


Cite this: *RSC Adv.*, 2020, 10, 19199

# Selective production of bio-based aromatics by aerobic oxidation of native soft wood lignin in tetrabutylammonium hydroxide†

Takashi Hosoya,<sup>a</sup> Kohei Yamamoto,<sup>a</sup> Hisashi Miyafuji<sup>\*a</sup> and Tatsuhiko Yamada<sup>b</sup>

Aerobic oxidation of native soft wood lignin in an aqueous solution of Bu<sub>4</sub>NOH facilitates efficient production of vanillin (4-hydroxy-3-methoxybenzaldehyde), which is one of the platform chemicals in industry. Oxidation of Japanese cedar (*Cryptomeria japonica*) wood flour at 120 °C for 4 h under O<sub>2</sub> in Bu<sub>4</sub>NOH-based aqueous solutions produced vanillin in 23.2 wt% yield based on the Klason lignin content of the starting material. This yield was comparable to that in alkaline nitrobenzene oxidation of the same material (27.2%), which indicated that our aerobic oxidation exploited the full potential of the wood flour for vanillin production. Further mechanical investigation with lignin model compounds suggested that the vanillin formation occurred mainly through following successive reactions: alkaline-catalyzed degradation of β-ether linkages in middle units of lignin polymer to form a glycerol end group, oxidation of the glycerol end group by O<sub>2</sub> to a HC=O moiety, and release of vanillin from the HC=O end. One of the reasons for the high performance of Bu<sub>4</sub>NOH for the vanillin production was explained by the general understanding in organic chemistry that Bu<sub>4</sub>OH is a stronger base than simple alkali, e.g. NaOH. The other more fundamental mechanical aspect was that Bu<sub>4</sub>N<sup>+</sup> suppressed disproportionation of the vanillin precursor (the C<sub>α</sub>HO end group) probably due to strong interaction between the cation and the HC=O end group.

Received 17th April 2020

Accepted 11th May 2020

DOI: 10.1039/d0ra03420g

rsc.li/rsc-advances

## Introduction

Vanillin (3-methoxy-4-hydroxybenzaldehyde) is a major target compound to be produced from soft wood lignin. Quite a few lignin depolymerization methods such as degradation with various oxidants,<sup>1–14</sup> catalytic degradation,<sup>6,12–15</sup> and pyrolytic processes<sup>16</sup> make it clear that vanillin is one of the major minima in the potential energy map in those lignin degradation reactions. Also, vanillin is a platform compound in the chemical industry, and is a source of several medicines, polymer materials, etc.<sup>17,18</sup>

Until the 1990s industrial vanillin production was based mainly on aerobic oxidation of liginosulfonate, a major component of waste water from sulfite pulping.<sup>3,6,19–21</sup> This vanillin production was carried out in alkaline media under compressed air with the yield of vanillin being ~5% based on the original liginosulfonate.<sup>3,6,7</sup> However, management of waste water containing sulfur compounds is a major problem of this

biomass-based vanillin production process. Due to this drawback, recent vanillin production is almost completely substituted with phenol-based ones, where phenol is manufactured from fossil resources. Considering recent environmental requirements, however, the biomass-based vanillin production is worth being re-investigated and re-developed.

Our previous studies have reported that selective vanillin production can be made by aerobic oxidation of several soft wood lignin samples, e.g. soft wood flour, milled wood lignin, and several types of technical lignins including liginosulfonate, at 120 °C in the presence of tetrabutylammonium ion Bu<sub>4</sub>N<sup>+</sup> and OH<sup>–</sup>.<sup>5,8</sup> When Japanese cedar (*Cryptomeria japonica*) wood flour is degraded in 1.25 mol L<sup>–1</sup> Bu<sub>4</sub>NOH aq. at 120 °C under air, vanillin and vanillic acid are produced in 15.4 and 3.9%, respectively, based on the Klason lignin content of the wood.<sup>8</sup> These yields are considerably higher than those obtained in NaOH aq. with the same OH<sup>–</sup> concentration,<sup>5,8</sup> indicating that the Bu<sub>4</sub>NOH solution exhibits much better performance for vanillin production than the corresponding NaOH aq.

The Bu<sub>4</sub>NOH-based oxidation method has several advantages over the process with liginosulfonate: this method employs reaction temperature (120 °C) significantly lower than that of the liginosulfonate process (~170 °C);<sup>3</sup> the process can utilize non-sulfur containing low materials such as wood flour and soda-lignin as well as liginosulfonate. Also, the use of molecular oxygen as an ideal oxidation reagent in this process should be

<sup>a</sup>Graduate School of Life and Environmental Sciences, Kyoto Prefectural University, 1-5 Shimogamo-hangi-cho, Sakyo-ku, Kyoto 606-8522, Japan. E-mail: miyafuji@kpu.ac.jp

<sup>b</sup>Forestry and Forest Products Research Institute, 1 Matsunosato, Tsukuba, Ibaragi 305-8687, Japan

† Electronic supplementary information (ESI) available: Total ion chromatogram in GC/MS analysis of the acetylated reaction mixture obtained after the degradation of LM1. Values in Fig. 1, 3, and 5. See DOI: 10.1039/d0ra03420g



highly emphasized.<sup>4b</sup> On the other hand, there are several issues to be further managed: considerably long reaction times (up to 72 h) and unclear mechanical aspects of the reaction involved in the aerobic oxidation, especially the roles of  $\text{Bu}_4\text{N}^+$  in overall reactions. It is also noted that the highest yield of the target compound obtained with the  $\text{Bu}_4\text{NOH}$ -based method is still lower than those obtained in the alkaline nitrobenzene (AN) oxidation,<sup>8</sup> which is used as a benchmark to evaluate the performance of lignin oxidation processes.

The first half of this article handles the above issues of reaction time and the yields of vanillin and vanillic acid. We will report the reaction time required to reach the maximum vanillin and vanillic acid yields is significantly shortened along with improved yields of the compounds, when the reaction was carried out with the introduction of pure  $\text{O}_2$  to the reaction system. In the second half of this article, we will report results obtained with lignin model compounds (see Scheme 1 for their structures) and discuss the reasons for the high performance of  $\text{Bu}_4\text{NOH}$ , including the roles of  $\text{Bu}_4^+$  in the oxidation process.

## Experimental

### Materials

1.5 mol  $\text{L}^{-1}$   $\text{Bu}_4\text{NOH}$  aq. was purchased from the Sigma-Aldrich Co. The solution was diluted to 1.25 mol  $\text{L}^{-1}$  with distilled water and used as reaction solution. Vanillin, vanillic acid, veratraldehyde, veratric acid, veratryl alcohol, and sodium hydroxide were purchased from FUJIFILM Wako Pure Chemical Co. The particle size of Japanese cedar wood flour was 90–180  $\mu\text{m}$ . Lignin model compounds, veratryl glycerol- $\beta$ -guaiacyl ether (**LM1**) and guaiacyl glycerol- $\beta$ -guaiacyl ether (**LM2**), were purchased from Tokyo-Kasei Co. and used without purification (see Scheme 1 for the structures of **LM1** and **LM2**).

### Degradation of samples and analysis of reaction mixture

Starting material (the wood flour or the lignin model compound, 3.0–20 mg) was placed in a 10 mL glass tube. After adding the reaction solution (1.25 mol  $\text{L}^{-1}$   $\text{Bu}_4\text{NOH}$  aq. or 1.25 mol  $\text{L}^{-1}$   $\text{NaOH}$  aq., 1.0–2.0 mL), the tube was tightly sealed. In several experiments, the concentration of  $\text{OH}^-$  of the  $\text{Bu}_4\text{NOH}$  aq. was increased to 3.75 mol  $\text{L}^{-1}$  by the addition of solid  $\text{NaOH}$  (200 mg in the case of 2.0 mL of the reaction solution). In the experiments that were performed under  $\text{O}_2$  or  $\text{N}_2$ , the tube was flushed

with the corresponding gas and immediately sealed. The tube was then heated at 120  $^\circ\text{C}$  in an oil bath with stirring. At a certain reaction time, the tube was cooled with cold water and then 1,5-dihydroxy-1,2,3,4-tetrahydronaphthalene/ethanol solution (2.0 g  $\text{L}^{-1}$ , 800  $\mu\text{L}$ ) was added as an internal standard. A sample (50  $\mu\text{L}$ ) of the resulting reaction mixture was taken and added to acetonitrile (450  $\mu\text{L}$ ) containing 1.5% acetic acid. The solution was filtered and used directly for high-performance liquid chromatography (HPLC) analysis. The conditions for the HPLC analysis were described in our previous studies.<sup>5,8</sup>

Gas chromatography/mass spectrometric (GC/MS) analysis was also carried out for the reaction mixture. Prior to the GC/MS analysis, the pH of the reaction solution (1.0 mL) after the degradation experiment was adjusted to  $\sim 5$  by the addition of saturated citric acid aq. The solution was then extracted with ethyl acetate (2.0 mL) and the organic layer was dried with anhydrous  $\text{Na}_2\text{SO}_4$  and evaporated under reduced pressure. The residue was acetylated in 1.0 mL of acetic anhydride/pyridine (1/1, v/v) and directly used for the GC/MS analysis. The GC/MS analysis was carried out with Shimadzu GCMS-QP2010 ultra apparatus under the following conditions: column, Agilent J&W DB-5ms; injector temperature, 250  $^\circ\text{C}$ ; profile of column oven temperature, 60  $^\circ\text{C}$  (1 min), 60  $\rightarrow$  300  $^\circ\text{C}$  (1  $\rightarrow$  48 min), 300  $^\circ\text{C}$  (10 min); carrier gas, helium; flow rate, 1.5 mL  $\text{min}^{-1}$ ; emission current, 20  $\mu\text{A}$ ; ionization time, 2.0 ms.

### Identification of enol ethers, 2-methoxy-4-[2-(2-methoxyphenoxy)vinyl]phenol

Model compound **LM2** (20 mg) was degraded in 1.25 mol  $\text{L}^{-1}$   $\text{Bu}_4\text{NOH}$  aq. (2.0 mL) at 120  $^\circ\text{C}$  for 1 h according to similar manner described above. After cooling the tube with cold water, saturated citric acid aq. was added to the reaction solution to adjust the pH to  $\sim 5$ . The reaction mixture was then extracted with ethyl acetate (6 mL) and the organic layer was dried with anhydrous  $\text{Na}_2\text{SO}_4$ . Evaporation of ethyl acetate under reduced pressure gave crude target compounds. The products were purified with silica gel column with the eluent being ethyl acetate/*n*-hexane (1/1, v/v) to obtain *cis/trans*-2-methoxy-4-[2-(2-methoxyphenoxy)vinyl]phenol (**EEs**, 8.0 mg). *trans*-2-Methoxy-4-[2-(2-methoxyphenoxy)vinyl]phenol:  $^1\text{H}$  NMR (400 MHz, 1.25 mol  $\text{L}^{-1}$   $\text{NaOD}/\text{D}_2\text{O}$ ):  $\delta$  (ppm) = 3.50 (s, 3H), 3.62 (s, 3H), 6.00 (d,  $J$  = 11.8 Hz, 1H), 6.33 (d,  $J$  = 9.5 Hz, 1H), 6.54 (dd,  $J_1$  = 8.0 Hz,  $J_2$  = 2.1 Hz, 1H), 6.65 (d,  $J$  = 1.5 Hz, 1H), 6.78 (dt,  $J_1$  = 7.1 Hz,  $J_2$  = 2.1 Hz, 1H), 6.83 (d,  $J$  = 12.0, 1H), 6.90 (m, 3H). *cis*-2-Methoxy-4-[2-(2-methoxyphenoxy)vinyl]phenol:  $^1\text{H}$  NMR (400 MHz, 1.25 mol  $\text{L}^{-1}$   $\text{NaOD}/\text{D}_2\text{O}$ ):  $\delta$  (ppm) = 3.48 (s, 3H), 3.64 (s, 3H), 5.47 (d,  $J$  = 6.8 Hz, 1H), 6.22 (d,  $J$  = 6.8 Hz, 1H), 6.34 (d,  $J$  = 8.3 Hz, 1H), 7.16 (d,  $J$  = 1.5 Hz, 1H), the other protons were not discernable due to their overlapping with the signals from the *trans*-isomer.

The HPLC analysis was performed for isolated **EEs** under the analytical conditions identical to those presented above to the same internal standard being employed. The obtained calibration curves were used for quantification of **EEs** formed by the degradation of **LM2**.



Scheme 1  $\beta$ -O-4 type dimeric lignin model compounds employed in this study.



## Results and discussion

### Vanillin production from wood flour with introduction of O<sub>2</sub>

Our previous study reported that aerobic oxidation of the wood flour (14 mg) in 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH aq. (2.0 mL) under air for 43 h produced vanillin and vanillic acid in 15.4 and 3.9 wt% yields, respectively, based on the Klason lignin amount of the wood flour.<sup>8</sup> The 1.25 mol L<sup>-1</sup> aqueous solution of Bu<sub>4</sub>NOH is the molten form of the Bu<sub>4</sub>NOH·30H<sub>2</sub>O crystal. To further enhance the degradation, we carried out similar degradation experiments after flushing the reaction system (sealed 10 mL test tube) with pure O<sub>2</sub>. We will hereafter call this “degradation under O<sub>2</sub>” for convenience, although the atmosphere of the reaction system is not fully substituted with O<sub>2</sub>. Note that 1.25 mol L<sup>-1</sup> is the best concentration of Bu<sub>4</sub>N<sup>+</sup> in terms of vanillin production according to our previous study:<sup>5</sup> increase in [Bu<sub>4</sub>N<sup>+</sup>] to more than 1.25 mol L<sup>-1</sup> scarcely boosts the vanillin yield and also results in degradation of Bu<sub>4</sub>N<sup>+</sup> probably into BuOH and Bu<sub>3</sub>N.

Fig. 1A shows changes in the yield of vanillin during the degradation in the Bu<sub>4</sub>NOH aq. under O<sub>2</sub> along with our previous results obtained under air in the same reaction medium (Fig. 1C). It becomes clear that the vanillin formation is significantly faster under O<sub>2</sub>: the time required for reaching the maximum vanillin yield was 8 h under O<sub>2</sub> whereas the reaction under air needed 43 h. The maximum yield of vanillin was also increased to 19.8 wt% (8 h) from 15.4 wt% (43 h) by the O<sub>2</sub> substitution. After reaching the maximum yield in 8 h, the yield of vanillin was decreased to 17.0 wt% at 20 h and this degradation of vanillin was more significant under O<sub>2</sub> than under air. This indicates that vanillin is somewhat reactive toward O<sub>2</sub> and reaction time should be carefully controlled when the vanillin production is carried out under O<sub>2</sub> instead of air.

Fig. 1 also shows the yield of vanillic acid (3-methoxy-4-hydroxybenzoic acid) along with that of vanillin, as vanillic acid is the second major product, as reported previously.<sup>5,8</sup> The reaction under O<sub>2</sub> tends to form more vanillin than vanillic acid, when it is compared to the one under air (Fig. 1A and C). It is

thus stated that O<sub>2</sub> introduction made the reaction more vanillin selective. One of the possible reasons for this selectivity change is that vanillic acid is more reactive toward O<sub>2</sub> than vanillin and readily release CO<sub>2</sub>. As shown in Fig. 1A, the maximum yield of vanillic acid was achieved at 4 h in the Bu<sub>4</sub>NOH aq. under O<sub>2</sub> and then the yield gradually decreased. Note that increase in the yield of vanillic acid was not observed during the degradation of vanillin from 8 to 20 h, which suggested oxidation of vanillin to vanillic acid was not important under the employed conditions.

We then carried out the degradation of the wood flour (14.0 mg) in 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH aq. (2.0 mL) under O<sub>2</sub> with the addition of NaOH(s) (200 mg) to increase the OH<sup>-</sup> concentration of the reaction solution to 3.75 mol L<sup>-1</sup>, as vanillin formation is significantly enhanced in stronger alkaline media.<sup>5</sup> In this alkaline-enhanced solution, as shown in Fig. 1B, the reaction time required for the maximum yield of vanillin was further shortened to 4 h. The yield of vanillin was also improved to 23.2 wt% by the addition of NaOH. We thus tried further addition of NaOH to the solution, but when the concentration of OH<sup>-</sup> was set at 5.0 mol L<sup>-1</sup> by the addition of 300 mg of NaOH, significant decrease in the vanillin yield was observed.

Table 1 summarizes the maximum yield of vanillin obtained from the wood flour in the above Bu<sub>4</sub>NOH-based reaction solutions along with that obtained in alkaline nitrobenzene (AN) oxidation of the same wood flour. AN oxidation is one of the most selective methods to convert various lignin samples to the corresponding monomeric benzaldehydes (vanillin in the case of soft wood lignins) and used as a benchmark to measure the performance of lignin conversion methods. The maximum vanillin yield (23.0 wt%) and the shortest reaction time (4 h) were both achieved when the reaction was carried out under O<sub>2</sub> in the Bu<sub>4</sub>NOH aq. with the addition of NaOH. Considering that our previous study about the reaction under air required 43 h reaction time to achieve much lower maximum vanillin yield (15.4 wt%), the O<sub>2</sub> introduction investigated in this study had drastic effects for improving the performance of our vanillin production method. Also, the 23.0 wt% vanillin yield obtained



Fig. 1 Changes with time in yields of vanillin (●), vanillic acid (■), and their total yields (△) during degradation of Japanese cedar wood flour (14 mg) in 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH aq. (2.0 mL) under O<sub>2</sub> (A), under O<sub>2</sub> with the addition of NaOH(s) (200 mg) (B), and under air<sup>8</sup> (C) at 120 °C. The total amount of Klason lignin and acid-soluble lignin of the wood flour was 34.3 wt%.

**Table 1** Yields (wt%, based on the Klason lignin amount) of vanillin and vanillic acid from the Japanese cedar wood flour (14.0 mg) degraded in the Bu<sub>4</sub>NOH aq.-based reaction media (2.0 mL) at 120 °C and their yields from alkaline nitrobenzene (AN) oxidation

Medium	Atmosphere	Reaction time <sup>a</sup> (h)	Yield (wt%)		
			Vanillin	Vanillic acid	Total
Bu <sub>4</sub> NOH aq. + NaOH(s) <sup>b</sup>	O <sub>2</sub>	4.0	23.2	1.2	24.4
Bu <sub>4</sub> NOH aq. <sup>8c</sup>	Air	43	15.4	3.9	19.3
AN oxidation <sup>8</sup>	Air	2.5	27.2	1.2	28.4

<sup>a</sup> The reaction times that result in the maximum vanillin yield are selected for each column. For AN oxidation, the reaction time was 2.5 h according to the standard procedure. <sup>b</sup> Reaction solution was prepared by the addition of NaOH(s) (200 mg) to 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH aq. (2.0 mL). <sup>c</sup> These are the results presented in our previous study,<sup>8</sup> where 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH aq. (2.0 mL) was used without the NaOH addition.

in the NaOH-added Bu<sub>4</sub>NOH aq. under O<sub>2</sub> was comparable to those in AN oxidation (Table 1). This also indicates that our Bu<sub>4</sub>NOH-based reaction system well exploits vanillin forming potential of the wood flour.

### Mechanical investigation with lignin model compounds

We have so far shown that vanillin is effectively produced by aerobic oxidation of the wood flour in the Bu<sub>4</sub>NOH-based solutions. Since such effective vanillin production cannot be achieved in a simple alkali solution (*e.g.* NaOH aq.) with the same OH<sup>-</sup> concentration as that of the Bu<sub>4</sub>N<sup>+</sup>-based one,<sup>5,8</sup> it is clear that chemical nature specific for Bu<sub>4</sub>NOH plays pivotal roles in the vanillin formation. To investigate the mechanisms underlying the vanillin production in the Bu<sub>4</sub>NOH solution, degradation of several types of lignin model compounds (mainly **LM1** and **LM2**, see Scheme 1) was carried out in 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH and NaOH solutions and the reaction behaviors were carefully compared. In these model experiments, we carried out the degradation under air (not under O<sub>2</sub>) to minimize degradation of the products.

Fig. 2 presents a HPLC chromatogram of the reaction mixture obtained from the degradation of **LM1** (20 mg) in the Bu<sub>4</sub>NOH aq. (2.0 mL) under air, where β-O-4 is the most abundant linkage type in native lignin. **LM1** formed vanillin along with veratraldehyde (3,4-dimethoxybenzaldehyde), veratryl alcohol (3,4-dimethoxybenzyl alcohol), veratric acid (3,4-dimethoxybenzoic acid), and guaiacol. The compounds with the veratryl moiety and vanillin are most likely to be formed from the A ring of **LM1** and guaiacol is derived from the B ring (see Scheme 1 for the definition of the A- and B-rings).

As shown in Fig. 3A, degradation of **LM1** for short reaction times gave guaiacol and small amount of the A-ring-derived compounds. At the 1 h reaction time (the second plot from the left), for instance, guaiacol was formed in 12.3 mol% yield and the A-ring-derived compounds, mainly veratraldehyde, were produced in 7.2 mol% yield, with 86.4% of **LM2** remaining intact. This suggests that the initial step of the degradation is alkaline-catalyzed β-ether cleavage shown as pathway A in Scheme 2, as reported in many studies.<sup>22–25</sup> This β-ether cleavage results in the formation of veratryl glycerol from the A-ring along with the releasement of guaiacol from the B-ring. Veratryl glycerol was not detected in the HPLC analysis

probably due to its very high polarity, but the presence of significant amount of the compound in the reaction mixture was strongly suggested from the GC/MS analysis of the acetylated reaction mixture (see Fig. S1 in ESI†). The yields of the A-ring-derived compounds were gradually increased at prolonged reaction times (Fig. 3A). Veratraldehyde was predominant in the A-ring derived products until 6 h and vanillin then became the major product with almost full consumption of **LM1**. At 43 h vanillin and veratraldehyde were finally formed in 15.7 mol% and 2.2 mol% yields, respectively, with the **LM1** recovery being 3.7%. Note that the required 43 h reaction time is in good agreement with the experimental fact that vanillin yield became almost constant after 43 h in the degradation of the wood flour in the Bu<sub>4</sub>NOH aq. under air (see Fig. 1C).<sup>8</sup>

The above results suggest that, as presented in Scheme 2, veratryl glycerol formed by the β-ether cleavage is gradually oxidized into veratraldehyde by O<sub>2</sub> *via* pathway B. However, our attempts to detect any intermediates in this aerobic oxidation step were not successful. Veratraldehyde then undergoes a demethylation reaction on the 4-OMe group to finally form vanillin *via* pathway C. The detailed mechanism of this demethylation is not clear at the moment. One of the possibilities is a simple S<sub>N</sub>2 reaction on the methyl group by OH<sup>-</sup>, but a mechanism involving a nucleophilic addition of OH<sup>-</sup> on the 4-position of the benzene ring followed by the elimination of MeO<sup>-</sup> cannot be ruled out due to the presence of a strong electron-withdrawing CHO group at the 1-position. It is also noted that the demethylation of the 3-OMe group is disfavored because of the lack of the influence of the CHO group at the 3-position.

Fig. 2 and 3 indicate the reaction mixture also contains considerable amount of veratric acid and veratryl alcohol. It is likely that these two compounds are produced through disproportionation of veratraldehyde *via* Cannizzaro reaction shown in pathway D in Scheme 2. This consideration is supported by the fact that the amount of these three compounds increased with the gradual decrease in the amount of veratraldehyde (Fig. 3A). There also might be another pathway where **LM1** directly gave veratraldehyde, pathway E in Scheme 2, as suggested from the result that the sum of the guaiacol yield and the **LM1** recovery was less than 100% at 43 h reaction time. However, this pathway must be minor compared to the





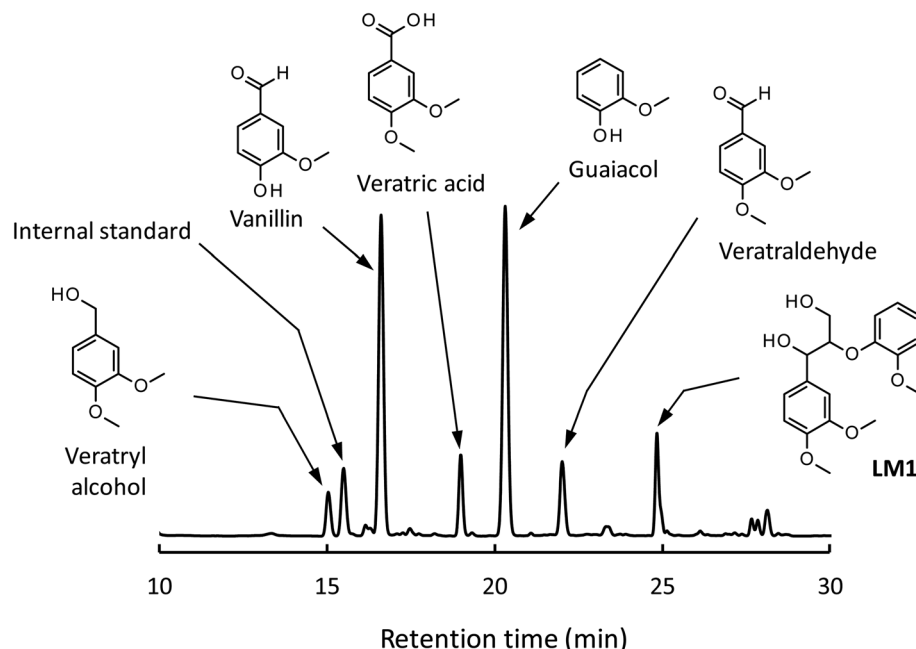


Fig. 2 HPLC chromatogram of the reaction mixture obtained after the degradation of LM1 (20 mg) in 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH aq. (2.0 mL) under air for 4 h.

veratraldehyde formation *via* the pathways A and B, since the guaiacol yield is quantitative at least at the initial stage of the reaction, as discussed above. It is also noted that guaiacyl moieties including guaiacol degrade in the presence of O<sub>2</sub> (ref. 26–30) and this is probably one of the reasons for the small yield of the compound at the prolonged reaction times.

We then performed the degradation of LM1 in 1.25 mol L<sup>-1</sup> NaOH aq., a simple alkaline solution with the same OH<sup>-</sup> concentration as that of the Bu<sub>4</sub>NOH aq. As shown in Fig. 3B, the degradation velocity of LM1 was lower in the NaOH aq. than in the Bu<sub>4</sub>NOH aq. The maximum yield of vanillin in the NaOH aq. (0.8 mol%, 6 h) was also much lower in the NaOH solution. One of the plausible reasons for this is that the activity of OH<sup>-</sup> is greater in the Bu<sub>4</sub>NOH aq. than in the NaOH aq. even when their OH<sup>-</sup> concentrations are the same. In other words, OH<sup>-</sup> in the Bu<sub>4</sub>NOH aq. is less influenced by the counter cation Bu<sub>4</sub>N<sup>+</sup>, which renders the Bu<sub>4</sub>NOH solution more basic over the NaOH aq. The fast degradation of LM1 will result in smooth formation of the veratryl glycerol, which is the major origin of vanillin (Scheme 2).

There is another mechanical aspect that accounts for the better performance of Bu<sub>4</sub>NOH for vanillin production. Table 2 summarizes the yields of the major products quantified after the degradation of LM1 for 43 h. In the Bu<sub>4</sub>NOH aq. LM1 formed the aldehyde products (veratraldehyde and vanillin) in 17.9 mol% (18.6 mol%) yield, where the yield in the parenthesis is the one based on degraded LM1. The other non-aldehyde A-ring derived products (veratric acid and veratryl alcohol) were formed in 15.8 mol% yield (16.5 mol%) in total, which was similar to that of the aldehyde products. These results suggest that the reactions *via* the pathways C and D almost evenly occur in the Bu<sub>4</sub>NOH aq. It is also noted that total yield of the four

compounds was 33.7 mol% (35.1 mol% based on degraded LM1) and the rest (64.9 mol%) undetected products probably involve considerable amount of veratryl glycerol (see above discussion and Fig. S1 in ESI†).

The degradation of LM1 in the NaOH aq., on the other hand, formed relatively small amounts of the four A-ring-derived products (the total yield: 14.9 mol% after 43 h degradation), as summarized in Table 2. This is because complete degradation of LM1 was not achieved in the NaOH aq. even after 43 h degradation (see Fig. 3B). The total yield in the NaOH aq. eventually became comparable to that in Bu<sub>4</sub>NOH when it was calculated based on the degraded LM1: 35.1 mol% in the Bu<sub>4</sub>NOH aq. and 34.7 mol% in the NaOH aq. It is therefore likely that reactivity of veratryl glycerol toward O<sub>2</sub> to form veratraldehyde – in other words the velocity of the reactions involved in the pathway B – is almost constant no matter whether the reaction was carried out in the Bu<sub>4</sub>NOH aq. or the NaOH aq. However, as shown in Table 2, the total yield of the aldehyde products in NaOH aq. based on degraded LM1 (13.0 mol%) was smaller than that in Bu<sub>4</sub>NOH (18.6 mol%) with the total yields of the non-aldehyde products in NaOH aq. (21.7 mol%) being greater than that in Bu<sub>4</sub>NOH (16.5 mol%). These different yields of the aldehyde and the non-aldehyde products suggest that the pathway C is more favored over the pathway D in the Bu<sub>4</sub>NOH aq., which results in the increased yield of vanillin.

To check this idea, we degraded veratraldehyde (5.0 mg) at 120 °C for 4 h under N<sub>2</sub> either in the Bu<sub>4</sub>NOH aq. or the NaOH aq. (1.0 mL) and compared the product distribution between the degradations in the two reaction media. As summarized in Table 3, the degradation of veratraldehyde in Bu<sub>4</sub>NOH resulted in the formation of vanillin, veratryl alcohol, and veratric acid in

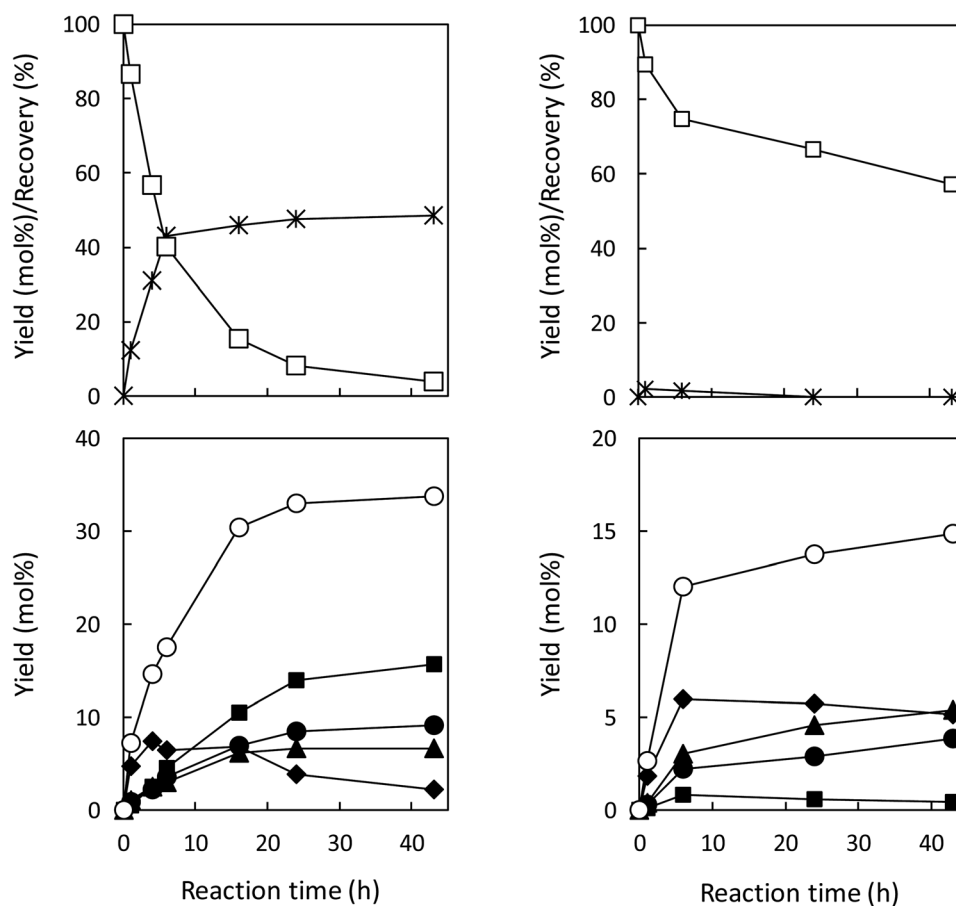
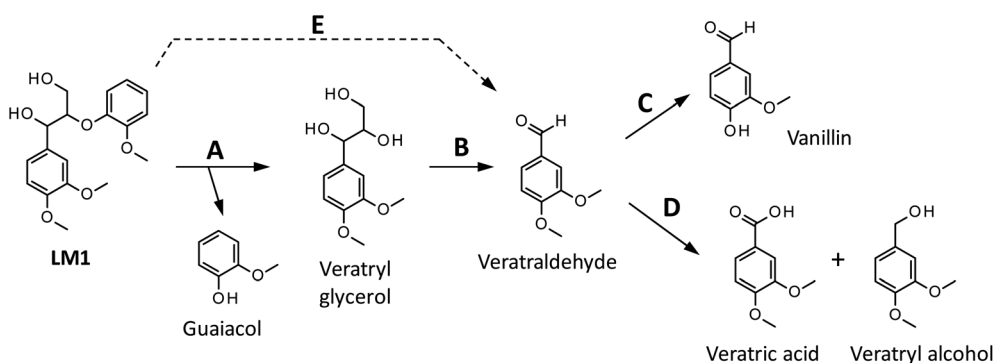
(A)  $\text{Bu}_4\text{NOH}$  aq.(B)  $\text{NaOH}$  aq.

Fig. 3 Changes with time in recovery of LM1 ( $\square$ ), yields of guaiacol ( $\times$ ), veratraldehyde ( $\blacklozenge$ ), vanillin ( $\blacksquare$ ), veratric acid ( $\blacktriangle$ ), veratryl alcohol ( $\bullet$ ), and the total yield of the A-ring-derived products ( $\circ$ ) during degradation of LM1 (20 mg) at  $120^\circ\text{C}$  under air in  $1.25\text{ mol L}^{-1}$   $\text{Bu}_4\text{NOH}$  aq. (2.0 mL) (A) and in  $1.25\text{ mol L}^{-1}$   $\text{NaOH}$  aq. (2.0 mL) (B).



Scheme 2 Reaction pathways from LM1 to major products detected in this study.

very similar yields. On the other hand, the degradation in  $\text{NaOH}$  aq. gave much smaller amount of vanillin and more amount of veratryl alcohol and veratric acid. This is in complete agreement with the above consideration that the demethylation pathway C (Scheme 2) is more favored over the disproportionation pathway D in the  $\text{Bu}_4\text{NOH}$  aq. We also carried out similar degradation in

$\text{Bu}_4\text{NCl}$ -added  $\text{NaOH}$  aq., where the  $1.25\text{ mol L}^{-1}$   $\text{Bu}_4\text{NOH}$  aq. was mimicked by the addition of the corresponding amount of  $\text{Bu}_4\text{NCl}$  to  $1.25\text{ mol L}^{-1}$   $\text{NaOH}$  aq. The addition of  $\text{Bu}_4\text{NCl}$  also increased the selectivity toward vanillin as indicated from the higher vanillin yield (20.2 mol%) based on the degraded veratraldehyde and the lower yield of veratryl alcohol and veratric



**Table 2** Yields (mol%) of major A-ring-derived products after the degradation of **LM1** (20 mg) at 120 °C for 43 h under air in 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH aq. and 1.25 mol L<sup>-1</sup> NaOH aq. (2.0 mL)

	Aldehydes			Non-aldehydes			
	Vanillin	Veratraldehyde	Total	Veratryl alcohol	Veratric acid	Total	Total
Bu <sub>4</sub> NOH aq.	15.7 (16.3) <sup>a</sup>	2.2 (2.3)	17.9 (18.6)	9.1 (9.5)	6.7 (7.0)	15.8 (16.5)	33.7 (35.1)
NaOH aq.	0.4 (0.9)	5.2 (12.1)	5.6 (13.0)	3.9 (9.1)	5.4 (12.6)	9.3 (21.7)	14.9 (34.7)

<sup>a</sup> The value in the parenthesis shows the yield based on the amount of degraded **LM1**: 96.3% and 42.9% in the Bu<sub>4</sub>NOH aq. and the NaOH aq. based on the initial amount of **LM1**, respectively.

**Table 3** Yields (mol%) of vanillin, veratryl alcohol, and veratric acid along with recovery (%) of veratraldehyde after degradation of veratraldehyde (5.0 mg) at 120 °C for 4 h under N<sub>2</sub> in 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH aq. and NaOH aq. (1.0 mL)

	Yield			Recovery
	Vanillin	Veratryl alcohol	Veratric acid	
Bu <sub>4</sub> NOH aq.	30.6 (33.5) <sup>a</sup>	28.1 (30.7)	31.2 (34.1)	8.6
NaOH aq.	5.9 (6.7)	38.3 (43.3)	41.6 (47.0)	11.5
NaOH aq. + Bu <sub>4</sub> NCl(s) <sup>b</sup>	8.7 (20.2)	12.7 (29.5)	13.9 (32.3)	57.0

<sup>a</sup> The value in the parenthesis shows the yield based on the amount of degraded veratraldehyde. <sup>b</sup> Solid Bu<sub>4</sub>NCl was added to the NaOH solution so that the concentration of Bu<sub>4</sub>N<sup>+</sup> in the reaction solution became 1.25 mol L<sup>-1</sup>.

acid (29.5 and 32.3 mol%, respectively) than those obtained in the simple NaOH aq. Interestingly, in this Bu<sub>4</sub>NCl-added system, the degradation of veratraldehyde was considerably suppressed: much more starting material (57.0%) was recovered in the Bu<sub>4</sub>NCl-added NaOH aq. These results suggest that Bu<sub>4</sub>N<sup>+</sup> slows down both pathways C and D, and along with that, makes the degradation more vanillin-oriented. Similar recoveries of the starting material obtained between the Bu<sub>4</sub>NOH and the NaOH aq. – they are 11.5 and 8.6%, respectively – would be explained by the idea that the slowing-down effect by Bu<sub>4</sub>N<sup>+</sup> was compensated by the strong basicity of Bu<sub>4</sub>NOH (see above).

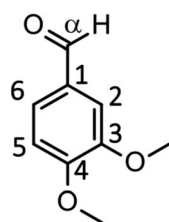
To obtain deeper insights into the effect of Bu<sub>4</sub>N<sup>+</sup>, we carried out <sup>1</sup>H NMR analyses of veratraldehyde in 1.25 mol L<sup>-1</sup> NaOD/

D<sub>2</sub>O-based solutions. As summarized in Table 4, the signal of all protons of veratraldehyde considerably shifted to lower magnetic fields by 20 to 112 Hz, when Bu<sub>4</sub>NCl was added to the NaOD/D<sub>2</sub>O. This shift scarcely occurred when the same molar amount of NaCl was added to the solution, which strongly suggested that the shift was caused by Bu<sub>4</sub>N<sup>+</sup> and not by Cl<sup>-</sup>. It is therefore likely that veratraldehyde is in a close contact with Bu<sub>4</sub>N<sup>+</sup> in the solutions containing Bu<sub>4</sub>N<sup>+</sup>. The largest shift observed for the aldehyde proton (112 Hz) suggests strong interaction between Bu<sub>4</sub>N<sup>+</sup> and the aldehyde group. The disproportionation reaction is eventually suppressed when both reactants are in the “cage” of Bu<sub>4</sub>N<sup>+</sup>. On the other hand, in the case of the demethylation (pathway C in Scheme 2), one of the

**Table 4** Chemical shifts (ppm) in <sup>1</sup>H NMR analyses of veratraldehyde (0.5 mg) in 1.25 mol L<sup>-1</sup> NaOD/D<sub>2</sub>O solution (0.75 mL) and those with the additions<sup>a</sup> of Bu<sub>4</sub>NCl and NaCl

	C <sub>2</sub> -H (d)	C <sub>5</sub> -H (d)	C <sub>6</sub> -H (dd)	C <sub>α</sub> -H (s)	C <sub>3</sub> -OCH <sub>3</sub> (s)	C <sub>4</sub> -OCH <sub>3</sub> (s)
1.25 mol L <sup>-1</sup> NaOD/D <sub>2</sub> O	7.16	6.89	7.32	9.33	3.64	3.69
1.25 mol L <sup>-1</sup> NaOD/D <sub>2</sub> O + Bu <sub>4</sub> NCl	7.29 (+52) <sup>b</sup>	7.09 (+80)	7.50 (+72)	9.61 (+112)	3.69 (+20)	3.75 (+24)
1.25 mol L <sup>-1</sup> NaOD/D <sub>2</sub> O + NaCl	7.18 (+8)	6.93 (+40)	7.36 (+16)	9.38 (+20)	3.67 (+12)	3.73 (+16)

<sup>a</sup> Bu<sub>4</sub>NCl and NaCl were added to the NaOD solution with the concentration of the additives being set at 1.25 mol L<sup>-1</sup>. <sup>b</sup> Changes in the chemical shift (Hz) caused by the additive were shown in the parenthesis.



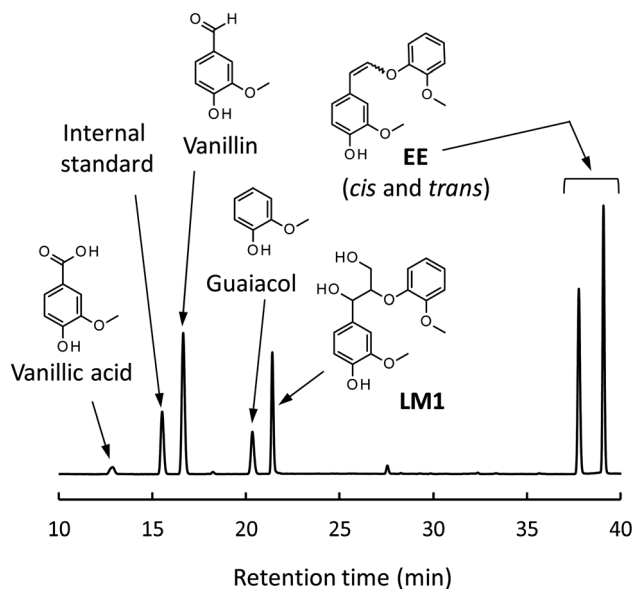


Fig. 4 HPLC chromatogram of the reaction mixture obtained after the degradation of **LM2** (5 mg) in  $1.25 \text{ mol L}^{-1}$   $\text{Bu}_4\text{NOH}$  aq. (1.0 mL) under air for 1 h.

reactants is  $\text{OH}^-$ , which is a small molecule and hence can more easily squeeze itself into the “cage”. Although further investigation is necessary to elucidate more detailed mechanism, this idea can reasonably explain the above experimental facts. According to these mechanisms, it can be stated that  $\text{Bu}_4\text{N}^+$  does not have a specific catalytic site, but the interaction between the aldehyde group and  $\text{Bu}_4\text{N}^+$  is a major origin of the good performance of  $\text{Bu}_4\text{NOH}$  for the vanillin production. Also, as shown in Fig. 3, the yield of guaiacol in the degradation in the  $\text{Bu}_4\text{NOH}$  aq. is extremely higher than that in the  $\text{NaOH}$  aq. and this result may be also explained with the idea that guaiacol was protected from the  $\text{O}_2$  attack by the cage effect caused by the presence of  $\text{Bu}_4\text{N}^+$ .

Fig. 4 shows a typical HPLC chromatogram of the reaction mixture obtained after the degradation of the phenolic lignin model **LM2** (5.0 mg) in  $1.25 \text{ mol L}^{-1}$   $\text{Bu}_4\text{NOH}$  aq. (1.0 mL) at  $120^\circ\text{C}$  under air. In the case of **LM2**, vanillin and vanillic acid were detected as major A-ring-derived products along with guaiacol as B-ring-derived one. We also found two large peaks at 37.6 and 39.0 min, which were assigned as *cis*- and *trans*-isomers of the enol ether **EE** with  $^1\text{H}$  NMR analysis after their isolation from the reaction mixture with column chromatography (see experimental section for details). The formation of the *trans*-isomer was favored in the degradation. Note that **EE** are reported as major products in degradation of phenolic lignin models under alkaline conditions in many previous studies.<sup>22,31–33</sup>

In the degradation of **LM2**, as shown in Fig. 5A, vanillin, guaiacol, and **EEs** were produced from the initial stage of the degradation in the  $\text{Bu}_4\text{NOH}$  aq. After 2 h reaction time, the yield of **EEs** started to decrease with increase in the yield of vanillin and guaiacol. At 4 h reaction time, vanillin and guaiacol were produced in 59.5 and 61.9 mol% yields,

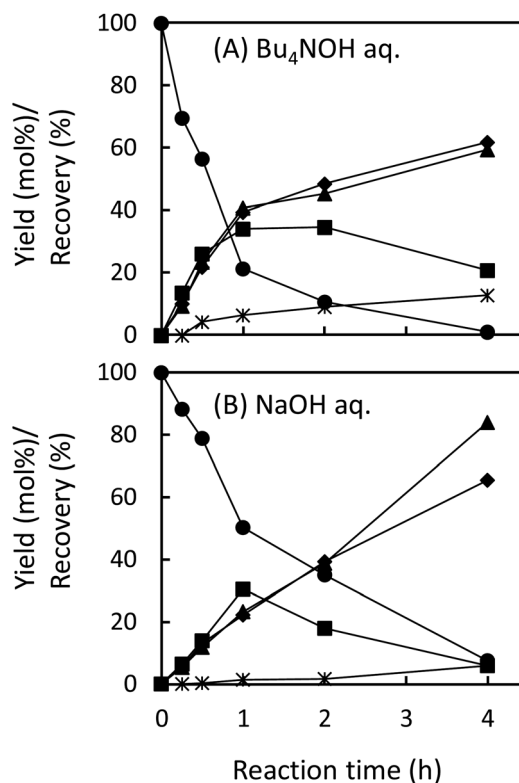


Fig. 5 Changes with time in recovery of **LM2** (●), yields of guaiacol (◆), vanillin (▲), vanillic acid (\*), and enol ethers **EEs**<sup>a</sup> (■) during degradation of **LM2** (5.0 mg) at  $120^\circ\text{C}$  under air in  $1.25 \text{ mol L}^{-1}$   $\text{Bu}_4\text{NOH}$  aq. (1.0 mL) (A) and in  $1.25 \text{ mol L}^{-1}$   $\text{NaOH}$  aq. (1.0 mL) (B).  
<sup>a</sup> The yields of **EEs** are shown as the sum of the *cis*- and *trans*-isomers.

respectively (see also Table 5). Vanillic acid started to form after 15 min and the yield reached 12.7 mol% at 4 h, although the compound was not detected in the reaction mixture before 15 min. These results suggest that **LM2** is first degraded to **EE** as presented in pathway F in Scheme 3 and **EE** is then degraded into vanillin and vanillic acid along with the release of guaiacol (pathway G). The pathway F is a simple alkaline degradation process *via* quinone methide formation followed by succeeding elimination of  $\text{C}_\gamma$  as formaldehyde, as extensively investigated previously.<sup>22,31–33</sup> The pathway G requires  $\text{O}_2$  according to the previous studies reporting that **EE** is substantially stable under  $\text{N}_2$  even at elevated temperatures ( $\sim 170^\circ\text{C}$ ) but readily to be oxidized into vanillin and guaiacol in the presence of  $\text{O}_2$ .<sup>26,28</sup> Note that, according to comparison between the results in Fig. 3 and 5, the degradation of **LM2** was much faster than that of **LM1** and this will be discussed in the next section.

We also carried out degradation of *cis/trans* mixture of isolated **EE** (3.0 mg) in the  $\text{Bu}_4\text{NOH}$  aq. (1.0 mL) under air. As summarized in Table 5, the degradation for 4 h resulted in the formation of 43.6, 22.2, and 41.4 mol% of vanillin, vanillic acid, and guaiacol, respectively. Thus, the yields of vanillin and guaiacol from **EE** are moderately smaller than those from **LM2** obtained under the same reaction conditions (vanillin: 59.5 mol% and guaiacol: 61.9 mol%, see Fig. 5 and Table 5).





**Table 5** Yields (mol%) of vanillin, vanillic acid, and guaiacol and the recovery (%) of the starting material after the degradation of *cis/trans* mixture of **EE** (3.0 mg) at 120 °C for 4 h under air in 1.25 mol L<sup>-1</sup> Bu<sub>4</sub>NOH aq. and 1.25 mol L<sup>-1</sup> NaOH aq. (2.0 mL)

Starting material	Reaction medium	Yield (mol%)				Recovery (%)
		Vanillin	Vanillic acid	Guaiacol	<b>EE</b>	
<b>LM2</b>	Bu <sub>4</sub> NOH aq.	59.5	12.7	61.9	7.0	1.0
<b>LM2</b>	NaOH aq.	83.8	5.9	65.5	6.0	7.4
<b>EE</b>	Bu <sub>4</sub> NOH aq.	43.6	22.2	41.4	—	29.2
<b>EE</b>	NaOH aq.	51.8	6.5	49.7	—	17.7



**Scheme 3** Reaction pathways from **LM2** to the products detected in this study. The formation of vanillic acid *via* pathway H is less significant than that *via* pathway G.

These results mildly suggest that there is a reaction pathway forming vanillin and guaiacol directly from **LM2** (pathway H in Scheme 3). For vanillic acid, on the other hand, the yield from **EE** (22.2 mol%, Table 5) was greater than that from **LM2** (12.7 mol%, Fig. 5 and Table 5), which suggests that vanillic acid is formed mostly *via* **EE** in the degradation of **LM2**.

The degradation of **LM2** in the NaOH aq. was then carried out under the same reaction conditions. As shown in Fig. 5B, we observed reaction behaviors qualitatively the same as those observed in the case of the Bu<sub>4</sub>NOH aq. This indicates that the degradation follows the pathways in Scheme 3 both in the Bu<sub>4</sub>NOH and the NaOH aq. Through quantitative comparison of the reaction behaviors between the Bu<sub>4</sub>NOH and the NaOH aq. (Fig. 5), the degradation in the NaOH aq. exhibited (1) slower degradation of **LM2**, (2) lower yields and faster degradation of **EE**, (3) larger yields of vanillin and guaiacol, and (4) lower yields of vanillic acid. We will discuss these four differences below.

The relatively slow degradation of the starting material in the NaOH aq., the first difference mentioned above, can be explained again with the stronger basicity of Bu<sub>4</sub>OH over NaOH. The reactions in the pathway G (Scheme 3) requires the deprotonation of the phenolic OH of **LM2** and C<sub>7</sub>-OH of the intermediate quinone methide. These deprotonation steps are considered to be less feasible in the NaOH aq., ending up the slow degradation of **LM2**.

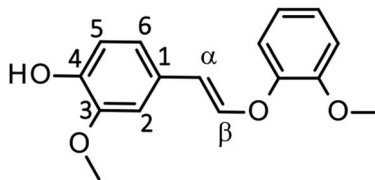
The second and third differences are closely linked together, as the faster degradation of **EE** is the greater the yields of the products (vanillin and guaiacol) should become. It is possible that, as an analogy to the stabilization of veratraldehyde by Bu<sub>4</sub>N<sup>+</sup> (see previous section), **EE** is stabilized by the presence of Bu<sub>4</sub>N<sup>+</sup>. The larger recovery of **EE** (29.2%) after the degradation for 4 h in the Bu<sub>4</sub>NOH aq. than that in the NaOH aq. (17.7%, Table 5) also supports this idea. As summarized in Table 6, <sup>1</sup>H

NMR analyses of *trans*-**EE** in the 1.25 mol L<sup>-1</sup> NaOD/D<sub>2</sub>O with and without the addition of Bu<sub>4</sub>NCl indicated that C<sub>2</sub>-H and C<sub>6</sub>-H on the benzene ring and the protons on the C<sub>α</sub>=C<sub>β</sub> group significantly shifted to upper magnetic fields when Bu<sub>4</sub>NCl was added to the NaOD/D<sub>2</sub>O solution, whereas the shift observed for C<sub>5</sub>-H was relatively small. The addition of the same molar amount of NaCl again did not cause those shifts. These results suggest that Bu<sub>4</sub>N<sup>+</sup> is located mainly around the C<sub>α</sub>=C<sub>β</sub> bond of **EE**. It has been reported that the initial step of the aerobic oxidation of **EE** to vanillin is addition of O<sub>2</sub> to the C<sub>α</sub>=C<sub>β</sub> group.<sup>26,28</sup> Binding of the C<sub>α</sub>=C<sub>β</sub> group to Bu<sub>4</sub>N<sup>+</sup> will render the O<sub>2</sub> addition more demanding, by which the degradation of **EE** to vanillin is inhibited. Note that the changes in the chemical shifts of **EE** by the addition of Bu<sub>4</sub>N<sup>+</sup> (Table 6) were opposite from those observed for the veratraldehyde–NaOD/D<sub>2</sub>O system (Table 4), that is, upper-magnetic field shift and downer one were observed in the **EE** and in the veratraldehyde solutions, respectively. However, the reasons for this difference are not clear at the moment.

The reasons for the low yield of vanillic acid in the NaOH aq. (the fourth difference between the Bu<sub>4</sub>NOH aq. and the NaOH aq. mentioned above) are not clear at the moment. As presented in Table 5, this vanillic acid-oriented degradation behavior was re-produced also in the degradation of **EE** in the Bu<sub>4</sub>NOH aq.: **EE** formed vanillic acid in 22.2 mol% on the basis of degraded starting material in the Bu<sub>4</sub>NOH aq., whereas the yield of the compound was much smaller in the NaOH aq. (6.5 mol%). This suggests that the degradation of **EE** (pathway G in Scheme 3) is modified by the presence of Bu<sub>4</sub>N<sup>+</sup> to be more vanillic acid-selective. The interaction between **EE** and Bu<sub>4</sub>N<sup>+</sup> discussed above would play some roles in this selectivity change, but more systematic investigation is necessary to elucidate the underlying mechanism.



**Table 6** Chemical shifts (ppm) of several protons of *trans*-EE<sup>a</sup> (1.0 mg) in its <sup>1</sup>H NMR analyses in 1.25 mol L<sup>-1</sup> NaOD/D<sub>2</sub>O (0.75 mL) and those with the additions<sup>b</sup> of Bu<sub>4</sub>NCl and NaCl



	C <sub>2</sub> -H (d)	C <sub>5</sub> -H (d)	C <sub>6</sub> -H (dd)	C <sub>α</sub> -H (s)	C <sub>β</sub> -H (s)
1.25 mol L <sup>-1</sup> NaOD/D <sub>2</sub> O	6.65	6.33	6.54	6.83	6.00
1.25 mol L <sup>-1</sup> NaOD/D <sub>2</sub> O + Bu <sub>4</sub> NCl	6.46 (−76) <sup>c</sup>	6.27 (−24)	6.38 (−64)	6.71 (−48)	5.89 (−44)
1.25 mol L <sup>-1</sup> NaOD/D <sub>2</sub> O + NaCl	6.65 (±0)	6.36 (+12)	6.56 (+8)	6.85 (+8)	6.02 (+8)

<sup>a</sup> The results only for the *trans*-isomer are shown as most of the *cis*-isomer signals were overlapped with those of the *trans*-isomer. <sup>b</sup> Bu<sub>4</sub>NCl and NaCl were added to the NaOD solution with the concentration of the additives being set at 1.25 mol L<sup>-1</sup>. <sup>c</sup> Changes in the chemical shift (Hz) caused by the additive were shown in the parenthesis.

### Effects of Bu<sub>4</sub>N<sup>+</sup> on aerobic oxidation of lignin polymer

We have so far discussed the degradation behavior of the lignin model compounds processing β-O-4 linkages, which consist around 50% of the inter-unit linkages of native lignin polymer. In this section we wish to discuss aerobic oxidation of native lignin polymer focusing mainly on vanillin production, on the basis of the results obtained above. In the discussion below, we assume that the non-phenolic model **LM1** represents the reactivity of the monomeric unit in the middle of the polymer and the phenolic model **LM2** corresponds to that of the phenolic end of the polymer.

The initial step of the degradation of lignin polymer is simple alkaline degradation of the phenolic end, which is the fastest reaction observed in this study (Fig. 5). When the phenolic end has a β-O-4 linkage, the degradation results in the formation of an enol ether end group. The enol ether end formed – if it is in contact with O<sub>2</sub> – is further oxidized into vanillin or vanillic acid and forms a new phenolic end in the adjacent monomeric unit. When these stepwise reactions continued, lignin polymers could degrade completely into the low molecular weight compounds. However, this type of “unzipping” reaction seems not to play major roles in the degradation. The reaction time required for completing the degradation of **LM2** was ~8 h, which was far from sufficient for vanillin production from the wood flour under the same conditions: at least 43 h is necessary to fully produce vanillin from the wood flour at 120 °C under air,<sup>8</sup> although the introduction of pure O<sub>2</sub> shortens the reaction time (see above). On one hand, the unzipping vanillin/vanillic acid production may be stopped when the reaction “bumps” into a less reactive linkage such as β-5, β-β, 4-O-5 and 5-5' linkages. On the other hand, other types of reactions such as condensations are possible to prevent the vanillin/vanillic acid production from the phenolic end.

Our results obtained for **LM2** revealed that Bu<sub>4</sub>N<sup>+</sup> did no good for the vanillin production after all: Bu<sub>4</sub>N<sup>+</sup> stabilizes the enol ether to make the vanillin formation slow and changes the

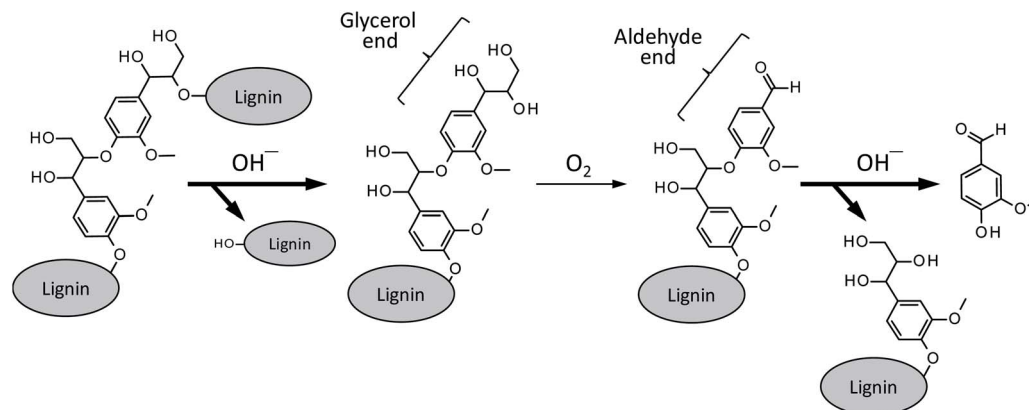
selectivity to vanillic acid-oriented. However, these negative effects of Bu<sub>4</sub>N<sup>+</sup> are not very serious in the vanillin production from native lignin in Bu<sub>4</sub>NOH, since the vanillin production from the phenolic end is fundamentally of little importance in entire vanillin production reactions.

Besides a series of the reactions on the phenolic end, alkaline degradation of non-phenolic middle units gradually takes place. As shown in Scheme 4, the initial step of the degradation on a non-phenolic β-O-4 type middle unit is alkaline-catalyzed ether link cleavage to form a glycerol end group, which corresponds to the pathway A in Scheme 2. This step is significantly enhanced in Bu<sub>4</sub>NOH due to its strong basicity and this is one of the benefits in the utilization of Bu<sub>4</sub>NOH instead of NaOH.

The oxidation of the glycerol group by O<sub>2</sub>, pathway B in Scheme 2 in the case of the model compound **LM1**, then occurs to form a benzaldehyde end group (vanillin end group when the lignin sample is derived from soft wood lignin). There are two possibilities for the fate of the benzaldehyde end group. One is the free benzaldehyde formation by the cleavage of the ether link connecting the benzaldehyde end to the adjacent monomeric unit, which corresponds to the pathway C in Scheme 2. The other is the disproportionation of the aldehyde group resulting in the formation of benzoic acid and benzyl alcohol ends (pathway D in Scheme 2). The degradation in Bu<sub>4</sub>NOH facilitates the former reaction pathway to increase the benzaldehyde yield.

These proposed reactions suggest that the reaction mixture from the wood flour should involve some amount of vanillyl alcohol. However, the compound was not detected in the degradation of the wood flour under any conditions, although vanillic acid was detected as a major product (Fig. 1). This is probably because vanillyl alcohol end group is unstable due to the presence of benzyl hydroxy group which is readily subjected to condensation reactions.<sup>22</sup> It is also noted that vanillic acid, unlike vanillyl alcohol, can also be formed from the oxidation of the enol ether end, as indicated from Fig. 5, and some of the origins of vanillic acid produced from the wood flour is considered to be phenolic end groups of lignin polymer.





Scheme 4 Vanillin formation from a  $\beta$ -O-4 middle unit of lignin polymer. The pathways with bold arrows are positively influenced by  $\text{Bu}_4\text{N}^+$ .

## Conclusions

The degradation of Japanese cedar wood flour under  $\text{O}_2$  produced vanillin and vanillic acid in 23.2 and 1.2% yields on the basis of the Klason lignin amount, respectively, at  $120^\circ\text{C}$  for 4 h in  $1.25\text{ mol L}^{-1}\text{ Bu}_4\text{NOH aq.}$ , where the  $\text{OH}^-$  concentration was enhanced to  $3.75\text{ mol L}^{-1}$  by the addition of NaOH. These yields have been significantly improved, compared to those obtained under air reported in our previous studies.<sup>8</sup> Also, the reaction time required for achieving the maximum vanillin and vanillic acid yields was drastically shortened to 4 h by the  $\text{O}_2$  introduction. It should be noted that the yields of the compounds were comparable to those obtained in the AN oxidation, which is a benchmark for evaluating selectivity of lignin depolymerization methods.

The mechanical investigation with the lignin model compounds suggested that the major vanillin formation pathway involved the alkaline-catalyzed  $\beta$ -ether cleavage on the non-phenolic middle units of lignin polymer to produce the glycerol end group, followed by the oxidation of the end group by  $\text{O}_2$  to aldehyde and subsequent release of free vanillin. The positive effect of  $\text{Bu}_4\text{NOH}$  over NaOH with regard to the vanillin formation was partially attributed to the basicity of  $\text{Bu}_4\text{NOH}$  stronger than that of NaOH. More fundamentally,  $\text{Bu}_4\text{N}^+$  significantly suppressed the disproportionation of the aldehyde end so that the release of vanillin became to play more roles in entire degradation.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This work was supported by the Technologies for Creating Next-Generation Agriculture, Forestry, and Fisheries under the Cross-Ministerial Strategic Innovation Promotion Program (SIP) administered by the Council for Science, Technology, and Innovation (CSTI), Japan, and a Grant-in-Aid for Young Scientists (B) (No. 17K18008) from the Japan Society for the

Promotion of Science. The GC/MS analysis was carried out with the apparatus in Kyoto Research Park Corp.

## References

- 1 H.-M. Chang, Oxidation, in *Lignins—Occurrence, Formation, Structure and Reactions*, ed. K. V. Sarkanen and C. H. Ludwig, John Wiley and Sons, NY, 1971, pp. 433–485.
- 2 T. P. Schultz and M. C. Templeton, Proposed Mechanism for the Nitrobenzene Oxidation of Lignin, *Holzforschung*, 1986, **40**, 93–97.
- 3 (a) M. B. Hocking, Vanillin: Synthetic Flavoring from Spent Sulfite Liquor, *J. Chem. Educ.*, 1997, **74**, 1055–1059; (b) D. Havkin-Frenkel, Vanillin, *Kirk-Othmer Encyclopedia of Chemical Technology*, 2018, pp. 1–12.
- 4 (a) J. R. Silverman, A. M. Danby and B. Subramaniam, Intensified ozonolysis of lignins in a spray reactor: insights into product yields and lignin structure, *React. Chem. Eng.*, 2019, **4**, 1421–1430; (b) A. Gavrilidis, A. Constantinou, K. Hellgardt, K.-K. Hii, G. J. Hutchings, G. L. Brett, S. Kuhn and S. P. Marsden, Aerobic oxidations in flow: opportunities for the fine chemicals and pharmaceuticals industries, *React. Chem. Eng.*, 2016, **1**, 595–612.
- 5 M. Maeda, T. Hosoya, K. Yoshioka, H. Miyafuji, H. Ohno and T. Yamada, Vanillin Production from Native Softwood Lignin in the Presence of Tetrabutylammonium Ion, *J. Wood Sci.*, 2018, **64**, 810–815.
- 6 M. Fache, B. Boutevin and S. Caillol, Vanillin Production from Lignin and Its Use as a Renewable Chemical, *ACS Sustain. Chem. Eng.*, 2016, **4**, 35–46.
- 7 S. G. Santos, A. P. Marques, D. L. D. Lima, D. V. Evtuguin and V. I. Esteves, Kinetics of Eucalypt Lignosulfonate Oxidation to Aromatic Aldehydes by Oxygen in Alkaline Medium, *Ind. Eng. Chem. Res.*, 2011, **50**, 291–298.
- 8 K. Yamamoto, T. Hosoya, K. Yoshioka, H. Miyafuji, H. Ohno and T. Yamada, Tetrabutylammonium Hydroxide 30-Hydrate as Novel Reaction Medium for Lignin Conversion, *ACS Sustain. Chem. Eng.*, 2017, **5**, 10111–10115.
- 9 P. C. Rodrigues Pinto, E. A. Borges da Silva and A. E. Rodrigues, Insights into Oxidative Conversion of

- Lignin to High-Added-Value Phenolic Aldehydes, *Ind. Eng. Chem. Res.*, 2011, **50**, 741–748.
- 10 J. D. P. Araújo, C. A. Grande and A. E. Rodrigues, Vanillin Production from Lignin Oxidation in a Batch Reactor, *Chem. Eng. Res. Des.*, 2010, **88**, 1024–1032.
  - 11 A. Rahimi, A. Ulbrich, J. J. Coon and S. S. Stahl, Formic-acid-induced Depolymerization of Oxidized Lignin to Aromatics, *Nature*, 2014, **515**, 249–252.
  - 12 T. Rinesch, J. Mottweiler, M. Puche, P. Concepción, A. Corma and C. Bolm, Mechanistic Investigation of the Catalyzed Cleavage for the Lignin  $\beta$ -O-4 Linkage: Implications for Vanillin and Vanillic Acid Formation, *ACS Sustain. Chem. Eng.*, 2017, **5**, 9818–9825.
  - 13 S. Gharehkhani, Y. Zhang and P. Fatehi, Lignin-derived Platform Molecules through TEMPO Catalytic Oxidation Strategies, *Prog. Energy Combust. Sci.*, 2019, **72**, 59–89.
  - 14 R. Rinaldi, R. Jastrzebski, M. T. Clough, J. Ralph, M. Kennema, P. C. A. Bruijninx and B. M. Weckhuysen, Paving the Way for Lignin Valorisation: Recent Advances in Bioengineering, Biorefining and Catalysis, *Angew. Chem., Int. Ed.*, 2016, **55**, 8164–8215.
  - 15 C. Li, X. Zhao, A. Wang, G. W. Huber and T. Zhang, Catalytic Transformation of Lignin for the Production of Chemicals and Fuels, *Chem. Rev.*, 2015, **115**, 11559–11624.
  - 16 H. Kawamoto, Lignin Pyrolysis Reactions, *J. Wood Sci.*, 2017, **63**, 117–132.
  - 17 A. Llevot, E. Grau, S. Carlotti, S. Grelier and H. Cramail, From Lignin-derived Aromatic Compounds to Novel Biobased Polymers, *Macromol. Rapid Commun.*, 2016, **37**, 9–28.
  - 18 H. Zhang, X. Yong, J. Zhou, J. Deng and Y. Wu, Biomass Vanillin-Derived Polymeric Microspheres Containing Functional Aldehyde Groups: Preparation, Characterization, and Application as Adsorbent, *ACS Appl. Mater. Interfaces*, 2016, **8**, 2753–2763.
  - 19 G. H. Tomlinson and H. Hibbert, Studies on Lignin and Related Compounds. XXIV. The Formation of Vanillin from Waste Sulfite Liquor, *J. Am. Chem. Soc.*, 1936, **58**, 345–348.
  - 20 G. H. Tomlinson and H. Hibbert, Studies on Lignin and Related Compounds. XXV. Mechanism of Vanillin Formation from Spruce Lignin Sulfonic Acids in Relation to Lignin Structure, *J. Am. Chem. Soc.*, 1936, **58**, 348–353.
  - 21 P. Ding, M. Garrett, Ø. Loe, A. W. Nienow and A. W. Pacek, Generation of Hydrogen Gas during the Catalytic Oxidation of Sodium Lignosulfonate to Vanillin: Initial Results, *Ind. Eng. Chem. Res.*, 2012, **51**, 184–188.
  - 22 J. Gierer, Chemistry of Delignification Part 1: General Concept and Reactions during Pulping, *Wood Sci. Technol.*, 1985, **19**, 289–312.
  - 23 D. R. Dimmel and L. F. Schuller, Structural/Reactivity Studies (I): Soda Reactions of Lignin Model Compounds, *J. Wood Chem. Technol.*, 1986, **6**, 535–564.
  - 24 T. F. Hubbard, T. P. Schultz and T. H. Fisher, Alkaline Hydrolysis of Nonphenolic  $\beta$ -O-4 Lignin Model Dimers: Substituent Effects on the Leaving Phenoxide in Neighboring Group vs. Direct Nucleophilic Attack, *Holzforschung*, 1992, **46**, 315–320.
  - 25 W. E. Collier, T. H. Fisher, L. L. Ingram Jr, A. L. Harris and T. P. Schultz, Alkaline Hydrolysis of Nonphenolic  $\beta$ -O-4 Lignin Model Dimers: Further Studies of the Substituent Effect on the Leaving Phenoxide, *Holzforschung*, 1996, **50**, 420–424.
  - 26 J. Gierer, Chemistry of Delignification Part 2: Reactions of Lignins during Bleaching, *Wood Sci. Technol.*, 1986, **20**, 1–33.
  - 27 E. Johansson and S. Ljunggren, The Kinetics of Lignin Reactions During Oxygen Bleaching. IV. The Reactivities of Different Lignin Model Compounds and the Influence of Metal Ions on the Rate of Degradation, *J. Wood Chem. Technol.*, 1994, **14**, 507–525.
  - 28 J. Gierer, T. Reitberger, E. Yang and B.-H. Yoon, Formation and Involvement of Radicals in Oxygen Delignification Studied by the Autoxidation of Lignin and Carbohydrate Model Compounds, *J. Wood Chem. Technol.*, 2001, **21**, 313–341.
  - 29 S. Kuitunen, A. Kalliola, V. Tarvo, T. Tamminen, S. Rovio, T. Liitiä, T. Ohra-aho, T. Lehtimaa, T. Vuorinen and V. Alopaeus, Lignin Oxidation Mechanisms under Oxygen Delignification Conditions. Part 3. Reaction Pathways and Modeling, *Holzforschung*, 2011, **65**, 587–599.
  - 30 S. Ohmura, T. Yokoyama and Y. Matsumoto, Progress of Oxidation of Non-phenolic Lignin Moiety in an Oxygen Bleaching Process via the Conversion of Non-phenolic into Phenolic Lignin Moiety, *J. Wood Sci.*, 2012, **58**, 243–250.
  - 31 D. R. Dimmel and L. F. Bovee, Pulping Reactions of Vinyl Ethers, *J. Wood Chem. Technol.*, 1993, **13**, 583–592.
  - 32 S. Kubo, K. Hashida, S. Hishiyama, T. Yamada and S. Hosoya, Possibilities of the Formation of Enol-Ethers in Lignin by Soda Pulping, *J. Wood Chem. Technol.*, 2015, **35**, 62–72.
  - 33 K. Lundquist and S. v. Unge, Stability of Arylglycerols During Alkaline Cooking, *Holzforschung*, 2004, **58**, 330–333.

