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Core–shell silica@Cu_xZnAl LDH catalysts for efficient CO₂ hydrogenation to methanol†

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The efficient production of methanol by reduction of CO₂ using green hydrogen is a promising strategy from both a green chemistry and a carbon net zero perspective. Herein, we report the synthesis of well-dispersed core–shell catalyst precursors using silica@Cu_xZnAl-LDHs that can convert CO₂ to methanol. The catalyst precursors can be formed using either a commercially available silica (ES757) or a mesoporous silica (e.g. MCM-48). These hybrid materials show significantly enhanced catalytic performance compared to the equivalent unsupported Cu_xZnAl LDH precursor. Space-time yields of up to 0.7 g_{MeOH} g_{cat}⁻¹ h⁻¹ under mild operating conditions were observed.

To reverse the rapid increase in atmosphere CO₂ concentrations it is both urgent and critical we develop efficient strategies to reduce carbon emissions and reach a carbon net zero goal. To date, prodigious efforts have been devoted to developing alternative renewable non-fossil fuel energy sources, as well as CO₂ capture and utilization strategies. Some of the most important approaches involve the conversion of CO₂ into liquid hydrocarbons, formic acid, and methanol.¹ In particular, hydrogenation of CO₂ to methanol using renewably sourced hydrogen will be strategically a very important component in the portfolio of processes to reach both our emission and decarbonisation targets.^{2–4} Today, hydrogen can be produced from sustainable resources by utilising hydropower, solar energy, and biomass, thus offering the potential for a green “methanol economy”.⁵

Cu_xZn_yAlO_z based-catalysts are some of the most widely used catalysts for methanol synthesis from CO₂.^{6,7} Metallic Cu nanoparticles are generally recognised as the active species, while ZnO and Al₂O₃ act as both electronic and geometric promoters for Cu. Several synthetic methods have been developed to assemble these compositions.^{6–8} Layered double hydroxides (LDHs) are a family of anionic 2D layered materials with the general formula,

$[(M_{1-x}^{z+}M'^{y+}_x(OH)_2)^{w+}(A^{n-})_{w/n} \cdot mH_2O]$, where M and M' are typically divalent and trivalent metal cations, octahedrally coordinated by hydroxyl groups and Aⁿ⁻ represents the charge-compensating intercalated anion.⁸ Cu²⁺, Zn²⁺ and Al³⁺ cations can be incorporated into the LDH structure and used as precursors to Cu_xZn_yAlO_z catalysts for methanol synthesis. To obtain a robust catalyst exhibiting high activity, selectivity and lifetime for CO₂ hydrogenation, two main strategies have been explored for Cu_xZn_yAlO_z catalysts derived from LDHs; (i) incorporation of elemental promoters such as Y, Zr, Ga into the Cu_xZn_yAl LDH;^{9–11} and (ii) exfoliation and dispersion of the LDH layers using the aqueous miscible organic solvent treatment (AMOST) method.⁸ These strategies strive to generate high surface area metallic Cu and also inhibit the Cu nanoparticles from sintering as it is generally accepted that the catalytic activity is a function of exposed metallic Cu surface area to volume ratio. In practise, unsupported Cu_xZn_yAl LDH platelets tend to stack/aggregate together and following calcination and reduction this results in a decrease in the exposed metallic Cu surface area to volume ratio which limits subsequent catalytic activity.

Herein, we report a new catalyst strategy by synthesising Cu_xZnAl-CO₃ LDH precursors supported on a both commercially available silica (ES757) and some mesoporous silica (e.g. MCM48, SBA-16) cores, to form an SiO₂@Cu_xZnAl LDH core@shell structure. The core@shell catalyst precursors formed using a commercially available silica (ES757) as the core show significantly enhanced catalytic performance compared to the equivalent unsupported Cu_xZnAl LDH precursor. Using the larger pore volume core silica such as MCM48 provides even further improvements in catalytic performance. The general synthesis procedure of core–shell catalyst is shown in Fig. 1a using ES757 as an exemplar core. ES757 is initially dispersed in Na₂CO₃ solution, then Cu_xZnAl-CO₃ LDH is generated using an

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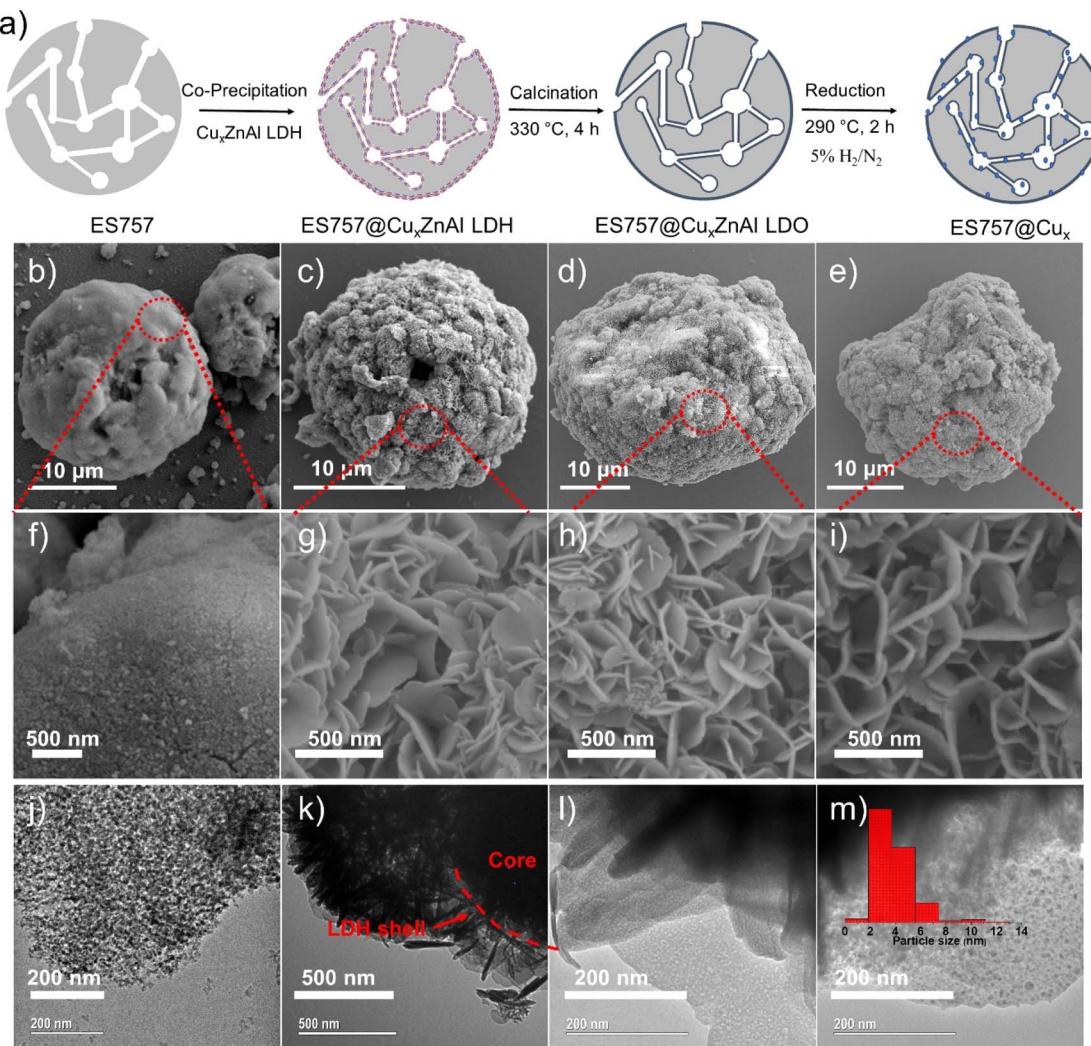


Fig. 1 (a) Synthesis scheme of Cu nanoparticles from ES757@Cu_xZnAl LDH. SEM images of (b and f) ES757; (c and g) ES757@Cu_{1.3}ZnAl LDH; (d and h) ES757@Cu_{1.3}ZnAl LDO and (e and i) ES757@Cu_{1.3}. TEM images of (j) ES757; (k) ES757@Cu_{1.3}ZnAl LDH; (l) shell of ES757@Cu_{1.3}ZnAl LDO; (m) shell of ES757@Cu_{1.3}.

in situ co-precipitation approach, the Cu_xZnAl-CO₃ LDH nucleates and then grows on both the external and internal surfaces of the ES757 particles to form ES757@Cu_xZnAl LDH. Calcination at 330 °C for 4 h produces ES757@Cu_xZnAl LDO, in which the LDH shell is transformed into uniform mixed metal oxide, often referred to as layered double oxide (LDO). The final active catalyst is prepared by reduction of ES757@Cu_xZnAl LDO under a dilute hydrogen atmosphere (5% H₂/N₂) at 290 °C for 2 h. We refer to the finished active catalyst as ES757@Cu_x.

As shown in Fig. 1b, ES757 is supplied as large spherical agglomerates (*ca.* 25 μm diameter) with a relatively smooth surface (Fig. 1f and S1a†). The spherical agglomerates are decorated with a number of tiny silica nanoparticles (*ca.* 10–20 nm diameter) as indicated in Fig. 1j. When Cu_{1.3}ZnAl LDH is carefully co-precipitated in the presence of a suspension of ES757 the LDH nucleates and grows from the silica surface. For the LDH coating, we observe a rosette platelet morphology with individual platelets between 300–500 nm (Fig. S2a and d†). In

our optimised synthesis conditions, the LDH platelets cover the entire surface, the LDH platelets grow hierarchically from the ES757 surface forming uniform core-shell particles (Fig. 1c and k) and a honeycomb surface (Fig. 1g and S1b†) texture. As a control, a physical mixture of ES757 and Cu_{1.3}ZnAl-CO₃ LDH (prepared by manually mixing the two solids in 40 : 60 the weight ratio) shows separated particles that retain their individual morphological features (Fig. S1c and d†). After calcination at 330 °C, the unsupported Cu_{1.3}ZnAl LDO platelets condense and aggregate together (Fig. S2b and e†). In contrast, calcination of ES757@Cu_{1.3}ZnAl LDH produces LDO platelets still immobilised on the ES757 and retaining their honeycomb structure (Fig. 1d and h). Further reduction by hydrogen, produces metallic Cu nanoparticles embedded on the LDO matrix which we refer to as ES757@Cu_{1.3}.^{8,12} In ES757@Cu_{1.3}, the metallic Cu(0) nanoparticles are well dispersed with size distribution of 3.9 ± 1.6 nm (Fig. 1m). In comparison, hydrogen reduction of the unsupported Cu_{1.3}ZnAl LDH (named as Cu_{1.3})



produces nanoplatelets stacked together (Fig. S2c and f†), with lower exposed metallic Cu(0). The electron mapping images (Fig. 2a–e) of ES757@Cu_{1.3}ZnAl LDH demonstrate that Cu, Zn and Al from the Cu_{1.3}ZnAl LDH and Si from ES757 are homogeneously dispersed across the whole spherical particle.

Powder X-ray diffraction data (Fig. 2f) for ES757 exhibits a broad feature between $2\theta = 15\text{--}35^\circ$ typical of an amorphous silica-based material. The XRD of ES757@Cu_{1.3}ZnAl LDH shows this amorphous background superimposed with the characteristic (00l) and (110) Bragg reflections associated with the crystalline LDH layer. The *d*-spacing of the (003) Bragg reflection of ES757@Cu_{1.3}ZnAl LDH at $2\theta = 7.58^\circ$ indicates a carbonate-intercalated LDH.¹³ After calcination, the characteristic LDH Bragg reflections disappear and they are replaced by a broad weak Bragg reflection at $2\theta \approx 38^\circ$ (Fig. 2f and S8b†). This feature can be assigned to the formation of copper oxide. Following reduction by hydrogen, a very weak Bragg reflection at $2\theta \approx 43^\circ$ corresponding to (111) reflection from metallic copper is observed.

The FTIR spectrum (Fig. 2g) of ES757@Cu_{1.3}ZnAl LDH exhibits both the characteristic IR vibrations bands of ES757 (the Si–O stretching at 1050 cm^{-1}) and LDH shell (the metal–oxygen (M–O) vibration at 750 cm^{-1} and the O–H stretching of M–OH and water at 3440 cm^{-1} , and water bending at 1600 cm^{-1}).^{13–15} Upon calcination, the water bending absorbance (1600 cm^{-1}) disappears and the O–H stretching band (3500 cm^{-1}) reduces in intensity due to dehydration and dihydroxylation of the LDH shell. A sharp band at 1350 cm^{-1} in ES757@Cu_{1.3}ZnAl LDH confirmed the presence of intercalated carbonate ions.^{16,17,19}

The chemical composition of both unsupported Cu_{1.3}ZnAl LDH and ES757@Cu_{1.3}ZnAl LDH were investigated using elemental analyses and thermogravimetric analysis (TGA). The Cu/Al ratio of both pristine Cu_{1.3}ZnAl LDH and the core–shell materials was determined by inductively coupled plasma optical emission spectrometry (ICP-OES). The data agree with the predicted values (Table S1†). The TGA data (Fig. S3†) for ES757@Cu_{1.3}ZnAl LDH show the typical weight loss stages for an LDH, we can also use the TGA data to determine the ES757 : LDH ratio in the core–shell materials as 40 : 60, again in agreement with the predicted value. The formula of Cu_{1.3}ZnAl LDH and ES757@Cu_{1.3}ZnAl LDH can be obtained from elemental analysis and TGA, which are $[\text{Cu}_{1.31}\text{Zn}_{0.93}\text{Al(OH)}_{6.49}(\text{CO}_3)_{0.49}\cdot 4\text{H}_2\text{O}]$ and $[\text{SiO}_2]_{3.85}[\text{Cu}_{1.29}\text{Zn}_{1.03}\text{Al(OH)}_{6.64}(\text{CO}_3)_{0.50}\cdot 1.49\text{H}_2\text{O}]_{1.05}$, respectively.¹⁰

N₂ adsorption and desorption isotherms were used to investigate the porosity of the samples. The specific surface areas (Fig. S5a†) of ES757 and Cu_{1.3}ZnAl LDH using BET analysis are $273\text{ m}^2\text{ g}^{-1}$ and $48\text{ m}^2\text{ g}^{-1}$, respectively. Upon forming ES757@Cu_{1.3}ZnAl LDH, the BET surface area becomes $189\text{ m}^2\text{ g}^{-1}$, which is still higher than the theoretical surface area ($138\text{ m}^2\text{ g}^{-1}$) considering the 40 : 60 weight ratio (ES757 : LDH). As shown in Fig. S4a,† Cu_{1.3}ZnAl LDH exhibits a type II isotherm with a H3 loop, indicating the agglomerate of platelets with slit-like pores. The BJH derived pore size distribution for Cu_{1.3}ZnAl LDH (Fig. S4b†) shows a wide pore size distribution with no clear maxima due to intense interplatelet aggregation.²⁰ ES757 presents a type II isotherm with a H2b hysteresis loop, indicating that it is a mesoporous material in which the pore body is slightly larger than the pore neck. The pores in ES757 have

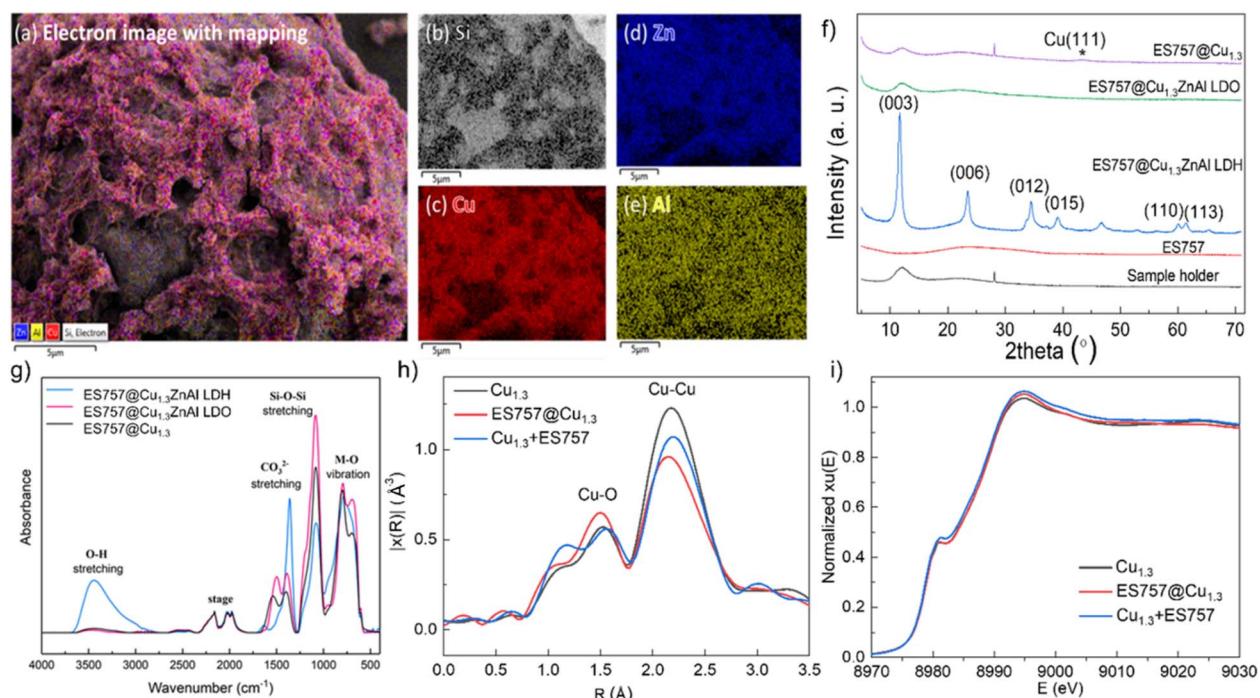


Fig. 2 Structural evolution during the preparation of ES757@Cu_{1.3}. (a) Electron image with Zn, Al, Cu, Si element mapping; (b) Si; (c) Cu; (d) Zn; (e) Al of ES757@Cu_{1.3}ZnAl LDH; (f) powder X-ray diffraction patterns; (g) FTIR spectra; (h) Fourier transformed magnitudes of the experimental Cu K-edge EXAFS spectra; (i) normalised Cu K-edge XANES spectra.



a diameter in the range of 25–125 nm. The N_2 adsorption and desorption isotherms of $ES757@\text{Cu}_{1.3}\text{ZnAl}$ LDH are identical to that of $ES757$, demonstrating the overall pore structure is retained following the formation of the core–shell structure. The pore size of $ES757@\text{Cu}_{1.3}\text{ZnAl}$ LDH is smaller and in a narrower range (Fig. S4b†), indicating some $\text{Cu}_{1.3}\text{ZnAl}$ LDH may slightly block some of the pore openings in $ES757$. These observations indicate that immobilising an LDH on a porous substrate can avoid the aggregation of LDH platelets and exposes more surface area. A similar trend was found in total pore volume (Fig. S5b†). Finally, calcination followed by reduction by hydrogen did not cause significant changes to the overall structural morphology the hybrid materials (Fig. S4†). We observe a slight increase in the specific surface area after calcination (Fig. S5†) which is due to the formation of amorphous porous network for $\text{Cu}_{1.3}\text{ZnAl}$ LDO.

The X-ray absorption near-edge structure (XANES) spectroscopy and extended X-ray absorption fine structure (EXAFS) measurements were measured to probe the nature of Cu species in three catalysts prepared by calcination and reduction of (i) $\text{Cu}_{1.3}\text{ZnAl}$ LDH, (ii) $ES757@\text{Cu}_{1.3}\text{ZnAl}$ LDH and (iii) $\text{Cu}_{1.3} + ES757$ (a physical mixture of $\text{Cu}_{1.3}\text{ZnAl}$ LDH and $ES757$). All the samples show two characteristic features in the first shell (Fig. 2h). The most noticeable scattering was observed at 2.2 \AA which is ascribed to the Cu–Cu separation. A weak feature at 1.7 \AA is assigned to Cu–O. According to the fitting of the EXAFS (Fig. S6, S7 and Table S3†), $ES757@\text{Cu}_{1.3}$ has the lowest number of Cu–Cu nearest neighbour interactions, indicating $ES757@\text{Cu}_{1.3}$ has the best dispersion compared to $\text{Cu}_{1.3}$ and $\text{Cu}_{1.3} + ES757$. XANES spectra in Fig. 2i shows that the Cu K edge feature falls at the highest energy in $ES757@\text{Cu}_{1.3}$ which suggests Cu is more electronic deficient ($\text{Cu}^{\delta+}$), these data are consistent with formation of well dispersed Cu nanoparticles in contact to the support through Cu–O interactions.

The catalytic performance of $\text{Cu}_{1.3}$, $ES757@\text{Cu}_{1.3}$ and $\text{Cu}_{1.3} + ES757$ for CO_2 hydrogenation to methanol was evaluated. As shown in Fig. 3a, $ES757@\text{Cu}_{1.3}$ and $\text{Cu}_{1.3} + ES757$ exhibit higher CO_2 conversion (23% and 26%, respectively) than that of $\text{Cu}_{1.3}$ (16%). It is believed that the introduction of $ES757$ has a synergistic effect benefiting mass transfer and therefore promote CO_2 conversion.²¹ Noteworthy, the CO_2 conversions of $ES757@\text{Cu}_{1.3}$ and $\text{Cu}_{1.3} + ES757$ are approaching the equilibrium value under our catalytic testing conditions.²² More

importantly, $ES757@\text{Cu}_{1.3}$ shows the highest methanol selectivity of 48% (the only other C-product detected was CO) which is significantly higher than that of $\text{Cu}_{1.3} + ES757$ (28%). The particle sizes are listed in Table S2,† it indicates high dispersion of Cu species. It should be noted that the particle sizes derived from TEM are a bit larger than those from XRD. We believe that this may arise from the high copper dispersion as evidenced from EXAFS and the measured copper surface area (S_{Cu}). It is widely accepted that stable, well-dispersed metallic copper with a large S_{Cu} is linked to overall methanol productivity.²³ $N_2\text{O}$ chemisorption was used to determine the S_{Cu} . The copper dispersion¹⁸ is then determined from exposed copper surface (S_{Cu})^{24,25} and total copper loading. We found that both the copper dispersion and exposed copper surface area of $ES757@\text{Cu}_{1.3}$ (25%, $32.14\text{ m}^2\text{ g}_{\text{catalyst}}^{-1}$) is much higher than that of $\text{Cu}_{1.3}$ (13.57%, $23.05\text{ m}^2\text{ g}_{\text{catalyst}}^{-1}$) and $\text{Cu}_{1.3} + ES757$ (1.88%, $17.07\text{ m}^2\text{ g}_{\text{catalyst}}^{-1}$) (Table S2†). It is apparent that a catalyst prepared without a support or simply mixing the catalyst with porous silica cannot avoid the aggregation between LDH platelets, leading to much lower exposed copper surface. Immobilising and orienting the LDH catalyst precursor on the porous silica creates a highly dispersed and exposed surface bound active metallic copper sites, resulting in the superior CO_2 conversion and methanol selectivity. This enables $ES757@\text{Cu}_{1.3}$ to exhibit the highest space-time yield for methanol ($\text{STY}_{\text{MeOH}} 0.64\text{ g}_{\text{methanol}}\text{ g}_{\text{cat}}^{-1}\text{ h}^{-1}$) among these three catalysts.

We further studied the effects of copper dispersion and S_{Cu} by preparing a series of $ES757@\text{Cu}_x\text{ZnAl}-\text{CO}_3$ –LDH core–shells with different copper loadings. The core–shells were prepared using the same procedure as $ES757@\text{Cu}_{1.3}\text{ZnAl}$ LDH, the copper content was controlled by the ratio of metal salts used in the co-precipitation step. The series of precursors, $ES757@\text{Cu}_x\text{ZnAl}-\text{CO}_3$ –LDH ($x = 0.8\text{--}4$) were prepared and following calcination and hydrogen reduction were named $ES757@\text{Cu}_x$ ($x = 0.8\text{--}4$). HR-SEM images (Fig. S8†) confirm the formation of core–shell structures and the powder XRD data (Fig. S9a†) indicate no other crystalline impurities. Following calcination, $ES757@\text{Cu}_x\text{ZnAl}$ LDOs do not present any LDH Bragg reflections. Following hydrogen reduction, the intensity of metallic Cu 111 Bragg reflection increases in intensity with increasing copper loading. The copper loading, dispersion, S_{Cu} and the catalytic performance (turnover frequency (TOF) and space time

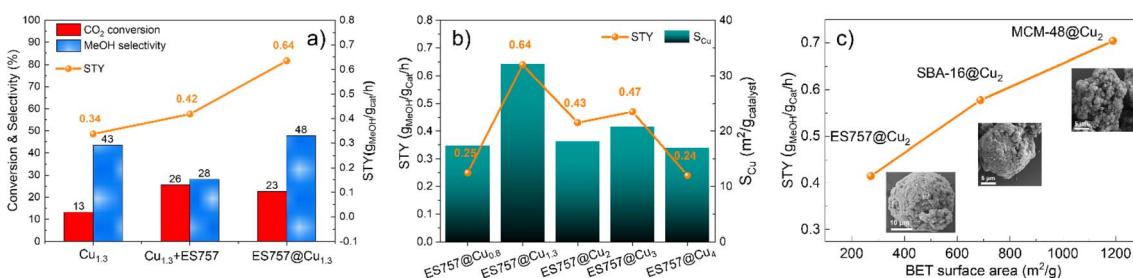


Fig. 3 Catalytic performance and structure relationship. The effect of (a) core–shell structure, (b) Cu loading and Cu surface area and (c) specific surface area (insets are the HRSEM of core–shells) on the catalytic performance. Reaction condition: temperature = $270\text{ }^\circ\text{C}$, pressure = 45 bar, $\text{H}_2 : \text{CO}_2$ (molar) = 3 : 1, WHSV = $18\,000\text{ mL g}_{\text{catalyst}}^{-1}\text{ h}^{-1}$.



yield STY) are summarised in Table S2.† The relationship between STY_{MeOH} and S_{Cu} is shown in Fig. 3b. It is found that both copper dispersion and S_{Cu} increase with increasing copper loading, reaching a maximum at ES757@Cu_{1.3}. Further increasing the copper loading results in the decrease of copper dispersion and S_{Cu} due to the sintering of the metallic Cu nanoparticles at high loadings. The STY_{MeOH} follows the same trend as copper dispersion and S_{Cu} . ES757@Cu_{1.3} with the highest copper dispersion and largest S_{Cu} exhibits the highest STY_{MeOH} among all core–shell materials we have studied.

The catalytic effects of other porous silica cores were explored. We have use of SBA-16 and MCM-48 with specific surface areas of 688 and 1186 m² g⁻¹ respectively. The synthesis method is the same as that of ES757@Cu_xZnAl LDHs, the copper loading was kept constant at Cu : Zn : Al = 2 : 1 : 1. The calcined and reduced catalysts derived from SBA-16@Cu₂ZnAl-CO₃ LDH and MCM-48@Cu₂ZnAl-CO₃ LDH were named SBA-16@Cu₂ and MCM-48@Cu₂ respectively. As shown in Fig. 3c (inset HRSEM) and Fig. S9–14,† these samples formed the similar core–shell structures as that of ES757@Cu_{1.3}ZnAl LDH. A uniform distribution of Cu, Zn and Al is observed over the MCM-48 and SBA-16 particles as evidenced by EDX mapping. The influence of the specific surface areas of these cores on the catalytic performance of the final catalyst can be seen in Fig. 3c. Generally, the catalysts with higher surface area exhibit higher STY_{MeOH}. It is possible that copper may distribute more evenly over the surface when employing a silica core with a higher surface area.^{21,26}

The catalytic performance of the core–shell catalysts developed in this work were compared with those of an commercial Cu/ZnO/Al₂O₃ catalyst and our best Cu-catalyst (Cu_{1.3}ZnGaO₃) derived from the exfoliated Cu_{1.3}ZnGa LDH precursor, under the same catalytic conditions.⁸ As shown in Table S3†, both ES757@Cu_{1.3} and MCM-48@Cu₂ exhibit higher CO₂ conversion and methanol selectivity. These catalysts deliver superior STY_{MeOH} of 0.64 and 0.7 g_{methanol} g_{cat}⁻¹ h⁻¹, respectively more than Cu_{1.3}ZnGa (STY_{MeOH} = 0.59 g_{methanol} g_{cat}⁻¹ h⁻¹), delivering nearly twice the commercial catalyst (STY_{MeOH} = 0.38 g_{methanol} g_{cat}⁻¹ h⁻¹) under our testing conditions. It is also important to note that the copper loadings in our core–shell catalysts is typically 19.81–24.5 wt%, significantly lower than that of Cu_{1.3}ZnGa (33.5 wt%) and commercial catalyst (50.0 wt%). Therefore, on a per Cu atom basis these core–shell catalysts contain significantly more active individual catalytic sites.

Conclusion

We have developed effective syntheses of a series of core–shell catalysts using micro- and mesoporous silica cores and a Cu_x-ZnAl LDH as a functional shell. The silica cores have excellent coverage by the LDHs platelets and are robust to calcination. Hydrogen reduction of the silica@Cu_xZnAl LDO precursors produces robust and highly dispersed metallic Cu nanoparticles with high S_{Cu} . We believe this strategy delivers an effective pathway to prevent the aggregation of the active catalytic sites under catalytic conditions. ES757@Cu_{1.3} was found as our best performing catalyst to date among the ES757@Cu_x family,

although this can be further improved by using a higher surface area silica core (e.g. MCM-48). The STY_{MeOH} for these materials places them as some of the best performing catalytic systems for CO₂ hydrogenation to MeOH, especially if you normalise on a per Cu basis.

Data availability

Experimental procedures, and spectroscopic data can be found in the ESI.†

Author contributions

Meng Lyu and Jianwei Zheng, performed the synthetic and catalysis experimental work; Claire Coulthard assisted with the electron microscopy studies; Ren Jing, and Yufei Zhao recorded and interpreted the X-ray absorption analysis; Shik Chi Edman Tsang, Chunping Chen, and Dermot O'Hare conceptualised the research, acquired funding, and supervised the work; all authors revised and edited the manuscript. All authors have read and agreed to the published version of the manuscript.

Conflicts of interest

The authors declare no competing financial interests.

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Notes and references

- 1 R.-P. Ye, J. Ding, W. Gong, M. D. Argyle, Q. Zhong, Y. Wang, C. K. Russell, Z. Xu, A. G. Russell and Q. Li, *Nat. Commun.*, 2019, **10**, 1–15.
- 2 S. Kattel, P. J. Ramírez, J. G. Chen, J. A. Rodriguez and P. Liu, *Science*, 2017, **355**, 1296–1299.
- 3 H. Bahruji, M. Bowker, G. Hutchings, N. Dimitratos, P. Wells, E. Gibson, W. Jones, C. Brookes, D. Morgan and G. Lalev, *J. Catal.*, 2016, **343**, 133–146.
- 4 O. Martin, A. J. Martín, C. Mondelli, S. Mitchell, T. F. Segawa, R. Hauer, C. Drouilly, D. Curulla-Ferré and J. Pérez-Ramírez, *Angew. Chem., Int. Ed.*, 2016, **55**, 6261–6265.
- 5 D. W. Stephan, *Nature*, 2013, **495**, 54–55.
- 6 X. Jiang, X. Nie, X. Guo, C. Song and J. G. Chen, *Chem. Rev.*, 2020, **120**, 7984–8034.
- 7 F. Meshkini, M. Taghizadeh and M. Bahmani, *Fuel*, 2010, **89**, 170–175.
- 8 M. M.-J. Li, C. Chen, T. c. e. Ayvalı, H. Suo, J. Zheng, I. F. Teixeira, L. Ye, H. Zou, D. O'Hare and S. C. E. Tsang, *ACS Catal.*, 2018, **8**, 4390–4401.
- 9 P. Gao, F. Li, F. Xiao, N. Zhao, W. Wei, L. Zhong and Y. Sun, *Catal. Today*, 2012, **194**, 9–15.



10 P. Gao, F. Li, N. Zhao, F. Xiao, W. Wei, L. Zhong and Y. Sun, *Appl. Catal., A*, 2013, **468**, 442–452.

11 S. Kühl, J. Schumann, I. Kasatkin, M. Hävecker, R. Schlögl and M. Behrens, *Catal. Today*, 2015, **246**, 92–100.

12 M. Behrens, F. Studt, I. Kasatkin, S. Kühl, M. Hävecker, F. Abild-Pedersen, S. Zander, F. Girgsdies, P. Kurr and B.-L. Kniep, *Science*, 2012, **336**, 893–897.

13 F. Cavani, F. Trifiro and A. Vaccari, *Catal. Today*, 1991, **11**, 173–301.

14 R.-P. Ye, L. Lin, C.-C. Chen, J.-X. Yang, F. Li, X. Zhang, D.-J. Li, Y.-Y. Qin, Z. Zhou and Y.-G. Yao, *ACS Catal.*, 2018, **8**, 3382–3394.

15 S. O. Akpotu and B. Moodley, *J. Mol. Liq.*, 2018, **261**, 540–549.

16 M. Smyrnioti, C. Tampaxis, T. Steriotis and T. Ioannides, *Catal. Today*, 2020, **357**, 495–502.

17 J. Lavallee, *Catal. Today*, 1996, **27**, 377–401.

18 R.-C. Zeng, X.-T. Li, Z.-G. Liu, F. Zhang, S.-Q. Li and H.-Z. Cui, *Front. Mater. Sci.*, 2015, **9**, 355–365.

19 A. M. Cardinale, C. Carbone, S. Consani, M. Fortunato and N. Parodi, *Crystals*, 2020, **10**, 443.

20 C. Chen, A. Wangriya, J.-C. Buffet and D. O'Hare, *Dalton Trans.*, 2015, **44**, 16392–16398.

21 M. K. Koh, M. Khavarian, S. P. Chai and A. R. Mohamed, *Int. J. Hydrogen Energy*, 2018, **43**, 9334–9342.

22 K. Stangeland, H. Li and Z. Yu, *Ind. Eng. Chem. Res.*, 2018, **57**, 4081–4094.

23 G. V. Sagar, P. V. R. Rao, C. S. Srikanth and K. V. Chary, *J. Phys. Chem. B*, 2006, **110**, 13881–13888.

24 D. S. Brands, E. K. Poels, T. A. Krieger, O. V. Makarova, C. Weber, S. Veer and A. Bliek, *Catal. Lett.*, 1996, **36**, 175–181.

25 W. Robinson and J. Mol, *Appl. Catal.*, 1990, **63**, 165–179.

26 P. S. Murthy, W. Liang, Y. Jiang and J. Huang, *Energy Fuels*, 2021, **35**, 8558–8584.

