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Mesolytic Cleavage of Homobenzylic Ethers for Programmable Endof-Life Function in Redoxmers

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Author contributions

H.Q., M.J.C., H.A.D., J.R.L., R.S.A., and J.S.M. conceived the research; H.Q. and N.S.P. performed synthesis and fragmentation studies; M.J.C., N.A.I., A.S.D., and W.S. performed electrochemistry studies; H.A.D performed computational studies; H.Q., M.J.C., and H.A.D. analyzed data and wrote the paper. J.R.L., R.S.A., and J.S.M. provided guidance during all stages of the project. All authors have given approval to the final version of the manuscript. [†]H.Q., M.J.C, and H.A.D. contributed equally to this work

This paper is dedicated in memoriam of Susan A. Odom.

Abstract: Irreparable chemical damage to redox-active monomers, oligomers, and polymers (i.e. *redoxmers*) limits the lifetime of energy storage devices (e.g. redox flow batteries) by causing electrode and membrane fouling, as well as irreversible capacity loss. To predictably restore device and materials performance, it is desirable to add programmed destruction capabilities into these damage-prone materials. Here, we report the use of triggerable retrograde reactions to achieve programmable end-of-life function in redoxmers. Retrograde reactions are intended to break up damaged redoxmer materials into more soluble small-molecule constituents to prevent irreparably fouling battery interfaces. We investigated the redox-triggered mesolytic cleavage of homobenzylic ethers (HBEs) for this purpose. Combining experimental methods with simulations, we probed the influence of ring substituents on the programmable bond-scission behavior of HBEs. Variation of para-substituents on the HBEs allowed us to modify the oxidation potential, degradation pathway, and electrochemical mechanisms of the generated products. Given its ideal oxidation potential, we selected the *para*-methoxy-based HBE as the cleavage scaffold and integrated it with dialkoxybenzene, TEMPO, viologen, and *para*-nitrobenzene redox centers for compatibility, bulk deconstruction, and electrode defouling tests. Upon applying a high oxidation potential, the redox-active pendant is cleaved from the backbone via HBE bonds; of the four redox centers tested, three of them remained fully redox active. Viologen-appended redox active polymers with HBE linkers were cleaved to fully separate the redox centers from the backbone. Polymer-filmed electrodes were partially restored following HBE oxidation defouling. These studies highlight the co-design of new materials functions for developing sustainable energy storage materials.

Introduction

Analogous to biological systems that have evolved to cope with the chemical demands of oxidative phosphorylation,^{1,2} artificial energy conversion (e.g. photovoltaics) and storage (e.g. batteries) systems also operate under extreme chemical stress. Thus, accumulated damage, including both physical and chemical, becomes unavoidable and is detrimental to longevity of energy capture and storage devices.^{3–5} To prevent and repair damage, numerous healing strategies based on additives, which are extrinsic to the active material, have been developed.⁶ For example, power conversion efficiency losses and long-term damage caused by the effects of humidity in lead halide perovskite photovoltaics are prevented through the addition of polyethylene glycol as a water adsorption layer.⁷ Similarly, in Li-ion batteries, the addition of crack-healing agents (e.g. lowmelting point metallic alloys,^{8,9} self-healing polymer binders,^{10,11} and new self-healing polymer electrolytes^{12–14} prevents capacity fade ascribed to the formation of micro-cracks upon cycling.

Irreparable chemical damage of battery components due to the demands of the electrochemical environment requires new mitigation strategies, as the above physical barrier and healing strategies are not relevant in all cases. Failure to remove degraded species may result in dysfunctional cell operation due to irreversible deposition of films on electrodes and membrane fouling. For instance, defects in the formation of solid electrolyte interphase layers at Li-ion battery anodes lead to capacity fade and power loss,⁴ and the precipitation of vanadium electrolytes in redox flow batteries (RFBs) causes blockages in the stacks and pumps that suppress the energy density and capacity of RFBs.⁵ For these systems it would be desirable to develop a strategy that relies on conditionally activating an intrinsic redox response that would help dealing with irreversible damage.



Scheme 1. Restoring Fouled Redox Flow Battery (RFB) Components with Programmable End-of-Life Function in Redoxmers (a) Fouling of RFB caused by consecutive processes of absorption, redox process, deactivation, and accumulation of redoxmers; (b) Application of HBEs with redoxmer architectures for programmable redoxmer deconstruction *via* mesolytic cleavage.

Redoxmers, alternative RFB electrolytes incorporating multiple copies of redox-active units into a single molecule, are of great interest for size-exclusion RFBs.¹⁵ These redoxmers are also known to produce insoluble species in extreme electrochemical environments. Damaged or overcharged redoxmers passivate the electrodes, foul separator membranes, and contaminate electrolyte solutions, thus lowering the energy storage efficiency, overall performance, and long-term operation (Scheme 1a).^{16,17} Early intervention *via* a restoration regime would halt the deterioration of power and storage capacities before system failure. We imagined the need to add new functionality that enables programmable deconstruction of redoxmers that reverts them back to their small-molecule constituents,¹⁸ which would be more soluble in electrolytes and limit pre-

cipitation of blocking films. Further down the line, this operation might enable the separation of the damaged components and perhaps even their re-assembly. Organic redoxmers are the ideal platform to incorporate the programmable end-of-life functionality because of their structural versatility and synthetic accessibility.

A complete redoxmer restoration requires, in its simplest form, detachment of damaged redox centers from the redoxmer backbone followed by reattachment of fully functional centers. As a first step towards this long-term objective, we set out to demonstrate the value of retrograde reactions that break up redoxmers in response to a redox-triggering event. In searching for retrograde processes in redoxmers, we again take inspiration from nature since many biomacromolecules are well suited for multi-generation lifecycles. For example, lignin is a class of complex organic biopolymers in which the β -aryl ether (i.e., a homobenzylic ether) is the most common linkage (45–60% of all linkages).¹⁹ Lignin scission at the C α -C β bonds occurs by a catalytic oxidative cleavage pathway triggered by bacteria and fungi.²⁰ An electron transfer reaction followed by a bond breaking reaction is the elementary reaction step known as mesolytic cleavage.²¹

Mesolytic cleavage is a thermodynamically favorable bond scission reaction driven by a diminished bond dissociation free energy of a radical ion. This results in the formation of one radical and one ion.²² There have been many molecular scaffolds reported that undergo mesolytic cleavage, such as alkoxyamines,^{23–26} aromatic disulfides,²⁷ benzylic thioethers,^{28,29} enol carbonates,³⁰ haloacetonitriles,³¹ and others.^{32–35} Synthetic chemists have utilized these cleavage reactions for various purposes,^{36,37} such as *in situ* carbocation generation for organic synthesis,^{24,25,28,37} single-molecular conductance control *via* electrostatic cleavage,³⁸ synthesis of terminal functionalized polymers,³⁹ and photo-controlled cationic polymerization *via* mesolytic cleavage of dithioester chain transfer agents.^{40,41} Mesolytic cleavage of homobenzylic ethers (HBEs,

Scheme 1b), were first investigated by Arnold *et al.*,^{42,43} then exploited by Floreancig and others,⁴⁴ who developed electron-transfer-initiated cyclization reactions using mesolytic cleavage of HBEs.^{45–49}

By utilizing the fundamental reaction step of mesolytic bond cleavage, we imagined redoxmer architectures in which an HBE scaffold is appended with redox-active pendant groups. The pendant groups are the energy-storage redox center, chosen to exhibit stable, reversible electrochemical performance. Programmable end-of-life deconstruction is imagined as requiring a redox potential that is outside the operational window of the pendant group. To realize this design, the mesolytic cleavage pathway of the HBE must be tightly controlled. Despite many historical precedents, there are yet no systematic studies on tuning fragmentation and electrochemical behaviors of HBEs. Here, we advanced the fundamental chemistry for this purpose. We computationally screened and synthesized a series of HBEs with different electron donating (EDG) and withdrawing (EWG) groups at the *para*-position of the aryl core (Scheme 2), selecting the most practical HBE scaffold using the methods shown in Scheme 1b. Our results not only show that it is possible to achieve compatibility with various redox active centers and the deconstruction reaction, but also demonstrate an important step in the development of programmable electroactive materials.



Scheme 2. The Chemical Structures of Homobenzylic Ethers (HBEs) with various substituents (R_i) for the Studies of Oxidative Mesolytic Cleavage *via* a Benzylic C_{α}-C_{β} Bond (Red).

Experimental

Materials and Methods

Synthetic procedures and characterization (NMR and HRMS) of HBEs and HBE-incorporated redox monomers, dimers, and polymers (i.e. viologen-appended polystyrenes with (**P**_B-**Vio-HBE**) or without (**P**_B-**Vio**) HBE linkers, and linear viologen-based redox active polymers with (**P**_M-**Vio-HBE**) or without (**P**_M-**Vio**) HBE linkers inserted into main-chain backbones) were detailed in SI.

Fragmentation Studies

Chromatograms of fragmentation were acquired using a GC-MS system (Agilent Inc, CA, USA) consisting of an Agilent 6890 gas chromatograph, an Agilent 5973 MSD and a HP 7683B autosampler (see details in SI). All results were reproduced on a Shimadzu Gas Chromato-graph/Mass Spectrometer (GCMS-QP2010Plus) equipped with an auto injector (AOC-20i) to confirm the accuracy of fragmentation pattern. The error bar of relative intensity between ben-zylic and oxocarbenium cations was estimated from standard deviation of the average of three measurements.

Electrochemistry Studies

Tetrabutylammonium hexafluorophosphate (TBAPF₆, 98%, TCI) was recrystallized twice from ethanol and dried under vacuum before use. Acetonitrile (MeCN, 99.7%, anhydrous, Sigma-Aldrich) was dried over molecular sieves in an argon-filled glovebox prior to use.

All electrochemical experiments were carried out in an argon-filled glovebox ($O_2 < 0.1$ ppm, $H_2O < 0.1$ ppm). HBE solutions containing 2-5 mM HBE and 100 mM TBAPF₆ in MeCN were used. The working electrode was a 3 mm diameter glassy carbon disc for standard CV stud-

ies. The counter electrode in all cases was a 0.5 mm platinum wire. The reference electrode was a 0.5 mm Pt wire on which a polypyrrole film was deposited as described by Ghilane et al.,⁵⁰ and this electrode was sealed in a glass tube filled with 0.1 M TABPF₆ in MeCN and fit with a porous glass frit. This ensured the potential did not drift during extended testing of each molecule. The reference was tested against ferrocene at the end of each experiment. For redoxmer-HBE molecules, a silver wire was used as quasi-reference, as any shift in potential shift could be tracked since the redoxmer potential versus ferrocene is known.

For collection experiments, a double-barreled theta ultramicroelectrode was used. Platinum wires (25 µm diameter, 99.99%, Goodfellow) were sealed in each barrel of the glass capillary. The finished theta-ultramicroelectrode (theta-UME) had the electrodes 100 µm apart (Fig. S6). The collection efficiency (collector-to-generator current ratio) was only \leq 3%, but the high throughput in these tests was valued more than high collection efficiency that could be achieved with standard scanning electrochemical microscopy (SECM; data not shown). The generator electrode was held at a mass transfer-limited potential to oxidize the HBE. The collector electrode was scanned over a 2-3 V window from near the oxidation potential (1 V vs. Fc/Fc⁺) to the negative limit of the system (usually -2 V) at 20 mV/s and back. Blanks were performed by leaving the generator at open circuit and scanning the collector. The redox potentials of the products were defined as the half-wave potentials of the reduction waves (Fig. S7).

Bulk electrolysis (BE) experiments were carried out in a W-cell with glass frits separating three compartments. Supporting electrolyte was placed in the reference and counter compartments, and the HBE solution was placed in the central working compartment. BEs were carried out with carbon felt, graphite rod, and gold slug working electrodes; carbon felt was the counter electrode, and silver wire was used as a quasi-reference electrode. Gold electrodes were deemed incompatible with HBE oxidation, as the process seemed to catalytically dissolve the gold. CVs of the products of HBE **2** using a graphite rod working electrode are shown in Fig. S11. Like theta-UME collection experiments, two reductions are seen and show minimal electrochemical reversibility.

To investigate oxidative deconstruction of redoxmers in bulk solution, membrane permeability studies were carried out in a custom Teflon H-cell with a Daramic-175 membrane separating the compartments. One cell was filled with 2 mM (repeat unit) **P**_B-**Vio-HBE**, 100 mM TBAPF₆ in MeCN solution (origin cell), and the other was filled with 100 mM TBAPF₆ in MeCN (blank cell) at equal volumes of 3.6 mL. A Pt microelectrode (25 μ m diameter) was used as working electrode in the blank cell, where CVs (100 mV/s) were run at regular intervals to quantify viologen (Vio) content based on steady-state currents. A carbon rod counter/reference electrode was used in the origin cell. Results, permeability calculations, and current corrections based on evaporation are presented in the Fig. S16.

To investigate oxidative deconstruction of redoxmers at electrode interfaces, film removal studies were performed with a 1.5 mm-diameter Pt macroelectrode. **P**_B-**Vio**, **P**_B-**Vio**-**HBE**, **P**_M-**Vio**, and **P**_M-**Vio**-**HBE** films were electrodeposited by cyclic voltammetry in 1 mM (repeat unit) polymer, 100 mM TBAPF₆ in MeCN; one cycle accessing the second reduction of viologen is adequate to precipitate multiple polymer layers on the electrode. Filmed electrodes were then gently rinsed with MeCN and placed in a blank 100 mM TBAPF₆ solution. Vio content was determined by CV (20 mV/s) of the first reduction of viologen and quantified based on the integrated area of the anodic peak. E_{ox} was accessed by CV (100 mV/s) sweeping to those potentials, leaving the film at or above the potential of HBE oxidation for a total of 3 seconds. Convection was accomplished by stirring the solution with a stir bar directly underneath the filmed electrode.

Computational Studies

All Density Functional Theory (DFT) calculations were performed using the B3LYP/6-31+G(d,p)⁵¹ level of theory as implemented in Gaussian 16, Revision A.03.⁵² To account for the free energies of solvation in acetonitrile solvent (dielectric constant = 37.5) when necessary, selfconsistent reaction-field (SCRF) calculations using the conductor-like polarizable continuum model (CPCM)^{53,54} was employed. Numerical integrations were carried using an ultra-fine grid. Equations for calculating the oxidation potentials (E_{ox}), the bond dissociation Gibbs free energy change of a radical cationic HBE (Δ G), and the bond dissociation free energy of a neutral HBE (BDFE_{Sub}) are described in detail in SI.

Results and Discussion

Fragmentation Analysis of HBEs. The *para*-substituted HBE derivatives **1-11** (Scheme 2) were synthesized from commercially available starting materials (see details in SI). All compounds were fully characterized using NMR spectroscopy and mass spectrometry. In order to probe the fragmentation behaviors of HBE radical cations, we first employed gas chromatography-mass spectrometry (GC-MS) in which neutral HBE molecules are ionized to the corresponding radical cations under electron ionization (EI) conditions and the results are shown in Fig. 1. The resulting radical cations undergo a variety of fragmentation pathways in the gas phase, and the generated cationic species are analyzed by mass spectrometry. For example, in HBE **2**, three representative cationic species with m/z values at 166.10, 121.07, and 45.03 were observed and assigned to the parent radical cation (red), benzylic cation (blue), and oxocarbenium cation (pink), respectively (Fig. 1a). Similar fragmentation patterns, with the benzylic cation displaying the highest intensity, were also found in HBEs **1**, **3**, **4**, and **5**, which all have EDGs at the *para*-position (Fig. S3, b–e). As for HBEs **6**, **7**, **9**, **10**, and **11**, which have a hydrogen atom or

EWGs at their *para*-position, the oxocarbenium cation became the most intense fragment (Fig. S3, f, g, and i–k).[§]



Fig. 1. Fragmentation Patterns of HBEs (a) GC-MS results of 2 (red, blue, and pink denote radical cations, benzylic cations, and oxocarbenium cation, respectively); (b) Proposed mesolytic cleavage pathways of HBEs (pink and blue for pathways I and II, respectively); (c) The plot of the logarithmic m/z intensity ratio between benzylic and oxocarbenium cations (Log(I_B/I_O)) as a function of the Hammett constant (σ_p^+). The error was estimated using the standard deviation of the average of three measurements; (d) The empirical σ_p^+ parameter is able to predict the distribution ratio of two major mesolytic cleavage pathways for various HBEs as well as the Boltzmann factor (BF). The BF values are calculated using the inset equation with predicted ΔG values for each cleavage pathway.

Comparison of GC-MS fragment intensities allowed us to quickly establish structurereactivity trends in the fragmentation patterns (Fig. 1b). We hypothesized that HBE electronic structures dominate the preferred selection of the competing fragmentation pathways (i.e., benzylic *vs.* oxocarbenium ion formation), as indicated by the respective pathways I and II in Fig. 1b. A plot of the logarithmic value of the intensity ratio between benzylic and oxocarbenium cations *vs.* the Hammett *para*-substituent constant σ_p^+ showed a linear correlation (Fig. 1c). As σ_p^+ shifted from negative to positive values, the fragmentation pathway shifted from benzylic-cationdominated to oxocarbenium-dominated. This indicates that control over the fragmentation pathway – at least in the gas phase – is achievable by choice of the *para*-substituent.^{55,56}

We next used these experimental observations as benchmarks for developing a computational screening and discovery tool. In particular, we employed DFT to compute oxidation potentials of HBEs and their mesolytic cleavage fragments (Eq. S1 and Table S2), as well as the Gibbs free energy change of all possible mesolytic cleavage pathways associated with HBE radical cations, ΔG_{meso} (Eq. S2).⁵⁷ By comparing the ΔG_{meso} values (Table S3), the two most thermodynamically favorable cleavage pathways for most HBE cation radicals (except for HBE 4) are Pathways I and II in Fig. 1b, thus validating the computed patterns against the GC-MS observations. Pathway I results in a benzylic radical and an oxocarbenium cation, while the Pathway II gives the opposite charge and multiplicity distribution for the two fragments. The lowest ΔG_{meso} associated with each HBE was reported in Table 1, which ranges from 1 to 2 eV.* In contrast to ΔG_{meso} , the corresponding homolytic bond dissociation free energies of the benzylic C_{α} -C $_{\beta}$ bond (BDFE_{sub}) of all HBE molecules are much larger and in a range of 3.90 – 4.13 eV (Table 1).[¶] age pathway from II to I (Table 1). This indicates that the radical cations of HBEs with *para*-substituted EDGs are relatively more difficult to fragment than the ones with *para*-substituted EWGs. A more quantitative probability analysis of two mesolytic pathways was performed by computing their associated Boltzmann factors (Fig. 1d), which shows the same decreasing trend as that observed by GC-MS (Fig. 1c). Comparing HBEs **2** and **3**, it is apparent that a more stabilized benzylic cation will lead to a higher probability of mesolytic cleavage pathway II.⁴³

| HBEs | $\frac{E_{\rm ox,1}{}^a}{\rm (V \ vs. \ Fc/Fc^+)}$ | Simulated $E_{\text{ox},1}^{d}$ (V vs. Fc/Fc ⁺) | $\frac{E_{\rm ox,2}{}^b}{\rm (V \ vs. \ Fc/Fc^+)}$ | Simulated $E_{\text{ox},2}^{e}$ (V vs. Fc/Fc ⁺) | BDFE _{sub} ^c (eV) | ΔG_{meso} (eV, Fav. Path.) ^f |
|------|--|---|--|---|--|--|
| 1 | 0.30 | 0.37 | 1.42 | 0.94 | 3.90 | 1.86 (II) |
| 2 | 1.10 | 1.14 | 1.41 | 1.68 | 3.98 | 1.79 (II) |
| 3 | 1.10 | 1.19 | 1.41 | 1.18 | 3.68 | 0.99 (II) |
| 4 | 1.55 | 1.60 | 2.00 | 1.91 | 3.96 | $1.77 (II)^{h}$ |
| 5 | 1.36 | 1.32 | 1.85 | 1.44 | 3.93 | 1.94 (II) |
| 6 | 1.78 | 1.83 | 2.27 | 2.05 | 4.00 | 1.74 (I) |
| 7 | 1.71 | 1.76 | 2.09 | 2.11 | 4.01 | 1.86 (I) |
| 8 | 2.20 | 2.27 | ^g | 2.63 | 4.13 | -1.26 (I) |
| 9 | 2.40 | 2.12 | 2.90 | 2.30 | 3.97 | 1.35 (I) |
| 10 | 2.45 | 2.08 | 2.98 | 2.45 | 3.93 | 1.31 (I) |
| 11 | 2.12 | 2.20 | <i>g</i> | 2.58 | 3.92 | 1.05 (I) |

Table 1. Summary of electrochemical and corresponding computational results of HBEs

^{*a,b*}Taken as the half-wave potentials of the respective oxidation waves at 50 mV/s; ^{*c*}Bond dissociation free energy of neutral HBE substrates (BDFE_{sub}) calculated from homolysis *via* a benzylic C_{α} - C_{β} bond in gas phase; ^{*d*}Simulated oxidation potential of neutral HBEs to their radical cations in MeCN solvent; ^{*e*}Simulated oxidation potential of benzylic cations to double cations (Fig. 2c) in MeCN solvent; ^{*f*}The calculated lowest Gibbs free energy change of mesolytic cleavage (ΔG_{meso}) is considered as the most favorable cleavage pathway (see Fig. 1b) in gas phase; ^{*g*}Second oxidation waves do not appear or overlap with electrolyte breakdown; ^{*h*}Pathway II is the second favorable cleavage pathway, as the fragments in the more favorable pathway are not observed experimentally

Electrochemistry Studies of HBEs. We used cyclic voltammetry (CV) to assess the redox potential and electrochemical reversibility of these HBEs within a specified window (Fig. 2a). Oxidations of all tested molecules[#] showed total chemical irreversibility, as they lack return reduction waves even at and above 1 V/s scan rates (Figs. 2a and S5). Only one of the solutions containing HBE **11** showed a reduction processes ascribed to the redox of the phenyl-NO₂ group as a primary electrochemical event.^{||} This lack of reductive electrochemistry makes HBEs excel-

lent candidates for exclusively oxidation-triggered rapid mesolytic cleavage of bonds in redoxmer structures. The DFT-computed oxidation potential values of the substrate to the radical cation species ($E_{ox,1}$) (Table 1) correlate well with the CV results with a mean absolute error (MAE) of 100 mV. Increasing values for σ_p^+ were reflected in the experimental $E_{ox,1}$ which shifted from 0.30 to 2.12 V vs. Fc/Fc⁺.⁵⁸ The same $E_{ox,1}$ (1.10 V) found in HBEs 2 and 3 indicates that alkylation of the benzylic position does not affect the oxidation potential of the aryl group in neutral HBEs. This is instructive for selecting a proper *para*-functionality based on the value of σ_p^+ and including other chemistries on C_a and C_β for programmable redoxmer design.

A second oxidation wave was observed in many tested HBEs (Fig. 2a). For some HBEs like **2**, these waves were much less than 500 mV more positive than the first oxidation, a benchmark that is useful for characterizing if a second redox process occurs within the same redox motif as expected by electrostatic effects upon consecutive electron transfer.⁵⁹ This is further evidence that the radical cation undergoes a bond scission step yielding two new fragments with different redox potentials. We suggest that the second oxidation belongs to the benzylic cation fragment (*vide infra*).



Fig. 2. Electrochemical Oxidation of HBEs and Collection of Cleavage Products (a) Cyclic voltammograms of three HBEs with currents normalized to the experimental oxidative peak currents (50 mV/s, 3 mm glassy carbon electrode, 0.1 M TBAPF₆ in MeCN; CVs for all HBEs are in Fig. S5); (b) Cyclic voltammogram (20 mV/s, 25 μ m Pt microelectrode) of collected products after oxidation of **2** at 1.35 V *vs.* Fc/Fc⁺ with a neighboring 25 μ m Pt microelectrode. Arrows indicate scan direction, boxes and lines refer to product groups in (c) and (d); (c) Summary of all reduction potentials of products (left) from HBE cleavage at $E_{ox,1}$ and $E_{ox,2}$ and steady state current ratios (right) of product group 2 (purple box) to group 1 (green box) after oxidation at $E_{ox,1}$. $E_{ox,1}$ and $E_{ox,2}$ correspond to values for each molecule in Table 1. Asterisks denote that products from HBEs **1**, **8**, **9**, and **10** are not in these potential ranges to compare with the current; (d) Proposed cleavage and further electrochemical pathways of HBEs based on electrochemical data. Colored pathways match redox processes outlined in (b) and (c). This mechanistic scheme represents the most possible cleavage pathways. For the sake of clarity, other cleavage pathways as well as the quenching of short-lived charged species by various nucleophiles in solution are not shown.

To determine the identity and stability of the fragments, we employed a generationcollection technique with a double-barreled theta-UME (Fig. S6). This high-throughput method enabled potentiostatic oxidation of the HBE at one electrode and oxidation or reduction of the fragmented products via CV at a neighboring electrode, just 100 µm away. The results for HBE 2 are shown in Fig. 2b; all HBE results are in Fig. S7 and summarized in Fig. 2c. For HBEs 2-7 that have EDGs or weak EWGs on the benzene ring, two reduction waves are seen in the same potential ranges, one group at -0.6 \pm 0.3 V and one at -1.7 \pm 0.2 V vs. Fc/Fc⁺. Additionally, the steady-state current from group 2 is consistently 2 to 3 times that of group 1, indicating that the products between HBEs are similar in size since currents are based on diffusion, which in turn depends on molecular size. This is expected from a controlled C_{α} - C_{β} bond cleavage as opposed to random fragmentation in the molecule. Both reductions are related to the benzylic fragment as proposed in the mechanism in Fig. 2d, as oxidation of a methoxybenzene with a butyl chain instead of the benzylic ether showed products at the same reduction potentials as HBE 2 (Fig. S8). Based on the difference in size between the oxocarbenium and benzylic cations, the current intensity differences observed for the two reduction processes (Fig. 2c) support the reduction of the benzylic cation (group 1) followed by reduction of both the oxocarbenium and benzylic species (group 2). It is also possible that group 1 contains the reduction of both benzylic and oxocarbenium cations, and that group 2 contains the second reduction of these species along with the reduction of other chemical adducts (e.g. cationic species chemically trapped by decomposed solvent and electrolyte, as shown in Fig. S22) (vide infra). Thus, the generation-collection currents we observe may be from a mixture of multiple components, including the proposed reactive intermediates in Fig. 2d and various quenched products.

Based on DFT calculations, the methoxy-substituted benzylic and oxocarbenium radicals have oxidation potentials at 0.01 and -0.04 V and reduction potentials at -1.93 and -2.20 V vs. Fc/Fc⁺, respectively (Table S2). Two reductions and no oxidations are seen experimentally because when the HBE is cleaved into radical and cation at the electrode, the radical (whether on the ether or benzylic group) is immediately oxidized since the electrode is well positive of their predicted standard redox potentials.[†] This suggests that the oxidation of these HBEs follows an Electrochemical-Chemical-Electrochemical (ECE) mechanism, where the first electrochemical step (oxidation of the HBE) is followed by a rapid irreversible chemical step (mesolytic cleavage) that produces oxidizable products (radicals) which are rapidly oxidized and only observed once reduced (Fig. 2b). The one-electron reduction of the p-NO₂ moiety in HBE acts as an internal standard to probe the mobility of the parent HBE. We compared its Randles-Sevcik slope to that obtained via the oxidative cleavage process (Fig. S10). Our analysis showed that the oxidative process displays a current intensity 1.5 times higher than the reduction peak of the p-NO₂ aryl moiety, thus suggesting a multi-electron process as expected for the proposed ECE mechanism. A multi-electron transfer mechanism is apparent from macrodisk voltammetry of other HBEs, where the currents for HBE oxidation favor n = 2 electrons based on calculations using the Randles-Sevcik equation (Fig. S10).⁶⁰ The double oxidation phenomenon essentially overrides the distinction between differentiated cleavage pathways I and II as discussed above, since both cations are inevitably formed. However, qualitatively, we observed more electrode passivation (via unwanted chemical degradation, polymerization, etc.) with EWG-containing HBEs, which may be due to pathway differences and/or the high potentials required to oxidize these molecules. Nonetheless, the ECE mechanism is advantageous for two reasons: it mostly eliminates chemically reactive radicals, and it produces two charged products from a neutral molecule, making the fragments more soluble in polar solvents.

Similar experiments were carried out with bulk electrolysis (BE) of HBE 2 (Fig. S11), in which the entire solution of HBE was electrolyzed and the products detected with a UME. The resultant fragments detected qualitatively match collections from theta-UME experiments, i.e., reduction potentials and current ratios are similar. This shows that these cationic products are stable over wide timescales, from single seconds (theta-UME) to tens of minutes and hours (BE). However, the products are not electrochemically reversible, as the reduction of these cations show minimal re-oxidation. Additionally, the experimental reduction potentials differ greatly (up to 500 mV more negative) from the predicted potentials (Table S2), indicating that either these products undergo a secondary chemical step or they are strongly dependent on solvent and electrolyte interactions that are not accurately predicted by our modelling. Previous studies on the electrooxidation of *p*-methoxytoluene have shown that aryl-aryl coupling can occur between oxidized methoxybenzene species in non-aqueous conditions, where two radical cations couple followed by deprotonation.⁶¹ This was shown to occur on the 10⁻⁵ s timescale, which indicates a moderately high kinetic barrier to this process. We believe the C-C bond cleavage dominates in our system for three reasons: 1) the C-C bond cleavage is predicted to be the most energetically favored (Fig. S95), 2) the deprotonation will also be slow in the absence of base, and 3) the low concentration of our HBEs (<5 mM) should limit the rate of bimolecular reaction. Additionally, we see no coupling in our HBE-containing polymers following oxidation (vide infra), indicating that dimerization does not occur even when the HBEs are in high concentration by being tethered together in the polymer. ¹H NMR of the oxidized products of **HBE 2** show very little aromatic signals aside from the parent molecule and the cleaved products that would indicate this process

(Fig. S26). Still, this mechanism may operate at higher concentrations (the >0.5 M in a RFB) and requires study in future. ¹⁹F NMR studies on bulk electrolyzed products (Fig. S22) indicate that new fluorine adducts were generated after BE, which may be attributed to the decomposition of PF_6^- in the electrolyte followed by association of the fluoride anion with the carbocation products. Chemical trapping analysis on the products from mesolytic cleavage was also examined to confirm the formation of oxocarbenium cations (Figs. S23 and 24).^{**,37} While further spectroscopic studies are underway to elucidate the chemical mechanisms and product identities, our results here show that HBEs are cleaved to form stable, soluble products in non-aqueous systems *via* oxidation at an electrode.

Applications of HBEs in Redoxmer Dimers. Redox-triggered deconstruction of the HBE scaffold must occur outside of the redox potential window of the redox-active centers. Moreover, the oxidation of cleavage moieties should not chemically or electrochemically interfere with the redox-active unit's charge and discharge. To demonstrate this, we appended four different redox active moieties to dimer systems based on HBE 2: two catholytes, TEMPO and a dialkoxybenzene (DAB),⁶² and two anolytes, ethyl viologen (Vio)[‡] and *para*-nitrobenzene (NP) (Fig. 3). The DAB redox potential is sufficiently negative (0.5 V negative compared to **HBE 2**) so that the HBE is not cleaved under normal cycling conditions, while the remaining three are significantly more negative than the cleavage potential for the HBE linkage.



Fig. 3. Compatibility Tests with HBE-Containing Redoxmer Dimers Slow (left) and fast (right) CV scans of (a) **TEMPO dimer**, (b) **DAB dimer**, (c) **DiHBE Vio**, and (d) **NP dimer**, (3 mm glassy carbon electrode, 0.5-1 mM dimer, 0.1 M TBAPF₆ in MeCN) before and after cleavage of the HBE core. Slow scans demonstrate chemical compatibility of the redox unit with HBE cleavage products and no film formation on the electrode, while fast scans reveal how compatible the redox units are with the high positive potentials applied to cleave the HBE. "Before" corresponds to CVs just in the potential window of the redoxmer. "After" corresponds to CVs of the redoxmer after the HBE had been oxidized in the same CV scan. Gray arrows show the emergence of new peaks in (b); pink arrows show smaller, distorted peaks in (d). Full CVs are shown in Fig. S12.

To initially judge the chemical and electrochemical compatibility of these redoxmers and HBEs, we tested these species at slow ($\leq 100 \text{ mV/s}$) and fast ($\geq 1 \text{ V/s}$) scan rates. Scanning slowly allows time (≥ 4 s here) for potential chemical processes (redoxmer deactivation by HBE products, film formation, etc.) to occur after HBE cleavage, as products are released into solution from the electrode surface. Fast scan CV gives a better idea of electrochemical compatibility because molecules have less time (<0.5 s in the case of the DAB dimer) to diffuse from the electrode surface as the electrode surface at the electrode.

Fig. 3 compares fast and slow scan CVs for HBE architecture appended with the four different redox units. At all scan rates, **TEMPO dimer** and **DiHBE Vio** show well-behaved, reversible signals.^{††} The **DAB dimer** is mostly the same, although the potentials used to cleave the HBE are nearing potentials of the second oxidation of DAB, which is known to be highly irreversible and produce side products like quinones and biphenyls⁶³ that might yield different rereduction current profiles as seen in Fig. 3b (gray arrows). In contrast, the **NP dimer** showed degradation in both fast and slow scans. At fast scan rates, cleavage products are reduced before and along with the nitrobenzenes; any chemical reactivity between these species may deactivate the nitrobenzene and thus lower overall currents compared to the neat condition (pink arrows, Fig. 3d). At slow scan rates, in which more time is allowed for HBE oxidations, a film slowly accumulates on the electrode surface for this particular HBE, limiting the re-oxidation of the nitrobenzene; similar observations were made while testing HBE **11** (Fig. S9). Further evidence of HBE cleavage of redoxmer-HBE architectures is seen in BE collection experiments (*vide infra*), as the products show the same reduction potentials as the pure HBEs.



Fig. 4. Bulk Electrolysis Studies of an HBE-Containing Redoxmer Top Row: Outline of the BE steps to test the HBE-TEMPO shown. Middle Row: Charge and discharge curves corresponding to the BE steps. Bottom Row: UME CVs (25 μ m Pt microelectrode) taken of the solution following BE steps showing the TEMPO redox. The solution contained 2 mM HBE-TEMPO, 0.1 M TBAPF₆ in MeCN, and BE was carried out with a carbon felt working electrode in a W-cell (see Electrochemistry Studies in SI for details).

We also tested the extreme condition where all HBEs in solution are cleaved *via* BE to determine if large-scale programmed degradation is possible. Fig. 4 shows the BE results of a TEMPO-appended HBE monomer. Full charge and discharge of the redox unit is facile. After the first charge-discharge cycle (Fig. 4, II-III), the HBE was cleaved (Fig. 4, IV); at these potentials, TEMPO will also be oxidized. CVs with a UME in the solution revealed that the TEMPO⁺ product is electroactive, showing that the redox center survived the high cleavage potentials. Discharging (re-reducing, Fig. 4, V) the now-cleaved TEMPO⁺ yields the expected charge value

(ca. 0.8 C here), but UME CVs surprisingly show that the TEMPO has become almost entirely redox inactive. It is possible that the TEMPO interacts with reactive species from HBE oxidation, forming a N-O-R complex that is redox inactive in the usual potential window.³⁸ Indeed, these complexes showed some partial release of redox active TEMPO after re-oxidizing them at high potentials (Fig. S14).⁵⁵ This result is consistent with the CV data of this species (Fig. S13), as here the whole solution has ample time and stirring to react TEMPO with the HBE products compared to small quantities in the diffusion layer in CVs. While re-reduction in the presence of HBE products is inadvisable in this case, the TEMPO/TEMPO⁺ redox couple can withstand the high potentials needed to cleave the HBE, proving this architecture can be of practical use for redox-triggered degradation.

BE tests were also run with the **DiHBE Vio** from Fig. 3c and show similar trends to **HBE-TEMPO** (Fig. S15). Charge and discharge before cleavage show reversible electrochemical signals, but once the molecules are cleaved, the viologen reduction occurs at a similar potential as the HBE products. Further charging of the solution ends up reducing the HBE products (at the electrode surface and through Vio⁺⁺ mediation), eliminating the Vio wave. While this shows that cleaved products should not be fully recharged after cleavage, it is promising that both redoxmers and HBE products are stable and thus could be recovered and separated downstream after cleavage (*vide infra*).

Application of HBEs in Redox Active Polymers. Redox active polymers (RAPs) show promise for use in RFBs due to their low crossover between compartments separated by sizeexclusion membranes that decrease RFB cell resistance.¹⁵ However, RAPs have a tendency deposit on electrode interfaces over time compared to monomeric and dimeric redoxmers.^{64,65} This challenge could be addressed by employing the deconstruction chemistry of HBEs. Here we incorporated cleavable HBE linkers into both branched and main-chain RAPs to evaluate their programmable deconstruction at electrode interfaces and in bulk solutions.



Fig. 5. HBE-Incorporated RAPs and Deconstruction at the Electrode Interface. Structures of (a) viologen-appended polystyrenes with (P_B -Vio-HBE) or without (P_B -Vio) HBE linkers, and (b) linear viologen RAPs with (P_M -Vio-HBE) or without (P_M -Vio) HBE linkers inserted in-

to main-chain backbones; (c) Cartoon demonstrating the partial removal of electrodeposited film content following the applied potential (E_{ox}); CVs of electrodeposited thin films of (d) **P**_B-Vio-**HBE** and (e) **P**_M-Vio-HBE as deposited, after applying potentials to oxidize the HBE, and after stirring the solution for various times. Normalized charges of Vio reduction from electrodeposited films of (f) branched and (g) main-chain polymers after oxidation and solution stirring. Error bars are average of three trials with three different electrodes and films. More information can be found in the SI.

As a proof-of-concept, we first took a well-studied viologen-appended polystyrene (**P**_B-**Vio**) as a control RAP and inserted a *p*-methoxy HBE linker between the Vio center and the polystyrene backbone to obtain a cleavable RAP (**P**_B-**Vio**-**HBE**) (Fig. 5a). **P**_B-**Vio** is known to deposit films on the electrode surface when overcharged (i.e., accessing potentials negative enough to reduce Vio^{2+} to Vio^{0}). While these films mediate charge transfer with solution species, films that are too thick impede electron transfer rates and reduces the power output of the battery over time.⁶⁵ The ability to remove these films periodically would provide simple way to maintain cells without replacing the electrode (Fig. 5c).We individually electrodeposited **P**_B-**Vio**-**HBE** and **P**_B-**Vio RAPs** on electrode surfaces to generate films with similar thickness for proof-of-concept defouling tests (Fig. S17). To understand the effect of polymer architecture on defouling behavior, we also synthesized and tested main-chain viologen polymers with (**P**_M-**Vio**-**HBE**) and without (**P**_M-**Vio**) HBE linkers within the backbone (Fig. 5b).

Filmed electrodes were defouled under two conditions: application of positive potentials (E_{ox}) that will oxidize HBE linkers, and solution convection underneath the filmed electrode, which imitate the effect of potential and flow in an RFB, respectively. Film content was quantified by integrating the charge from CVs of the Vio-containing RAP film (Figs. S18 and S19). For **P**_B-**Vio-HBE**, immediately applying E_{ox} for 3 seconds has little effect on removing the film; only convection directly following film oxidation leads to the decrease of the film viologen con-

tent, though not by more than 30% (Figs. 5d and f). Additionally, there is no significant difference between the polymer with HBE and without HBE, indicating that although some HBEs are oxidized (likely just what is near the electrode surface and can transfer electrons), it does not disrupt the polymer film. This holds true for thin (one electrodeposition cycle, Fig. 5d) and thick films (ten electrodeposition cycles, Fig. S18), showing a fundamental limit of removal for this specific viologen polymer structure. In contrast, the main-chain polymer PM-Vio-HBE loses 30% of the viologen signal upon oxidation, and over 50% of the film is removed with convection. Like the branched equivalent, however, there is only slightly more removal with the HBEcontaining **P**_M-Vio-HBE compared to the non-HBE-containing **P**_M-Vio, although more than 50% of the film can be removed under these conditions. Additionally, after application of E_{ox} , **P**_M-Vio-HBE displays a slight positive shift and broadening of the CV wave, suggesting a small change in the energetics of adsorption and on the electrostatic interactions experienced by the adsorbed redox species.^{65, 66} This suggests that, while not removing the adsorbed polymer, bond cleavage in **PM-Vio-HBE** may still lead to morphological changes detectable by its redox chemistry.

These results reveal several aspects of RAP-electrode interface design. First, polymer architecture – and by extension film morphology – plays a significant role in electrode passivation with RAP adsorption and how easily those films can be removed. Second, HBE incorporation into RAPs in this initial form plays a trivial role in film removal. As alluded to above, this is likely due to the fact only the HBE linkers near the electrode surface (within the first few nanometers) are oxidized. Since the ether linkage cleaves rapidly, there is little time for the oxidative charge to percolate out further in the film before a "dead layer" of cleaved polymer forms on the electrode surface. This is evidenced by the persistence of the viologen signal even after multiple removal treatments. Third, the removal of these particular Vio-containing RAPs is mostly driven by convection and electrostatic desorption, as evidenced by Fig. 5g where the P_M -Vio is removed almost as much as P_M -Vio-HBE after applying E_{ox} . This suggests another design strategy for film removal: non-faradaic desorption caused by charge repulsion between the backbone of the polymer and the electrode surface. All of these discoveries can direct future RAP design with or without cleavage chemistries to improve electrode longevity.



Fig. 6. Deconstruction of HBE-Containing RAPs in Bulk Solution and Interactions with Size-Exclusion Membranes. (a) Schematic representation of the membrane permeability of HBE-Containing RAPs before and after oxidative deconstruction; (b) Microelectrode cyclic voltammograms of 2 mM (repeat unit) **PB-Vio-HBE** solution before and after bulk cleavage of the HBE linkers. Redox peaks in neat **PB-Vio-HBE** (black lines) are typical for RAPs that adsorb onto the electrode surface. When cleaving Vio units from **PB-Vio-HBE** RAPs, a higher current that is commensurate with an increase in apparent diffusion coefficient and the disappearance of

RAP peaks are observed; (c) Crossover experiments using a Daramic 175 size-exclusion membrane show two orders of magnitude faster crossover of the cleaved Vio monomers compared to the neat P_B -Vio-HBE RAP.

Beyond the removal of thin films from electrode interfaces, we investigated the deconstruction of HBE-containing RAPs in bulk solutions and how they would interact with other RFB components, namely the separator membrane between catholyte and anolyte compartments (Fig. 6a). To test this, bulk electrolysis was used to oxidize all the HBEs in a 2 mM solution of P_{B} -Vio-HBE. Microelectrode CVs before and after bulk electrolysis show both an increase in the Vio reduction current, which is indicative of a larger diffusion coefficient for the repeat unit versus the polymer, and a loss of **P**_B-Vio-HBE peak features in the oxidative sweep, indicating the removal of the Vio side chains from the polymer backbone (Fig. 6b).⁶⁵ NMR analysis of electrolyzed products also shows efficient cleavage of polymeric Vio species to monomeric ones (Fig. S21). Using a size-exclusion membrane (Daramic 175),⁶⁷ the crossover rates of cleaved Vio species and neat P-HBE-Vio between two compartments were compared. The cleaved redoxmer shows two orders of magnitude higher permeability⁶⁸ ($1.0 \times 10^{-3} \text{ cm}^2/\text{min}$) than the un-cleaved form $(1.2 \times 10^{-5} \text{ cm}^2/\text{min})$, and after 24 hrs, nearly half of the cleaved species (~45% of Vio units) pass through the membrane, which is close to full crossover relying on diffusion alone (Fig. 6c). An important aspect of deconstructing RAPs *in-situ* is to separate the cleaved products from un-cleaved RAPs. These results demonstrate that size-exclusion is an effective way to separate deconstructed components from RAPs that are still functioning in the bulk solution of the RFB, as long as measures are taken to prevent excessive crossover to the opposite RFB compartment.



Scheme 3. Proposed Utilization of Programmable End-of-Life Chemistries in RFBs. Cleavage chemistries incorporated into redoxmer architectures provide a way to defoul interfaces (A) and recycle redox components at the bulk scale (B). In practice, we envision redoxmer deconstruction triggered by redox stimuli happening through electrolysis at the electrode interface (shorter time of triggering stimuli for surface defouling, longer for larger volume recycling) followed by flow through a secondary collection system. This system can utilize size-exclusion membranes to separate redox centers from organic backbones, and ideally would allow chemistries for redoxmer regeneration *via* the re-appending of intact redox centers to the backbone and injecting the regenerated redoxmer solution back into the primary system. In such a way, a selfcontained and integrated RFB system could directly solve its capacity fade problems to sustain battery lifetimes. Note: the schematic redoxmer cartoon represents a universal programmable architecture rather than a single branched one.

Finally, we present a vision for the application of these concepts in a practical RFB (Scheme 3). Should the electrodes foul or redoxmers chemically degrade, removal of those species is key to sustaining battery lifetime. Redox active linkers within redoxmers are cleavable at the electrode as demonstrated above. To prevent accumulation of deconstructed components in the primary tank and limit crossover between catholyte and anolyte compartments, the contaminated solution is flowed through a secondary system. This collection system is used to separate

cleaved species from un-cleaved redoxmers *via* a membrane based on size (as demonstrated in Fig. 6), charge, or other properties. The products are then filtered through the system to separate redox centers and backbones, which would then ideally be regenerated, reattached (through chemical or electrochemical means), and recycled into the primary system. In this way, RFBs sustain their power and energy density by recycling dysfunctional material without the need for fully shutting down the system to refill and rebalance the solution. There are several chemical and engineering challenges to make this a reality, but this work provides the first steps – controlled deconstruction, and the tools to design and analyze new materials – towards this sustainable goal.

Conclusion

In summary, we have systematically studied the oxidation-triggered mesolytic cleavage of a series of HBE molecules for potential use in redoxmer architectures. By changing the *para*substituent on the aryl core of HBE molecules, we were able to tune the most favorable mesolytic fragmentation pathway and oxidation potentials of HBE substrates. DFT, GC-MS, and generation-collection electrochemical methods were used to confirm these fragmentation pathways and offered insight into relevant structure-activity properties of HBEs to guide redoxmer design. Due to its oxidation potential and stable charged products, the HBE with the *para*-OMe group was chosen and integrated with various redox centers, among which TEMPO, DAB, and viologen are left chemically and electrochemically compatible with the cleavage of HBE linkages. As a proof-of-concept, Vio-containing RAPs incorporating HBE linkers were prepared to elucidate programmable deconstruction of redoxmers from an interface for electrode defouling and in bulk solution for potential downstream recycling. Deconstruction efficiency of cleavable redoxmers from an interface was improved by using main-chain RAPs compared to branched ones. The design of programmatically cleavable redoxmers takes the first step towards the development of sustainable materials for electrochemical and energy storage devices. Further research will investigate the long-term stability and the charge capacity recovery of these cleavable redoxmers in a flow battery cell. The HBE chemistries reported here may also be applicable in aqueous organic redox flow batteries,⁶⁹ as HBE oxidation in the presence of water would yield soluble alcohols.⁷⁰ The chemistries are applicable to both catholyte and anolyte materials, although care must be taken to ensure full redoxmer-cleavage moiety compatibility. We are currently exploring other mesolytic cleavage chemistries so that a synthetic toolkit will be available for all redoxmers to incorporate programmable cleavage.

Conflicts of interest

There are no conflicts to declare

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