sub>2</sub>O + Mg → CH<sub>4</sub> + CH<sub>3</sub>OH + HCOOH + H<sub>2</sub> + Mg<sub>5</sub>(CO<sub>3</sub>)<sub>4</sub>(OH)<sub>2</sub>·4H<sub>2</sub>O], which proceeds at room temperature without any external energy. The mechanism of this process is determined by several independent (also *in situ*)

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techniques, backed-up by theoretical calculations. This study demonstrates the first step towards sustainable CO<sub>2</sub> utilization to produce fuel and chemicals.

## Results and discussion

Transmission electron microscopy (TEM) indicated that the Mg nanoparticles (NPs) were aggregates with sizes ranging from 200 to 500 nm (Fig. 1a, inset), composed of nanocrystals. Powder X-ray diffraction (PXRD, Fig. 1a) analysis confirmed the crystallinity of the Mg nanoparticles, with N<sub>2</sub> sorption indicating a specific surface area of 13 m<sup>2</sup> g<sup>-1</sup> (Fig. S1†). Elemental analysis by EDX showed the presence of Mg and oxygen (Table S1†), indicating the presence of the MgO layer on the Mg NP surface. The average crystallite size calculated using Scherrer's equation was found to be 32 nm. The CO<sub>2</sub> reduction reaction on Mg NPs in water was evaluated in a batch reactor at room temperature and atmospheric pressure. The products were identified and quantified by online gas chromatography (micro GC) with a thermal conductivity detector (TCD). Conversion of CO<sub>2</sub> in air yielded 3.5 μmol methane per gram Mg in just 10 minutes (Fig. 1b). For pure CO<sub>2</sub> gas, ~100 μmol methane g<sup>-1</sup> was obtained in 15 minutes (Fig. 1c).

Next, we studied the performance of bulk Mg powders and Mg-alloys with Al, Ni, and Ca. Even bulk (granules) and micron-sized (powder) Mg converted CO<sub>2</sub> to methane with good yield (Fig. 1d and Table S2†), but at a slower rate than nanoparticles. This indicated that the nano-size of the Mg NPs, leading to high specific surface area (SSA), facilitated efficient chemisorption of CO<sub>2</sub> and water on the Mg surface, accelerating methane formation. MgH<sub>2</sub> and pure calcium did not produce any methane (Fig. 1d), suggesting that the bare Mg<sup>0</sup> surface was necessary. Mg–Al, Mg–Ni, and Mg–Ca alloys showed less methane formation than Mg NPs (Fig. 1d and Table S2†), indicating a unique behavior of pure Mg for CO<sub>2</sub> conversion. The liquid reaction mixtures were analyzed by <sup>1</sup>H nuclear magnetic resonance (NMR) spectroscopy and the formation of methanol and formic acid was also observed (Fig. 1e and f). Mg NPs yielded 25.6 μmol g<sup>-1</sup> of methanol and 26.2 μmol g<sup>-1</sup> of formic acid. Bulk Mg, as well as its alloys, also yielded methanol and formic acid, but a lower amount than yielded by Mg NPs. MgH<sub>2</sub> and Ca produced only minute amounts of methanol and formic acid, confirming their lower ability to adsorb and activate CO<sub>2</sub>. The Mg nanoparticles showed selectivity of 65.8, 16.7 and 17.2% for methane, methanol and formic acid production, respectively (Fig. S2†).



**Fig. 1** (a) PXRD patterns (TEM image in the inset) of Mg NPs along with the standard XRD pattern of Mg (JCPDS no. 01-089-7195); cumulative methane yield with reaction time for CO<sub>2</sub> reduction by Mg NPs using (b) CO<sub>2</sub> directly from the air and (c) 99.99% CO<sub>2</sub>; (d) comparison of yields of various metals and Mg–metal alloys (99.99% CO<sub>2</sub>); (e) methanol, formic acid, and methane yields after 1 h, for CO<sub>2</sub> (99.99%) reduction on Mg NPs, micro powder and bulk Mg, Mg–metal alloys, MgH<sub>2</sub> and Ca metal; (f) methane, methanol, and formic acid yield quantified after 1, 5, and 15 min, for reduction of CO<sub>2</sub> using Mg NPs. All reactions were carried out in water at room temperature and atmospheric pressure. Error bars are omitted in (d) for clarity and were less than 10%. The selectivity for carbon-containing products such as methane, methanol and formic acid is given in Fig. S2.†



Table 1 Comparison of metal-assisted CO<sub>2</sub> conversion under atmospheric conditions, using water as a hydrogen source

S. N.	Material	CO <sub>2</sub> source	Energy source	Reaction time (h)	Methane yield (μmol g <sup>-1</sup> )	Methanol yield (μmol g <sup>-1</sup> )	Product (methane + methanol) formation rate (μmol g <sup>-1</sup> h <sup>-1</sup> )	Ref.
1	Mg NPs	Pure CO <sub>2</sub>	No external energy <sup>a</sup>	0.4	100 ± 10%	25.6 ± 10%	314	This work
2	Mg NPs	CO <sub>2</sub> from air	No external energy <sup>a</sup>	0.1	3.5 ± 10%	2.4 ± 12%	59	This work
3	Pd <sub>7</sub> Cu <sub>1</sub> /TiO <sub>2</sub>	Pure CO <sub>2</sub>	UV light (2 mW cm <sup>-2</sup> )	1	19.6	0	19.6	35
4	Rb <sub>0.33</sub> WO <sub>3</sub>	Pure CO <sub>2</sub>	UV to NIR (300 W Xe lamp)	4	0	60	15	33
5	Rb <sub>0.33</sub> WO <sub>3</sub>	CO <sub>2</sub> from air	UV to NIR (300 W Xe lamp)	4	0	9	2.25	33
6	Au-Co	Pure CO <sub>2</sub>	VIS light (100 mW cm <sup>-2</sup> )	1	0.13	0	0.13	36
7	Black gold	Pure CO <sub>2</sub>	VIS to NIR light (1 W cm <sup>-2</sup> )	12	1.5	0	0.125	11
8	Au NPs	Pure CO <sub>2</sub>	VIS light (300 mW cm <sup>-2</sup> )	10	0.63	0	0.063	34

<sup>a</sup> No external energy means energy available in the reaction vessel at room temperature is sufficient for this reaction to proceed.

## CO<sub>2</sub> conversion process efficiency comparison

Table 1 summarizes some of the best (to our knowledge) CO<sub>2</sub> (from the air or pure) conversion processes under ambient conditions.<sup>11,33–36</sup> Our Mg process produced 314 μmol g<sup>-1</sup> h<sup>-1</sup> total products when pure CO<sub>2</sub> was used, which was significantly higher than those produced by the best-known catalysts, Pd<sub>7</sub>Cu<sub>1</sub>/TiO<sub>2</sub> (19.6 μmol g<sup>-1</sup> h<sup>-1</sup>),<sup>35</sup> or Rb<sub>0.33</sub>WO<sub>3</sub> (15 μmol g<sup>-1</sup> h<sup>-1</sup>),<sup>33</sup> both using high-power UV light (Table 1, S. N. 3 and 4). The Mg-assisted CO<sub>2</sub> conversion efficiency was also better than that of Au-catalysts (0.063–0.13 μmol g<sup>-1</sup> h<sup>-1</sup>, Table 1, S. N. 6–8).<sup>11,34,36</sup> Even for CO<sub>2</sub> directly from the air, Mg showed a productivity of 59 μmol products g<sup>-1</sup> h<sup>-1</sup>, while the highest reported value so far was 2.25 μmol products g<sup>-1</sup> h<sup>-1</sup> using Rb<sub>0.33</sub>WO<sub>3</sub>, which requires high power UV light (Table 1, S. N. 5). Thus, Mg NPs are a very good alternative to photocatalysts for sustainable CO<sub>2</sub> to fuel conversion under ambient conditions.

The comparison of a non-catalytic process with catalytic ones seems inappropriate. However, this is intentionally made to demonstrate that this Mg process, even being not catalytic, is still efficient and more sustainable than reported room temperature catalytic processes. For example, the Mg protocol yields 100 μmol g<sup>-1</sup> methane in 0.4 h and to achieve the same methane yield, an Au catalyst needed 1587 h, *i.e.* 66 days (and solar energy for 66 days).<sup>34</sup> None of the reported room temperature nano-catalysts showed stability for 1587 h and were often deactivated in just 12 to 24 h (Table 1). Thus, catalysts are not consumed by definition, but in reality, most of them get deactivated in a few hours (“indirectly consumed”). The deactivated catalysts can be ideally regenerated/activated, but this has a substantial energy penalty and hydrogen gas consumption (and in the case of deactivation by nanoparticle sintering, no regeneration is possible). In contrast, Mg regeneration can be carried out by using a solar energy-driven laser without any hydrogen gas and for only 1 USD per kg.<sup>21</sup>

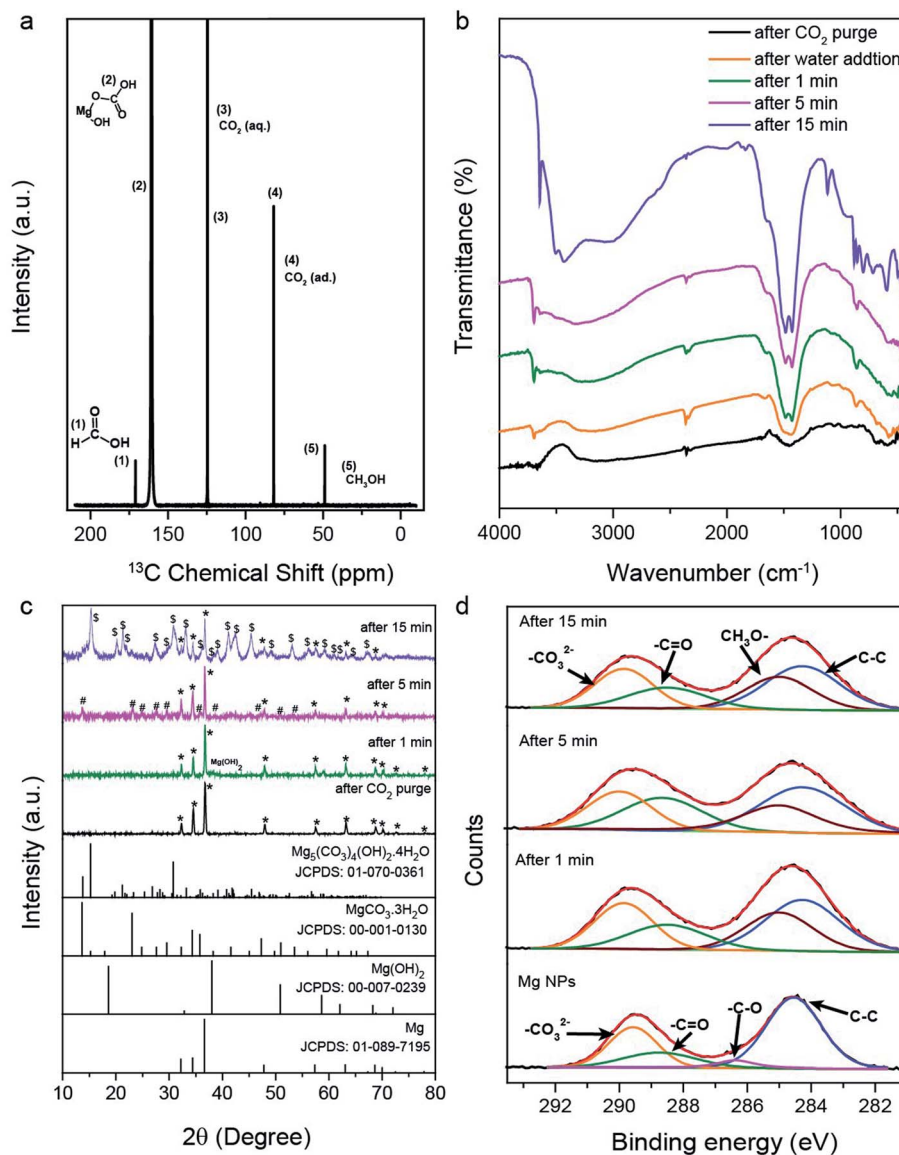
To prove that CO<sub>2</sub> was indeed the carbon source of products, a control experiment was conducted in argon gas (without CO<sub>2</sub>), in which the formation of methane, methanol and formic acid was not observed. For further confirmation, we used isotopically labeled <sup>13</sup>CO<sub>2</sub> and analyzed the products by GC (Fig. S2†) and <sup>13</sup>C NMR spectroscopy (Fig. 2a). The <sup>13</sup>C NMR spectrum (Fig. 2a) indicated methanol and formic acid. As a further control experiment, unlabeled CO<sub>2</sub> was used. The formation of methanol and formic acid was evident from <sup>1</sup>H NMR, whereas no <sup>13</sup>C signal was obtained with the same NMR pulse sequence and the total number of scans (Fig. S1b†). This was due to the low natural abundance (1%) of <sup>13</sup>C in unlabeled CO<sub>2</sub> (Fig. S1b†). The reaction products were monitored after 0, 1, 5, 15, 30 and 60 min reaction time, using a GC with TCD, flame ionization detector (FID) and mass spectrometer (MS). The reduction of <sup>13</sup>CO<sub>2</sub> produced isotopic <sup>13</sup>CH<sub>4</sub> (*m/z* = 17, Fig. S1g†), which confirmed CO<sub>2</sub> as a carbon source for methane, methanol, and formic acid.

## Reaction mechanism of Mg mediated CO<sub>2</sub> conversion

To examine the overall reaction pathway, we characterized surface species and (intermediate) products after CO<sub>2</sub> and water







**Fig. 2** (a)  $^{13}\text{C}$  NMR spectrum of the reaction mixture (using labeled  $^{13}\text{C}$ CO $_2$ ) after 1 h of reaction on Mg NPs; (b) FTIR spectra, (c) PXRD patterns and (d) XPS C 1s spectra of solid products recovered after 1, 5, and 15 min of the reaction of CO $_2$  with Mg NPs and water, at room temperature and atmospheric pressure. (\*Mg metal, #MgCO $_3$ ·3H $_2$ O and  $^{\text{S}}$ Mg $_5$ (CO $_3$ ) $_4$ (OH) $_2$ ·4H $_2$ O). Standard XRD patterns of Mg (JCPDS no.: 01-089-7195), Mg(OH) $_2$  (JCPDS no.: 00-007-0239), MgCO $_3$ ·3H $_2$ O (JCPDS no.: 00-001-0130) and Mg $_5$ (CO $_3$ ) $_4$ (OH) $_2$ ·4H $_2$ O (JCPDS no.: 01-070-0361) are included in (c). In (d), orange  $-\text{CO}_3^{2-}$ , green  $-\text{C}=\text{O}$ , violet  $-\text{C}-\text{O}$ , blue  $-\text{C}-\text{C}$ , and purple  $-\text{CH}_3-\text{O}$ .

addition, and after 1, 5 and 15 min reaction time. Increasing levels of methane, methanol and formic acid yields were observed upon increase in reaction time (Fig. 1f). The solid reaction mixture was then isolated, dried and analyzed by diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) and PXRD (Fig. 2b and c). The IR spectrum of the Mg NPs after exposure to only CO $_2$  showed a broad absorption at 1259–1621  $\text{cm}^{-1}$ , indicating adsorbed carbonate species.<sup>37</sup> The FTIR spectrum of the sample after 15 min reaction time contained bands corresponding to carbonate species of basic magnesium carbonate [Mg $_5$ (CO $_3$ ) $_4$ (OH) $_2$ ·4H $_2$ O].<sup>38,39</sup> IR analysis thus indicated the formation of magnesium carbonate within 1 and 5 min, and basic magnesium carbonate after 15 min of reaction. Corresponding PXRD patterns (Fig. 2c) confirmed the

formation of magnesium carbonate at 5 min and basic carbonate after 15 min. A small amount of Mg was still present at 15 min of reaction time, although product formation was nearly stopped at this stage. However, when we recorded the PXRD patterns of the products recovered after 1 h of reaction (Fig. S4†), the Mg signal was not observed. This indicates that the small amount of Mg present at 15 min is catalytically active; however, its contribution was so small that the increase in product yield was not detected in the GC, although those traces of Mg reacted and vanished during 1 h reaction time.

The reaction mechanism was also investigated by *ex situ* X-ray photoelectron spectroscopy (XPS), with Mg 2p, C 1s, and O 1s spectra of the solid materials acquired after 1, 5, and 15 minutes of reaction (Fig. 2d and S3†). For Mg NPs (before



reaction), C 1s indicated adsorbed carbonates (289.4 eV; orange), carbonyl (288.7 eV; green), C–O (286.4 eV; magenta) and carbon (284.5 eV; blue) (Fig. 2d).<sup>40,41</sup> The C 1s spectra of samples recovered after different reaction times show peaks at 285.0, 288.6, 289.9 and 284.2 eV, corresponding to  $-\text{OCH}_3$ ,<sup>42</sup> the carbonyl group of formate, carbonate, and support carbon, respectively. The contribution of carbonyl, carbonate and  $-\text{OCH}_3$  species increased with reaction time, indicating that they are the intermediates formed during the reaction (Table S3†).

The XPS data (Fig. S3a†) are in accordance with *ex situ* FTIR (Fig. 2b) and PXRD (Fig. 2c) analysis. The O 1s XPS peaks at 529.39 (blue), 531.29 (green) and 532.78 eV (orange) correspond to MgO,<sup>43</sup> Mg(OH)<sub>2</sub> and magnesium carbonate species, respectively (Fig. S3a†).<sup>40</sup> In O 1s, magnesium methoxide and hydroxide appear at a similar binding energy of 531.29 eV.<sup>42</sup> As the reaction proceeded, the contributions of carbonate, hydroxide and methoxide were found to increase. The Mg 2p of the solid recovered at different time intervals showed four different peaks at 48.6, 49.3, 50.3 and 51.07 eV, again attributed to Mg,<sup>44</sup> MgO, Mg(OH)<sub>2</sub>/Mg–OCH<sub>3</sub> and magnesium carbonate, respectively (Fig. S3b†);<sup>40,42,44,45</sup> the latter three contributions increased as the reaction proceeded, indicating the CO<sub>2</sub> conversion to products *via* these intermediates.

To corroborate that (basic) carbonate species were reaction intermediates, the reaction progress of the purged reactor was then further monitored with time (Fig. S4†) and, the formation of methane was still observed, confirming that

basic magnesium carbonates were reaction intermediates, which were then converted to methane. These studies suggest that water, CO<sub>2</sub>, and surface atoms of the Mg NPs react to produce intermediate basic magnesium carbonate, while Mg atoms in the sub-surface layers acted as an electron donor for the reduction step. The effect of the MgO shell (surface layer) was studied by Mg oxidation in air at 80 °C for 1, 3, and 11 days (Fig. S5a†). There was no significant effect on product yield (Fig. S5b†), indicating no role of MgO, and even pure MgO showed no methane, methanol and formic acid formation.

*In situ* attenuated total reflectance-Fourier transform infrared spectroscopy (ATR-FTIR) was employed to examine the mechanistic pathways under reaction conditions of CO<sub>2</sub> conversion on Mg NPs by using water (Fig. 3). When CO<sub>2</sub> gas was passed over the (pretreated, Fig. S6†) Mg surface at room temperature, a doublet appeared from the asymmetric stretching mode of CO<sub>2</sub> gas, which after switching to He transformed into a singlet at 2341 cm<sup>-1</sup>, characteristic of the stretching mode of CO<sub>2</sub> chemisorbed on the Mg surface (Fig. 3a). The presence of additional weak absorption bands in the region of 2800–3000 cm<sup>-1</sup>, corresponding to the C–H stretching modes (inset of Fig. 3b), indicates that the conversion of CO<sub>2</sub> into hydrocarbons was initiated in the presence of H<sub>2</sub>O traces. Furthermore, when the Mg NPs were first exposed to water, He, and then CO<sub>2</sub> gas, signals for unidentate carbonate (1511, 1392 and 1052 cm<sup>-1</sup>), bidentate carbonate (1666, 1346 and 1007 cm<sup>-1</sup>), bicarbonates (1626, 1409 and 1273 cm<sup>-1</sup>), MgCO<sub>3</sub>·3H<sub>2</sub>O

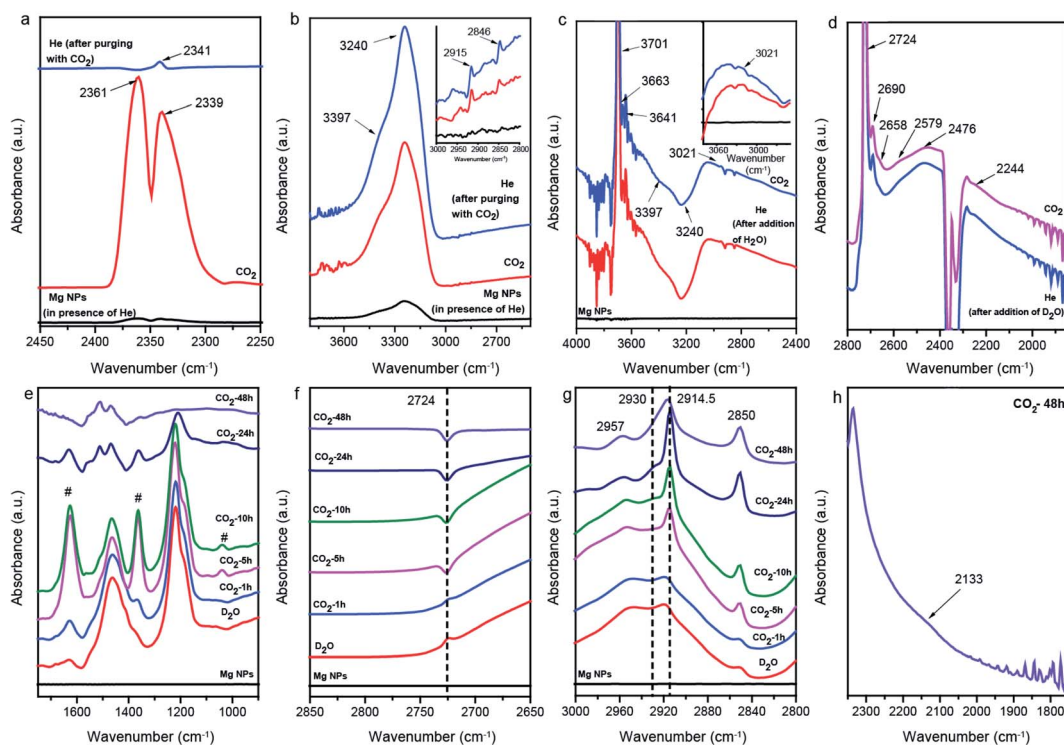


Fig. 3 *In situ* ATR-FTIR spectra: (a and b) in He, CO<sub>2</sub>, and again He, (c) after adding H<sub>2</sub>O to the Mg NPs and subsequently purging with He and CO<sub>2</sub> gas, (d) after adding D<sub>2</sub>O to the Mg NPs and subsequently purging with He and CO<sub>2</sub> gas, and (e–h) after adding D<sub>2</sub>O to the Mg NPs and then purging with CO<sub>2</sub> for 1, 5, 10, 24 and 48 h.





yielding methanol. Species (VI) on further reduction forms a methyl radical intermediate (VII), which is then reduced by H<sup>•</sup> to yield methane. The formed magnesium hydroxide (IX) reacts with CO<sub>2</sub> to give basic carbonate (I). Ideally, the reaction cycle should continue, but the product concentration saturated after approximately 15 min and no further reaction was observed due to the nearly complete conversion of Mg to basic carbonate, leaving no unreacted Mg to act as an electron donor. Mg can then be regenerated, *e.g.* by using a solar-energy pumped laser.<sup>53,54</sup>

To confirm that a water proton was reduced to a H<sup>•</sup> radical by an electron from Mg, CO<sub>2</sub> conversion was carried out using gaseous hydrogen (with no water present). When H<sub>2</sub> was used, no methane, methanol and formic acid formation occurred, supporting the proposed role of water in the mechanism.

Another aspect to consider is that if Mg(0) transformed into Mg(II) upon reaction with water, it would no longer be able to provide electrons for CO<sub>2</sub> reduction. Once Mg metal is exposed

to water, a layer (or shell) of poorly soluble magnesium hydroxide forms on the Mg NP surface. The presence of this layer on the surface restricts the contact of H<sub>2</sub>O with sub-surface Mg metal present underneath. However, in the presence of CO<sub>2</sub>, this magnesium hydroxide layer interacts with CO<sub>2</sub> to form basic magnesium carbonate, which has a higher water solubility than magnesium hydroxide. The presence of metallic Mg during the reaction was observed in the PXRD pattern (Fig. 2c), while its interactions with CO<sub>2</sub> were detected in FTIR (Fig. 2b and 3) and NMR (Fig. 2a) spectra. The Mg atoms in the sub-surface layers transfer electrons to basic carbonate on the surface layers, converting it to methane, methanol and formic acid. As the basic magnesium carbonate is soluble in water, it does not restrict the access of fresh reactant molecules (H<sub>2</sub>O and CO<sub>2</sub>) to the Mg atoms present underneath the layer. This process continues till Mg metal is consumed. Thus, various *ex situ* and *in situ* studies fully support the reaction mechanism proposed in Fig. 4.

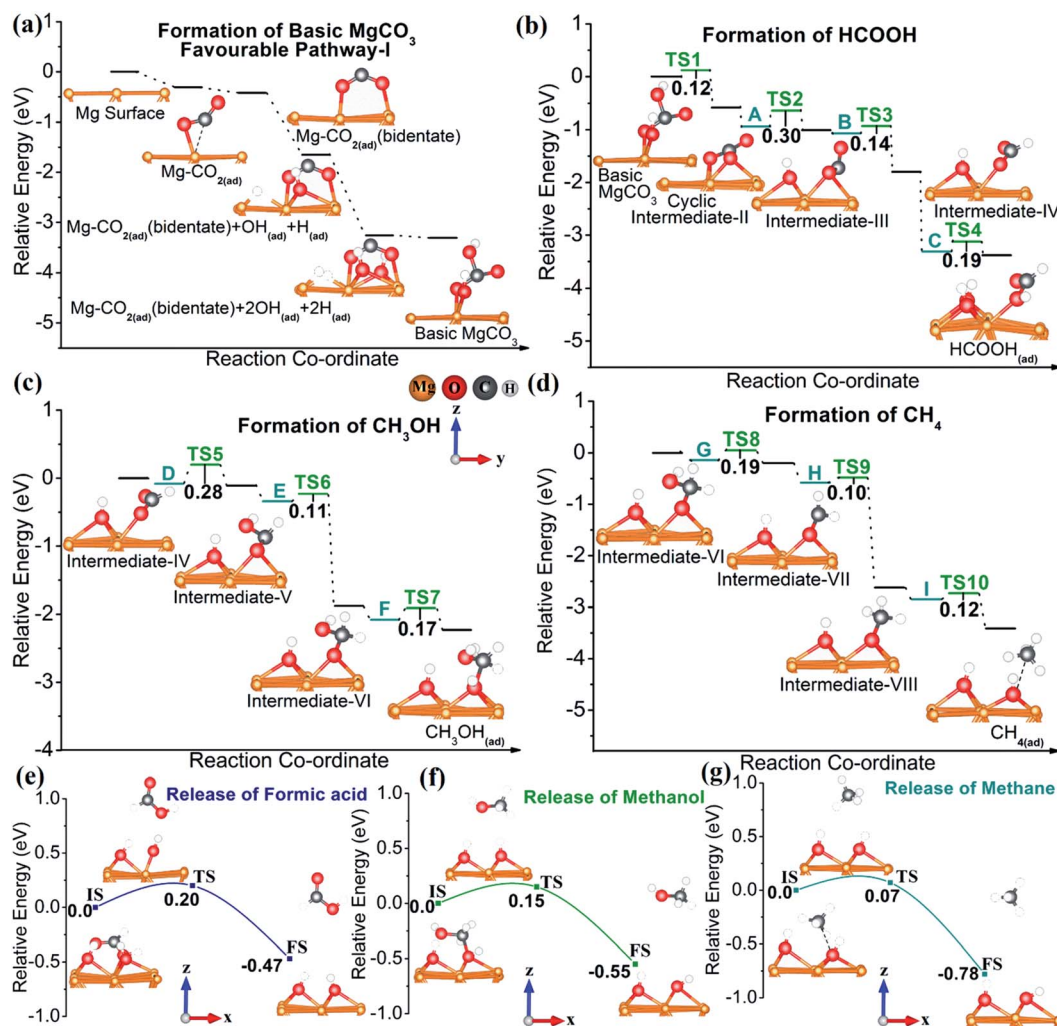


Fig. 5 Potential energy surface (PES) for CO<sub>2</sub> reduction: (a) formation of basic MgCO<sub>3</sub> via pathway-I (for the PES of pathways-II & III see Fig. S10 and S11 in the ESI<sup>†</sup>), (b) formation of formic acid, (c) formation of methanol, and (d) formation of methane; release steps of different products from the Mg NP surface during CO<sub>2</sub> reduction to (e) formic acid, (f) methanol, and (g) methane. z,y coordinates shown in (c) are the same for (a, b and d).





## Density functional theory (DFT) study of the CO<sub>2</sub> conversion process

In order to confirm and refine the proposed mechanistic pathways, we have performed a density functional theory (DFT) study, based on first-principles calculations using the Vienna *Ab Initio* Simulation Package (VASP).<sup>55</sup> CO<sub>2</sub> activation is the key step in the CO<sub>2</sub> reduction reaction.<sup>56–58</sup> Upon adsorption on the Mg surface, the linear CO<sub>2</sub> molecule gets bent, with one of the oxygen atoms strongly adsorbing on Mg while the carbon atom weakly interacts with Mg (Fig. 5a, S9 and Table S4†). Based on the experimental results, the activation of CO<sub>2</sub> may proceed through three different probable pathways (Fig. 5a and S9†) towards MgCO<sub>3</sub> formation. As depicted in Fig. 5a, S9 and S10† both pathways I & II (CO<sub>2</sub> adsorption on pristine and hydrated Mg (Mg–OH<sub>(ad)</sub> + H<sub>(ad)</sub>) surfaces, respectively) are thermodynamically favorable as all the steps are downhill of the potential energy surface (PES). In contrast, pathway-III (where CO<sub>2</sub> activation occurs on the Mg(OH)<sub>2</sub> surface) is thermodynamically unfavorable, due to the uphill CO<sub>2</sub> adsorption step in the PES (Fig. S11, S9e and f†). Furthermore, CO<sub>2</sub> is activated more effectively in pathways I & II than in pathway-III (Fig. S9 and Table S4†), following an activation order: pathway-I ≥ pathway-II ≫ pathway-III. The CO<sub>2</sub> adsorption energy of the most feasible pathway (pathway-I) is –0.31 eV, paralleled by lengthening of the C=O bond from 1.16 Å (equilibrium bond length) to 1.22 and 1.19 Å, and a change of the OCO bond angle from 180 to 141°. Both clearly suggest a more efficient CO<sub>2</sub> activation.<sup>56–58</sup> In addition, Bader charge analysis<sup>59,60</sup> indicates a charge transfer of 0.17e from Mg to CO<sub>2</sub> and a charge density difference (CDD) plot further supports CO<sub>2</sub> activation through negative charge localization on the carbon atom (Fig. S12†).

Fig. 5b shows the relative energy diagram of all elementary steps involved in formic acid formation from basic MgCO<sub>3</sub>. The downhill pathway from basic MgCO<sub>3</sub> to surface-adsorbed HCOOH proves the thermodynamic feasibility of HCOOH formation. As evident from Fig. 5b and S13a–c,† the low activation barriers (*i.e.* ≤ 0.3 eV) also suggest kinetic viability of the proposed pathway at room temperature and ambient pressure. The high stabilization energy of C (*i.e.* hydrated intermediate-IV) accounts for the formation of formic acid. The formation of methanol also shows a downhill pathway for each elementary step (Fig. 5c and S13d–f). Apart from this, the methanol pathway is kinetically feasible with activation barriers of the elementary steps less than 0.3 eV (Fig. 5c). Interestingly, the route to CH<sub>4</sub> formation is not only thermodynamically highly feasible, with each of the elementary steps downhill, but also kinetically accessible under the experimental conditions. A close look at the relative energy diagram (Fig. 5d) demonstrates that the formation of surface-adsorbed CH<sub>4</sub> (CH<sub>4(ad)</sub>) on Mg occurs from intermediate-VIII, *via* I abstracting two protons from adjacent sites (Fig. S13i†). The reaction pathway for CH<sub>4</sub> formation reveals that the breakage of the C–O bond (carbon atom from CH<sub>4(ad)</sub>) and the O atom adsorbed on Mg) is essential for the formation of gaseous CH<sub>4</sub> (Fig. 5e and S14c†). A detailed analysis of CH<sub>4(ad)</sub> discloses that the C–O bond distance for CH<sub>4(ad)</sub> is 2.6 Å while the equilibrium C–O bond length is 1.43 Å (Fig. S9

and Table S4†). This pronounced lengthening of the C–O bond in the CH<sub>4(ad)</sub> state clearly indicates the high feasibility of CH<sub>4</sub> formation, both thermodynamically and kinetically. Accordingly, a close analysis of HCOOH<sub>(ad)</sub> and CH<sub>3</sub>OH<sub>(ad)</sub> reveal the necessity of Mg–O (bond between the Mg surface and O atom of HCOOH<sub>(ad)</sub>) and C–O (C atom of CH<sub>3</sub>OH<sub>(ad)</sub> and the adsorbed O atom on Mg) bond breaking, respectively. As expected, these bonds are elongated with respect to their equilibrium bond lengths, indicating a weak interaction between the Mg surface and these adsorbed species (Fig. 5f–g, S14a, b and Table S5†). Most importantly, the extent of bond elongation follows the order HCOOH<sub>(ad)</sub> ≤ CH<sub>3</sub>OH<sub>(ad)</sub> < CH<sub>4(ad)</sub>, indicating that the formation of molecular CH<sub>4</sub> is most feasible. Therefore, a relatively low kinetic barrier and high reaction energy (*E<sub>r</sub>*) make methane formation more feasible than that of HCOOH and CH<sub>3</sub>OH (*E<sub>r</sub>* for CH<sub>4</sub> is –0.68 eV, whereas for HCOOH and CH<sub>3</sub>OH it is –0.26 and –0.32 eV, respectively).<sup>57</sup>

The release of the product species also affects the reaction rate,<sup>10,57</sup> with HCOOH and CH<sub>3</sub>OH having low desorption activation barriers from Mg of 0.2 and 0.15 eV, respectively (Fig. 5e and f). However, methane desorption from the Mg surface is remarkably facile with a low activation barrier of 0.07 eV for activation compared to those of HCOOH (*c.f.* activation barrier = 0.20 eV) and CH<sub>3</sub>OH (*c.f.* activation barrier = 0.15 eV) (Fig. 5g). Hence, based on both experimental findings and theoretical calculations, the Mg NP surface can indeed convert CO<sub>2</sub> to HCOOH, CH<sub>3</sub>OH, and CH<sub>4</sub>, with the latter dominating at room temperature and ambient pressure.

There are a few “uphill” increments in energy barriers during various elementary steps, as well as during desorption (to release product species from the Mg surface), which need to be overcome before the following step(s) can take place. As evident from the relative energy diagram (Fig. 5), the maximum activation energy barrier for the transition state is 0.3 eV, *i.e.* 29 kJ mol<sup>–1</sup>, which is in the range of room temperature activation energy barriers for elementary reactions. Along with that, the desorption activation barriers for formic acid, methanol and methane are low (0.2, 0.15 and 0.07 eV respectively). Therefore, the activation energy barriers for the transition states, as well as the desorption steps can be easily overcome at room temperature.

Furthermore, magnesium has a standard electrode potential of –2.69 V *vs.* the standard hydrogen electrode. As the standard reduction potential of Mg is more negative than the reduction of water, Mg readily reacts with water to form hydrogen.<sup>23</sup> The reaction of magnesium with water (Mg + H<sub>2</sub>O → Mg(OH)<sub>2</sub> + H<sub>2</sub>) is exothermic (Δ*H* = –354 kJ mol<sup>–1</sup>),<sup>22</sup> and this released energy can also be used to overcome the energy barriers. Thus, under reaction conditions, it is basically the surrounding environment that provides the small energy to overcome the activation barriers. Note that this is a “no external energy” process and not a “no energy” process.

### Process sustainability

The crucial magnesium electrolysis step to produce magnesium from Mg<sup>2+</sup> requires low energy,<sup>61</sup> and Mg is one of the metals with the lowest energy demand for production (Fig. S15†).<sup>62,63</sup>



CO<sub>2</sub> produced by other metals, as compared to Mg, is summarised in Fig. S16,† indicating that Mg is one of the metals producing the lowest amount of CO<sub>2</sub> during production. If one compares the price of methane produced by our Mg protocol with the price of methane produced by other reported protocols (Table S6†), one can see nearly a million times difference in cost. This is because Mg is 45 000–50 000 times cheaper than all other well-known metal catalysts for CO<sub>2</sub> reduction, and the Mg process has far better CO<sub>2</sub> conversion efficiency/productivity than the reported catalysts.

Hydrogen yield with reaction time during the reduction of CO<sub>2</sub> at room temperature and ambient pressure is given in Fig. S17.† Notably, in the absence of CO<sub>2</sub>, Mg does not react efficiently with water and hydrogen yield was extremely low, 100 μmol g<sup>-1</sup> as compared to 42 000 μmol g<sup>-1</sup> in the presence of CO<sub>2</sub>. This was due to poor solubility of magnesium hydroxide formed by the reaction of Mg with water, restricting the internal Mg surface to react further with water. However, in the presence of CO<sub>2</sub>, magnesium hydroxide gets converted to carbonates and basic carbonates, which are more soluble in water than magnesium hydroxide and get peeled off from Mg, exposing a fresh Mg surface to react with water. Thus, this protocol can even be used for hydrogen production (940 mL g<sup>-1</sup>), which is nearly 420 times more than the hydrogen produced by the reaction of Mg with water alone (2.24 mL g<sup>-1</sup>).

Using this protocol, 1 kg of magnesium *via* simple reaction with water and CO<sub>2</sub> produces 2.43 liters of methane, 940 liters of hydrogen (Fig. S17†) and 3.85 kg of basic magnesium carbonate (green cement), and also small amounts of methanol, and formic acid. Thus, it is important to note that hydrogen was the predominant product, as the reaction of water with magnesium was preferred over the reaction of CO<sub>2</sub> and water with magnesium.

Notably, this entire production happens in just 15 minutes, at room temperature and atmospheric pressure, in this exceptionally simple and safe protocol. Unlike other metal nanoparticles, the nano-Mg powder is extremely stable and can be handled in air without any loss in activity. If the use of fossil fuels and natural methane gets banned or restricted, there will be a need for a CO<sub>2</sub> neutral process for various chemicals and fuels (methane, methanol, formic acid and hydrogen). This Mg protocol will then be the cheapest of any other reported CO<sub>2</sub> conversion protocols in the literature to date. Further considerations with respect to the Mg process sustainability (energy demand, CO<sub>2</sub> production and global warming impact) are discussed in ESI, Fig. S15 and S16.†

Regeneration of the consumed Mg NPs is required to make the whole CO<sub>2</sub> conversion process feasible and this can be achieved *via* a commercially available process.<sup>21,53</sup> It is thus essential to note that although no external energy is required during the CO<sub>2</sub> conversion process, external energy is required to regenerate Mg. Recently, Mg was regenerated for ~1 USD per kg of Mg using a solar-energy pumped laser.<sup>53,54</sup> The product magnesium hydroxide carbonate can also be used as green cement.<sup>64</sup> Accordingly, the Mg-assisted CO<sub>2</sub> conversion process is economical, even though it is non-catalytic. Also, the Mg nanopowder is stable due to the presence of a thin MgO passivation surface layer and can be stored in air without loss of

activity (Fig. S5†). There was no need to remove the thin MgO layer before the reaction, as it reacted with water to form magnesium hydroxide. This makes the overall process safe.

### Magnesium assisted CO<sub>2</sub> conversion to fuel on the Mars' surface

Planet Mars' environment has 95.32% of CO<sub>2</sub>, while its surface has water in the form of ice. Recently, the presence of magnesium on Mars in abundant amounts was also reported.<sup>65–67</sup> Therefore, to explore the possibility of the use of this Mg-assisted CO<sub>2</sub> conversion process on Mars, we carried out this Mg-assisted CO<sub>2</sub> conversion at -1 to +1 °C temperature. Notably, methane was produced in a reasonable amount (35 μmol g<sup>-1</sup>) in just 20 minutes, although at a slower rate as compared to the room temperature reaction (Fig. S18†), due to the low reaction temperature. A good amount of methanol (28 μmol g<sup>-1</sup>) and formic acid (37 μmol g<sup>-1</sup>) formation was also observed. These results indicate the potential of this Mg-process to be used in the Mars' environment, a step towards magnesium utilization on Mars, although more detailed studies are needed.

## Conclusions

Magnesium converted CO<sub>2</sub> (directly from the air or pure) at room temperature and atmospheric pressure to methane, methanol, and formic acid, using water as the hydrogen source. No external energy (such as light, heat, or electricity) was required. The reaction was very fast, with a maximum product yield after 15 min. Hydrogen was predominant as compared to carbon-based products, as the reaction of water with magnesium was favored over the reaction of CO<sub>2</sub> and water with magnesium. Although Mg was converted to basic magnesium carbonate, its regeneration to Mg NPs is possible using a solar-energy pumped laser process.

We observed a unique ability of Mg not only to chemisorb and activate CO<sub>2</sub> but also to transfer electrons to facilitate CO<sub>2</sub> reduction. We observed a distinctive cooperative action of magnesium, basic magnesium carbonate, CO<sub>2</sub>, and water to convert CO<sub>2</sub> to methane, methanol, and formic acid. <sup>13</sup>C isotopic labeling experiments, *ex situ* PXRD, NMR, FTIR, XPS and *in situ* ATR studies identified the relevant reaction intermediates and reaction mechanism, which was supported by density functional theory (DFT).

Thus, it was demonstrated for the first time that magnesium (nanoparticles and bulk), an inexpensive and the eighth-most abundant element, converted pure CO<sub>2</sub> (as well as CO<sub>2</sub> from the air) to fuel at room temperature using only water as the hydrogen source. This Mg-process has the potential to be used in the Mars' environment for fuel production.

## Experimental

### Characterization

Electron microscopy imaging was performed on an FEI Tecnai transmission electron microscope. Samples were prepared by



drop-casting diluted ethanolic suspensions of the relevant powder onto a copper grid (for TEM). PXRD patterns were obtained using a Panalytical X'Pert Pro powder X-ray diffractometer with Cu-K $\alpha$  radiation. FTIR spectra were recorded using a JASCO FT/IR-4700. N<sub>2</sub> adsorption measurements were performed using a Micromeritics 3-Flex Surface Analyzer. The samples were degassed at 110 °C overnight before analysis. The NMR study was carried out using a Bruker AVANCE II spectrometer  $B_0 = 9.4T$  ( $V_0 = 800$  MHz for <sup>1</sup>H). Methanol and formic acid were identified by <sup>1</sup>H NMR spectroscopy and quantified by using the external calibration method. <sup>13</sup>C NMR spectroscopy was used to identify the liquid products of the labeled <sup>13</sup>CO<sub>2</sub> experiment, and gaseous products of the labeled <sup>13</sup>CO<sub>2</sub> experiment were analyzed by using a gas chromatograph equipped with a TCD, FID and mass spectrometer (Agilent 7890B, Agilent Technologies), and an Agilent hybrid column CP7430 and helium as a carrier gas. XPS analysis was carried out using a Thermo K $\alpha$  spectrometer with micro-focused and monochromated Al-K $\alpha$  radiation (1486.6 eV) as the X-ray source. A pellet of the magnesium powder was made and fixed on carbon tape. The carbon signal at 284.6 eV was used as an internal reference. Peak fitting of the spectra was performed using an XPSPEAK 4.1 by using a Shirley background.

### CO<sub>2</sub> reduction experiments

CO<sub>2</sub> conversion was carried out by taking 50 mg of Mg (or other metals/alloys) in a 350 mL batch reactor. The Mg nanopowder, its alloy and other metals were purchased from Nanoshel Inc. with purity > 99.9%. All the samples were used without further purification.

Initially, 50 mg of magnesium was taken in a round bottom (RB) flask with a volume of 350 mL and then sealed with a rubber septum. With the help of a needle, CO<sub>2</sub> gas was purged into the RB flask for 30 min (optimized) for better contact with Mg surfaces. The flow of the gas was controlled using a mass flow controller (MFC). After purging, the magnesium surface was saturated with CO<sub>2</sub> and the RB flask was also filled with CO<sub>2</sub>, and then DI water was injected into the RB flask quickly in ~20 s while the reaction mixture was stirred using magnetic bid. This allowed all three reaction components (Mg, CO<sub>2</sub> and water) to be in good contact with each other. Note that the reaction was initiated as soon as water was added. The progress of this fast reaction was monitored with a Micro GC connected online to the RB reactor, as shown in ESI-experimental section.†

Methane and hydrogen were quantified using an Agilent Technologies 490 Micro GC with a molecular-sieve column and TCD detector. Liquid products such as methanol and formic acid were identified and quantified by <sup>1</sup>H NMR spectroscopy. The detailed procedure for the detection of the liquid products by <sup>1</sup>H NMR spectroscopy is given in the ESI.†

Instead of pure CO<sub>2</sub>, air was purged through Mg NPs taken in a batch reactor for 4 h with the flow rate of 200 mL min<sup>-1</sup> in order to carry out the reaction using CO<sub>2</sub> present in the air. Isotopically labeled experiments were carried out by using <sup>13</sup>CO<sub>2</sub> and gaseous products were analyzed by using a GC coupled with a TCD, FID and mass spectrometer (Agilent 7890B,

Agilent Technologies). For GC-MS analysis, helium was used as the carrier gas and an Agilent hybrid column CP7430 as the stationary phase.

### *In situ* attenuated total reflection (ATR) infrared spectroscopy

*In situ* ATR-FTIR studies were carried out to examine the mechanistic pathways.<sup>68</sup> Before *in situ* ATR-FTIR studies, the temperature-programmed desorption (TPD) experiment was carried out under a He flow using 20 mg catalysts with a heating rate of 10 °C min<sup>-1</sup> up to 350 °C. Analysis of desorbed species was carried out by using a differentially-pumped quadrupole mass spectrometer (Prisma Plus QMG 220, Pfeiffer Vacuum).

*In situ* ATR-FTIR experiments were performed with a Vertex 70 (Bruker Optics) spectrometer equipped with a liquid-nitrogen-cooled mercury cadmium telluride (MCT) detector and a commercial mirror unit. The ZnSe crystal (52 mm × 20 mm × 2 mm) was coated with a film of the catalyst and was placed into the vertical commercial reactor-cell (Specac). The background was recorded with the catalyst under a He flow at room temperature, but in the absence of the liquid phase. Thereafter, the reactants or He were flown through the system. A series of consecutive (*in situ*) spectra (256–512 scans per spectrum; resolution 4 cm<sup>-1</sup>) were then collected.

### Computational details

All the spin-polarized calculations were performed within the framework of density functional theory (DFT), using the plane-wave technique as implemented in the Vienna *Ab Initio* Simulation Package (VASP).<sup>55</sup> The exchange-correlation energy was accounted within the generalized gradient approximation method (GGA) parameterized by Perdew–Burke–Ernzerhof (PBE).<sup>69</sup> We used the projector augmented wave potential (PAW) to treat the ion–electron interactions. The DFT-D2 empirical correction method proposed by Grimme was applied for describing the effect of van der Waals interactions.<sup>70</sup> In all computations, the kinetic energy cut off is set to be 500 eV in the plane-wave expansion. All the structures were fully relaxed (lattice constant and atomic position) using the conjugated gradient method and the convergence threshold was set to be 10<sup>-4</sup> eV in energy and 0.01 eV Å<sup>-1</sup> in force. For geometry optimization, the Brillouin zone was sampled using a 5 × 5 × 1 Monkhorst–Pack *k*-point mesh. In order to calculate the charge transfer between the surface adsorbed CO<sub>2</sub> and Mg NP surface slab, we chose the Bader charge-population analysis method.<sup>59,60</sup> For structure optimization of the CO<sub>2</sub> molecule in the gas phase, we used the B3LYP/6-31+G(d,p) method as implemented in Gaussian 09.<sup>71</sup> The climbing image nudged elastic band method (CI-NEB) was used to calculate the activation barriers and six intermediate images were considered along the minimum energy path (MEP) to search for transition states for the intermediate states toward CO<sub>2</sub> reduction.<sup>72</sup> For all the pathways, the activation barriers ( $\Delta E^\ddagger$ ) were calculated using the following equations:  $\Delta E^\ddagger = E_{TS} - E_{IS}$  and  $\Delta E = E_{FS} - E_{IS}$ ; where IS, TS and FS correspond to the initial state, transition state and final state, respectively. The adsorption energy ( $E_{ad}$ ) of adsorbates (*i.e.* intermediate molecules and/or atoms on the Mg





surface) was defined as:<sup>57</sup>  $E_{\text{ad}} = E_{\text{A/S}} - E_{\text{A}} - E_{\text{S}}$  where  $E_{\text{A/S}}$ ,  $E_{\text{A}}$  and  $E_{\text{S}}$  represent total energies of the Mg surface slab with adsorbates, only adsorbates and the Mg surface respectively. The reaction energy ( $E_{\text{r}}$ ) was calculated using the following equation<sup>67</sup>  $E_{\text{r}} = E_{\text{FS}} - E_{\text{IS}}$ . The Mg NP surface was modelled considering a four-layer periodic surface slab consisting of a  $3 \times 3$  surface cell ( $9.15 \times 9.15 \text{ \AA}^2$ ) with 36 Mg atoms. To avoid the spurious interactions between the neighboring slabs, a vacuum layer of 20 Å is used in the direction perpendicular to the surface (along the Z-direction) and the nearest distance between the two adsorbed molecules in the adjacent supercell is  $\sim 6 \text{ \AA}$ .

## Author contributions

V. P. proposed the research direction and designed and planned the experiments. V. P., S. R., and R. B. performed various CO<sub>2</sub> conversion experiments and characterization, assisted by A. M. and A. B. NMR and FT-IR studies were performed by S. R. ATR and TPD experiments were conducted by N. Y. and G. R. DFT calculations were carried out by R. J. and A. D. All the data were analyzed by V. P. and S. R. V. P. wrote the manuscript with inputs from S. R., which was commented on by all authors.

## Conflicts of interest

There are no conflicts to declare.

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