



Cite this: *Green Chem.*, 2021, **23**, 4980

Received 25th May 2021,  
Accepted 24th June 2021

DOI: 10.1039/d1gc01852c

rs.c.li/greenchem

## Enzyme entrapment, biocatalyst immobilization without covalent attachment

Hasan T. Imam,  Patricia C. Marr \* and Andrew C. Marr \*

In entrapment an active species, which is often a catalyst, is trapped within a material by a solid or gel forming event; thus, it becomes dispersed within the solid or semi-solid matrix. Entrapment methods can be used to immobilize isolated enzymes and render them more stable, and easier to separate and recycle. Entrapment immobilization methods are well established for whole cell biocatalysis. Despite this the applications of entrapment towards isolated enzyme immobilization have lagged the use of covalent attachment and crosslinking methods. In this review entrapment methods are contrasted with other methods of enzyme immobilization and literature methods of enzyme entrapment are reviewed. A key advantage of this approach is that no formal interaction with the protein is required, but this must be balanced against the threat of enzyme leaching, or introduction of mass transfer limitations. The main methods of entrapment are characterized, and some recent innovations are highlighted.

### 1. Introduction

When assessed against the guidelines of green chemistry and atom economy,<sup>1–4</sup> isolated enzyme catalyzed reactions hold extreme promise. Enzymes catalyze a myriad of chemical transformations rapidly and cleanly in order to make the living cell functional. Location within the cell provides the enzyme with an optimized local environment in terms of pH, temperature, ionic strength and redox properties, and this supports high activity and exceptional selectivity.<sup>5–9</sup> In order to harness the power of enzyme efficiency for green chemical synthesis, the

enzyme must be optimized for use in a chemical reactor.<sup>10–14</sup> Steps can be taken to mimic the cellular environment, for example, by using aqueous buffer, but overall the conditions will be alien to the natural enzyme; additionally many chemical reactions operate better in man-made media such as organic solvents or ionic liquids.<sup>12,15–19</sup> Despite these challenges, many enzymes have been successfully applied as catalysts in industrial processes and isolated enzymes are becoming a major force in chemicals manufacture. This is in no small part due to rapid technical advancements in molecular biology, biochemistry and biotechnology that enable over expression of targeted enzymes in genetically modified organisms, e.g. *E.coli*, and isolation of enzymes in a partially or fully purified form. Industrial biocatalysis can be performed in two

School of Chemistry and Chemical Engineering, Queen's University Belfast, Belfast, UK. E-mail: p.marr@qub.ac.uk, a.marr@qub.ac.uk



Hasan Tanvir Imam

Dr Hasan Tanvir Imam is a post-doctoral research fellow in Queen's University Belfast, UK working with Dr A. C. Marr and Dr P. C. Marr. His interests include biocatalysis, bio-inorganic chemistry and sustainable chemistry. He completed his PhD in Warwick University, UK on metal binding studies of cysteine rich metalloproteins. He previously worked as a PDRA in Texas A&M University, USA and with Prof. P. C. J. Kamer at the University of St-Andrews, UK.



Patricia C. Marr

Dr Patricia C. Marr is a senior faculty member in the School of Chemistry & Chemical Engineering, Queen's University Belfast, UK specialising in materials, green & sustainable chemistry and ionic liquids. Following a PhD in materials at the University of St-Andrews, UK, her interest in materials, colloids, neoteric solvents and green and sustainable chemistry intensified as a result of postdoctoral work at The University of Nottingham and the University of Bristol.



ways, whole cell and isolated enzyme biocatalysis.<sup>18,20,21</sup> Whole cell biocatalysis retains the local environment around the enzyme, as the enzyme is accessed within a cell, such as a bacterium. Isolated enzyme methods require extra purification of the protein, and the loss of the cell environment around the protein, but this can be offset as the result of catalysis is often near total selectivity.<sup>18,22</sup> The application of biocatalysts as isolated enzymes requires the operator to counter the inherent instability of biocatalysts under operational conditions. In isolated form enzymes have a wide range of stabilities. Lipase, a class of hydrolase tuned to operate on hydrophobic substrates, is an exceptional example, as this enzyme has proven stability in harsh reaction environments, leading to application in pharmaceuticals, fine chemicals, consumer chemicals, polymers and foods.<sup>23–28</sup> However, for other classes of enzyme stability must be carefully optimized.<sup>16,29–34</sup> A vital component of this is the application of immobilization methods (section 2).

In applied industrial biocatalysis the choice of solvent(s) is a key consideration. The majority of enzymes will lend themselves naturally to aqueous enzymatic processes, however substrates may be insoluble or sparingly soluble in these media. Operating biocatalysis in organic solvents or in aqueous/organic biphasic media circumvents solubility challenges, but solvent toxicity can pose an environmental threat and/or damage the protein structure. Ionic liquids, famed for their low vapor pressure and tunable chemical and physical properties, have emerged as alternative solvents for biocatalysis (section 5).<sup>17,31,35–38</sup>

Established enzyme immobilization materials and methods have been reviewed.<sup>39,40,41–48,49</sup> This review focuses on emerging enzyme immobilization methods that do not require covalent attachment of the protein to the support (section 3 & 4). These methods, termed ‘entrapment’ methods, are complementary with protein optimization, as they allow the protein to be supported as optimized with no further modification. In addition, entrapment methods offer the facile tuning and optimization of the support, so that the perfect environment can be created to stabilize and enhance the activity of the enzyme.



**Andrew C. Marr**

*Dr Andrew C. Marr is a senior faculty member in the School of Chemistry & Chemical Engineering, Queen's University Belfast, UK specialising in green catalysis with biocatalysts, organometallic complexes and ionic liquids. After a PhD in the University of St-Andrews, UK, his fascination with biocatalysis was ignited during postdoctoral research on hydrogenases with Prof. Martin Schröder at The University of Nottingham.*

This review will mainly focus on enzyme immobilization *via* entrapment methods, highlighting pioneering work and recent developments. In the section 2, the suitability, and robustness of other enzyme immobilization methods, namely adsorption, covalent attachment and crosslinking, will be compared to entrapment.

## 2. Summary of enzyme immobilization methods

Biocatalysis technologies are rapidly developing and finding industrial applications. However, isolated enzymes can be short-lived and their inherent instability towards long term storage and reuse poses a threat to the sustainability of biocatalytic chemical processes. Technological advances, in particular genome mining (metagenomics), next generation gene sequencing and bioinformatics, assist the isolation of efficient natural enzyme catalysts.<sup>50,51</sup> Introduction of directed evolution has greatly improved biocatalyst stability and activity.<sup>52–54</sup> Computational aided, *de novo* design has further enhanced the understanding of biocatalysts leading to wider substrate scopes.<sup>55–61</sup> However, the economic viability of such optimized biocatalytic systems commonly suffers from a lack of reusability, and reuse and recycling are vital components of a green and circular economy. Immobilization of the isolated enzyme, defined as the association of the biocatalyst with a support material, significantly lowers the environmental and economic impact of the enzyme catalyzed reaction. The support protects the enzymes from deactivation/degradation and facilitates separation and recycling; thus, biocatalyst immobilization has considerable industrial importance and has the potential to overcome challenges associated with widespread application. Immobilized enzymes can also be used in flow systems, thus offering operational flexibility.

Immobilized enzymes have been applied in the fine chemical, food and pharmaceutical industries.<sup>28,62–66</sup> Covalent attachment of the protein to a solid is a leading method of immobilization in industry. Supports are typically obtained off the shelf from third party manufacturers, with organic polymer supports featuring prominently. The efficiency of the immobilized enzyme depends on the complementarity of the support for the protein and the chemical process targeted.

In scientific research many methods of enzyme immobilization have been reported. These can be classified as depicted in Fig. 1. The main methods for rendering an enzyme insoluble and recyclable can be divided into physical and chemical methods. In the physical method, the enzyme physically (without forming any formal chemical bonds) interacts with the carrier material/support material. The protein can either be adsorbed on the surface of the material or entrapped within. In the chemical method, the enzyme is crosslinked or covalently bonded to the support material. As of 2021 the leading methods employed for enzyme immobilization in the chemical industry are chemical methods. Enzyme immobilization can be further classified into four categories-adsorption,



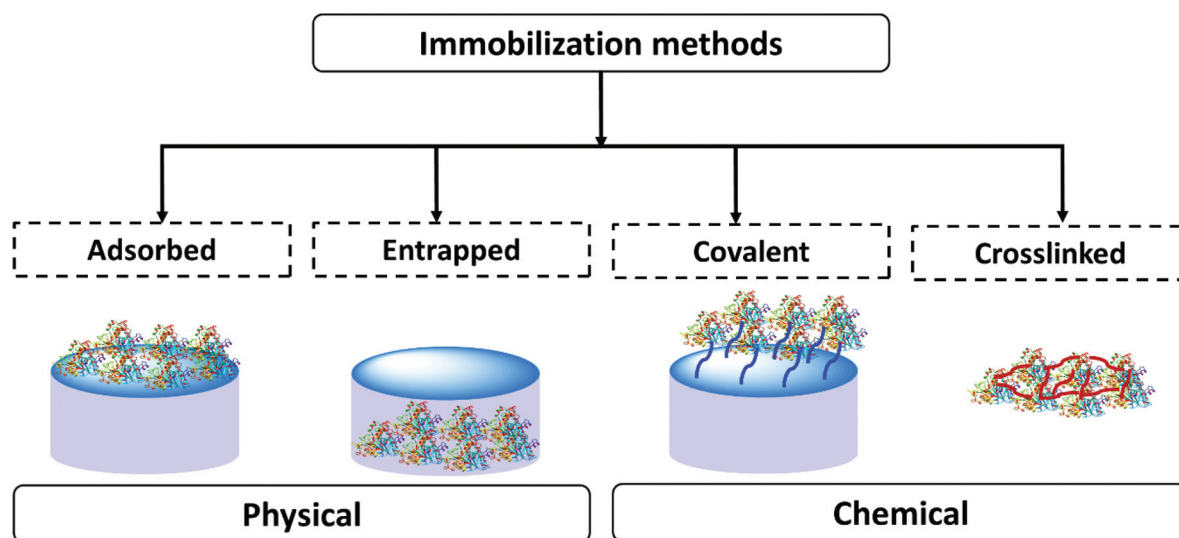


Fig. 1 The classification of enzyme immobilization methods.

entrapment, covalent linking and crosslinking (Fig. 1).<sup>18,44,67–70</sup> Table 1 summarizes and compares the different enzyme immobilization methods.

In the adsorption process, the enzyme is physically adsorbed onto a pre-prepared support material *via* hydrophilic–hydrophobic, van der Waals, H-bonding and/or ionic interactions.<sup>71</sup> The process is easy and relatively cheap. As adsorption methods allow the enzymes close contact with the reaction media, the stability of this system is profoundly influ-

enced by reaction conditions, like the solvent pH and ionic strength. The use of a pre-made support material provides little control over material properties. Interactions with the support material may change the enzyme surface charge distribution and activity. A couple of recent representative examples are given. Lipase from *Aspergillus niger* was adsorbed on a zirconium based metal organic frame work (UiO-66) and hydrophobic polydimethyl-siloxane (PDMS) modified UiO-66 *via* hydrophobic interactions, by mixing the enzyme with the

Table 1 Comparison of enzyme immobilization methods

Observations	Adsorbed	Entrapped	Covalent	Crosslinked
Preparation	Enzyme binds to the support material by physical interaction	Support material forms in the presence of the enzyme trapping it	Enzyme binds to the support material <i>via</i> covalent bonds	Enzymes are cross-linked to enzyme/protein/support to form an enzyme aggregate or crystal
Process	Partial or incomplete adsorption on the surface of support Requires an excess of enzyme to favor the equilibrium towards adsorption Protein and support material must be complementary	Support formed in the presence of the protein, protein fully entrapped Minimal loss of the support material and enzyme	Number of attachment points to the support can vary Require an excess of the support to favor complete covalent attachment	Extent of crosslinking can vary, can involve a support material Minimal loss of the support material and enzyme
Enzyme structure	Enzyme interaction with the support is required	Minimal changes in enzyme structure. Some interaction with the matrix	Enzyme structure modified to form covalent bonds	Scope for tuning crosslinking. Reproducibility can be challenging Interaction with the crosslinkers
Operational stability	Binding is weak. Process stability depends on the reaction conditions	High operational stability. Leaching could be caused by soft material breakdown or poor enzyme matrix interaction	High operational stability. Strong binding to the support. Potential for some leaching depending on how well the protein is anchored	Good operational stability. Leaching could be caused by soft material breakdown or poor enzyme matrix interaction
Diffusion/mass transfer	Enzyme comes in close contact with the reaction medium. Easy diffusion is expected	Solid support protects the enzyme from direct contact with the reaction medium. Diffusion depends on the material design	Enzyme comes in close contact with the reaction medium. Possibility of reduction of mass transfer due to tethering	Structure can vary. Diffusion will depend on the size of the aggregate or crystal



support material in buffer.<sup>72</sup> Increased activity was observed for PDMS modified UiO-66 in butyryl hydrolysis. Immobilized lipase on PDMS modified UiO-66 exhibited methanolysis of soybean oil for biodiesel production with 88% yield at 24 h and retained 83% activity after 10 runs. Lipase B from *Candida Antarctica* was immobilized in mesoporous silica (SBA-15) *via* electrostatic forces. The supported enzyme was active for ethyl hexanoate hydrolysis at pH 5, but at pH 7 the surface charge of the enzyme became negative, thus reducing the electrostatic interaction with the negatively charged support.<sup>260</sup>

Adsorption of an enzyme onto a support is relatively simple but the interaction between the support and protein is minimal, and these materials are vulnerable to leaching.

At the time of writing (2021) the covalent method was a common choice for enzyme immobilization. Enzymes are covalently attached to a support material, often a commercial polymer, by providing reactive points on the polymer that anchor onto the protein.<sup>73,74</sup> For example, lipase A from *Bacillus subtilis* was immobilized *via* covalent modification of silica supported poly(sulfobetaine methacrylate) (PSBMA) polymer brushes.<sup>75,76</sup> The enzyme was bound to the polymer brush by covalent modification of lysine with an NHS group (*N*-hydroxysuccinimide). The enzyme was immobilized on the polymer brush by mixing the enzyme with the polymer brush in buffer. At 20 °C, both immobilized and free enzymes exhibited similar activity in the hydrolysis of resorufin butyrate in buffer. At 50 °C the immobilized enzyme demonstrated a 100 fold increase in activity compared to the activity observed at 20 °C, whereas the free enzyme underwent a 2-fold increase in activity at its optimum temperature of 30 °C. Polymers that are ready to bind proteins are frequently provided by third party specialist manufacturers.

Covalently immobilized enzymes are expected to have good stability and recyclability under process conditions, and this has led to their commercial success. However, such strong attachment is a significant modification of the protein and can sometimes lead to changes in the protein hydrophilic/hydrophobic properties, which can significantly affect performance. There is some flexibility in material choice, with third parties providing a number of polymers with differing points of attachment and/or hydrophilicity/hydrophobicity, but there are few options for bespoke support design and polymers tend to be used as supplied. It may be necessary to modify the protein surface in order to improve the covalent attachment to the support, and it may be advantageous to optimize the protein and support together to ensure best performance.

In the crosslinking method, a material crosslinks enzymes with each other, with another protein, and/or with a support material.<sup>77–79</sup> In general, enzyme crosslinking is a two-step process.<sup>80,81</sup> In the first step the enzyme is precipitated to form aggregates or crystals, using different organic and inorganic precipitants. These precipitants can include glycol, dimethoxyethane, acetone, acetonitrile and ammonium sulphate. Often aqueous ammonium sulphate solution is used to make a crystal. The second step is the crosslinking of the aggregated or crystalized enzyme, to form a crosslinked

enzyme aggregate (CLEA) or crosslinked enzyme crystal (CLEC), which is active and functional. The crosslinking material can target specific amino acids. Glutaraldehyde, benzoquinone and dextran-polyaldehyde are common crosslinking agents for lysine crosslinking whilst, polyethyleneimine and carboxylate activating carbodiimide are used for crosslinking glutamic or aspartic acid residues.<sup>78,82–85</sup> CLEA is a leading method of enzyme immobilization. Sheldon *et al.* have highlighted the usefulness of CLEA for enzyme immobilization over the years and have recently updated the progress in their reviews.<sup>86,87</sup> A representative example is given. The enzyme nitrile hydratase was precipitated with ammonium sulfate and crosslinked with glutaraldehyde to make CLEAs for the hydration of hexanenitrile.<sup>88</sup> The nitrile hydratase CLEA showed 77% of the free enzyme activity at (8%v/v) substrate concentration. However, activity dropped significantly upon batch recycling.

Crosslinking is an established method of enzyme immobilization, and the materials can be relatively stable and recyclable under process conditions. Effort must be taken to ensure the mechanical stability of CLEAs and CLECs. Process optimization must concentrate on the reliability of the synthesis, ensuring that the structure formed is reproducible.

In this review entrapment is defined as a method in which a solid or gel is formed or reformed in the presence of the enzyme, due to an event that occurs between molecules that end up as part of the support. This solid or gel forming event does not formally involve the enzyme, but the presence of the enzyme is expected to have a templating influence. The enzyme becomes trapped inside the material matrix as the support material grows, either due to size effects, supramolecular forces, or most likely, a combination of the two.<sup>49,70,89</sup> The material formed is often a gel. A gel comprises a solid crosslinked matrix and a confined liquid. The liquid within provides an environment for the protein which can be engineered to optimize performance. Ideally the enzyme retains the native structure as no strong modifications happen within the gel. The matrix protects the enzyme from direct contact with the bulk reaction conditions, and renders the bulk material solid-like, yet allows the substrate and the product to diffuse, a schematic presentation of an ideal entrapped enzyme is given as Fig. 2.

Mass transfer limitations can be a drawback of this method, and the material must be designed with appropriate pore size and matrix properties. However, a material that is too porous, or has pores that are too large will readily leach, and defects in the matrix may also lead to enzyme leaching. The key to successful entrapment is to provide the correct environment inside a porous material that allows for free diffusion of the substrate and product, but restricted movement of the protein. Differences in size and chemical nature of the enzyme protein and substrate molecule render this an achievable goal, but it must be considered as the primary design criterion. Many entrapment methods allow for control over the shape and thickness of the material, and this can help to control mass transport of the substrate and product.



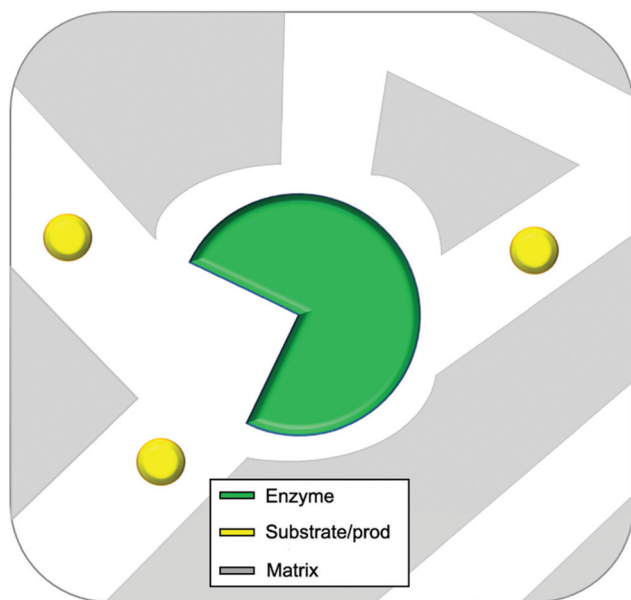


Fig. 2 Idealized representation of an entrapped enzyme. The substrate/product and enzyme are of realistic proportional size.

The gel can be hard or soft. We define a hard gel as a gel in which the polymerization is essentially irreversible. Hard gels tend to be the result of a covalent polymerization, such as the formation of an organic polymer, or an inorganic oxide. In a soft gel the gel can be disrupted and reformed, for example, by heating and cooling. Soft gels tend to be formed by supramolecular interactions.

This review is concerned with the development and possible future applications of entrapment methods that do not involve covalent linking to the protein. For more details on the

research and industrial application of covalent bonding and crosslinking to enzyme immobilization an up to date review was recently published by Sheldon *et al.*<sup>87</sup>

### 3. Enzyme entrapment in gels

A gel comprises a liquid phase entrapped within a solid 3D network.<sup>90,91</sup> To form a gel precursors to the solid matrix are self-assembled, dispersed or polymerized within the liquid phase. Depending on how the solid matrix is formed, gels can be classified as molecular (supra-molecular), colloidal and polymeric (macromolecular). However, gels are also classified based on the liquid phase, for example, if water is used as the liquid phase, the gel is known as a hydrogel.

The entrapment of enzymes in gels is generally a mild process which allows the enzyme to retain its optimized structure. It can be achieved in four main ways: sol-gel methods, polymerisation to form insoluble polymers, crosslinking of biopolymers, and supramolecular assembly (Fig. 3). In general sol-gel forms a hard gel, supramolecular assembly forms a soft gel, and polymer and biopolymer gels can be hard or soft.

#### 3.1 Sol-gel methods

In the sol-gel process, soluble precursors to a solid oxide matrix, typically reactive oxides or alkoxides *e.g.*, tetraethyl-orthosilicate (TEOS), are dissolved in a solvent, *e.g.*, a mixture of alcohol and water. Upon initiation of the reaction, which may require the addition of an acidic or basic catalyst, a sol forms, (Fig. 4A). The suspended oxide particles of the sol react together until the gel point is reached (Fig. 4B). An enzyme can be added to the precursor solution resulting in an oxide gel containing an immobilized enzyme. During the gel for-

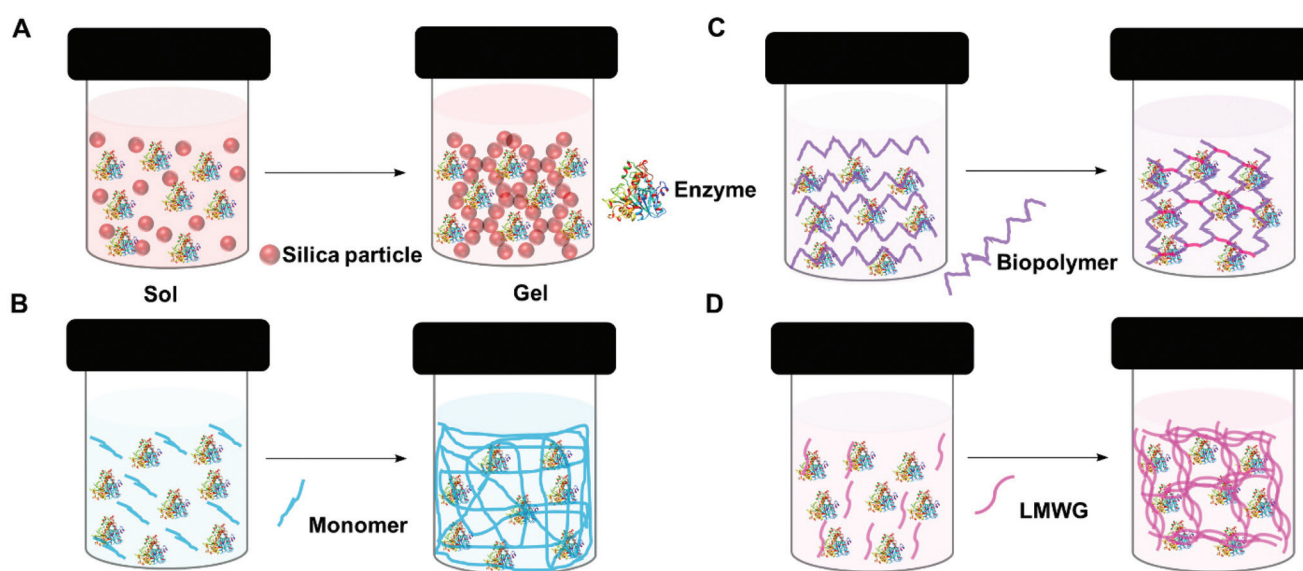


Fig. 3 Schematic representation of enzyme entrapment in gels. (A) Sol-gel (silica gel) (B) polymerization (C) crosslinking biopolymer and (D) supra-molecular assembly (low molecular weight gel).



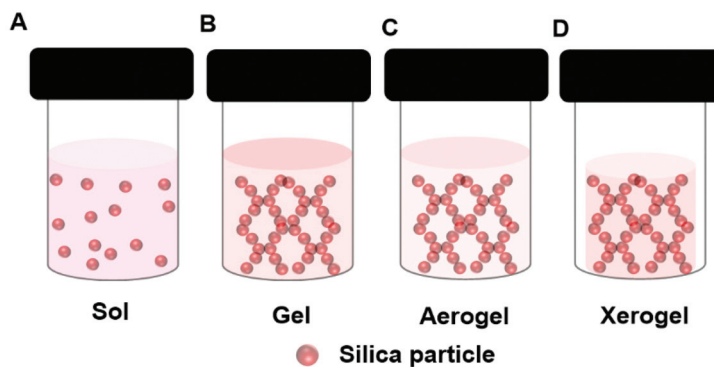


Fig. 4 Schematic presentation of different structures formed during the sol-gel formation of a silica gel depicting a (A) Sol, (B) Gel, (C) Aerogel, (D) Xerogel.

mation the oxide precursor undergoes hydrolysis and condensation processes. Production of a stable gel requires ageing of the gel. During this time the reaction continues, but at a much slower rate. Drying plays a critical role in the gel morphology. Working up the gel in different ways enables the design of tailor-made materials with controlled pore and surface area. This affects diffusion rates through the final material. Sol-gel prepared oxides can be coated on a surface, or made into powders or spheres. Employing supercritical  $\text{CO}_2$  drying removes the solvent from the gel rapidly, yet retains the 3D gel network, and this produces a very high surface area material known as an aerogel (Fig. 4C). Normal drying at ambient conditions leads to greater pore collapse, and the production of a xerogel (Fig. 4D). Gel shrinking can be minimized by the inclusion of additives like synthetic or bio-polymers or ionic liquids (section 5).

Some of the common reactions that are catalyzed by entrapped enzymes are summarized in Fig. 5.

Avnir and co-workers pioneered the entrapment of enzymes in silica using sol-gel processes. An aqueous solution of alkaline phosphatase was entrapped in silica gel, using a base catalyzed process and tetramethylorthosilicate (TMOS) as the silica precursor. The sol-gel process was performed in the presence of small amount of methanol by mixing an ice-cold enzyme solution with the TMOS solution, base and methanol at  $-20\text{ }^\circ\text{C}$ , and the gel was dried and aged at  $37\text{ }^\circ\text{C}$ .<sup>92</sup> The immobilized enzyme retained 30% of the activity of the free enzyme for the hydrolysis of *p*-nitrophenyl phosphate (pNPP) in glycine buffer. The immobilized enzyme exhibited enhanced thermal operation stability at  $70\text{ }^\circ\text{C}$  and retained activity for two months when stored in water at room temperature. Since then, an increasing number of enzymes have been entrapped in silicate gels using sol-gel procedures. Many of these materials have been applied as sensors.<sup>93,94</sup> For example a tetraethylorthosilicate (TEOS) and ethanol sol-gel process was used to immobilized glucose oxidase and the material was applied to glucose sensing.<sup>95</sup> Alcohol in these sol-gel processes can deactivate the immobilized enzyme and activity is typically lower than the free enzyme. Yamanaka and co-workers used aqueous buffer in an acid catalyzed TMOS sol-gel process, and entrapped single and multiple enzymes

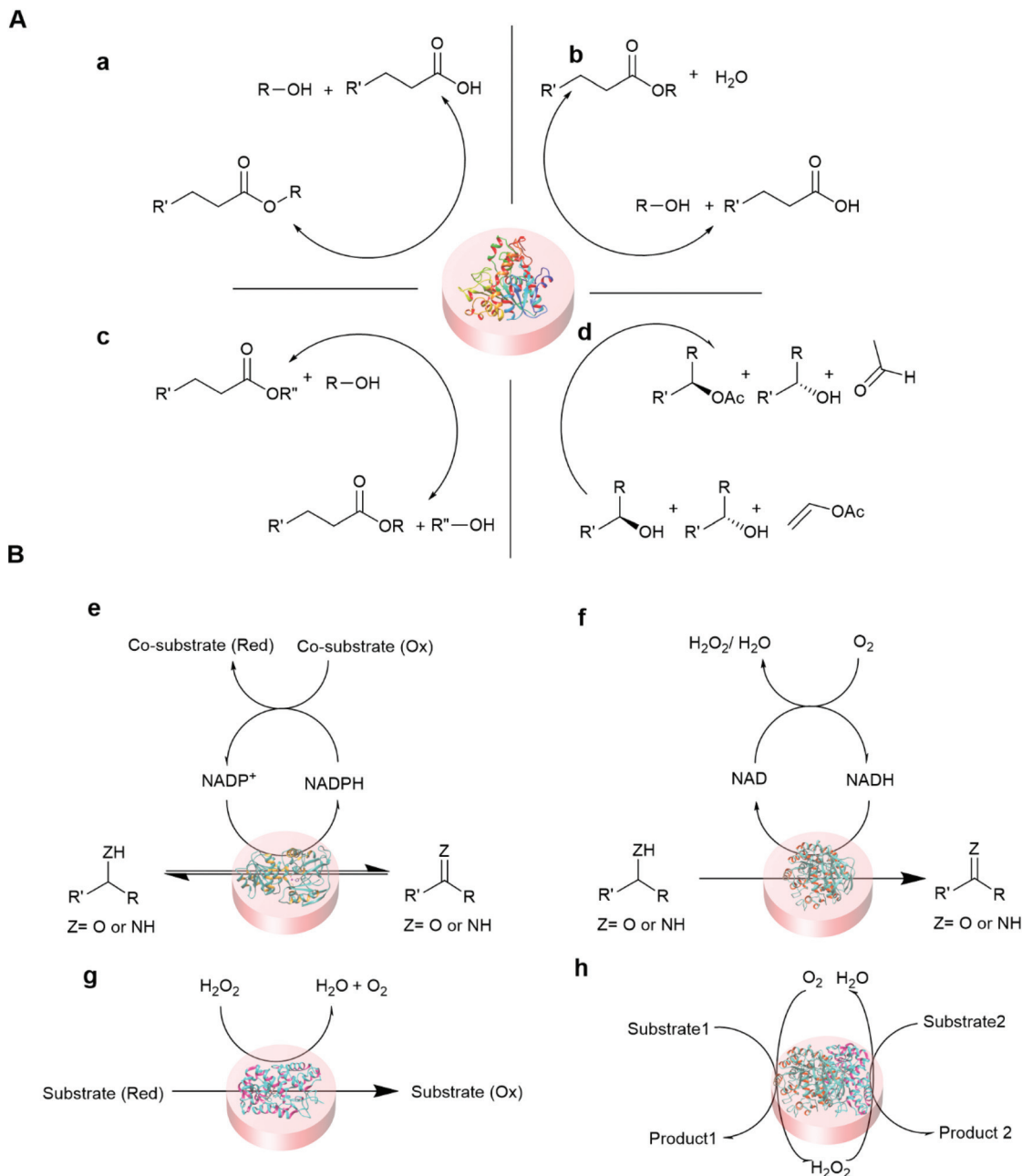
including glucose oxidase from *Aspergillus niger* and horseradish peroxidase, in a transparent gel.<sup>96</sup> Sonication of TMOS, water and acid gave the sol, the sol was then buffered and finally the enzyme(s) in buffer was mixed with the buffered sol and left at  $4\text{ }^\circ\text{C}$  to dry. A cascade reaction was carried out using immobilized glucose oxidase and peroxidase. The immobilized enzymes retained 20% of the activity of the free enzymes. Aqueous solutions of glucose oxidase and peroxidase were also entrapped in silica gel using TMOS with 0.5% polydimethylsiloxane.<sup>97</sup>

The addition of additives to the sol-gel media further improved the sol-gel entrapment process. Addition of polyethylene glycol (PEG-6000) to a TMOS-derived gel of trypsin led to good retention of activity, as the trypsin stayed active for several months, and also increase the half-life of alkaline phosphatase.<sup>98</sup>

Metal oxide methods tend to be faster and harder to control than silica-based sol-gel methods. Hybrid materials of cellulose acetate with oxide of titanium isopropoxide ( $\text{Ti}(\text{iOPr})_4$ ) and zirconium tetra-*n*-butoxide ( $\text{Zr}(\text{OBU})_4$ ), respectively, were used to entrap urase from jack bean and glucose oxidase from *Aspergillus niger* using modified sol-gel methods.<sup>99</sup> The hybrid Zr material was made by mixing cellulose acetate in acetone with the enzyme in buffer, followed by dropwise mixing of the cellulose-enzyme solution to  $\text{Zr}(\text{OBU})_4$  solution in acetone, the mixture was left for 30 min and the gel fibers were dried in the fridge. The immobilized glucose oxidase in cellulose-Zr gel fibers had 10 times lower activity than the free enzymes for glucose oxidation. However, increase in activity was observed with consequent runs, and it was speculated that the increase in activity with reuse originated from different orientations/configurations of the enzyme. A very similar result was observed for immobilized urase.

Using hydrophobic silica precursors for enzyme entrapment has proven a successful method for immobilizing biocatalysts for chemical synthesis, particularly for lipase.<sup>89,104-110</sup> Reetz and co-workers added hydrophobic silica precursors to their sol-gel enzyme entrapment process. A lipase silica gel of *Ps. cepaci* (Amano PS) derived from TMOS exhibited only 5% activity in lauric acid esterification. Using silica precursors





**Fig. 5** Representative reaction schemes of immobilized hydrolase and oxidoreductase biocatalysis. (A) Hydrolase (lipase) catalyzed reaction<sup>100,101</sup> (a) hydrolysis (b) esterification (c) transesterification, and (d) kinetic resolution. (B) Oxidoreductase catalyzed reactions<sup>102,103</sup> (e) dehydrogenase (f) oxidase (g) peroxidase and (h) cascade reaction of oxidase and peroxidase.

TMOS/ $RSi(OCH_3)_3$ , or pure  $RSi(OCH_3)_3$  ( $R = C_nH_{2n+1}$ ,  $n = 1, 2, 3, 4$ , and  $18$ ), not only enhance the activity, but also increased the enzyme loading.<sup>105</sup> In a sodium fluoride (NaF) catalyzed methyltrimethoxysilane MTMS ( $RSi(OCH_3)_3$  ( $R=CH_3$ )) derived silica gel of lipase, the esterification activity of lauric acid with *n*-octanol in isoctane was increased by 1300%, and >99% ee was obtained in the kinetic resolution of *L*-phenylethanol with acetic anhydride in benzene.<sup>104</sup>

The inclusion of additives into the sol-gel enzyme entrapment process can lead to significant improvements in enzyme

stability. This has increased the scope of the chemistry that could be achieved with isolated enzymes. For example a TMOS derived gel of two highly pH sensitive enzymes alkaline phosphatase (optimal activity at pH 9.5) and acid phosphatase (optimal activity at pH 4.5), were doped with the surfactants sodium dioctylsulfosuccinate (AOT) and cetyltrimethylammoniumbromide (CTAB), and this enabled the application of the enzymes to the hydrolysis of *p*-nitrophenyl phosphate (pNPP) at low and high pH of 0.9 and 13.0 respectively.<sup>111</sup> A TEOS derived silica gel of laccase from *Trametes* sp. retained 100%



oxidation activity of 2,6-dimethoxyphenol (2,6-DMP) after 70 days of storage at 27 °C in the presence of polymer additives of polyvinyl alcohol (PVA), whereas the additive free immobilized enzyme retained only 30% activity.<sup>112</sup> Isopropyl alcohol and polyvinyl alcohol were added to a silica gel of  $\omega$ -Transaminase from *Arthrobacter sp.* derived from TMOS/RSi(OCH<sub>3</sub>)<sub>3</sub> (R = C<sub>n</sub>H<sub>2n+1</sub>, n = 1, 2, 3, 4), enabling the kinetic resolution of 1-phenylethylamine with sodium pyruvate and pyridoxal-5-phosphate monohydrate using dimethylsulfoxide (DMSO) as co-solvent in buffer at relatively high substrate concentration of 100 mM.<sup>113</sup> The conversion was 54% at 24 h with >99% ee obtained for the product 1-phenylethylamine. The immobilized enzyme was recycled 5 times with conversions of 51% at 24 h and >99% ee. Adding polyethylenimine to a silica gel of lipase from *Thermomyces lanuginosus* immobilized by a TEOS sol-gel process increased the enzyme loading, thermal stability and catalytic activity.<sup>114</sup> Similarly adding poly-L-lysine to silica gels of lipase and glucose oxidase enhanced the stability, reusability and thermal stability.<sup>115,116</sup> Adding polyethylene oxide to a TEOS derived silica gel of  $\beta$ -glucuronidase from *Helix pomatia* enabled the microfluidic (the reaction was operated in small quantities of liquids within narrow channels) hydrolysis of *p*-nitrophenyl- $\beta$ -D-glucuronide (pNP-GluA).<sup>117</sup>

Enzymes can be entrapped in alumina (Boehmite) gels by sol-gel processes. Liu *et al.* claimed that hydrophilic alumina had advantages over silica, particularly, the retention of activity at high enzyme loading and the immobilization of low isoelectric point enzymes.<sup>118,119</sup> Alumina entrapped enzymes are prepared from an alumina sol (Fig. 6). One approach is to make the sol from aluminium alkoxides at high temperature; this is followed by acid (such as HCl) catalyzed hydrolysis. Finally, the enzyme is added to the sol before gel formation (Fig. 6A). Aluminium alkoxides produce alcohols during the hydrolysis process, and this can denature the enzyme. If the enzyme is sensitive to alcohol, the alcohol can be evaporated prior to protein addition. Yang and co-workers used sodium

aluminate in an acid catalyzed sol-gel process to entrap catalase from bovine liver in buffer.<sup>120</sup> The gel morphology, studied by SEM and TEM, suggested boehmite (isoelectric point PI 9.1) formed positively charged nano-needles at pH 7, at that pH catalase (PI 5.4) remained negatively charged thus electrostatically attached to the boehmite, later, boehmite self-assembled into a nano strip and entrapped the enzyme. The catalase entrapped in alumina gel achieved 30% activity relative to the free enzyme in buffer at pH 7.0, 25 °C. However, the gel achieved 86% of the free enzyme's activity at pH 4. The gel exhibited poor recyclability due to enzyme leaching. Another approach was employed by Avnir and co-workers, who precipitated aluminium alkoxide in water, and ultrasonicated the precipitate to give a transparent sol (Fig. 6B). Human serum albumin was added to the sol at room temperature.<sup>121</sup> Human serum albumin entrapped in alumina gel exhibited increased stability, with an increase in denature temperature of 54 °C. This was attributed to the ability of the alumina gel to retain water at elevated temperatures. The same group compared proteinase and xylanase activity in silica and alumina gels.<sup>122</sup> Both the enzymes performed better in alumina gel than silica gel. In addition, a heat-treated alumina gel of xylanase at the elevated temperature of 200 °C for 3 min retained 73% activity in xylan degradation to xylose in buffer, whereas, the silica gel lost activity after heat treatment at 200 °C. The hard-crystalline alumina gel retained the enzyme's native structure and essential water within the confined environment of the gel. Plasminogen activator, a serine protease, entrapped in alumina gel was applied as an injectable material for thrombosis treatment.<sup>123</sup> Alumina gels of three therapeutic enzymes, acid phosphatase (AcP), horseradish peroxidase (HRP), and asparaginase (ASP) all exhibited thermostability of 30–50 °C higher than the aqueous enzyme.<sup>124</sup> The alumina sol-gel process was shown to refold an unfolded carbonic anhydrase and the entrapped enzyme exhibited activity of 180% higher than the native enzyme in hydrolysis of *p*-nitrophenyl acetate (pNPA) in buffer.<sup>125</sup> Alumina gel also protected carbonic anhydrase, acid phosphatase and Horseradish peroxidase from photodegradation.<sup>126</sup> Alumina gels of bovine serum albumin are used as a protein carrier for biomedical applications.<sup>127</sup>

Sol-gel methods for enzyme entrapment have been demonstrated to form a wide range of active biocatalytic materials, particularly for hydrophobic enzymes such as lipase. In the presence of modifying groups, good activity and stability can be supported, and alumina gels appear to have significant advantages at higher temperatures. Historically the application of hard oxide gels suffered from the lack of structure-function understanding, with each entrapment method appearing as a 'one off', giving little opportunity for systematic tuning. The addition of ionic liquids could change this and lead to systematic design of the local enzyme environment. Ionic liquids are discussed in section 5.

### 3.2 Synthetic polymers

The immobilization of an enzyme using a synthetic polymer (Fig. 7A) is an old method, but it is still evolving and is there-

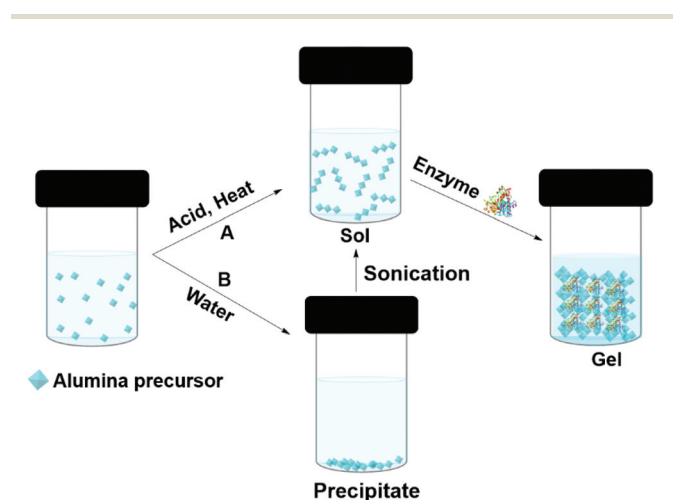
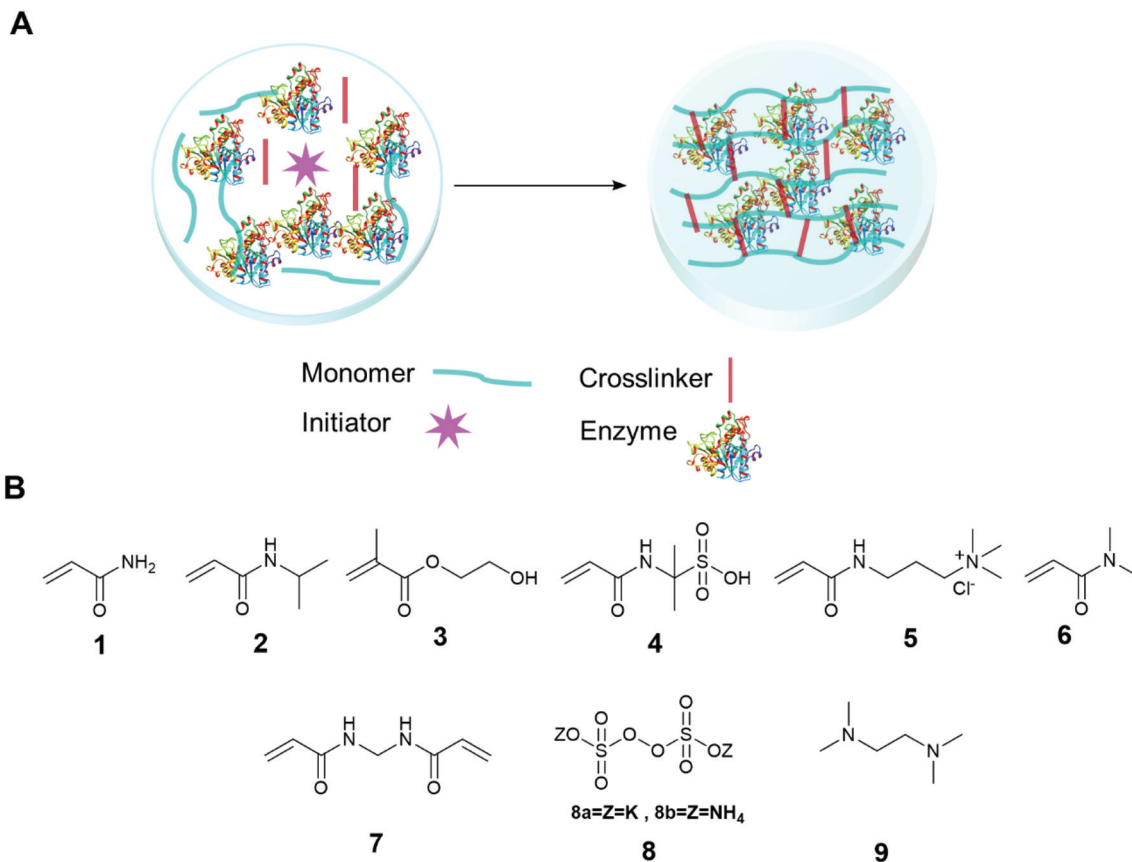


Fig. 6 Different approaches (A and B) to entrapping enzymes in alumina (boehmite) gels by sol-gel methods.







**Fig. 7** Enzyme entrapment in synthetic polymer gels. (A) Schematic presentation of entrapment in synthetic polymer gels; (B) chemical structure of some common monomers, crosslinker and initiators.

fore worthy of discussion.<sup>128,129</sup> In general, entrapping an enzyme in a polymer matrix involves mixing the enzyme with monomers, and sometimes crosslinkers, and an initiator to mediate the polymerization process. Often polymerization is achieved *via* free radical formation. Different approaches are used to generate free radicals, some commonly used processes are photochemical, redox and enzyme mediation. Redox mediated free radical formation is a mild process and is commonly used for enzyme entrapment. Bernfeld and Wan pioneered methods for immobilizing enzymes and antigens in polymer gels, and these methods provide a good example to illustrate the scope of synthetic polymer entrapment.<sup>130</sup> The monomers used in these and related methods (Fig. 7B) are known to form hydrogels in water. Bernfeld and Wan entrapped seven different enzymes and antigens in poly-acrylamide gels formed by the free radical polymerization of acrylamide **1** and *N,N'*-methylenebisacrylamide **7** in an aqueous buffer at 35 °C, the polymerization reaction was initiated using potassium persulphate (KP) **8a**. The immobilized antigen exhibited antibody binding activity.

Demirel and co-workers entrapped glucose isomerase in a poly(acrylamide) hydrogel using a free radical polymerization reaction of **1** and **7** in an aqueous solution using tetramethylethylenediamine (TEMED) **9** and ammonium persulfate (APS)

**8b** at room temperature.<sup>131</sup> The immobilized enzyme exhibited optimal glucose isomerase activity at 60 °C, and retained 75% activity at the high temperature of 70 °C, at the same temperature the free enzyme retained only 40% activity. The immobilized enzyme retained 81% activity after 42 days storage at 4 °C and retained 98% activity after 25 recycles. Yamak *et al.* immobilized laccase in a poly(acrylamide-*N*-isopropylacrylamide) hydrogel by mixing the enzyme with **1**, *N*-isopropylacrylamide **2**, **7** (as a crosslinker), and **8b** and **9** (as redox initiators) in buffer at room temperature.<sup>132</sup> The immobilized laccase exhibited similar oxidation catalytic efficiency with substrate syringaldazine to free enzymes. The immobilized enzyme retained 91% activity after 56 days storage at 4 °C and retained 78% activity after 10 uses. Demirci *et al.* immobilized  $\alpha$ -glucosidase and co-factor reduced *L*-glutathione in a poly(2-hydroxyethyl methacrylate) (p(HEMA)) gel.<sup>133</sup> The entrapment process was carried out by mixing  $\alpha$ -glucosidase and *L*-glutathione, with monomer 2-hydroxyethyl methacrylate, **3**, and **7** and **9**. The resulting solution was placed in a cryogenic (low temperature) environment of -18 °C and finally, **8a** was added to the cold enzyme solution with mixing. The polymerized gel, a cryogel, formed at -18 °C. The hydrolytic activity of the immobilized enzyme was investigated using *p*-nitrophenyl- $\beta$ -glucopyranoside



(pNPG) as a substrate in buffer. The immobilized enzyme retained 92% of the activity of the free enzyme and 50% of its activity after 10 days storage at 25 °C. A drop in activity of 50% was observed after 10 reuses. The same research group further studied the entrapment of  $\alpha$ -glucosidase and co-factor reduced L-glutathione in neutral, anionic and cationic polymers of 1, 2-acrylamido-2-methyl-1-propane sulfonic acid (AMPS) 4, 3-acrylamidopropyltrimethyl ammonium chloride 5 (APTMAcL) cryogel and investigated the enzyme activity using  $\beta$ -glucopyranoside (p-NPG) as a substrate in buffer.<sup>134</sup> The immobilized gels exhibited 81%, 62%, and 60% activity, respectively, compared to the free enzymes. The anionic (p(AMPS)) and cationic (p(APTMAcL)) cryogels exhibited unusual pH stability and retained 100% activity at pH 8 and pH 5, respectively.

Wang and co-workers immobilized HRP in a self-catalyzed poly(*N,N*-dimethylacrylamide) gel in a water-in-oil (O/W) emulsion.<sup>135</sup> The oil phase was prepared using the surfactants tween 20 and span 80 in octane and acetylacetone. An aqueous solution of HRP, *N,N*-dimethylacrylamide 6 and 7 were added slowly to the oil phase to form the water-in-oil emulsion. Addition of hydrogen peroxide to the emulsion initiated the HRP mediated radical formation of acetylacetone that mediated the polymerization reaction, and HRP was entrapped within the polymer hydrogel. The process was carried out under argon to suppress radical quenching. The catalytic activity of the immobilized HRP retained 75% activity compared to the free enzyme for the oxidation of *o*-phenylenediamine (OPD) in the presence of H<sub>2</sub>O<sub>2</sub>. The immobilized enzyme retained 98.5% activity after 3 months storage at 4 °C. The enzyme immobilized gel exhibited good thermal stability and retained 33% activity after heating at 70 °C for 30 min, higher than the free enzyme, which retained only 14% activity under the same conditions.

LentiKats® is a polymer entrapment system based on a polyvinyl alcohol (PVA) matrix which has demonstrated excellent performance with whole cell biocatalysts.<sup>136</sup> LentiKats® technology has also been applied to enzyme immobilization. An enzyme can be entrapped in LentiKats® by dissolving PVA and polyethyleneglycol (PEG) in water at 90 °C, and while the solution is cooling at 40 °C, an enzyme solution is added. Beads are made by using a LentiPrinter device.<sup>137,138</sup> Rebroš *et al.* immobilized the enzyme glucoamylase in LentiKats® for the hydrolysis of maltose to glucose.<sup>139</sup> The immobilized enzyme exhibited 35% residual activity compared to the free enzyme, however, the immobilized enzyme maintained 80% activity after 100 recycles in a batch process at 30 °C. In addition, the immobilized enzyme retained the initial activity of 60% conversion for 1520 h in a continuous process at 60 °C. The initial activity loss of immobilized glucoamylase was high, however, the stability and reusability of the process circumvented the initial activity loss.

Polymerisation methods based on hydrogel formation have a wide applicability. Akin to sol-gel methods, the techniques involved can be quite specialized and would benefit from simple protocols that are widely applicable.

### 3.3 Biopolymers

The immobilization of enzymes and biocatalysts in biopolymers, such as proteins and carbohydrates is well established and has been the subject of recent reviews.<sup>46,140–142</sup> Biomaterials are attractive due to their non-toxicity, biodegradability, flexibility and availability.<sup>142</sup> This review will concentrate on methods in which the enzyme becomes entrapped. There is some overlap between entrapment and crosslinking methods, as biopolymers are frequently gelled by the addition of a crosslinking agent, such as Ca<sup>2+</sup> for alginates. In this review we define entrapment as a solid or gel forming event which occurs in the presence of the enzyme and incorporates it within the structure, but does not directly involve the enzyme. The term 'crosslinked' is reserved for immobilization methods that formally involve the protein of the enzyme in the crosslinked structure. The biopolymer method depends on the initiation of additional bonds (supramolecular or covalent) to a macromolecule that is already formed (Fig. 3C). Biopolymer gels can be soft or hard gels depending on whether the method of crosslinking is reversible or not. Carbohydrate based biopolymers alginate 10, cellulose 11, chitosan 12, chitin 13 and agarose 14 (Fig. 8) are promising materials for enzyme immobilization.

Carbohydrate-based biopolymers are highly biocompatible and contain multiple functional groups that make these molecules suitable for enzyme immobilization *via* entrapment methods. Bilal and Iqbal have recently reviewed and highlighted the potential of carbohydrate based natural polymer for enzyme immobilization.<sup>46</sup> In this section progress on biopolymer-based materials for enzyme entrapment will be discussed, with representative examples. We refer the reader to published reviews for further details. Discussions will concentrate on alginate and silk fibroins for enzyme/biocatalyst entrapment.

Alginate 10 is a negatively charged polysaccharide, and in the presence of divalent metal ions, particularly calcium (Ca<sup>2+</sup>), alginate crosslinks to form a biopolymer gel. Arruda and Vitolo immobilized invertase in Ca-alginate for sucrose hydrolysis.<sup>143</sup> The enzyme was immobilized by the dropwise addition of enzyme-alginate solution to CaCl<sub>2</sub> solution and left for 24 h. The immobilized enzyme retained 73% activity compared with the free enzymes at pH 4.6 and 30 °C. Quiroga *et al.* immobilized cysteine protease araujain in Ca-Alginate beads, and demonstrated high thermal stability at 70 °C and pH range 5–9.5.<sup>144</sup> The enzyme retained 92% of its initial activity and 78% of its activity after 20 runs. The enzyme performance was optimized in biphasic 1 : 1 aqueous/ethyl acetate.

The protein silk fibroin (SF) has a stable and flexible conformation that allows the design of immobilized materials with different shapes and sizes, like powders, scaffolds, membranes, films, and spheres.<sup>141</sup> Fukui and co-workers first reported entrapment of  $\beta$ -glucosidase in a silk fibroin membrane.<sup>145</sup> The enzyme immobilized silk membrane was made by mixing the aqueous solution of the silk fibroin and the enzyme, and the resultant mixture was air dried for 24 h at



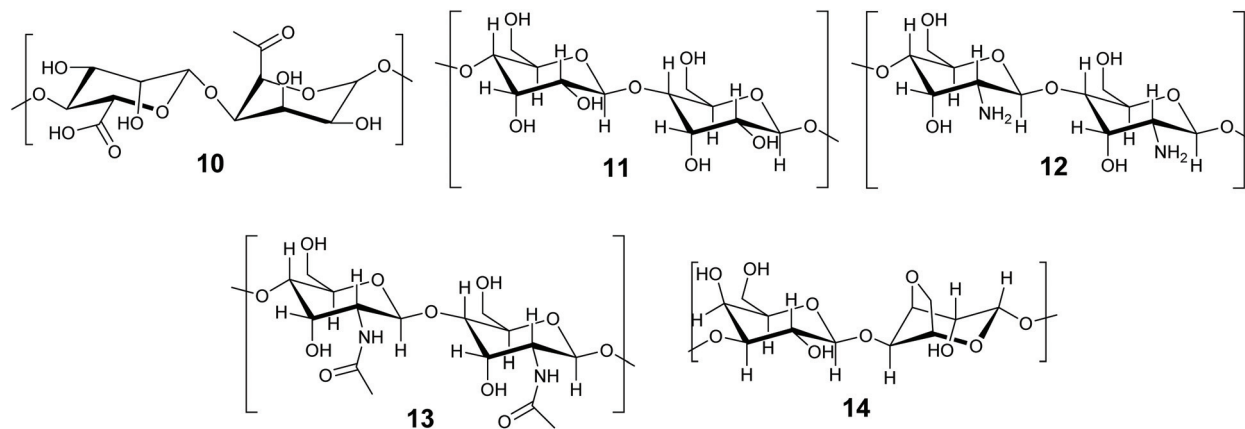


Fig. 8 The chemical structure of some biopolymers used for enzyme entrapment.

20 °C. The membrane entrapped enzyme retained 47% of the activity of the soluble enzyme in the hydrolysis of *p*-nitrophenyl- $\beta$ -D-glucopyranoside in acetate buffer (50 mM, pH 5.7) at 25 °C, and exhibited high thermal stability, retaining 90% activity at 55 °C, compare to 50% activity for the free enzyme. Activity dropped to 87% with 20 re-uses in 20 days with storage in the buffer containing the substrate. Glucose oxidase entrapped in a silk fibroin membrane exhibited 80% activity compared to the free enzyme in the oxidation of glucose in buffer at 25 °C, and was stable for 30 days.<sup>146</sup> Immobilized enzyme activity was found to decrease with increased enzyme loading.

Silk fibroin entrapped horseradish peroxidase was used as a sensor for hydrogen peroxide detection using tetrathiafulvalene as the electron carrier.<sup>147</sup> Murine anti-TGF $\beta$  and IgG1 mono-clonal antibodies were entrapped in a silk fibroin hydrogel and lyophilized gel.<sup>148</sup> The gels were made by sonicating silk fibroin to make a sol, then the antibody was added to the sol to form a silk fibroin hydrogel and lyophilization of the hydrogel produced the lyophilized gel, both the gels were used for controlled release of the antibody.

Carbonic anhydrase (CA) was entrapped in a metal mediated photochemically induced SF hydrogel.<sup>149</sup> The hydrogel was made by mixing the enzyme and silk fibroin in buffer with a solution of APS **8b** (Fig. 7B) and [Ru(bpy)<sub>3</sub>]Cl<sub>2</sub>. The resulting solution was mixed, and irradiated using white light (100 W fiber optics) for 10 min. The immobilized CA hydrogel exhibited >60% activity relative to the free enzyme in the hydrolysis of *p*-nitrophenyl acetate (pNPA) in buffer. Some increase in stability was reported at pH 3.

Biopolymer methods are often simple and cheap, and this makes them easily accessible. Development of these method must concentrate on achieving good reproducibility of structure and performance.

### 3.4 Supramolecular assembly using low molecular weight gelators

Low molecular weight gelators (LMWGs), are small to medium size (usually organic) molecules used to gel solvents by supra-

molecular assembly (Fig. 9). A LMWG that gels an organic solvent is referred to as an organogelator. LMWGs can also gel water to form a hydrogel, or an ionic liquid to form an ionic liquid gel. LMWGs form gels by supramolecular interactions such as H-bonds, hydrophobic interactions and  $\pi$ - $\pi$  stacking to form supramolecular assemblies, thus LMW gels are frequently soft and reversible in nature.<sup>150,151</sup> The self-assembly process requires the LMWG to dissolve in the solvent, and under influence of a stimulus, the gelator will self-organized to form the gel. The common stimuli are heating and cooling, pH change and enzyme activity.

Xu and co-workers immobilized methemoglobin, horseradish peroxidase, laccase and  $\alpha$ -chymotrypsin in a 9-fluorenylmethoxycarbonyl-L-lysine (Fmoc-K) **15** and Fmoc-L-phenylalanine (Fmoc-F) **16** hydrogel.<sup>152</sup> The enzyme immobilized hydrogel was made using a heating-cooling process by heating the aqueous suspension of **15**, **16** and sodium carbonate at 60 °C to give a solution, when the solution was cooling at 35–40 °C, aqueous enzyme was added to the solution and cooling at room temperature gave the enzyme immobilized hydrogel. The immobilized enzyme gels exhibited better oxidation activity in toluene than in aqueous buffer. For example, immobilized methemoglobin and free methemoglobin showed very similar activity in pyrogallol oxidation to purpurgallin in buffer, however, the immobilized enzyme exhibited 8 times higher oxidation activity in toluene than the free enzyme oxidation in the aqueous buffer. UV-Vis and CD spectroscopic studies revealed that the immobilized enzymes in the hydrogel retained the structure as it was in water.

Ulijn and co-workers, immobilized lipase B in a peptide hydrogel of Fmoc-diphenylalanine (Fmoc-FF) **17** co-assembled with Fmoc-amino acid **18a–18d**. The resultant gel was further stabilized using silica nano particles.<sup>153</sup> The enzyme immobilized hydrogel was made using a pH variation method by dissolving **17** and **18** in basic aqueous media followed by sonication to give a solution, the pH was adjusted to 7.8 and addition of CaCl<sub>2</sub> formed the gelator solution. The enzyme in buffer was added to the gelator solution, and the enzyme-gelator solution was dispersed into silica nanoparticles in



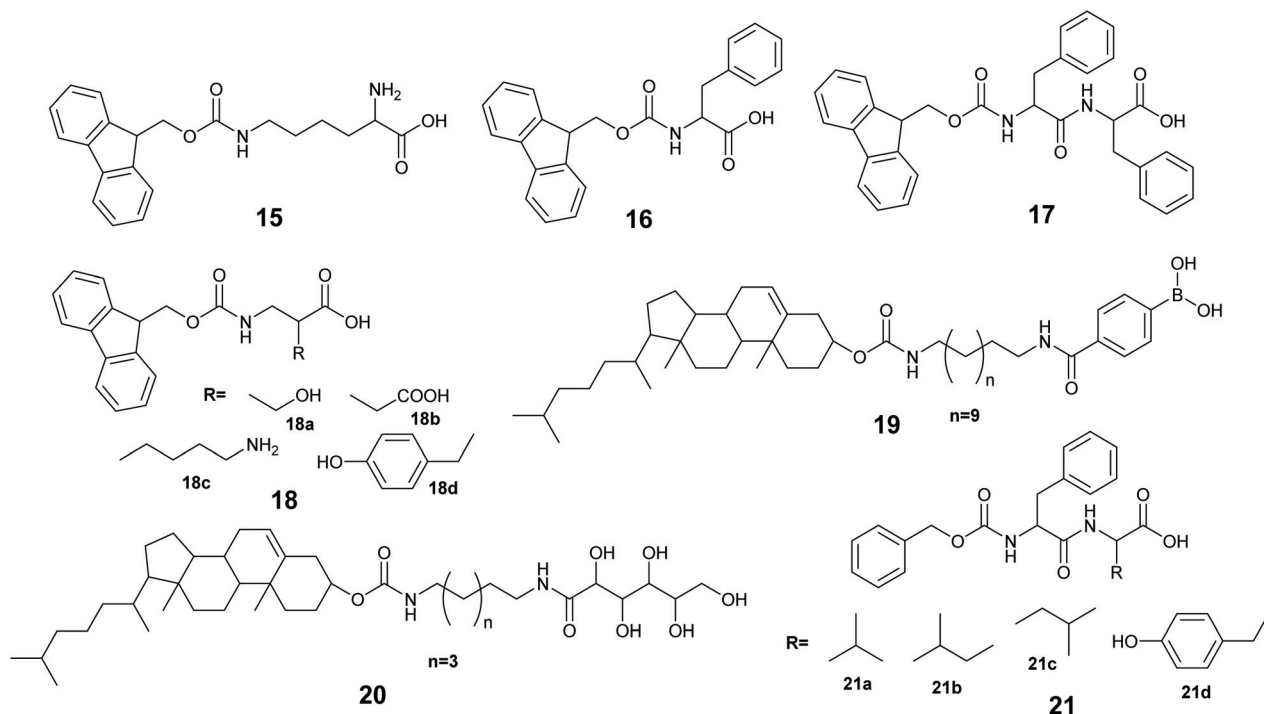


Fig. 9 The chemical structures of LMWGs used to entrap enzymes in gels.

heptane. After homogenization, the resultant mixture was left at 2–8 °C for silica stabilized peptide gel formation. The silica stabilized enzyme hydrogel made from **17** and **18a** exhibited 4 times higher activity compared with the free enzyme in the transesterification of 1-octanol and octanoic acid in heptane.

Das and co-workers developed cholesterol based phenylboronic acid, and glucose based LMWGs **19** and **20** that gel DMF-water mixtures.<sup>154</sup> A gel of **19** was used to entrap lipase and **20** was used to entrap the prodrug chloramphenicol ester or a model substrate *p*-nitrophenyl-*n*-octanoate. Mixing of the gels was found to destruct both due to the formation of a boronate-diol adduct that allowed the lipase to catalyze the prodrug/substrate and control the release of the active drug/product.

Roy and co-workers immobilized Lipase from *Candida rugosa* in a hydrogel *via* co-assembly of the enzyme with LMW dipeptides **21a–21d**.<sup>155</sup> The dipeptides **21a–21d** were unable to form the hydrogel, however, addition of the enzyme induced gel formation.<sup>155</sup> The gelation occurred *via* weak interactions of the peptide with lipase. The entrapped lipase hydrogel was active at catalyzing the hydrolysis of *p*-nitro phenylbutyrate (pNPB) in water.

The use of soft gels to support biocatalysts offers the advantages of ease of synthesis and recycle. An effective environment can be created swiftly to support enzyme activity at little cost, allowing enzymes to be operated in solvent environments they would not otherwise be stable in. The application of LMWGs to enzyme entrapment is less developed than sol–gel methods, but the area holds much promise, particularly if reliable methods to mechanically strengthen the gels can be found.

The choice of LMWG should be informed by the principles of green chemistry and favour the use of molecules derived from nature which require little chemical modification to render them gel forming. Examples of sugar derived LMWGs are given in section 5.3.3.

## 4. Innovations in enzyme entrapment

In this section recent developments in the entrapment of enzymes, that do not fit exclusively into the traditional categories described in section 3, are discussed. Innovations that involve ionic liquids are discussed separately in section 5.

### 4.1 Metal-organic frameworks

A metal organic framework (MOF) is a metallic cage in which metals are connected by organic ligands acting as linkers, that provide the cage with a high porosity and surface area. MOFs have been utilized to entrap many molecules, including enzymes.<sup>156–158</sup> The enzyme can be adsorbed, crosslinked, covalently bonded, diffused and entrapped in a MOF.<sup>159</sup> In entrapment by *in situ* processes, the MOF forms from the MOF precursor building blocks in the presence of the enzyme (Fig. 10). MOF enzyme entrapment can be achieved *via* biomineralization and co-precipitation methods.

Liu and co-workers first reported *in situ* enzyme immobilization in a MOF.<sup>160</sup> They immobilized Cytochrome C (Cyt C) in MOF ZIF-8 (a zeolitic imidazolate framework, constructed from Zn<sup>2+</sup> and 2-methylimidazolate ions). Polyvinylpyrrolidone was added to stabilize the enzyme in methanol. The entrapped



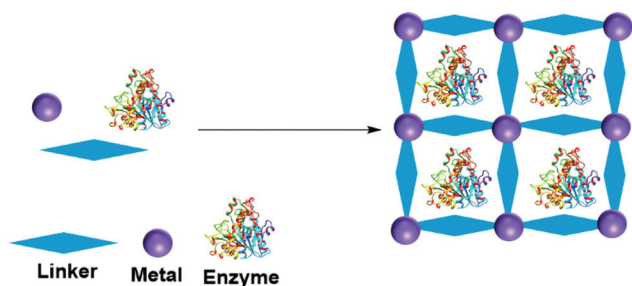


Fig. 10 Schematic representation of *in situ* enzyme entrapment in a MOF.

Cyt C exhibited 10 times higher peroxidase activity in the oxidation of 2,2'-azinobis(2-ethylbenzthiazoline-6-sulfonate) (ABTS) in the presence of H<sub>2</sub>O<sub>2</sub> in buffer compared to the free Cyt C in solution. In parallel three other research groups developed mild aqueous processes for *in situ* non-covalent enzyme entrapment in MOFs.<sup>161–163</sup> Tsung and co-workers immobilized catalase in ZIF-90 MOF crystals from ZIF-90 precursors of 2-imidazolecarboxaldehyde and zinc nitrate in an aqueous media. The enzyme was entrapped within pores that were smaller than the size of the enzyme.<sup>161</sup> The MOF entrapped catalase exhibited hydrogen peroxide degradation activity and protected catalase from protease degradation. However, mass transfer limitations due to the structure resulted in low hydrogen peroxide degradation activity compared to the enzyme in solution.

Liang *et al.* immobilized bovine serum albumin in ZIF-8, using a biomineralization method.<sup>162</sup> In the biomineralization method, the enzyme acts as the nucleation point and influences the MOF crystal growth and material porosity. This method allows the enzyme to be released from the MOF crystal by a pH change. Using the biomineralization method, they were able to immobilize 11 different proteins with 86–100% loading efficiency and with enhanced catalytic activity. Horseradish peroxidase (HRP) in ZIF-8 oxidized 88% of pyrogallol to purporogallin in the presence of trypsin, compare to 20% for the free enzyme.

Liu and co-workers entrapped glucose oxidase (GOx) and Horseradish peroxidase (HRP) for glucose detection in ZIF-8 in a one pot reaction employing the MOF building blocks in aqueous solution.<sup>163</sup> Ouyang and co-workers immobilized glucose oxidase (GOx) and CytC in ZIF-8 MOF, from MOF precursors.<sup>164</sup> They found that GOx in ZIF-8 retained a similar activity to the free enzyme, whereas Cyt C retained only 10% activity. The study revealed that the enzyme type and enzyme nucleation ability influenced the activity of the enzyme within the MOF. GOx initiated a rapid MOF nucleation and retained enzyme activity. In contrast to GOx, Cyt C does not take part in MOF nucleation leading to a slow nucleation. The slow nucleation process allowed Cyt C to interact with the MOF building blocks, resulting in deactivation. Thermophilic lipase QLM, immobilized in ZIF-8 MOF exhibited enhanced activity towards *p*-nitrophenyl caprylate (pNPC) hydrolysis and (*R,S*)-2-octanol kinetic resolution.<sup>165</sup> lipase QLM in ZIF-8 retained

90% of hydrolysis activity compared to the free enzyme. When exposed to 1 mM of Zn<sup>2+</sup> ions the free enzyme exhibited only 54% activity. The lipase QLM in ZIF-8 MOF retained activity for 5 days at 37°. 76% activity was retained after 5 days at 60 °C. In kinetic resolution of (*R,S*)-2-octanol with vinyl acetate in dichloromethane (DCM) the lipase QLM in ZIF-8 MOF gave 80% ee, lower enantioselectivity than the free lipase with 85% ee. One pot immobilization of lipase with ZIF-8 precursors increased the lipase heat stability, storage ability and recyclability.<sup>166</sup> ZIF-8 nMOF (nano-MOF) enabled multiple enzyme entrapment for enzymatic cascade reactions.<sup>167</sup> For example, enzymes GOx and HRP entrapped in ZIF-8 nMOF retained >90% free enzyme activity.

MOFs have exhibited some impressive qualities as matrices for enzyme entrapment. However, MOFs by nature are metal-rich and the life cycle, cost and recyclability of these systems will have to be considered if they are to be employed in an industrial setting.

#### 4.2 Smart gels: enzyme responsive entrapment

Enzyme assisted gel formation is a smart approach to the entrapment of enzymes in a non-covalent way, with applications in biomedical, drug delivery, sensing and biocatalysis (Fig. 11 & 12).<sup>168–170</sup> The enzyme activates the gelator and initiates gelation *via* self-assembly, cross-linking, surface activation or polymerization.<sup>48</sup> Low molecular weight gelators and polymeric materials are commonly used as the target for the enzyme.

Acid phosphatase (AP) was used to hydrolyze the phosphate group of the phosphate functionalized molecule **22** and liberate the gelator **23**. This initiated hydrogelation, and the enzyme was entrapped within the hydrogel.<sup>171</sup> The immobilized AP retained 75% activity compared with the free enzyme in the hydrolysis of *p*-nitrophenyl phosphate (pNPP) in water. The immobilized enzyme exhibited 100 times enhanced hydrolytic activity in chloroform compared to water. CD spectroscopy verified the structural integrity of the immobilized AP. Horseradish peroxidase (HRP) catalyzed the polymerization reaction of acetylacetone in the presence of hydrogen peroxide, silica nanoparticles, acrylated Human Serum Albumin (HSA) and *N,N*-dimethylacrylamide (DMAA) resulting in a polymer hydrogel.<sup>172</sup> The enzyme entrapped in the polymer hydrogel exhibited high thermal stability and recyclability in the oxidation reaction of *o*-phenylenediamine (OPD) in toluene and in water. Cascading enzymatic oxidations involving glucose oxidase (GOx) and horseradish peroxidase (HRP) led to co-immobilization of these enzymes into a self-assembled-polymerized hydrogel.<sup>173,174</sup> In the cascade reaction, glucose and acetylacetone were oxidized in the presence of methacrylate PEGMA and NapFFK-acrylic acid as a LMWG. The gel showed activity for the oxidation of *o*-phenylenediamine (OPD) in the presence of H<sub>2</sub>O<sub>2</sub>.

Hydrolytic activity of the enzyme subtilisin was employed to convert the methyl ester protected Fmoc-dipeptide **24** to the parent acid **25**, initiating the formation of a highly ordered gel structure *via* supramolecular assembly.<sup>175</sup> Atomic force microscopy (AFM) revealed formation of self-assembled nano



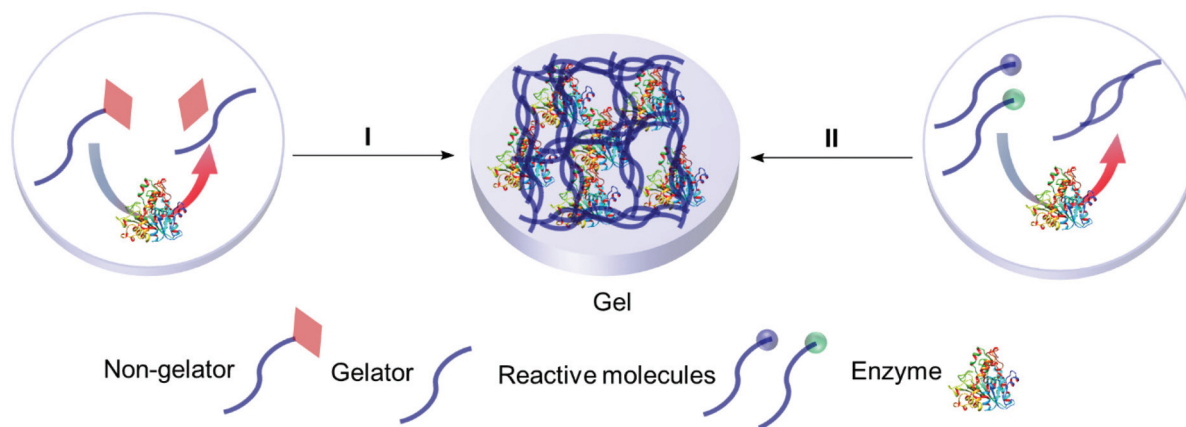


Fig. 11 Schematic presentation of enzyme responsive gel formation.

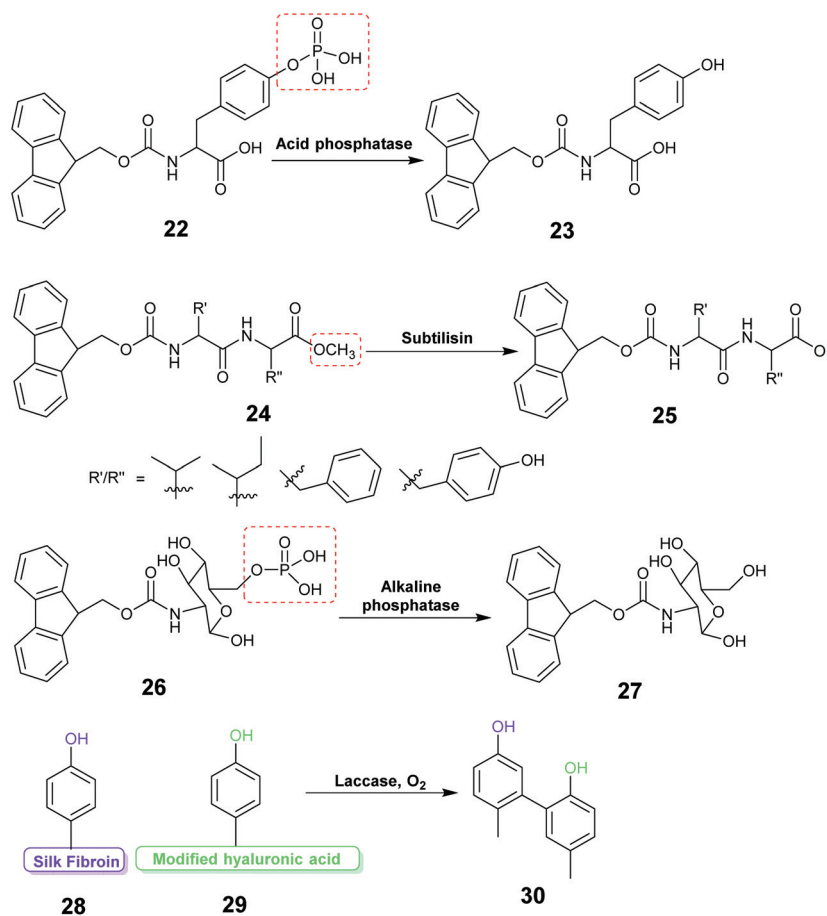


Fig. 12 Examples of reaction schemes for enzyme assisted gel formation.

and micro structure near the enzyme active site forming a catalytic cluster within the gel. The enzyme content was found to affect the gel morphology.

Enzyme responsive gel formation has been demonstrated *in vivo*. Alkaline phosphatase induced dephosphorylation converted the carbohydrate based precursor **26** into the hydrogelator **27**.<sup>176</sup> The process was investigated *in vivo* in the osteo-

sarcoma cell line, SaOs2. The gelation depended on the alkaline phosphatase concentration thus allowing cell selective gelation. Recently the enzyme laccase was used to catalyze the coupling reaction between the tyrosine of silk fibroin (SF) protein and tyramine modified hyaluronic acid to form a highly elastic and mechanically stable SF hydrogel for drug delivery (**28**, **29**, **30**).<sup>177</sup>



Gels that form due to the activity of enzymes are an impressive development. These highly technical systems have specific applications, for example in sensors and medicine.

### 4.3 3D printing

Additive manufacturing, more well known as 3D printing, is a material fabrication process that enables the design of complicated bespoke 3D structures for various applications. Most often the material used as the 'ink' for printing is gel-like in nature. This provides opportunities for the 3D printing of enzyme-containing gels to form different shapes. This could find applications in, for example, flow biocatalysis.<sup>178</sup>

$\beta$ -Galactosidase ( $\beta$ -Gal) from *Aspergillus oryzae* in water-in-oil high internal phase emulsions (HIPEs) was used as a 3D printable bio-ink for enzyme entrapment in a cylinder shape hydrogel surrounded by a porous polymeric material.<sup>179</sup> The water-in-oil emulsions were made by mixing an oil phase containing of 2-ethylhexyl acrylate (EHA), isobornyl acrylate (IBOA), trimethylolpropane triacrylate (TMPTA), surfactant Pluronic® L-121, and photo initiator (Darocur®TPO) with a water phase, made from acrylic acid (AA), poly(ethyleneglycol) diacrylate (PEG-DA700), lithium phenyl-2,4,6-trimethylbenzoylphosphinate (LAP) and  $\beta$ -galactosidase. The emulsion was molded in a 48 cylindrical well microplate and subjected to UV-LED for polymerization at  $25\text{mW cm}^{-2}$  for 2 min to give a hydrogel surrounded by an outer porous polymeric material. Extensive washing was required to remove unbound material. Activity in the hydrolysis of *ortho*-nitrophenyl  $\beta$ -D-galactopyranoside (ONPG) in buffer depended on the content of the monomer and aqueous phase. The printing nozzle size influenced the activity, with a fourfold increase in specific activity observed for  $110\ \mu\text{m}$  nozzles, compare to  $840\ \mu\text{m}$  nozzles. The system suffered from mass transfer limitations and enzyme inactivation.

Laccase was immobilized within a cube shaped pore structure by 3D printing and the activity of the enzyme investigated for *p*-chloro phenol degradation.<sup>180</sup> For 3D printing, the enzyme solution with or without hydroxyapatite (a calcium mineral) was added to a hydrogel solution of the biopolymer precursor sodium alginate **10** (Fig. 8) and  $\text{CaCl}_2$  with synthetic polymer (polyacrylamide) precursor **1** (Fig. 7B) and BIS **7**, TEMED **9** and APS **8b**. The enzyme hydrogel solution was molded into a cube shape using 3D printing. The immobilized laccase exhibited good stability, retaining over 80% of its

initial activity after 72 h of storage. Conversion of the substrate dropped to 60% after 7 reuses.

3D printing holds a lot of promise, particularly for the application of industrial biocatalysis for flow reactions. This area is expected to expand rapidly.

### 4.4 Hybrid materials

In this review we use the term hybrid material to refer to substances that are a mixture of more than one material type. Such as an organic polymer modified with an inorganic oxide. Combining two or more different materials can afford better stability, mass transfer and reaction compatibility to the enzyme entrapped material. Many combinations can be envisaged of inorganic & organic materials, LMWGs, MOFs and biopolymers.

Smith and co-workers entrapped alkaline phosphatase in a LMWG gel of **31** strengthened with polymer **32** (Fig. 13). This hybrid enabled the formation of a ring shaped bioreactor.<sup>181</sup> This was constructed by mixing the enzyme into a solution of **31** in DMSO/water at  $80\ ^\circ\text{C}$ , the hot enzyme-gelator solution was then poured into a glass mold to form the gel. The monomer for **32** and photo initiator (Irgacure 2959) were added and allowed to diffuse through the gel. Irradiation with long wavelength UV light resulted in alkaline phosphatase immobilized in the polymer reinforced LMWG gel. The entrapped enzyme was active for the hydrolysis of *p*-nitrophenol phosphate (pNPP).

Epoxide hydrolase SpEH and Bovine serum albumin (BSA) were entrapped into a hybrid inorganic-organic capsule made from Fmoc-FF **17** (Fig. 9), sodium silicate and polyethyleneimine in aqueous solution.<sup>182</sup> The enzyme immobilized hybrid capsule was made by the dropwise addition of a homogeneous aqueous solution of enzyme, **17** and sodium silicate at pH 7–10 to an aqueous polyethyleneimine solution at pH 7.5. The enzyme capsule exhibited high enzyme loading, low enzyme leaching and high activity in the hydrolysis of cyclohexene oxide. The capsule was recycled 20 times and retained 87% of the initial activity.

The aluminium oxide boehmite was combined with alginate **10** (Fig. 8) to make hybrid beads which were used to immobilize yeast alcohol dehydrogenase (YADH).<sup>183</sup> The enzyme was immobilized by mixing an enzyme solution in buffer into the boehmite sol, this was further mixed with an alginate solution. Finally, the homogeneous enzyme-boehmite-alginate solution was added dropwise to a  $\text{CaCl}_2$  solution to

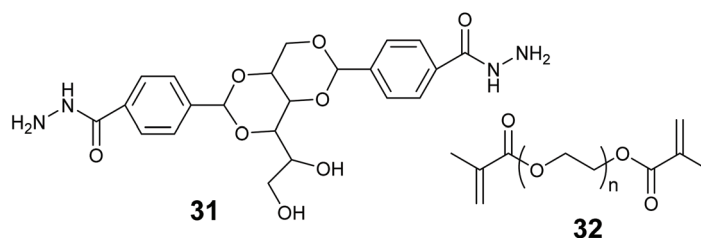


Fig. 13 Chemical structure of the LMWG and polymer used to make a hybrid reactor for biocatalysis.



form beads. The immobilized YADH hybrid beads retained 7% of the activity of the free enzyme in the reduction of formaldehyde to methanol in the presence of nicotinamide adenine dinucleotide (NADH) in buffer. The low activity of the immobilized enzyme was attributed to mass transfer limitations due to the compact nature of the beads. After 12 cycles the immobilized enzyme retained 87% of its original activity without leaching.

Carbonic anhydrase (CA) was entrapped in magnetite sol-gel matrices by mixing the enzyme solution in buffer with a magnetite sol and drying for 24 h. The immobilized enzyme retained similar activity to the free enzyme for the hydrolysis of *p*-nitrophenyl acetate (pNPA) in buffer.<sup>184</sup> The immobilized enzyme exhibited higher thermal stability, retaining 95% activity at 65 °C, at this temperature the free enzyme retained 55% activity. Incorporation of magnetic Fe<sub>3</sub>O<sub>4</sub> nanoparticles during the sol-gel process facilitated the easy separation of the immobilized enzyme.<sup>109</sup> The process enhanced the esterification activity of lauric acid with *n*-octanol by 200–300% and gave 97–99% ee in the kinetic resolution of 2-pentylamine with ethyl acetate in *t*-butylmethyl ether.

Lipase (Cal B) was immobilized in an agarose **14** (Fig. 8) hydrogel stabilized by magnetic a ZIF-8 MOF capsule.<sup>185</sup> Cal B in the hybrid magnetic ZIF-8 MOF capsules exhibited 2.6 times higher activity compared to the Cal B in the hydrogel alone in the transesterification reaction of 1-butanol and vinyl acetate in acetone, however, with large substrates 3-(4-hydroxyphenyl)propan-1-ol and vinyl laurate, no detectable transesterification was observed for Cal B in hybrid magnetic ZIF-8 MOF capsules after 12 h, and only 7.5% conversion was observed at 48 h, whilst 100% conversion was obtained for the Cal B hydrogel at 12 h. Mass transfer limitations and capsule pore blockage were suggested as reasons for the low conversions.

Enzymes tyrosinase (Tyr) and  $\beta$ -glucosidase ( $\beta$ -glu) were co-immobilized in magnetic polydopamine-alginate beads using enzyme assisted polymerization and gelation processes.<sup>186</sup> The enzyme immobilized hybrid beads were made by mixing a homogeneous solution of Fe<sub>3</sub>O<sub>4</sub> nanoparticles,  $\beta$ -glucosidase and substrate *D*(+)-gluconic acid  $\delta$ -lactone into a homogeneous solution of tyrosinase, sodium alginate, substrate dopamine hydrochloride and hydroxylapatite (a calcium mineral). The polymerization and gelation process occurred as tyrosinase polymerized dopamine to poly-dopamine and  $\beta$ -glucosidase converted *D*(+)-gluconic acid  $\delta$ -lactone to gluconic acid. The gluconic acid subsequently released Ca<sup>2+</sup> ions from the hydroxylapatite, initiating the gelation of the alginate. In order to form beads the homogeneous solution was dropped into a CaCl<sub>2</sub> solution with excess *D*(+)-gluconic acid  $\delta$ -lactone. The immobilized enzyme beads were investigated for the inhibitory activity of tea polyphenol extracts using levodopa and *p*-nitrophenyl- $\beta$ -*D*-glucosidase (pNPG) as substrates in buffer. The immobilized  $\beta$ -glucosidase and tyrosinase retained 79% and 78% activities compared to 54% and 46% for the free enzymes, respectively, after 35 days at 4 °C.

Methods that require relatively few synthetic steps and create hybrid materials with desirable properties promise to

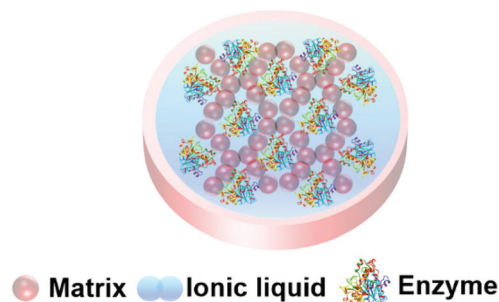
widen the potential applications of entrapped enzymes, by creating materials with physical properties that can be tuned and fitted to suit process parameters.

## 5 Ionic liquid materials for enzyme entrapment

### 5.1 A brief introduction to ionic liquids

Ionic liquids are a class of liquid comprised entirely of positive and negative ions held together by electrostatic interactions. The term ionic liquid (IL) is usually reserved for ionic materials that are liquid under mild to moderate conditions. ILs are a diverse class of materials, but research in the public domain has mainly concentrated on larger cations with significant organic groups (imidazolium, pyrrolidinium, ammonium, phosphonium) and relatively small anions (halide, triflate, sulfonate, acetate). The diversity of ILs provides opportunities to manipulate chemical and physical properties and create combinations that are significantly different from common salts and existing solvents.<sup>187,188</sup> This tuning of the ionic liquid's properties makes ILs unique liquids for enzymes and biocatalysis, and the low volatility and flammability of ILs render them safer and less likely to damage biomaterials.<sup>35,37,38,189–195</sup>

Enzymes tend to degrade when stored in conventional aqueous and organic solvents, potentially limiting their widespread industrial applications in chemical synthesis. The reuse and recovery of biocatalysts is particularly challenging. ILs can be tuned to support protein stability by manipulating properties such as hydrophobicity, electrostatic properties, H-bonding, and Brønsted acidity/basicity, thus offering a bespoke environment for a given enzyme, and supporting structural folding and catalytic activity.<sup>193</sup> As the protein-stabilizing properties of ionic liquids have become apparent, the entrapment of enzymes within IL materials has begun. A green and sustainable enzyme entrapment method should retain the enzyme activity for a long time and render the enzyme reusable without leaching of the enzyme nor the entrapment material to the reaction medium. The principle of entrapment in an ionic liquid material (Fig. 14) is that, by tuning the solubility of the IL, the passage of chemicals into and out of the



**Fig. 14** Schematic presentation of an ionic liquid gel. The matrix exterior protects the enzyme and the ionic liquid supports enzyme activity.





gel can be controlled, in order to protect the catalyst from harsh reaction conditions.<sup>197</sup> The ionic liquid keeps the enzyme in a liquid environment that promotes the right protein conformation for catalytic activity.<sup>63,161,162,196</sup> Enzyme entrapment in an IL gel can thus act to encapsulate and store enzymes in their active form. Key to achieving these beneficial effects is the understanding of an enzyme's dissolution, stability and structure–activity relationships within ILs.

## 5.2 Enzymes in ionic liquids

A large variety of enzymes and ionic liquids exist, thus offering many opportunities to manipulate an enzyme-IL pair to maximize enzyme solubility and stability.

### 5.2.1 Enzyme solubility & dissolution in ionic liquids.

Enzyme dissolution in a neat IL can take 1–5 days at temperatures of 30–60 °C.<sup>199–201</sup> Good dissolution will require interaction between the protein and the IL, but care must be taken that the interaction is not strong enough to disrupt protein folding. For this reason, very small ions, such as thiocyanate, are not usually employed.<sup>201</sup> High viscosity ionic liquids should also be avoided as they will reduce enzyme activity due to substrate mass transfer limitation. High viscosity, poor solubility and detrimental interactions can be overcome by operating in an ionic liquid mixture, or an ionic liquid/aqueous solution.<sup>202–209</sup> Water content plays a significant role in enzyme stability. At higher water content, the IL will behave as a solute/osmolyte for the enzyme.<sup>210</sup> This can lead to strong interactions with the enzyme, and enzyme inactivation. The optimum ratio of water and IL will depend on the specific protein/ionic liquid combination.

Judicious choice of the ionic liquid can promote refolding of aggregated proteins. For example aggregated Concanavalin

A (ConA) was shown to be resolvable in a hydrophobic phosphonium ionic liquid with a long alkyl chain (C<sub>16</sub>), and dihydrogen phosphate (dhp) anion at low water content.<sup>211</sup> The intrinsically disordered protein Anti-Sigma factor (FlgM), folded in an aqueous solution of the hydrophobic IL 1-butyl-1-methylpyrrolidinium bis(trifluoromethylsulfonyl)amide ([Bmpy][NTf<sub>2</sub>] Fig. 15, 39).<sup>212</sup> The IL [Bmpy][NTf<sub>2</sub>] was shown to increase the alpha helix content of the protein.

Recently ionic liquid research has shifted towards the design and application of biomass derived, less toxic, and environmentally benign ionic liquids. Many of these ILs will have good enzyme compatibility. Of major interest are IL cations derived from choline and lactam, and anions derived from amino acids and fatty acids. Protic ionic liquids are enjoying a come-back, as they can be derived from inexpensive, bulk chemicals, preferably from renewable resources, and are easier to make.<sup>213–215</sup> Cholinium [Ch] (cation of Fig. 15, 34) ionic liquids can be biodegradable, non-toxic and aqueous water/buffer soluble.<sup>216,217</sup> Cholinium ILs with different anions, for example amino acids, are emerging as a green and sustainable ionic liquid media for enzyme/protein stability and activity studies.<sup>204,217–219,220,221</sup> Fatty acid<sup>222–225</sup> and lactam<sup>226,227</sup> based ionic liquids are also likely to significantly contribute towards the library of greener ILs for future industrial biocatalytic processes.

Proteins can be rendered more soluble in ionic liquids by manipulating the surface charges. The protein modification can be achieved by covalently bonding charged or neutral molecules onto the protein. For example polyether carboxylic acid and amine modifiers have been used to significantly enhance the activity of myoglobin dissolved in neat anhydrous ILs, thermal stability was also enhanced.<sup>228</sup> In addition to

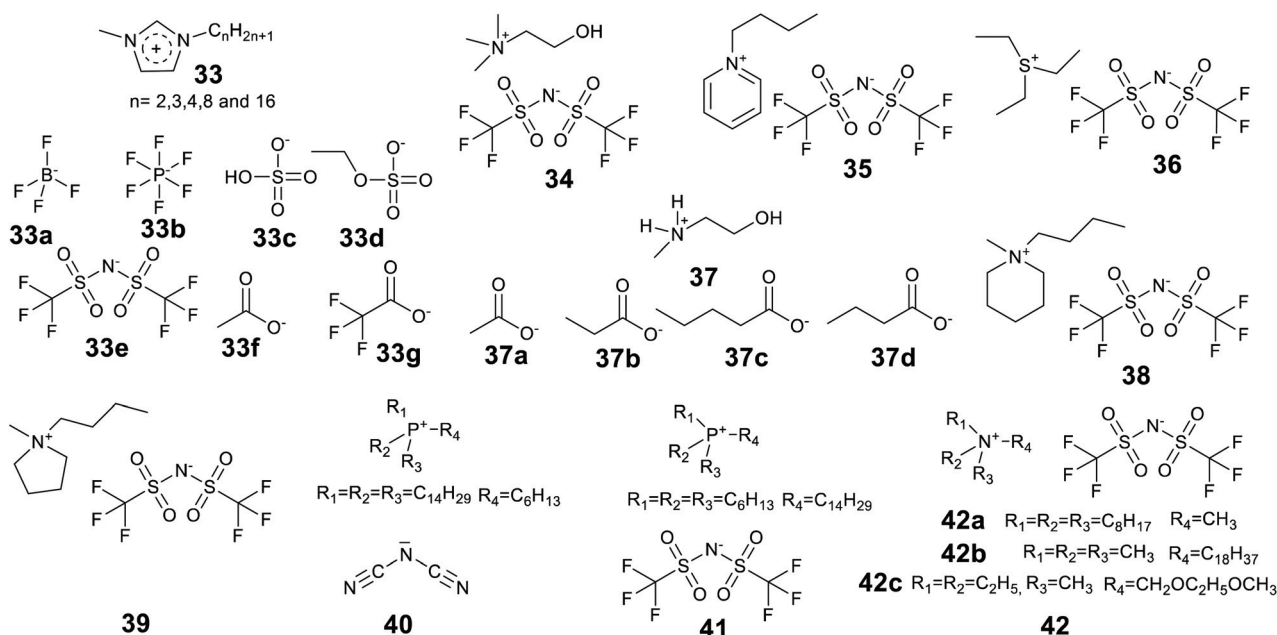


Fig. 15 The chemical structure of some ionic liquids used in enzyme research.



covalent modification, genetic manipulation by site directed mutagenesis can also be used.

### 5.2.2 Enzyme structure and activity in ionic liquids.

Examples of rate enhancement in enzymes due to the addition of ionic liquids are well known. It has been proposed that aqueous 'hydrophobic' ILs form a microenvironment for the enzyme enhancing the stability and activity and that this relates to structural enhancement.<sup>229</sup> Ion-protein interactions are highly complex and specific and there are currently no shortcuts to trial-and-error searches for the optimal IL to enhance enzyme activity. However, modelling and spectroscopic methods are improving rapidly.

### 5.3 Co-entrapment of enzymes and ionic liquids

Ionic liquids have been found to assist the formation of gels for enzyme entrapment (Table 2). Methods were briefly reviewed in 2016,<sup>91</sup> here we provide an updated and more comprehensive treatment of the progress of enzyme entrapment in ionic liquid gels.

**5.3.1 Enzymes encapsulated or coated in ionic liquids.** In order to provide a historic perspective on the use of ionic liquids in enzyme entrapment some exemplar studies are discussed here that are not strictly entrapment as defined in this review. They are included as they provide valuable insights into the use of ionic liquids in isolated enzyme biocatalysis.

Lee and Kim introduced the technique of coating enzymes in ionic liquids. Lipase from *Pseudomonas cepacia* was coated in 1-(3'-phenylpropyl)-3-methylimidazolium hexafluorophosphate [PPMIM][PF<sub>6</sub>] ionic liquid for the preparation of acetate esters of secondary alcohols in toluene at 25 °C.<sup>230</sup> This ionic liquid is solid at room temperature and becomes liquid at 53 °C. Enzyme powder was added to the liquid form of the ionic liquid and mixed to form a homogeneous solution and then the ionic liquid was allowed to solidify at room temperature. The ionic liquid coated enzymes were active and exhibited higher enantioselectivity than the unmodified enzymes. In addition, the ionic liquid enzymes were recycled 5 times maintaining 93% of activity of the native enzyme in the

**Table 2** Entrapment methods used to co-entrap ionic liquids and enzymes

Method	Matrix (catalyst)	Ionic liquid(s)	Enzyme	Test reaction	Ref.
Sol-gel	Silica (HCl)	[BMIM][BF <sub>4</sub> ]	Peroxidase (Horseradish, HRP)	Oxidation	236 and 237
Sol-gel	Silica (HCl)	[EMIM][BF <sub>4</sub> ], [EMIM][PF <sub>6</sub> ], [OMIM][PF <sub>6</sub> ], [EMIM][NTf <sub>2</sub> ], [HDMIM][NTf <sub>2</sub> ], [HDMIM][BF <sub>4</sub> ], [HDMIM][Cl]	Lipase ( <i>Candida rugosa</i> )	Hydrolysis /esterification	243
Sol-gel	Silica (HCl)	[EMIM][BF <sub>4</sub> ], [OMIM][BF <sub>4</sub> ], [BMIM][PF <sub>6</sub> ], [OMIM][PF <sub>6</sub> ], [EMIM][NTf <sub>2</sub> ], [OMIM][NTf <sub>2</sub> ]	Lipase ( <i>Candida rugosa</i> )	Hydrolysis /esterification	238
Sol-gel	Silica (NaF)	[EMIM][BF <sub>4</sub> ], [EMIM][COOC <sub>2</sub> H <sub>5</sub> ], [EMIM][COOC <sub>3</sub> H <sub>7</sub> ], [PMIM][BF <sub>4</sub> ], [BMIM][BF <sub>4</sub> ], [HMIM][BF <sub>4</sub> ], [BMIM][PF <sub>6</sub> ], [BMIM][NTf <sub>2</sub> ], [OMIM][BF <sub>4</sub> ]	Lipase ( <i>Pseudomonas fluorescens</i> )	Acylation	239
Sol-gel	Silica/glycerol (HCl)	Alkyl, hydroxy functionalized imidazolium ILs	Naringinase	Deglycosylation	240
Sol-gel	Silica (HCl)	[N-MMEA][COOC <sub>2</sub> H <sub>5</sub> ], [N-MMEA][COOC <sub>3</sub> H <sub>7</sub> ], [N-MMEA][COOC <sub>4</sub> H <sub>9</sub> ], [BMIM][PF <sub>6</sub> ], [BMIM][BF <sub>4</sub> ]	Lipase ( <i>Bacillus sp. ITP-001</i> ) ( <i>B. cepacia</i> )	Hydrolysis	244 and 245
Self-assembly silica coating	Silica (lipase)	[OMIM][NTf <sub>2</sub> ], [OMIM][PF <sub>6</sub> ], [EMIM][NTf <sub>2</sub> ], [EPY][NTf <sub>2</sub> ], [Ch][NTf <sub>2</sub> ], [S <sub>2,2,2</sub> ][NTf <sub>2</sub> ], [BMIM][NTf <sub>2</sub> ], [BMPI][NTf <sub>2</sub> ], [N <sub>8,8,8,1</sub> ][NTf <sub>2</sub> ], [P <sub>6,6,6,14</sub> ][NTf <sub>2</sub> ], [P <sub>14,14,14,6</sub> ][dca]	Lipase ( <i>Pseudomonas fluorescens</i> )	Esterification	241 and 242
Entrapment polymer-IL gel	Polymer inclusion ionic liquid membranes/polyvinylchloride	[EMIM][NTf <sub>2</sub> ], [EPY][NTf <sub>2</sub> ], [Ch][NTf <sub>2</sub> ], [S <sub>2,2,2</sub> ][NTf <sub>2</sub> ], [BMIM][NTf <sub>2</sub> ], [BMPI][NTf <sub>2</sub> ], [N <sub>8,8,8,1</sub> ][NTf <sub>2</sub> ], [P <sub>6,6,6,14</sub> ][NTf <sub>2</sub> ], [P <sub>14,14,14,6</sub> ][dca]	Laccases ( <i>Trametes versicolor</i> )	oxidation	246
Entrapment polymer-IL gel	<i>N</i> -Iso-propylacrylamide/ <i>N,N</i> O-methylene-bis(acrylamide)/[bis( <i>n</i> -5-cyclopentadienyl) iron]/dimethoxy-phenylacetophenone	[EMIM][EtSO <sub>4</sub> ]	Lactate oxidase	oxidation	247
Microemulsion-based	Hydroxypropyl-methyl cellulose HPMC	[BMIM][PF <sub>6</sub> ]	Lipase B ( <i>Candida Antarctica lipase B</i> )	Esterification	248

Ionic liquids: Cations: [EMIM] 1-ethyl-3-methylimidazolium, [PMIM] 1-propyl-3-methyl-imidazolium, [BMIM] 1-butyl-3-methyl-imidazolium, [HMIM] 1-hexyl-3-methyl-imidazolium, [OMIM] 1-octyl-3-methylimidazolium, [HDMIM] 1-hexadecyl-3-methylimidazolium, [N-MMEA] *N*-methylmonoethanol amine, [Ch] Cholinium, [N<sub>8,8,8,1</sub>] trioctylmethylammonium, [P<sub>6,6,6,14</sub>] trihexyltetradecylammonium, [P<sub>14,14,14,6</sub>] tritradecylhexylammonium, [EPY] *N*-ethylpyridinium, [BMPI] 1-butyl-1-methylpiperidinium, [S<sub>2,2,2</sub>] triethylsulfonium. Anions: [BF<sub>4</sub>] tetrafluoroborate, [PF<sub>6</sub>] hexafluorophosphate, [NTf<sub>2</sub>] bis[(trifluoromethyl)sulfonyl]amide, [COOC<sub>2</sub>H<sub>5</sub>] acetate, [COOC<sub>3</sub>H<sub>7</sub>] butyrate, [COOC<sub>4</sub>H<sub>9</sub>] pentanoate, [COOCF<sub>3</sub>] trifluoroacetate, [dca] dicyanamide, [HSO<sub>4</sub>] hydrogen sulphate, [EtSO<sub>4</sub>] ethyl sulfate, [Cl] chloride.



5<sup>th</sup> recycle. The technique of coating has been significantly developed since, and the review of Itoh and the references therein provide a detailed story.<sup>37</sup> Landmarks include the considerable enhancements of lipase performance, stability and recycling discovered by Itoh *et al.*<sup>231,232</sup> Recently Itoh and co-workers demonstrated complete retention of lipase activity for 2 years when stored coated in the IL [N<sub>221MEM</sub>][NTf<sub>2</sub>] (Fig. 15, 42c).<sup>233</sup>

Lozano *et al.* developed a sponge-like hydrophobic ionic liquid with a long alkyl chain, namely *N*-octadecyl-*N,N,N*-trimethylammoniumbis(trifluoromethylsulfonyl)amide [C18tma][NTf<sub>2</sub>] (42b).<sup>234</sup> This ionic liquid is solid and sponge-like at room temperature and forms a liquid at 60 °C. At 60 °C the liquid phase was used as the reaction medium for the production of biodiesel by lipase-catalyzed methanolysis of triolein with 100% yield at 8 h. The reaction mixture was then cooled and fractionated by centrifugation to separate three phases, the solid IL, the glycerol by-product and pure biodiesel. The enzyme could be fully recovered and reused. The system offered high enzyme stability with a half-life time of 1370 days at 60 °C.

These literature examples illustrate the potential of ionic liquids to facilitate the recycling and support the stable and enhanced activity of isolated enzyme biocatalysts.

**5.3.2 Sol-gel and polymerisation methods employing ionic liquids.** Ionic liquids have a welcome effect on the sol-gel process.<sup>91,198</sup> The low volatility reduces damage to the gel on aging, and the relatively high viscosity of the ionic liquid helps to slow down basic catalyzed reactions.<sup>235</sup>

Aqueous horseradish peroxidase (HRP) in buffer was immobilized in a 1-butyl-3-methylimidazolium tetrafluoroborate [BMIM][BF<sub>4</sub>] silica gel.<sup>236</sup> The IL doped silica gel was 30 times more active for the oxidation of guaiacol in buffer in the presence of H<sub>2</sub>O<sub>2</sub>, at ambient temperature, compare to a silica gel without IL. It was noted that the IL doped silica gel also exhibited good thermally stability. It was suggested that the IL played a dual role as template for the silica matrix and protector of the enzyme structure. The same IL doped silica gel technology was later used in a biosensor.<sup>237</sup> Lipase from *Candida rugosa* in buffer was entrapped in a TEOS-derived silica gel with various imidazolium ILs.<sup>238</sup> The activities of the IL silica gels was investigated in the hydrolysis of *p*-nitrophenyl butyrate operated in buffer and the esterification of benzyl alcohol and benzyl acetate in water saturated hexane. The 1-methyl-3-octylimidazolium bis[trifluoromethylsulfonyl]amide ([OMIM][NTf<sub>2</sub>]) doped gels exhibited the best performance with 5 times higher hydrolytic activity and 16 times higher esterification activity compared to the silica gel without IL. The gel retained 80% of its initial activity after incubation at 50 °C for 5 days.

Lipase from *Pseudomonas fluorescens* was immobilized in a silica gel using different silane sol-gel precursors and various imidazolium based ILs as co-dopants.<sup>239</sup> The gels were made two ways. In the first method silane precursors were added to a pre-mixed solution of lipase in buffer, IL, *i*PrOH and NaF. In the second approach silane precursors in EtOH were added to the lipase in buffer and IL solution. Gels made up from 1 : 1 octyltetramethoxysilane : tetramethoxysilane (OcTMOS : TMOS) silane

precursors and [OMIM][BF<sub>4</sub>] exhibited the best performance in the acylation of 2-heptanol and vinyl acetate in hexane, however the specific activity was low. Naringinase from *Penicillium decumbens* in buffer was immobilized in a silica gel (from TMOS) in the presence of different alkyl, and hydroxy functionalized alkyl imidazolium ILs with glycerol.<sup>240</sup> The IL [OMIM][NTf<sub>2</sub>] and glycerol doped silica gel exhibited better recyclability in *p*-nitrophenyl  $\alpha$ -*L*-rhamnopyranoside (pNRP) hydrolysis in buffer than a similar gel without IL. Bhargava and co-workers studied the self-assembly of the enzymes phytase and lipase in ionic liquids [BMIM][BF<sub>4</sub>] and [BMIM][PF<sub>6</sub>].<sup>241,242</sup> In the ionic liquids the enzymes self-assembled to form enzyme capsules. The phytase capsule was added to TEOS and hydrolysis formed hollow and dense silica nano-structures. Two different orientations of the enzyme with the IL were observed by SEM and TEM analysis. In [BMIM][PF<sub>6</sub>] the enzyme active site was directed towards the hydrophilic part of the IL resulting in a hollow silica structure, whereas in [BMIM][BF<sub>4</sub>] the enzyme active site self-assembled inward to form a solid silica structure. The hollow silica structure retained enzyme activity and was reusable for four runs, whereas the solid silica structure was inactive.

Ionic liquid containing polymer gels are often termed 'ionogels'. Eleven ionic liquids were separately co-entrapped with Laccase from *Trametes versicolor* in polymer gels.<sup>246</sup> The gel was made by mixing an IL containing solution of the enzyme in buffer with a homogeneous solution of IL and polyvinyl chloride (PVC). [Ch][NTf<sub>2</sub>] was noted as the IL that supported the best performance in the oxidation of ABTS in buffer. This in an interesting example of the use of ionic liquids in the creation of immobilized enzymes, in this case the abilities of ILs to stabilize the protein and solubilize the polymer were exploited. A solid forming event did occur in the presence of ionic liquid and enzyme, but it is unclear whether it represents a true entrapment of the enzyme. Khodagholy *et al.*, reported the entrapment of lactate oxidase (LOx) (for lactate sensing) in a polymer ionogel.<sup>247</sup> The ionogel solution was made by mixing the ionic liquid 1-ethyl-3-methylimidazolium ethylsulfate ionic liquid, [EMIM][EtSO<sub>4</sub>], with monomer 2, cross-linker 7 (Fig. 7B), the metal complex [bis(*n*-5-cyclopentadienyl)iron] and photoinitiator dimethoxy-phenylacetophenone (DMPA). The resultant mixture was sonicated at 45 °C for 10 min to make a homogeneous solution. The enzyme in buffer was added to the ionogel solution, and a small amount of the enzyme-ionogel solution poured onto a dimethylsiloxane (PDMS) modified well of the sensor device. Photo-irradiation using UV-light at 365 nm with an intensity of approximately 330mW cm<sup>-2</sup> for 1 min resulted in an enzyme ionogel. The device was able to detect lactate at the 10–100 mM concentration range.

The addition of ionic liquids to the sol-gel entrapment of enzymes has been shown to afford significant advantages compared to the entrapment in silica alone. The same protein stabilization is expected in the entrapment of enzymes in polymer ionogels, but the effects have been less explored. In this area the right balance must be struck between sufficient porosity to maximize substrate and product mass transfer, and



good mechanical stability to promote ease of handling and minimize leaching.

**5.3.3 Supramolecular and biomolecular methods employing ionic liquids.** Soft gels of water, organic solvents, and oils that form *via* self-assembly are well established. Ionic liquid soft gels have emerged relatively recently. Molecules that have been shown to gel ionic liquids are frequently derived from biomolecules. The structures of some LMWGs that gel ILs are given in Fig. 16.

The best LMWGs are able to gel a wide range of ILs.<sup>151</sup> Polymer poly(methyl methacrylate) (PMMA) coating of a LMW gel of 50 gel has been used to increase the mechanical strength.<sup>258</sup>

Supramolecular methods for co-entrapping enzymes and ionic liquids are comparatively rare, but the method shows considerable promise. An aqueous solution of Lipase B from *Candida Antarctica* and lipase from *Chromobacterium viscosum* in buffer was immobilized as a microemulsion with [BMIM][PF<sub>6</sub>] in a hydroxypropyl-methyl cellulose (HPMC) organogel.<sup>248</sup> Immobilized lipase from *Chromobacterium viscosum* exhibited a >4 times higher activity than the enzyme operated

in water emulsion for the esterification of lauric acid with 1-butanol in isooctane at 30 °C. The immobilized lipase retained 60% of its initial activity when stored in isooctane at 50 °C for 5 days, under the same storage conditions the free enzymes retained only 5% activity.

Even though a large number LWMGs have now been developed for ionic liquids, enzyme immobilization in LMW ionic liquid gels is largely unexplored, and this area is expected to expand significantly in the next few years. Key to the success of these materials will be the straightforward creation of robust materials with good mechanical stability and low leaching. This will require careful tuning of the supramolecular interactions, and the wide range of gelators and ILs available will be a significant advantage.

## 6. Conclusions and future directions

The use of isolated enzymes for the synthesis of chemicals is on the rapid increase. Isolated enzymes are relatively fragile,

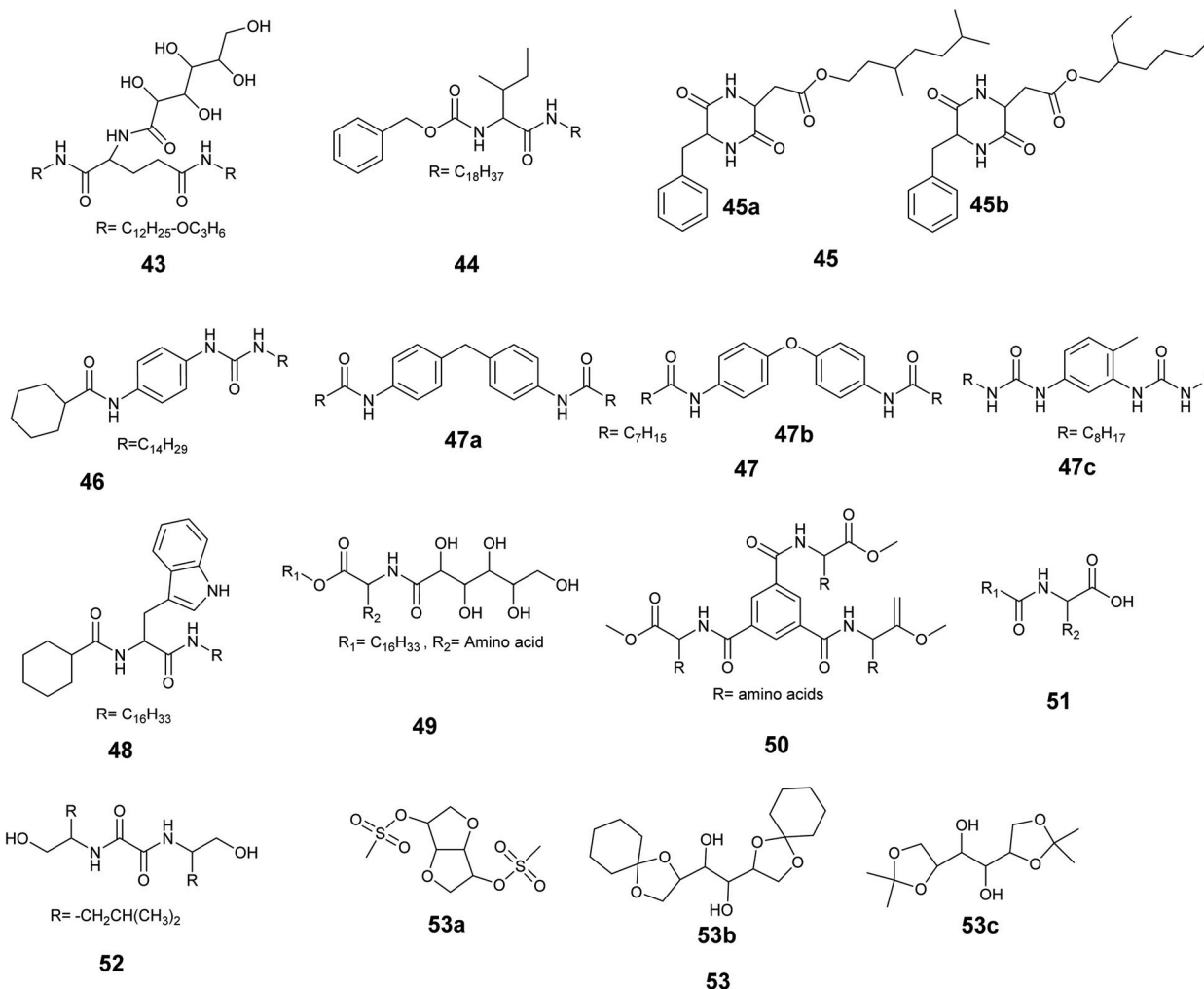


Fig. 16 Chemical structure of some LMW ionic liquid gelators. 43,<sup>249</sup> 44,<sup>250,251</sup> 45,<sup>252</sup> 46,<sup>253</sup> 47,<sup>254</sup> 48,<sup>255</sup> 49,<sup>256</sup> 50,<sup>257</sup> 51,<sup>258</sup> 52,<sup>259</sup> 53.<sup>151</sup>



and in order to improve separation and ensure recycling enzyme immobilization should be encouraged. To be fit for purpose methods must complement the advances in biotechnology and be readily adapted in response to changes in the protein and/or bioprocess conditions.

When adopting an immobilization method, a company must consider cost, reproducibility, and chemical regulations. As a result, long and complex methods of immobilization will not be adopted by biocatalysis producers nor end users. Simplicity and reliability are key to success. Such simplicity also lends itself to a better life cycle analysis (LCA) and represents greener chemistry.

The entrapment of an isolated enzyme in a support material has the potential to deliver adaptability, simplicity and reliability. Entrapment can be as simple as carrying out a polymerization in the presence of an enzyme or adding a low molecular weight gelator to an enzyme solution with heating and cooling. Entrapment does not depend on any direct interactions with the enzyme to achieve immobilization. The environment within the matrix can be changed to support enzyme activity, and changes in the protein within an enzyme library are unlikely to render an entrapment method obsolete.

As befits a successful immobilization strategy, and as demonstrated by the best chemical methods, entrapped enzymes have frequently demonstrated good enzyme activity, with enhanced thermal and pH stability, and there are examples in which the activity within the matrix is better than the activity of the free enzyme. Enzyme entrapment can be considered under-utilized in industry, and this can be attributed to doubts over simplicity and reliability. Moving forward researchers must consider diffusion, leaching and recycling as primary design criteria. Academia must work closely with industry to address the concerns of end users, and entrapment methods must be demonstrated under industrial conditions. Such collaboration will lead to greater adoption of enzyme entrapment for chemical manufacture and subsequent improvements in enzyme catalyzed bioprocesses.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

Professor Thomas Moody and Dr Stefan Mix of Almac Sciences and Dr Sebastian Cosgrove of Keele University, UK. This work is supported by Engineering and Physical Sciences Research Council (UK) grants EP/R026645/1, The UK Catalysis Hub 'Science': 2 Catalysis at the Water-Energy Nexus, and EP/M013219/1, Biocatalysis & Biotransformation: A 5th Theme for the National Catalysis Hub.

## References

- 1 P. Anastas and N. Eghbali, *Chem. Soc. Rev.*, 2010, **39**, 301–312.
- 2 R. A. Sheldon, *Chem. Commun.*, 2008, 3352–3365.
- 3 P. T. Anastas, L. G. Heine and T. C. Williamson, *Green Chemical Syntheses and Processes, ACS Symposium Series 767*; American Chemical Society: Washington, DC, 2000, pp. 1–6.
- 4 R. A. Sheldon and J. P. M. Sanders, *Catal. Today*, 2015, **239**, 3–6.
- 5 P. K. J. Kinnunen, *Cell. Physiol. Biochem.*, 2000, **10**, 243–250.
- 6 S. Martínez Cuesta, S. A. Rahman, N. Furnham and J. M. Thornton, *Biophys. J.*, 2015, **109**, 1082–1086.
- 7 J. Boonstra and A. J. Verkleij, *Adv. Enzyme Regul.*, 2004, **44**, 61–73.
- 8 R. T. Schimke and D. Doyle, *Annu. Rev. Biochem.*, 1970, **39**, 929–976.
- 9 D. E. Atkinson, *Annu. Rev. Microbiol.*, 1969, **23**, 47–68.
- 10 E. Romero, B. S. Jones, B. N. Hogg, A. Rué Casamajo, M. A. Hayes, S. L. Flitsch, N. J. Turner and C. Schnepel, *Angew. Chem., Int. Ed.*, 2021, 2–34.
- 11 S. Wu, R. Snajdrova, J. C. Moore, K. Baldenius and U. T. Bornscheuer, *Angew. Chem.*, 2021, **60**, 88–119.
- 12 B. Hauer, *ACS Catal.*, 2020, **10**, 8418–8427.
- 13 R. A. Sheldon and D. Brady, *Chem. Commun.*, 2018, **54**, 6088–6104.
- 14 U. T. Bornscheuer, G. W. Huisman, R. J. Kazlauskas, S. Lutz, J. C. Moore and K. Robins, *Nature*, 2012, **485**, 185–194.
- 15 S. Wu, R. Snajdrova, J. C. Moore, K. Baldenius and U. T. Bornscheuer, *Angew. Chem.*, 2021, **60**, 88–119.
- 16 J. M. Woodley, *Curr. Opin. Green Sustain. Chem.*, 2020, **21**, 22–26.
- 17 R. A. Sheldon, *Curr. Opin. Green Sustain. Chem.*, 2019, **18**, 13–19.
- 18 R. A. Sheldon and J. M. Woodley, *Chem. Rev.*, 2018, **118**, 801–838.
- 19 J. M. Choi, S. S. Han and H. S. Kim, *Biotechnol. Adv.*, 2015, **33**, 1443–1454.
- 20 V. G. Yadav, M. De Mey, C. G. Lim, P. K. Ajikumar and G. Stephanopoulos, *Metab. Eng.*, 2012, **14**, 233–241.
- 21 T. Tanaka and A. Kondo, *Biotechnol. Adv.*, 2015, **33**, 1403–1411.
- 22 T. Hudlicky and J. W. Reed, *Chem. Soc. Rev.*, 2009, **38**, 3117–3132.
- 23 B. R. Facin, M. S. Melchioris, A. Valério, J. V. Oliveira and D. De Oliveira, *Ind. Eng. Chem. Res.*, 2019, **58**, 5358–5378.
- 24 S. Naik, A. Basu, R. Saikia, B. Madan, P. Paul, R. Chatterjee, J. Brask and A. Svendsen, *J. Mol. Catal. B: Enzym.*, 2010, **65**, 18–23.
- 25 A. C. Carvalho, T. de S. Fonseca, M. C. de Mattos, M. da C. de Oliveira, T. L. de Lemos, F. Molinari, D. Romano and I. Serra, *Int. J. Mol. Sci.*, 2015, **16**, 29682–29716.
- 26 N. Sarmah, D. Revathi, G. Sheelu, K. Yamuna Rani, S. Sridhar, V. Mehtab and C. Sumana, *Biotechnol. Prog.*, 2018, **34**, 5–28.



- 27 G. M. Borrelli and D. Trono, *Int. J. Mol. Sci.*, 2015, **16**, 20774–20840.
- 28 F. J. Contesini, M. G. Davanço, G. P. Borin, K. G. Vanegas, J. P. G. Cirino, R. R. de Melo, U. H. Mortensen, K. Hildén, D. R. Campos and P. de O. Carvalho, *Catalysts*, 2020, **10**, 1–33.
- 29 K. Chen and F. H. Arnold, *Nat. Catal.*, 2020, **3**, 203–213.
- 30 B. A. Sandoval and T. K. Hyster, *Curr. Opin. Chem. Biol.*, 2020, **55**, 45–51.
- 31 R. A. Sheldon and D. Brady, *ChemSusChem*, 2019, **12**, 2859–2881.
- 32 J. M. Woodley, *Curr. Opin. Chem. Biol.*, 2013, **17**, 310–316.
- 33 H. Kries, R. Blomberg and D. Hilvert, *Curr. Opin. Chem. Biol.*, 2013, **17**, 221–228.
- 34 N. J. Turner and M. D. Truppo, *Curr. Opin. Chem. Biol.*, 2013, **17**, 212–214.
- 35 A. A. M. Elgharbawy, M. Moniruzzaman and M. Goto, *Biochem. Eng. J.*, 2020, **154**, 107426.
- 36 M. Pätzold, S. Siebenhaller, S. Kara, A. Liese, C. Syldatk and D. Holtmann, *Trends Biotechnol.*, 2019, **37**, 943–959.
- 37 T. Itoh, *Chem. Rev.*, 2017, **117**, 10567–10607.
- 38 P. Lozano, E. Alvarez, J. M. Bernal, S. Nieto, C. Gomez and G. Sanchez-Gomez, *Curr. Green Chem.*, 2017, **4**, 116–129.
- 39 M. Romero-Fernández and F. Paradisi, *Curr. Opin. Chem. Biol.*, 2020, **55**, 1–8.
- 40 R. C. Alnoch, L. A. Dos Santos, J. M. de Almeida, N. Krieger and C. Mateo, *Catalysts*, 2020, **10**, 1–29.
- 41 J. Liang and K. Liang, *Adv. Funct. Mater.*, 2020, **30**, 1–24.
- 42 J. Liu, R. T. Ma and Y. P. Shi, *Anal. Chim. Acta*, 2020, **1101**, 9–22.
- 43 D. G. Filho, A. G. Silva and C. Z. Guidini, *Appl. Microbiol. Biotechnol.*, 2019, **103**, 7399–7423.
- 44 B. Thangaraj and P. R. Solomon, *ChemBioEng Rev.*, 2019, **6**, 157–166.
- 45 G. Cottone, S. Giu, S. Bettati, S. Bruno, B. Campanini, M. Marchetti, S. Abbruzzetti, C. Viappiani, A. Cupane, A. Mozzarelli and L. Ronda, *Catalysts*, 2019, **9**, 1–29.
- 46 M. Bilal and H. M. N. Iqbal, *Int. J. Biol. Macromol.*, 2019, **130**, 462–482.
- 47 E. P. Cipolatti, A. Valério, R. O. Henriques, D. E. Moritz, J. L. Ninow, D. M. G. Freire, E. A. Manoel, R. Fernandez-Lafuente and D. De Oliveira, *RSC Adv.*, 2016, **6**, 104675–104692.
- 48 R. V. Ulijn, *J. Mater. Chem.*, 2006, **16**, 2217–2225.
- 49 D. Avnir, O. Lev and J. Livage, *J. Mater. Chem.*, 2006, **16**, 1013–1030.
- 50 D. P. Gavin, F. J. Reen, J. Rocha-Martin, I. Abreu-Castilla, D. F. Woods, A. M. Foley, P. A. Sánchez-Murcia, M. Schwarz, P. O'Neill, A. R. Maguire and F. O'Gara, *Sci. Rep.*, 2019, **9**, 1–15.
- 51 M. Ferrer, F. Martínez-Abarca and P. N. Golyshin, *Curr. Opin. Biotechnol.*, 2005, **16**, 588–593.
- 52 J. C. Moore, A. Rodriguez-Granillo, A. Crespo, S. Govindarajan, M. Welch, K. Hiraga, K. Lexa, N. Marshall and M. D. Truppo, *ACS Synth. Biol.*, 2018, **7**, 1730–1741.
- 53 O. F. Brandenburg, R. Fasan and F. H. Arnold, *Curr. Opin. Biotechnol.*, 2017, **47**, 102–111.
- 54 M. Schober, C. MacDermaid, A. A. Ollis, S. Chang, D. Khan, J. Hosford, J. Latham, L. A. F. Ihnken, M. J. B. Brown, D. Fuerst, M. J. Sanganee and G. D. Roiban, *Nat. Catal.*, 2019, **2**, 909–915.
- 55 W. Finnigan, L. J. Hepworth, S. L. Flitsch and N. J. Turner, *Nat. Catal.*, 2021, **4**, 98–104.
- 56 D. Rother and S. Malzacher, *Nat. Catal.*, 2021, **4**, 92–93.
- 57 J. Planas-Iglesias, S. M. Marques, G. P. Pinto, M. Musil, J. Stourac, J. Damborsky and D. Bednar, *Biotechnol. Adv.*, 2021, **47**, 107696–107718.
- 58 H. A. Bunzel, J. L. R. Anderson and A. J. Mulholland, *Curr. Opin. Struct. Biol.*, 2021, **67**, 212–218.
- 59 M. Ali, H. M. Ishqi and Q. Husain, *Biotechnol. Bioeng.*, 2020, **117**, 1877–1894.
- 60 S. Basler, S. Studer, Y. Zou, T. Mori, Y. Ota, A. Camus, H. A. Bunzel, R. C. Helgeson, K. N. Houk, G. Jiménez-Osés and D. Hilvert, *Nat. Chem.*, 2021, **13**, 231–235.
- 61 M. Kaushik, P. Sinha, P. Jaiswal, S. Mahendru, K. Roy and S. Kukreti, *J. Mol. Recognit.*, 2016, **29**, 499–503.
- 62 A. Liese and L. Hilterhaus, *Chem. Soc. Rev.*, 2013, **42**, 6236–6249.
- 63 R. Di Cosimo, J. Mc Auliffe, A. J. Poulouse and G. Bohlmann, *Chem. Soc. Rev.*, 2013, **42**, 6437–6474.
- 64 C. Ottone, O. Romero, C. Aburto, A. Illanes and L. Wilson, *Compr. Rev. Food Sci. Food Saf.*, 2020, **19**, 595–621.
- 65 A. Basso and S. Serban, *Mol. Catal.*, 2019, **479**, 110607.
- 66 M. P. Thompson, I. Peñafiel, S. C. Cosgrove and N. J. Turner, *Org. Process Res. Dev.*, 2019, **23**, 9–18.
- 67 J. Luo, S. Song, H. Zhang, H. Zhang, J. Zhang and Y. Wan, *Eng. Life Sci.*, 2020, **20**, 441–450.
- 68 X. Wang, P. C. Lan and S. Ma, *ACS Cent. Sci.*, 2020, **6**, 1497–1506.
- 69 E. T. Hwang and S. Lee, *ACS Catal.*, 2019, **9**, 4402–4425.
- 70 A. C. Pierre, *Biocatal. Biotransform.*, 2004, **22**, 145–170.
- 71 T. Jesionowski, J. Zdarta and B. Krajewska, *Adsorption*, 2014, **20**, 801–821.
- 72 Y. Hu, L. Dai, D. Liu and W. Du, *Green Chem.*, 2018, **20**, 4500–4506.
- 73 L. S. Wong, F. Khan and J. Micklefield, *Chem. Rev.*, 2009, **109**, 4025–4053.
- 74 S. Smith, K. Goodge, M. Delaney, A. Struzyk, N. Tansey and M. Frey, *Nanomaterials*, 2020, **10**, 1–39.
- 75 J. S. Wetz, D. F. Kienle, D. K. Schwartz and J. L. Kaar, *ACS Catal.*, 2019, **9**, 4992–5001.
- 76 J. S. Wetz, D. F. Kienle, D. K. Schwartz and J. L. Kaar, *J. Am. Chem. Soc.*, 2020, **142**, 3463–3471.
- 77 O. Singh, P. Y. Lee, S. Matysiak and H. Bermudez, *Phys. Chem. Chem. Phys.*, 2020, **22**, 19779–19786.
- 78 T. Akkas, A. Zakharyuta, A. Taralp and C. W. Ow-Yang, *Enzyme Microb. Technol.*, 2020, **132**, 109390.
- 79 R. A. Sheldon, *Biochem. Soc. Trans.*, 2007, **35**, 1583–1587.
- 80 H. Yamaguchi, Y. Kiyota and M. Miyazaki, *Catalysts*, 2018, **8**, 4–6.
- 81 R. A. Sheldon, *Pharm. Process Chem.*, 2010, 159–181.



- 82 N. L. S. Clair and M. A. Navia, *J. Am. Chem. Soc.*, 1992, **114**, 7314–7316.
- 83 L. Cao, F. Van Rantwijk and R. A. Sheldon, *Org. Lett.*, 2000, **2**, 1361–1364.
- 84 S. Wang, D. Zheng, L. Yin and F. Wang, *Enzyme Microb. Technol.*, 2017, **107**, 22–31.
- 85 M. Q. Xu, S. S. Wang, L. N. Li, J. Gao and Y. W. Zhang, *Catalysts*, 2018, **8**, 1–20.
- 86 R. A. Sheldon, *Catalysts*, 2019, **9**, 1–31.
- 87 R. A. Sheldon, A. Basso and D. Brady, *Chem. Soc. Rev.*, 2021, **50**, 5850–5862.
- 88 S. van Pelt, S. Quignard, D. Kubáč, D. Y. Sorokin, F. van Rantwijk and R. A. Sheldon, *Green Chem.*, 2008, **10**, 395–340.
- 89 P. Tielmann, H. Kierkels, A. Zonta, A. Ilie and M. T. Reetz, *Nanoscale*, 2014, **6**, 6220–6228.
- 90 A. C. Marr and P. C. Marr, *Dalton Trans.*, 2011, **40**, 20–26.
- 91 P. C. Marr and A. C. Marr, *Green Chem.*, 2016, **18**, 105–128.
- 92 S. Braun, S. Rappoport, R. Zusman, D. Avnir and M. Ottolenghi, *Mater. Lett.*, 1990, **10**, 2843–2846.
- 93 D. Avnir, S. Braun, O. Lev and M. Ottolenghi, *Chem. Mater.*, 1994, **6**, 1–5.
- 94 D. Avnir, S. Braun, O. Lev and M. Ottolenghi, *Chem. Mater.*, 1994, **6**, 1605–1614.
- 95 Y. Tatsu, K. Yamashita, M. Yamaguchi, S. Yamamura, H. Yamamoto and S. Yoshikawa, *Chem. Lett.*, 1992, 1615–1618.
- 96 S. A. Yamanaka, L. M. Ellerbv, C. R. Nishida, J. I. Zink, F. Nishida, B. Dunn, S. J. Valentine and J. I. Zink, *Chem. Mater.*, 1992, **4**, 495–497.
- 97 S. Braun, S. Shtelzer, S. Rappoport, D. Avnir and M. Ottolenghi, *J. Non-Cryst. Solids*, 1992, **147–148**, 739–743.
- 98 S. Shtelzer, S. Rappoport, D. Avnir, M. Ottolenghi and S. Braun, *Biotechnol. Appl. Biochem.*, 1992, **15**, 227–235.
- 99 Y. Kurokawa, H. Ohta, M. Okubo and M. Takahashi, *Carbohydr. Polym.*, 1994, **23**, 1–4.
- 100 E. Busto, V. Gotor-Fernández and V. Gotor, *Chem. Soc. Rev.*, 2010, **39**, 4504–4523.
- 101 M. T. Reetz, *Curr. Opin. Chem. Biol.*, 2002, **6**, 145–150.
- 102 F. Hollmann, I. W. C. E. Arends, K. Buehler, A. Schallmey and B. Bühler, *Green Chem.*, 2011, **13**, 226–265.
- 103 D. Romano, R. Villa and F. Molinari, *ChemCatChem*, 2012, **4**, 739–749.
- 104 M. T. Reetz, A. Zonta and J. Simpelkamp, *Angew. Chem., Int. Ed. Engl.*, 1995, **34**, 301–303.
- 105 M. T. Reetz, A. Zonta and J. Simpelkamp, *Biotechnol. Bioeng.*, 1996, **49**, 527–534.
- 106 M. T. Reetz, P. Tielmann, W. Wiesenhöfer, W. Könen and A. Zonta, *Adv. Synth. Catal.*, 2003, **345**, 717–728.
- 107 M. T. Reetz, R. Wenkel and D. Avnir, *Synthesis*, 2000, 781–783.
- 108 M. T. Reetz, *Adv. Mater.*, 1997, **9**, 943–954.
- 109 M. T. Reetz, A. Zonta, V. Vijayakrishnan and K. Schimossek, *J. Mol. Catal. A: Chem.*, 1998, **134**, 251–258.
- 110 M. T. Reetz, A. Zonta, J. Simpelkamp and W. Konen, *Chem. Commun.*, 1996, 1397–1398.
- 111 H. Frenkel-Mullerad and D. Avnir, *J. Am. Chem. Soc.*, 2005, **127**, 8077–8081.
- 112 N. A. Mohidem and H. Bin Mat, *J. Sol-Gel Sci. Technol.*, 2012, **61**, 96–103.
- 113 M. Päiviö and L. T. Kanerva, *Process Biochem.*, 2013, **48**, 1488–1494.
- 114 S. Escobar, C. Bernal, J. M. Bolivar, B. Nidetzky, F. López-Gallego and M. Mesa, *Mol. Catal.*, 2018, **449**, 106–113.
- 115 Y. Kawachi, S. I. Kugimiya, H. Nakamura and K. Kato, *Appl. Surf. Sci.*, 2014, **314**, 64–70.
- 116 H. Z. Ma, X. W. Yu, C. Song, Q. L. Xue and B. Jiang, *J. Mol. Catal. B: Enzym.*, 2016, **127**, 76–81.
- 117 C. Muderrisoglu, S. Sargin and O. Yesil-Celiktas, *Biotechnol. Lett.*, 2018, **40**, 773–780.
- 118 Z. Liu, B. Liu, M. Zhang, J. Kong and J. Deng, *Anal. Chim. Acta*, 1999, **392**, 135–141.
- 119 Z. Liu, B. Liu, J. Kong and J. Deng, *Anal. Chem.*, 2000, **72**, 4707–4712.
- 120 Y. Zhu, Z. Jiang, L. Zhang, J. Shi and D. Yang, *Ind. Eng. Chem. Res.*, 2012, **51**, 255–261.
- 121 A. Rutenberg, V. V. Vinogradov and D. Avnir, *Chem. Commun.*, 2013, **49**, 5636–5638.
- 122 V. V. Vinogradov and D. Avnir, *RSC Adv.*, 2015, **5**, 10862–10868.
- 123 V. V. Vinogradov, A. V. Vinogradov, V. E. Sobolev, I. P. Dudanov and V. V. Vinogradov, *J. Sol-Gel Sci. Technol.*, 2015, **73**, 501–505.
- 124 V. V. Vinogradov and D. Avnir, *J. Mater. Chem. B*, 2014, **2**, 2868–2873.
- 125 V. V. Vinogradov and D. Avnir, *Sci. Rep.*, 2015, **5**, 1–7.
- 126 O. E. Shapovalova, D. Levy, D. Avnir and V. V. Vinogradov, *Colloids Surf., B*, 2016, **146**, 731–736.
- 127 Y. V. Solovev, A. Y. Prilepskii, E. F. Krivoshapkina, A. F. Fakhardo, E. A. Bryushkova, P. A. Kalikina, E. I. Koshel and V. V. Vinogradov, *Sci. Rep.*, 2019, **9**, 1–14.
- 128 K. F. O'Driscoll, *Methods Enzymol.*, 1976, **44**, 169–183.
- 129 M. Nöth, E. Gau, F. Jung, M. D. Davari, I. El-Awaad, A. Pich and U. Schwaneberg, *Green Chem.*, 2020, **22**, 8183–8209.
- 130 P. Bernfeld and J. Wan, *Science*, 1963, **142**, 678–679.
- 131 G. Demirel, G. Özçetin, F. Şahin, H. Tümtürk, S. Aksoy and N. Hasirci, *React. Funct. Polym.*, 2006, **66**, 389–394.
- 132 O. Yamak, N. A. Kalkan, S. Aksoy, H. Altinok and N. Hasirci, *Process Biochem.*, 2009, **44**, 440–445.
- 133 S. Demirci, M. Sahiner, S. Yilmaz, E. Karadag and N. Sahiner, *Biotechnol. Rep.*, 2020, **28**, e00534.
- 134 S. Demirci and N. Sahiner, *Chem. Eng. J.*, 2021, **409**, 128233.
- 135 S. Bao, D. Wu, T. Su, Q. Wu and Q. Wang, *RSC Adv.*, 2015, **5**, 44342–44345.
- 136 V. Krasňan, R. Stloukal, M. Rosenberg and M. Rebroš, *Appl. Microbiol. Biotechnol.*, 2016, **100**, 2535–2553.
- 137 M. Rebroš, A. Pilniková, D. Šimčíková, L. Weignerová, R. Stloukal, V. Křen and M. Rosenberg, *Biocatal. Biotransform.*, 2013, **31**, 329–334.



- 138 M. Rebroš, M. Rosenberg, Z. Mlichová and L. Křištofiková, *Food Chem.*, 2007, **102**, 784–787.
- 139 M. Rebroš, M. Rosenberg, Z. Mlichová, L. Křištofiková and M. Paluch, *Enzyme Microb. Technol.*, 2006, **39**, 800–804.
- 140 S. Kaushik, P. D. Thungon and P. Goswami, *ACS Biomater. Sci. Eng.*, 2020, **6**, 4337–4355.
- 141 S. Lv, *Molecules*, 2020, **25**, 4929–4954.
- 142 C. S. Bezerra, C. M. G. De Farias Lemos, M. De Sousa and L. R. B. Gonçalves, *J. Appl. Polym. Sci.*, 2015, **132**, 1–15.
- 143 L. M. O. Arruda and M. Vitolo, *Appl. Biochem. Biotechnol., Part A*, 1999, **81**, 23–33.
- 144 E. Quiroga, C. O. Illanes, N. A. Ochoa and S. Barberis, *Process Biochem.*, 2011, **46**, 1029–1034.
- 145 S. Miyairi, M. Sugiura and S. Fukui, *Agric. Biol. Chem.*, 1978, **42**, 1661–1667.
- 146 M. Demura, T. Asakura and T. Kuroo, *Biosensors*, 1989, **4**, 361–372.
- 147 J. Qian, Y. Liu, H. Liu, T. Yu and J. Deng, *Biosens. Bioelectron.*, 1997, **12**, 1213–1218.
- 148 N. Guziewicz, A. Best, B. Perez-Ramirez and D. L. Kaplan, *Biomaterials*, 2011, **32**, 2642–2650.
- 149 Y. Han, S. Yu, L. Liu, S. Zhao, T. Yang, Y. Yang, Y. Fang and S. Lv, *Mol. Catal.*, 2018, **457**, 24–32.
- 150 E. R. Draper and D. J. Adams, *Chem*, 2017, **3**, 390–410.
- 151 P. McNeice, Y. Zhao, J. Wang, G. F. Donnelly and P. C. Marr, *Green Chem.*, 2017, **19**, 4690–4697.
- 152 Q. Wang, Z. Yang, L. Wang, M. Ma and B. Xu, *Chem. Commun.*, 2007, 1032–1034.
- 153 G. Scott, S. Roy, Y. M. Abul-Haija, S. Fleming, S. Bai and R. V. Ulijn, *Langmuir*, 2013, **29**, 14321–14327.
- 154 D. Mandal, P. Choudhury, D. Sarkar and P. K. Das, *Chem. Commun.*, 2017, **53**, 7844–7847.
- 155 R. Jain, V. K. Pal and S. Roy, *Biomacromolecules*, 2020, **21**, 4180–4193.
- 156 S. Huang, X. Kou, J. Shen, G. Chen and G. Ouyang, *Angew. Chem., Int. Ed.*, 2020, **59**, 8786–8798.
- 157 J. Mehta, N. Bhardwaj, S. K. Bhardwaj, K. H. Kim and A. Deep, *Coord. Chem. Rev.*, 2016, **322**, 30–40.
- 158 S. S. Nadar, L. Vaidya and V. K. Rathod, *Int. J. Biol. Macromol.*, 2020, **149**, 861–876.
- 159 E. Gkaniatsou, C. Sicard, R. Ricoux, J. P. Mahy, N. Steunou and C. Serre, *Mater. Horiz.*, 2017, **4**, 55–63.
- 160 F. Lyu, Y. Zhang, R. N. Zare, J. Ge and Z. Liu, *Nano Lett.*, 2014, **14**, 5761–5765.
- 161 F. K. Shieh, S. C. Wang, C. I. Yen, C. C. Wu, S. Dutta, L. Y. Chou, J. V. Morabito, P. Hu, M. H. Hsu, K. C. W. Wu and C. K. Tsung, *J. Am. Chem. Soc.*, 2015, **137**, 4276–4279.
- 162 K. Liang, R. Ricco, C. M. Doherty, M. J. Styles, S. Bell, N. Kirby, S. Mudie, D. Haylock, A. J. Hill, C. J. Doonan and P. Falcaro, *Nat. Commun.*, 2015, **6**, 4–11.
- 163 X. Wu, J. Ge, C. Yang, M. Hou and Z. Liu, *Chem. Commun.*, 2015, **51**, 13408–13411.
- 164 G. Chen, X. Kou, S. Huang, L. Tong, Y. Shen, W. Zhu, F. Zhu and G. Ouyang, *Angew. Chem.*, 2020, **132**, 2889–2896.
- 165 H. He, H. Han, H. Shi, Y. Tian, F. Sun, Y. Song, Q. Li and G. Zhu, *ACS Appl. Mater. Interfaces*, 2016, **8**, 24517–24524.
- 166 S. S. Nadar and V. K. Rathod, *Enzyme Microb. Technol.*, 2018, **108**, 11–20.
- 167 W. H. Chen, M. Vázquez-González, A. Zoabi, R. Abu-Reziq and I. Willner, *Nat. Catal.*, 2018, **1**, 689–695.
- 168 D. D. Díaz, D. Kühbeck and R. J. Koopmans, *Chem. Soc. Rev.*, 2011, **40**, 427–448.
- 169 J. Hu, G. Zhang and S. Liu, *Chem. Soc. Rev.*, 2012, **41**, 5933–5949.
- 170 R. J. Williams, R. J. Mart and R. V. Ulijn, *Biopolymers*, 2010, **94**, 107–117.
- 171 Q. Wang, Z. Yang, Y. Gao, W. Ge, L. Wang and B. Xu, *Soft Matter*, 2008, **4**, 550–553.
- 172 T. Su, D. Zhang, Z. Tang, Q. Wu and Q. Wang, *Chem. Commun.*, 2013, **49**, 8033–8035.
- 173 Q. Wei, M. Xu, C. Liao, Q. Wu, M. Liu, Y. Zhang, C. Wu, L. Cheng and Q. Wang, *Chem. Sci.*, 2016, **7**, 2748–2752.
- 174 Q. Wei, W. Xu, M. Liu, Q. Wu, L. Cheng and Q. Wang, *J. Mater. Chem. B*, 2016, **4**, 6302–6306.
- 175 A. R. Hirst, S. Roy, M. Arora, A. K. Das, N. Hodson, P. Murray, S. Marshall, N. Javid, J. Sefcik, J. Boekhoven, J. H. Van Esch, S. Santabarbara, N. T. Hunt and R. V. Ulijn, *Nat. Chem.*, 2010, **2**, 1089–1094.
- 176 R. A. Pires, Y. M. Abul-Haija, D. S. Costa, R. Novoa-Carballal, R. L. Reis, R. V. Ulijn and I. Pashkuleva, *J. Am. Chem. Soc.*, 2015, **137**, 576–579.
- 177 L. Wang, F. Wang, B. Xu, M. Zhou, Y. Yu, P. Wang and Q. Wang, *Langmuir*, 2021, **37**, 478–489.
- 178 V. Sans, *Curr. Opin. Green Sustain. Chem.*, 2020, **25**, 100367.
- 179 L. Wenger, C. P. Radtke, J. Göpper, M. Wörner and J. Hubbuch, *Front. Bioeng. Biotechnol.*, 2020, **8**, 1–17.
- 180 J. Liu, X. Shen, Z. Zheng, M. Li, X. Zhu, H. Cao and C. Cui, *Int. J. Biol. Macromol.*, 2020, **164**, 518–525.
- 181 P. R. A. Chivers, J. A. Kelly, M. J. S. Hill and D. K. Smith, *React. Chem. Eng.*, 2020, **5**, 1112–1117.
- 182 R. Huang, M. Wu, M. J. Goldman and Z. Li, *Biotechnol. Bioeng.*, 2015, **112**, 1092–1101.
- 183 Q. Ai, D. Yang, Y. Zhu and Z. Jiang, *Ind. Eng. Chem. Res.*, 2013, **52**, 14898–14905.
- 184 A. S. Drozdov, O. E. Shapovalova, V. Ivanovski, D. Avnir and V. V. Vinogradov, *Chem. Mater.*, 2016, **28**, 2248–2253.
- 185 J. Huo, J. Aguilera-Sigalat, S. El-Hankari and D. Bradshaw, *Chem. Sci.*, 2015, **6**, 1938–1943.
- 186 H. Zhang, M. Lu, H. Jiang, Z. Y. Wu, D. D. Zhou, D. Q. Li and F. Q. Yang, *Colloids Surf., B*, 2020, **188**, 110800.
- 187 Z. Lei, B. Chen, Y. M. Koo and D. R. Macfarlane, *Chem. Rev.*, 2017, **117**, 6633–6635.
- 188 T. Welton, *Biophys. Rev.*, 2018, **10**, 691–706.
- 189 R. A. Sheldon, *RSC Catal. Ser.*, 2014, **2014-Janua**, 20–43.
- 190 R. A. Sheldon, R. M. Lau, M. J. Sorgedragger, F. van Rantwijk and K. R. Seddon, *Green Chem.*, 2002, **4**, 147–151.
- 191 A. Kumar, M. Bisht and P. Venkatesu, *Int. J. Biol. Macromol.*, 2017, **96**, 611–651.
- 192 L. E. Meyer, J. von Langermann and U. Kragl, *Biophys. Rev.*, 2018, **10**, 901–910.





- 193 A. Schindl, M. L. Hagen, S. Muzammal, H. A. D. Gunasekera and A. K. Croft, *Front. Chem.*, 2019, **7**, 1–31.
- 194 H. Zhao, *Biotechnol. Adv.*, 2020, **45**, 107638.
- 195 A. A. M. Elgharabawy, M. Moniruzzaman and M. Goto, *Curr. Opin. Green Sustain. Chem.*, 2021, **27**, 100406.
- 196 C. Rizzo, A. Mandoli, S. Marullo and F. D'Anna, *J. Org. Chem.*, 2019, **84**, 6356–6365.
- 197 P. McNeice, A. Reid, H. T. Imam, C. McDonagh, J. D. Walby, T. J. Collins, A. C. Marr and P. C. Marr, *Environ. Sci. Technol.*, 2020, **54**, 14026–14035.
- 198 A. P. S. Brogan, C. J. Clarke, A. Charalambidou, C. N. Loynachan, S. E. Norman, J. Douth and J. P. Hallett, *Mater. Horiz.*, 2020, **7**, 820–826.
- 199 R. M. Lau, M. J. Sorgedragger, G. Carrea, F. Van Rantwijk, F. Secundo and R. A. Sheldon, *Green Chem.*, 2004, **6**, 483–487.
- 200 M. Bihari, T. P. Russell and D. A. Hoagland, *Biomacromolecules*, 2010, **11**, 2944–2948.
- 201 S. Strassburg, H. Bermudez and D. Hoagland, *Biomacromolecules*, 2016, **17**, 2233–2239.
- 202 G. A. Baker and W. T. Heller, *Chem. Eng. J.*, 2009, **147**, 6–12.
- 203 J. A. Widegren, A. Laesecke and J. W. Magee, *Chem. Commun.*, 2005, 1610–1612.
- 204 K. Fujita and H. Ohno, *Biopolymers*, 2010, **93**, 1093–1099.
- 205 Y. Kohno and H. Ohno, *Chem. Commun.*, 2012, **48**, 7119–7130.
- 206 P. Lozano, T. de Diego, S. Gmouh, M. Vaultier and J. L. Iborra, *Biocatal. Biotransform.*, 2005, **23**, 169–176.
- 207 Y. Nikawa, S. Tsuzuki, H. Ohno and K. Fujita, *Aust. J. Chem.*, 2019, **72**, 392–399.
- 208 G. Chevrot, E. E. Fileti and V. V. Chaban, *J. Mol. Model.*, 2016, **22**, 258.
- 209 K. Fujita, M. Kajiyama, Y. Liu, N. Nakamura and H. Ohno, *Chem. Commun.*, 2016, **52**, 13491–13494.
- 210 K. Fujita, D. R. MacFarlane, M. Forsyth, M. Yoshizawa-Fujita, K. Murata, N. Nakamura and H. Ohno, *Biomacromolecules*, 2007, **8**, 2080–2086.
- 211 K. Fujita, R. Nakano, R. Nakaba, N. Nakamura and H. Ohno, *Chem. Commun.*, 2019, **55**, 3578–3581.
- 212 E. E. Carter, A. J. Heyert, M. De Souza, J. L. Baker and G. E. Lindberg, *Phys. Chem. Chem. Phys.*, 2019, **21**, 17950–17958.
- 213 L. Gontrani, *Biophys. Rev.*, 2018, **10**, 873–880.
- 214 T. L. Greaves and C. J. Drummond, *Chem. Rev.*, 2015, **115**, 11379–11448.
- 215 H. Ohno and K. Fukumoto, *Acc. Chem. Res.*, 2007, **40**, 1122–1129.
- 216 M. Petkovic, J. L. Ferguson, H. Q. N. Gunaratne, R. Ferreira, M. C. Leitão, K. R. Seddon, L. P. N. Rebelo and C. S. Pereira, *Green Chem.*, 2010, **12**, 643–664.
- 217 A. Yazdani, M. Sivapragasam, J. M. Leveque and M. Moniruzzaman, *J. Microb. Biochem. Technol.*, 2016, **8**, 5.
- 218 M. Bisht, I. Jha and P. Venkatesu, *ChemistrySelect*, 2016, **1**, 3510–3519.
- 219 Y. H. Bi, Z. Q. Duan, X. Q. Li, Z. Y. Wang and X. R. Zhao, *J. Agric. Food Chem.*, 2015, **63**, 1558–1561.
- 220 R. R. Mazid, R. Vijayaraghavan, D. R. MacFarlane, C. Cortez-Jugo and W. Cheng, *Chem. Commun.*, 2015, **51**, 8089–8092.
- 221 D. R. MacFarlane, R. Vijayaraghavan, H. N. Ha, A. Izgorodin, K. D. Weaver and G. D. Elliott, *Chem. Commun.*, 2010, **46**, 7703–7705.
- 222 R. Gusain, A. Khan and O. P. Khatrri, *J. Mol. Liq.*, 2020, **301**, 112322.
- 223 T. Gundolf, N. Weyhing-Zerrer, J. Sommer, R. Kalb, D. Schoder, P. Rossmannith and P. Mester, *ACS Sustainable Chem. Eng.*, 2019, **7**, 15865–15873.
- 224 P. Oulego, J. Faes, R. González, J. L. Viesca, D. Blanco and A. H. Battez, *J. Mol. Liq.*, 2019, **292**, 111451–111459.
- 225 A. Mezzetta, L. Guazzelli, M. Seggiani, C. S. Pomelli, M. Puccini and C. Chiappe, *Green Chem.*, 2017, **19**, 3103–3111.
- 226 A. M. M. Bessa, M. S. C. Venerando, F. X. Feitosa, L. M. Alexandre e Silva, F. A. N. Fernandes, R. S. de Santiago-Aguiar and H. B. de Sant'Ana, *J. Mol. Liq.*, 2020, **313**, 113586.
- 227 H. Yang, B. Jiang, Y. Sun, L. Hao, Z. Huang and L. Zhang, *Chem. Eng. J.*, 2016, **306**, 131–138.
- 228 A. P. S. Brogan and J. P. Hallett, *J. Am. Chem. Soc.*, 2016, **138**, 4494–4501.
- 229 T. De Diego, P. Lozano, S. Gmouh, M. Vaultier and J. L. Iborra, *Biomacromolecules*, 2005, **6**, 1457–1464.
- 230 J. K. Lee and M. Kim, *J. Org. Chem.*, 2002, **67**, 6845–6847.
- 231 T. Itoh, S. Han, Y. Matsushita and S. Hayase, *Green Chem.*, 2004, **6**, 437–439.
- 232 T. Itoh, Y. Matsushita, Y. Abe, S. H. Han, S. Wada, S. Hayase, M. Kawatsura, S. Takai, M. Morimoto and Y. Hirose, *Chem. – Eur. J.*, 2006, **12**, 9228–9237.
- 233 T. Nishihara, A. Shiomi, S. Kadotani, T. Nokami and T. Itoh, *Green Chem.*, 2017, **19**, 5250–5256.
- 234 P. Lozano, J. M. Bernal, G. Sánchez-Gómez, G. López-López and M. Vaultier, *Energy Environ. Sci.*, 2013, **6**, 1328–1338.
- 235 K. M. Bothwell and P. C. Marr, *ACS Sustainable Chem. Eng.*, 2017, **5**, 1260–1263.
- 236 Y. Liu, M. Wang, J. Li, Z. Li, P. He, H. Liu and J. Li, *Chem. Commun.*, 2005, 1778–1780.
- 237 Y. Liu, L. Shi, M. Wang, Z. Li, H. Liu and J. Li, *Green Chem.*, 2005, **7**, 655–658.
- 238 S. H. Lee, T. T. N. Doan, S. H. Ha and Y. M. Koo, *J. Mol. Catal. B: Enzym.*, 2007, **45**, 57–61.
- 239 C. Zarcula, L. Coríci, R. Croitoru, A. Ursoiu and F. Peter, *J. Mol. Catal. B: Enzym.*, 2010, **65**, 79–86.
- 240 H. Vila-Real, A. J. Alfaia, J. N. Rosa, P. M. P. Gois, M. E. Rosa, A. R. T. Calado and M. H. Ribeiro, *J. Biotechnol.*, 2011, **152**, 147–158.
- 241 S. Sarkar, K. Mantri, D. Kumar, S. K. Bhargava and S. K. Soni, *RSC Adv.*, 2015, **5**, 105800–105809.
- 242 S. K. Soni, R. Ramanathan, P. J. Coloe, V. Bansal and S. K. Bhargava, *Langmuir*, 2010, **26**, 16020–16024.



- 243 S. H. Lee, T. T. N. Doan, S. H. Ha, W. J. Chang and Y. M. Koo, *J. Mol. Catal. B: Enzym.*, 2007, **47**, 129–134.
- 244 R. L. Souza, E. L. P. Faria, R. T. Figueiredo, S. Mettedi, O. A. A. Santos, A. S. Lima and C. M. F. Soares, *J. Therm. Anal. Calorim.*, 2017, **128**, 833–840.
- 245 R. L. de Souza, E. L. P. de Faria, R. T. Figueiredo, L. dos S. Freitas, M. Iglesias, S. Mattedi, G. M. Zanin, O. A. A. dos Santos, J. A. P. Coutinho, Á. S. Lima and C. M. F. Soares, *Enzyme Microb. Technol.*, 2013, **52**, 141–150.
- 246 S. Haj Kacem, S. Galai, A. Pérez de los Ríos, F. J. Hernández Fernández and I. Smaali, *J. Chem. Technol. Biotechnol.*, 2018, **93**, 174–183.
- 247 D. Khodagholy, V. F. Curto, K. J. Fraser, M. Gurfinkel, R. Byrne, D. Diamond, G. G. Malliaras, F. Benito-Lopez and R. M. Owens, *J. Mater. Chem.*, 2012, **22**, 4440–4443.
- 248 I. V. Pavlidis, K. Tzafestas and H. Stamatis, *Biotechnol. J.*, 2010, **5**, 805–812.
- 249 N. Kimizuka and T. Nakashima, *Langmuir*, 2001, **17**, 6759–6761.
- 250 W. Kubo, T. Kitamura, K. Hanabusa, Y. Wada and S. Yanagida, *Chem. Commun.*, 2002, **4**, 374–375.
- 251 W. Kubo, S. Kambe, S. Nakade, T. Kitamura, K. Hanabusa, Y. Wada and S. Yanagida, *J. Phys. Chem. B*, 2003, **107**, 4374–4381.
- 252 K. Hanabusa, H. Fukui, M. Suzuki and H. Shirai, *Langmuir*, 2005, **21**, 10383–10390.
- 253 N. Mohmeyer, D. Kuang, P. Wang, H. W. Schmidt, S. M. Zakeeruddin and M. Grätzel, *J. Mater. Chem.*, 2006, **16**, 2978–2983.
- 254 L. Tan, X. Dong, H. Wang and Y. Yang, *Electrochem. Commun.*, 2009, **11**, 933–936.
- 255 S. Dutta, D. Das, A. Dasgupta and P. K. Das, *Chem. – Eur. J.*, 2010, **16**, 1493–1505.
- 256 N. Minakuchi, K. Hoe, D. Yamaki, S. Ten-No, K. Nakashima, M. Goto, M. Mizuhata and T. Maruyama, *Langmuir*, 2012, **28**, 9259–9266.
- 257 Y. Ishioka, N. Minakuchi, M. Mizuhata and T. Maruyama, *Soft Matter*, 2014, **10**, 965–971.
- 258 T. Kataoka, Y. Ishioka, M. Mizuhata, H. Minami and T. Maruyama, *ACS Appl. Mater. Interfaces*, 2015, **7**, 23346–23352.
- 259 W. K. Restu, Y. Nishida, T. Kataoka, M. Morimoto, K. Ishida, M. Mizuhata and T. Maruyama, *Colloid Polym. Sci.*, 2017, **295**, 1109–1116.
- 260 N. S. Rios, M. P. Pinheiro, M. L. B. Lima, D. M. G. Freire, I. J. da Silva, E. Rodríguez-Castellón, H. B. de Sant’Ana, A. C. Macedo and L. R. B. Gonçalves, *Chem. Eng. Res. Des.*, 2018, **129**, 12–24.

