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Multiscale modelling of CO₂ hydrogenation of TiO₂-supported Ni₈ clusters: on the influence of anatase and rutile polymorphs†

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The selection of TiO_2 phase, whether anatase or rutile, for supporting small Ni clusters significantly influences the activity and selectivity in CO_2 hydrogenation to methane. To model and understand these variances, we developed a hierarchical multiscale catalytic model. Utilizing a hybrid approach combining genetic algorithms and density functional theory, we identified the putative global minimum structures of Ni_8 clusters supported on anatase (Ni_8/TiO_2 -a) and rutile (Ni_8/TiO_2 -r), which are morphologically distinct. Microkinetics simulations based on the energetics derived from DFT calculations over these distinct clusters reveal the mechanism of CO_2 hydrogenation to CO, CH_4 and CH_3OH . On both Ni_8/TiO_2 -a and Ni_8/TiO_2 -r, CH_4 is the main product at low temperature while a shift to CO occurs with increasing temperature. In comparison to Ni_8/TiO_2 -r, Ni_8/TiO_2 -a exhibits a higher activity and keeps a higher selectivity towards CH_4 with increasing temperature. Using a sensitivity analysis, we identify the steps responsible for the observed selectivity difference and rationalize the observed barrier differences for these steps between the different clusters by means of detailed electronic structure analysis.

1. Introduction

In recent decades, the escalating levels of atmospheric carbon dioxide ($\rm CO_2$) contribute significantly to rising global temperatures, sea-level rise, altered weather patterns, and various ecological disruptions. To mitigate these adverse effects and transition towards a more sustainable and carbon-neutral future, innovative approaches and technologies capable of reducing $\rm CO_2$ emissions at scale are required. The Sustainably produced hydrogen, for example from excess wind and solar power, can be utilized to convert $\rm CO_2$ to $\rm CH_4$ in the so-called power-to-gas concept. The An important benefit of $\rm CH_4$ is that existing infrastructure for storage and transport can be repurposed.

For the practical implementation of CO₂ hydrogenation to CH₄, catalysts are essential to ensure both high reaction rates and selectivity towards the desired product. While methanation catalysts have been extensively studied, Ru stands out for its superior performance among investigated transition metals. ^{10,11} However, the widespread industrial application of Ru catalysts

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is hindered by its relatively high cost. In contrast, Co and Ni also demonstrate high conversion rates in CO₂ methanation, with Ni being the preferred choice for industrial applications, as it is the cheaper of the two metals.^{12–14}

The activity of supported transition metal catalysts is affected by many factors, with the size of the nanoparticles being a dominant one, strongly affecting the abundance of specific surface atom arrangements relevant to dissociation and association reactions below 10 nm. 15 The effect of nanoparticle size on the activity and selectivity of CO2 hydrogenation to CO and CH4 remains a topic of intense debate. Two dominant trends can be identified in the literature. Some studies show an increased surface-normalized CO2 conversion with increasing particle size, 16-21 while others find an optimum. 22-24 In a recent study of Simons et al., it was found that Ni-catalyzed CO2 methanation uses two different types of active sites, one for reverse-water-gas-shift (RWGS) reaction yielding intermediary CO and another type of site for CO conversion to methane. While RWGS is structure-independent, the activity of CO methanation shows strong structure-dependence caused by the particle size dictating the abundancy of this latter type of active site.25

In addition to nanoparticle size, the support material can influence the morphology of the nanoparticles. Apart from the wetting properties of the support affecting the nanoparticle, the surface structure of the support also has an epitaxial effect that influences nanoparticle morphology by favoring specific

alignments at the support-nanoparticle interface. ²⁶⁻²⁹ A notable example is found when using TiO2 as a support material, which exists in three primary crystalline forms, being anatase, rutile and brookite. CO2 methanation catalyzed by TiO2-supported nanoparticles show different activity and selectivity trends based on the phase of TiO₂. 30-33 Li et al. showed that for similarly sized Co nanoparticles (~20 nm), the anatase-supported particles mainly produce CO under CO2 hydrogenation conditions, while the rutile-supported counterpart exhibits high methane selectivity.30 Wang et al. reported a similar effect for small Ru nanoparticles (~2-3 nm), where the rutile phase is significantly more active and selective towards CH4 than the anatase phase. This enhanced selectivity is assigned to the formation of a favorable overlayer structure guided by the interfacial compatibility between the RuO2 precursor phase and rutile, prior to reduction. In contrast, on anatase only small nanoparticles are formed.³² Likewise, the works of Lin et al. and Messou et al. observe for similarly sized Ni nanoparticles (~30 nm) an increased activity and selectivity towards CH4 for the rutile phase over the anatase phase in CO2 hydrogenation. The increased activity is assigned to the rutile phase giving rise to Ni nanoparticles that portray facile CO dissociation and H2 activation.31,33

Clearly, the choice of TiO₂ phase, whether anatase or rutile, has a strong impact on the catalytic activity, even when the nanoparticles are roughly the same size. Different support materials, their phases and surface termination determine the metal-support interaction strength and thus modulate particle sizes invoking known structure sensitivity patterns. When nanoparticle sizes remain comparable between different support structures, yet a different kinetic response is observed, this is a strong indicator that the support influences the particle shape. Computational catalysis can aid in understanding these effects, yet the scale of these systems remains still prohibitively large for detailed electronic structure calculations. One way to tackle this is by means of DFT-based force fields, as performed earlier by us for both unsupported Co nanoparticles²⁶ as well as Co nanoparticles on a model support material.³⁴ In this work, rather than producing such a force field, the system is made computationally accessible by focusing on small Ni clusters. Small Ni clusters provide an excellent model system to study active site configurations that are guided by the alignment of the support substructure.

To understand and characterize how support effects can influence the activity and selectivity in CO2 hydrogenation to methane for small clusters, we construct a multiscale model for Ni₈ clusters supported on rutile and anatase. Although experimentally always a range of particle size distributions is observed, these small Ni₈ clusters are representative for particle sizes below 1 nm. By means of a DFT-based genetic algorithm in conjunction with machine learning, we explore the configuration space of TiO2-supported Ni8 clusters and identify the putative global minimum configuration. Next, the kinetic pathways for CO₂ hydrogenation to CH₄ are calculated. By means of microkinetics simulations, we found that Ni₈/ TiO₂-anatase in comparison to Ni₈/TiO₂-rutile exhibits a much

higher activity while also portraying a higher selectivity to CH₄ with increasing temperature. Using a sensitivity analysis, we identified that the preferred manner of C-O bond scission - hydrogen-assisted pathway via HCO* for Ni₈/TiO₂-anatase, while in a direct fashion for Ni₈/TiO₂-rutile - dictates the observed activity and selectivity differences. These differences are caused by the specific topology of the active site dictated by the alignment of Ni atoms with the support structure. By means of a crystal orbital Hamilton population analysis, the difference in barrier for CO dissociation is rationalized. This study adds to our understanding by which mechanism the catalyst support can modulate the catalytic reaction.

2. Methods

2.1 DFT calculations

All density functional theory (DFT) calculations were performed using the Perdew-Burke-Ernzerhof (PBE) exchange-correlation functional35 as implemented in the Vienna ab initio simulation package (VASP) software.36,37 All DFT calculations were conducted with spin-polarization taken into account. The interaction of the core-electrons and nucleus was described with the Projector Augmented Wave (PAW) method. 38-40 The cut-off energy was set to 400 eV. The Brillouin zone was sampled using a 1 × 1 × 1 grid. Gaussian smearing with a width of 0.05 eV determined partial occupancies for each orbital. Ionic convergence was achieved when the forces were smaller than 0.05 eV Å⁻¹ for each atom in each Cartesian direction. A Vander-Waals correction was added to our calculation using the DFT-D3 method with the Becke-Johnson damping function. 41,42 Climbing image nudged elastic band (CI-NEB) was employed to investigate the transition pathway. 43,44 The transition state was optimized using a quasi-Newton algorithm and the optimized geometry was examined by vibrational mode analysis. It was verified that all transition states have a single imaginary mode in the direction of the reaction coordinate. We employed a finite difference approach to construct the Hessian matrix for frequency analysis by perturbing the atomic positions by 0.01 Å in each Cartesian direction. Furthermore, the vibrational mode analysis was used to construct zero-point energy corrections.

2.2 Structural models

For anatase and rutile TiO2, the periodically repeated (101) and (110) surface terminations were employed as supports for Ni₈ clusters, as these surfaces are known to be the most thermodynamically stable for their respective phases. 45,46 Ni₈ clusters deposited on (101) surface of TiO₂ anatase and (110) surface of TiO2 rutile are denoted as Ni8/TiO2-a and Ni8/TiO2r, respectively. We specifically selected Ni₈ clusters because they are large enough to potentially support step-edge configurations, which are known to promote C-O bond scission.47 However, this does not guarantee that these active site patterns are thermodynamically favorable, as the support interface also plays a crucial role. Nevertheless, choosing smaller cluster sizes would a priori prevent studying such sites.

The lattice parameters of TiO2-a and TiO2-r bulks were optimized and found to be 3.816 Å \times 3.816 Å \times 9.539 Å and $4.650 \text{ Å} \times 4.650 \text{ Å} \times 2.966 \text{ Å}$, respectively. These optimized lattice parameters are in good agreement with the values obtained from experimental results. 48,49 For TiO₂-a, a 1 \times 3 (101) surface termination with dimensions of 10.42 $\text{Å} \times 11.46$ Å was constructed. Its slab model hosts three O-Ti-O layers with the bottom layer fixed while the top two layers are allowed to relax.⁵⁰ For Ni₈/TiO₂-r, a 5 \times 2 (110) surface termination with dimensions of 14.85 Å \times 13.18 Å was constructed. The corresponding slab model has four O-Ti-O layers. The bottom layer was fixed while the top three layers were allowed to perturb. To avoid the spurious interaction of neighboring supercells in the z-direction, the TiO2-a and TiO2-r super cells have a vacuum space of at least 15 Å. A depiction of the supercells is given in the ESI† in Fig. S1.

2.3 Genetic algorithm

In order to search for the putative global minimum structure of Ni₈ clusters deposited on the anatase (101) and rutile (110) surface of TiO2, a GA-DFT algorithm based on the approach as described by Hammer et al. was employed.51 In this approach, an ensemble of cluster configurations is procedurally generated and the stability of these clusters on the surface is assessed by DFT calculations. To efficiently probe the configuration space of cluster configurations, a genetic algorithm method is used wherein new cluster configurations are generated by a sequence of operations including translations, rotations, atomic migrations and mixing of clusters. For each generation, at least 12 candidates are generated to form the next generation. To enhance the diversity of the population, approximately 30% to 50% of the structures are mutated. Each cluster is subjected to a geometry optimization in a conventional DFT simulation and based on the energies of the clusters they are ranked in terms of stability. New generations of clusters are derived from an older generation using stability and similarity metrics. This yields a strong (i.e. containing many stable structures) yet sufficiently diverse population between all iterations. The algorithm is considered to be converged when no new more stable configurations are found for a number of generations, typically between 5-10. Details of the GA-DFT procedure can be found in the earlier work of Chang et al.⁵²

To assess the similarity of the clusters and identify common shapes, an unsupervised non-linear dimensionality reduction was conducted via the t-distributed stochastic neighbor embedding (t-SNE) method as implemented in the sklearn Python library. 53,54 The dimensionality reduction is applied to a $N \times N$ square distance metric matrix M with N being the number of clusters. Each element in M corresponds to the minimized Hilbert-Schmidt norm⁵⁵ of the distancedifference matrix between two clusters. The minimized Hilbert-Schmidt norm is constructed by first constructing an atomic distance matrix R for each cluster.

$$\mathbf{R} = \begin{pmatrix} 0 & \dots & r_{ij} \\ \vdots & \ddots & \vdots \\ r_{ii} & \dots & 0 \end{pmatrix}, \tag{1}$$

wherein r_{ij} is the Euclidean distance between atom i and atom j in a cluster. As such, the matrix R is symmetric and has zeros on its diagonal. Given two atomic distance matrices \mathbf{R}_k and \mathbf{R}_l for clusters k and l, a similarity metric S_{kl} can be constructed by evaluating

$$S_{kl} = \sqrt{\sum_{ij} (r_{ij}^{(k)} - r_{ij}^{(l)})^2}.$$
 (2)

Although the distance matrix R is translationally and rotationally invariant, it is not permutationally invariant and as such, the value of S_{kl} depends on the specific indexing of the atoms. Consequently, the value of S_{kl} needs to be minimized by considering all possible permutations of the atomic indices for one of the clusters. Given the small number of atoms in the clusters, it is possible to employ a brute force approach wherein all 8! = 40320 permutations were explicitly considered. The lowest value found, i.e. Skl,min, is then used as the elements to construct M. For the construction of M, we used the in-house developed program Bramble which employs a GPU-accelerated procedure to evaluate all permutations.⁵⁶

2.4 Microkinetics simulations

Microkinetics simulations based on DFT-derived reaction networks were conducted to determine the catalytic performance of Ni₈/TiO₂-a and Ni₈/TiO₂-r for CO₂ hydrogenation. All microkinetics simulations were performed using the in-house developed MKMCXX program. 57,58 For each elementary reaction step in the chemokinetic network as given by

$$\nu_{\rm a}A + \nu_{\rm b}B \stackrel{k^+}{=} \nu_{\rm c}C + \nu_{\rm d}D,$$
 (3)

a corresponding rate expression, i.e. an ordinary differential equation in time, can be constructed by

$$r_{\rm A} = -rac{{
m d}[A]}{{
m d}t} =
u_{
m a} (k^+[A]^{
u_{
m a}}[B]^{
u_{
m b}} - k^-[C]^{
u_{
m c}}[D]^{
u_{
m d}})$$
 (4)

Herein, v_X is the stoichiometric coefficient of component X and k^+ and k^- are the rate constants for the forward and backward reaction, respectively. From harmonic transition state theory, the reaction rate constants are calculated by the Eyring equation

$$k = \frac{k_{\rm B}T}{h} \frac{f_{\rm TS}^{\#}}{f_{\rm IS}} \exp\left(-\frac{\Delta E_{\rm a}}{k_{\rm B}T}\right) \tag{5}$$

wherein h is the Planck constant, ΔE_a the activation energy, k_B the Boltzmann constant, T the temperature, and finally $f_{TS}^{\#}$ and f_{IS} are the partition functions of the transition state and the initial state, respectively.

For the adsorption steps, it is assumed that the adsorbing molecule loses one of the translational degrees of freedom with respect to the initial state. The rate constant for

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adsorption is then determined by the rate of surface impingement of gas-phase molecules for non-activated molecular adsorption and is given by 59

$$k_{\rm ads} = \frac{PA}{\sqrt{2\pi m k_{\rm B} T}},\tag{6}$$

wherein P corresponds to the partial pressure of the adsorbate in the gas phase, A the effective surface area of the adsorption site, and m the mass of the adsorbate.

Considering the reversibility of the adsorption step, the molecule regains all its rotational degrees of freedom (*i.e.* three degrees of freedom for non-linear molecules and two degrees of freedom for linear molecules) and two translational degrees of freedom in the desorption step. Therefore, the desorption rate is given by

$$k_{\text{des}} = \frac{k_{\text{B}}T}{h} \frac{q_{\text{vib,gas}}q_{\text{rot,gas}}q_{\text{tran2D,gas}}}{q_{\text{vib,ads}}} \exp\left(\frac{\Delta E_{\text{ads}}}{k_{\text{B}}T}\right)$$
(7)

wherein $\Delta E_{\rm ads}$ is the adsorption energy. $q_{\rm vib,gas}$, $q_{\rm rot,gas}$ and $q_{\rm tran2D,gas}$ represent the vibrational, rotational and two-dimensional translation partition function of a molecule in gas phases, respectively. $q_{\rm vib,ads}$ refers to the vibrational partition function of the molecule upon adsorption.

In our simulations, the initial gas phase contained a mixture of CO_2 and H_2 in a 1:4 ratio at a total pressure of 1 atm, in line with the conditions used in the experiment.⁶⁰ To identify the elementary reaction steps that control the overall rate of CO_2 consumption, Campbell's degree of rate control analysis was employed.⁶¹

3. Results and discussions

3.1 Ni_8 clusters supported on anatase and rutile TiO_2

To find the most stable structures for $\rm Ni_8$ clusters supported on anatase and rutile $\rm TiO_2$, a GA-DFT algorithm was employed which produced 244 and 104 candidate structures for the anatase and rutile systems, respectively. The candidates were ranked based on the total energy of the system. The 10 most stable structures for anatase and rutile $\rm TiO_2$ are given in Fig. S2 and S4,† respectively. To investigate whether there are multiple cluster configurations that are topologically distinct yet portray a similar stability on the surface, a similarity analysis was conducted by calculating the minimized Hilbert–Schmidt norm between all clusters. Using a non-linear dimensionality reduction based on the t-SNE method, we could classify all clusters into distinct categories as shown in Fig. 1. Representative cluster configurations for each of these groups are shown in Fig. 1 as well.

The most stable Ni cluster on the anatase TiO_2 (101) surface, representative of group 1, adopts a bilayer configuration in which 6 Ni atoms are located in the bottom layer forming two fourfold type of adsorption sites on which the two atoms of the top layer are located. The clusters in groups 2–4 exhibit fewer Ni atoms binding to the O atoms of the support and are higher in energy. In Fig. S3,† the 9 most similar clusters with respect to the most stable cluster are shown. We can readily observe that

these structures are related to the most stable structure either *via* a rotation or *via* a migration of one or two Ni atoms.

On the rutile TiO2 (110) surface, the most stable cluster of Ni₈ also adopts a bilayer configuration. In contrast to the anatase system, the bottom layer has a triangular shape exposing four threefold adsorption sites. The top layer is constructed by the adsorption of two Ni atoms on two of these threefold adsorption sites. The t-SNE manifold learning shows that, for this system, also four distinct groups of clusters are found. The most stable configuration belongs to group 1, group 2 shows a different configuration yet similar to group 1 on anatase TiO₂(101) with 6 atoms in the bottom layer and two atoms in the top layer. In contrast, groups 3 and 4 show a configuration with 5 atoms in the bottom layer and 3 in the top layer. Groups 2, 3 and 4 are, on average, higher in energy than group 1 as they either lack a strong interaction with the support (groups 3 and 4) or have more undercoordinated metal atoms (group 2).

Furthermore, due to known SMSI effects, we also investigated planar Ni_8 clusters that optimize the contact area between the TiO_2 -support and the Ni_8 cluster. The configurations are shown in Fig. S6 in the ESI.† It was found that on both TiO_2 anatase and rutile, a planar Ni_8 cluster is less stable than a non-planar cluster by 1.35 eV and 1.06 eV, respectively. As such, we proceeded with evaluating the elementary reaction steps for CO_2 hydrogenation using non-planar cluster configurations.

3.2 Chemical reactivity of $\rm CO_2$ hydrogenation over $\rm Ni_8/TiO_2$ -a and $\rm Ni_8/TiO_2$ -r

3.2.1 Adsorption of CO_2 and H_2. In Fig. 2, the two most stable cluster configurations for anatase and rutile are shown. To label the different types of active sites involved in the mechanism, we employ the following notations:

- T_i : the top site of Ni_i .
- B_{i-j} : the bridge site located between N_i and Ni_j .
- H_{i-j-k} : the hollow site that comprises Ni_i , Ni_j , and Ni_k .
- $F_{i-j-k-l}$: the four-fold site formed by Ni_i , Ni_j , Ni_k , and Ni_l .

First, the preferred adsorption configurations of CO₂ and H₂ on the various active sites are explored. For H₂, we considered both molecular as well as dissociative adsorption. In Fig. 3 and 4, an overview is given of the different adsorption modes and corresponding adsorption energies of CO2 and H2 on Ni8/TiO2-a and Ni8/TiO2-r, respectively. From the results in Fig. 3 and 4, it can be seen that dissociative H₂ adsorption is more exothermic as compared to molecular adsorption and the H atoms preferentially reside at the metal-support interface. The most stable configurations for H_2 adsorption correspond to adsorption energies of ΔE_{ads} = -1.23 eV and $\Delta E_{ads} = -1.37$ eV for Ni₈/TiO₂-a and Ni₈/TiO₂-r, respectively. In these configurations, H2 is dissociatively adsorbed to form 2H*. This process is activated by 0.11 eV and 0.39 eV for Ni₈/TiO₂-a and Ni₈/TiO₂-r, respectively. These results are similar to H_2 dissociation on a Ni_{13} cluster (ΔE_{act} = 0.21 eV) and Ni/In₂O₃ (ΔE_{act} = 0.22 eV).^{62,63} H spillover is

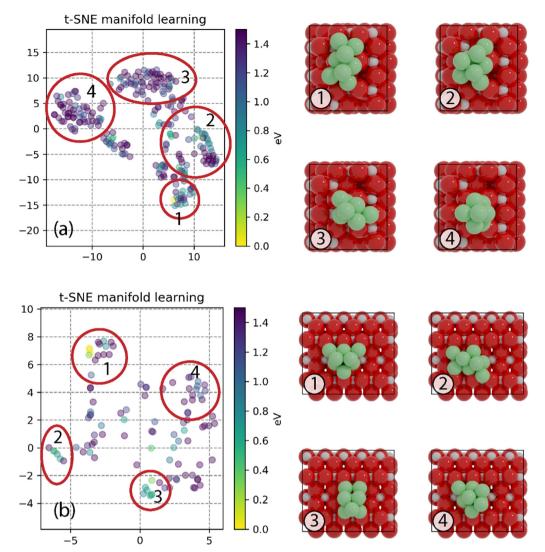


Fig. 1 t-SNE manifold learning of GA-DFT generated structures of Ni₈/TiO₂-a (a) and Ni₈/TiO₂-r (b), with clusters of similar structures encircled and labeled 1-4. Representative structures for each part are displayed on the right of t-SNE figures. Color codes: red: O; light gray: Ti; green: Ni. The energies of all structures relative to the most stable one are shown using a color map. The structure's stability decreases as the color transitions from yellow to purple.

commonly discussed experimentally.⁶⁴ Therefore, H spillover is also considered on these two models. As shown in Fig. S7,† H spillover occurs with activation energies of $\Delta E_{\rm act}$ = 0.89 eV and $\Delta E_{\rm act}$ = 1.09 eV on Ni₈/TiO₂-a and Ni₈/TiO₂-r, respectively.

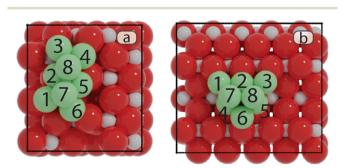


Fig. 2 The most stable models of Ni₈/TiO₂-a (a) and Ni₈/TiO₂-r (b). Color codes: red: O; light gray: Ti; green: Ni. The numbering of Ni atoms corresponds to the active sites as described in the main text.

This step is endothermic with reaction energies of $\Delta E_{\rm R} = 0.67$ eV and $\Delta E_R = 0.50$ eV for Ni₈/TiO₂-a and Ni₈/TiO₂-r, respectively. Given the endothermic nature of the H spillover reaction and the fact that CO2 adsorption takes place on Ni clusters (vide infra), H spillover is not further considered in the evaluation of the reaction mechanism. On Ni₈/TiO₂-a, CO₂ adsorption is preferred at the B₇₋₈ or H₅₋₇₋₈ sites, both sites yielding an adsorption energy of $\Delta E_{\rm ads} = -0.93$ eV. On Ni₈/TiO₂-r, the most stable site for CO₂ adsorption is H₁₋₄₋₇ with an adsorption energy of $\Delta E_{\rm ads} = -0.70$ eV. Based on the preferred adsorption sites of H2 and CO2, we also considered the co-adsorption of CO2 and H2. For Ni8/TiO2-a we find a total adsorption energy of $\Delta E_{\rm ads}$ = -2.39 eV, which is more exothermic than the sum of the individual CO2 and H2 adsorption energies. In a similar fashion, we find for Ni₈/ TiO_2 -r that the co-adsorbed state is more exothermic ($\Delta E_{ads} =$ -2.64 eV) than the sum of the individual adsorption energies. As these co-adsorbed states represent favorable adsorption

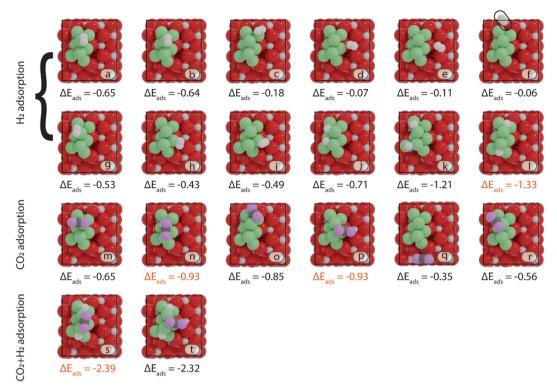


Fig. 3 Configurations of adsorbed H_2 (a–I), CO_2 (m–r) and co-adsorption of CO_2 and H_2 (s and t) on Ni_8/TiO_2 -a. Color scheme: white: H; pink: O in CO₂; gray: C. A black border has been used to indicate the location of H₂ in f. The most stable configuration is indicated by the orange labels.

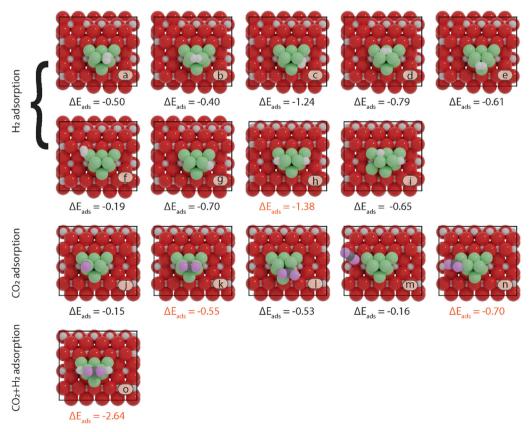


Fig. 4 Configurations of adsorbed H₂ (a-i), CO₂ (j-n) and co-adsorption of CO₂ and H₂ (o) on Ni₈/TiO₂-r. Color scheme: white: H; pink: O in CO₂; gray: C. The most stable configuration is indicated by the orange labels.

modes, we considered these in the further exploration of the reaction pathways.

3.2.2 CO₂ hydrogenation. We computed the reaction energetics of CO2 hydrogenation to CH4, CO, and CH3OH on the most stable models identified in the previous section. The networks of elementary reaction steps and their forward and backward activation energies are displayed in Fig. 5 and 6 for Ni₈/TiO₂-a and Ni₈/TiO₂-r, respectively. In this section, we will explore the pathways related to elementary reaction steps involving CHx and HxCO intermediates in detail. Microkinetic simulations (as discussed later) revealed that the kinetic network associated with HxCO2 intermediates has a minimal impact on the overall reaction mechanism; therefore, this aspect is addressed in Sections S1 and S2 of the ESI.†

3.2.2.1 Ni₈/TiO₂-a

Pathway involving CH_x intermediates. We first discuss the elementary reaction steps among the CH_x intermediates (R1 to

R19; brown section in Fig. 5) with CH₄ and CO as the main products. Initially, the reaction proceeds by adsorption and activation of H₂ (R1) and CO₂ (R2). Direct dissociation of CO^{*}₂ (R3) needs to overcome an activation energy of 0.99 eV and this step is exothermic by 0.81 eV. After CO2 dissociation, the resulting O* is removed from the surface as H₂O via two consecutive hydrogenation steps. The H* located at H₁₋₆₋₇ site reacts with O*, leading to the formation of OH* (R4, $\Delta E_{\rm act}$ = 1.40 eV, $\Delta E_{\rm R}$ = 0.26 eV). After a hydrogen migration step with a minor energy change ($\Delta E_{\rm R} = 0.06$ eV), the OH intermediate can be hydrogenated to H₂O (R5). Including the migration step, this step has activation and reaction energies of 1.39 eV and 1.07 eV, respectively. Finally, the desorption of H₂O (R6) is endothermic by $\Delta E_{\rm des}$ = 0.94 eV, leaving an adsorbed CO* on Ni₈/TiO₂-a. This CO* species can either desorb from the surface (R7) with an energy of 1.93 eV or dissociate to form C* and O* (for H-assisted CO* dissociation, see below). It should be

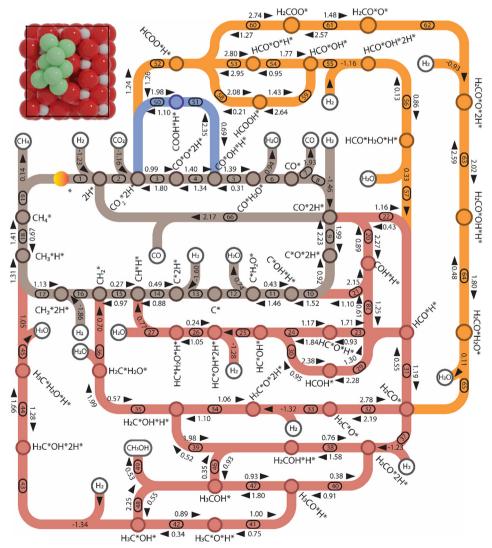


Fig. 5 Reaction network for CO₂ hydrogenation on Ni₈/TiO₂-a. The numbers correspond to the elementary reaction steps in Tables S1 and S2 and Fig. S8-S11.† The activation energy, adsorption energy, and desorption energy are reported in eV and include a zero-point energy correction (colors: brown: CH_x -intermediates pathway; red: H_xCO -intermediates pathway; and orange and blue: H_xCOO -intermediates pathways).

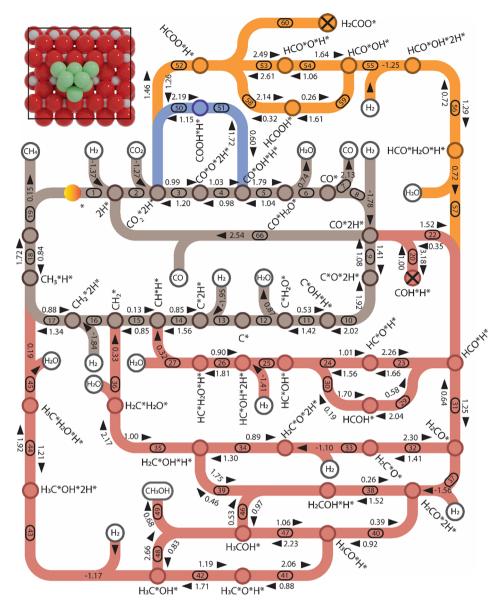


Fig. 6 The forward and backward activation energies in the network of CO_2 hydrogenation in C_1 chemistry for Ni_B - TiO_2 -r (colors: brown: CH_{x^-} intermediates pathway; red: H_xCO -intermediates pathway; and orange and blue: H_xCOO -intermediates pathways). The energy reported here is zero-energy corrected and given by eV. The cross on COH^*H^* and H_2COO^* signifies that their formation is impeded by high activation energies, leading to the exclusion of subsequent reactions. The numbers correspond to the elementary reaction steps in Table S1 and S2 and Fig. S12–S15.† The activation energy, adsorption energy, and desorption energy are reported in eV and include a zero-point energy correction.

emphasized that CO desorption can also occur at the states CO*O*2H*, CO*OH*H* and CO*2H* with desorption energies of 2.18, 2.16 and 2.17 eV, respectively. These pathways are not explicitly shown in Fig. 5, though they are taken into account in the microkinetic modelling (*vide infra*).

The adsorption of $\rm H_2$ on the surface containing CO* (R8) is exothermic by –1.46 eV. The direct dissociation of CO* (R9, $\Delta E_{\rm act} = 1.99$ eV, $\Delta E_{\rm R} = -0.24$ eV) generates an adsorbed C* at $\rm F_{1-2-7-8}$ site and an adsorbed O* at $\rm H_{5-6-7}$ site, which can be hydrogenated to CH₄ and H₂O, respectively. Compared to the direct CO dissociation on Ni₈/In₂O₃ ($\Delta E_{\rm act} = 3.24$ eV), ⁶² which shares a similar Ni₈ cluster morphology as Ni₈/TiO₂ anatase, a lower activation energy is observed on Ni₈/TiO₂ anatase.

This suggests that Ni/TiO $_2$ is a more effective catalyst for CO $_2$ methanation than Ni/In $_2$ O $_3$, the latter mainly producing methanol. In contrast, the work of Sterk $et~al.^{65}$ shows that for the Ni(110) extended surface a relatively low barrier of $\Delta E_{\rm act} = 1.56$ eV is found for CO dissociation. Hydrogenation of O* to OH* (R10) is endothermic by 0.60 eV with an activation energy of 1.52 eV. The OH* reacts with another H* to form an H $_2$ O molecule (R11, $\Delta E_{\rm act} = 1.46$ eV, $\Delta E_{\rm R} = 1.03$ eV), which then desorbs from the surface (R12, $\Delta E_{\rm des} = 0.74$ eV) and leaves an adsorbed C* species. H $_2$ adsorption (R13) provides two H* with an adsorption energy of –1.60 eV. C* is subsequently hydrogenated to CH* (R14, $\Delta E_{\rm act} = 0.88$ eV, $\Delta E_{\rm R} = 0.39$ eV) and CH $_2^*$ (R15, $\Delta E_{\rm act} = 0.97$ eV, $\Delta E_{\rm R} = 0.70$ eV). In

order to form CH₄, one more H₂ molecule adsorbs (R16, $\Delta E_{\rm ads} = -1.86$ eV). The reaction between CH₂* and H* results in the formation of CH₃* (R17, $\Delta E_{\rm act} = 1.31$ eV, $\Delta E_{\rm R} = 0.49$ eV). Next, H* migrates from B₆₋₇ to H₁₋₆₋₇ resulting in a more stable configuration ($\Delta E_{\rm R} = -0.31$ eV). This H* reacts with CH₃* forming CH₄* (R18) with an activation energy of 1.41 eV and this step is endothermic by 0.74 eV. The final step is CH₄ desorption (R19) closing the catalytic cycle.

Pathway involving H_xCO intermediates. For many transition metals, it has been observed that when direct C-O bond scission is associated with a prohibitively high barrier, CO dissociation will occur via COH* or HCO* intermediates.65 These steps correspond to the red section in Fig. 5. Starting at co-adsorbed CO and H₂ (between R8 and R9), CO* can become hydrogenated to COH* (R20) with an activation energy of $\Delta E_{\rm act}$ = 2.27 eV ($\Delta E_{\rm R}$ = 1.38 eV). Its subsequent dissociation (R21, $\Delta E_{\rm act}$ = 1.10 eV, $\Delta E_{\rm R}$ = -1.05 eV) results in the same configuration of C*OH*H* as found in the direct CO* dissociation pathway. The overall activation energy for COH* dissociation is 2.48 eV, which is higher than the activation energy for the direct CO* dissociation. The alternative pathway proceeds via the hydrogenation of CO* to form HCO* (R22), which is endothermic by 1.06 eV and has an activation energy of 1.16 eV. Next, the H* located at H₃₋₄₋₈ migrates to a more stable site (B_{6-7}) with an exothermic reaction energy of 0.33 eV. HCO* dissociation generates an adsorbed CH* and O* (R23, $\Delta E_{\rm act}$ = 0.93 eV, $\Delta E_{\rm R}$ = -0.79 eV). The overall activation energy for the HCO* formation and dissociation is 1.66 eV, lower than the overall barriers found for direct CO* dissociation and COH* pathways, corresponding to 1.99 and 2.48, respectively. The overall activation energy of 1.66 eV lies in between the values found for Ni₈/In₂O₃ (1.80 eV)⁶² and for a stepped Ni(110)⁶⁵ surface (1.21 eV).

After HCO* dissociation, the O* reacts with the remaining H* forming OH* (R24). The activation energy and reaction energy for OH* formation are $\Delta E_{\rm act} = 1.84$ eV and $\Delta E_{\rm R} = 0.67$ eV, respectively, including the migration of H* and OH*. H₂ adsorption provides two H* located at H₁₋₆₋₇ and H₃₋₄₋₈ (R25, $\Delta E_{\rm ads} = -1.28$ eV). The OH* then is hydrogenated to H₂O* (R26, $\Delta E_{\rm act} = 1.05$ eV, $\Delta E_{\rm R} = 0.81$ eV), which desorbs from the surface (R27) and generates the same configuration of CH*H* as found in the direct CO dissociation pathway.

Alternatively, HCO* can be hydrogenated to form HCOH* (R29, $\Delta E_{\rm act}$ = 2.28 eV, $\Delta E_{\rm R}$ = 0.99 eV), which can alternatively be obtained through COH* hydrogenation (R28, $\Delta E_{\rm act}$ = 1.25 eV, $\Delta E_{\rm R}$ = 0.64 eV). HCOH* dissociation yields HC* and OH* (R30) with an activation energy of 0.95 eV and a reaction energy of -1.43 eV. The overall activation energies of HCOH* dissociation *via* COH* and HCO* are 2.97 eV and 2.98 eV, respectively. Both these pathways are higher in energy than the overall activation energy of HCO* dissociation, implying that the HCOH* dissociation pathway is unlikely to occur.

Another mode of H-assisted CO dissociation proceeds via the hydrogenation of HCO* to form H_2CO * which can subsequently dissociate (R31 and R32). These two steps require activation energies of 1.19 eV and 2.19 eV, respectively. The corresponding reaction energies are 0.63 eV and -0.60 eV.

The overall activation energy from CO*2H* to H_2 C*O* is 3.52 eV, implying that this pathway is likely not the most favorable pathway. H_2 adsorption (R33, $\Delta E_{\rm ads} = -1.32$ eV) provides two H* to remove the O* through the formation of H_2 O. The reaction starts with the interaction of O* and H* (R34, $\Delta E_{\rm act} = 1.10$ eV, $\Delta E_{\rm R} = 0.04$ eV), leading to the formation of OH* which can be further hydrogenated to H_2 O* (R35, $\Delta E_{\rm act} = 1.99$ eV, $\Delta E_{\rm R} = 1.42$ eV). Finally, H_2 O desorbs from the catalyst surface (R36, $\Delta E_{\rm des} = 0.70$ eV), leaving behind CH*2 as an adsorbate on the catalyst surface and linking back to the CH*x-intermediates section of the kinetic network.

CH₃OH formation can proceed via twofold hydrogenation of H₂CO*. Two H* are supplied by the adsorption of H₂ (R37, $\Delta E_{\rm ads} = -1.23$ eV) after which H₂CO* can be hydrogenated to form H_3CO^* (R40, $\Delta E_{act} = 0.91$ eV, $\Delta E_R = 0.53$ eV). The H_3CO^* intermediate can be further hydrogenated to form adsorbed CH₃OH (R47, ΔE_{act} = 1.80 eV, ΔE_{R} = 0.87 eV) or dissociate into H_3C^* and O^* (R41, $\Delta E_{act} = 0.75$ eV, $\Delta E_R = -0.25$ eV), the latter being clearly more favorable. The dissociated O* combines with the H* forming OH* (R42) with an activation energy of 0.34 eV. Alternatively, this state can also be obtained via H_3COH^* dissociation (R48, $\Delta E_{act} = 0.55$ eV, $\Delta E_R = -1.70$ eV). H₂ adsorption on the surface containing CH₃ and OH* (R43) is exothermic by 1.34 eV. The resulting H* atoms can hydrogenate OH* forming H₂O (R44, ΔE_{act} = 1.66 eV, ΔE_{R} = 0.38 eV) which can desorb from the surface with a desorption energy of 1.05 eV (R45) leaving CH3 and H*.

The last branch in the H_xCO^* section of the kinetic network involves the conversion of the O-terminated H_2CO^* intermediate. H_2CO^* can be hydrogenated to form H_2COH^* (R38, $\Delta E_{\rm act} = 1.58$ eV, $\Delta E_{\rm R} = 0.82$ eV) which in turn can dissociate into H_2C^* and OH^* (R39) with an activation energy of 0.52 eV. This step is exothermic by 1.46 eV. Alternatively, H_2COH^* is hydrogenated to H_3COH^* (R46), which is associated with an activation energy of 0.93 eV and an endothermic reaction energy of 0.58 eV.

3.2.2.2 Ni₈/TiO₂-r

Pathway involving CH_x intermediates. The brown section in Fig. 6 corresponds to the elementary reaction steps among the CH_x intermediates over Ni₈/TiO₂-r. After adsorption of H₂ (R1) and CO₂ (R2), direct dissociation of CO₂ generates adsorbed CO* and O* (R3, $\Delta E_{\rm act}$ = 0.99 eV, $\Delta E_{\rm R}$ = -0.21 eV). The dissociated O* atom is removed by H* through the formation and desorption of H2O. The formation of OH* (R4), including a migration of O* from H_{2-7-8} to H_{2-3-8} , requires and activation energy of 1.03 eV and is endothermic by 0.25 eV. To facilitate the formation of H₂O, the remaining H* needs to migrate to the H₂₋₃₋₈ site to be close to the OH* ($\Delta E_{\rm R}$ = 0.54 eV). The activation energy and reaction energy for H₂O* formation (R5) are 1.25 eV and 0.21 eV, respectively. Finally, the desorption of H_2O (R6) is endothermic by $\Delta E_{des} =$ 0.74 eV, leaving an adsorbed CO* on Ni₈/TiO₂-r. This remaining CO* species can either desorb from the surface (R7) with a desorption energy of $\Delta E_{\text{des}} = 2.13$ eV or dissociate to form C* and O*. Similar to the Ni₈/TiO₂-a system, CO desorption can also occur at the states CO*O*2H*,

CO*OH*H* and CO*2H* with desorption energies of 2.11, 2.23 and 2.54 eV, respectively. These pathways are not explicitly shown in Fig. 6, though they are taken into account in the microkinetic modelling (vide infra).

The adsorption of H₂ on the surface containing CO* (R8) is exothermic by 1.78 eV. It is important to note that CO can desorb from CO*2H*, generating 2H* species (R66, $\Delta E_{\rm des}$ = 2.54 eV), which should be considered as a part of the rWGS cycle. A relatively low activation energy of 1.41 eV is required for direct CO* dissociation (R9, $\Delta E_{\rm R}$ = 0.33 eV). The dissociated O* fragment is two-fold hydrogenated to form H_2O . After the formation of OH* (R10, $\Delta E_{act} = 2.02$ eV, $\Delta E_R =$ 0.80 eV), the OH* migrates from H_{2-7-8} to B_{7-8} ($\Delta E_R = -0.70$ eV). Subsequently the OH* reacts with the remaining H* forming H₂O* (R11, $\Delta E_{\rm act}$ = 1.42 eV, $\Delta E_{\rm R}$ = 0.89 eV). After the desorption of H₂O (R12, $\Delta E_{\rm des}$ = 0.87 eV), the C* undergoes four consecutive hydrogenation steps yielding CH₄. H₂ adsorption (R13, $\Delta E_{\rm ads} = -1.95$ eV) provides two H* for the hydrogenation of C* to CH* (R14, $\Delta E_{\rm act}$ = 1.56 eV, $\Delta E_{\rm R}$ = 0.71 eV) and CH₂* (R15, $\Delta E_{\rm act}$ = 0.85 eV, $\Delta E_{\rm R}$ = 0.75 eV). CH₂* will be hydrogenated to CH3 and CH4 by the presence of two H* (R16, $\Delta E_{\rm ads} = -1.84$ eV). CH₃ formation (R17) is endothermic by 0.47 eV overcoming an activation energy of 1.34 eV. CH*3 migration from T_{6-7-8} to B_{7-8} ($\Delta E_R = 0.02$ eV) is followed by the formation of CH₄. The activation energy and reaction energy for CH₄ formation (R18) are 1.72 eV and 0.86 eV, respectively. Once CH₄ is formed, it desorbs from the catalyst (R19, $\Delta E_{\rm des} = 0.15 \text{ eV}$).

Pathway involving H_xCO intermediates. In the red section of Fig. 6, the elementary reaction steps involving H_xCO species are shown. Part of this network is comprised of the H-assisted CO dissociation. Due to the high activation energy required to form COH* formation (R20, ΔE_{act} = 3.18 eV), we did not proceed with the calculation of the subsequent COH* dissociation or COH* hydrogenation to HCOH*. The alternative route for CO* hydrogenation by C-H bond formation leading to HCO* (R22) has an activation energy of 1.52 eV and is endothermic by 1.17 eV. Subsequent dissociation of HCO* (R23) results in the formation of CH* located at H_{6-7-8} and O^* located at H_{1-4-7} . The activation energy and reaction energy associated with the dissociation of HCO* are 1.66 eV and -0.60 eV, respectively. Due to the large distance between O* and H*, H* needs to migrate to H_{1-2-7} site first ($\Delta E_R = 0.35$ eV). Formation of OH* (R24) requires an activation energy of 1.21 eV, accompanied by a reaction energy of 0.20 eV. H2 adsorption (R25) provides H* to hydrogenate the OH* to H2O* and is associated with an adsorption energy of -1.41 eV. OH* reacts with H* located at H_{2-7-8} forming H_2O (R26, $\Delta E_{act} = 1.81$ eV, $\Delta E_R = 0.91$ eV), which desorbs generating CH*H* (R27, $\Delta E_{des} = 0.32$ eV), linking back to the CH_x-intermediates section. HCO* can be hydrogenated to HCOH* (R29) by overcoming an activation energy of 2.04 eV. The formation of HCOH* is endothermic by 1.46 eV. HCOH* can be dissociated into CH* and OH* (R30) with an activation energy of $\Delta E_{act} = 0.19$ eV and a reaction energy of $\Delta E_{\rm R}$ = -1.51 eV.

HCO* can undergo hydrogenation to form H₂CO* (R31, $\Delta E_{\rm act}$ = 1.25 eV, $\Delta E_{\rm R}$ = 0.61 eV), which then dissociates into H₂C* and O* by overcoming an activation energy barrier of 1.41 eV (R32). The dissociation of H₂CO* is exothermic by 0.89 eV. The O* species is subsequently hydrogenated to H₂O*. The adsorption of H₂ on the surface containing H₂C* and O* is exothermic by 1.10 eV (R33). The initial hydrogenation of O* leads to the formation of OH* (R34), involving an activation energy of 1.30 eV and a reaction energy of 0.40 eV. The migration of H* occurs to react with OH* and form H_2O ($\Delta E_R = 0.52$ eV). Subsequently, the formation of H₂O (R35) is endothermic by 0.65 eV, requiring an activation energy of 1.65 eV. Finally, H2O desorbs into the gas phase (R36) with a reaction energy of 0.33 eV and leaving an adsorbed CH₂ species on the surface. The subsequent hydrogenation of CH₂ to CH₄ has been discussed in the CH_x intermediates pathway (vide supra).

The adsorption of H₂ on the surface containing H₂CO* provides two H* species, which are subsequently utilized for the hydrogenation of H2CO*. This adsorption process is exothermic by 1.56 eV (R37). Hydrogenation of H₂CO* can occur either via hydrogenation at the O-terminus or at the Cterminus, resulting in the formation of H_2COH^* (R38, ΔE_{act} = 1.52 eV, $\Delta E_{\rm R}$ = 1.27 eV) or H₃CO* (R40, $\Delta E_{\rm act}$ = 0.92 eV, $\Delta E_{\rm R}$ = 0.53 eV), respectively. The dissociation of H₂COH* gives rise to H₂C*OH*H* (R39, $\Delta E_{\rm act}$ = 0.46 eV, $\Delta E_{\rm R}$ = -1.29 eV), which serves as an intermediate in the H₂CO* dissociation pathway. H₃CO* resulting from H₂CO* hydrogenation can either undergo another hydrogenation step to form H₃COH* (R47) or dissociate into H₃C* and O* (R41). The dissociation of H₃CO* is more favorable, exhibiting an activation energy of $\Delta E_{\rm act}$ = 0.88 eV and is exothermic by $\Delta E_{\rm R}$ = -1.17 eV. In comparison, its hydrogenation has an activation energy of $\Delta E_{\rm act}$ = 2.23 eV and a reaction energy of $\Delta E_{\rm R}$ = 1.18 eV. Upon the dissociation of H₃CO*, the O* reacts with the remaining H* forming OH* (R42, $\Delta E_{\rm act}$ = 1.71 eV, $\Delta E_{\rm R}$ = 0.52 eV). This configuration can alternatively be obtained through the dissociation of the C-O bond in H_3COH^* (R48, $\Delta E_{act} = 0.83$ eV, $\Delta E_{\rm R}$ = -1.83 eV). The OH* is hydrogenated to H₂O* in the presence of H* (R44, $\Delta E_{\rm act}$ = 1.92 eV, $\Delta E_{\rm R}$ = 1.21 eV). The H* is provided by the adsorption of H2 (R43), which is exothermic by 1.17 eV. Finally, H2O desorbs from the surface with a desorption energy of 0.19 eV (R45). On the surface, there exist a CH3 species along with a remaining H* species, and the reaction between these two entities has been previously described within the context of the CH*x intermediates pathway. Finally, hydrogenation of H2COH* leads to the formation of H₃COH* with an activation energy of 0.97 eV and a reaction energy of 0.44 eV (R46), which can desorb from the surface (R49, $\Delta E_{\text{des}} = 0.68 \text{ eV}$).

3.2.2.3 Comparison of reaction networks. Overall, our investigations on both Ni₈/TiO₂-a and Ni₈/TiO₂-r surfaces indicate that the direct dissociation of CO2 is favored over H-assisted CO₂ dissociation. The corresponding reaction energy diagrams for this pathway is shown in Fig. S16.† This finding aligns with the observations made by Zhang et al.,

who conducted DFT calculations on Ni₄/CeO₂ (111) and reported activation energies of 2.55 eV for HCOO* formation, 2.80 eV for COOH* formation, and 1.60 eV for CO2 direct dissociation.66

The activation energy for the direct dissociation of CO* on Ni₈/TiO₂-a is 1.88 eV. In comparison, the overall activation energy for HCO* formation and dissociation is 1.66 eV whereas the overall activation energy for H₂CO* formation via $CO^*2H^* \rightarrow HCO^*H^* \rightarrow H_2CO^*$ is 1.92 eV. Based on these values, the H-assisted CO* dissociation via HCO* is energetically the most favorable pathway. For Ni₈/TiO₂-r, it was found that direct dissociation of CO* requires an activation energy of 1.41 eV. In comparison, the overall activation energy for HCO* formation and dissociation is 2.83 eV while the overall activation energy for H₂CO* formation is 2.42 eV. Based on these numbers, direct CO* dissociation is energetically the most likely pathway over Ni₈/ TiO₂-r.

Finally, comparing Ni₈/TiO₂-r to Ni₈/TiO₂-a, the former exhibits a lower activation energy for the direct dissociation of CO*, but the subsequent hydrogenation steps are associated with higher barriers. For example, the overall activation energy for CH₂* hydrogenation to CH₄ on Ni₈/TiO₂-a and Ni₈/TiO₂-r are 1.59 eV and 2.18 eV, respectively. Nevertheless, assessment of the most facile pathways purely based on the DFT energetics remains in absence of the surface coverages limited and microkinetics simulations are conducted to further study the kinetic behavior of these systems.

3.3 Microkinetics simulations

Microkinetics simulations are conducted to predict the catalytic performance of Ni₈/TiO₂-a and Ni₈/TiO₂-r for CO₂ hydrogenation. The activation energies and pre-exponential factors as determined by DFT were employed for these microkinetics simulations.

Fig. 7 depicts the reaction rate and product distribution for Ni₈/TiO₂-a and Ni₈/TiO₂-r. Ni₈/TiO₂-a exhibits a significantly higher CO2 conversion rate than Ni₈/TiO2-r. These turn-overfrequencies are lower than those observed by Liu et al., who report a TOF = 2.14×10^{-3} for Ni nanoparticles of 2.2 nm at a temperature of T = 200 °C. Abir et al. reported a TOF = 2 × 10^{-2} for 2.9 nm particles at T = 350 °C.⁶⁸ In both studies, a mixed anatase/rutile support was used. In contrast, Li et al. report a TOF = 5.1×10^{1} s⁻¹ for 1 nm particles supported on TiO_2 -anatase at T = 500 °C.⁶⁹ These latter results align well to our results found for Ni₈/TiO₂-a. At low temperature, both surface models produce mainly CH₄, while the selectivity to CO increases with temperature at the expensive of the CH₄ selectivity. The selectivity towards CH3OH is negligible at all temperatures considered. At a temperature of 350 K, Ni₈/TiO₂-a only produces CH₄, while the CH₄ selectivity for Ni₈/TiO₂-r is 85%.

To determine the dominant pathway for CO₂ hydrogenation within the chemokinetic network of Ni₈/TiO₂-a and Ni₈/TiO₂-r, a reaction pathway analysis is conducted. Fig. S17 and S18† provide the molar rate fluxes for Ni_8/TiO_2 -a and Ni_8/TiO_2 -r at T =600 K. The dominant reaction pathways for product formation at this temperature are indicated in Fig. 8. For both models, direct dissociation of CO2 is preferred over H-assisted CO2 dissociation. The manner of CO dissociation differs between Ni₈/TiO₂-a and Ni₈/TiO₂-r. On Ni₈/TiO₂-a, the former favors H-assisted CO dissociation while the latter favors direct CO* dissociation.

To determine which steps control the overall activity and selectivity, DRC and DSC analyses (with respect to CO2 consumption) are conducted. Fig. 9a shows that at low temperature, the desorption of H₂O (R6 in Fig. 5) is the ratedetermining step on Ni₈/TiO₂-a. The dominant species on the surface is CO*O*2H* (Fig. 9b). This observation can be attributed to the fact that the elementary reactions R4, R5, and R6 in Fig. 5 are endothermic. As such, CO*O*2H* is the state lowest in energy prior to the rate-determining step R6 which consequently becomes the most abundant state under these conditions. From Fig. 9c, we can see that the apparent activation energy is around 200 kJ mol⁻¹ at low temperature and decreases with increasing temperature. This result can be rationalized from Fig. 9g which shows the potential energy diagram for CH4 formation via the HCO* dissociation pathway. The dominant intermediary state is highlighted in

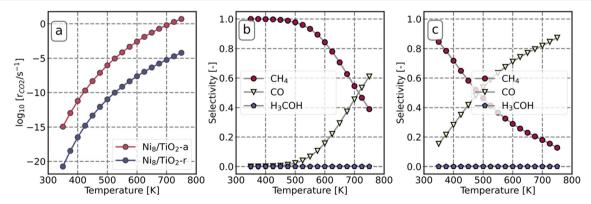


Fig. 7 Reaction rate of CO₂ as a function of temperature (a). The selectivity of CO, CH₄ and H₃COH as a function of temperature on Ni₈/TiO₂-a (b) and Ni_8/TiO_2 -r (c).

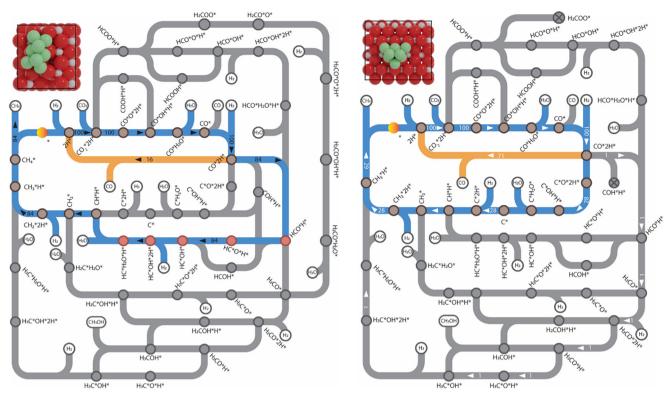


Fig. 8 Preferred pathways for CO₂ hydrogenation on Ni₈/TiO₂-a (left) and Ni₈/TiO₂-r (right). The production of CO and CH₄ is represented by the yellow and blue paths, respectively. All values are normalized with respect to the rate of adsorbed CO2 and are given in percentages (%).

red and the overall barrier for H2O desorption (the ratedetermining step) with respect to this state is determined to be 2.08 eV, which is in agreement with the apparent activation energy. The reaction orders are in line with this observation. Since the dominant CO*O*2H* state already has two hydrogen atoms present, no further hydrogen is necessary to proceed towards the rate-determining step and consequently the reaction order in H2 (Fig. 9c) is observed to zero. Likewise, since the dominant state already represents the fragments of CO2 dissociation, a reaction order of 0 in CO_2 is found.

At temperatures between T = 500 K and T = 650 K, H_2O desorption becomes less rate-limiting to the rate of CO₂ consumption while HCO*H* ≠ HC*O*H* (R23) and CH*3 hydrogenation (R18) becomes more rate-limiting. Simultaneously, it is observed that CO desorption (R66) becomes rate-inhibiting. Due to the increase in temperature, there is more thermal energy available to overcome the H2O desorption barrier resulting in barriers further down the kinetic pathway to become rate-limiting. Since CO desorption (R66) prevents the formation of CH₄ which is still the dominant product under these conditions, this step is rateinhibiting. Further increasing the temperature above T = 650K results in further decreasing the degree of rate control of the H₂O desorption reaction. Simultaneously, HCO*H* ≠ HC*O*H* (R23) becomes rate-inhibiting, whereas CH* hydrogenation (R18) and CO desorption (R66) become ratelimiting. These changes reflect the change in selectivity from

CH₄ to CO. At elevated temperature, the dominant pathway switches from CH₄ production via the HCO* intermediate to a rWGS pathway via R66. Since H2O desorption is a step in the kinetic network for both CO as well as CH₄ production, this step remains rate-limiting to some extent. CH3 hydrogenation is also still a rate-limiting step as even at elevated temperature there remains a significant selectivity towards CH₄. Nevertheless, the rate of CO₂ consumption for CH₄ production is lower than for CO and a change in selectivity towards CH4 by lowering the barrier for HCO*H* ≠ HC*O*H* would result in a decreased overall activity, explaining why this step becomes rate-inhibiting at elevated temperature. The DSC analysis as shown in Fig. S19† further reflects upon this. From this figure, it can be seen that HCO*H* ≠ HC*O*H* and CO* desorption control the selectivity between CH4 and CO. The apparent activation energy and reaction orders change accordingly as a function of temperature. With increasing temperature, the catalyst tends to reside in states further down the kinetic pathway with respect to CO*O*2H*, specifically CO*OH*H*, CO*2H*, C*O*2H*, C*2H* and CH*2H*. From Fig. 9f it can be readily seen that these states are all higher in energy with respect to CO*O*2H*. With respect to the barrier of the dominant ratelimiting step for these intermediates, i.e. either CH*3 hydrogenation or CO* desorption, the energy difference is somewhat smaller than between CO*O*2H* and the barrier for H₂O* desorption. Since all these intermediary species already contain fragments arising from CO₂* adsorption, the

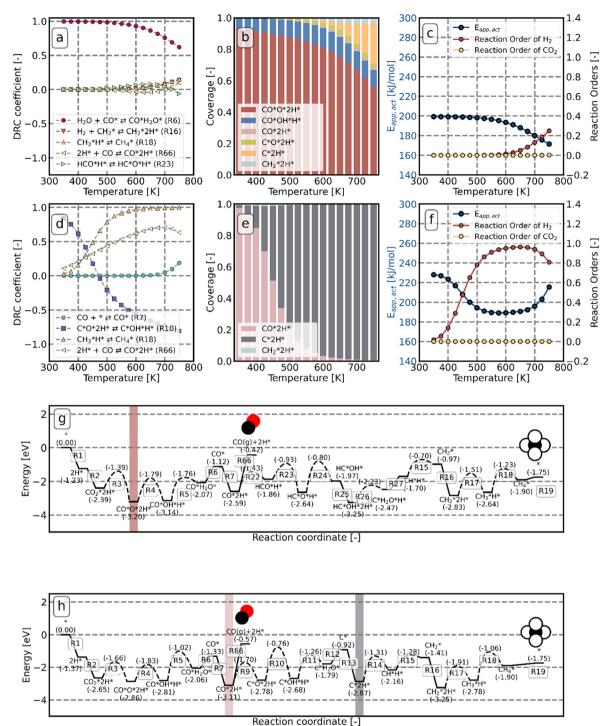


Fig. 9 Degree of rate-control coefficient with respect to CO₂ consumption (a and d), the steady state of surface coverage (b and e), the apparent activation (c and f), the reaction orders of CO2 and H2 (c and f) as a function of temperature. Ni₈/TiO2-a: a-c; Ni₈/TiO2-r: d-f. The potential energy diagram of CO₂ methanation on Ni₈/TiO₂-a (g) and Ni₈/TiO₂-r (h). In figures (g) and (h), the predominant species are accentuated using consistent color coding in the coverage plots.

reaction order in CO₂ remains zero. In contrast, with the exception of CH22H*, all other abundant intermediary states require the adsorption of another H2 molecule in order to proceed to the rate-limiting step of CH* hydrogenation. Consequently, the increased reaction order in H2 reflects the decrease in surface abundance of CO*O*2H* in favor of a number of intermediates that are precursor species towards CH₄ formation that requires the adsorption of H₂ to produce CH_4 .

In Fig. 9d, the DRC analysis for Ni₈/TiO₂-r is shown. At low temperatures, the reaction is mainly controlled by the rate of C*O*2H* ≠ C*OH*H* (R10) and CO*2H* is the most

abundant cluster configuration. The desorption of CO requires 2.54 eV, whereas the activation energy between CO*2H* and R10 is 2.35 eV. At low temperature CH₄ formation is preferred, yet the selectivity towards CH₄ rapidly decreases in favor of CO with increasing temperature as desorption rates increase more rapidly with increasing temperature in comparison to surface reactions. With increasing temperature, the degree of rate-control of step R10 decreases in favor of CO* desorption (R66) and CH3 hydrogenation (R18) becoming rate-limiting steps. A further increase in temperature results in C*O*2H* ≠ C*OH*H* becoming rate-inhibiting while the degree of rate-control for CO* desorption and CH₃ hydrogenation increase further. From Fig. 9e, it is found that CO*2H is the dominant surface state at the low temperature regime whereas with increase in temperature C*2H* becomes the most abundant surface state. The change in surface coverage reflects the degree of rate-controlling, the state lowest in energy prior to the barrier of this step corresponds to CO*2H*. When this step is no longer rate-limiting due to the increase in temperature, the state C*2H* is the next state lowest in energy prior to one of the rate-limiting steps (i.e. R18 and R66).

The apparent activation energy and the reaction orders as shown in Fig. 9f are in line with these trends. At low temperature, a value of 230 kJ mol⁻¹ is found, corresponding to the difference in energy between the CO*2H state (Fig. 9h, highlighted in pink) and the height of the transition state for C*O*2H hydrogenation. With increasing temperature, the system spends more time in the C*2H* state which lies higher in energy. Consequently, the apparent activation energy decreases. In contrast to the low temperature situation, a facile quantitative comparison between the energy levels of the states in the potential energy diagram and the apparent activation energy is not possible for the high temperature situation as no single elementary reaction step is predominantly rate-controlling. The increase in the apparent activation energy for T > 700 K is caused by the deposition of carbonaceous species leading to catalyst deactivation. The observation that C*O*2H* hydrogenation is strongly rate-inhibiting is in line with this observation. As this step becomes more facile, O* that could otherwise be used to recombine with C* to form CO* which can desorb from the surface, is now removed as H2O. In absence of O* and with C* + 2H* being very stable on the surface, further progression towards CH4 is prevented. The branch in the kinetic network via R9-R13 effectively leads to a dead state of the catalyst. Finally, Fig. 9f shows that the reaction order in CO₂ remains close to zero, irrespective of temperature whereas the reaction order in H2 increases as a function of temperature. Since both the CO*2H* intermediate and the C*2H* intermediates already contain the dissociation fragments of CO2 necessary for the rate-limiting steps to proceed, an increase or decrease in the partial pressure of CO₂ will not affect the overall rate. In contrast, in the high temperature regime the dominant state lacks 2H* species for

the CH₃* + H* reaction to proceed. The reaction order in H₂ therefore reflects the extent to which this pathway controls the overall reaction rate. At temperatures T > 700 K, we however observe that the reaction order in H2 slightly decreases. Here, additional H* is detrimental to the activity of the catalyst as it leads to further O* removal and thus the formation of strongly bound C*.

Conclusively, the lower reactivity observed for the Ni₈/ TiO2-r system in comparison to Ni8/TiO2-a is caused by the presence of a relative facile direct CO dissociation. The low barrier for CO dissociation coincides with C* being strongly bound to the catalyst leading to catalyst deactivation. In contrast, for Ni₈/TiO₂-a, direct CO dissociation is difficult, and a H-assisted pathway is more facile. This is already indicative for C* being less strongly bound to the catalyst benefiting its activity. These results are according to the Sabatier principle which shows that although strong adsorption leads to facile activation of the adsorbates, it prevents the desorption of the products, poisoning the catalyst.

As the utilization of the PBE functional commonly leads to an overestimation of the binding energy of CO,70-72 we need to critically assess its effect. As such, additional microkinetic simulations were conducted wherein simultaneously the CO and CO₂ adsorption energy were decreased in a range of 0.0 to 0.3 eV on both Ni₈/TiO₂-a and Ni₈/TiO₂-r models, ensuring that this modification does not affect the overall thermodynamics of the reaction. The resulting reaction rates of CO₂ and selectivity were analyzed and summarized in Fig. S26 and S27.† Decreasing the CO adsorption energy on both Ni₈/TiO₂-a and Ni₈/TiO₂-r catalysts results in an increase in the CO selectivity. For these two surfaces, CO becomes the main product when the correction of CO adsorption energy was set to 0.3 eV at 600 K.

Although we established that H-spillover is associated with relatively high barriers, we nevertheless explored the effect of an enhanced H* coverage on the Ni8-clusters. This analysis was however limited to CO and HCO dissociation and HCO formation as these steps were found to affect the selectivity of the reaction (Fig. S19†). As we determined H-spillover to be difficult, thus assuming that accumulation of additional H* species on the clusters would proceed via adsorption from the gas phase, we furthermore calculated the adsorption energy of H₂ as function of the H* coverage. The results are shown in Tables S3-S5 in the ESI.† From Tables S3 and S4,† it can be seen that on Ni₈/TiO₂-anatase, the overall activation energies for HCO* formation and dissociation are always higher than the activation energies for direct dissociation of CO*. Conversely, on the Ni₈/TiO₂ rutile surface, the direct CO* dissociation exhibits a lower activation energy as compared to the HCO* formation and dissociation. Therefore, the conclusion that Ni₈/ TiO2 anatase predominantly follows the HCO* pathway while Ni₈/TiO₂-rutile favors the direct CO* dissociation pathway remains valid, irrespective of the H* coverage. Furthermore, from Table S5† it can be observed that additional H* accumulation is associated with a significantly decreased

adsorption energy. Given the loss of entropy of H2 upon adsorption, we estimate, especially at higher temperature, that the presence of more than two H* species, in addition to H_xCO, on the Ni₈ clusters is highly unlikely.

From these additional simulations we can conclude that the Ni₈ clusters have a vastly lower activity as compared to experiment, 67,68 even when taking potential effects of overbinding and H-accumulation into account. Despite that Ni₈/TiO₂-r allows for a direct CO dissociation, it results in the formation of a very stable C* species effectively poisoning the catalyst surface. This poisoning condition is less severe on Ni₈/TiO₂-a, yet compared to extended Ni surfaces, also here much higher adsorption energies are observed for the reaction intermediates. We assign the increased adsorption strength of CO* and C* to the presence of coordinatively undersaturated Ni atoms in these clusters, which due to the specific alignment of the Ni atoms with the support, lead to much stronger adsorption energies for Ni₈/TiO₂-rutile as compared to Ni₈/TiO₂-anatase.

3.4 Electronic structure analysis

Microkinetic simulations show that for both Ni₈/TiO₂-a as well as Ni₈/TiO₂-r the initial C-O bond scission in CO₂ proceeds in a direct fashion. After removal of the dissociated O* fragment as H2O, the remaining CO* fragment needs to dissociate as well for CH₄ formation. For this step, the two models differ in the preferred pathway as shown in Fig. 8. For Ni₈/TiO₂-a, C-O bond scission proceeds in a H-assisted fashion via an HCO* intermediate, whereas for Ni₈/TiO₂-r it proceeds in a direct fashion. This observation can be readily explained based on the activation energies. The activation energy of CO direct dissociation for Ni₈/TiO₂-r is 1.41 eV, whereas for Ni₈/TiO₂-a a higher activation energy of 1.99 eV is found. The barriers for CO* hydrogenation to HCO* and its subsequent dissociation to CH* and O* are 1.16 eV and 0.93 eV. Despite the initial hydrogenation step being endothermic by 0.70 eV, the effective barrier for the H-assisted step is 1.66 eV, making the H-assisted pathway preferred over the direct pathway.

To better understand the differences in the activation energies of CO* direct dissociation, we performed a density of states (DOS) and Crystal Orbital Hamilton Population (COHP) analysis on CO* and the transition state of its dissociation towards C* + O* for Ni₈/TiO₂-a and Ni₈/TiO₂-r. The results of this analysis are shown in Fig. 10 and S24.† In Fig. S21a and f,† the DOS and COHP for the C-O interaction of CO in the gas phase is shown. Note that a more negative COHP coefficient indicates that the Kohn-Sham states provide a bonding contribution to the pair of atoms, while a more positive COHP coefficient indicates that the Kohn-Sham state provides a more anti-bonding contribution. Fig. S21a† displays the canonical molecular orbitals of CO and their occupancies. These molecular orbitals are commonly divided among σ - and π -type orbitals based on the presence or absence of a nodal plane alongside the C-O bonding axis. It can be readily observed that the number of valence electrons of CO in the gas phase corresponds to 10. From Fig. S21f,† the bonding character for each of the orbitals is seen including the integrated COHP (iCOHP) at the Fermi level which is a quantitative measure of the C-O bond strength. Upon adsorption, we can see from Fig. S24a and c† that the 3 σ and 4 σ interactions are largely unchanged due to a limited mixing of these molecular orbitals with the d-orbitals on Ni. In contrast, the 1π and 5σ orbitals show pronounced mixing as evidenced by the broadening of the peaks. Furthermore, due to the mixing of the anti-bonding $2\pi^*$ orbitals with the d-orbitals on Ni, the newly formed states derived from these orbitals descent below the Fermi level and become occupied. The integrated DOS (iDOS) at the Fermi level for adsorbed CO shows that the electron density around CO increases, in line with the higher electronegativity

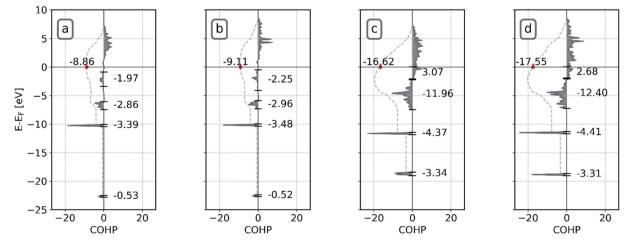


Fig. 10 COHP analysis of Ni-CO bonds in the initial state (IS) and transition state (TS) of CO direct dissociation on Ni₈/TiO₂-a and Ni₈/TiO₂-r. (a) IS on Ni₈/TiO₂-a; (b): IS on Ni₈/TiO₂-r; (c) TS on Ni₈/TiO₂-a; (d): TS on Ni₈/TiO₂-r. The numeric values above Fermi level indicate the integrated COHP (iCOHP)

of CO as compared to Ni and resulting in the occupation of the anti-bonding orbitals. The occupation of these antibonding orbitals together with the reduction in bonding character of the 1π -type orbitals lead to an activation of the CO molecule, as evidenced by the reduced iCOHP value shown in Fig. S21† corresponding to -15.86 and -16.09 for Ni₈/TiO₂-a and Ni₈/TiO₂-r, respectively. These values are however sufficiently similar that we cannot attribute the difference in the dissociation barrier to a difference in the activation of the CO molecule upon adsorption. The C-O interaction in the transition state, as shown in Fig. S21,† are also substantially similar from which we infer that both clusters have the same propensity towards activating CO and we hypothesize that the difference in the CO dissociation barrier should therefore be caused by differences in the stabilization of the pre-dissociated fragments in the transition state. It should be noted that this result contrasts with CO activation patterns typically found for extended metals, as showcased in the work of Fariduddin et al.⁷³

To test our hypothesis, in Fig. 10a-d, a COHP analysis is conducted for the Ni-CO interaction. Similar to the results found for the C-O interaction, here the COHP acts as a metric to assess the interaction strength between the cluster and the C* and O* fragments. The iCOHP values for adsorbed CO*, i.e. in the initial state, at the Fermi level are -8.86 and -9.11 for Ni₈/TiO₂-a and Ni₈/TiO₂-r. These values are in line with the observed adsorption heats of -2.14 eV and -2.54 eV for Ni₈/TiO₂-a and Ni₈/TiO₂-r, respectively. For the transition state, significantly lower iCOHP values of -16.62 and -17.55 are found for Ni₈/TiO₂-a and Ni₈/TiO₂-r, respectively. Clearly, Ni₈/TiO₂-r shows a significant increase in the Ni-CO interaction strength between the TS and IS in comparison to Ni₈/TiO₂-a, explaining the much lower reaction barrier observed. We attribute this enhanced bonding interaction of pre-dissociated C* and O* in the transition state on Ni₈/TiO₂-r to the presence of a very stable fivefold adsorption site for C, whereas for Ni₈/TiO₂-a a less favorable quasi-fourfold adsorption site is present (as shown in Fig. S25†). This five-fold site of Ni₈/TiO₂-r hosts a squareplanar motif for which exceptional stability for C* has been identified earlier in the work of Nandula et al.74

Conclusively, a critical factor in the preferred kinetic pathway is assigned to the presence of a low CO dissociation barrier. In the absence of such a barrier, a H-assisted route is preferred as seen for Ni₈/TiO₂-a. In contrast, Ni₈/TiO₂-r allows for a direct CO dissociation due to the availability of an active motif for which the COHP analysis predicts enhanced stability for the dissociation fragments.

4. Conclusions

In this study, the effect of the TiO₂ phase, anatase or rutile, on CO₂ hydrogenation over small Ni₈ cluster was investigated. Using a hybrid genetic algorithm/density functional theory approach, the putative global minimum structure for Ni₈ clusters supported on the most stable anatase and rutile surface terminations were searched. Due to different metal-support interactions, the Ni₈ clusters adopt different morphologies on anatase and rutile TiO2.

By means of density functional theory calculations, all elementary reaction steps relevant to CO2 hydrogenation, i.e. direct and H-assisted CO2 and CO dissociation as well as subsequent hydrogenation steps to form CH₄ and CH₃OH were calculated. By means of microkinetic modelling, we observed that the anatase supported Ni₈ clusters yielded a higher activity towards CO₂ consumption as compared to the rutile equivalent. For both clusters, at the low temperature the selectivity is mainly towards CH₄ whereas with increasing temperature, the selectivity switches to CO. The amount of CH₃OH produced remains negligible.

Both catalysts exhibit direct CO2 dissociation. Ni8/TiO2-r shows direct dissociation whereas for Ni₈/TiO₂-a the H-assisted route via a HCO* intermediate is preferred. Analysis of the reaction energy diagram and the DFT calculations reveal that this difference can be assigned to the stronger adsorption for carbonaceous species on Ni₈/TiO₂-r as compared to Ni₈-TiO₂-a. Not only leads this to a lower barrier for direct dissociation for the former catalyst, it also leads to the reaction intermediates being too strongly bound to the catalyst, effectively deactivating the catalyst. This rationalizes the consistent lower activity observed for Ni₈-TiO₂-r.

Analysis of the kinetic network pinpoints the CO dissociation barrier playing a critical role in determining the overall activity and mechanistic route. To understand the underlying electronic effects leading to the difference in CO dissociation barrier between the anatase and rutile supported Ni₈ clusters, a combined density of states and crystal orbital Hamilton population analysis was conducted. The integrated COHP value for the Ni-CO interaction at the Fermi level for the transition states for these two structures reveal that CO is more tightly bound to Ni₈ supported on rutile as compared to a cluster supported on anatase. This is not caused by electronic metal support interactions but rather by the different morphology of the cluster. For Ni₈/TiO₂-r, the morphology allows for highly stable fivefold-coordinated CO whereas for Ni₈/TiO₂-a, only a fourfold-coordinated mode is available which leads to less strongly bound CO.

This study showcases the potential role the support has in affecting the preferred pathway, selectivity and activity of a catalyst by inducing a preferred morphology of adsorbed clusters.

Data availability

The data supporting this article have been included as part of the ESI.†

Author contributions

Lulu Chen: conceptualization, data curation, formal analysis, investigation, validation, visualization, writing-original draft; Ying-Ying Ye: data curation, formal analysis, investigation,

visualization; Rozemarijn D. E. Krösschell: data curation, formal analysis visualization; Emiel J. M. Hensen: conceptualization, supervision, writing-review & editing, funding acquisition; Ivo A. W. Filot: conceptualization, methodology, resource, visualization, supervision, writing-review & editing, funding acquisition.

Conflicts of interest

The authors declare that there are no conflicts of interest regarding the publication of this paper.

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References

- 1 C. Vogt, M. Monai, G. J. Kramer and B. M. Weckhuysen, Nat. Catal., 2019, 2.
- 2 J. C. Navarro, M. A. Centeno, O. H. Laguna and J. A. Odriozola, Catalysts, 2018, 8.
- 3 L. Guerra, S. Rossi, J. Rodrigues, J. Gomes, J. Puna and M. T. Santos, J. Environ. Chem. Eng., 2018, 6, 671-676.
- 4 K. Müller, M. Städter, F. Rachow, D. Hoffmannbeck and D. Schmeißer, Environ. Earth Sci., 2013, 70, 3771-3778.
- 5 S. Chen and A. M. Abdel-Mageed, Int. J. Hydrogen Energy, 2013, 48, 24915-24935.
- 6 M. Götz, J. Lefebvre, F. Mörs, A. McDaniel Koch, F. Graf, S. Bajohr, R. Reimert and T. Kolb, Renewable Energy, 2016, 85,
- 7 M. Lehner, R. Tichler, H. Steinmüller and M. Koppe, Powerto-Gas: Technology and Business Models, Springer Briefs in Energy, 2014.
- 8 F. Graf, Impact, 2018, 2018, 81-83.
- O. Mohan, S. Shambhawi, R. Xu, A. A. Lapkin and S. H. Mushrif, ChemCatChem, 2021, 13, 2420-2433.
- 10 P. Frontera, A. Macario, M. Ferraro and P. L. Antonucci, Catalysts, 2017, 7, 59.
- 11 A. Quindimil, U. De-La-Torre, B. Pereda-Ayo, A. Davó-Quiñonero, E. Bailón-García, D. Lozano-Castelló, J. A. González-Marcos, A. Bueno-López and J. R. González-Velasco, Catal. Today, 2020, 356, 419-432.
- 12 A. Parastaev, V. Muravev, E. H. Osta, T. F. Kimpel, J. F. M. Simons, A. J. F. van Hoof, E. Uslamin, L. Zhang, J. J. C. Struijs, D. B. Burueva, E. V. Pokochueva, K. V. Kovtunov, I. V. Koptyug, I. J. Villar-Garcia, C. Escudero, T. Altantzis, P. Liu, A. Béché, S. Bals, N. Kosinov and E. J. M. Hensen, Nat. Catal., 2022, 5, 1051-1060.
- 13 Z. Liu, X. Gao, B. Liu, W. Song, Q. Ma, T. s. Zhao, X. Wang, J. W. Bae, X. Zhang and J. Zhang, Appl. Catal., B, 2022, 310, 121303.
- 14 S. Tada, T. Shimizu, H. Kameyama, T. Haneda and R. Kikuchi, Int. J. Hydrogen Energy, 2012, 37, 5527-5531.
- 15 R. van Hardeveld and A. van Montfoort, Surf. Sci., 1966, 4, 396-430.

- 16 G. Melaet, A. E. Lindeman and G. A. Somorjai, Top. Catal., 2014, 57, 500-507.
- 17 X. Wang, H. Shi, J. H. Kwak and J. Szanyi, ACS Catal., 2015, 5, 6337-6349.
- 18 V. Iablokov, S. K. Beaumont, S. Alayoglu, V. V. Pushkarev, C. Specht, J. Gao, A. Paul Alivisatos, N. Kruse and G. A. Somorjai, Nano Lett., 2012, 12, 3091-3096.
- 19 J. H. Kwak, L. Kovarik and J. Szanyi, ACS Catal., 2013, 3, 2449-2455.
- 20 P. Panagiotopoulou, Appl. Catal., A, 2017, 542, 63-70.
- 21 N. L. Visser, O. Daoura, P. N. Plessow, L. C. J. Smulders, J. W. de Rijk, J. A. Stewart, B. D. Vandegehuchte, F. Studt, J. E. S. van der Hoeven and P. E. de Jongh, ChemCatChem, 2022, 14, e202200665.
- 22 C. Vogt, E. Groeneveld, G. Kamsma, M. Nachtegaal, L. Lu, C. J. Kiely, P. H. Berben, F. Meirer and B. M. Weckhuysen, Nat. Catal., 2018, 1, 127-134.
- 23 C. Vogt, F. Meirer, M. Monai, E. Groeneveld, D. Ferri, R. A. van Santen, M. Nachtegaal, R. R. Unocic, A. I. Frenkel and B. M. Weckhuysen, Nat. Commun., 2021, 12, 7096.
- 24 Y. Guo, S. Mei, K. Yuan, D. J. Wang, H. C. Liu, C. H. Yan and Y. W. Zhang, ACS Catal., 2018, 8, 6203-6215.
- 25 E. J. M. H. Jérôme, F. M. Simons, T. J. de Heer, R. C. J. van de Poll, V. Muravev and N. Kosinov, J. Am. Chem. Soc., 2023, 145, 20289-20301.
- 26 M. P. C. Van Etten, B. Zijlstra, E. J. M. Hensen and I. A. W. Filot, ACS Catal., 2021, 11, 8484-8492.
- 27 S. Liang, C. Hao and Y. Shi, ChemCatChem, 2015, 7, 2559-2567.
- 28 R. Zhou, N. Rui, Z. Fan and C. Liu, Int. J. Hydrogen Energy, 2016, 41, 22017-22025.
- 29 C.-J. Pan, M.-C. Tsai, W.-N. Su, J. Rick, N. G. Akalework, A. K. Agegnehu, S.-Y. Cheng and B.-J. Hwang, J. Taiwan Inst. Chem. Eng., 2017, 74, 154-186.
- 30 W. Li, G. Zhang, X. Jiang, Y. Liu, J. Zhu, F. Ding, Z. Liu, X. Guo and C. Song, ACS Catal., 2019, 9, 2739–2751.
- 31 Y. Lin, Y. Zhu, X. Pan and X. Bao, Catal. Sci. Technol., 2017, 7, 2813-2818.
- 32 J. Zhou, Z. Gao, G. Xiang, T. Zhai, Z. Liu, W. Zhao, X. Liang and L. Wang, Nat. Commun., 2022, 13, 327.
- 33 D. Messou, V. Bernardin, F. Meunier, M. B. Ordoño, A. Urakawa, B. F. Machado, V. Collière, R. Philippe, P. Serp and C. Le Berre, J. Catal., 2021, 398, 14-28.
- 34 M. P. C. Van Etten, M. E. De Laat, E. J. M. Hensen and I. A. W. Filot, J. Phys. Chem. C, 2023, 127, 15148-15156.
- 35 J. P. Perdew, K. Burke and M. Ernzerhof, Phys. Rev. Lett., 1996, 77, 3865-3868.
- 36 G. Kresse and J. Furthmüller, Comput. Mater. Sci., 1996, 6, 15-50.
- 37 G. Kresse and J. Furthmüller, Phys. Rev. B: Condens. Matter Mater. Phys., 1996, 54, 11169.
- 38 P. E. Blöchl, Phys. Rev. B: Condens. Matter Mater. Phys., 1994, 50, 17953-17979.
- 39 D. Joubert, Phys. Rev. B: Condens. Matter Mater. Phys., 1999, **59**, 1758-1775.
- 40 P. W. Fry, I. E. Itskevich, S. R. Parnell, J. J. Finley, L. R. Wilson, K. L. Schumacher, D. J. Mowbray, M. S. Skolnick,

- A. G. Cullis, M. Hopkinson, J. C. Clark and G. Hill, Phys. Rev. B: Condens. Matter Mater. Phys., 2000, 62, 784-791.
- 41 S. Grimme, J. Antony, S. Ehrlich and H. Krieg, J. Chem. Phys., 2010, 132, 154104.
- 42 S. Grimme, S. Ehrlich and L. Goerigk, J. Comput. Chem., 2011, 32, 1456-1465.
- 43 G. Henkelman, B. P. Uberuaga and H. Jónsson, J. Chem. Phys., 2000, 113, 9901-9904.
- 44 G. Henkelman and H. Jónsson, J. Chem. Phys., 2000, 113, 9978-9985.
- 45 N. Martsinovich and A. Troisi, Phys. Chem. Chem. Phys., 2012, 14, 13392-13401.
- 46 D. H. M. Azevedo, G. S. L. Fabris, J. R. Sambrano and J. M. M. Cordeiro, Comput. Mater. Sci., 2020, 171, 109222.
- 47 R. D. E. Krösschell, E. J. M. Hensen and I. A. W. Filot, J. Phys. Chem. C, 2024, 128, 8947-8960.
- 48 C. J. Howard, T. M. Sabine and F. Dickson, Acta Crystallogr., Sect. B: Struct. Sci., 1991, 47, 462-468.
- 49 S. Wu, X. Luo, Y. Long and B. Xu, IOP Conf. Ser.: Mater. Sci. Eng., 2019, 493, 012010.
- 50 S. Ma, W. Song, B. Liu, H. Zheng, J. Deng, W. Zhong, J. Liu, X. Q. Gong and Z. Zhao, Catal. Sci. Technol., 2016, 6, 6128-6136.
- 51 L. B. Vilhelmsen and B. Hammer, J. Chem. Phys., 2014, 141, 044711.
- 52 M. W. Chang, L. Zhang, M. Davids, I. A. W. Filot and E. J. M. Hensen, J. Catal., 2020, 392, 39-47.
- 53 L. Van Der Maaten and G. Hinton, J. Mach. Learn. Res., 2008, 9, 2579-2605.
- 54 F. Pedregosa, G. Varoquaux, A. Gramfort, V. Michel, B. Thirion, O. Grisel, M. Blondel, A. Müller, J. Nothman, G. Louppe, P. Prettenhofer, R. Weiss, V. Dubourg, J. Vanderplas, D. Cournapeau, M. Brucher and M. Perrot, J. Mach. Learn. Res., 2011, 12, 2825-2830.
- 55 I. Gohberg, S. Goldberg and M. A. Kaashoek, Classes of Linear Operators, Birkhäuser Basel, Basel, 1990, vol. I, pp. 138-147.
- 56 I. A. W. Filot, M. P. C. van Etten, D. W. J. G. Trommelen and E. J. M. Hensen, J. Open Source Softw., 2023, 8, 5710.
- I. A. W. Filot, Introduction to microkinetic modeling, Technische Universiteit Eindhoven, 2018.

- 58 I. A. W. Filot, R. A. Van Santen and E. J. M. Hensen, Angew. Chem., Int. Ed., 2014, 53, 12746-12750.
- 59 P. Nitoń, A. Zywociński, M. Fiałkowski and R. Hołyst, Nanoscale, 2013, 5, 9732-9738.
- 60 W. L. Vrijburg, E. Moioli, W. Chen, M. Zhang, B. J. P. Terlingen, B. Zijlstra, I. A. W. Filot, A. Züttel, E. A. Pidko and E. J. M. Hensen, ACS Catal., 2019, 9, 7823-7839.
- 61 C. T. Campbell, Top. Catal., 1994, 1, 353-366.
- 62 F. Cannizzaro, E. J. M. Hensen and I. A. W. Filot, ACS Catal., 2023, 13, 1875-1892.
- 63 Q. Ke, L. Kang, X. Chen and Y. Wu, Chem. Sci. J., 2020, 132, 1-11.
- 64 A. Mahdavi-Shakib, T. N. Whittaker, T. Y. Yun, K. B. Sravan Kumar, L. C. Rich, S. Wang, R. M. Rioux, L. C. Grabow and B. D. Chandler, Nat. Catal., 2023, 6, 710-719.
- 65 E. B. Sterk, A. E. Nieuwelink, M. Monai, J. N. Louwen, E. T. C. Vogt, I. A. W. Filot and B. M. Weckhuysen, JACS Au, 2022, 2, 2714-2730.
- 66 J. Zhang, Y. Yang, J. Liu and B. Xiong, Appl. Surf. Sci., 2021, 558, 149866.
- 67 J. Liu, C. Li, F. Wang, S. He, H. Chen, Y. Zhao, M. Wei, D. G. Evans and X. Duan, Catal. Sci. Technol., 2013, 3, 2627-2633.
- 68 M. A. Abir, R. E. Phillips, J. Z. M. Harrah and M. R. Ball, Catal. Sci. Technol., 2024, 14, 4506-4521.
- 69 J.-Y. Li, X.-M. Lai, H. Gu, C.-X. Wang, X.-P. Fu, W.-W. Wang, O. Fu, F. Ryan Wang, C. Ma and C.-J. Jia, ChemRxiv, 2023, preprint, DOI: 10.26434/chemrxiv-2023-bm0gl.
- 70 F. Abild-Pedersen and M. P. Andersson, Surf. Sci., 2007, 601, 1747-1753.
- 71 J. Wellendorff, T. L. Silbaugh, D. Garcia-Pintos, J. K. Nørskov, T. Bligaard, F. Studt and C. T. Campbell, Surf. Sci., 2015, 640, 36-44.
- 72 O. Mohan, Q. T. Trinh, A. Banerjee and S. H. Mushrif, Mol. Simul., 2019, 45, 1163-1172.
- 73 I. A. W. Filot, F. Fariduddin, R. J. P. Broos, B. Zijlstra and E. J. M. Hensen, Catal. Today, 2016, 275, 111-118.
- A. Nandula, Q. T. Trinh, M. Saeys and A. N. Alexandrova, Angew. Chem., Int. Ed., 2015, 54, 5312-5316.