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The application of machine learning for predicting the methane uptake and working capacity of MOFs

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Multiple linear regression analysis, as a part of machine learning, is employed to develop equations for the quick and accurate prediction of the methane uptake and working capacity of metal–organic frameworks (MOFs). Only three crystal characteristics of MOFs (geometric descriptors) are employed for developing the equations: surface area, pore volume and density of the crystal structure. The values of the geometric descriptors can be obtained much more cheaply in terms of time and other resources compared to running calculations of gas sorption or performing experimental work. Within this work sets of equations are provided for the different cases studied: a series of MOFs with NbO topology, a set of benchmark MOFs with outstanding methane storage and working capacities, and the whole CoRE MOF database (11 000 structures).

Introduction

Methane, as a major component of natural gas, is considered to be an alternative fuel to oil. Natural gas is much cleaner than gasoline or diesel.¹ Methane is a gas at room temperature and pressure and has a very low energy density. To overcome this problem, there are two forms of stored natural gas in automobiles – liquified for trucks and compressed for personal cars. MOFs have been studied for years as promising adsorbents for automobile applications. MOFs are promising materials for different applications: gas storage^{2–6} and separation,^{7–9} catalysis,^{10–12} sensing,¹³ electrochemical energy storage,^{14–16} memory devices,¹⁷ biomedical imaging,^{18,19} biomolecule encapsulation and drug delivery.^{20–23} The US Department of Energy (DoE) has established targets of 50 wt% and 263 cm_(STP)³ cm^{−3} for methane storage methods suitable for such employment. On the one hand, recent results show that it is almost impossible to simultaneously get both the gravimetric and volumetric methane working capacities at room temperature.²⁴ On the other hand, there have been some recent improvements showing the great potential of MOFs for effective methane storage.²⁵

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Computational approaches have played a great role in studying MOFs and other porous materials for gas storage: grand canonical Monte Carlo methods (GCMC) for revealing adsorption isotherms, classical molecular dynamics (MD) for studying gas diffusion in MOFs, density functional theory for obtaining favourable binding sites and crystal structure change, *etc.* Material simulations have been predicting novel advanced not yet synthesized MOFs since 2004,²⁶ when the design of new IRMOF materials was proposed for methane storage using computer simulations. The large-scale screening of hypothetical MOFs has been performed computationally by creating porous structures from chemical databases of building blocks, which are based on known MOFs.²⁷ More than 300 MOFs have been identified with outstanding methane storage capacities and structure–property relationships were also revealed. A total of 122 835 MOFs have been designed computationally to reveal both the total methane uptake and working capacity as a function of the void fraction, volumetric surface area and heat of adsorption, identifying a maximal working capacity at room temperature.²⁸

A lot of effort has been put into creating a database of structures for computational screening, which are free from solvents, disorders, *etc.* The Computation-Ready, Experimental Metal–Organic Framework Database (CoRE MOF Database) contains over 14 000 porous, three-dimensional MOFs.²⁹ It is very convenient for potential users that pore analytics and physical property data are included as well.²⁹ Another database is a subset of the Cambridge Structural Database (CSD), where 69 666 MOF materials were identified by the Cambridge Crystallographic Data Centre (CCDC).³⁰ A total of 13 512 MOFs with 41 different edge-transitive topologies were generated using the ToBaCCo code, which employed a reverse topological approach.³¹ The structure files of MOFs obtained experimentally and published can contain some disorders, solvent molecules, *etc.* which are not suitable for computational work.

Recently, machine learning (ML) has become an important tool in designing new materials, leading materials chemistry towards more rational design.³² The World Economic Forum identified the union of big data and artificial intelligence as the Fourth Industrial Revolution, which can dramatically improve the research process.³³ The high-throughput screening (HTC) of databases employing MD or GCMC is computationally very intensive and demanding. On the one hand, the employment of ML methods can significantly decrease the complexity of computational screening, and at the same time provides results with high accuracy, and on the other hand, the existing results of the HTC of databases are an outstanding opportunity for employing ML methods to reveal desired properties. ML has been employed to perform an analysis of the chemical diversity of MOFs.³⁴ ML methods are significantly developed nowadays, but in the case of MOFs there is still a lot of work that needs to be done. ML is very promising approach in discovering new MOFs, revealing structure–property relationships. Predictive algorithms are employed to help and sometimes replace simulations. There are some nice examples of employing ML for discovering the properties of porous materials: an artificial neural network has been used to identify the performance limits of methane storage in zeolites, and revealed good agreement in the methane working capacity of the top structures between the zeolites and the structures generated by the neural network.³⁵ A MOF generation approach based on ML was discovered in ref. 36 by devising and constructing the supramolecular variational autoencoder (SmVAE). SmVAE is employed for the “inverse design”, where MOFs with the best



performance are identified and generated. A generative adversarial artificial neural network has been created to produce 121 crystalline porous materials, employing inputs in the form of energy and material dimensions.³⁷ Finally, there has been a nice overview of ML algorithms for the chemical sciences.³⁸

Experimental and/or computational work needs to be done to reveal the desired property of a structure. In case of identifying the sorption properties of experimentally obtained MOFs, computer simulations need to be done or specific equipment should be employed. This is acceptable for studying several crystals, but in the case of revealing the properties of a big family of structures conventional approaches are too costly in terms of time, money, workforce, *etc.* ML can help a lot for revealing the properties of MOFs, saving both experimental and computational efforts. In spite of the wide employment of ML techniques, they have been used very rarely for developing equations describing the sorption properties (including the working capacity) of MOFs.

Linear regression is a supervised ML algorithm. Simple linear regression employs the slope–intercept form, where x is the input data (independent variable), $f(x)$ is the prediction (dependent variable), k is the slope coefficient for the x variable and b is the y intercept, which are adjusted *via* learning to give the accurate prediction: $f(x) = kx + b$. Multiple linear regression is the most popular form of linear regression. Multiple linear regression is employed to show the relationship between one dependent variable and two or more independent variables: $f(x, y, z) = ix + jy + kz + b$, where x, y and z are the independent variables, $f(x, y, z)$ are the dependent variables and i, j, k and b are the adjustable parameters.

The main goal of this work is to show that multiple linear regression analysis is an outstanding tool for revealing the structure–property relationships of MOFs. More importantly, by employing multiple linear regression analytical equations can be developed, showing that the methane total and working capacity values at different thermodynamic conditions can be calculated from three variables based on the crystal characteristics of MOFs (geometric descriptors): surface area, pore volume and density. The values of the descriptors can be obtained routinely and very quickly in comparison to GCMC simulations or experimental work by well known and highly efficient simulation packages such as Poreblazer,^{39,40} Zeo++,⁴¹ *etc.*

Therefore, if an experimentalist or theoretician has a file with a crystal structure, or a bunch of files, she/he can easily obtain the methane total and working capacities by simply employing the equations. The performance of the model designed can be measured by several characteristics: the mean absolute error (MAE), mean square error (MSE), root-mean-square error (RMSE) and the coefficient of determination, R^2 , as described below, where x_i is obtained from experiments or GCMC simulations, y_i is the value predicted by multiple linear regression and \bar{y} is the average of the predicted values.

$$\text{MAE}(x, y) = \frac{1}{n} \sum_{i=1}^n |x_i - y_i|$$

$$\text{MSE}(x, y) = \frac{1}{n} \sum_{i=1}^n (x_i - y_i)^2$$



$$\text{RMSE}(x, y) = \sqrt{\frac{1}{n} \sum_{i=1}^n (x_i - y_i)^2}$$

$$R(x, y)^2 = 1 - \frac{\sum_{i=1}^n (x_i - y_i)^2}{\sum_{i=1}^n (y_i - \bar{y})^2}$$

It should be noted that a higher value of R^2 and lower values of MAE, MSE and RMSE show the better accuracy of the ML model used. R^2 is in the range between 0 and 1, where 1 shows that the prediction is performed without any error from the set of geometrical descriptors and 0 means that the prediction cannot be performed by any of the geometrical descriptors.

Results and discussion

Application of multiple linear regression analysis for developing equations from a set of MOFs with one topology (NbO)

The application of multiple linear regression analysis has shown very exciting results for developing equations of the methane total uptake and working capacity of a family of MOFs with the same topology. Multiple regression analysis has been applied to reveal structure–property relationships, employing data obtained for MOFs with NbO topology studied by different groups, pioneered by Chen *et al.*,⁴² and then Schröder *et al.*^{43–45} and Bai *et al.*⁴

The following parameters (descriptors) of the crystal structures of MOFs of different sizes are used to develop the equations for predicting the gravimetric total uptake and working capacity of methane sorption obtained at a pressure range of 65–5 bar at a temperature of 298 K: surface area (Sa), density of a crystal (Dc) and pore volume (Pv). The data of the crystal structure parameters, as well as the values of the total uptake (at a pressure of 65 bar) and working capacity (at a pressure range of 65–5 bar) at a temperature of 298 K are summarized in Table 1.

The equations developed are shown below:

$$\text{Total_uptake} = 181.726 + 0.02 \times \text{Sa} + 138.777 \times \text{Pv} - 38.763 \times \text{Dc}$$

$$R^2 = 0.931; \text{MAE} = 7.59 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 111.47; \text{RMSE} = 10.56 \text{ cm}^3 \text{ g}^{-1}.$$

$$\text{Working_capacity} = 266.409 + 0.038 \times \text{Sa} + 23.013 \times \text{Pv} - 176.169 \times \text{Dc}$$

$$R^2 = 0.913; \text{MAE} = 9.33 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 151.56; \text{RMSE} = 12.31 \text{ cm}^3 \text{ g}^{-1}.$$

The results obtained with multiple linear regression analysis show that for the family of MOFs with the same topology (NbO) $R^2 = 0.931$ for the total uptake and $R^2 = 0.913$ for the working capacity. Delightfully, the MAE is very small: $7.59 \text{ cm}^3 \text{ g}^{-1}$ and $9.33 \text{ cm}^3 \text{ g}^{-1}$ for the total uptake and working capacity, respectively. The RMSE shows moderate values: $10.56 \text{ cm}^3 \text{ g}^{-1}$ and $12.31 \text{ cm}^3 \text{ g}^{-1}$ for the total uptake and working capacity, respectively.



Table 1 Geometrical descriptors (Sa, Pv and Dc), total uptake (at 65 bar) and working capacity (at 65–5 bar) at 298 K

MOFs	Sa, m ² g ^{−1}	Pv, cm ³ g ^{−1}	Dc, g cm ^{−3}	Total uptake, cm ³ g ^{−1}	Working capacity, cm ³ g ^{−1}	Ref.
ZJU-5a	2829	1.08	0.679	367	277	46
UTSA-75a	2836	1.06	0.698	360	275	46
UTSA-76a	2820	1.09	0.699	368	282	46
UTSA-77a	2807	1.08	0.690	361	272	46
UTSA-78a	2840	1.09	0.694	363	275	46
UTSA-79a	2877	1.08	0.697	366	277	46
NOTT-101a	2805	1.08	0.688	344	263	46
UTSA-111a	3252	1.229	0.590	397	309	25
UTSA-20a	1620	0.66	0.909	278	206	47
UTSA-88a	1771	0.685	0.860	288	215	48
UTSA-80a	2280	1.03	0.694	336	251	49
PCN-14	2000	0.85	0.829	334	228	47
NOTT-100a	1661	0.677	0.927	248	150	50
NOTT-102a	3342	1.268	0.587	404	327	50
NOTT-103a	2958	1.157	0.643	367	285	50
NOTT-109a	2110	0.850	0.790	306	215	50
NJU-Bai 41	2370	0.92	0.741	331	232	4
NJU-Bai 42	2830	1.07	0.693	356	278	4
NJU-Bai 43	3090	1.22	0.639	397	310	4

The main conclusion from this part is that from using only the crystal structure parameters of a series of MOFs with NbO topology anyone can calculate the methane working capacity and total uptake, using the equations developed, very easily and extremely fast with a high precision. This is extremely useful for discovering new structures and screening MOFs with the same topology. For example, a user can draw and optimize a MOF in Material Studio (or employing other programs), reveal the values of the geometrical descriptors using the simulation packages Poreblazer or Zeo++, or tools in Material Studio, then use the equations to get the accurate values of the methane total uptake and working capacity. Of course, the same approach can be expanded for other MOFs with other topologies. Once equations are developed, there is no need to run simulations and/or perform experimental work.

Application of multiple linear regression analysis for developing equations from the set of benchmark MOFs

Another case to have a look at is the set of benchmark MOFs, obtained by different groups around the globe: NiMOF-74, UTSA-20, MOF-505, PCN-14, HKUST-1, NOTT-109, NU-135, UTSA-80, NOTT-101, UTSA-76, NOTT-103, NOTT-102, NOTT-122a/NU-125, NU-800, ZJU-36, NU-140, NU-111 and Al-soc-MOF-1. These frameworks have outstanding methane total uptakes and working capacities, and this data is considered for applying multiple linear regression analysis for developing equations. It should be noted that there has been a nice attempt to develop an empirical equation for the prediction of methane storage capacity at 65 bar and 270 K for the set of benchmark MOFs.⁵¹ The average deviation was found to be below 4%, which shows good applicability. The empirical equation can be used



for predicting the methane storage of MOFs, employing the following parameters: density of the crystal and pore volume. The set of benchmark MOFs is always of interest to compare with new MOFs obtained experimentally or theoretically.^{24,52,53} The following geometrical descriptors are employed to develop the equations for predicting the gravimetric total uptake and working capacity: Sa, Dc, Pv. The data of the crystal structure parameters, as well as the values of the total uptake (at a pressure of 65 bar) and working capacity at temperatures of 240 K, 270 K and 298 K (at a pressure range of 65–5 bar), are shown in Table 2.

In contrast to the previous case considered, several equations are developed for the set of benchmark MOFs, which have different topologies, metals in nodes, *etc.*, therefore the values of R^2 , MAE and RMSE are expected to be more moderate. The equations are developed for the quick and accurate prediction of the methane uptake and working capacity employing only three crystal characteristics of MOF (descriptors): surface area, pore volume and density of the MOFs. The equations are shown below:

At 298 K

$$\text{Total_uptake} = 233.476 + 0.062 \times \text{Sa} + 2.595 \times \text{Pv} - 87.024 \times \text{Dc}$$

$$R^2 = 0.965; \text{MAE} = 14 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 291; \text{RMSE} = 17.07 \text{ cm}^3 \text{ g}^{-1}.$$

$$\text{Working_capacity} = 189.033 + 0.061 \times \text{Sa} + 4.318 \times \text{Pv} - 135.846 \times \text{Dc}$$

Table 2 Total uptake (at 65 bar) and working capacity (at a pressure range of 65–5 bar) at temperatures of 240 K, 270 K and 298 K

MOFs	Sa, $\text{m}^2 \text{ g}^{-1}$	Pv, $\text{cm}^3 \text{ g}^{-1}$	Dc, g cm^{-3}	Total uptake, $\text{cm}^3 \text{ g}^{-1}$			Working capacity, $\text{cm}^3 \text{ g}^{-1}$			Ref.
				240 K	270 K	298 K	240 K	270 K	298 K	
NiMOF-74	1350	0.56	1.195	251	232	210	67	89	108	47
UTSA-20	1620	0.66	0.909	319	297	253	129	182	187	47
MOF-505	1661	0.68	0.927	300	270	248	97	121	150	50
PCN-14	2000	0.85	0.829	362	326	277	145	185	189	47
HKUST-1	1850	0.78	0.883	369	341	302	120	190	215	47
NOTT-109	2110	0.85	0.790	362	341	306	138	199	215	50
NU-135	2530	1.02	0.751	387	357	306	188	232	226	54
UTSA-80	2280	1.03	0.694	442	390	336	207	258	251	49
NOTT-101	2805	1.08	0.684	472	414	346	231	276	265	50
UTSA-76	2820	1.09	0.699	491	431	368	240	293	282	55
NOTT-103	2958	1.16	0.643	496	440	367	252	306	285	50
NOTT-102	3342	1.27	0.587	532	477	404	310	354	327	50
NOTT-122a/NU-125	3120	1.29	0.578	519	469	401	296	334	317	56 and 57
NU-800	3149	1.34	0.546	559	452	359	410	370	310	58
ZJU-36	4014	1.60	0.496	617	514	409	458	425	353	59
NU-140	4300	1.97	0.43	728	591	465	551	484	395	60
NU-111	4930	2.09	0.409	856	694	504	653	584	438	47
Al-soc-MOF-1	5585	2.30	0.34	882	712	579	697	632	518	24



$$R^2 = 0.979; \text{MAE} = 12 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 208; \text{RMSE} = 14.41 \text{ cm}^3 \text{ g}^{-1}.$$

At 270 K

$$\text{Total_uptake} = 200.152 + 0.057 \times \text{Sa} + 99.547 \times \text{Pv} - 78.894 \times \text{Dc}$$

$$R^2 = 0.980; \text{MAE} = 15 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 339; \text{RMSE} = 18.40 \text{ cm}^3 \text{ g}^{-1}.$$

$$\text{Working_capacity} = 53.433 + 0.059 \times \text{Sa} + 121.325 \times \text{Pv} - 94.025 \times \text{Dc}$$

$$R^2 = 0.987; \text{MAE} = 14 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 282; \text{RMSE} = 16.81 \text{ cm}^3 \text{ g}^{-1}.$$

At 240 K

$$\text{Total_uptake} = 106.071 + 0.040 \times \text{Sa} + 249.422 \times \text{Pv} - 35.399 \times \text{Dc}$$

$$R^2 = 0.984; \text{MAE} = 18 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 473; \text{RMSE} = 21.75 \text{ cm}^3 \text{ g}^{-1}.$$

$$\text{Working_capacity} = -224.435 + 0.007 \times \text{Sa} + 379.715 \times \text{Pv} + 50.945 \times \text{Dc}$$

$$R^2 = 0.990; \text{MAE} = 19 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 674; \text{RMSE} = 25.97 \text{ cm}^3 \text{ g}^{-1}.$$

The equations developed in this section will be an opportunity to estimate the methane total uptake and working capacity of newly designed MOFs. The values of R^2 , MAE and RMSE show the robustness of the models obtained. The coefficients of determination for the working capacity are: $R^2 = 0.979$ at $T = 298$ K, $R^2 = 0.987$ at $T = 273$ K and $R^2 = 0.990$ at $T = 240$ K. The coefficients of determination for the total uptake are: $R^2 = 0.965$ at $T = 298$ K, $R^2 = 0.980$ at $T = 273$ K and $R^2 = 0.984$ at $T = 240$ K. An interesting trend is observed: the lower the temperature, the higher the R^2 .

Application of multiple linear regression for developing equations from the CoRE MOF database

Multiple linear regression analysis has been employed to develop equations to describe methane working capacities at 35–5.8 bar considering the database obtained from high-throughput GCMC calculations⁶¹ of the CoRE MOF database (11 000 MOFs). The details of the methane sorption simulation *via* GCMC simulations are presented in that work. The CoRE MOF database considered contains a wide range of different kinds of MOFs with different topologies, forms of linkers, metals in nodes, *etc.*, and it is obvious that the values of R^2 , MAE and RMSE will be a bit smaller than in case of studying MOFs with one topology. The equation developed based on only three geometrical descriptors – surface area, pore volume and density of the MOFs – is shown below:

$$\text{Working_capacity (35–5.8 bar)} = 39.989 + 0.026 \times \text{Sa} + 12.789 \times \text{Pv} - 14.862 \times \text{Dc}$$

$$R^2 = 0.899; \text{MAE} = 9.23 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 158.76; \text{RMSE} = 12.60 \text{ cm}^3 \text{ g}^{-1}.$$

A much smaller set of MOFs can be studied for the comparison of the models' performances. The following equation is developed by employing 500 randomly chosen MOFs for training from the CoRE MOF database:

$$\text{Working_capacity_500 MOFs (35–5.8 bar)} = 51.567 + 0.022 \times \text{Sa} + 13.989 \times \text{Pv} - 20.526 \times \text{Dc}$$



$$R^2 = 0.898; \text{MAE} = 9.52 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 182.39; \text{RMSE} = 13.51 \text{ cm}^3 \text{ g}^{-1}.$$

The employment of 500 MOFs for training shows that the R^2 is almost the as that when employing 11 000 MOFs. The MAE and RMSE are a little bit bigger.

Also, the equation developed *via* training with 500 MOFs can be applied to the rest of the CoRE MOF database, treating it as a test set. The following values of the model's characteristics are obtained:

$$R^2 = 0.895; \text{MAE} = 9.69 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 165.29; \text{RMSE} = 12.86 \text{ cm}^3 \text{ g}^{-1}.$$

These results show that the model's characteristics are very close to those obtained *via* the employment of 11 000 MOFs: the R^2 is a bit smaller, while the MAE, MSE and RMSE are a little bit bigger.

The accuracy of the prediction may be further enhanced by implementing in the equation some more geometrical descriptors:⁶¹ void fraction, LCD (largest cavity diameter) and PLD (pore limiting diameter)

$$\text{Working_capacity (35–5.8 bar)} = 36.191 + 0.023 \times \text{Sa} - 3.405 \times \text{Pv} - 14.153 \times \text{Dc} + 35.154 \times \text{Vf} + 0.689 \times \text{LCD} - 0.695 \times \text{PLD}$$

$$R^2 = 0.899; \text{MAE} = 9.26 \text{ cm}^3 \text{ g}^{-1}; \text{MSE} = 159.78; \text{RMSE} = 12.63 \text{ cm}^3 \text{ g}^{-1}.$$

Interestingly, no increase in the accuracy of the model is observed by employing the equation with six descriptors: the R^2 values are the same and the MAE, MSE and RMSE are almost the same. In the case of the equations with three descriptors, these characteristics are even a little bit better.

Conclusions

This work aimed to show that multiple linear regression analysis is a fast and highly efficient approach for revealing the methane total uptake and working capacity of MOFs. Only three variables – geometric descriptors obtained from the crystal structure information: surface area, pore volume and density of the MOFs – need to be employed to develop the equations for the methane total uptake and working capacity values. The analytical equations obtained can predict the methane total and working capacity values with high accuracy employing only these three descriptors. The values of the descriptors can be obtained much faster than the actual GCMC simulations or experimental work for revealing sorption isotherms, employing simulation packages such as Poreblazer or Zeo++, or tools in Material Studio.

A set of equations is developed for predicting the methane total uptake and working capacity for MOFs with the same topology (NbO, in the case studied). The model exhibits very high accuracy. Several equations are developed for the set of benchmark MOFs, which have different topologies, metals in nodes, *etc.* The values of R^2 , MAE and RMSE show the robustness of the models obtained, for example for the working capacity: $R^2 = 0.979$ at 298 K, $R^2 = 0.987$ at 273 K and $R^2 = 0.990$ at 240 K. The GCMC results from the CoRE MOF database are considered for developing equations for predicting the methane working capacity which take into account only three parameters. The $R^2 = 0.899$, MAE = 9.23 cm³ g⁻¹ and RMSE = 12.60 cm³ g⁻¹. The further enhancement of the model by



employing more descriptors does not lead to increase in the accuracy of the model. This is very convenient for both experimentalists or theoreticians to easily obtain the methane total and working capacities *via* employing equations and just having a file of a crystal structure(s) and the values of the three descriptors.

Conflicts of interest

The author declares that there are no conflicts of interest.

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