Energy Advances



REVIEW ARTICLE

View Article Online



Cite this: Energy Adv., 2022,

Received 15th February 2022, Accepted 19th June 2022

DOI: 10.1039/d2ya00043a

rsc.li/energy-advances

Progress in electrode and electrolyte materials: path to all-solid-state Li-ion batteries

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This review presents a brief scenario regarding the development of cathodes, anodes, and electrolytes for next-generation Li-ion batteries (LIBs) and supercapacitors for future energy technologies. The specific capacity and power density are two prime requirements for energy storage devices, which are mainly decided by the microstructure and composition of electrodes. Electrolyte, which is the highway for ions between electrodes, plays a crucial role in developing advanced batteries. Miniaturized electrode-based LIBs with high energy storage densities are a smart approach toward huge future energy demands, where nanomaterials play a crucial role. The ultra-large surface of nanostructurebased electrodes offers improved electrochemical performance per unit electrode area and/or material mass. Porous nanostructured material-based electrodes/electrolytes provide fast and shortened transportation pathways for carriers, facilitating improved reaction kinetics. This review presents the fabrication and electrochemical performances of different nanomaterial-based LIBs, including their critical challenges such as thermal runaway and dendrite growth. An overview of all-solid-state Li-ion batteries (ASSLIB), with the potential to bridge the gap between the laboratory and market, is presented. Finally, the status, challenges, and outlook for enhancing the performance of cathodes, anodes, electrolytes, and their integration in ASSLIB are briefly covered for the attention of the wider functional and energy material communities.

1. Introduction to energy systems

Currently, society depends on fossil fuels to generate electricity, drive vehicles, and power industries using internal combustion engines.1 Battery-driven energy has found a realistic way to liberate society, 2-5 where green energy can be generated from natural resources such as solar energy, hydro power, windturbines, and wave upthrust.^{6,7} After harvesting energy, it needs to be stored it in an efficient system for long-lasting and maximum intercalation-deintercalation. According to the literature, energy storage systems have existed since ancient times. The first energy storage system was introduced by Agastya Rishi (Sages

in Ancient Indian civilization) approximately ~5000 BC.8 In 1780 AD, Luigi Galvani performed a unique electricity experiment on a frog, called the frog legs experiment.9 Later, based on the concept of the frog legs experiment, an Italian physicist, Sir Alessandro Volta, used metallic elements instead of a biological cell or living entities to produce electricity. Then, he investigated a way to store the produced energy, which was called a battery. 10 In continuation of the investigation of energy storage devices, Edison invented the nickel-iron battery in 1968, producing a rechargeable system having nickel oxide-hydroxide positive plates and negative iron plates, with potassium hydroxide as the electrolyte. 11 Thus, the development of energy storage systems dates back to the study by Agastya Sanhita, resulting in high energy density for the application of ASSLIB in HEV and smart/mobile devices.

1.1 Solid-state electrolyte/batteries

The major challenges associated with electric-drive vehicles include their cost and performance, especially regarding their batteries, which are responsible for a large portion of the cost of these vehicles. 12-14 The main thrust as the foundation for Li-ion batteries (LIBs) occurred after the oil crisis in the 1970s. Subsequently, the research community focused on developing the fossil-fuel-free natural energy harvesting and energy storage

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sectors to fulfill energy requirements globally. 15,16 Accordingly, a suitable candidate with potential for energy storage was the LIB, which is a green energy storage system with a no-memory loss effect. 17-20 The operative mechanism of LIBs is a simple principle similar to that of other storage systems, i.e., moving electrons from one region (anode) to another (cathode), which generates an electrical current. LIBs are considered safer compared to conventional batteries such as lead-acid and CdS, which exhibit several issues including the emission of toxic gases and overheating during charging and discharging.

All-solid-state batteries (ASSBs) have attracted significant attention for application in future technologies due to their safety and high energy densities. However, many ASSBs are limited by their Coulombic efficiency, poor power performance, and short cycling life due to the high resistance at the interfaces in ASSBs. Banerjee et al. 21 explored suitable materials that can serve as SEs for the fabrication of ASSBs, namely, materials with high ionic conductivity ($\sigma_{\text{Li}^+} > 0.1 \text{ mS cm}^{-1}$, which are commonly referred to as "superionic conductors", but possess lower electronic conductivity ($\sigma_{\rm e}$ < 10^{-7} mS cm $^{-1}$). These materials include polymer-, oxide-, and sulfide-based electrolytes. Before elaborating on LIBs, solid-state electrolytes (SSE) enable the utilization of Li metal anodes, which are considered the most promising anodes for next-generation rechargeable batteries due to their ultrahigh theoretical specific capacity of 3860 mA h g⁻¹ and lowest negative electrochemical potential (-3.04 V versus the standard hydrogen electrode). However, in conventional organic electrolytes, lithium metal suffers from an unstable solid-state interphase, dendrite penetration, and pulverization issues. The state-of-the-art batteries possessing SSEs have been reviewed by Xu et al. 22 to guarantee the development of next-generation battery systems with improved energy density and high safety. Numerous compounds including oxides, sulfides, and polymer ionic conductors have been developed and several achievements comparable to liquid electrolytes have been obtained. Materials possessing high theoretical capacities, such as lithium, sulfur, and lithium intercalation compounds, have also been introduced in the "solid family."

The novel class of fast lithium ion-conducting metal oxides with the chemical composition $Li_5La_3M_2O_{12}$ (M = Nb and Ta) possess a garnet-related structure. Among the investigated compounds with garnet-related structures, Li₆BaLa₂Ta₂O₁₂ exhibit the highest Li⁺ ion conductivity of 4×10^{-5} S cm⁻¹ at 22 °C with an activation energy of 0.40 eV; however, its bulk and total conductivity at room temperature are not sufficiently high to develop an ideal all-solid-state lithium ion rechargeable battery. Murugan et al.23 reported that due to the high lithium ion conductivity, good thermal and chemical stability against reactions with prospective electrode materials, environmental benignity, availability of its starting materials, low cost, and ease of preparation and densification of Li₇La₃Zr₂O₁₂ make it a promising solid electrolyte for all-solid-state lithium ion rechargeable batteries (ASSLIBs).

Lithium garnet (i.e., Li_{6.4}La₃Zr_{1.4}Ta_{0.6}O₁₂, LLZTO) particlebased composite membranes and Li-salt-free polyethylene oxides (PEOs) as SSE were reported by Zhang et al.,24 which were crucial for the enhancement in the conductivity of the membranes containing 40 nm LLZTO particles due to the difference in the specific surface area and related to the percolation effect. Compared to the conventional PEO doped with lithium salt, the insulating PEO in PEO:LLZTO membrane electrolyte was conductive to the suppression of lithium dendrite growth because it hindered the current flow. The PEO:LLZTO membrane electrolyte exhibited a conductivity of $2.1 \times 10^{-4} \ \mathrm{S \ cm^{-1}}$ at 30 °C and $5.6 \times 10^{-4} \text{ S cm}^{-1}$ at 60 °C, and consequently the solid-state LiFePO₄/PEO:LLZTO/Li and LiFe_{0.15}Mn_{0.85}PO₄/PEO:LLZTO/Li cells delivered energy densities of 345 W h kg⁻¹ (662 W h L⁻¹) and 405 W h kg⁻¹ (700 W h L⁻¹, without the package weight or volume) with a good rate capability and cycling performance. The combination of nano-scale Li-ion-conducting particles and an insulating polymer provided a promising solution to produce powerful SSEs for high-performance solid-state lithium batteries (SSLBs). Thus, a polymer with improved stability is available, and consequently SSLBs can be constructed with enlarged voltage cathodes such as LiNi_{0.5}Mn_{1.5}O₄ to further increase the energy density.

Zhang et al.²⁵ reported that Li_{6.75}La₃Zr_{1.75}Ta_{0.25}O₁₂ (LLZTO) ceramics could trigger structural modification in the poly(vinylidene fluoride) (PVDF) polymer electrolyte, which was prepared using the conventional solution-casting method. The LLZTO-modified PVDF membrane was shown to be a promising electrolyte material for use in ASSLIBs with significantly enhanced performances (a high ionic conductivity of about 5×10^{-4} S cm⁻¹ at 25 °C, high mechanical strength, and good thermal stability). Furthermore, the LiCoO₂|PVDF/LLZTO-CPE|Li cell presented a satisfactory rate capability and cycling stability at room temperature, which showed that PVDF/LLZTO-CPE has great potential to be used as the electrolyte in SSLBs.

An electrical current is created in LIBs because of the chemical reactions and movement of ions inside these batteries. Electrons move in the cell from the anode to cathode, which are located at the opposite ends of the cell. Significant progress has been achieved in the development of rechargeable LIBs since their introduction in the early 1990s, which are an integral part of all portable electronics and popular for powering hybrid vehicles. 26,27 They can be recharged by using appropriate adaptors for several cycles (500-1000 cycles). The electrolytes inside these batteries also play an important role in the migration of ions from the anode to cathode, and vice versa. In the case of solid electrolytes, they can simultaneously act as a separator between the anode and cathode.²⁸

In the modern digital era, among the various energy storage systems, LIBs represent the most popular rechargeable batteries for use in portable electronic devices such as mobile phones and laptops due to their long cycle life and high specific capacity. LIBs can also be formed into many shapes, making them ideal for use in the essential products of laptops, tablets, and cell phones. LIBs are widely used in these devices because of their rechargeability and negligible memory effect. Owing to their long cycle life and high capacity, LIBs are considered suitable for next-generation advanced mobile electronic devices (flexible and transparent devices), electric vehicles (EVs), hybrid

Annual lithium-ion battery demand

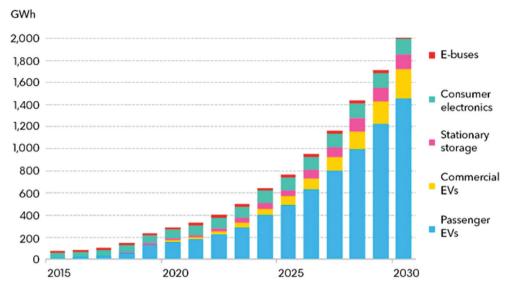


Fig. 1 Li-ion battery demand forecast (https://about.bnef.com/electric-vehicle-outlook/)

electric vehicles (HEVs), and renewable energy storage applications.²⁹ Fig. 1 shows the increasing demand of LIBs since 2015 and will continue to rise sharply over the next few decades.

The greatest demand for electric passenger/commercial vehicles is expected to occur in the near future with stationary storage systems. However, the relatively low charge/discharge rates and safety concerns of these systems have limited their use in applied applications requiring both high-power density and high capacity for EVs and HEVs. Thus, the major scientific challenge associated with ASSLIBs is enhancing their power density, cycle life, recyclability, and safety concerns. 30-32 The energy obtained from different sources can be stored in LIBs, and subsequently used according to the demand. Fig. 2(a) presents an overview of the energy production and storage from various energy sectors, including the functions of LIBs. To determine suitable candidates for the fabrication of LIBs, active, hybrid, and Si-based nanostructured materials must be tested to fulfill requirements of reversible capacity, good ionic and electrical conductivity, long cycle life, high lithium diffusion rate in the active material, and conclusively low cost and eco-compatibility.

Currently, LIBs are the dominant power source for mobile phones, laptops, and numerous other portable electronic devices. Also, they have been increasingly used in electric vehicles (EVs) and flexible/mobile electronics since their commercialization. The Sony Corporation (1991) commercialized the first modern LIB, which held twice the energy density and was almost 10-times cheaper than the existing Li batteries.34 The Li-battery was first introduced by the American chemist Gilbert Newton Lewis (G. N. Lewis) in 1912, 35 while the first lithium battery was invented in the 1970s, and the first attempts to develop rechargeable batteries were made in the 1980s by Bell Labs.36

Lithium (Li) is one of the lightest metals with the highest electrochemical potential, which can provide the largest specific

energy density. It requires careful and systematic handling, where the development of breakthrough technologies based on new anodes, cathodes, and non-aqueous electrolytes can enable a steady improvement in high-energy lithium battery systems. Although LIBs are expensive, they have never experienced the memory issues that affect other battery technologies. LIBs exhibit a slightly lower energy density than lithium metal batteries; however, LIBs are safer than Li batteries and provide certain precautions during charging and discharging. Also, the LIB is a low-maintenance battery, and no schedule is required for cycling to prolong its lifetime. Compared to nickelcadmium (Ni-Cd) batteries, the self-discharge of LIBs is less than half and is well-fitted for modern fuel gauge applications.

Based on the enormous success achieved from the laboratory to daily life, the discovery of lithium-ion batteries led to the 2019 Nobel Prize in Chemistry. The three key contributors to the development of LIBs were John B. Goodenough, M. Stanley Whittingham, and Akira Yoshino. Stanley Whittingham focused on developing titanium disulfide (TiS₂)-based cathodes for LIBs, which possess space for ion intercalation, as shown in Fig. 2b. The metallic lithium was used as an anode for lithium batteries, which easily provides electrons. The battery had a very high energy density and a voltage of 2 V.37 The discovery of this battery was a big announcement at that time, but the formation of lithium whiskers/dendrites potentially led to short-circuiting in the battery (Fig. 2c). Goodenough investigated this failure and proposed the use of transition metal oxide-based cathodes instead of TiS2. His group discovered that lithium-cobalt oxide (LiCoO₂) is a suitable cathode material, which was stable during cell operation (Fig. 2d). They successfully increased the voltage to 4 V. 38,39 Then, another scientist interested in the development of lightweight LIBs was Akira Yoshino from the Asahi Kasei Corporation, Japan. He used LiCoO2 as a cathode and tried different carbon materials as the

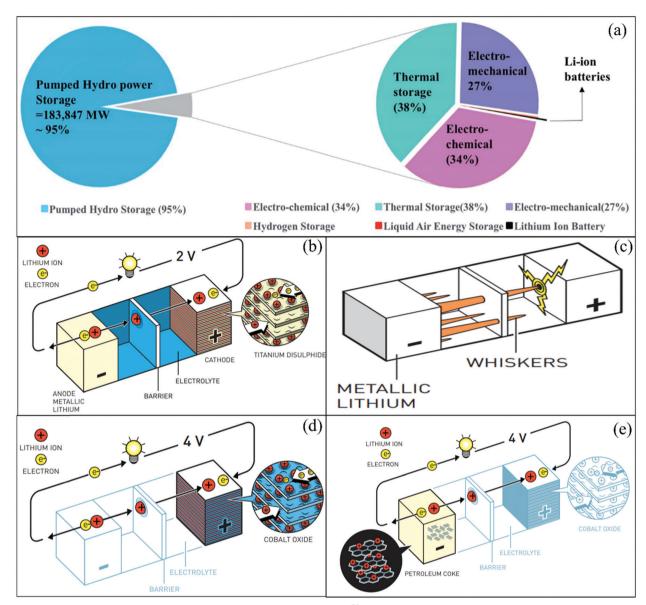


Fig. 2 (a) Contribution of worldwide energy storage projects to grid applications. 30 (b) Lithium-based battery using Li_xTiS₂ as the cathode. (c) Formation of lithium whiskers/dendrites potentially leading to short-circuiting. (d) Lithium-based battery using $\text{Li}_x \text{CoO}_2$ as the cathode. (e) Ion transfer cell lithiumion battery configuration. (©Johan Jarnestad/Royal Swedish Academy of Sciences³³)

anode. Finally, petroleum coke was used as the anode and a full battery was developed (Fig. 2e), which demonstrated a high capacity and voltage.40

1.2 Principle of LIBs

An LIB consists of four components including a positive electrode (cathode), a negative electrode (anode), a separator (to separate electrodes), and electrolyte for the movement of ions through chemical reactions. The existing LIBs use LiCoO2 as the cathode and graphite as the anode. The standard electrolyte is liquid LiPF₆, soaked by the separator between electrodes. For the cathode, Al is used as a current collector, and for the anode, Cu is used as a current collector (Fig. 3). During charging, the cathode releases Li⁺ (Li-ions), which

moves through the electrolyte and gets accommodated in the anode (means energy stored). Meanwhile, electrons flow through the external circuit and the separator blocks the flow of electrons due to its insulating nature and provides easy access for ions. In the discharging process, Li+ ions migrate back to the cathode via the electrolyte and release the energy stored inside the battery. The performance of LIBs strongly depends on the utilized electrode materials, which is mainly decided by various parameters, such as, the physical and chemical properties, microstructure and composition of the material. Fig. 4(a) shows some important parameters (specific capacity, coulombic efficiency, power density, capacity retention, voltage stability and conductivity, toxicity and safety issues) that demonstrate the potential of electrode materials

DISCHARGE

CHARGE

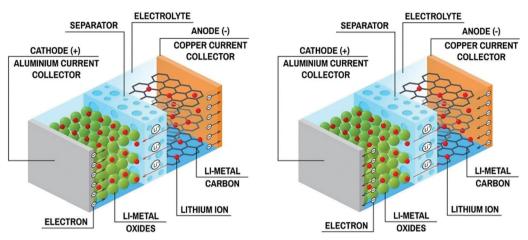


Fig. 3 Charge-discharge process in Li-ion battery (Image Credit: https://sivVector/Shutterstock.com).

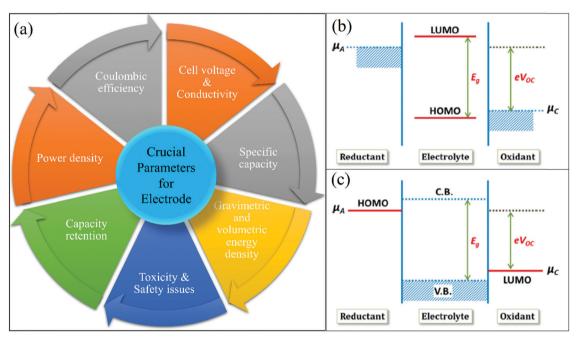


Fig. 4 (a) Performance parameters of electrodes: specific capacity, coulombic efficiency, power density, capacity retention, voltage stability and conductivity, toxicity and safety issues. (b) Liquid electrolyte with solid electrodes (relative energies of the electrolyte window (E_{α}) and the electrochemical potentials of the electrode, μA and μC with no electrode/electrolyte reaction). (c) Solid electrolyte with liquid or gaseous reactants.⁴¹ (Reproduced with permission from the American Chemical Society⁴¹).

for use in LIBs. The voltage stability window of the cell is examined by evaluating the molecular properties of its materials via quantum chemical characterization of their highest occupied molecular orbital (HOMO) and lowest unoccupied molecular orbital (LUMO). The relative energies of the electrolyte window (E_g) and the electrochemical potentials of the electrode, μA and μC , with no electrode/electrolyte reactions are shown in Fig. 4b. The difference between the HOMO and LUMO of a liquid electrolyte or the bottom of the conduction

band and the top of the valence band of the solid electrolyte decides the electrochemical stability window (ESW) (Fig. 4b and c).

To achieve stability, the ESW must be larger than the open circuit energy $(V_{oc} = (\mu_A - \mu_C)/e)$ (difference in Li chemical potential in each electrode). 41-44 Table 1 summarizes the critical cell performance parameters that need to be examined before commencing large scale commercial production. 45,46 Another significant task in the case of battery technology is to carefully identify the failure mechanism (physical/electrical/

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Table 1 Essential parameters for testing the performance of a lithium-ion cell⁴⁵

Parameter	Measuring unit	Measuring formula	Information
Operating voltage	Volts (V) mA g ⁻¹	Instrumental	Energy density and safety
Current density	$mA g^{-1}$	Instrumental	For testing rate capabilities
Theoretical capacity	$mA h g^{-1}$	$TC = \frac{F \times x}{3.6 \times M.M \times y}$	Lithium-ion storage capability
Gravimetric capacity	${ m mA~h~g}^{-1}$	$C = \frac{I(\text{mA}) \times t(\text{h})}{m(\text{g})}$	Li ⁺ storage capability measured per unit mass
Areal capacity	mA h cm ⁻²	$C = \frac{I(\text{mA}) \times t(\text{h})}{A(\text{cm}^2)}$	Li ⁺ storage capability measured per unit area
Volumetric capacity	mA h cm ⁻²	$C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$	Li ⁺ storage capability measured per unit volume
Specific energy density	W h g ⁻¹ or W h cm ⁻² or W h cm ⁻³ W g ⁻¹ or W cm ⁻² or W cm ⁻³	$E = C \times V$	How much energy can be extracted
Power density	W g^{-1} or W cm ⁻² or W cm ⁻³	$P = I \times V$	How fast the energy can be extracted
$C_{ m rate}$	h^{-1}	$C_{\text{rate}} = \frac{J \left(\text{mA g}^{-1} \right)}{C \left(\text{mA h g}^{-1} \right)}$	Rate of charging/discharging
Coulombic efficiency	N/A	$\%E = \frac{C_{\text{charging}}}{C_{\text{discharging}}} \times 100$	Reversible capacity
State of charge (SOC)	NA	SOC = remaining	Remaining capacity of a battery
		capacity/rated capacity	
Depth of discharge (DOD)	NA	DOD = 1 - SOC	Percentage of the total discharge battery capacity
Cycle life	NA	_	Number of discharge-charge cycles handled by a battery at a specific DOD
Calendar life	NA	_	The expected life span of the battery under storage or periodic cycling conditions.

mechanical/chemical). Thus, the failure mode, mechanism, and effect analysis (FMMEA) methodology has been adopted to discover the failure mechanism, as shown in Table 2. The FMMEA methodology provides details on the cell components, mode, and the cause of failure. 47 Table 2 also summarises the anode and cathode active materials and the current collectors, separator for Li-ions, electrolyte salts (organics solvents), and the terminals.

Before preparing the electrode materials, it is crucial to select the parent material based on parameters such as costeffectiveness, non-toxicity, abundance, and safety. The low cost of the raw material and the preparation conditions (NTP) will lead to an overall cost that is within the affordable limit of the consumer market. The non-toxic nature of electrode materials is the primary requirement for the safe use of the device. The electrode materials should be abundant in nature to be commercialized and able to balance the supply according to the demand from the consumer sector. The most feasible elements from the periodic table are transition elements, and thus extensive studies have been performed based on their composites with various phases and structures (Fig. 5). It should be noted that parameters such as the ionic radius (helps in stabilizing oxidation states), ionization energy (decides oxidizing and reduction power), and electronegativity (helps in altering the redox potential) of elements need to be considered before the preparation of electrode materials. 48 Table 3 describes the anode and cathode electrodes, separator, etc., including their deficiencies and remedies.

Crabtree pointed out the next breakthroughs expected at the other end of the battery for making better anodes. The anode stores lithium ions when the battery is charged and sends them to the cathode as the battery releases power. Japanese

electronics giant Sony introduced carbon anodes to replace the troublesome lithium metal anodes in the early 1990s. These batteries were losing their performance, making necessary to restore it. Currently, one of the major problems is the graphite anodes developed after the lithium metal anodes, which eliminate lithium ions from the batteries, but they returning to the anode during charging. This leads to the formation of tree-like dendrite structures instead of a coating on the anode surface.

Materials scientist Nitash Balsara, University of California, Berkeley, explained that carbon anodes can accept lithium ions at a given rate. "If you try to send lithium (through the battery) too fast (while charging), the lithium doesn't go into the graphite, it sticks on the outside. It becomes a safety hazard." Small-size batteries can easily grow dendrites across the electrolyte and contact the opposite pole, as demonstrated by Goodenough. Permeable membranes, e.g., separators, are generally used to prevent the contact between electrodes, and thus stop short circuits, while allowing the flow of ions from the electrolyte. Nevertheless, this process involves a high risk of breaking the dendrite structures, leading to pore blockage. This often hampers the ion migration to the separator, thereby impacting the lifetime of the battery.

Electrodes for Li-ion batteries

2.1 Cathode materials of lithium-ion batteries (LIBs)

2.1.1 Lithium cobalt oxide (LiCoO₂). LiCoO₂ is a lithiumion intercalation material introduced in 1980 by Prof. John B. Goodenough, which has a terminal voltage of over 3 V.50 The LIB with this cathode exhibited a specific power of 250-340 W kg⁻¹ with an efficiency of 90%, which is much higher than that of the

Table 2 The failure mode, mechanism, and effect analysis (FMMEA) for lithium-ion batteries (LIBs)⁴⁷

Battery	Potential failure	Potential failure	Mechanism		Potential	Likelihood of	Severity of	Ease of
component		mechanism (s)	type	Observed effect	failure causes		occurrence	
	Thickening of solid electrolyte interphase layer	Chemical reduction reaction and deposition	Wear out	Increased charge transfer resistance, reduction of capacity, reduction of power	Chemical side reactions between lithium, electrode, and solvent	High	Low	High
	Particle fracture	Mechanical stress	Over stress	Reduction of capacity, reduction of power	Intercalation stress	Moderate	Low	Low
	Reduced electrode porosity	Mechanical degradation	Wear out	Increased diffusion resistance, reduction of capacity, reduction of power	Dimensional changes in electrode	Moderate	Low	Low
	Lithium plating and dendrite growth on anode surface	Chemical reaction	Wear out	Can cause a short circuit if dendrites puncture the separator	Charging the battery at low temperatures or high rates	Low	High	Low
Anode (current collector)	Free copper particles or copper plating	Chemical corrosion reaction and dissolution	Wear out	Increased resistance, reduction of power, reduction of current density	Over-discharge of the battery	Low	High	Low
Cathode (active material)	Thickening of solid electrolyte interphase layer	Chemical reduction reaction and deposition	Wear out	Increased charge transfer resistance, reduction of capacity, reduction of power	Chemical side reactions between lithium, electrode, and solvent	High	Low	High
	Particle fracture	Mechanical stress	Over stress	Reduction of capacity, reduction of power	Intercalation stress	Moderate	Low	Low
	Reduced electrode porosity	Mechanical degradation	Wear out	Increased diffusion resistance, reduction of capacity, reduction of power	Dimensional changes in electrode	Moderate	Low	Low
	Gas generation and bloating of cell casing	Thermally driven electrode decomposition	Over stress	Reduction of capacity	Overcharge of the battery or short circuit	Low	High	Low
Cathode (current collector)	Pitting corrosion of aluminum	Chemical corrosion reaction	Wear out	Increased resistance, reduction of power, reduction of current density	Overcharge of the battery	Low	Moderate	Low
Separator	Hole in separator	Mechanical damage	Over stress	High heat generation due to Joule heating, bloating of cell casing, drastic voltage reduction	Dendrite for- mation, external crushing of cell	Low	High	Moderate
	Closing of separator pores	Thermally- induced melt- ing of separator	Over stress	Inability to charge or discharge the battery	High internal cell temperature	Low	High	High
Lithium ions	Reduction in lithium ions, thickening of solid electrolyte inter-phase layer	Electrolyte reduction and solid product formation	Wear out	Reduction of capacity	Chemical side reactions between lithium, electro- des, and solvent	High	Low	High
Electrolyte salt	Decrease in lithium salt concentration	Chemical reduction reaction and deposition	Wear out	Increased diffusion resistance	Chemical side reactions between lithium, electro- des, and solvent	Low	High	Low
Organic solvents	Gas generation and bloating of cell casing	Chemical	Over stress	Increased diffusion resistance, and may lead to thermal runaway	High external temperature, over- charging of the cell	Low	High	Low
	Thickening of solid electrolyte interphase layer	Chemical	Wear out	Increased charge transfer resistance, reduction of capacity, reduction of power	Chemical side reactions between lithium, electro- des, and solvent	High	Low	High
	External corrosive path between positive and negative leads	Chemical cor-	Wear out	High heat generation due to Joule heating, bloating of cell casing, drastic voltage reduction		Low	High	Moderate
	Solder cracking	Thermal fatigue mechanical vibration fatigue		Loss of conductivity between battery and host device	Circuit disconnect		Moderate	High
Casing	Internal short circuit between anode and cathode		Over stress	High heat generation due to Joule heating, bloating of cell casing, drastic voltage reduction		Low	High	Moderate

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Oxidizing Power = Ionic Radii Electronegativity 10 12 13 14 15 16 radioactive H toxic heavy expensive Be suitable for batteries Mg A Ar K Ca Sc Mn Ga Ge As Se Br Rb Tc Pd ZrMo Ag Sn Sb Nb Ru Rh Cd ln Te Ba W Re Os Pt Au Pb Bi At Re Cs La Hf Ta Hg ΤI Ra Ac

Fig. 5 Periodic table is available to design new electrode materials. The colored squares are excluded due to either their high cost, low availability, toxicity, or radioactivity. This slightly restricts the elements available for the design of new materials but can be useful in guiding synthetic methods. Despite their toxicity, some transition metals, such as V and Co, are still actively investigated. 48 Reproduced with permission from the American Chemical Society.48

Table 3 Deficiencies in the present LIBs and their possible remedies⁴⁹

Location of deficiency	Deficiencies	Possible remedies
Carbonaceous anode (negative electrode)	Low capacity density (A h l ⁻¹)	Replace carbon with an improved alloy anode that allows high coulombic efficiency, good power capability, low irreversible capacity, and low cost with little or no loss of specific capacity or cell voltage
Negative electrode- electrolyte interface	Low coulombic efficiency with alloy anodes caused by solid electrolyte interphase (SEI) growth on the first cycle and continuing with cycling	Improved coatings, functional binders, and/or electrolyte additives to protect the interface during large volume changes
Positive electrode (lithiated transition metal oxide or phosphate)	Low specific capacity (A h kg ⁻¹) and charging voltage limited	Replace with new cathode material that allows high coulombic efficiency, good power capability, low irreversible capacity, and lower cost with little or no loss of capacity density or cell voltage
Positive electrode– electrolyte interface	Low coulombic efficiency at higher voltage limiting specific capacity and cycle life and causing increased cell impedance with cycling	Improve coating of cathode material, binders, and/or electrolyte additives that can prevent impedance increase with cycling, dissolution of transition metal ions
Separator	Penetration with conductive particles or lithium dendrites	Improved coatings of separators that do not impede ion flux, salt diffusion, or fluid flow, but can improve penetration strength or combine chemically with lithium dendrites
Metal collectors	Solid metal foils add to cost and take away from energy as they are inert in the system, yet must be thick enough to provide adequate electrical and thermal conductance	Perforated or expanded metal collectors are in common use for primary lithium batteries and secondary aqueous batteries, but have not been engineered for lithium-ion

existing lead-acid and Ni-Cd secondary batteries (at that time). The crystal structure of layered LiCoO₂ is identical to the α-NaFeO₂type structure, (space group R3m). The lithium and cobalt ions are located in octahedral 3a and 3b sites, respectively, separated by layers of cubic close-packed oxygen ions. The unit cell is comprised of three slabs of edge-sharing CoO6 octahedra and separated by interstitial layers of Li.51 Mizushima et al.52 presented the first report on LiCoO2 as a cathode material, which was used as a commercial cathode in the first commercial Li-ion battery (with graphite as the anode) by Sony Corporation in 1991. The theoretical capacity of $LiCoO_2$ was 274 mA h g^{-1} , while the experimental capacity was measured to be 160 mA h g⁻¹. Lithium-ion-cobalt batteries have been made from lithium carbonate and cobalt to achieve a very high capacity. These batteries are used in cell phones, laptops, electronic cameras, and several other devices. The battery has a cobalt oxide cathode and a graphite carbon anode. During intercalation and/or de-intercalation, the lithium ions move from the anode to cathode and vice versa.

However, due to their short lifespan and limited specific power, these batteries also exhibit certain drawbacks.

Cho et al. 53 synthesized a high-performance LiCoO₂ cathode via the sol-gel coating of Al₂O₃ on the LiCoO₂ particle surface, followed by heat treatment at 600 °C for 3 h. The Al₂O₃-coated LiCoO₂ cathode showed no decrease in its original specific capacity of 174 mA h g⁻¹ compared to the pristine cathode (vs. lithium metal) together with excellent capacity retention (97% of its initial capacity) between 4.4 and 2.75 V (after 50 cycles). This enhancement in capacity retention has been attributed to the improvement in the structural stability of LiCoO2 during cycling owing to the presence of Al atoms on the electrode surface.

Li et al. 54 examined the effects of halogen doping on the structural stability, electronic state, electrode potential, and Li diffusion behavior of LiCoO2 systems via density functional theory (DFT) calculations. It was observed that fluorine, chlorine, and bromine substitution of oxygen species suppresses the lattice changes upon Li de-intercalation. In contrast, an enhancement in structural stability, electronic conductivity, and Li mobility was confirmed from the intercalation-deintercalation studies. Chen et al.55 reported the synthesis of LiCoO2 (LCO) cathodes coated with a gel polymer Li-ion conductor layer, P(VDF-HFP)/ LiTFSI (PHL) via the solution-casting technique at low temperature. The coated LCO cathode (thickness = 3 µm) exhibited 88.4% capacity retention of its original capacity (184.3 mA h g⁻¹) after nearly 200 cycles in the range of 3.0-4.6 V. This is higher than that of the uncoated cathode, which showed only 80.4% of its original capacity (171.5 mA h g⁻¹). This enhancement was attributed to the compact nature of the PHL layer, which forms a highly continuous surface coverage and penetrates the bulk of LCO. It also prevents side reactions between the charged LCO surface and electrolyte, leading to enhanced structural stability in LCO. Xie et al.56 reported the synthesis of an LiCoO2 cathode by modifying it with chemically inert and ionically conductive LiAlO2 interfacial layers. This conductive layer provides a path for the diffusion of lithium and also prevents interfacial reactions, as evidenced by Raman and impedance spectroscopy investigations. A capacity value close to 200 mA h g⁻¹ was achieved for the LiCoO2 electrodes with commercial-level loading densities, cycled at the cut-off potential of 4.6 V versus Li⁺/Li for 50 stable cycles. This represents a 40% capacity gain with respect to the values obtained for the commercial samples cycled at the cut-off potential of 4.2 V versus Li⁺/Li.

2.1.2 Lithium manganese oxide (LiMn₂O₄). Lithium manganese oxide (LiMn₂O₄) has been considered a superior cathode material due to its low cost and high voltage of 4 V compared to that of Li⁺/Li.⁵⁷ One drawback of LiMn₂O₄ is the capacity fading due to the concentration of Mn. Disbanding of Mn leads to the degradation of the overall active material, resulting in an increase in the internal resistance owing to Mn²⁺ deposition on the anode. 58 Various strategies have been adopted to enhance the cyclic stability by eliminating the capacity fading issue.⁵⁹ Selvamani et al.60 prepared a core-shell-type spinel LiMn₂O₄/ carbon composite via the mechanofusion method (dry particle coating) with a highly uniform coating.

The surface-engineered core-shell-like material demonstrated an excellent retention rate and cycling stability compared to pristine LMO. This enhancement was due to the increase in intrinsic conductivity and easy electrolyte access. For the full cell, the core-shell material exhibited 70% capacity retention, whereas the pristine material retained only 53% capacity after 1000 cycles at 0.1 A g⁻¹. Abbas et al. 61 examined the electrochemical performance of silver-modified LiMn₂O₄ cathode materials and the influence of the calcination atmosphere (vacuum and air). It was concluded that ~ 3 wt% Ag coating is effective to minimize the drawbacks of the spinel LiMn₂O₄ (Mn dissolution and cycling instability). The Ag/ LMO(v) electrode showed high capacity retention and good cyclability at the C/2 rate. Lee et al.62 synthesized a novel $LiMn_2O_4$ heterostructure with epitaxially grown layered $(R\bar{3}m)$ surface phase. No defect was observed at the interface between the host spinel and layered surface phase, which provided an efficient path for ionic and electronic mobilities. The heterostructure LiMn₂O₄ phase exhibited a discharge capacity of 123 mA h g^{-1} and retained 85% of its initial capacity after 100 cycles (at 60 °C). Zhu et al. 63 reported the synthesis of Al₂O₃- and PPy-coated LiMn₂O₄ (PPy/Al₂O₃/LMO) via the sol-gel method, followed by oxidative chemical polymerization. The discharge capacity of PPy/Al2O3/LMO was reaching a value of 121.73 mA h g^{-1} at a rate of 1C. A high retention of around 95.81% was observed even after 100 charge/discharge cycles.

2.1.3 Lithium iron phosphate (LiFePO₄). LiFePO₄ emerged as an alternative to the LiCoO₂ and LiMn₂O₄ cathode materials and has attracted the attention from researchers due to its lowcost and high capacity, which was first proposed by Padhi et al. 64 However, it has the drawback of poor electronic conductivity, which can be easily eliminated by adopting different strategies such as coating. Lithium iron phosphate batteries generally use phosphate as the cathode material. Li-Iron phosphate batteries exhibit the benefit of resistance properties, which enhance their safety and thermal stability, while maintaining other advantages at the same level, including high durability and long cycle life. The fully charged batteries can be stored with little change to the total lifespan of the battery charge. Li-Phosphate batteries are often the most cost-effective options with a long life cycle. 65,66 However, the lower voltage of Li-phosphate batteries means that they have less energy than other types of lithium batteries, and thus exhibit a lower temperature-based performance. These batteries are often used in electric motorcycles and other applications due to their long life cycles and safety. According to their battery space, electric cars also use these batteries.

LiFePO₄ belongs to the olivine family of lithium orthophosphates and has an orthorhombic lattice structure (space group *Pnma*), ^{64,67} with the lattice parameters of a = 10.33 Å, b = 6.01 Å, c = 6.04.69 Å and $V = 291.2 \text{ A}^3$. Its structure consists of corner-shared FeO₆ octahedra and edge-shared LiO₆ octahedra, running parallel to the b-axis, which are linked by PO₄ tetrahedra. In this structure, the Fe atoms occupy the octahedral (4c) sites (dark shading), the P atoms occupy the tetrahedral (4c) sites (light shading), and the Li ions (small circles) occupy octahedral (4a) sites.⁶⁸

Li et al. 69 prepared LiFePO₄/graphite composites, which demonstrated a high reversible capacity (160 mA h g⁻¹ under 0.2C), ultrahigh rate capability (107 mA h g⁻¹ under 60C), and outstanding cycle performance (>95% reversible capacity retention over 2000 cycles). The high volumetric energy density of 427 W h L⁻¹ under 60C was achieved. Wang et al.⁷⁰ synthesized lithium iron phosphate (LFP) with Y-F co-doping. It was observed that the electronic conductivity increased upon doping with F owing to the rearrangement of the PO₄³⁺ electron cloud. Doping of Y reduced the space resistance of Li-ion owing to the introduction of Li⁺ vacancies. The XRD analysis confirmed that Y and F doping led to weakening of the Li-O bond and widening of the lithium-ion diffusion tunnel. The prepared cathode showed a discharge-specific capacity of 135.8 mA h g⁻¹ at 10C and a discharge-specific capacity of 148.6 mA h g⁻¹ without attenuation after 700 cycles at 5C.

Hsieh et al. 71 examined the effect of the carbon layer on the cell performance of LiFePO4 (LFP). The carbon content on the surface of LFP powder was tuned via the addition of glucose. The moderate carbon layer-coated cathode exhibited a discharge capacity of ~ 161.5 mA h g⁻¹ at 0.1C and ~ 99.6 mA h g⁻¹ at 10C. However, at a higher content of glucose, a slow diffusion rate (D_{Li}) and high equivalent series resistance (R_{ES}) were observed due to the formation of inter-grain LFP aggregates. The highest specific energy and specific power densities were observed to be 400 W h kg⁻¹ and 1200 W kg⁻¹, respectively. Motivated by the theoretical calculation, Gao et al.72 reported the synthesis of an Ru-doped LiFe_{1-x}Ru_xPO₄/C cathode through the sol-gel method. The sample designated as LFP-1 (x = 0.01) delivered excellent specific capacities of 162.6 and 110.6 mA h g⁻¹ under 0.1 and 10C conditions, respectively. The capacity retention was 95.6% after 300 cycles at 5C. Liu et al. 73 prepared $\text{Li}_{1-X}\text{Na}_X\text{FePO}_4$ (X = 0, 0.01 or 0.05) composite cathode materials via the simple solvothermal method. The Li_{0.99}Na_{0.01}FePO₄ cathode showed an excellent rate capacity (86.7% after 500 cycles at 10C) and cycle stability.

2.1.4 Lithium nickel manganese cobalt (Li-NMC) oxide. Lithium-manganese cobalt oxide (Li-NMC) batteries are made of several materials that are common in other lithium-iron (Li-Fe) batteries. Li-Fe batteries can have either high specific energy or high specific power. This type of battery is most commonly used in power tools and powertrains for vehicles. The cathode combination ratio is usually one-third nickel, one-third manganese, and one-third cobalt (Ni:Mn:Co = 1/3:1/3:1/3), and thus the raw material cost is lower than the cobalt-based batteries.74,75

Ren et al.76 prepared a lithium nickel manganese cobalt oxide (NMC) cathode, which was designated as LiNi_{0.33}Mn_{0.33}-Co_{0.33}O₂ (NMC-111). This showed a superior electrochemical performance compared to the commercial NMC-111 (c-NMC), with discharge capacities of 138 and 131 mA h g⁻¹ at high current rates of 20 and 30C, respectively. Even at both room temperature and at 50 °C, the cyclic stability was better. Reissing et al.77 investigated the combination of Zr as a common dopant in commercial materials with effective Li₂WO₄ and WO₃ coatings in nickel-cobalt-manganese (NCM)||graphite cells. It was concluded that the Zr4+ dopant diffused to the

surface during annealing, improving the electrochemical performance compared to the samples without additional coatings. The pristine NCM graphite cell displayed an initial discharge capacity of 180 mA h g^{-1} at 0.1C and 173 mA h g^{-1} at 0.33C in the cell voltage window of 2.8-4.2 V, while its end of life was reached after approximately 343 cycles with an average Coulombic efficiency (CE) of 99.8%. The WO₃-coated sample showed a similar initial discharge capacity and enhanced the life cycle up to > 700 cycles.

2.1.5 Lithium nickel cobalt aluminum (NCA) oxide. Lithium nickel cobalt aluminum (NCA) oxide batteries, named NCA batteries, are very important for electric powertrains and grid storages. NCA batteries are not common in the consumer industry, but they are a promising contender for the automotive industry. However, although NCA is a high-energy density battery with a good life span/stability, it is not safe enough and very expensive. The Argonne National Laboratory (ANL) investigated the potential of NCA batteries and their possible material issues. Assuming the market share of electric vehicles and the demand for lithium batteries in the US, the consistent use of NCA batteries may skyrocket. According to the Battery Report 2020, the US battery demand surpasses current world production trends. However, NCA batteries must be accompanied with safety measures in cars that monitor their performance and behavior to keep drivers secure. 78,79

Cao et al.80 reported the synthesis of an LiNi_{0.88}-Co_{0.09}Al_{0.03}O₂ cathode via solvothermal and co-precipitation method. The discharge capacity of the solvothermal prepared cathode was observed to be 154.6 mA h g⁻¹ at 55 °C after 100 cycles with the capacity retention of 75.93%. In contrast, the cathode prepared via the co-precipitation method delivered only 130.3 mA h g⁻¹ after 100 cycles, with a capacity retention of 63.31%. Xiao et al.81 reported the synthesis of an LiNi_{0.88}-Co_{0.09}Al_{0.03}O₂ cathode with the addition of trimethyl borate (TMB) in the commercial electrolyte, which enhanced the interfacial stability. The LiNi_{0.88}Co_{0.09}Al_{0.03}O₂ electrode with 10% TMB-containing electrolyte could achieve a capacity retention of up to 82% after 300 cycles at 1C rate (1C = 200 mA h g^{-1}). Zhang et al. 82 reported the synthesis of a high-nickel-content NCA (LiNi_{0.88}Co_{0.09}Al_{0.03}) cathode material with a non-spherical morphology, which showed a good cycle performance (at both 25 °C and 45 °C), and also enhanced structural stability with suppressed phase transition from H₂ to H₃. The capacity retention of the pouch-type cells with non-spherical NCA as the cathode was greater than 91% after 1000 cycles.

2.1.6 Lithium titanate (Li-titanate). The lithium titanate (Li-titanate) battery class can be employed in various applications. The main advantage of Li-titanate batteries is to enhance the fast recharge time due to advanced nanotechnology. Currently, manufacturers of electric automobiles are using Lititanate batteries and further investigating the use of these types of batteries for electric buses for public transportation. However, these batteries have a lower inherent voltage or a lower energy density than lithium-ion batteries, which can raise issues upon powering. Nevertheless, the density of Li-titanate batteries is still higher than that of non-lithium-ion batteries.

Table 4 The comparison of electrochemical properties and price for cathode materials⁸⁸

Material	${ m LiFePO_4}$	${\rm LiMn_2O_4}$	${\rm LiCoO_2}$	$\text{Li}(\text{Ni}_x\text{Co}_y\text{Mn}_z)\text{O}_2$	$\mathrm{LiNi_{0.8}Co_{0.15}Al_{0.05}O_{2}}$
Average voltage (V)	3.4	3.8	3.7	3.6	3.6
Specific capacity (mA h g ⁻¹)	130-140	100-120	135-150	160-220	180-200
Cycle number	2000-5000	500-2000	500-1000	800-2000	800-2000
Safety performance	Excellent	Good	Poor	Poor	Poor
Price (thousand \$ ton ⁻¹)	7.4-14.7	4.4-8.8	50-57	22-29	26-35

These batteries can be used for military and aerospace technologies together with energy storage for energy conversion systems such as wind and solar to create smart grids. The battery space suggests that these batteries can also be used in system-critical backups for power systems. The electrochemical properties of important cathode materials are summarized in Table 4. The structural design of these cathodes play a major role in the efficiency of batteries. Many researchers have significantly focused on improving the remarkable features of these batteries. Carbon-based nanomaterials, such as graphene, carbon nanotubes, and graphene oxide, have shown great potential as cathode materials in energy storage devices. Significantly focused on the shown great potential as cathode materials in energy storage devices.

The limitation of traditional cathodes (layered, spinel, and olivine) has limited the capacity mismatch with that of silicon anodes (~ 1000 mA h g⁻¹). Thus, to fill this gap, Li-rich oxide (LRO) materials have emerged as a potential alternative to replace future cathodes due to their high theoretical capacity ($\sim 300 \text{ mA h g}^{-1}$) and high specific energy ($\sim 900 \text{ W h kg}^{-1}$). For LROs, the Li/TM ratio is greater than 1 (0 < x < 1), which is commonly referred to as Li_{1+x}TM_{1-x}O₂ (e.g., Li₂MnO₃ and Li₂RuO₃).^{89,90} The research on LRO materials started in the early 1960s with the development of Li₂SnO₃ and Li₂MnO₃. 91,92 Two remarkable developments were made by Thackeray's group,93 who synthesized Li_{1.09}Mn_{0.91}O₂ (1991), and Dahn's group, who synthesized $\text{Li}[\text{Ni}_x\text{Li}(\frac{1}{3-2x/3})\text{Mn}(\frac{2}{3-x/3})]\text{O}_2^{-94}$ in 2001. Two types of Li-rich materials are (i) layered lithiumrich oxides (LLROs), which exhibit a high working potential, low cost, and desirable cyclic stability, and (ii) cation disordered lithium-rich oxides (DLROs), which exhibit structural stability, high specific capacity, and poor cycling stability. Three major challenges with the precision use of LROs can be summarized as follows: (1) they regulate the oxygen loss/oxygen vacancy, where the excessive oxygen vacancies may shrink the cell volume, introduce stacking faults, cation mixing, and an undesirable new phase, which collectively decrease the electrochemical performance. 95-97 (2) To obtain the deep insights into the bulk and surface structural evolutions during cycling, the structure transformation in LRO for the initial and final process showed a lower coulombic efficiency and interface breakdown. 96 (3) To understand the relationship between the structure/chargetransfer mechanisms and electrochemical performance of LROs, they can be analysed using some advanced techniques (X-ray diffraction, neutron diffraction, X-ray and neutron pair distribution function (xPDF and nPDF), EXAFS, Raman spectroscopy, and Mössbauer spectroscopy). The performance of Lirich cathode materials can be improved by five strategies, as follows: (i) elemental doping, (ii) controlling the morphology

(iii) tuning the structure, (iv) optimisation of composition, and (v) electrolyte additives. 98 Juan et al. 99 prepared sulphur doped Li-rich cathode materials (LNMOS) via a co-precipitation method. The XRD-analysis confirmed the presence of the sulfur (S) dopant, which reduced the mixing degree of cations in the LNMOS and increased the ordered arrangement of the layered structure. The S-doped lithium-rich material released a higher initial efficiency of 96.06% (87.63% for LNMO), a specific capacity of 293.3 mA h g^{-1} (243.3 mA h g^{-1} for LNMO), and better cycling stability and rate performance (a capacity of 117 mA h g^{-1} , maintained at a current density of 5C). Cui et al. 99 prepared the stable O₂-structured Li_{1.2}Ni_{0.13}-Co_{0.13}Mn_{0.54}O₂ (O₂-LR-NCM) cathode, which demonstrated a high coulombic efficiency (CE) >99.82% and high reversible capacity of 278 mA h g⁻¹. After 100 cycles, 83.3% capacity was retained by this optimised cathode material.

2.1.7 Anode materials of lithium-ion batteries. Despite the investigation on cathode materials, the anode also plays an effective role in the efficient operation of LIBs. 100,101 The principal characteristics of the anode influence the cell performance parameters, such as its rate capability, cycle life, energy density, and power density. 102 Before the fabrication of batteries, these characteristic parameters, such as conductivity, reducing power, structural defects, chemical/mechanical/thermal stability, and morphology, need to be examined to understand how they alter the operational behavior of the cells. These parameters need to be optimised to achieve a better electrode performance, simultaneously focusing on improving the overall cell performance. The important anode materials have been developed from carbon-based alloys, transition metal oxides, and silicon-based composites. The advantages and disadvantages of important anode materials are summarized in Table 5.

Recently, Eftekhari *et al.*¹⁰³ categorized anode materials in four classes based on the particular voltage range of their operation. Firstly, for low-voltage materials (group IV and V elements), the majority of the delithiation capacity can be achieved under 1.0 V *versus* Li/Li⁺, while secondly for mid-voltage materials (transition metal oxides and chalcogenides), the majority of the delithiation capacity can be achieved in the range of 1.0–2.0 V. The third type, *i.e.*, high-voltage operating materials, the majority of the delithiation capacity occurs over 2.0 V. The fourth category covers nanostructured and mixed valence-based material, where their potential window varies in the range of 0–3.0 V and includes a wide variety of materials with nanostructured and mixed valences (Fig. 6).

2.1.8 Nanostructured Al anode. For rechargeable batteries, lithium metal anodes (negative electrodes) can provide both

Advantages and disadvantages of various anode materials

Anode materials	Advantages	Disadvantages
Carbon	High electronic conductivity	Low specific capacity
	Nice hierarchical structure	Low rate capacity
	Abundant and low-cost resources	Safety issues
Alloys	High specific capacity (400–2300 mA h g ⁻¹)	Low electronic conductivity
·	Good security	Large volume change (100%)
Transition metal oxides	High specific capacity (600–1000 mA h g^{-1})	Low coulombic efficiency
	Nice stability	Large potential hysteresis
Silicon	Highest specific capacity (3579 mA h g ⁻¹)	Large volume change (300%)
	Rich, low-cost, clean resources	<i>3 3</i> . ()

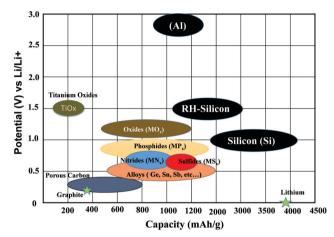


Fig. 6 Comparison chart for potential versus specific capacity of various anode materials

high voltage and excellent capacity, resulting in an extraordinarily high energy density. Aluminum (Al) has been considered as an anode electrode of LIBs since Hamon et al. tested a non-carbonaceous anode material, for example, Al thin film with a thickness of 0.5 µm at room temperature, and obtained a specific capacity above >1000 mA h g⁻¹.³⁷ Nanostructured aluminum thin films (Al nanorod) showed a consistent specific capacity, which have been deliberated for possible application in next-generation LIBs. 38-40 Nanostructured Al thin films can be grown via physical and chemical synthetic methods. The specific capacity and Coulombic efficiency of pure nanostructured Al and Al-alloy thin films are summarized in Table 6.104-116

2.1.9 Si and Si-based composite anode electrodes. Silicon (Si) is one of the most exciting and promising alternative anode materials to replace the most commonly used graphite anode electrodes because it possesses the highest theoretical specific capacity (4200 mA h g⁻¹). Among the metals and metal-oxidetype anodes, Si-based batteries have ten-times higher specific capacity than the theoretical specific capacity of graphite anodes (372 mA h g⁻¹). Silicon is the second most abundant element in the Earth by mass (25.7%) but very rarely occurs in nature as the pure free element. 117 Silicon is one of the principal components of most semiconductor devices such as integrated circuits (ICs) and microchips. 42,43,118-120 However, two major scientific and technical challenges have hindered their practical applications in energy storage devices. Firstly, due to the alloying mechanism, a large number of lithium atoms are inserted into Si, breaking the chemical bonds between Si atoms. The structural pulverization induced by a large volume change (~300% at room temperature) during Li insertion and extraction leads to the loss of electrical contact between the active material and the current collector, resulting in capacity fading and shortening of the battery lifetime. 41,45 Secondly, due to the volume expansion and shrinkage, a thick solid-electrolyte interphase (SEI) layer can be formed, which is derived from the irreversible side reactions with the organic electrolyte. 47-49 This causes a degradation in the battery performance due to the consumption of electrolyte and lithium ions, the electrically insulating nature, and relatively long

Table 6 The specific capacity and other parameters (current, voltage, scanning rates and coulombic efficiency) of Al and Al-based anode electrodes

S. no.	Materials	Current (mA g ⁻¹)	Voltage (V)	Capacity (mA h g ⁻¹)	Scanning rate (mV s^{-1})	Coulombic efficiency (%)	Ref.
1	Al		0.01-1.2	890	10		104
	Al nanorods	458	1.35	324	20	91.5	105
2	Al nanorod	700 (0.5C)	0.01-3	1243	0.1		106
3	Al nanorod	700	0.01-3	1293		91	107
4	Fe ₂ Al ₅		0.01-3	485	1	30	108
5	Al-Sn Composite	$0.1~\mathrm{mA~cm}^{-2}$	0.05 - 1.25	972.8	0.1-0.5	81	109
6	Al-Sn composite	$0.1 - 04 \text{ mA cm}^{-2}$	0.05 - 1.25	752	0.1-0.5	83	110
7	Al-Fe ₃ O ₄ -rGO	C/10-10C	0.005-3	717.4		99.17	111
8	Al foil	182	-0.02 to $+0.55$	967		92.6	112
9	Si-Al	$0.05 \; \mathrm{mA} \; \mathrm{cm}^{-2}$	0.005-2	3348		93.6	113
10	CNS/Si/Al ₂ O ₃	1 A g^{-1}	0.01-1	1560	1	84.8	114
11	Al nanorod	1C	0.01-1	977	1		115
12	Si-Al thin film	0.5C	0-1.5	2257.8	0.05	85.9	116

Table 7 The specific capacity of Si and Si-based anodes of LIBs

S. no.	Materials	Current (mA g ⁻¹)	Voltage (V)	Capacity (mA h g ⁻¹)	Scanning rate (mV s ⁻¹)	Coulombic efficiency (%)	Ref.
1	C-Si _{RH}	0.1-3C	0.01-1	1554	_	99.7	128
2	Si-G	200-2000	0.01 - 1.5	1000	0.5	70	129
3	Si	C/50	0.01-1	2790	0.02	99.3	130
4	Si	100	0.01-1.2	3420	_	71.8	131

lithium diffusion length through the thick SEI.²⁷ Thus, to make silicon a good anode candidate for LIBs, two major issues must be settled, i.e., minimizing the degradation of mechanical integrity and maintaining the stability of the SEI. Nowadays, the extracted Si from rice husk (RH) appears to be the most promising anode material for LIBs. 114,121-127 The nano-Si has attracted considerable attention as a promising anode material in next-generation Li-ion batteries for electric vehicles and portable electronics. The nanostructured Si (n-Si) and Si-based anodes are summarized in Table 7.128-131

However, the major problem in utilizing Si and Si-based anodes is their poor conductivity and very large volume change (about 310% for Li₄Si) during the lithium alloying/dealloying (or lithiation/delithiation) process, which cause mechanical failure of the active material. Thus, it results in pulverization and poor cycle performance of the electrode. 113 The specific capacity, coulombic efficiency, and scanning rates are summarized in Table 8. 132-180

2.1.10 Nanostructured carbon/graphene anode. Dispersing Si in a carbon matrix has been well-developed in which the carbonaceous materials can buffer the volume change and improve the electrical conductivity of Si active materials. Different types of carbon materials, including amorphous carbon (a-C), graphite, carbon nanotubes (CNTs), carbon nanofibers, 102,181 have been investigated to improve the cycling stability of Si active materials. The specific capacity, Coulombic efficiency, and scanning rates of C-based anode electrodes are summarized in Table 9.182-206

2.1.11 Nanostructured tin anode. Due to the high theoretical capacity (994 mA h g⁻¹) of tin (Sn), it is a spectacular material for the fabrication of anode electrodes. Sn-based anode electrodes of LIBs, such as SnO2, SnS2, and SnSe2, have been investigated.²⁰⁷ Several intermetallics of different compositions, including Li₂₂Sn₅, Li₇Sn₂, Li₃Sn, Li₅Sn, LiSn, and Li₂Sn₅, are present in the equilibrium phase diagram of Li-Sn. These intermetallics can be produced via the electrochemical lithiation of a tin electrode immersed in an Li-ion containing an electrolyte such as LiClO₄.²⁰⁸

The pulverization and disintegration of the active materials from the current collector increase by Li intercalation/deintercalation, leading to the formation of an unstable solid-electrolyte interphase (SEI) and severe capacity fading. Besides, one of the major obstacles of Sn-based anodes is the poor electrical conductivity of SnO2 nanostructures, which hinders the reaction with Li during the discharge. Several methods, such as, nano-scaled structure, doping, and core-shell structures, have been reported to overcome these limitations.²⁰⁹ Table 10 highlights the tin-based anode electrodes for charging and discharging parameters. 210-215

2.1.12 Methods for enhancing the electrode performance. With the advancement of electrode materials, it has been concluded that the surface, interface and internal chemistry of electrode materials play an essential role in the electrochemical performance of batteries. Various strategies have been investigated by researchers to improve the specific capacity and energy density of the batteries by tuning the cathode and anode materials. This also aims to reduce the gap between the theoretical and practical specific capacity of the electrode material. Surface modification, doping, and controlled morphology variation are the most important strategies considered for the effective alteration of the electrode efficiency.

2.1.13 Surface modification. Surface modification or coating is an effective approach to minimize the possibility of side reactions and improve the stability of electrode materials. The modified electrode surface prevents direct contact with the electrolyte, which eliminates the possibility of electrode degradation by reducing the phase transition tendency. 216 This can be achieved in two ways, as follows: (a) in situ and (b) ex situ. It is very important to mention here that that it is necessary to first optimize the suitable conditions for surface modification via coating. Generally, to achieve the optimum electrode performance, some key points need to be considered during modification. Firstly, the coating should be uniform and thin as possible to minimize the overall weight of the electrode. Secondly, the materials for surface modification must be stable and have high electronic/ionic conductivity. Finally, the modified material must be mechanically stable to constrain any degradation (e.g., cation dissolution in the electrolyte) during cell operation (volume change may occur). 217,218

LiNi_{0.5}Co_{0.2}Mn_{0.3}O₂ (NCM523) is an interesting cathode due to its high discharge capacity and good cyclic stability. However, its safety issue and poor thermal stability are recognized as major drawbacks. Recently, Chen et al. 219 examined the performance of NCM523 by modifying the surface of the electrode with Li₃PO₄ to eliminate the performance degradation. Fig. 7(a) shows the modification approach and role of coating in ion migration. The XRD analysis suggests that the coating did not affect the structure of bare NCM523. The FE-SEM and EDS analysis confirmed the formation of a coreshell structure and encapsulation of the bare cathode. The impedance analysis after 200 cycles showed the lower charge transfer resistance value for the coated NCM523 (156.5 Ω) compared to that of the bare NCM523 (340.1 Ω). Compared to the pristine cathode (D_{Li}^+ = 7.29 × 10⁻¹³ cm² s⁻¹), the diffusion coefficient was enhanced after the coating (D_{Li}^{+} = 1.43 \times 10⁻¹² cm² s⁻¹). The discharge capacity, rate capability, and coulombic efficiency improved for the coated electrode (NCM523).

Table 8 The battery parameters (specific capacity, coulombic efficiency, and scanning rates) of Si and Si-based nanocomposite alloys for anodes

s. no. b. Materials Current (mA g ⁻¹) Voltage (W) Capacity (mA h g ⁻¹) Scanning rate (mV s ⁻¹) Coulombic efficiency (%) Ref. 1 a COSi 100 A cm ⁻² (C2) 0.20-1.2 2500 — 9.5 132 3 a SISIO _C /CIC 15-60C 0-1.5 3107 — 83 133 4 a SIG 100-140 0-1.5 3107 — 92.5 133 5 a SI thin film 0.025C 0-1.5 3134 0.05 87.1 136 6 3 D-SiC nanowire 0-1.4 g ⁻¹ 1.1-2 2300 — 91 137 7 Buddle-Si hanorod 410 0-1.5 180 — 99 149 10 Si SiGo, C 100 0-1.5 180 — 99 149 11 Si C 100 0-1.5 780 0.5 — 99 141 12 Si C 100 0-1.5 780 0.5 — 99 141 14		31	1 3.		<u>, </u>	•		
2 SiC 15-60C 0-1.5 3107 — 83 1313 a a-SiGO (C/C) 100-140 0.01-1.5 2810 — 99.2 1345 a a-SiG (In thill) 0.01-1.5 2858 — 92.5 135 5 a-Si thin film 0.025C 0-1.5 2134 0.05 87.1 135 6 3D-Si/C nanowire 0.4 Ag ¹ 0.1-2 2300 — 91 137 7 Buddles inanorod 410 0-2 2411 — 94 133 8 C-Si 200 0-1.5 1280 — 99 139 9 SiSiOs/C 100 0-1.5 781 0.5 — 90 141 10 Si Caratrix 0.2C 0.01-3 2950 — 99.6 143 14 Hollow prous-SiO ₂ 100 0-1 300 — 99.6 143 15 Si W-C <th>S. no.</th> <th>Materials</th> <th></th> <th>- , ,</th> <th>Capacity (mA h g⁻¹</th> <th>) Scanning rate (mV s⁻¹)</th> <th>Coulombic efficiency (%)</th> <th>Ref.</th>	S. no.	Materials		- , ,	Capacity (mA h g ⁻¹) Scanning rate (mV s ⁻¹)	Coulombic efficiency (%)	Ref.
3 s SiSiSiO _c (CrC 100 100-140 0.1.5 810 — 92.2 134 4 a.SIG 100-140 0.025C 0-1.5 3134 0.05 87.1 136 6 3DSI(Cr) annowire 0.4 A g ⁻¹ 0.1-2 3000 — 91 137 136 6 3DSI(Cr) annowire 0.4 A g ⁻¹ 0.1-2 3000 — 91 137 136 8 5 5 8 5 5 5 100 0.0 1.5 1280 — 99 138 9 SiSiO _s (CrC 100 0.1-1.5 786 0.5 — 99 138 9 138 9 SiSiO _s (CrC 100 0.01-1.5 786 0.5 — 90 141 11 11 SiC 100 0.1-1.5 786 0.5 — 90 141 11 11 SiC 100 0.1-1.5 786 0.5 — 90 141 11 11 SiC 100 0.1-1.5 786 0.5 — 90 141 11 11 SiC 100 0.1-1.5 781 0.05 — 91 0.05 0.1 141 11 11 SiC 100 0.1-1.5 781 0.05 — 91 0.05 0.1 141 11 SiC 100 0.1-1.5 781 0.05 — 91 0.05 0.1 141 11 SiC 100 0.1-1.5 781 0.05 — 91 0.05 0.1 141 11 11 SiC 100 0.1-2 3193 1 1 90 0.1 141 11 11 SiC 100 0.1-2 3193 1 1 90 0.1 141 11 11 SiC 100 0.1-2 3193 1 1 90 0.1 141 11 11 11 11 11 11 11 11 11 11 11 1	1	a-C/Si	$100 \text{ A cm}^{-2} (\text{C/2})$	0.02 - 1.2		_	99.5	132
44 aSiG 100-140 0.01-1.5 285R — 92.5 1315 6 a D-Si/C nanowire 0.4 A g ⁻¹ 0.1-2 2300 — 91 137 7 Buddle Si nanorod 410 0-2 2411 — 94 138 8 C-Si 200 0-1.5 1280 — 99 139 9 SiSiOyC 100 0.01-1.5 786 0.5 — 90 10 Si 0.4 mA cm ⁻² 0-1.5 781 0.05 61.8 141 11 Si 0.4 mA cm ⁻² 0-1.5 781 0.05 61.8 142 12 Si-C matrix 0.2C 0.01-3 2950 — 99.6 143 13 Si NWC C/20 0.01-2 3103 1 90 144 14 Hollow porous -SiO ₂ 100 0.01-2 3103 1 73 145 15 Si NWC C/10 <td>2</td> <td></td> <td>15-60C</td> <td>0-1.5</td> <td></td> <td>_</td> <td>83</td> <td>133</td>	2		15-60C	0-1.5		_	83	133
5 a Ssi thin film 0.025C 0-1.5 3134 0.05 87.1 136 6 a SbSi(Or annowire 0.4 A g^-1 0.1-2 2300 — 94 138 8 C-S annord 410 0-1.5 1280 — 99 139 9 Si/SiO ₂ /C 100 0.01-1.5 786 0.5 — 140 11 Si/SiO ₂ /C 100 0.01-1.5 786 0.5 — 140 11 Si/C 100 0-1.5 781 0.05 61.8 142 11 Si/C 100 0-1.5 781 0.05 61.8 142 13 Si/C 100 0-3 919 0.1 79 90 144 15 Si/WC C/10 0.01-2 2000 — 96 146 15 Si/WC C/10 0.01-2 2000 — 99 144 15 Si/We C/10	3	a-Si/SiO _x /Cr/C	100	0-1.5	810	_	99.2	134
65 DSDI/C nanowire 0.4 A g ⁻¹ 0.1–2 2300 — 99 138 86 C-SI 200 0-1,5 1280 — 99 139 95 SiSO _O C 100 0.01-1.5 786 0.5 — 140 10 Si 0.4 m A cm ⁻² 0-1 3900 0.5 90 141 11 SiC 10 0.4 m A cm ⁻² 0-1.5 781 0.5 90 141 12 Si-C matrix 0.2C 0.01-3 2950 — 99.6 143 13 Si NW C2O 0.01-2 3193 1 90 144 14 Hellow porous -SiO ₂ 100 0.3 919 0.1 73 916 143 15 ISi allow 50 0.01-2 3100 — 96 146 16 Li-Si allow 50 0.01-1 300 — 99.7 148 17	4	a-SiG	100-140	0.01 - 1.5	2858	_	92.5	135
7 Buddle-Si nanorod 410 0-2 2411 — 94 138 8 C-Si (200) 0-1-5 1280 — 99 139 9 Si/SiOyC 100 0.01-1.5 786 0.5 — 140 11 Si (200) 100 0-1.5 781 0.05 61.8 142 12 Si-Cmatrix 0.20 0.01-3 2950 — 99.6 143 13 Si NW C/20 0.01-2 3193 1 90 144 14 Hollow prous -SiO₂ 100 0.3 919 0.1 73 145 15 Si NW-C C/10 0.01-2 2000 — 93 147 16 Li-Si alloy 50 0.01-1 3000 — — 93 147 18 Mesoporous Si 0.1 4 g⁻¹ 0.05-1.5 750 — 99.7 149 18 Pas certa 0.01-1.5	5	a-Si thin film		0-1.5	3134	0.05	87.1	136
7 Buddle-Si nanorod 410 0-2 2411 — 94 138 8 C-Si (200) 0-1-5 1280 — 99 139 9 Si/SiOyC 100 0.01-1.5 786 0.5 — 140 11 Si (200) 100 0-1.5 781 0.05 61.8 142 12 Si-Cmatrix 0.20 0.01-3 2950 — 99.6 143 13 Si NW C/20 0.01-2 3193 1 90 144 14 Hollow prous -SiO₂ 100 0.3 919 0.1 73 145 15 Si NW-C C/10 0.01-2 2000 — 93 147 16 Li-Si alloy 50 0.01-1 3000 — — 93 147 18 Mesoporous Si 0.1 4 g⁻¹ 0.05-1.5 750 — 99.7 149 18 Pas certa 0.01-1.5	6	3D-Si/C nanowire	$0.4 \; { m A g^{-1}}$	0.1-2	2300	_	91	137
9 SiSiO _O C 100 0.01 - 1.5 786 0.5 90 141 11 SiC 100 0-1.5 781 0.05 61.8 142 12 Si-Cmatrix 0.2C 0.01-3 2950 - 996 143 13 Si NW C/2O 0.01-2 3193 1 90 144 14 Hollow porous SiO ₂ 100 0-3 319 0.1 73 145 16 Li-Si alloy 50 0.01-15 1000 - 93 147 16 Mesoporous SiO ₂ 100 0.01-15 3000 - 93 147 18 Mesoporous SiO ₂ 100 0.01-1 3000 - 99.7 149 19 P-Si NP 0.1-1,5C -3 2113 - 61.1 150 20 Si spheres C/2O 0.01-2 3105 0.2 100 99.1 152 21 Macos	7	Buddle-Si nanorod		0-2	2411	_	94	138
10 Si 0.4 mA cm²² 0-1.5 3900 0.5 90 141 11 SiC 100 0-1.5 781 0.05 61.8 142 12 Si-C matrix 0.2C 0.01-3 2950 — 99.6 143 13 Si NW C/20 0.01-2 3193 1 99 144 14 Hollow porous -SiO₂ 100 0.3 919 0.1 73 145 15 Si NW-C C/10 0.01-1.5 1000 — 93 147 16 Li-Si alloy 50 0.01-1.5 1000 — 99.7 149 17 Mesoporous SiO₂ 100 0.01-1.5 750 — 99.7 149 19 P-Si NP 0.1-1.5C 0-3 2113 — 61.1 150 21 Nano-Si 2 A g⁻¹ 0.01-2 2305 — 80.3 152 22 SiPANI 2 A g⁻¹	8		200	0-1.5	1280	_	99	139
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	9	Si/SiO ₂ /C		0.01 - 1.5	786	0.5	_	140
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	10		$0.4~\mathrm{mA~cm}^{-2}$	0-1	3900	0.5	90	141
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	11	Si/C		0-1.5	781	0.05	61.8	142
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	12	Si-C matrix	0.2C	0.01 - 3	2950	_	99.6	143
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	13	Si NW	C/20	0.01-2	3193	1	90	144
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	14	Hollow porous -SiO ₂	100	0-3	919	0.1	73	145
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	15	1 2	C/10	0.01-2		_	96	146
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$						_		
18 Mesoporous Si 0.1 A g $^{-1}$ 0.05 - 1.5 750 — 99.7 149 19 P-Si NP 0.1 - 1.5C 0-3 2113 — 61.1 150 20 Si spheres C/20 0.01 - 1 1024 0.02 100 151 21 Nano-Si 2 A g $^{-1}$ 0.01 - 1 1024 0.02 99.1 152 22 Si/PANI 2 A g $^{-1}$ 0.01 - 1 766.6 0.1 72.5 153 23 Si/CNT 100 0.02 - 1.2 2050 — 80.3 154 24 Mesoporous Si 200 0.01 - 3 1038 — 98.4 155 26 Si/PANI 100 0.01 - 1.5 840 0.5 56 157 26 Si/PANI 100 0.01 - 1.5 1947 — 76.1 158 28 Si/PANI 100 0.01 - 1.5 1947 — 76.1 159 29 Si NWs C/10 0.01 - 1.5 1947 — 76.1 159 <td></td> <td>•</td> <td></td> <td></td> <td></td> <td>_</td> <td></td> <td></td>		•				_		
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$			$0.1 \text{ A } \text{ o}^{-1}$			_	99.7	
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$			0.1-1.5C					
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$ \begin{array}{cccccccccccccccccccccccccccccccccccc$			2 A s^{-1}					
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$			$\frac{2 \text{ A g}}{2 \text{ A g}^{-1}}$					
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$			2 A g					
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$ \begin{array}{cccccccccccccccccccccccccccccccccccc$								
$\begin{array}{cccccccccccccccccccccccccccccccccccc$			0.2C					
$\begin{array}{cccccccccccccccccccccccccccccccccccc$			0.2 A g					
$\begin{array}{cccccccccccccccccccccccccccccccccccc$			0.1 A g					
$\begin{array}{cccccccccccccccccccccccccccccccccccc$			1.0 A g					
38 Si-CNT 0.8 A g^{-1} (C/5) $0.01-1$ 1200 43 169 39 Si/rGO-P 50 $0-3$ 1261 0.1 66 170 40 Si-M C 100 $0.01-2$ 1220.9 0.1 56 171 41 Si-Mn/rGO 100 $0.01-3.25$ 600 0.1 97.6 172 42 Si/Cu-Al-Fe 120 $0-1.5$ 836 $ 80.5$ 173 43 SC-Si/G 1.0 A g^{-1} $0.005-1$ 1611 0.1 76.9 174 44 SiO ₂ C/2 $0-3$ 1266 0.1 98.5 175 45 Si-SWNT-Cu $0.1C$ $0.005-3$ 2221 $ 98$ 177 46 Si-CNT C/5 $0.01-1$ 494 $ 98$ 177 47 Tobacco Mosaic Virus (TMV)-Si $1C$ $0-1.5$ 3343 $ 100$ 178 48 Si Np-rGO 0.5 A g^{-1} $0.005-1.5$								
$\begin{array}{cccccccccccccccccccccccccccccccccccc$			0.6 A g (0.2C)			_		
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$						0.1		
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45 Si-SWNT-Cu 0.1C 0.005-3 2221 — 74 176 46 Si-CNT C/5 0.01-1 494 — 98 177 47 Tobacco Mosaic Virus (TMV)-Si 1C 0-1.5 3343 — 100 178 48 Si Np-rGO 0.5 A g ⁻¹ 0.005-1.5 956.7 — 82.8 179 49 PS@C 100 0.05-2 1980 82 180								
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49 PS@C 100 0.05-2 1980 82 180		,				-		
<u>e</u>						_		
50 rGO-porous Si 100 0.01–1.5 815 0.5 96.4 181		<u>C</u>						
	50	rGO-porous Si	100	0.01 - 1.5	815	0.5	96.4	181

The coating of the Li₃PO₄ layer acted as a carpet for Li-ion movement (Fig. 7a).

The Ni_{0.8}Co_{0.1}Mn_{0.1}O₂ (NCM811) cathode is another promising electrode for batteries due to its high capacity. However, its poor thermal stability and tendency to react with moisture pose some challenges that need to be resolved. Becker et al. 220 examined the electrochemical performance of NCM811 with a coating of Li₂WO₄ via the sol-gel method. Li₂WO₄ was chosen due to its high Li⁺ conductivity, non-toxic nature, and desirable thermal stability.²²¹ The increased thermal stability of the coated electrode was analyzed using XRD patterns. A comparison of the capacity retention for the coated and uncoated NCM811 is shown in Fig. 7(b), corresponding to different cyclic conditions (temperature and voltage). The state of health (SOH) of the cell is the ratio of discharge capacity of the actual cycle to the discharge capacity of the fifth cycle at 0.5C. For a SOH of about 80%, the coated electrode-based cell demonstrated an improved performance.

The NCM523 (LiNi_{0.5}Co_{0.2}Mn_{0.3}O₂) cathode is used for battery fabrication due to its low toxicity, cost-effectiveness, good safety, and high capacity.²²² However, this type of electrode exhibits one drawback, it restricts the cyclic stability due to corrosion issues with the electrolyte. To eliminate the abovementioned issue, Wang et al. 223 recently examined an Li2O-B₂O₃-LiBr-coated (~10 nm) electrode to improve the electrochemical performance of NCM523. The discharge capacity of

Table 9 Anode electrodes based on carbon nanocomposite and battery parameters

S. no.	Materials	Current (mA g^{-1})	Voltage (V)	Capacity (mA h g^{-1})	Scanning rate (mV $\rm s^{-1}$)	Coulombic efficiency (%)	Ref.
1	CNT	0.5C	0-3	446		95	182
2	Co ₃ O ₄ /CoO/graphene	21.12	0.005-3	1153.81	0.1	76	183
3	Graphene nanosheet	$0.2~\mathrm{mA~cm^{-2}}$	0.01 - 3.5	672	_	_	184
4	Fe ₂ O ₃ @MWCNTs	100	0-3	515	0.1	95	185
5	Fe ₂ O ₃ /graphene	50	0.001-3	1069	0.1	77.2	186
6	Fe ₂ O ₃ /Fe ₃ C–graphene	0.17C	0.01 - 3	1118	0.5		187
7	Fe ₂ O ₃ -graphene	0.1C	0.05 - 3	1074.9	0.1	65	188
8	Co ₃ O ₄ /graphene	50	0.01 - 3	935	1	98	189
9	Graphene NR/SnO ₂	100	0.01 - 2.5	1130	0.5	98.3	190
10	G-CNT-Fe	100	0-3	1024	0.05	99	191
11	G/C-Si	300	0.02 - 1.2	902		57.3	192
12	G-CoS ₂	100	0.01 - 3	800	0.05	98	193
13	$G-M-SnO_2$	100	0.005 - 3	1354	0.1	98	194
14	GO/G/CNT	0.5C	0.01-3	1172.5	0.1	58	195
15	MnO/RGO	0.16 A g^{-1}	0.01-3	855	0.1	69.7	196
16	CNT-Si	C/10	0.01-1	1711	_	98	197
17	C-Graphite	0.1-3C	0-2.5	358	_	81	198
18	C/Si	500	0.02 - 1.5	1018	_	98	199
19	Nitrogen-doped-graphene	100	0.01 - 3	2132	0.1	99.2	200
20	nC-pSiMPs	C/4	0.01-1	1500	_	78	201
21	p-CNTs@CFO	0.1 A g^{-1}	0.01 - 3	1077		_	202
22	Porous-G–C	100	0-3	722	0.5	98	203
23	N–C spheres	50	0.005-3	816	0.2	_	204
24	rGO/BN	100	0-3	278	0.1	100	205
25	Li ₂ S-G	0.1C	0-3.5	791	0.1	_	206

Table 10 Charging and discharging parameters of tin-based anode electrodes

S. no.	Materials	Current (mA g^{-1})	Voltage (V)	Capacity (mA h g ⁻¹)	Scanning rate (mV s ⁻¹)	Coulombic efficiency (%)	Ref.
1	SnO ₂ /N-G	$0.5~{\rm A~g^{-1}}$	0.005-3	1352	0.1	97	210
2	Sn/Cu ₆ Sn ₅ thin film	$100 \mu \text{A cm}^{-2}$	0-1.5	1127	0.5	92	211
3	SnO ₂ /Co ₃ O ₄ /rGO	100	0.01-3	1038	0.1	66.8	212
4	SnO ₂ /graphene	100	0.01-3	2213	0.1	66.74	213
5	C/Sn	200	0-3	1300	0.2	100	214
6	SnO _{2/} C	0.5C	0.01-2	908	0.5	98	215

the $\text{Li}_2\text{O-B}_2\text{O}_3$ -LiBr-coated coated electrode increased from 181.8 to 189.7 mA h g⁻¹, and the coulombic efficiency was enhanced from 94.5% to 97.7%. Fig. 7(c) shows a comparison of the data for the rate capability of the bare and coated NCM523 electrode, where the discharge capacity was observed to be higher for the coated electrodes at all C-rates. Superior cyclic stability was also detected for the coated electrode, which is attributed to the elimination of side reactions and corrosion issues with the electrolyte. The capacity retention was observed to be 87.7% for the coated electrode, which was 29.8% higher than the uncoated electrode up to 100 cycles.

Gan et al.²²⁴ reported the preparation of an NCM811 cathode via modification with a coating of WO₃. The modified layer thickness was around 10 to 15 nm, which was also confirmed via XRD and XPS analysis. The oxygen peak in the XPS survey of the modified electrode was detected, which was weaker than that of the uncoated NCM811 electrode, suggesting the presence of more reactive oxygen on uncoated NCM811. The presence of more reactive oxygen may provoke side reactions between the electrode and electrolyte. The negligible change in electrochemical performance was investigated in the voltage range of 2.8–4.3 V. Although no improvement was observed in the capacity, the rate capability and reversible capacity

drastically improved. The capacity retention was 87.7% for the coated electrode, which was 29.8% higher than that of uncoated electrode for up to 100 cycles.

Therefore, it can be concluded that the coating or surfacemodification of electrodes is a promising approach to tune the electrode surface chemistry. The notable features lead to (i) enhanced thermal stability, (ii) improved rate capability and capacity retention, (iii) prevention of side reactions and electrode corrosion due to the electrolyte, and (iv) suppressed capacity fading during long cycle run. Some of the important materials for electrode modification are suggested to be, for example, carbon (C), TiO2, ZnO, CuO, ZrO2, CeO2, Al2O3, and MgO. Ionic conducting materials such as PEDOT, LLTO (Li_{0.125}La_{0.625}TiO₃), Li₃PO₄, Li₃VO₄, and LiAlO₂ are also auspicious materials for the enhancement of electronic conductivity on the electrode surface. Some important modifications of (coating) materials and their comparative performances (capacity, voltage, capacity retention, and coulombic efficiency) are summarized in Table 11. 218-220,223-242

2.1.14 Role of dopant materials. Doping is an effective strategy or process to enhance the electrode performance by tailoring its crystal lattice at the atomic scale. Doping can tune the charge distribution, defect density, bandgap, and cation

Review

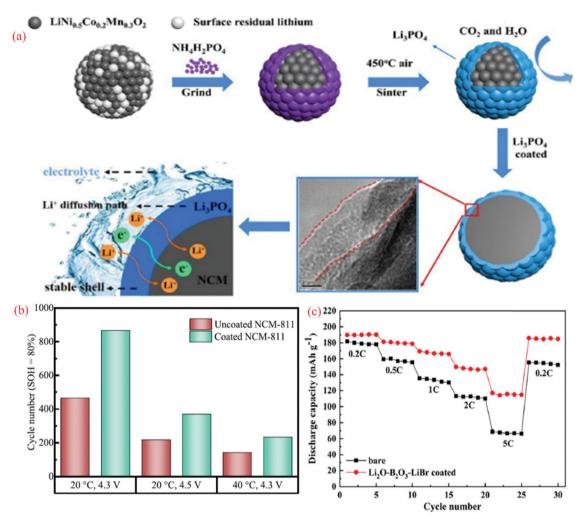


Fig. 7 (a) Schematic diagram of the experimental process.²¹⁹ (b) Achieved cycle numbers for different cycling conditions at an SOH of 80%. The calculation of the SOH is based on the capacity of the fifth cycle and (c) rate performance for uncoated NCM 523 and Li₂O-B₂O₃-LiBr-coated NCM523. Reproduced with permission from Elsevier. 219

order. Another important strategy is to enhance its electrochemical performance, which involves the substitution of cations (Ti, Cu, Ni, Cr, Mn, Mg, Fe, etc.), anions (F), and doping of mixed elements.²⁴³ This is an alternative to surface coating or electrode modification to enhance the electronic conductivity. The dopant may alter the structure and affect the structural stability and charge compensation. Doping is the key parameter to increase the conductivity (electronic/ionic), capacity/ energy density, and delithiation potential. The doping process occurs inside the material at the atomic level for the movement of charge carriers, where the dopant concentration cannot the affect grain boundaries.

Recently, Zheng et al. 244 prepared the Li_{1,2}Mn_{0.54}Ni_{0.13}-Co_{0.13}O₂ (LMNCO) cathode with gadolinium-doped ceria (GDC) via doping using a wet-chemical deposition approach. The XRD pattern suggested that the structure of LMNCO was not changed by the GDC dopant concentration. The increased interlayer spacing of LMNCO indicated the successful doping of Ce⁺³/Ce⁺⁴ or Gd⁺³ without changing the structural properties. The investigated electrochemical performance was found to be

superior for the LMNCO-GDC3 electrode with discharge capacities of 267.5 mA h g^{-1} and 255.2 mA h g^{-1} for the pristine electrode with the charging rate of 0.1C at different intervals. Therefore, it was concluded that the GDC-based modified electrode reduced the charge transfer resistance and promoted Li⁺ migration. After 100 cycles, the capacity retention of LMNCo-GDC3 was 92.9%, which was higher than that of the pristine electrode (75.3% at 0.5C). Fig. 8(a) shows the capacity fading mechanism in the pristine LMNCO. The electrolyte reacts with the electrode and side reactions occur. HF is released from the decomposition of the LiPF₆ salt and reacts with the electrode, which leads to the formation of LiF, resulting in the reduction of Li ions. In contrast, the direct contact between the electrode and electrolyte was restricted in the modified electrode of LMNCO with GDC (Fig. 8b). Overall, this minimized the electrode dissolution tendency and loss of the active material.

Another environment-friendly material, LiNi_{0.5}Mn_{1.5}O₄ (LNMO), has attracted attention from the energy storage community due to its spinal structure, high operating voltage (4.7 V

Table 11 The comparative performance of modified/coated materials used to enhance the battery performance

Coating	Host	Voltage (V)	Capacity (mA h g ⁻¹)	Capacity retention	Efficiency (%)	Ref
Li ₃ PO ₄	$\mathrm{LiNi_{0.5}Co_{0.2}Mn_{0.3}O_{2}}$	2.7-4.3	186.36 (184.36 for pristine)	83% after 200 cycles (68.5 for pristine)	86.06% (83.26% for pristine)	219
Li ₂ WO ₄	NCM 811 (LiNi _{0.8} Co _{0.1} Mn _{0.1} O ₂)	2.5-4.3	192 (188 for pristine)	. ,	80% after 765 cycles (pristine after 465 cycles)	220)
Li ₂ O-B ₂ O ₃ -LiBr	NCM523 (LiNi _{0.5} Co _{0.2} Mn _{0.3} O ₂)	2.5-4.5	116.9 at 5C (68.7 for pristine)	87.7% after 100 cycles (29.8% for pristine)	97.7%	223
LiVPO ₄ F hybrid	LiNi _{0.8} Co _{0.1} Mn _{0.1} O ₂	2.8 - 4.3	214.9 (208.1 for pristine)	95.93 (91.68 for pristine)	90.7 (85.5 for pristine)	224
LLTO	NCA	2.0 - 4.4	135 at C/20	99% capacity after 10 cycles	_	218
A1 O	$(\text{LiNi}_{0.8}\text{Co}_{0.15}\text{Al}_{0.05}\text{O}_2)$	20.42	(125 for pristine)	(85% for pristine)	00.00 (-ft 1-+)	225
Al ₂ O ₃ ZrO ₂	$LiNi_{0.8}Co_{0.1}Mn_{0.1}O_2$ (NCM811)	2.8-4.3	199.2 (201.7 for pristine) 198.7 (201.7 for pristine)	99.61, after 100th cycle 99.66, after 100th cycle	88.02 (after 1st) 88.04 (after 1st)	225
LBO (Li ₂ O-	(NCM011)		204.3 (201.7 for pristine)	99.78% after 100th cycle	88.83 (after 1st cycle)	
B ₂ O ₃ -LiBr)						
Li ₂ O-B ₂ O ₃ -LiBr	$\text{Li}_{1+x}\text{Mn}_2\text{O}_4$	3-4.2	122.5 (12.5 for pristine)	93% after 20 cycles (15.14% for pristine)	_	226
ZrO_2	LiMn ₂ O ₄	3.0-4.3	118.8 (124.4 for pristine)	90.1% after 400 cycles	96.7	227
2	2 .		,	(at 55 °C)		
CeO ₂	$\text{Li}_{1.2}\text{Ni}_{0.2}\text{Mn}_{0.16}\text{O}_2$	2.0 - 4.8	270 at 0.1C (235 for pristine)		80.54	228
Li ₂ O-B ₂ O ₃ -LiBr	$\mathrm{LiNi_{0.8}Co_{0.15}Al_{0.05}O_{2}}$	3.0-4.3	181 (175 for pristine)	94.2% after 100 cycles	91	229
Ta and	$LiNi_{0.6}Co_{0.2}Mn_{0.2}O_2O_2$	1.88-3.88	115 at 34 mA g ⁻¹	91% after 30 cycles	95.9 (87.4 for pristine)	230
***			(52.7 for pristine)	(75% for pristine)	00.6 (07.4 for mainting)	
W			93.3 (52.7 for pristine)	82% after 30 cycles (75% for pristine)	92.6 (87.4 for pristine)	
Carbon	NCM811	3.0-4.3	188.6 (192.8 for pristine)	87.8% after 80 cycles	_	231
	$(LiNi_{0.8}Co_{0.1}Mn_{0.1}O_2)$		r	(74.3% for pristine)		
Li ₅ AlO ₄	NCM811 (LiNi _{0.8} Co _{0.1} Mn _{0.1} O ₂)	2.8-4.3	147.61 (127.86 for pristine)	89.15% after 100 cycles (75.06% for pristine)	_	232
Li ₃ PO ₄	$LiNi_{0.8}Co_{0.1}Mn_{0.1}O_2$	3.0-4.3	192.4 (186.0 for pristine)	86.7% after 250 cycles	86.4 (83.9 for pristine)	233
3 4	0.0 0.1 0.1 2		1 /	(85.2% for pristine)	(1)	
Li ₂ CuO ₂	$LiNi_{0.33}Co_{0.33}Mn_{0.33}O_{2} \\$	2.4-4.2	192 (182 for pristine)	69% after 100 cycles	99 after 30 cycle	234
				(30% for pristine)	(93 for uncoated)	
Co ₃ O ₄ and	$LiNi_{0.8}Co_{0.1}Mn_{0.1}O_2$	2.7-4.5	203.9 at 0.1C	91.4% after 100 cycles	89.1 after 1st cycle	235
LiMn ₂ O ₄ layer	LiNi _{0.6} Co _{0.2} Mn _{0.2} O ₂ O ₂	3.0-4.3	(202.9 for pristine) 124.5	(73.5% for pristine) 86.4% at 0.5C after	(87.8 after pristine)	236
$Ti_3C_2(OH)_2$	$\text{LIM}_{0.6}\text{CO}_{0.2}\text{MII}_{0.2}\text{O}_2\text{O}_2$	3.0-4.3	124.3	200 cycles		230
				(71.2% for pristine)		
Nickel catalyzed	$LiFe_{1-x}Ni_xPO_4$	2.8 - 4.0	181.9 at 0.1C	95.6% at 1C after	> 99 after 200 cycles	237
graphitized carbon			(143.3 for pristine)	500 cycles	•	
Li-Nb-O shell	$\text{Li}_{1.2}\text{Ni}_{0.13}\text{Co}_{0.13}\text{Mn}_{0.54}\text{O}_{2}$	2.0-4.6	219.5 (212.3 for pristine)	96.44% capacity	92.59%	238
				retention after		
				100 cycles (83.09%		
N-Doped	LiNi _{0.6} Co _{0.2} Mn _{0.2} O ₂ O ₂	3.0-4.5	199.4 at 0.2C	for pristine) 82.7% after 100 cycle	_	239
carbon-coated	LIIVI _{0.6} CO _{0.2} WIII _{0.2} O ₂ O ₂	3.0 4.3	(202.4 for pristine)	(61.1% for pristine)		233
Nano-WO ₃	$LiNi_{0.5}Co_{0.2}Mn_{0.3}O_2O_2$	3.0-4.5 V	138 (at 25 °C) and 170.9	80.80% after 200 cycles	87.39 after 1st cycle	240
			(at 50 °C) (107.8 at 25 °C, and 143.9 at 50 °C	•	(83.19 for pristine)	
			for pristine)			
$LiBO_2$	$LiNi_{0.6}Co_{0.2}Mn_{0.2}O_2O_2$	2.8-4.3	123 after cycling at 0.5C after 150 cycles	84.3% during 150 cycles at 0.5C	93.7 (90.6 for pristine)	241
			(94 for pristine)	(68.3% for pristine)		
LFP	$LiNi_{0.82}Co_{0.12}Mn_{0.06}O_2$	3.0-4.2	165.3 after 500 cycles at	91.65% after 500 cycles	_	242
			1C (130.7 for pristine)	(70.65% for pristine)		

versus Li) and rate capability. LNMO has a theoretical specific energy of $\sim 650 \text{ W h kg}^{-1}$ and observed to be superior in comparison to other cathodes. 247,248 The cation ordering in LNMO can be tuned by the annealing parameters, which disorder the spinel. To prepare disordered spinels, Bhuvaneswari et al.245 prepared Sc-doped LNMO (LNMSO) via the solution combustion method. Its XRD pattern confirmed the formation of a disordered spinel structure with the $Fd\bar{3}m$ space group. The IR spectra also supported this, evidencing the absence of an ordered spinel structure (P4332). The first discharge capacity for LNMSO was 131 mA h g-1 with a

coulombic efficiency of 88%, while the undoped LNMO demonstrated the first discharge capacity of 123 mA h g-1 with a coulombic efficiency of 81% at 0.1C. Even after 1000 cycles, LMNSO exhibited the capacity of 102 mA h g⁻¹ (capacity retention = 98%), which was higher than that of LMNO (79 mA h g^{-1} with the capacity retention of 90% at 5C). Fig. 8(c) shows the rate capability in the range of 0.1C to 12C. The LMNSO electrode demonstrated a superior performance to the bare LMNO at all current rates. Even at a high C-rate, the capacity retention for LMNSO was observed to be 61%, which was higher than that of LMNO (45%). This enhancement in

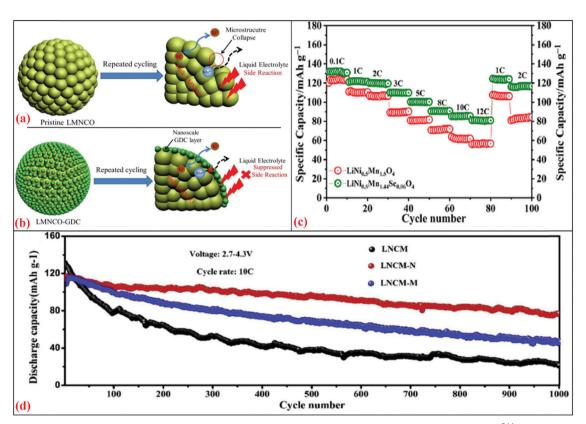


Fig. 8 Schematic illustrations of (a) pristine LMNCO interfacial side reactions with liquid electrolyte after repeated cycling²⁴⁴ and (b) GDC coating layer acts as a protection layer to suppress the unwanted interfacial side reactions after repeated cycling. 245 (c) Rate capability for LNMO and LNMSO cathode for 0.1–12C. (d) Cycling performances for LNCM, LNCM-N, LNCM-M at C-rate of 10C. 246 Reproduced with permissions from Elsevier. 244–246

specific capacity and rate capability was attributed to the creation of disorder in Ni/Mn by Sc-doping, which facilitated faster Li diffusion. Higher D_{Li}^+ (10^{-10} – 10^{-14} cm² s⁻¹) values were obtained for LNMSO compared to LNMO (10⁻¹⁰-10⁻¹⁵ cm² s⁻¹), suggesting the fast cation diffusion regarding Sc concentration.

The atomic substitution of foreign elements is an effective strategy to improve the thermal stability and the rate capability of the NCM cathode. Li et al. 246 examined the effect of Al3+ doping in the Ni-rich LiNi_{0.8}Co_{0.1}Mn_{0.09}Al_{0.01}O₂ cathode via a continuous co-precipitation method. The samples were designated as LNCM-N (LiNi_{0.8}Co_{0.1}Mn_{0.09}Al_{0.01}O₂), LNCM-M (LiNi_{0.8}Co_{0.1}Mn_{0.09}Al_{0.01}O₂), and NCM811 (LiNi_{0.8}Co_{0.1}Mn_{0.1}O₂). XRD evidenced the shift to the 003 reflection, which was the highest. This suggests that the incorporation of Al³⁺ was the highest for LNCM-N. The FE-SEM image indicated the uniform distribution of Al³⁺. Compared to the Ni²⁺ on Li slabs of LNCM-M and LNCM, the XPS analysis indicated that the presence of a lower Ni²⁺ content on the Li slabs for LNCM-N. The lower Ni²⁺ content was favorable for the faster cation (Li⁺) intercalation/deintercalation, which showed the highest capacity in the electrochemical analysis. LNCM-N demonstrated a higher discharge capacity (at 1C) of about 126 mA h g^{-1} (capacity retention = 78.92%) after 200 cycles compared to LNCM-M (90 mA h g^{-1} ; capacity retention = 59.69%) and LNCM (83 mA h g^{-1} ; capacity retention = 48.62%). Fig. 8(d) shows the performance of the three cells for 1000 cycles at 10C. It shows the highest discharge capacity for LNCM-N

(with the efficiency of >98% and capacity retention = 70%) compared to LNCM-M and PNCM. The diffusion coefficients of LNCM, LNCM-M, and LNCM-N were investigated to be 3.62 \times $10^{-14} \, \mathrm{cm}^2 \, \mathrm{s}^{-1}$, $6.51 \times 10^{-14} \, \mathrm{cm}^2 \, \mathrm{s}^{-1}$, and $9.77 \times 10^{-14} \, \mathrm{cm}^2 \, \mathrm{s}^{-1}$ respectively. The high value of the Li⁺-diffusion coefficient and low impedance (evidenced by the XPS) led to better cyclic stability and enhanced capacity.

Cation substitution is an attractive strategy to tune electrodes, which reduces the cation mixing to promote the structural integrity and increase the Coulombic efficiency of the electrode. This approach was used by Huang et al., 249 who investigated the effect of partial Mn substitution with Mg by preparing LiNi_{0.6}Co_{0.2}Mn_{0.2-x}Mg_xO₂ via the hydroxide co-precipitation method. Mg reduced the cation mixing, preventing the structural collapse of the Li layer, i.e., stable pillar effect. The electrochemical performance was evaluated between 2.8-4.3 V at RT. The initial discharge capacity at 0.1C was 180.94 mA h g⁻¹ for the pristine electrode and 186.23 mA h g^{-1} for x = 0.01. The capacity retention for the Mg-doped electrode was 91.04% for x = 0.03, which is higher than that of the pristine electrode (81.34%) for 100 cycles. This was attributed to the decreased cation mixing, which reduced the barrier for Li migration and enhanced the structural stability owing to strong Mg-O bonding. The effect of doping elements and metallic species on the specific capacity, capacity retention, Coulombic efficiency, and scanning rates is summarized in Table 12.^{239,244-246,249-261}

Table 12 Summary of different bulk substitutions and corresponding performances

Dopant	Host	Voltage (V)	Capacity (mA h g ⁻¹)	Capacity retention	Efficiency (%)	Ref.
Gadolinium- doped ceria (GDC)	$\text{Li}_{1.2}\text{Mn}_{0.54}\text{Ni}_{0.13}\text{Co}_{0.13}\text{O}_{2}$	2.0-4.8	267.5 at 0.1C (255.2 for pristine)	92.9% after 100 cycles at 0.5C (75.3% for pristine)	83.3 (73.7 for pristine)	244
Sc	$\rm LiNi_{0.5}Mn_{1.5}O_4$	3.5-4.9	131 (123 for undoped)	94% after 300 cycles at 1C	88 after 1st cycle (81 for un-doped)	245
Al ³⁺	$LiNi_{0.8}Co_{0.1}Mn_{0.1}O_2$	2.7-4.3	126 at 1C (83 for undoped)	78.92% at 1C rate after 200 cycles, 70.0% at 10C rate after 1000 cycles.	98%	246
Mg	$LiNi_{0.6}Co_{0.2}Mn_{0.2}O_2$	2.8-4.3	186.23 at 0.1C (180.94 for pristine)	91.04% after 100 cycles (81.34%) for pristine)	89.16 for first cycle (87.03 for pristine)	249
Mn Ti	$LiNi_{0.85}Co_{0.10}Al_{0.05-x}$	3.0-4.3	171.4 (156.5 for pristine) 179.6 (156.5 for pristine)		88.6 (79.4 for pristine) 81.7(79.4 for pristine)	250
F	$Li_{1.15}Ni_{0.275}Ru_{0.575}O_2$	2.2 - 4.3	103 (94 for pristine)	42.2% (43.0% for undoped)	_ ` ´ ´	251
Ti	$LiNi_{0.8}Co_{0.1}Mn_{0.1}O_2$	2.8-4.3	165.02 (147.41 for undoped)	77.01% after 150th at 1C	82.5 after 1st cycle (79.3 for pristine)	252
Nb^{5+}	LiV ₃ O ₈ nanorods	1.8 - 4.0	401 at 0.1C	99.7% after 500 cycles	>90	253
N	$\mathrm{LiNi_{0.6}Co_{0.12}Mn_{0.22}}$	3.0-4.5	156.6 at 5C	82.7% at 1C after	_	239
			(129.2 for undoped)	100th cycles (61.1% for undoped)		
1D Nb	$LiNi_{1/3}Co_{1/3}Mn_{1/3}O_2$	2.7-4.3	118.7 at 5C	83.3% capacity retention	92.3 at 0.1C	254
••	7 '7 C DO		(109.6 for undoped)	after 200 cycles at 5C	0.407	
V	LiMnPO ₄	2.2-5.0	126 at 0.2C	74.4 after 50 cycles	94%	255
W	$LiNi_{0.90}Co_{0.05}Mn_{0.05}O_2$	2.7-4.4	235	89% of after 500 cycles (60% for pristine)	_	256
Nb	$\text{Li}_{1,2}(\text{Ni}_{0.13}\text{Co}_{0.13}\text{-}\\ \text{Mn}_{0.54})_{1-x}\text{Nb}_{x}\text{O}_{2}$	2.0-4.8	287.5 (234.2 for pristine)	98.50% after 300 cycles (86.68% for pristine)	_	257
ZrO_2	$\mathrm{LiNi}_{0.92}\mathrm{Co}_{0.08}\mathrm{O}_{2}$	2.8-4.3	207.2 at 0.2C (201.3 for pristine)	82.90% after 100 cycle (59.01% for pristine)	84.74 after 1st cycle	258
Mg	NCM811 (LiNi _{0.8} Co _{0.1} Mn _{0.1} O ₂)	3.0-4.5	226.5 at 0.1C (208 for pristine)	81% over 350 cycles at 0.5C (67% for pristine)	_	259
Mn	LiFePO ₄	3-4.4	45.7 at 0.05C after 1st cycle (43.8 for pristine)	84% after 100 cycles at 0.5C	94% after 100 cycles at 0.5C	260
W	Li ₄ Ti5O ₁₂ /brookite	1.0-3.0	\sim 205 at 0.1 A g ⁻¹ at $-$ 20 °C (\sim 53 for pristine LTO)	96% after 1000 cycles at 1 A g ⁻¹	~100%	261

2.1.15 Morphology and mesostructure design. The morphological aspects of electrode materials play an effective role in deciding the electrochemical performance of the device. Different morphologies such as nanoparticles, nanoflowers, nanorods, nanowires, nanospheres, and nanotubes can be selected for electrodes to enhance the recyclability of batteries. Nanoparticles are beneficial for the electrochemical performance due to their large surface area. Nanorods and nanowires are the most suitable nanostructures to reduce the traps of electrons or ions in the electrode. The high surface area of nanoparticles facilitates the complete use of the active sites in the material, which provides smooth ion dynamics by decreasing the diffusion length (L) for active charged ions and electrons. Therefore, the particle size can be tuned to enhance the cyclic stability and energy density. The Li⁺-ion diffusion coefficient shows an inverse relation with the diffusion path length and characteristic time (τ) $\left(\tau = \frac{L^2}{4\pi D}\right)$, where L is the particle size, D is the diffusion coefficient, and τ is the characteristic time. 262 The synthetic method determines the morphology and the structure. Some of the important synthetic methods of nanoparticles include sol-gel, solid-state precipitation, hydrothermal, and solvothermal. The important parameters that are key to achieving a desirable morphology include the growth tempera-

temperature. Another important approach is the formation of coreshell microstructures, where the core and shell are tailored to achieve a balanced and optimum performance electrode. For the formation of good core-shell microstructures, the structural mismatch between the core and the shell must be eliminated or reduced to obtain the desired stability during the cell operation. The capacity and capacity retention of microstructure-based electrodes (nanoplate, rectangular prism, nanorods, hexagonal nanorods, nanowires, triaxial nanowires, nanotubes, and chain-like nanowires) are summarized in Table 13.263-270

2.1.16 Synthesis methods for cathode materials. Many synthetic methods have been developed for the preparation of cathode materials. The reaction time, precursors, growth temperature, and pressure are important parameters that must be controlled to obtain the desired materials. The synthesis method affects the particle shape, size, distribution, phase, and active material stability. The synthesis methods used include the sol-gel, solid-state precipitation, hydrothermal, microwave sintering, template-free hydrothermal, co-precipitation, and spray-drying methods. Gong et al.271 prepared the LiNi_{0.8}Co_{0.2}O₂ cathode material via the sol-gel method (Method-A) and solid-state reaction (Method-B). The XRD analysis confirmed the formation of a pure phase, regardless of the synthesis method. The electrochemical performance of the prepared electrode was examined between 3.0-4.3 V with the first discharge capacity of

ture, stirring time, sintering time, pressure, pH, and calcination

Review

Table 13 Summary of different bulk substitutions and corresponding performance

Morphology	Material	Voltage (V)	Capacity (mA h g^{-1})	Capacity retention	Ref.
Nanoplate, rectangular prism nanorod	LiFePO ₄	2.4-4.2	163.8 at 0.2C	_	263
Nanoplate, hexagonal prism nanorod			144.4 at 0.2C	_	
Nanowire	LiFePO ₄ /C	2.5 - 4.1	155 at 1C rate	98% after 100 cycles at 20C rate	264
Nanowire	$LiFePO_4$	2-4.2	110 at a current	86% after 1000 cycles at a current rate of 10C.	265
			rate of 30C	•	
Triaxial nanowire	$LiFePO_4$	2-4.5	130 at 0.1 A g^{-1}	_	266
Nanowire	$LiCoO_2$	3.0 - 4.3	126 at 1 mA g^{-1}	80% after 100 cycles	267
Nanotube	$LiCoO_2$	3-4.3	185 at 10 mA g^{-1}	89% after 100 cycles	268
Nanotube	$LiNi_{0.8}Co_{0.2}O_2$		205 at 10 mA g^{-1}	71% after 100 cycles	
Nanotube	$LiMn_2O_4$		138 at 10 mA g^{-1}	69% after 100 cycles	
Chain like nanowire	$LiCoO_2$	3.0 - 4.2	103 at 10C	90% after 50 cycles	269
Aligned slanted nanowires	$LiCoO_2$	3.0 - 4.2	97.3 at 0.1C	89% after 150 cycles, 73% after 400 cycles	270
0				• •	

187 mA h g^{-1} and 185 mA h g^{-1} , via Method-A and Method-B, respectively. After 100 cycles at 0.2C, the cathode electrode prepared via Method-B (158 mA h g⁻¹ with a capacity retention of 85.4%) showed a better performance than Method-A (143 mA h g^{-1} with a capacity retention of 77.3%). The cathode electrode prepared via Method-B showed a better electrochemical performance with low and high charge-discharge rates (i.e., 0.2C and 1C). Although the microstructural properties for both synthesis methods were observed to be similar, their morphologies were different, where Method-A resulted in the formation of irregularly faceted pebbles, whereas that with Method-B was irregularly spherical. The porous structure of the Method-B cathode allowed faster Li⁺ intercalation and de-intercalation.

Jiang et al. 272 prepared an $\text{LiNi}_{0.9}\text{Co}_{0.05}\text{Mn}_{0.025}\text{Mg}_{0.025}\text{O}_2$ electrode via the sol-gel method and investigated the effect of calcination temperature and time on its electrochemical performance. The XRD analysis evidenced a decrease in cation mixing with respect to an increase in temperature (650 °C to 800 °C). The microscopic images showed the growth of nanoparticles with an increase in temperature, which increased the size of the nanoparticles from the nanometer to micrometer range. The specific capacity of the electrode was 128.4, 201.0, and 180.5 mA h g⁻¹ after the first cycle and 121.4, 199.6, and 170.0 mA h g⁻¹ after the 10th cycle regarding the calcination temperature of 650 °C, 700 °C, and 750 °C, respectively. The specific capacity decreased at high temperatures due to the large particle size (as evidenced from SEM), which reduces the diffusion distance. The SEM analysis confirmed that the morphology changed with agglomeration at the calcination time of 18 h, together with a good hexagonal structure. The specific capacity changed to 144.0, 187.6, and 132.1 mA h g^{-1} after the fifth cycle and 106.3, 172.3, and 105.1 mA h g⁻¹ at 1C with the calcination time of 6 h, 12 h, 18 h, respectively. The reduction in specific capacity at a high calcination time is attributed to the agglomeration tendency of particles, as evidenced by SEM. Table 14 summarizes the different methods, materials prepared, and performance parameters. 80,271-289

3. Electrolytes for Li-ion batteries

Since the first breakthrough in LIBs by John Goodenough and their commercialization by the Sony Corp. in 1991, these batteries have attracted global attention owing to their high energy density. Prof. J. B. Goodenough said that "the cost, safety, energy density, rates of charge/discharge and cycle life are critical for battery-driven cars to be more widely adopted". During battery operation, the simultaneous movement of ions and electrons occurs. Ions flow through the electrolyte, while electrons are generated at the anode (negative electrode) and flow towards the cathode (positive electrode) via an external circuit. The electrode accommodates charge storage in the stacking layers, while the electrolyte acts as a carpet for the ions. The capacity of the battery depends on the rate of Li⁺ migration to and from via the spacer between electrodes. Despite the effective role of the electrode in the stability and safety of batteries, the electrolyte is also a key component and must be chosen carefully because of its dual role. A separator is placed between electrodes, which prevents short-circuit and provides a medium for ion migration. 290,291 The electrolyte, together with the separator, must fulfill essential requirement. Table 15 provides a glimpse into the important electrolyte parameters for developing safe and efficient LIB separators. 292

The existing batteries are based on a liquid electrolyte; however, it threatens the safety of batteries due to the possibility of cell explosion as a result of side reactions. The leakage of the electrolyte may degrade the electrodes, causing capacity fading due to the loss of the active materials. This leads to the loss of sufficient ion storage sites in the electrode, low capacity, and energy density, resulting in a degradation of the battery performance. During the rapid charging-discharging process, the dendrites can grow at the anode and pass through the liquid electrolyte easily, which short-circuit the battery and explosion may also occur.

Unwanted chemical reactions between the liquid electrolyte and electrode lead to the release of gases inside, and pressure build-up occurs when the battery fails to accommodate the volume changes. The other main requirements for advanced batteries are the lower cost and weight. The current LIBs use both an electrolyte and separator, which affect their cost and weight. Therefore, these are some serious issues in the current battery systems that need to be resolved. They can be fixed by replacing the liquid electrolyte with solid electrolytes. Solid-state electrolytes (SSEs) are the main components in ASSLBs. 293,294 The recent progress in inorganic SSE systems mainly including oxide Table 14 Summary of different bulk substitutions and the corresponding performances

Method	Precursors	Voltage (V)	Capacity (mA h g ⁻¹)	Capacity retention (%)	Ref.
Sol-gel	LiNi _{0.8} Co _{0.2} O ₂	3.0-4.3	143 after 100 cycles at 0.2C	77.3	271
Solid-state			158 after 100 cycles at 0.2C	85.4	
Sol–gel (calcination temp = 650 °C)	LiNi _{0.9} Co _{0.05} -	2.8 - 4.3	128.4 after 1st cycle	121.4 after 10 cycles	272
Sol–gel (calcination temp = 700 °C)	$Mn_{0.025}Mg_{0.025}O_2$		201.0 after 1st cycle	199.6 after 10 cycles	
Sol–gel (calcination temp = 750 °C)			180.5 after 1st cycle	170.0 after 10 cycles	
Sol-gel (calcination time = 6 h)	$LiNi_{0.9}Co_{0.05}Mn_{0.025}$	2.8 - 4.3	144.0 (at 1C)	106.3 after 50 cycles	
Sol-gel (calcination temp = 12 h)	$Mg_{0.025}O_2$		187.6 (at 1C)	172.3 after 50 cycles	
Sol-gel (calcination temp = 18 h)			132.1 (at 1C)	105.1 after 50 cycles	
Sol-gel	$LiNi_{0.33}Mn_{0.33}Co_{0.33}O_{2}$	3.0 - 4.6	157	_	273
Thermal destruction	(NMC111)		147	_	
Solid-phase			172 at 1C/0.5C	95.2 after 10 cycles	
Hydrothermal	Li ₂ FeTiO ₄	1.5 - 4.8	153.8 at C/10	_	274
Template-free hydrothermal	Li ₂ FeSiO ₄ hollow sphere	1.5-4.8	152 at 0.05C	110 after 100 cycles at 0.1C	275
Hydrothermal	${\rm LiMn_2O_4}$	3.2-4.35	121 at a current density of 1/10C	111 mA h g ⁻¹ at 1/2C after 40th cycle	276
Urea-based hydrothermal	LiNi _{0.5} Co _{0.2} Mn _{0.3} O ₂	3.0-4.3	158.6 after 1st cycle at 20 mA h g ⁻¹	92.6 after 50 cycles	277
,	0.5 - 0.2	3.0-4.6	200 after 1st cycle at 20 mA h g ⁻¹	79.4 after 50 cycles	
Hydrothermal	LiFePO ₄	2.0-4.5	167 at 0.1C after 1st cycle	98 after 30 cycles	278
Microwave synthesis	LiFePO ₄ /Graphene	2.7 - 4.2	166.3 at 0.1C after 1st cycle	99.5 after 10th cycle	279
Microwave-assisted hydrothermal	LiFePO ₄	2.5-4.2	152.1 at 0.1C after 1st cycle	~95 after 40th cycle	280
Microwave synthesis	LiFePO ₄ /C	2.5 - 4.0	150 at 0.1C)	_	281
Microwave synthesis	LiMn _{1.5} Ni _{0.5} O ₄ Spinel	3.5-4.8	130 at the 25th cycle	100 between 10th and 50th cycle	282
Microwave-assisted solvothermal	Li ₂ MnSiO ₄	2.0 - 4.5	250 at C/10	_	283
Spray drying	$LiNi_{0.5}Mn_{1.5}O_4$	3.0 - 4.8	134 mA h g ⁻¹	95 at 3.5C	284
Modified co-precipitation	Al-Doped	3.0-4.3	159.7 mA h g^{-1} at 0.5C for 1st cycle	86.56 after 100 cycles	285
	$LiNi_{0.5}Co_{0.2}Mn_{0.3}O_2$			v	
Co-precipitation	LiNi _{0.5} Mn _{1.5} O ₄ (half-cell)	3.5 - 4.95	141 mA h g ⁻¹ at 1C after 200 cycles 141 mA h g ⁻¹ at 1C after 200 cycles	94 over 200 cycles at 1C	286
• •	LiNi _{0.5} Mn _{1.5} O ₄ (full cell)		141 mA h g ⁻¹ at 1C after 200 cycles	92.4 over 200 cycles at 1C	
	LiNi _{0.5} Mn _{1.5} O ₄ (full cell		133.2 mA h g ⁻¹ at 1C	93.3 over 100 cycles at 1C	
	at 55 °C		after 200 cycles	•	
Solvothermal	$\mathrm{LiNi_{0.88}Co_{0.09}Al_{0.03}O_{2}}$	3.0-4.3	210.7 mA \dot{h} g ⁻¹ at 0.1 after 1st cycle	75.93 after 100 cycles at 55 °C (0.1C)	80
Co-precipitation			203.2 mA h g ⁻¹ at 0.1 after 1st cycle		
Antisolvent precipitation	LiBO ₂ coated LiNi _{0.5} Co _{0.2} Mn _{0.3} O ₂	2.5-4.6	200 mA h g ⁻¹ at 0.1C	78.5 after 100th cycle	287
Template method	$LiNi_{0.5}CO_{0.2}MII_{0.3}O_2$ $LiNi_{0.5}Mn_{1.5}O_4$	3.5-5.0	\sim 129 mA h g ⁻¹ at 1C	96.6 after 100 cycles at 1C	288
Chloride co-precipitation	$LiNi_{0.8}Co_{0.1}Mn_{0.1}O_2$	2.7-4.3	184 mA h g ⁻¹ at 0.1C	169 mA h g ⁻¹ after 30 cycles.	289

Table 15 General requirements for separators used in lithium-ion batteries

Requirement
Stable for an extended period Wet out quickly and completely > 1000 kg cm ⁻¹ (98.06 MPa) 20–25 µm <1 µm 40–60% <0.025 s µm ⁻¹ No curl up and lay flat <5% shrinkage after 60 min at 90 °C Effectively shut down the battery at elevated temperatures

SSEs, sulfide SSEs, and halide SSEs has been reported by many researchers. 295-298 The ionic conductivity of the typical inorganic solid-state electrolyte is required $\sim 10^{-3} \, \mathrm{S \ cm^{-1}}$ at room temperature, which is very close to the ionic conductivity level of liquid electrolytes.²⁹⁹ The poor performance was observed due to high

interfacial impedance caused by the instability between the sulfide solid electrolyte and oxide cathode during the chargedischarge process. To overcome the interfacial impedance, the LiNbO₃-coated NCM811 cathode was reported to exhibit significantly improved electrochemical performances at 35 $^{\circ}\mathrm{C}$ and 60 $^{\circ}\mathrm{C}$ Review

in contrast to the bare cathode. Especially at 60 °C, the LiNbO₃coated NCM811 cathode displayed a discharge capacity of 203 mA h g⁻¹ at 0.1C and a rate performance of 136.8 mA h g⁻¹ at 5C, which are much higher than that for the reported oxide electrodes in ASSLIBs using sulfide solid electrolyte. 300

The fundamental benefits of solid electrolytes are as follows: (i) better thermal and mechanical stability, (ii) better cell packaging with high pressure, (iii) no possibility of side reactions due to solid nature, (iv) better interfacial contact and prevention of dendrite growth, (v) low cost due to dual role (electrolyte and separator), and (vi) higher safety and broad temperature range of operation.^{291,301} For an ideal electrolyte, high ionic and negligible electronic conductivity are favorable. 302 Ionic conductivity is linked to the number of free cations and electrolyte viscosity. 303 Thus, a high number of free charge carriers and low viscosity of the electrolyte are specific requirements. Furthermore, the voltage stability, thermal stability, and mechanical stability determine the overall safety of the battery operation. Fig. 9 shows the characteristic parameters of the electrolyte (crystallinity, packaging, ion transport number, interfacial contacts, broad temperature range, voltage stability window, conductivity, salt dissociations, inert towards electrodes, and glass transition temperature) that influence the ion dynamics, capacity, and energy density of the battery.

For the synthesis of new polymer electrolytes, the involved salts play a crucial role. The parameters of the salt are the main deciding factors for the performance of electrodes, and thus it should be carefully selected. The ion dynamics are linked with the anion size, anion mobility, molecular weight, ion conductivity, donor number, thermal stability, toxicity, dissociation constant, and lattice energy of the salt.304 Fig. 10 shows the possible structures of some of the dominant lithium salts in the R&D sector, and their key properties, that is, ionic conductivity, molecular weight, ion mobility, dissociation constant, and donor numbers are compared. Table 16 summarises the lithium salts according to their anion size and main characteristics (ionic conductivity, molecular weight, ion mobility, dissociation constant, and donor numbers), which affects the electrolyte conductivity.305

4. Major challenges associated with battery safety

The electrolyte used in commercial LIBs is an organic electrolyte, which threatens the safety of the battery during chargingdischarging. Because of the poor safety of batteries with organic

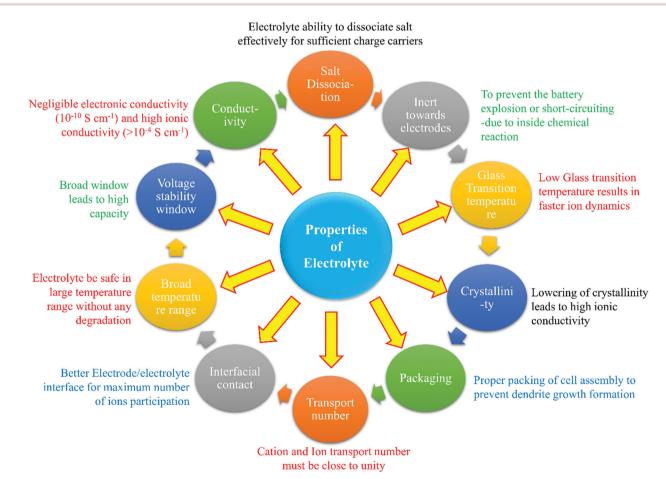


Fig. 9 Characteristic properties of crystallinity, packaging, ion transport numbers, interfacial contacts, broad temperature range, voltage stability window, conductivity, salt dissociations, inert towards electrodes, and glass transition temperature for electrolytes of LIBs.

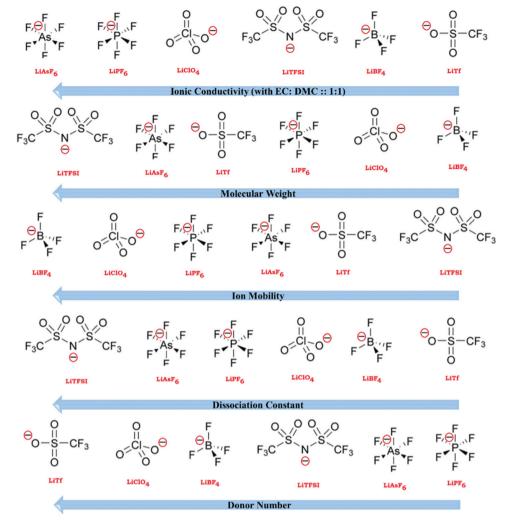


Fig. 10 Comparison of the different characteristics of lithium salt (ionic conductivity, molecular weight, ion mobility, dissociation constant, and donor numbers), reproduced with permission from Springer. 305

electrolytes, a high performance cannot be achieved (long cycle life and high-power density), where safety is one of the prime requirements for battery manufacturers. Due to major safety concerns, many challenges have been considered in the energy storage sector. Two important reasons that threaten the safety of LIBs are thermal runaway and dendrite growth, which both can cause battery explosion due to fire and short-circuit.307 Therefore, liquid electrolytes should be replaced with solid electrolytes for the safe operation of batteries, particularly for portable electronic devices and electric vehicles. Many accessories and precautions have been considered as a priority in the production of batteries to prevent heat generation and shortcircuiting. Nevertheless, a feasible and optimized solution can enhance their safety by eliminating the inherent issues faced by the electrode, electrolyte, and interfacial layers.

4.1. Thermal runaway issues

Thermal runaway (TR) indicates uncontrolled reactions inside the battery. Thermal runaway is initiated when the heat generated inside the battery cannot be compensated by heat loss to

the environment. Because of the heat generated during operation, the battery catches fire and may explode, which can be avoided by replacing the liquid electrolyte with solid electrolytes. In brief, TR disturbs the physical and chemical properties of the materials used in batteries. Various fire incidents associated with LIBs have been reported in portable electronic products and electric vehicles worldwide. When they were analyzed in detail, four common reasons were observed, as follows: (i) overheating and overcharging, (ii) short-circuit due to self-ignition or mechanical damage, (iii) failure of the battery due to handling management, and (iv) pressure build-up due to the release of gas after degradation of the electrolyte. 308,309 Fig. 11 shows the main causes of LIB damage or battery explosions due to reasons such as deformation, separator tearing, dendrite growth, and increase in temperature. 310

Fig. 12(a) shows the role of temperature and its effect on the battery operation for safety concerns. With an increase in the temperature of the battery due to overcharging, overheating, or external impact during its operation, the active material of the electrolyte starts decomposing. This activity occurs in various

Table 16 Structure and properties of commonly used lithium salts for studies on polymer electrolytes³⁰⁶

Lithium salt	Anion	Main characteristics
LiClO ₄	۰ ^{۲۵} .۰۰ ۱۳۰۵	 Broad electrochemical stability window Low solubility in commonly used carbonate-type solvents
${ m LiBF_4}$	F B F F	 Broad electrochemical stability window Low solubility in commonly used carbonate-type solvents
${ m LiPF}_6$	F,OP F F	 High ionic conductivity, favors SEI formation, passivates Al substrate at the cathode side Decomposes in the presence of moisture and reacts with electrolytes at elevated temperatures, resulting in the formation of HF
LiFSI	e, _e , v, e, e	 Higher ionic conductivity compared to LiTFSI and high electrochemical stability Unable to form passivation layers on Al current collectors (in the presence of LiCl) But purified LiCl free salt passivates Al collectors
LiBETI	$\begin{array}{cccc} & \circlearrowleft & \circlearrowleft & \circlearrowleft \\ F_3C & & \circlearrowleft & & \circlearrowleft & C_2^CCF_3 \\ F_2 & & & F_2 \end{array}$	 High solubility and high ionic conductivity and high electrochemical stability Unable to form passivation layers on Al current collectors
LiBOB	JOB OF	 High electrochemical stability and long-term stability Form highly resistive SEI-films (low conductivity in comparison to LiPF₆ and LiTFSI)
LiDFOB	F ₀ ,0	 High electrochemical stability and cycling behavior, Able to form a passivation layer on Al current collectors Lower solubility in carbonate type solvents compared to LiTFSI and LiPF₆, but higher than LiBOB
LiTFSI	O, O O, O F ₃ C, S, N, S, CF ₃	 High solubility and high ionic conductivity and high electrochemical stability Unable to form a passivation layer on Al current collectors (Al-degradation and corrosion)

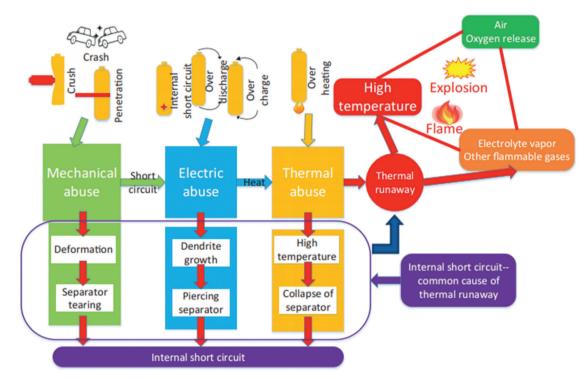


Fig. 11 Schematic illustration of LIB fire accidents.

side reactions of complex reaction mechanisms, which damage the battery. The cathode, anode, and electrolyte reactions lead to the decomposition of the SEI layer and electrolyte breakdown occurs with the release of harmful species (LiPF₆ \rightarrow LiF + PF₅). The release of oxygen, heat, and dendrite formation lead to thermal runaway.311

Although internal short-circuiting is one of reasons for TR, sometimes TR may occur without short-circuiting. The safety of the battery depends not only on the individual electrodes and

electrolyte, but also on the overall properties of the cell components. The chemical cross-talk between the cathode and anode may lead to the TR mechanism. Recently, Liu et al. 312 studied in detail large pouch cell batteries, where a polyethylene terephthalate (PET)-based ceramic separator was used to prevent short-circuiting of the battery. It was observed from DSC, heat generation, and the MS oxygen gas (m/z = 32)characterization versus temperature plot that the phase transition is linked to the generation of heat and release of oxygen.

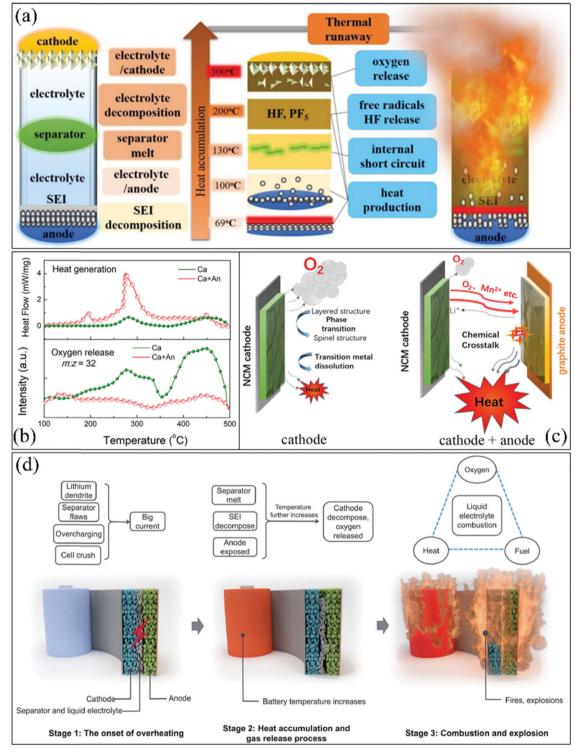


Fig. 12 (a) Schematic of thermal runaway stages of lithium-ion batteries: chemical crosstalk between the charged cathode and anode. (b) Charged cathode alone exhibits a strong oxygen release peak, while the mixture of cathode/anode releases virtually no oxygen but has sharp heat generation enhancement at the same temperature range. (c) Illustration of proposed chemical crosstalk process between the cathode and anode. (d) Three stages for the thermal runaway process. Stage 1: The onset of overheating. The batteries change from a normal to an abnormal state and the internal temperature starts to increase. Stage 2: Heat accumulation and gas release process. The internal temperature quickly rises and the battery undergoes exothermal reactions. Stage 3: Combustion and explosion. The flammable electrolyte combusts, leading to fires and explosions. The flammable electrolyte combusts, leading to fires and explosions. permission from AAAS Science. 309

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This released oxygen (at 276 °C) can diffuse through the separator and react with the reactive anode.

Fig. 12(b) shows the absence of any oxygen peak, which indicates that the anode consumed it, as also evidenced by the weight loss comparison. The cathode showed a larger (2.8%) weight loss than the cathode/anode mixture (0.7%). The exothermic reactions were larger for the cathode/anode mixture (770 J g^{-1}) than the individual cathode (108 J g^{-1}) . This chemical cross-talk between the cathode and anode is shown in Fig. 12(c). The individual cathode releases oxygen, which leads to the initial generation of heat. During the device operation (charging-discharging), the heat is generated rapidly, and oxygen reaction leads to TR. The authors also confirmed that the TR could not be stopped by purging with liquid nitrogen. The liquid nitrogen failed to stop the TR because of oxygen was supplied from inside the cathode of the battery. Therefore, a solution to overcome this issue seems to be improving the battery thermal management system. The safety of the device needs to be the priority together with its performance.

Fig. 12(d) shows the battery explosion due to a thermal runaway during operation.³⁰⁹ In stage-1, the main reasons for initial heat generation are battery crash, dendrite growth, overcharging, and internal short-circuiting. In stage-2, the battery temperature increases due to the accumulation of heat, which results in the decomposition of SEI; hence it releases gases from electrode-electrolyte reactions where the separator starts melting. The melting of the separator leads to the shortcircuiting of the battery, causing the breakdown of the active materials. In stage-3, the liquid electrolyte is present in the battery, resulting in the explosion of the battery or permanent shutdown. Simultaneously, the battery releases some gases due to internal pressure, which is a favorable condition for explosions. The electrolyte is a component that separates the electrodes, which prevents their interaction and plays an effective role in preventing the short-circuiting of the battery. The most feasible alternative electrolyte that has potential to eliminate the threat of thermal runaway is the solid electrolyte. The solid nature of electrolytes will automatically enhance the safety and prevent side reactions and there is no tendency to leak electrolytes.313

4.2 Dendrite growth: challenges and remedies

Together with the TR threat, the dendrite growth affects the safety of the battery, which diminishes the cyclic stability and restricts the operation or lifetime of the battery. Dendrites are generally rigid tree-like structures with needle-like projections (called whiskers) that grow at the anode. The growth of dendrite structures at the anode penetrates through the separator and reaches the cathode during the cell operation. Therefore, the specific capacity deteriorates and causes short-circuiting of the battery, and finally damages the device and shortens its life span. When increasing the miniaturization and compactness of devices, the growth of dendrite structures is one of the significant threats that need to be eliminated for developing high energy density and long life in the battery.

Recently, Zhao et al. 314 proposed the concept of ions redistribution to suppress the dendrite growth. The separator is an insulating layer through which Li-ions migrate/penetrate. These Li-ions accumulate on the anode surface through the pores of the separator. In the absence of distributed ions, the anode surface was faced with the separator skeleton. The Li-ion redistributor method is regulated to avoid the accumulation of ions on the anode electrode, where dendrite growth formation occurs (Fig. 13iA and B). A commercially available separator, named polypropylene (PP), was coated on Al-doped LLZTO (Al-doped Li_{6.75}La₃Zr_{1.75}Ta_{0.25}O₁₂), which regulated the ion diffusion owing to the presence of inherent 3D conduction channels. The coated electrode enhanced the mechanical strength and suppressed the formation of dendrites even with liquid electrolytes (Fig. 13ii). Considering the safety issue of batteries, Zhao et al.315 proposed a flexible anion-immobilized ceramic-polymer composite electrolyte, that is, polyethylene oxide (PEO) and lithium bis(trifluoromethylsulfonyl)imide (LiTFSI), for the application of Al-doped LLZTO. Fig. 13(ii(A) and (B)) demonstrates a potential electrolyte that guenched the formation of dendrite structures, which is attributed to the rigid nature of uniform ion distribution (due to the effective immobilization of anions). The demonstrated electrolyte was stable up to 5.5 V and used to fabricate batteries, achieving a specific capacity of 150 mA h g⁻¹. The internal health of the battery can provide a hint about the battery explosion, which can be prevented. D'innocenzo et al.316 developed a smart battery by changing the separator with a bifunctional separator (polymer-metal (Cu)-polymer triple layer configuration). This separator physically isolated the electrodes and reduced the voltage (Fig. 13iii-a and b). However, this type of separator did not stop the growth of dendrites, where the growth of dendrites increase with the time of cell operation, finally reaching the cathode.

To suppress the growth of dendrites on the Li-metal anode, generally the coating of a polymer and ceramic on the anode is performed, where the representative investigations are presented in Fig. 14(a) and (b). This strategy enabled the control of dendrite growth, but the low ionic conductivity of the polymer and poor interfacial contact remain a considerable drawback to the overall cell performance. 317 Thus, it becomes essential to prepare a suitable layer that provides faster ion diffusion and restricts the growth of dendrites. Xu et al. 318 prepared an artificial protective layer (APL) based on PVDF-HFP and LiF on the Li metal anode to suppress the growth of dendrites. Fig. 14(c) shows the uniform Li deposition on the soft polymer matrix. A full cell was fabricated using LFP as the cathode, APL-modified Li as the anode, and carbonate electrolyte of 1.0 M lithium hexafluorophosphate (LiPF₆)-ethylene carbonate/diethyl carbonate (v/v = 1:1). Initially, both cells (modified and unmodified Li anode) showed a capacity of 150.6 mA h g^{-1} with a Coulombic efficiency of >99%. After 50 cycles, the APL-modified cell demonstrated good cyclic stability up to 250 cycles with 80% capacity retention (Fig. 14d and e). In brief, the modified Li anode-based cells exhibited a 2.5-times longer cycle life than the unmodified anode. This approach may be very useful for the liquid electrolyte and a solid electrolyte, which can be adopted for the future design of Li-ion batteries.

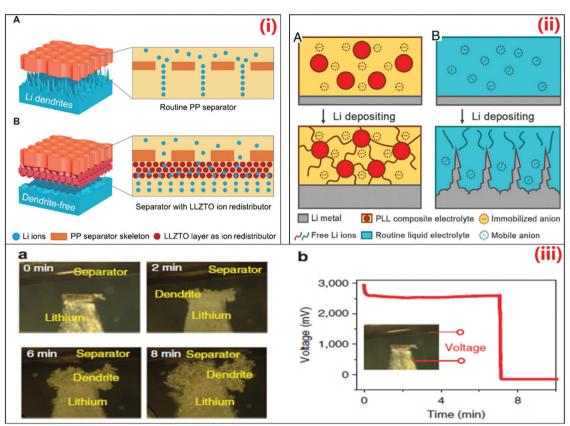


Fig. 13 (i) Schematic illustration of the electrochemical deposition behaviors of the Li metal anodes using (A) routine PP separator and (B) composite separator with the LLZTO layer as an ion redistributor for uniform Li-ion distribution. (ii) Schematic of the electrochemical deposition behavior of the Li metal anode with (A) PLL solid electrolyte with immobilized anions and (B) routine liquid electrolyte with mobile anions. 315 (iii) In situ observation of dendrite growth on lithium electrode. (a) Lithium anode and separator-wrapped lithium counter electrode with copper conductive layer facing the lithium anode housed in a glass cell for in situ optical microscopy observation. During charging of the cell, non-uniform deposition of lithium on the lithium electrode leads to mossy dendrite formation and growth on the surface. (b) Voltage profile of the device. The lithium dendrites contact the conductive copper layer on the separator within about 6-8 min, giving rise to a 3 V drop in VCu-Li, given that the potential difference between copper and lithium is dissipated on contact.³¹⁶ Reproduced with permission from Nature Publishing Group.³¹⁶

Besides the above-discussed strategies, some other strategies to moderate electrolytes include additive electrolyte, nanostructured electrolyte, solid electrolyte, and membrane modification. 101 However, although these strategies effectively suppress dendrite growth, there are some negative effects that restrict their use on a large scale. Thus, the best strategy may be the optimization of these factors to develop efficient and long life span batteries. Table 17 shows a comparison of the proposed methods to suppress Li dendrite growth. It seems that the use of solid electrolytes has the potential to suppress the dendrite issue, whereas the limit of ionic conductivity is one of the major drawbacks. Accordingly, the scientific community has focused on enhancing the ionic conductivity of solid electrolytes and developing commercial liquid electrolytes. In the next section, we explore the possible use of solid electrolytes for Li-ion batteries and how this has opened new doors for developing high-power density and long life span innovative batteries, i.e., all-solid-state Li-ion batteries (ASSLIBs).

4.3 Electrode/electrolyte interface (EEI) engineering

LIBs have various components that play a crucial role in deciding their performance. One of these crucial LIB components is recognized to be the electrode/electrolyte interface (EEI). The EEI is formed due to the decomposition of electrolytes and the electrode-electrolyte interactions, where (i) the interface generated on the negative electrode is the "solid electrolyte interphase" (SEI) and (ii) the interface generated on the positive electrode is the "cathode electrolyte interphase" (CEI). Generally, the effect of the cathode interface is smaller compared to that of the SEI. Two important challenges linked with the EEI are interfacial contact and chemical compatibility. In the EEI region, various phenomena occur such as charge transfer reactions, electrolyte decomposition, and electrode (cathode and anode) degradation. Thus, it becomes important to modify or tune the EEI for achieving optimum battery performances (high energy density, long cycle life, etc.). The EEI can be altered by varying the synthesis methods and engineering of the material. The quality of the EEI gives an idea about the safety and operation of the battery. An optimum EEI can be formed via three approaches, as follows: (i) minimizing the phase in the fabrication of the battery, (ii) enhancing the contact area by reducing the particle size and mixing the electrode and electrolyte, and (iii) addition of a buffer layer to enhance the chemical compatibility.320

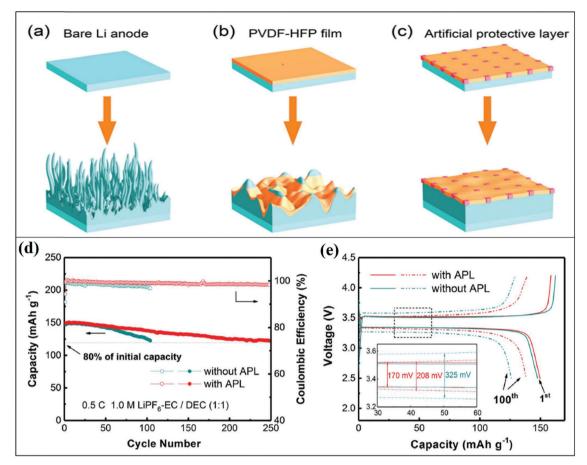


Fig. 14 Schematic illustrations of Li deposition: (a) without protection, lithium metal dendrites, and dead. Li forms after cycling. (b) Pure PVDF-HFP layer with poor mechanical modulus, where interfacial fluctuation with dendrites piercing the PVDF-HFP layer occurs after cycling. (c) With APL composed of organic PVDF-HFP and inorganic LiF, which is conformal and mechanically strong to suppress Li dendrite penetration and stabilize Li metal surface, and electrochemical performance of Li|LFP cells and morphology of cycled Li metal anodes. (d) Long-term cycling performance at 0.5C. (e) Galvanostatic charge-discharge profiles at the 1st and 100th cycle. 318 Reproduced with permission from Wiley-VCH. 318

Table 17 Comparison of proposed methods to suppress Li dendrite growth 319

	Advantage	Disadvantage
Electrolyte additive	(a) Facile operation (b) Forming a thin and highly conductive SEI	(a) Poor mechanical strength to suppress dendrite growth (b) Poor long-term stability during cycling
Super-concentrated	High Coulombic efficiency and cycling stability	(a) High price
Electrolyte		(b) Limited rate performance
Nanostructured electrolyte	High ionic conductivity	Complicated fabricating process
Solid-state electrolyte	(a) Without electrolyte leak (b) Suppressing dendrite growth	Low ionic conductivity
Structured anode	Suppressing Li dendrite growth	Low Coulombic efficiency
Membrane	(a) Stopping dendrites to the cathode	Less effect on the dendrite
Modification	(b) Detecting the dendrite growth	Nucleation and growth

The solid electrolyte interface (SEI) is an insulating film that covers the electrode surface to hinder the side reactions. Some key characteristics of the SEI film are, as follows: (1) high ionic conductance for ease of Li migration via the SEI, (2) stable morphology and chemical structure, (3) robust binding properties with active substances, (4) superior mechanical performance buffering volume expansion, and (5) superior electrochemical and thermal stability.³²¹ Fig. 15 displays the strategy to tune the interface in Li-ion battery by altering its structure.

Various fabrication techniques can be used to modify the surface of electrodes by creating a high-quality artificial buffer layer on the surface of SSE or/and electrode materials. The techniques classified based on this approach are (i) top-down approaches, including magnetron sputtering, spark plasma sintering, electron-beam evaporation, and pulsed laser deposition and (ii) bottom-up approaches, including sol-gel-derived synthesis, atomic layer deposition, chemical vapor deposition, and electrochemical-assisted synthesis.

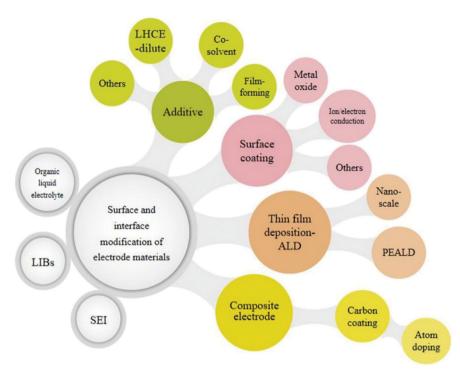


Fig. 15 Schematic diagram of surface-interface modification strategies and classification in organic liquid electrolytes for LIBs and map of this review (Fig. 2 from ref. 321).

Fig. 16(i) displays a typical schematic illustration of the SSB components and the interfacial challenges. Fig. 16(ii) shows the three types of interfaces (interphases), as follows: (i) intrinsically stable interface, where the solid-state electrolyte (SSE) is nonreactive with the Li metal and a distinct two-dimensional interface is formed (Fig. 16(ii)a) and (ii) solid-electrolyte interphase (SEI), with poor electron conductivity and desirable Li-ion conductivity (Fig. 16(ii)b). A perfectly stable interphase due to a selflimiting reaction between the SEI and Li effectively blocks electron transport. (iii) Mixed-conducting interphase, where the electronic conductivity is higher than the SSE (Fig. 16(ii)c). 322

Fig. 16(ii)d shows the potential drop from the SSE potential to Li metal at the interfaces for the first two types of SSEs, whereas the partial potential region of the third type of interphase drops below the potential of Li deposition. This drop indicates the growth of Li dendrites in the third type of interphase. The growth of dendrites is also attributed to the overpotentials during Li plating and the high electronic conductivity of SSEs. The high conductivity reduces the potential in the electron-conductive interphase (III' curve). By introducing artificial buffer layers (ABLs), nonreactive/reactive interface with an Li-stable interphase can be created. 323 The formation of an interface via this approach (between solid electrolyte and electrodes) provides enhanced chemical/electrochemical stabilities. By adding a compound with a special structure in the electrolyte, the properties of SEI can be tuned. Hogstrom et al. reported an increase in the irreversible capacity with the addition of an organic film-forming additive, propargyl methanesulfonate (PMS), and LiPF₆ in EC/DEC electrolyte. This was attributed to the better thickness of the SEI film. 324

Zheng et al. 325 used tris(pentafluorophenyl)borane (TPFPB), a boron-based anion receptor, to decrease the side products on the cathode surface. The high coordination ability and high oxygen solubility of TPFPB restricted the electrolyte decomposition and enhanced the stability of the electrode-electrolyte interface. The surface chemistry of the electrode determines the SEI, which can be monitored by coating the electrode surface to form a stable structure.326 Initially, mostly metal oxides (Al2O3, TiO2, and Co₃O₄) are used as a coating material, which play two key roles, as follows: (i) preventing electrode decomposition by reacting with the acid species present in the electrolyte and (ii) preventing direct contact between the two electrodes.327-329

The metal oxide coating affects the conductivity, and thus an alternative strategy is to use a lithium-ion conductive-material such as Li₃PO₄³³⁰ and Li_{0.1}B_{0.967}PO₄ (LBPO). Another strategy is to deposit a thin film via physical vapor deposition (PVD), chemical vapor deposition (CVD), molecular beam epitaxy (MBE), spin coating, and atomic layer deposition (ALD).332,333 Coating carbon on the electrode surface has also been shown to be efficient due to three actions, as follows: (i) enhancing the electrochemical performance, (ii) hindering the agglomeration of the electrode material for optimum use of the sites in the active material, and (iii) acting as a buffer layer to relieve the stress due to volume changes. 334,335

5. Overview of all-solid-state Li-ion batteries (ASSLIBs)

The optimization of the architecture is one of the key points for all-solid-state Li-ion batteries (ASSLIBs). ASSLIBs have an

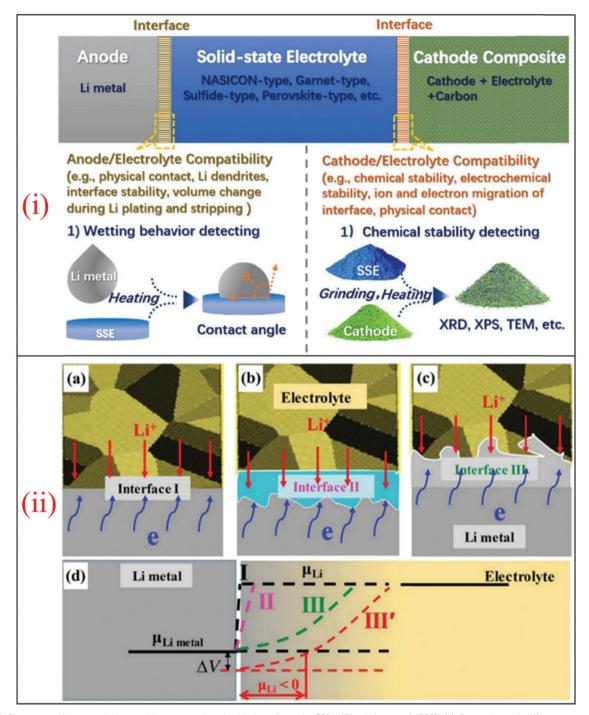


Fig. 16 (i) Summary of compatibility problems associated with interfaces in SSBs (Fig. 1 from ref. 322). (ii) Formation of different types of Li/SSE interphases. (a) Intrinsically stable interface between the Li metal and the SSE. (b) Metastable solid-electrolyte interphase between the Li metal and the SSE. (c) Reactive mixed-conducting interphase between the Li metal and the SSE. (d) Corresponding Li potentials between the Li metal and different SSEs. 322

inherent property for safety owing to the absence of flammable electrolytes. Further, the energy density and cycle stability are superior to the commercial LIBs.336 Heavy packaging makes batteries safer for commercial applications; however, it decreases their energy density. Fig. 17(i) and (ii)(a,b) show the key differences between the commercial LIBs and ASSLIBs in terms of their architecture. In ASSLIBs, a separator is not required, thus automatically opening the door for device miniaturization and weight/price reduction. The use of solid electrolytes eliminates all the barriers faced by commercial batteries such as dendrite growth (cause short-circuit), poor thermal stability, and poor safety. Another attractive feature of ASSLIBs is that they can be used as an anode with solid electrolytes. In commercial batteries, the liquid electrolyte

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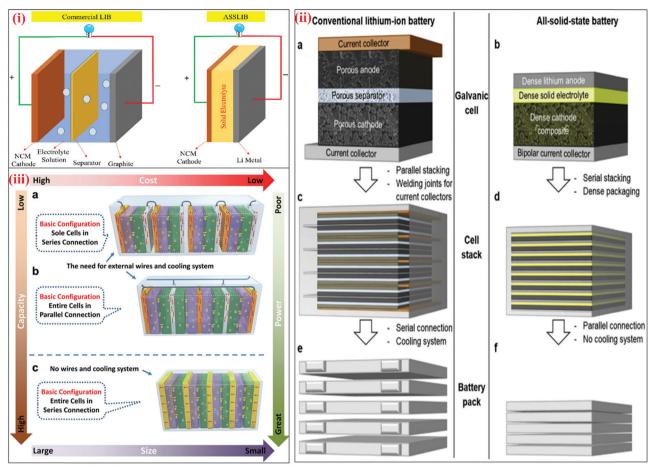


Fig. 17 (i) Architectural comparison of commercial LIB and all-solid-state LIB. (ii) Comparison of conventional lithium-ion battery and all-solid-state lithium battery at the cell, stack, and pack levels with potentials for increased energy density. (iii) Schematic illustration of the stack configuration in rechargeable batteries: (a) SEs, (b) MEs, and (c) BEs. The direction and intensity of the red arrow represent the discharging current. 337 Reproduced with permission from Wiley-VCH.337

interconnects all battery cell components with a parallel connection inside the cell stack (Fig. 17(ii)(c)). However, in allsolid-state batteries (ASSBs), the electrolyte is confined inside the galvanic cells and they enable bipolar stacking with single cells connected in series by a lithium-ion isolating layer.³³⁷ The bipolar stacking decreases the number of current collectors and increases the voltage of the battery cell (Fig. 17(ii)(d)). Also, the absence of a flammable electrolyte solvent in ASSBs eliminates the need for any type of cooling elements, as shown in Fig. 17(i).

The commercial advancement of fabricated LIBs depends on the optimization of their performance parameters. The electrochemical performance of the battery is indicated in terms of internal resistance, specific capacity, efficiency, capacity retention, and open-circuit voltage. Additionally, the measurement conditions (environment temperature and state of charge/discharge) need to be considered during electrochemical testing. Depending on the energy density demand, the capacity, material loading, thickness, and electrolyte uptake can be tuned. Table 18A summarizes the various performance parameters (top: Ionic conductivity, mechanical strength, interfacial functionality, safety, advantages and disadvantage and bottom: liquid, gel, SSP, and ceramic electrolytes)

and information that can be extracted from any LIB, that is, measuring unit and formula and information (Table 18B).

Using the existing materials, cell optimization (single electrodes, SEs and monopolar electrodes, MEs) can enhance the specific energy from 80 W h kg⁻¹ to 200 W h kg⁻¹.³⁴¹ The cell configuration allows the encapsulation of a greater amount of active materials, which significantly enhances the capacity and reduces the cost and size. Nowadays, bipolar electrodes (BEs) are also gaining attention, as shown in Fig. 17(iii)(c). Here, the cathode and anode slurries are separately coated on both sides of the substrate. This substrate allows the smooth migration of electrons with a lower ohmic resistance and homogeneous current distribution. The BEs demonstrated a superior specific energy, specific power, capacity, and voltage in contrast to SEs and MEs. 342 Overall, it can be concluded that ASSLIBs are safer and reliable compared to all commercial LIBs.

Three possible configurations are discussed, as follows: (i) all three components (cathode, anode, and electrolyte) in solid form, (ii) liquid/polymer-based cathode together with solid electrolyte and anode, and (iii) cell with cathode and the separator only (here anode formation occurs after the first

Table 18 (A) (top) Ranking of properties of Li-battery electrolytes (1 = best and 4 = worst). (bottom) Comparison of the advantages and disadvantages of different electrolytes. (B) Essential parameters for testing the performance of a lithium-ion cell (45,340)

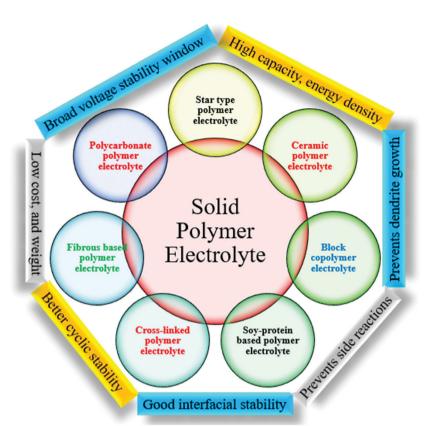
Electrolyte	Ionic conductivity	Mechanical strength	Price	Interfacial functionality	Safety
Liquid	1	4 (needs separator)	3	1	4
Gel	2	3	2	2	3
Polymer	4	2	1	3	2
Ceramic	3	1	4	4	1

Ceramic 5		-	4 1
Classification		Advantages	Disadvantages
Liquid		High ionic conductivity	Poor thermal stability
		Low interfacial impedance	Severe LiPS shuttling
Gel		High ionic conductivity	Poor thermal stability
		Low interfacial impedance	Low mechanical strength
		Suppressing LiPS shuttling	
Solid-state polymer		Low interfacial impedance	Low ionic conductivity
		Suppressing LiPS shuttling	Low mechanical strength
		Good thermal stability	
Ceramic		High ionic conductivity	High interfacial impedance
		Excellent thermal stability	Poor processability
		Preventing LiPS shuttling	
		Suppressing Li dendrite growth	
Polymer/ceramic compos	site	Low interfacial impedance	Low ionic conductivity
		Good thermal stability	
		Suppressing LiPS shuttling	
		Suppressing Li dendrite growth	
Parameters	Measuring unit	Measuring formula	Information
Operating voltage	Volts (V)	Instrumental	Energy density and safety
Current density	mA g ⁻¹	Instrumental	For testing rate capabilities
Theoretical capacity	$\mathrm{mA}\ \mathrm{h}\ \mathrm{g}^{-1}$	$F \times x$	Lithium ion storage capability
1 7	Ü	$TC = \frac{T \times x}{2.6 \times MM \times n}$	0 1 1

Operating voltage Current density $mA \ g^{-1}$ $mB \ g^{$	Operating voltage	Volts (V)	Instrumental	Energy density and safety
Theoretical capacity mA h g^{-1} $\text{TC} = \frac{F \times x}{3.6 \times \text{M.M} \times y}$ Lithium ion storage capability Gravimetric capacity mA h g^{-1} $C = \frac{I(\text{mA}) \times t(\text{h})}{m(\text{g})}$ Li ⁺ storage capability measured per unit mass Areal capacity mA h cm^{-2} $C = \frac{I(\text{mA}) \times t(\text{h})}{M(\text{cm}^2)}$ Li ⁺ storage capability measured per unit area Volumetric capacity mA h cm^{-2} $C = \frac{I(\text{mA}) \times t(\text{h})}{A(\text{cm}^2)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit volume $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit volume $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit volume $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit volume $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ How much energy can be extracted $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Rate of charging/di	Current density	$mA g^{-1}$		For testing rate capabilities
Gravimetric capacity $\operatorname{mA} \operatorname{h} \operatorname{g}^{-1}$ $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{m(\operatorname{g})}$ Li ⁺ storage capability measured per unit mass $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{m(\operatorname{g})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{cm}^2)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{cm}^2)}$ Li ⁺ storage capability measured per unit volume $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{cm}^2)}$ Li ⁺ storage capability measured per unit volume $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{cm}^2)}$ Li ⁺ storage capability measured per unit volume $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{cm}^2)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{cm}^2)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{cm}^2)}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = \frac{I(\operatorname{mA}) \times t(\operatorname{h})}{I(\operatorname{mA})}$ Li ⁺ storage capability measured per unit area $C = $	Theoretical capacity	$\mathrm{mA}\ \mathrm{\bar{h}}\ \mathrm{g}^{-1}$	$TC = \frac{F \times x}{3.6 \times M.M \times y}$	Lithium ion storage capability
Areal capacity mA h cm^{-2} $C = \frac{I(\text{mA}) \times t(\text{h})}{A(\text{cm}^2)}$ Li^+ storage capability measured per unit area Volumetric capacity mA h cm^{-2} $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ Li^+ storage capability measured per unit volume $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}^3)}$ $C = \frac{I(\text{mA}) \times t(\text{h})}{V(\text{cm}$	Gravimetric capacity	mA h g ⁻¹		Li ⁺ storage capability measured per unit mass
Volumetric capacity $\operatorname{mA} \operatorname{h} \operatorname{cm}^{-2}$ $C = \frac{I(\operatorname{mA}) \times I(\operatorname{h})}{V(\operatorname{cm}^3)}$ Li* storage capability measured per unit volume $C = \frac{I(\operatorname{mA}) \times I(\operatorname{h})}{V(\operatorname{cm}^3)}$ Li* storage capability measured per unit volume $C = \frac{I(\operatorname{mA}) \times I(\operatorname{h})}{V(\operatorname{cm}^3)}$ How much energy can be extracted or W h cm ⁻³ $C = I(\operatorname{mA}) \times I(\operatorname{mA})$ How fast the energy can be extracted or W cm ⁻³ $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{V(\operatorname{cm}^3)}$ Rate of charging/discharging $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{V(\operatorname{mA})}$ Rate of charging/discharging $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{V(\operatorname{mA})}$ Reversible capacity $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{V(\operatorname{mA})}$ Reversible capacity and $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ If SOH < 80%, battery need to be replaced $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity of the battery $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity $C = \frac{I(\operatorname{mA}) \times I(\operatorname{mA})}{I(\operatorname{mA})}$ Reversible capacity $C = \frac{I(\operatorname{mA}) \times I($	Areal capacity	mA h cm ⁻²		Li ⁺ storage capability measured per unit area
Specific energy $W h g^{-1} \text{ or } W h \text{ cm}^{-2}$ $E = C \times V$ How much energy can be extracted or $W h \text{ cm}^{-3}$ $W g^{-1} \text{ or } W \text{ cm}^{-2}$ $P = I \times V$ How fast the energy can be extracted or $W \text{ cm}^{-3}$ $C_{\text{rate}} = \frac{J(\text{mA g}^{-1})}{C(\text{mA h g}^{-1})}$ Rate of charging/discharging Coulombic efficiency $ \%E = \frac{C_{\text{charging}}}{C_{\text{discharging}}} \times 100$ Reversible capacity State of health $ SOH = \frac{Q_{\text{m}}}{Q_{\text{r}}} \times 100\%$ Q_{r} —rated capacity and Q_{m} —current maximum available capacity of the battery If SOH $<$ 80%, battery need to be replaced R_{e} —internal resistance under the current state; R_{e} —internal resistance of the battery when it reaches the end of life; and R_{n} —internal resistance	Volumetric capacity	mA h cm ⁻²		Li ⁺ storage capability measured per unit volume
Power density $W g^{-1}$ or $W cm^{-2}$ or $W cm^{-2}$ or $W cm^{-3}$ h ⁻¹ $C_{rate} = \frac{J(mA g^{-1})}{C(mA h g^{-1})}$ Rate of charging/discharging Coulombic efficiency $ \%E = \frac{C_{charging}}{C_{discharging}} \times 100$ Reversible capacity State of health $-$ SOH $= \frac{Q_m}{Q_r} \times 100\%$ Q_r —rated capacity and Q_m —current maximum available capacity of the battery If SOH $<$ 80%, battery need to be replaced R_c —internal resistance under the current state; R_c —internal resistance of the battery when it reaches the end of life; and R_n —internal resistance	Specific energy	W h g ⁻¹ or W h cm ⁻² or W h cm ⁻³		How much energy can be extracted
$C_{\text{rate}} = \frac{C_{\text{rate}}}{C(\text{mA h g}^{-1})}$ $\%E = \frac{C_{\text{charging}}}{C_{\text{discharging}}} \times 100$ $State of health - SOH = \frac{Q_{\text{m}}}{Q_{\text{r}}} \times 100\%$ $SOH = \frac{R_{\text{e}} - R_{\text{n}}}{R_{\text{e}} - R_{\text{n}}} \times 100\%$ $Reversible capacity$ $Q_{\text{r}} - \text{rated capacity and } Q_{\text{m}} - \text{current maximum available capacity of the battery}}$ $If SOH < 80\%, \text{ battery need to be replaced}$ $R - \text{internal resistance under the current state;}$ $R_{\text{e}} - \text{internal resistance of the battery when it reaches the end of life; and } R_{\text{n}} - \text{internal resistance}}$	Power density	W g ⁻¹ or W cm ⁻²	$P = I \times V$	How fast the energy can be extracted
State of health — $SOH = \frac{Q_{\rm m}}{Q_{\rm r}} \times 100\%$ $Q_{\rm r}$ available capacity and $Q_{\rm m}$ —current maximum available capacity of the battery If SOH $< 80\%$, battery need to be replaced R—internal resistance under the current state; $R_{\rm e}$ —internal resistance of the battery when it reaches the end of life; and $R_{\rm n}$ —internal resistance	$C_{ m rate}$	h ⁻¹	$C_{\text{rate}} = \frac{J(\text{mA g}^{-1})}{C(\text{mA h g}^{-1})}$	Rate of charging/discharging
State of health — $SOH = \frac{Q_{\rm m}}{Q_{\rm r}} \times 100\%$ $Q_{\rm r}$ available capacity and $Q_{\rm m}$ —current maximum available capacity of the battery If SOH $< 80\%$, battery need to be replaced R—internal resistance under the current state; $R_{\rm e}$ —internal resistance of the battery when it reaches the end of life; and $R_{\rm n}$ —internal resistance	Coulombic efficiency	_	$\%E = \frac{C_{\text{charging}}}{C_{\text{discharging}}} \times 100$	Reversible capacity
Internal resistance — $SOH = \frac{R_{\rm e} - R}{R_{\rm e} - R_{\rm n}} \times 100\%$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$ $= \frac{R_{\rm e} - internal resistance}{R_{\rm e} - internal resistance}$	State of health	_		
of the new battery.	Internal resistance	_	$SOH = \frac{R_e - R}{R_e - R_n} \times 100\%$	R —internal resistance under the current state; $R_{\rm e}$ —internal resistance of the battery when it reaches the end of life; and $R_{\rm n}$ —internal resistance
				of the new battery.

charge). The lithium-polymer differentiates itself from conventional battery systems in terms of the type of electrolytes used. In the original design back in the 1970s, a dry solid polymer electrolyte was used. This electrolyte resembles a plastic-like film, which does not conduct electricity but allows ion exchange (electrically charged atoms or groups of atoms). The polymer electrolyte replaces the traditional porous separator soaked in the electrolyte. Therefore, different types of electrolytes have been used. The solid electrolyte will provide only advantages, such as smaller size and higher energy density. 305,343,344 To achieve the characteristic parameter of polymer electrolytes, a different strategy was carried out by using a different polymer. Fig. 18 summarizes different architectures of polymer electrolytes that hold potential to replace the existing liquid electrolyte for developing an efficient and safe battery.

Ceramic-polymer electrolytes are prepared by adding nanoparticles to the polymer salt matrix. The addition of nanoparticles enhances the conductivity and thermal and mechanical properties owing to the Lewis-acid-based interaction of the surface groups of the nanofiller with the polymer and salt. The oxygen in



Different types of solid polymer-based electrolytes and their corresponding performances.

the surface groups (-OH) of the nanofiller also provides additional conducting sites for cation (Li^+) migration. $^{345-347}$ Another important and unique architecture block is the copolymer electrolyte, which is comprised of covalently bound polymers. It improves the electrical properties and stability compared to the individual polymer. 348,349 Polycarbonate (PC)-based solid polymer electrolytes are another category of electrolytes that have attracted significant attention. Given that amorphous content is desirable for fast ion conduction in polymer electrolytes, PC-based electrolytes have a high amorphous content, good chain flexibility, and a high dielectric constant. Overall, they can enhance the cation transport number and broad voltage stability window. 350,351

The ionic conductivity, voltage stability window, and ion transference number are three crucial parameters to enhance the overall cell performance. The ion transport is favored by the presence of amorphous content and segmental motion of the polymer chain. To promote faster ion migration, the crystallinity needs to be minimized (for faster segmental motion). The polymer must have a low glass transition temperature to achieve conductivity comparable to liquid electrolytes (10⁻⁴ S cm⁻¹). Ionic conductivity is directly linked to several free-charge carriers participating in the conduction. Thus, the salt dissociation in polymer electrolytes needs to be improved by the addition of nanoparticles (NPs). The surface interactions among the polymer, salt, and NPs alter the environment of the ions and ionic conductivity. For polymer electrolytes, both cations and anions are mobile, where the mobility of cations is

lower (than anions) due to their migration via the coordinating sites of the polymer matrix. The ratio of migrating Li⁺ to all the migrating ions including anions in the electrolyte is defined as the Li-ion transference number (LITN). For the optimum performance of the cell, the LITN must be high, which in the ideal case is 1. A high cation transference number also eliminates the issue of concentration polarization. By restricting the migration of anions via the addition of nanofillers, the cation migration can be improved. 352 High ionic conductivity is crucial to achieve high charge/discharge rates. Another important parameter is the voltage stability window of the electrolytes, which limits the charge and discharge characteristics of the electrode materials in a particular voltage range. For this voltage window, the polymer electrolytes must be stable to achieve the optimum performance. The polymer electrolyte must be thermally stable and should not show any signs of shape/volume change, shrinkage, or melting.

Cross-linking is an effective strategy to prepare novel polymer structures, offering an enhancement in the mechanical, electrical, and voltage stability properties. The physical and topological properties are further improved by using a new architecture based on star polymers, where this is attributed to the presence of outer spheres of arms, which enhance the ion mobility and conductivity. The presence of various branching points interrupts the polymer re-crystallization tendency and enhances the ion migration owing to their high flexibility. High surface area fiber-based polymer membranes are also being

 Table 19
 Comparison of the electrode, electrolyte, and cell performance parameters for ASSLIB

	Cathode	Anode	ESW (V)	$\begin{array}{c} \text{port} \\ \text{number} \left(t^{^{+}} \right) \end{array}$	Electrolyte conductivity (S cm^{-1})	Specific capacity (mA h g^{-1}) Capacity retention	Capacity retention	Efficiency	Ref.
POSS/LiTFSI/(P(EO-co-PO)) L	LFP	Li	5.1	0.62	$1.1 imes 10^{-4}$ at 25 $^{\circ}$ C	160 (at 25 °C) at 0.1C	75% at 0.3C after 100	$\sim\!100\%$	357
I	LFP	Ľį	4.99	I	3.23×10^{-4} at 25 °C and 8.58×10^{-4} at 45 °C	at 25 $^{\circ}$ C and 160.1 after 200 cycles at at 45 $^{\circ}$ C $^{\circ}$ C 0.4C	99.1% after 200 cycles	I	358
PEO-LiClO ₄ -g-C ₃ N ₄ L	LFP	Ľi	4.8	0.37	$ imes 10^{-5}$ at 25 °C	161.2 (at 1C)	81% after 200 cycles	99.7%	359
Functional gradient SPE L	LFP	Ľį	5.3	0.62	$2.45 imes 10^{-4}$ at $25^{\circ} \mathrm{C}$	163.2 (at 0.1C)	$^{ m at}$ 10.5% mA h $^{ m g}^{-1}$	95.3%	360
Garnet Si-Li,La ₃ Zr ₂ O ₁₂ N	NCM811 LFP	33	I	I	$6.68 imes 10^{-4}$ at $25~^{\circ} \mathrm{C}$	137 after 100 cycles	69.5% after 100 cycles	99.0% at 50 °C 98.5% after 100 cycles	361
	LFP	: ::	4.2	I	$1.6 \times 10^{-4} ({ m at \ RT})$ 1.14 × 10 ⁻³ (at 80 °C)	152 (at C/3), \sim 125 (affer 30th cycle)			362
P(VDF-HFP)-(PE-PM-PVH) L	LFP	Ľi	~ 5	0.72	0.81×10^{-3} (a. 30 °c)	(acc) (acc) (after 100th (acc))	%86	%66	363
	CCO	Graphite		1	$1.04 \pm 0.05 \times 10^{-3}$	134	93% (after 100th cycle)	I	364
PAN/PEO/PDMA I PVDF-co-HFP/oligomeric Liquide	LFP LFP	:: ::	4.5 4.5	0.58	$0.67 imes 10^{-3} \left(30\ ^{\circ} \mathrm{C} ight) \ 0.12 imes 10^{-3} \left(\mathrm{RT} ight)$	154 (at 0.1C) 152 (at 0.1C)	ı	— 99% (after 100th	365 366
DPC/LiTFSI/LAGP L PPC/LiTFSI/LAGP I PPC/LiTFSI I PPC/LI	LFP LATP.	:: :::	4.5	0.75	1×10^{-4}	138.3 at 0.1C	97.1% after 100 cycles	cycre) 	367
10 -	Coated	1							
Nanofiber-reinforced I	LFP	Ľį	4.5	I	1×10^{-4}	159 at 70 $^{\circ}$ C		%66<	369
	LFP	Li	4.8	0.50	0.53×10^{-3} at 23 °C,	\sim 134 at 1C	100% after 150th cycle	%86 <	370
PEO-LiTFSI/PI-g-PEO Lanofiher	LFP	Li	5	0.45	1.0×10^{-4} at 40 °C	140 at 0.05C	$120 \text{ mA h g}^{-1} \text{ after}$	99% at 0.05C	371
PVDF/LLTO-PEO/PVDF I 9-Type PS ₄ /Li ₃ PS ₄ I	LCO LFP	E E	5 5.1 (in situ)	0.67/0.70 0.33 (in situ)	$\sim 3.01 imes 10^{-3} \ 8.01 imes 10^{-4} \ (in situ)$	144 (at 1C) 153 (at 0.1C)	91.8% (after 100th cycle) 86.1% (after 100th cycle)	1.1	372 373
			4.9 (mechanical- mixing	0.28 (mechanical- mixing	6.98×10^{-4} (mechanical-mixing 60 °C)	,	85.9% (after 325th cycle)		
1	LFP	Ľ	5		$1.17 \times 10^{-4} ({ m at \ 30 \ ^{\circ}C})$	149.1 (at 0.1C), 139.1	I	100% (after 50th	374
I	LFP	Li	4.3	I	$0.16 \times 10^{-3} (30 ^{\circ} \text{C}),$	146.5, 144.5 (after	I	99%, 99.7%	375
PEO/LiTFSI/LLZO	LFP	Ľ	5.7	0.207 (at 60 °C)	$0.7 imes 10^{-3} \ (60\ ^{\circ}{ m C}) \ 5.5 imes 10^{-4} \ (30\ ^{\circ}{ m C})$	100th cycle) (at 0.2C) 150.1 (after 3 cycles); 149.5 (after 50 cycles), 121	93.2% (after 1st), 89 (after 100th cycle)	(after 100th cycle) 98.9%	376
PEO-PPC-LiTFSI-LLTO	LFP	Li	5.1	0.227	$5.66 \times 10^{-5} (at 25 ^{\circ}C),$ 5.7 × 10 ⁻⁴ (at 80 $^{\circ}C)$	(alter 100 cycles) 135 (at 0.5C), 130 (after 100th ewele)	%96	100%	377
PEO-LiTFSI/g-C ₃ N ₄ LFP BCP with PS and Jeffamine LFP	LFP LFP	Ľ.	4.7 5.8	0.56 0.08 (at 70 °C)	$1.7 \times 10^{-5} \ (\text{at } 30 \ ^{\circ}\text{C})$ $5.6 \times 10^{-4} \ (\text{at } 70 \ ^{\circ}\text{C})$,	(act 155 (after 150th Cy.) 140 (after 1st cycle)	1 1	99.5% 100% (after 30th)cycle	378 379
>	V_2O_5	Ľi	I	I	2×10^{-7} (at 25 °C)	11 μ A h cm ⁻² (areal	I		380
PEC/LiFSI Multi block copolymer (SI) N	LFP NCM	EE	5 4.8/4.9	0.5	$2.5 imes 10^{-5} ({ m at \ 30 \ ^{\circ}C})$ $3.2 imes 10^{-4}$	capacity) 120–130 (at C/10) 150 (at C/20)	%98 —	99.5% (after	381 382
I	LFP	Ľį	4.5 (80 °C)	0.45 (at 80 $^{\circ} \text{C})$		128 (at 0.2C	9% (after 100th cycle)	100%	383

Table 19 (continued)

				Cation trans-	Electrolyte conductivity				
Electrolyte	Cathode	Anode	ESW(V)	number (t^{+})	$({\rm S \ cm^{-1}})$	Specific capacity (mA h $\rm g^{-1})$ Capacity retention) Capacity retention	Efficiency	Ref.
PCPU/PCDL/HDI/DEG/ LiTFSI					2.2×10^{-6} (at 25 °C), 1.58×10^{-5} (at 60 °C) 1.12×10^{-4}	127 (after 100th cycle)	91% (after 600th cycle)		
WPU/PEG/HDI	LFP	Ľi	4.8 V (60 °C)	1	$egin{array}{l} ({ m at}\ 80\ ^{\circ}{ m C}) \ 7.3 imes 10^{-4} \ ({ m at}\ 60\ ^{\circ}{ m C}) \ 2.2 imes 10^{-3} \ ({ m at}\ 80\ ^{\circ}{ m C}) \end{array}$	151 (at 0.1C),	97% (after 50th cycle)	I	384
Polypoly(e-caprolactone)	LFP	Ľ	I	0.66 (at 60 °C),	4.1×10^{-5} (at 25 °C)	150 (at C/50),	I	100%	385
OV-POSS/PEGMEM	LFP	Li	5.31 (SCP5.1) 5.04 (LSP5.1)	0.35 (SCP5.1) 0.19 (LSP5.1)	$1.13 \times 10^{-4} \ (ext{SCP5.1}), \ 5.63 \times 10^{-5} \ (ext{LCP5.1})$	163.8, 147.8 (after 100th cycle)	90.2%	100%	
PEGDMA ₅₅₀ (Li-SPE550-Li)) LFP	ΙΪ	5.4	0.30	$2.82 \times 10^{-5} (ext{at } 20 ^{\circ} ext{C})$	137.7, 130.5 (after 150th cycle)	95%	97% (after 1st cycle), 98% (after 150th	386
$(HBPS-(PTFEMA-b-PPEGMA)_{1}/IJTFSI$	LFP	Ľi	4.9	0.26	2.36×10^{-5} (at 25 °C), 4.1 × 10 ⁻⁴ (at 80 °C)	139, 147 (after 5th Cy.)	1	100% (after 100th excle)	387
PEGMA/DLC-((PS) ₂₃) ₆ / LiTFSI	LFP	ij	5.1 (30 °C)	0.37	$1.94 \times 10^{-4} ({ m at \ 30 \ ^{\circ}C}),$	(ac 5.15, 50 5) 139 (at 0.1C), 130 (after 50th cycle) (at 60 °C)	I	cycle) c7% (97% (90%)	388
PEO-LiTFSI/LLTO	LFP	Ľi	4.5	0.33	$1.8\times10^{-4}(\mathrm{at\;RT})$	80 (at 0.3C), 25 $^{\circ}$ C	ı	90–100%	389
PVDF-HFP/LiTFSI/ LLZO nanofibre	LFP	Ľi	5.2	I	$9.5 imes10^{-4} \left({ m at}~20~^{\circ}{ m C} ight)$	140 (at 0.2C)	93% (after 150th cycle (Xv. at 0.5C)	%6.66	390
$\rm PEOEC/LiClO_4/OA\text{-}POSS$	V_2O_5	Ξ.	5.0	I	3.74×10^{-5} (at 30 °C),	280	$\sim 100\%$ (after 30 cycles)	I	391
PAN/SiO ₂ (MA-SiO ₂)/TEGDA NCM	A NCM	Graphite		I	2.25 × 10 (at 50 5) 1.1 × 10 ⁻³ (non-porous), 179.5, 157.9 (after 300 1.8 × 10 ⁻³ cycles) (mesonorous)	179.5, 157.9 (after 300 cycles)	88.0% (for mesoporous)	I	353
PEGDA/DVB PEG/LiTFSI/RTIL	LFP NMC	E E	5.4.8	0.23	1.4×10^{-4} 4×10^{-4} (at 25 °C), 1.45×10^{-3} (at 65 °C)	123, 138 (after 20 cycles) 118 (at C/10)	1.1	%66 —	392 393
PEO-TEGDMA-TEGDME	LFP	Ľ	5.38	0.56	$2.7 \times 10^{-4} (\text{at } 24 ^{\circ}\text{C})$	160 (at 0.05C)	98.8% (after	1	393
PEO/acryl-HBP/PEGDME	LFP-C	${ m Li}_4{ m Ti}_5{ m O}_1$	${ m Li_4Ti_5O_{12}}$ 4.5 (30 $^{\circ}{ m C})$	0.33 (at 30 °C)	1.24×10^{-4} (at 20 °C), 1.97×10^{-3} (at 80 °C) for benzoyl peroxide	140 (at C/10)		%96	394
PEO/acryl-HBP/PEGDME	LFP-C/Al (Full cell)	Cu/LTO	Cu/LTO 4.5 (30 °C)	0.33 (at 30 °C)	2.44 $\times 10^{-4}$ (at 25 °C), 3.22 $\times 10^{-3}$ (at 80 °C). For	42 (at C/10)	80% (after 340th cycle)	I	394, 395
PEO; UHMWPEO-LiClO ₄ / core-shell protein@TiO ₂ NW	(2° 58)	Ľi	5.4	0.62 & 0.41 (PEO only)	$1.1 imes 10^{-4} (ext{at RT}), \ 2 imes 10^{-3} (ext{at } 80 {}^{\circ} ext{C})$	135 (at 0.2C)	94.7% (after 70 cycles)	98.6%	
PEO-LiTFSI/MXene $(Ti_3C_2T_x)$	LFP (60 $^{\circ}$ C) Li) Li	5.2	0.18	$2.2 \times 10^{-5} ({ m at} \ 28 \ ^{\circ}{ m C}), \ 0.69 \times 10^{-3} ({ m at} \ 60 \ ^{\circ}{ m C})$	150 (at C/10)	91.4% (after 100th cycle)	>97% (after 100th cycle)	396
$ m PEO-LiClO_4-lepidolite$	LFP	Ľ	9	0.72	$1.39 \times 10^{-6} \ ({ m at \ RT}), \ 1.23 \times 10^{-4} \ ({ m at \ 60 \ ^{\circ}C})$	120 (at 0.15C)	I	100%	397

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Table	

Electrolyte	Cathode	Cathode Anode ESW (V)	ESW (V)	Cation transport Electrolyt (t^+) $(S \text{ cm}^{-1})$	Electrolyte conductivity (S cm $^{-1}$)	Specific capacity (mA h g^{-1}) Capacity retention) Capacity retention	Efficiency	Ref.
PEO-LiTFSI/vermiculite clay sheets	LFP	Ľi	5.35 (25 °C), 5.0 (100 °C)	0.246 (at 25 °C) 0.497 (at 90 °C)	0.246 (at 25 °C), 2.9 × 10 ⁻⁵ (at 25 °C), 159.9 (at 0.1C) 0.497 (at 90 °C) 1.2×10^{-3} (at 60 °C), 3.1×10^{-3} (at 60 °C), $(31 \times 100^{\circ})$	159.9 (at 0.1C)	I	I	398
PEO-LiTFSI/Vertically aligned vermiculite sheets	LFP	Li	1	0.47 (at RT)	1.89×10^{-4} (at 25 °C) 167 (at 0.1C)	167 (at 0.1C)	82% (after 200th cycle)	I	399
PEO-LITFSI-PAGP	LFP	Ľ.	5.0	1	1.6×10^{-5}	100 (at 0.1C)		> 99.5%	400
POSS-IL.s	LFP	Li	5.0	I	$8.0 \times 10^{-4} \ ({ m at} \ 22 \ ^{\circ}{ m C}) \ 2.0 \times 10^{-3} \ ({ m at} \ 62 \ ^{\circ}{ m C})$	136.3	1	1	401
PEO-LIX-LAO	LFP	Ľ	5.2	1	$1.36 imes 10^{-5} (ext{at } 30 \ ^\circ imes)$	153.1	1	%26	402
PEO/LiBOB/LLZTO	LFP	Li	~ 5.0	0.57	,	165.9	1		403
PEO-Zn (BEH)	LFP	Li	4.2	0.5 (at 60 °C)	0.5 (at 60 $^{\circ}$ C) 1.1×10^{-5} (at 30 $^{\circ}$ C), 2×10^{-4} (at 60 $^{\circ}$ C)	125, after 100th cycle at 0.1C	84% after 100th cycle	1	404
Li ₆ PS ₅ Cl/poly(ethylene oxide)	NCM	Li	I	I	$1 imes 10^{-3}$ (110.2 (at 60 °C)	91% over 200 cycles at 0.05C (at 30 $^{\circ}$ C)	I	405
LLZTÓ/PEO	LFP	Ľi	5.5	0.41	$1.22 \times 10^{-4} ({\rm at \ 30 \ ^{\circ}C}) 151.1 ({\rm after \ 200 \ cycles})$	151.1 (after 200 cycles)	98% after 200 cycles at 0.5C	99.5%	406
PVDF-PAN-ESFMs	CO	Ľ	5.1	I	$7.8 \times 10^{-3} ({ m at} \ 25 {}^{\circ}{ m C})$	120.4 (at 0.1C	93% (after 150th cycle)	I	407

investigated, which are better than linear polymers. They provide faster ion migration, a broad voltage window, and good interfacial contact.353,354 A new approach is using bio-based polymers such as soy-protein (SP). The ammonium group on SP interacts with the polymer chains and disrupts the crystallization tendency, which enhances the ion dynamics. 355,356 Table 19 compares the properties of different types of electrolytes.

The binder also plays an important role in the cell performance and its stability. Generally, polyvinylidene fluoride (PVDF) is used as an insulating binder. The cell performance can be amplified by replacing it with a conducting material such as lithium polyacrylate (PAALi) as a binder, which is solid up to 200 °C. Recently, He et al. 408 fabricated ASSLIBs using LNMO as the cathode, RuO2 as the anode, and an ionic conductive thermosetting material (PAALi) as the binder. Fig. 19(a) shows the full-cell ASSLIB with the structure of LNMO/LAGP/ RuO₂. The NASICON-structured Li_{1.5}Al_{0.5}Ge_{1.5} (PO₄)₃ (LAGP) was used as a solid-state electrolyte. The ionic conductivity of the ASSLIB was determined to be $1.03 \times 10^{-4} \, \mathrm{S \, cm^{-1}}$. Fig. 19(b) shows the discharge capacity and efficiency for PAALi-based cells. The discharge capacity of the ASSLIB was 87.5 mA h g^{-1} at 0.2C (at 23.8 $^{\circ}$ C) for 120 cycles and 146 mA h g⁻¹ at 0.5C and 50 °C for 43 cycles. The enhancement in the specific capacity is attributed to the decrease in resistance for Li-ion transportation with PAALi as a binder.

Another attractive candidate as a solid-state electrolyte is NASICON-structure Li_{1,3}Al_{0,3}Ti_{1,7}(PO₄)₃ (LATP). LATP has high ionic conductivity (1 mS cm⁻¹) and better stability in water and air, which is attributed to the P-O bonding in its structure. 409,410 The only drawback restricting its use is interfacial issues, which result in poor contact, side reactions, and formation of dendrites.411,412 The formation of a mixed ionic/electronic conducting interphase (MCI) was observed because the reduction of Ti4+ to Ti3+ led to the formation of dendrites. Interface engineering can eliminate these problems. Here, an interfacial layer with low electronic conductivity and high ionic conductivity was introduced to minimize the interfacial resistance and prevent side reactions.

PEO and polyacrylonitrile (PAN) were used by Liang et al., 413 which led to an improvement in mechanical stability and better performance. PEO enhanced the Li-ion migration and reduced the interfacial resistance; however, at high temperatures (80–100 °C) it cannot suppress the growth of dendrites. To overcome the above-mentioned issue, Jin et al.414 prepared a composite polymer electrolyte with LATP. Fig. 20(a) shows the interface evolution mechanism without modifying the interface microstructure. The growth of the dendrite structure occurred due to the formation of an MCI.

With the introduction of an LATP layer, no MCI formation occurs, which is attributed to the elimination of side reactions, facilitating the fast migration of Li⁺. The suppression of dendrites is because of the high shear modulus (81-115 GPa). The ionic conductivity of LATP-CPE was $4.6 \times 10^{-4}~\mathrm{S~cm^{-1}}$ at 20 $^{\circ}\mathrm{C}$ and $4 \times 10^{-3} \text{ S cm}^{-1}$ at 80 °C. This enhancement originated from the suppression of the crystalline phase and improvement in salt dissociation after the addition of LATP. The voltage

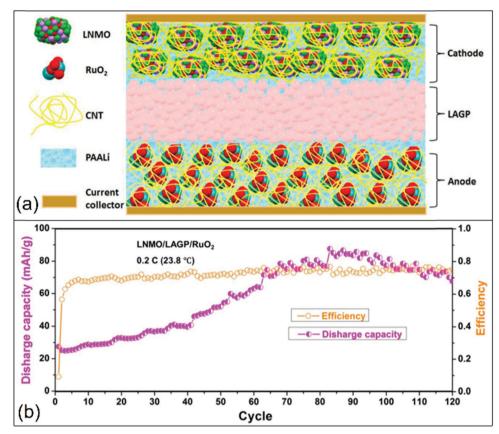


Fig. 19 (a) Schematic illustration of the full lithium-ion solid-state battery using LNMO/CNT/PAALi as the cathode, LAGP as the solid electrolyte, and RuO₂/CNT/PAALi as the anode, where both sides were sputtered with gold as current collectors. (b) Discharge capacity and efficiency of LNMO/LAGP/ RuO_2 at room temperature at 0.2C using PAALi as a binder. ⁴⁰⁸ Reproduced with permission from The Royal Society of Chemistry, UK. ⁴⁰⁸

window was close to 4.6 V. A solid-state battery (LFP/LATP/CPE/ Li) was fabricated and its electrochemical performance was examined. The initial specific discharge capacity of the cell was 113.1 mA h g⁻¹, which reached 139.5 mA h g⁻¹ after the 4th cycle. The specific capacity was reduced to 91.3 mA h g⁻¹ after 45 cycles, with a capacity retention of 80.7% and a Coulombic efficiency of >96% (Fig. 20b). PEO has been used as an electrolyte in batteries. However, the semi-crystalline nature of PEO hinders the desirable ionic conductivity. Thus, various strategies have been adopted to suppress the crystalline content of PEO. Some of the best-performance electrolytes are polymer blends, cross-linked polymers, co-polymers, block copolymers, networked solid polymer electrolyte (N-SPE), and polymers. The N-SPE is an attractive electrolyte due to the formation of a 3D radial network. It provides easy access to cation migration, which is associated with the segmental motion of polymer

Recently, Hsu et al. 357 prepared a network of solid polymer electrolyte (N-SPE), which is a cage-like polyhedral oligomeric silsesquioxane (POSS), serving as the hub of a network of poly(ethylene oxide-co-polypropylene oxide) (P(EO-co-PO)) with lithium bis(trifluoromethane sulfonyl)imide (LiTFSI). N-SPE demonstrated the highest conductivity of $\sim 1.1 \times 10^{-4} \text{ S cm}^{-1}$ at room temperature (25 $^{\circ}$ C) with an activation energy of 0.037 eV, which had a lower activation energy than PEO (0.5 eV). The lower

activation energy and high ionic conductivity of 3D POSS are attributed to its perfect polymer networking. The voltage stability window for the electrolyte was 5.4 V with a cation transport number of 0.62. Table 19 demonstrates the comparison of the electrode, electrolyte, and cell performance parameters for ASSLIBs.

A solid-state battery was assembled with the configuration of Li|N-SPE|LiFePO₄, as shown in Fig. 20(c). The N-SPE electrolyte was used as a sandwiched structure between two electrodes. It demonstrated a specific capacity of 160 mA h g⁻¹ at the rate of 0.1C. Fig. 20(d) shows the cycling performance of the cell at 0.1C and 0.2C, where $\sim 100\%$ coulombic efficiency with good capacity retention (95% at 0.1C and 92% at 0.2C) was observed. After 100 cycles with a high current rate (0.3C), the cell showed a capacity retention of 75% and Coulombic efficiency of 100%. The enhanced performance of the ASSLIB is attributed to the greater Li⁺ migration and good contact formation. Compared to the individual polymers, the blending of polymers is an effective strategy to suppress the crystallinity of PEO, facilitating higher electrical and mechanical properties. Recently, Bai et al. 358 prepared a polymer-ceramic hybrid electrolyte via the blending of PEO/PVDF and nanofiller Li_{6.4}La₃Zr_{1.4}Ta_{0.6}O₁₂ (LLZTO).

Fig. 21(a) shows the detailed preparation process of solid composite electrolyte-based PEO/PVDF/LLZTO/LiTFSI systems.

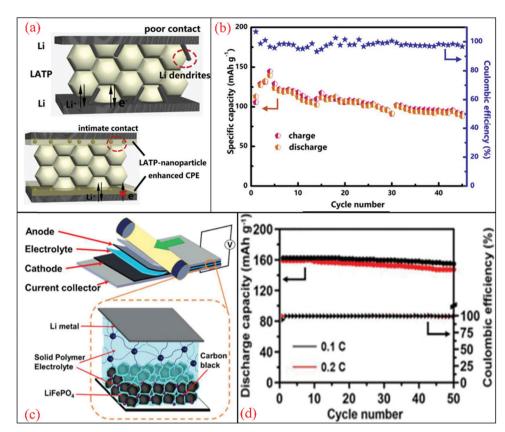


Fig. 20 Schematic illustration of the interface evolution between LATP and Li. (a) Without interface modification and after introducing LATP nanoparticles, which enhanced the CPE interfacial layer at LATP/Li interface. (b) Long-term cycling performance and coulombic efficiency of the solid-state LFP/LATP/CPE/Li cell at 0.05C, 80 °C.414 (c) Schematic of the roll-to-roll assembly of an Li|N-SPE|LiFePO₄ battery using a free-standing N-SPE film. (d) Variations in the capacity and Coulombic efficiency in the charge-discharge cycling at 0.1 and 0.2C-rates. The charge-discharge operated between 2.5 and 4.0 V, and the C rates were defined based on the theoretical capacity of LiFePO₄ (170 mA h g^{-1}). Reproduced with permission from Elsevier.414

The high tensile strength (5.21 MPa) and large strain (1888%) of the electrolyte film were achieved due to the reduction in crystallinity of the hybrid structure. The highest ionic conductivity was 3.23 imes 10⁻⁴ S cm⁻¹ at 25 $^{\circ}$ C and 8.58 imes 10⁻⁴ S cm⁻¹ at 45 °C with an activation energy of 0.32 eV. The enhancement in conductivity, reduction in crystallinity, and improved salt dissociation were attributed to the formation of additional conducting pathways with LLZTO due to the increased dielectric constant of PEO. Therefore, ASSLIBs were fabricated using LiFePO₄ as a cathode, Li metal as an anode, and the hybrid electrolyte.

Fig. 21(b) shows the cyclic performance of the fabricated LiFePO₄/Li cell at 0.4C (45 °C). The cell demonstrated a high discharge capacity of 160.1 mA h g⁻¹ and 99.1% capacity retention after 200 cycles. The smooth charge-discharge curves and low migration of discharge plateau with C-rate variation indicate better interfacial stability (Fig. 21c). This confirmed the better electrochemical performance, where the ASSLIB operated for 1000 h without short-circuit. Thus, it can be concluded from the above-detailed discussion on the different components of LIBs that the solid-state battery is the ultimate goal, which has the potential to eliminate the existing problems of liquid electrolytes. Fig. 22 provides a glimpse into the advantages and challenges of solid-state LIBs compared to liquid LIBs.

6. Improving performance of Si-based anode for LIBs

Significant efforts have been made to improve the performances of Si-based anode for LIBs. To overcome the volume expansion during the intercalation of electrochemical reactions, the inorganic/organic/Si nanocomposite anode of LIBs should be accommodated with the optimized microstructures. The hybrid nanostructured materials exhibit a genuine prospect to significantly impact the electrochemical performance of Si anodes. Therefore, the intercalation/deintercalation rates can be enhanced using Si-NP-based nanocomposites. The significance of nanosized Si (n-Si) for the battery performance was demonstrated by the LIB innovative researchers. 8,14,415

7. Limitations

The traditional LIBs are manufactured using liquid electrolytes, which cause toxic emissions and flammable accidents, which

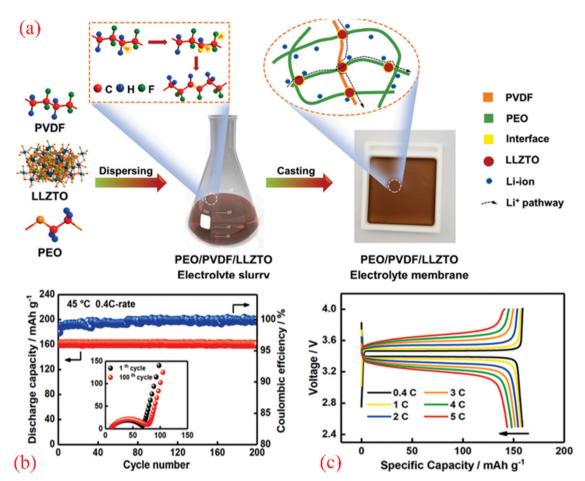


Fig. 21 (a) Fabrication process of the PLFF (PEO/PVDF/LLZTO/LiTFSI) solid composite electrolyte. (b) Cycling performances at 0.4C and 45 °C and the impedance of LiFePO₄/Li cell cycling with PLFY. (c) Different rates of galvanostatic charge-discharge profiles of LiFePO₄/PLFY/Li cells under 45 °C. 358 Reproduced with permission from Elsevier. 358

can be overcome by using solid electrolytes. In this case, LIBs can be manufactured without the use of a separator free with the implementation of solid-state electrolytes (SSE). ASSLIBs are manufactured as separator-free batteries, which automatically open the door for device miniaturization. Therefore, the weight/price can be controlled with the replacement of SSEs. The standard lifespan of LIBs is about three years (500 to 1000 cycles), where after this prescribed period, they usually do not show power backup and stability and seem to be worthless. The use of SSEs removes all the barriers faced by the commercial manufacturing of lithium ion-based batteries such as dendrite growth (cause short-circuit), pitiable thermal stability and safety concerns for portability and use.

The safety, cycle lifetime, and power density of LIBs cannot be easily controlled and tackled within the wide range of operational temperature conditions. Thus, a protection circuit must be included to maintain the voltage and current within safe limits together with the temperature sealing layers. The aging effect of LIBs is also a serious concern when these batteries are not in use and stored in a cool place. It significantly reduces the charge over time. There are transportation restrictions for the shipment of larger quantities, which may be

troubling for regulatory controls. These restrictions do not apply to personal carry-on batteries. Also, their manufacturing cost is about 40% higher than the nickel-cadmium batteries, even though the materials, metals, and chemicals are changing continuously.

8. Challenges

Over the past few decades, the progress in the development of materials for energy storage/conversion devices, especially Li-ion batteries (LIBs) has been satisfactory. However, although LIBs have been commercialized successfully with the use of liquid electrolytes, the scientific community has focused on alternative electrolytes to fulfill the dream of all-solid-state batteries (ASSBs). All three components of LIBs (cathode, anode, and electrolyte) need to be developed or innovated simultaneously to optimize the electrochemical performance of the cell. Accordingly, there are still several challenges related to LIBs that need to be resolved. A few of the major challenges are described, as follows: (i) disposing of damaged LIBs from mobile electronics, (ii) developing the large-scale production of

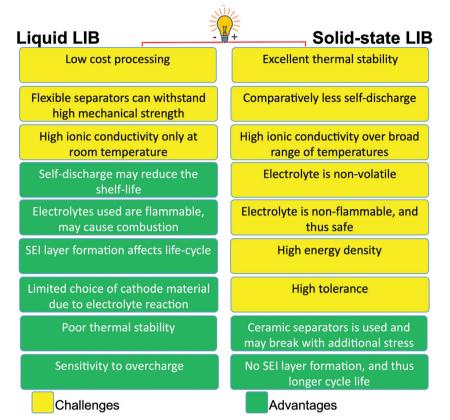


Fig. 22 Advantages and challenges in solid-state batteries (LIBs). [https://www.futurebridge.com/blog/solid-state-batteries/]

LIBs containing advanced electrodes and electrolytes for HEVs, (iii) fulfilling the required power density, and cyclability and (iv) recycling of automotive LIBs. Compared to lead-acid batteries, the recycling/disposal of LIBs are one of the most complicated issues, which have not been established to date, and thus further research is necessary for the recycling of the electrodes. The market for LIBs is driven by increasing the demand for mobile electronics, computers, and portable devices. The remarkable growth of mobile and robotic electronic systems has demonstrated that we need to improve the engineering and manufacturing process of Si-based nanocomposite electrodes. In response to the current demands of modern society and emerging ecological concerns, low-cost and environmentally friendly energy storage systems are required. Hence, the rapid R & D in energy storage systems should be aware of the market requirement. The performance of LIBs depends directly on the properties of their electrode materials and microstructure/compositions. Innovative materials chemistry demonstrates the advancement in energy storage mechanisms for LIBs. Some new strategies must be developed for stabilizing the cathode and anode to achieve the optimum performance in terms of durability. The contact between the current collector and active material needs to be examined for enhancing the charge transport via full use of the active material. The solid electrolyte interface needs to be improved to enhance the rate capability of the full cell. Therefore, no single modification strategy is suitable to achieve the optimum performance and the combination of various

strategies will be more efficient in tuning the properties of materials. Cobalt is an important raw material for batteries, considering that the search for alternative green electrodes for the next generation of ASSBs is a top priority.

The electrolyte is another crucial component of ASSLIBs. Solid polymer electrolytes have the potential to become a future electrolyte. Although significant efforts have been devoted by researchers to achieve better ionic conductivity, there is still a need to improve the ionic conductivity before commercialization. Different strategies have been adopted to design singleion conductors, as follows, (i) addition of nanoparticles, (ii) optimizing polymer chain movement, (iii) and designing new polymer backbones. The role of additives is to enhance the salt dissociation and provide additional conducting sites for cation migration. The surface groups of nanoparticles minimize the overall conducting path length for cations. However, in the development of solid polymer electrolytes (SPE), the ion transport mechanism needs to be investigated deeply. It can be understood from this review that the key approach is to adopt SPE, that is the fabrication of flexible energy storage devices to broaden the application range and durability. In this case, the key properties of SPEs such as thermal/chemical/electrochemical/ mechanical stability need to be examined. Furthermore, to maintain the energy density of ASSBs, these stability parameters play an important role. Further investigation needs to be focused on the performance of flexible batteries under different conditions such as bending, stretching, and reshaping. Nanostructured materials

have attracted the great interest in recent years because of their unique mechanical, electrical, optical properties and have the maximum surface area. To create a roadmap for nanomaterialbased electrodes for energy storage systems, the synthesis and manipulation of nanostructured materials need to be optimized for high-power density and long cycle ability.

The compatibility between electrodes and electrolyte needs to be enhanced for the fabrication of efficient ASSBs. Given that the internal resistance needs to be minimized for faster ion conduction from one electrode to another electrode, the interfacial stability between the components needs to be examined in detail together with electrochemical analysis. To meet the requirement of practical applications of LIBs, the optimization of the electrodes and the electrolyte is very important for the performance and durability. The aging effect of batteries and self-discharge are also a topic of research but hardly studied in the literature. To moderate the aging effect, some advanced characterization techniques should be used for the optimization of electrode materials such as neutron diffraction, small-angle X-ray scattering, and in situ tools for understanding of material behavior. Usually, all energy devices are operated at room temperature. Therefore, the current R&D of energy storage systems should be focused on low/high temperatures operation to achieve an efficient energy density and the memory effect. For the commercialization of LIBs globally, the universal testing parameters should be established for the comparison of data from various research groups/industries. Thus, the performance environment of ASSBs needs to consider the optimum feasibility worldwide. For the commercialization of LIBs, the cell architecture plays an important role in the performance and durability. The scientific community has devoted their efforts to the development of smart energy devices, which are superior to traditional devices. Thus, artificial intelligence (AI) and deep learning may be adopted for developing smart devices, which can optimize their performance themselves, strengthening the application of smart devices.

9. Future outlook

The recent development of novel negative electrodes (anodes) for lithium-ion batteries (LIBs) has focused on silicon-based nanostructured composites or hybrid materials. Silicon is one of the highest specific capacity anode materials, which can replace the standard C-based electrodes (carbon has a specific capacity of 372 mA h g⁻¹). Although the pure form of Si is not available in the Earth's crust or the environment, nanostructured Si can be obtained via synthetic methods or the biogenic synthesis. Nanostructured Si can be synthesized economically from biomass waste (biogenic silicon), which has the highest theoretical specific capacity (4200 mA h g^{-1}). For the setup of a materials database (cathode, anode, and electrolyte) for proper identification, research and development have been carried out to reduce the cost and processing time, resulting in efficient device development. To achieve a core-level understanding of the ion transport in the electrode/electrolyte, simulation tools can be used for the predetermination/demonstration before the experiment. To overcome the traditional instrument failure, advanced characterization techniques (cryo-electron microscopy) should be used to gain insights into materials and the interfaces in batteries. The utility and performance of ASSLIBs can be enhanced especially for HEVs and next-generation portable electronics due to the unique characteristics of materials and applications. Therefore, research needs to be carried out toward the development of solid electrolytes that exhibit high conductivity even at sub-zero temperatures. The progress and performance of ASSLIBs depend on their components and compatibility. To resolve the existing environmental and safety concerns, efficient ASSBs are future devices that have potential to promote growth in various sectors (from automobiles to the digital market).

Author contributions

Conceptualization: SKS, GS, AG, AA, YKM; data curation: SKS, GS, AG H-GR; formal analysis: SKS, GS, AG, AA, FSM, RA, J-SY, YKM H-GR; funding acquisition: SKS, YKM; investigation: SKS, GS, AA, AG, YKM; methodology: SKS, AG, AA, YKM; project administration: SKS, AG, YKM; supervision: SKS, AG, H-GR, YKM; writing, reviewing & editing: SKS, GS, AG, AA, FSM, RA, J-SY, YKM H-GR.

List of abbreviations

ASSLIB	All-solid-state	L1-10n	batteries

LIBs Li-ion batteries Electric vehicles EVs

HEVs Hybrid electric vehicles Titanium disulfide TiS₂ Lithium-cobalt oxide LiCoO₂

Highest occupied molecular orbital HOMO LUMO Lowest unoccupied molecular orbital **ESW** Electrochemical stability window

Failure mode, mechanism, and effect analysis **FMMEA**

Li-NMC Lithium-manganese-cobalt-oxide

Lithium nickel cobalt aluminum oxide batteries **NCA**

ANL Argonne national laboratory

a-C Amorphous carbon **CNTs** Carbon nanotubes

Solid-electrolyte interphase SEI **PVDF** Polyvinylidene fluoride **PAALi** Lithium polyacrylate

MCI Mixed ionic/electronic conducting interphase

PAN Polyacrylonitrile

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

Review

Prof. Sanjeev K. Sharma acknowledges the Government of Uttar Pradesh, India for sanctioned the project under UP-CST Research & Development programme (108/2021/2585/Sattar-4-2021-4(28)/2021/20). Danish authors acknowledge the funding by Interreg Deutschland-Denmark with money from the European Regional Development Fund, project number 096-1.1-18 (Access and Acceleration) and from the ESS lighthouse on hard materials in 3D, SOLID, funded by the Danish Agency for Science and Higher Education, grant number 8144-00002B.

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