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## A review on electrochemical CO<sub>2</sub>-to-CH<sub>4</sub> conversion for a sustainable energy future: from electrocatalysts to electrolyzers

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The electrochemical reduction of carbon dioxide (CO<sub>2</sub>) to methane (CH<sub>4</sub>) offers a promising route to renewable fuels and carbon circularity, addressing urgent climate and energy challenges. However, key bottlenecks such as limited selectivity, sluggish reaction kinetics, and insufficient long-term stability still hinder the practical deployment of this reaction and technology. Fundamental research has uncovered promising electrocatalysts and mechanistic insights to overcome these limitations, yet translating these advances into scalable industrial solutions remains a major challenge. This review addresses this critical gap by providing a comprehensive and focused overview of electrochemical CO<sub>2</sub>-to-CH<sub>4</sub> conversion, from fundamental reaction mechanisms to system-level implementation. This work systematically analyzes the most selective and active electrocatalysts developed to date, elucidating key design principles that govern CH<sub>4</sub> production. In addition, we assess the evolution of CO<sub>2</sub> electrolyzers tailored for CH<sub>4</sub>, comparing device configurations, operational strategies, and levels of technological maturity. Techno-economic evaluations are also integrated to identify bottlenecks and realistic near-term implementation scenarios. As the demand for green CH<sub>4</sub> rises at a pace that outstrips conventional CH<sub>4</sub> growth, this technology emerges as a timely solution to decarbonize hard-to-abate sectors using renewable electricity.

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## 1 Introduction

The average atmospheric carbon dioxide (CO<sub>2</sub>) concentration in 2024 has once again reached an unprecedented level of 422 ppm, surpassing all historical human records. Projections indicate that the 2025 annual average CO<sub>2</sub> concentration is expected to exceed a peak value of 427 ppm<sup>1</sup> for the first time in the last 800 000 years.<sup>2</sup> This trend is anticipated to continue in an upward trajectory in the coming years, and this high concentration of CO<sub>2</sub> in the atmosphere is already contributing to a substantial rise in global temperature,<sup>3,4</sup> ocean acidification<sup>5</sup> and the disruption of the carbon cycle.<sup>6</sup> This forces scientists to intensify their efforts to explore and develop environmentally friendly ways of energy production,<sup>7</sup> with a focus on technologies that should aim to either reduce or (ideally) fully replace the use of conventional fossil fuel-based methods.<sup>8,9</sup> Beyond this urgent need to foster the broad implementation of such renewable energy sources, short- to mid-term solutions require a decrease of non-abatable CO<sub>2</sub> emissions or even active strategies to capture atmospheric CO<sub>2</sub>. To strengthen the economic viability of such approaches, CO<sub>2</sub> capture<sup>10,11</sup> should ideally be followed by the conversion of the carbon dioxide into value-added chemicals useful for industrial

applications.<sup>12,13</sup> This CO<sub>2</sub> conversion encompasses different methods, including chemical conversion,<sup>14–16</sup> biological transformation,<sup>17,18</sup> photocatalytic reduction<sup>19–21</sup> and electrochemical reduction.<sup>22–24</sup>

These CO<sub>2</sub>-conversion methods are plagued by well-known drawbacks, such as high energy requirements, low conversion rates, *etc.* By comparison, the electrochemical CO<sub>2</sub> reduction reaction (ECO<sub>2</sub>RR) has recently emerged as a highly promising pathway due to the possibility of coupling it with renewable electricity, as pictured in Fig. 1.<sup>25,26</sup> Furthermore, some of the products of the ECO<sub>2</sub>RR (*e.g.*, CO and C<sub>2</sub>H<sub>4</sub>) can serve as valuable fuels or chemicals that integrate perfectly into existing industrial processes. Moreover, this electrochemical reaction is well-known for its controllable and mild reaction conditions (*i.e.*, close-to-atmospheric temperatures and pressures). Nonetheless, there are still notable challenges associated with the ECO<sub>2</sub>RR, including its limited operative current density (often << 1 A cm<sup>-2</sup>), poor selectivity towards producing a single desired product, and lack of stability.<sup>27–29</sup>

In an industrial context, two different application scenarios are envisaged for the ECO<sub>2</sub>RR. First, the reaction can be conducted within a standalone electrochemical system in which the resulting products are stored for subsequent use in other industries. Alternatively, the CO<sub>2</sub> can be electrochemically converted into a value-added product that is directly coupled to a second reactor, thus avoiding (or at least mitigating)

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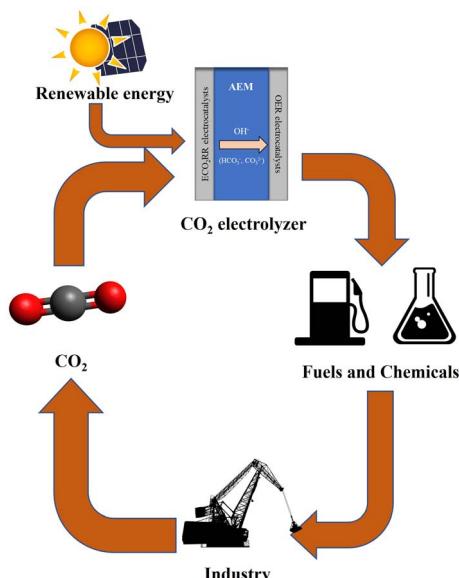


Fig. 1 Illustration of the closed carbon cycle enabled by a  $\text{CO}_2$  electrolyzer (in this example, relying on the use of an anion exchange membrane, AEM, and with the  $\text{O}_2$  evolution reaction (OER) as the anodic counter reaction) powered by renewable energy sources and that converts captured or emitted  $\text{CO}_2$  into chemicals or fuels for their direct usage in the industrial sector.

additional costs associated with product storage and transportation. This second approach is more demanding in terms of performance because the resulting products must be of extremely high purity. Since they are fed directly into another industrial process, they need to meet strict quality standards to ensure efficiency and prevent any negative impact on the subsequent production state. This represents an important bottleneck in the  $\text{ECO}_2\text{RR}$ , as many materials electrochemically reduce  $\text{CO}_2$  to a wide variety of carbon-containing chemicals and/or  $\text{H}_2$  with poor selectivity.<sup>30-32</sup>

One of these possible  $\text{ECO}_2\text{RR}$  products is methane ( $\text{CH}_4$ ), which has otherwise found extensive use as an energy source in the fields of low-pollution power generation, liquid-natural-gas vehicles and so on.<sup>30</sup>  $\text{CH}_4$  is particularly valuable where existing infrastructure for natural gas storage, distribution and consumption can be leveraged,<sup>23</sup> since 70–90% of this natural gas (which is mainly obtained from oil wells and coal beds<sup>33</sup>) is composed of  $\text{CH}_4$ .<sup>34</sup> As an extensive storage and distribution network already exists for natural gas, the development of electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  conversion would enable a rapid and widespread distribution of net-zero-carbon energy services.<sup>35,36</sup> The global high purity methane gas market was valued at USD 101 billion in 2020 and is projected to reach USD 153 billion by 2025,<sup>37</sup> which is by far superior to other  $\text{ECO}_2\text{RR}$ -derived products, such as CO (USD 3.3 billion in 2022 and projected to reach USD 4.5 billion by 2030)<sup>38</sup> or  $\text{HCOOH}$  (USD 2.1 billion in 2023 and projected to reach USD 3.8 billion by

2030).<sup>39</sup> Nevertheless, several challenges impede the widespread implementation of electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  conversion, including the low faradaic efficiencies (FEs), sluggish kinetics and poor durability exhibited by most catalysts and reactor configurations. Moreover, the electrochemical production of  $\text{CH}_4$  faces economic hurdles, as this gas possesses the lowest average market price among all  $\text{CO}_2$ -derived products.<sup>40</sup> Specifically, the cost of  $\text{CH}_4$  from the electrochemical reduction of  $\text{CO}_2$  is expected to stand at approximately 2.5–10 \$  $\text{kg}^{-1}$ , which is still higher than traditional  $\text{CH}_4$ -synthesis methods (0.2–0.5 \$  $\text{kg}^{-1}$ ).<sup>40</sup> In this regard, techno-economic analyses have suggested that the price of  $\text{ECO}_2\text{RR}$ -derived  $\text{CH}_4$  must be reduced to at least  $\approx 1.0$  \$  $\text{kg}^{-1}$  to effectively compete with traditional  $\text{CH}_4$ -production procedures.<sup>40</sup> Today, these elevated costs represent a major barrier for large-scale implementation, as achieving cost parity still requires substantial improvements in energy efficiency, catalyst durability, and system integration (or alternatively, stronger policy incentives to shift competitiveness). The successful integration of electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  conversion into existing natural gas infrastructure will strongly depend on consolidating the past achievements while addressing the remaining techno-economic challenges.

With this motivation, in this review we comprehensively examine the advancements in electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  conversion, focusing on the nature of electrocatalysts and the design of electrochemical cells and devices. We first discuss the fundamental principles of the  $\text{ECO}_2\text{RR}$ , including reduction mechanisms and electric double layer (EDL) effects. Subsequently, we delve deeply into the recent developments concerning electrocatalysts, operating conditions and  $\text{CO}_2$  electrolyzers. Finally, we offer insights into the future prospects of the  $\text{ECO}_2\text{RR}$  and highlight the challenges that must be addressed to enhance the efficiency and effectiveness of this electrochemical reaction to accomplish techno-economic requirements.

## 2 Fundamentals of the $\text{ECO}_2\text{RR}$

### 2.1 Thermodynamics and reaction mechanism

$\text{CO}_2$  is a thermodynamically stable molecule with linear geometry and a dissociation energy of the  $\text{C}=\text{O}$  bond of  $\approx 750$  kJ  $\text{mol}^{-1}$ .<sup>30,41</sup> This high energy requirement suggests a substantial activation energy for direct  $\text{C}=\text{O}$  bond dissociation. In the  $\text{CO}_2$  reduction mechanism, this activation must be considered as the first step, where the linear geometry of the pristine molecule is transformed into a bent configuration in which the  $\text{C}=\text{O}$  bond is weakened through the formation of chemical bonds between the  $\text{CO}_2$  molecules and the active sites.<sup>42</sup> After  $\text{CO}_2$  adsorption, the  $\text{ECO}_2\text{RR}$  goes through a series of reaction steps at the surface of the active phase involving the cleavage of C–O bonds, C–C coupling, or C–H formation, and multiple electron transfer processes (e.g., 2 electrons for  $\text{CO}$ , 6 electrons for  $\text{CH}_3\text{OH}$ ) and eventually leading to different products.<sup>43,44</sup>

In theory, this variety of  $\text{ECO}_2\text{R}$  reactions generally exhibits their thermodynamic equilibrium potentials at values close to 0.0 V *vs.* the reversible hydrogen electrode (RHE), as shown in Table 1, which also includes the competing (and undesired)  $\text{H}_2$ -



**Table 1** Electrochemical  $\text{CO}_2$  reduction potentials versus the standard hydrogen electrode (SHE) at pH 7. Hydrogen evolution reaction is included for comparison purposes

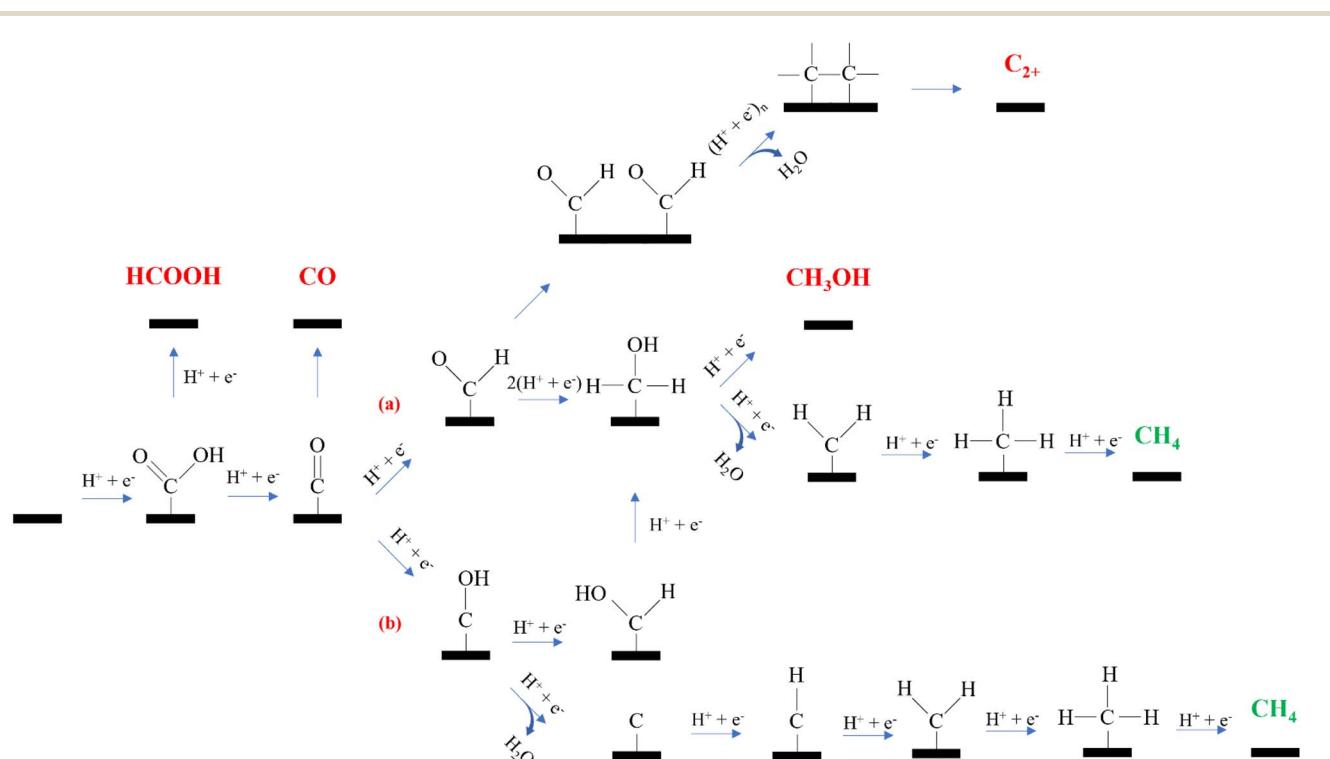
Electrochemical reaction	Thermodynamic potential/V vs. RHE
$\text{CO}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow \text{HCOOH}$	-0.12
$\text{CO}_2 + 2\text{H}^+ + 2\text{e}^- \rightarrow \text{CO} + \text{H}_2\text{O}$	-0.10
$\text{CO}_2 + 6\text{H}^+ + 6\text{e}^- \rightarrow \text{CH}_3\text{OH} + \text{H}_2\text{O}$	0.03
$\text{CO}_2 + 8\text{H}^+ + 8\text{e}^- \rightarrow \text{CH}_4 + 2\text{H}_2\text{O}$	0.17
$2\text{CO}_2 + 12\text{H}^+ + 12\text{e}^- \rightarrow \text{C}_2\text{H}_4 + 4\text{H}_2\text{O}$	0.08
$2\text{H}^+ + 2\text{e}^- \rightarrow \text{H}_2$	0.00

evolution reaction (HER). All potentials were calculated based on the Gibbs free energy of reaction, using gas-phase thermochemistry data and Henry's law data for aqueous products.<sup>24</sup> Beyond these thermodynamic considerations, one must bear in mind that large overpotentials are often required for achieving sufficiently high current densities due to the sluggish kinetics of these reactions.<sup>45–47</sup> Furthermore, the  $\text{ECO}_2\text{RR}$  is highly sensitive to the applied potential, as the selectivity towards a given product usually follows the tendency of increasing until a maximum value and then decreasing when more negative potentials are applied.

Concerning the electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  reduction reaction, it has been proposed that  $\text{CH}_4$  formation undergoes two stages schematized in Fig. 2: the first one is the initial formation of a CO intermediate adsorbed to the catalyst surface ( $^*\text{CO}$ ) and one water molecule, and the second stage is the subsequent

hydrogenation of the  $^*\text{CO}$  into  $\text{CH}_4$ .<sup>42,48</sup> The key factor determining the selectivity towards  $\text{CH}_4$  formation appears to be related to the binding energy of the  $^*\text{CO}$ . Namely, if the binding energy of this intermediate is too weak, most of the  $^*\text{CO}$  will desorb as carbon monoxide (CO), whereas a moderate binding energy between the active site and the C atom of the  $^*\text{CO}$  intermediate is mandatory to reach high selectivity towards  $\text{CH}_4$  formation. Computational studies have demonstrated that this hydrogenation can take place through (a) the hydrogenation of the C atom forming a so-called  $^*\text{CHO}$  intermediate, or (b) the weakening of the C=O bond through the hydrogenation of the O atom, to form a  $^*\text{C-OH}$  intermediate (see Fig. 2). The rate determining step in both mechanisms is the formation of the first hydrogenation intermediate (*i.e.*,  $^*\text{CHO}$  or  $^*\text{COH}$ ). It is worth pointing out that the  $^*\text{COH}$  intermediate might result in the formation of either  $\text{CH}_4$  or  $\text{CH}_3\text{OH}$ , while  $^*\text{CHO}$  can also proceed to form  $\text{C}_2\text{H}_4$  compounds. In pathway (b), water may be desorbed and lead to the  $\text{ECO}_2\text{RR}$  to proceed through a  $^*\text{C}$  intermediate. After electron–proton pair additions, this intermediate undergoes reduction reactions towards  $^*\text{CH}$ ,  $^*\text{CH}_2$  and so on.<sup>49</sup>

There are also several competitive reactions that can tune the selectivity towards  $\text{CH}_4$  formation from  $\text{CO}_2$ . In mechanism (a), the selectivity for  $\text{CH}_4$  generation over  $\text{CH}_3\text{OH}$  is determined by the last reduction step, where  $^*\text{CH}_3\text{OH}$  can undergo two different pathways leading to the hydrogenation of either the oxygen or the carbon atoms. At the same time, it has been demonstrated that  $\text{C}_2\text{H}_4$  and  $\text{CH}_4$  generation share similar pathways until the  $^*\text{CHO}$  intermediate.<sup>48</sup> If C–C coupling reactions are favored at the electrocatalyst's surface, the formation



**Fig. 2** Proposed mechanism for electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  conversion and competitive reactions towards other  $\text{CO}_2$ -derived products.



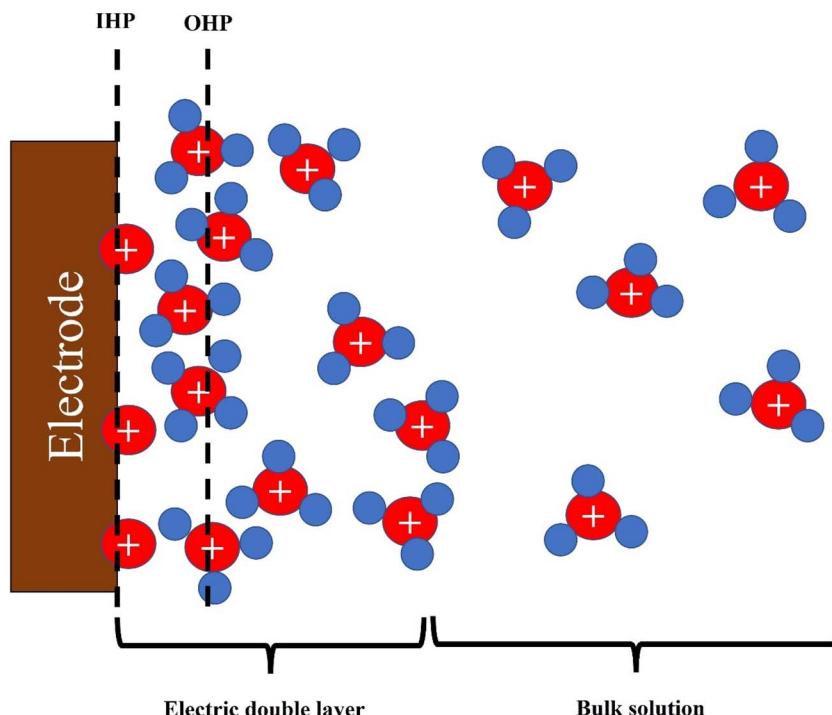


Fig. 3 Illustration of the inner Helmholtz plane (IHP) and outer Helmholtz plane (OHP) in the electric double layer. Red spheres represent the cation and blue spheres represent water molecules acting as solvation spheres. Anions in the solution are not incorporated for the sake of clarity.

of an  $\text{OHC}^*-\text{CHO}$  intermediate will predominate. Thus, in the search for highly selective  $\text{CO}_2$ -to- $\text{CH}_4$  electrocatalysts, the active sites should favor the completion of the  $\text{CH}_4$  pathway avoiding C-C coupling.

The HER is the main competing reaction in the cathodic reduction of  $\text{CO}_2$  in aqueous electrolytes, since it features a similar equilibrium potential (Table 1) and is particularly facile to catalyze in acid solutions.<sup>47</sup> The first reaction step involves the reduction of protons or  $\text{H}_2\text{O}$  molecules in the electrolyte to produce adsorbed H ( $\text{H}^*$ , known as the Volmer step) that is subsequently further reduced to generate  $\text{H}_2$  molecules. If the catalyst's active sites exhibit strong  $\text{H}^*$  adsorption, the HER will predominate and the  $\text{ECO}_2\text{RR}$  will be suppressed, and thus a good  $\text{ECO}_2\text{RR}$  electrocatalyst must feature a weak binding strength towards  $\text{H}^*$  and moderate  $\text{CO}_2$  activation.

## 2.2 Electric double layer

Although the electrolyte is sometimes considered chemically inert in many electrochemical reactions, the identity of the ions present in it is known to affect the reaction rates and product selectivity of many electrochemical reactions in impactful ways.<sup>50</sup> This is in part due to the electric double layer (EDL) that forms when a solution containing ions is in contact with a solid surface that holds stationary charges.<sup>51</sup> The EDL is the result of the attractive and repulsive electrostatic interactions between the ions in the electrolyte and the charged surface, creating a locally varied electric potential. The understanding of the EDL in electrochemical reactions has significantly advanced over the

decades. The proposed theories include (i) the blocking of the active sites by ions of the electrolyte, (ii) the redistribution of the potential drop in the double layer, which heavily affects the driving force for electron transfer, (iii) the interaction of the interfacial electric field with the electric dipole moments and polarizabilities of adsorbed intermediates, (iv) chemical interaction between ions and reaction intermediates, (v) the buffering of the interfacial pH by hydrated ions, and (vi) the alteration of the interfacial water structure.<sup>52</sup> To fully understand the EDL, it is worth mentioning that all these theoretical concepts are not strictly separable but interrelated.

For cathodic reactions like the  $\text{ECO}_2\text{RR}$ , the electrode is negatively polarized and its negative charge translates into an excess of cations and a depletion of anions in the vicinity of its surface (Fig. 3).<sup>53</sup> The outer Helmholtz plane (OHP) represents the closest approach of hydrated ions to the surface, while the inner Helmholtz plane (IHP) is formed by the ions that are chemically adsorbed onto the surface of the electrode.

Many studies have reported effects of the electrolyte's cation(s) on the  $\text{ECO}_2\text{RR}$  in aqueous media. One illustrative example is observed by substituting  $\text{Li}^+$  with  $\text{Cs}^+$ , where the latter cationic species leads to a substantial enhancement of the ethylene selectivity during the  $\text{ECO}_2\text{RR}$  on  $\text{Cu}(100)$ - and  $\text{Cu}(111)$ -oriented thin films.<sup>54</sup> Such a cationic effect is mainly related to the tendency of cations to chemically or physically adsorb on the electrode surface, which is governed by the reaction energetics and hydration shell of the cations.<sup>55</sup> The hydration capacity is stronger for smaller alkali cations, with the  $\text{Li}^+$  ion binding the water molecules more strongly and



being less likely to adsorb on the cathode surface. Conversely, bigger cations are more likely to adsorb onto the electrode surface, shifting the position of the OHL<sup>55</sup> and leading to a lower concentration of H<sup>+</sup> in the vicinity of the active surface that translates into reduced selectivity towards hydrogenated CO<sub>2</sub>RR products, such as CH<sub>4</sub>.<sup>55</sup> We encourage those readers interested in a more detailed discussion of the effect of the EDL structure on the ECO<sub>2</sub>RR to revisit the following literature.<sup>56–58</sup>

### 3 Electrocatalyst design

Electrocatalysts are essential for the ECO<sub>2</sub>RR, since they speed up the rate of this highly complex and kinetically demanding electrochemical reaction. These electrocatalysts hold the potential to substantially improve and modulate the selectivity and kinetics of electrochemical CO<sub>2</sub> reduction, all the while preserving their intrinsic properties. The urgent need to address climate change and reduce anthropogenic CO<sub>2</sub> has pointed out the key role of electrocatalyst design for the ECO<sub>2</sub>RR in the coming years.

In the 80s and 90s, ECO<sub>2</sub>RR electrocatalysts were classified into different groups according to the metal phase and resulting product selectivity.<sup>59</sup> However, it is currently known that activity and selectivity do not only depend on the nature of the metal phase, but also on complementary properties such as the electronic configuration, catalyst support, surface chemistry, morphology or electric conductivity.<sup>59–62</sup> It is proven that tuning the electronic properties, composition and morphology of the electrocatalysts can significantly modify the density and turnover frequency of the sites/phases active for the ECO<sub>2</sub>RR.

Thus, in this section we present and discuss recent developments in ECO<sub>2</sub>RR electrocatalysts based on their initial composition, to then delve into the influence of different electronic and structural properties that can tune the ECO<sub>2</sub>RR performance, with especial emphasis on electrochemical CO<sub>2</sub>-to-CH<sub>4</sub> conversion. To provide a quick overview for the readers, we summarize in Table 2 the most active catalysts reported to date, highlighting key electrochemical parameters.

#### 3.1 Metal electrocatalysts

A simple but vague classification can be made by considering the nature of the metallic phase for bulk materials.<sup>47</sup> Generally speaking, most of the transition metals electrocatalyze the HER more easily than the ECO<sub>2</sub>RR in aqueous media, rendering them useless for practical application when seeking CH<sub>4</sub> formation. This HER-selective material group includes Ti and Pt, among others. Complementarily, some transition metals exhibit higher ECO<sub>2</sub>RR *vs.* HER performance with preferred selectivity towards CO formation, as is the case of Au, Ag and Zn, or preference towards HCOOH formation, as is the case of In, Sn and Cd. In a more particular scenario, Cu-based electrocatalysts have arisen as the only category capable of converting CO<sub>2</sub> into hydrocarbons, including our target product, CH<sub>4</sub>.<sup>59</sup>

Bulk electrodes in the form of metal foils normally require high overpotentials to catalyze CO<sub>2</sub> conversion, and thus many studies have recently focused their efforts on nanostructured materials with a higher ratio of surface-accessible active sites. Moreover, nanostructured materials can exhibit rough surfaces, combinations of oxidation states, small crystalline features and defects that can enhance their ECO<sub>2</sub>RR performance with regard to the corresponding bulk transition metal. In the following subsection, we tackle the effect of structural, chemical and electric properties that result in high selectivity towards CH<sub>4</sub> formation.

**3.1.1. Cu-based electrocatalysts.** As mentioned before, copper (Cu) stands out among other metals due to its capability for converting CO<sub>2</sub> into hydrocarbons, including CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub> and C<sub>2</sub>H<sub>6</sub>, with low selectivity towards a single product.<sup>63</sup> However, understanding the factors that determine this catalytic activity remains a challenge. Modelling works grouped all Cu crystal facets in the order of their ECO<sub>2</sub>RR activity, Cu(211) being the most active surface, followed by Cu(110), Cu(100), and finally Cu(111).<sup>64</sup> The findings indicate that Cu(211) is the surface of pure Cu that exhibits the best electrocatalytic activity for both CO and CH<sub>4</sub> formation, which unfortunately makes them non-selective towards the formation of one unique product.

**Table 2** Summary of representative electrocatalysts for electrochemical CO<sub>2</sub>-to-CH<sub>4</sub> conversion, including their reported active sites, maximum CH<sub>4</sub> faradaic efficiency (FE), operating current density, applied potentials, stability metrics (if reported), and corresponding references. Current densities marked with \* refer to partial CH<sub>4</sub> current densities. \*\* refers to applied voltage instead of applied potential

Active site	CH <sub>4</sub> FE/%	j/mA cm <sup>-2</sup>	E/V <i>vs.</i> RHE	Stability	Electrolyzer	Reference
Cu nanoparticles	76	11	−1.35	—	H-type cell	71
Cu nanoparticles	58	105	−1.00	—	Flow cell	87
Cu nanoparticles	73	234	−1.10	—	Flow cell	88
Cu nanoparticles	60	230	4 V**	50 h	Zero-gap cell	88
CuN <sub>4</sub>	55	35	−1.25	12 h	H-type cell	93
CuN <sub>2</sub> B <sub>2</sub>	73	292	−1.46	8 h	Flow cell	95
CuN <sub>2</sub> O <sub>2</sub>	78	40	−1.44	6 h	H-type cell	97
La <sub>5</sub> Cu <sub>95</sub>	65	300	−1.72	—	Flow cell	99
Pd single atoms on Cu	60	118*	−1.10	—	Flow cell	103
N <sub>x</sub> C-encapsulated Ag nanoparticles	44	7	−1.40	10 h	H-type cell	108
N-doped carbons	15	30	−0.90	—	H-type cell	133
F- and N-doped carbons	99	0.2	−0.80	—	H-type cell	150
Cu single atoms	62	136	4 V**	110 h	Zero-gap cell	171
Cu single atoms	82	400	−0.90	5 h	Flow cell	201



Experimentally, initial studies with Cu foils<sup>65</sup> demonstrated that the preparation conditions of the Cu surface affect selectivity and efficiency towards certain products. The experiments showed that methane is produced when the Cu surface is cleaned with HCl rather than HNO<sub>3</sub> or oxidized in air, suggesting that the oxidation state of Cu significantly influences the reaction mechanisms. Some years later, a few studies demonstrated that improved hydrocarbon selectivity was observed in oxidized Cu foils due to the presence of Cu<sub>2</sub>O sites, which act as a more active phase for certain hydrocarbons than metallic Cu.<sup>66–68</sup> More precisely, the work of Mistry *et al.*<sup>66</sup> demonstrated that a H<sub>2</sub> plasma treatment of polycrystalline Cu led to a metallic Cu surface that yielded a large C<sub>1</sub> product selectivity, with a FE for CH<sub>4</sub> formation of 37%. In contrast, an O<sub>2</sub> plasma treatment of polycrystalline Cu produced an oxidized surface with nearly 0% C<sub>1</sub> product selectivity, but a high conversion to C<sub>2</sub> products, including a FE for C<sub>2</sub>H<sub>4</sub> of 60%.

Recently, it was demonstrated that the presence of an oxidizing agent in the electrolyte can also modulate the ECO<sub>2</sub>RR activity of Cu electrocatalysts. As shown in the literature,<sup>70</sup> oxygen-containing species not only enhance the rate of the ECO<sub>2</sub>RR, but also tune selectivity for certain products. The presence of H<sub>2</sub>O<sub>2</sub> accelerates the rate of CH<sub>4</sub> production by a factor of 200 in Cu electrodes, whereas in O<sub>2</sub>-containing solutions a strong decrease of CH<sub>4</sub> production is observed. The authors relate such behavior to an increase in the surface concentration of oxygen-containing Cu species that, when stabilized, can significantly enhance the ECO<sub>2</sub>RR activity and selectivity of such electrodes, in a very similar way to what was discussed above for pre-oxidized Cu samples. In addition, the same authors claimed that selectivity for different products can be tuned by the chemical structure of the oxygen-containing species.

**3.1.1.1 Cu nanoparticle electrocatalysts.** With advances in nanoparticle synthesis, controlling the size, composition, structure and morphology of Cu nanoparticles is nowadays possible. For such nanoparticulate materials, there are three main parameters that determine the ECO<sub>2</sub>RR performance: their composition, size and support. The size of Cu nanoparticles has proven to play a key role in ECO<sub>2</sub>RR catalysis. Cu nanoparticles showed high selectivity towards CH<sub>4</sub> formation (FE of 76%), which is substantially superior to the CH<sub>4</sub> FE of polycrystalline Cu (44%).<sup>71</sup> Nevertheless, Cu nanoparticles with a diameter below 15 nm tend to enhance competitive reactions, such as H<sub>2</sub>-evolution and electrochemical CO<sub>2</sub>-to-CO conversion, significantly lowering the FE towards CH<sub>4</sub>.<sup>69</sup> A controlled synthesis of Cu nanoparticles of different sizes is illustrated in the AFM images in Fig. 4A–F. As shown in Fig. 4G and H, the smaller the nanoparticle diameter, the higher the current density in linear sweep voltammetry curves. This enhanced current density is associated with not only an improvement of the ECO<sub>2</sub>RR performance, but also an increase in the HER activity. Smaller nanoparticles exhibit a substantial enhancement in selectivity towards H<sub>2</sub>, whereas larger nanoparticles tend to favor ECO<sub>2</sub>RR products.<sup>69</sup> As a result, large nanoparticle sizes are recommended for hydrocarbon production (Fig. 4I).

Another essential aspect when designing Cu-based electrocatalysts is the catalytic support. The main goal of this support is to inhibit nanoparticle agglomeration during catalyst synthesis and under working conditions,<sup>72</sup> and to provide diffusion channels for the supply of the reactant and the evacuation of the products.<sup>63</sup> Moreover, catalytic supports are also essential to assure electrical conduction paths to the metal sites. The most common supports are based on carbon materials,<sup>73</sup> although other materials can also act as effective supports, such as polymers,<sup>74–76</sup> CeO<sub>2</sub> (ref. 77 and 78) or molybdenum-based 2D materials.<sup>79–81</sup>

Carbonaceous materials are low-cost and abundant catalytic supports, making them promising for reducing electrocatalyst costs.<sup>28</sup> Anchoring metals on carbon materials has been an excellent approach for large-scale electrocatalyst production.<sup>82</sup> The metal phase provides active sites for the ECO<sub>2</sub>RR, while the carbon provides a high surface area that reduces diffusion limitations and exposes a higher number of Cu active sites, while ensuring that the metal-support assembly remains electrically conductive.<sup>28</sup> Carbon materials, especially those that are doped with heteroatoms, feature excellent nanoparticle-anchoring capabilities owing to their metal–heteroatom chemical bonds. Nitrogen (N) is by far the most studied heteroatom,<sup>69,83–85</sup> since its similar size to carbon and unique electronic configuration generate electron delocalization in the carbon layers, resulting in an n-type-like semiconductor, as the substitution of a carbon atom with nitrogen introduces an extra electron into the carbon structure, which can move through the electron cloud, enhancing electrical conductivity. Additionally, N atoms strongly interact with metal phases, avoiding nanoparticle leaching and agglomeration and thus enhancing the electrocatalyst's *operando* stability.<sup>96</sup>

One example of such an N heteroatom effect was observed by Dai *et al.*,<sup>87</sup> who anchored Cu on a carbon support through strong metal–heteroatom interaction using pyridine-based N-functionalities (pyridine-substituted graphdiyne (Py-GDY)) obtained by cross-coupling of 1,3,5-triethynyl-2,4,6-tris(4-pyridyl) benzene. The non-doped homologous material (GDY) exhibited larger and more heterogeneous Cu-nanoparticle sizes, and while the catalyst prepared with Py-GDY showed excellent ECO<sub>2</sub>RR selectivity with a CH<sub>4</sub> FE of 58% at a current density of 105 mA cm<sup>−2</sup>, the catalyst made with non-doped GDY had a methane faradaic efficiency of only 37% at the same current. The authors attributed this enhanced selectivity for CH<sub>4</sub> formation to the pyridyl groups, which led to strong metal–N interaction that resulted in uniformly dispersed Cu nanoclusters of about 2 nm.<sup>87</sup> In a similar study,<sup>88</sup> the authors prepared Cu nanoparticles supported on an N-doped carbon material that featured excellent properties towards CH<sub>4</sub> selectivity, with a maximum FE of 73% and a CH<sub>4</sub>-specific current density of 230 mA cm<sup>−2</sup> at −1.1 V vs. RHE, which is again much higher than that of the analogous catalyst prepared on a non-doped support at the same potential (CH<sub>4</sub>-specific current density and FE below 50 mA cm<sup>−2</sup> and 20%, respectively). In this case, the high methane selectivity was attributed to the pyrrolic N in the vicinity of the Cu nanoparticles, which accelerates the hydrogenation of reaction intermediates.



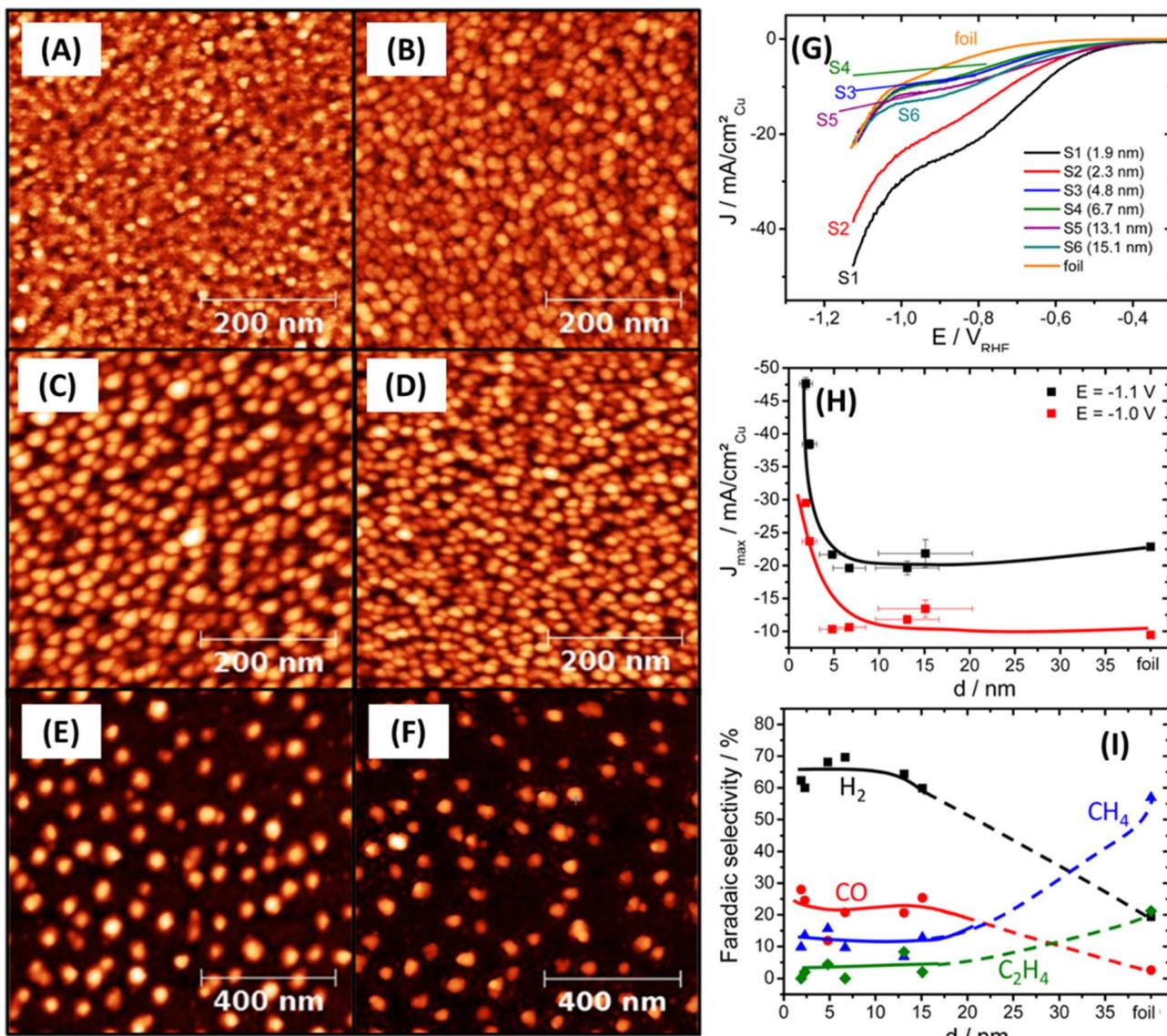


Fig. 4 Tapping-mode atomic force microscopy images of Cu nanoparticles supported on SiO<sub>2</sub> (4 nm)/Si(111): (A) S1, (B) S2, (C) S3, (D) S4, (E) S5, and (F) S6. (G) Linear sweep voltammograms recorded on glassy carbon supports, S1–S6, in a CO<sub>2</sub>-saturated 0.1 M KHCO<sub>3</sub> solution acquired at room temperature and at a scan rate of 5 mV s<sup>-1</sup>. Current densities were normalized by the Cu particle surface area after subtraction of the glassy carbon background signal at -1.1 V vs. RHE. A Cu foil is included as a reference. (H) Particle size effect during catalytic CO<sub>2</sub> reduction. The faradaic current densities at -1.1 and -1.0 V vs. RHE are plotted against the size of the Cu nanoparticles. The current densities have been normalized by the Cu particle surface area after subtraction of the glassy carbon background signal. (I) Particle size dependence of faradaic selectivity towards various reaction products during the CO<sub>2</sub> reduction reaction. Reproduced from ref. 69 with permission from the American Chemical Society, copyright 2014.

In summary, the surface functional groups in carbon supports have proven to be capable of modulating the selectivity and activity of electrochemical CO<sub>2</sub> reduction towards CH<sub>4</sub> conversion, and thus such functionalities may play a decisive role in the future development of highly effective electrocatalysts for this reaction.

**3.1.1.2 Cu single-atom electrocatalysts.** The maximized atomic utilization and well-defined coordination of single atom sites make them the most promising active centers among Cu-based ECO<sub>2</sub>RR electrocatalysts.<sup>89</sup> The rational design of the coordination of the metal center, including the nature and

number of the coordination atoms, affects substantially the electronic structure of the metal site and should cause significant changes in the reaction pathway and product selectivity with regard to the extended metal surface. A Cu–N<sub>4</sub> coordination is the most desirable configuration for the ECO<sub>2</sub>RR due to its high stability, stemming from its optimal thermodynamic interaction between Cu atoms and reaction intermediates.<sup>89</sup> It is widely acknowledged that Cu single atoms often produce hydrocarbons with only one carbon atom (*i.e.*, C<sub>1</sub> products) because the lack of adjacent active sites restrains C–C coupling. Beyond this general observation, some studies reported high

selectivity towards  $\text{CH}_3\text{OH}$  or  $\text{CH}_4$ , while a few other studies reported a preference for CO formation.<sup>90,91</sup> The reasons for this discrepancy remain unanswered, with new studies focusing more on electrocatalytic results rather than on understanding these disparities.

As an example, Cu single atoms displaying the above Cu–N<sub>4</sub> configuration and incorporated into carbon nanofibers electrochemically reduced  $\text{CO}_2$  to  $\text{CH}_3\text{OH}$  with a FE of 44% at a current density of 93 mA cm<sup>-2</sup>.<sup>92</sup> DFT modelling showed that these Cu–N<sub>4</sub> single atoms possess a high adsorption energy for the \*CO intermediate<sup>92</sup> and that the free energy barrier of the subsequent \*CHO to \*CHOH step is much lower than that of the \*CHO to \*CH<sub>2</sub>O path, thus favoring methanol over  $\text{CH}_4$  or CO production. However, in a different study, CuN<sub>4</sub> single atoms obtained from Cu phthalocyanine exhibited a high FE towards  $\text{CH}_4$  (55% at a current density of ~35 mA cm<sup>-2</sup>).<sup>93</sup> At the same time, a high  $\text{CO}_2$ -to-CO conversion was recently reported with CuN<sub>4</sub> single atoms anchored on carbon materials<sup>94</sup> that showed a FE towards CO of >90%. These are just a few examples of the large variety of selectivity trends reported for CuN<sub>4</sub> sites, for which the disparities remain elusive. All these previous studies have employed DFT calculations to support the reported selectivity and mechanisms, in principle proving the thermodynamic viability of the individual ECO<sub>2</sub>RR pathway towards  $\text{CH}_3\text{OH}$ ,  $\text{CH}_4$  or CO, but without modelling all other possible reaction mechanisms, which make these results inconclusive.

Another important factor that may account for these discrepancies is the nature of the supporting matrix. Beyond simply stabilizing the Cu–N<sub>4</sub> moieties, the substrate can strongly influence charge distribution, binding energies of intermediates, and even site stability. For instance, CuN<sub>4</sub> decorated on N-doped carbon dots has been reported to deliver FEs above 80% for ethanol,<sup>95</sup> while Cu single atoms embedded in a porphyrin-based MOF produced  $\text{CH}_4$  with a FE of ≈80%.<sup>96</sup> However, the substrate is clearly not the sole determinant: another study on Cu single atoms in a porphyrin-based MOF instead showed a high selectivity towards acetate (>40%) with negligible  $\text{CH}_4$  production.<sup>97</sup> These contrasting examples highlight that the catalytic outcome arises from a complex interplay between the atomic site and the physicochemical properties of the support and that decoupling these contributions remains a major challenge. It should also be emphasized here that many metal-free catalysts, especially carbon-based materials, are catalytically active for the ECO<sub>2</sub>RR (see Section 3.2 Metal-free carbon-based electrocatalysts), which further complicates the interpretation of activity trends.

A potential strategy to address the discrepancies is the application of advanced *in situ/operando* spectroscopic techniques capable of resolving reaction intermediates under realistic electrochemical conditions. We believe that by directly tracking adsorbed species and identifying the rate-determining steps, the field can move beyond purely thermodynamic DFT predictions, which often neglect alternative pathways and dynamic effects under operating conditions. At the same time, the current understanding of the role of the supporting material remains limited. In this regard, *in situ/operando* characterization will be essential not only to determine the intrinsic activity

of CuN<sub>4</sub> sites, but also to understand why their catalytic properties vary so markedly depending on other factors such as the local coordination environment, the supporting material, and the surrounding reaction microenvironment.

Nevertheless, given the current lack of mechanistic consensus, many studies have adopted an empirical approach by tuning the local environment of the SAC's metal centers to directly modulate ECO<sub>2</sub>RR selectivity. The introduction of B atoms into the local coordination of the Cu single atoms, especially in the Cu–N<sub>2</sub>B<sub>2</sub> configuration, results in a significant increase of the catalyst's selectivity towards  $\text{CH}_4$  formation, with a FE of 73% at a partial current density of ~292 mA cm<sup>-2</sup>,<sup>98</sup> as opposed to only 30%  $\text{CH}_4$  at barely 100 mA cm<sup>-2</sup> at the same potential (-1.46 V vs. RHE) for the analogous Cu–N<sub>4</sub>-based material. The authors attribute this improvement brought about by the introduction of B to a lower energy requirement for the \*CO to \*CHO thermodynamic barrier.

Interestingly, similar effects were found when introducing a low concentration (5% on a catalyst weight basis) of Cu single atoms in CeO<sub>2</sub> nanorods. Such an addition induced a substantial increase in the  $\text{CH}_4$  selectivity up to a FE of 58% due to the creation of oxygen vacancies surrounding the Cu–N<sub>4</sub> sites.<sup>99</sup> Similarly, the introduction of oxygen atoms coordinated directly to the Cu single atoms (*i.e.* in the form of CuN<sub>2</sub>O<sub>2</sub>) can also efficiently modify the electronic structure of the metal center for reducing the thermodynamic barriers towards  $\text{CH}_4$  formation.<sup>100</sup> As a result, the CuN<sub>2</sub>O<sub>2</sub>-containing electrocatalysts show a superior  $\text{CH}_4$  selectivity with a FE of 78% at -1.44 V with a total current density of 40 mA cm<sup>-2</sup>.

In summary, the modulation of chemistry in the local coordination or vicinity of Cu–N<sub>4</sub> sites seems to be a promising strategy to reach high selectivities towards  $\text{CH}_4$  formation. Further studies with different heteroatoms, defect engineering and pioneering synthesis strategies are mandatory to obtain even more selective materials and a better understanding of the mechanisms behind these phenomena.

**3.1.1.3 Cu-based bimetallic electrocatalysts.** The electrocatalytic activity of  $\text{CO}_2$ -to- $\text{CH}_4$  electrochemical conversion appears to be related to the linear relationship between the adsorption energies of \*CO and \*CHO intermediates, which restricts selectivity towards  $\text{CH}_4$  formation. The inclusion of a second metal either in the form of a single atom (using the so-called dual-site configuration) or through the alloying of metallic Cu with a second element can provide a new degree of freedom to modulate this adsorption energy difference, allowing better selectivity towards  $\text{CH}_4$ .<sup>101</sup>

Dual Cu adjacent sites have also been proposed as a promising pathway to increase selectivity towards hydrocarbon products.<sup>89,103</sup> Although this system is not strictly a bimetallic material, we find it useful to include it in this section because the results of adding an additional Cu atom closely resemble those observed in bimetallic materials rather than in single-atom Cu catalysts. In dual-site Cu catalysts, two neighboring Cu atoms are anchored onto a support and work cooperatively to enhance  $\text{CO}_2$  reduction activity. In these systems, Cu atoms serve as active sites for \*CO<sub>2</sub> adsorption and when two \*CO<sub>2</sub> intermediates are adsorbed close to each other, the proximity



significantly favors C–C coupling reactions, leading to the formation of hydrocarbons, especially  $C_{2+}$  products.<sup>103</sup> Such a synergistic effect of dual Cu sites was further demonstrated through the tuning of the distance between neighboring Cu sites, which modulated selectivity to different hydrocarbons, allowing the formation of  $C_{2+}$  products. At Cu concentrations above 4.9 mol%, the distance between adjacent  $CuN_4$  species was close enough to enable C–C coupling of  $ECO_2RR$  intermediates, resulting in high selectivity towards  $C_2H_4$ .<sup>104</sup> In contrast, concentrations below 2.4 mol% demonstrated high selectivity towards  $CH_4$ .<sup>104</sup> Thus, the metal content and corresponding distance between  $CuN_4$  sites are of high relevance for product selectivity.

In the case of bimetallic alloys, a large number of studies have tried to overcome the low selectivity of Cu-based electrocatalysts for the formation of  $CH_4$  through the synthesis of Cu-based bimetallic alloys. More precisely, trace amounts (from 0 to 7 at%) of oxophilic metals (La, Pr, Y, and Sm) were introduced into a pure Cu matrix for evaluating  $ECO_2RR$  performance.<sup>102</sup> As observed in Fig. 5A, DFT calculations showed that the oxophilicity of the alloying metal correlates strongly with the adsorption energy of  $^*CHO$ , which is known to be a key parameter for  $ECO_2RR$  selectivity. Experimentally, the

introduction of La into the Cu structure in a  $La_5Cu_{95}$  ratio resulted in an excellent partial current density of  $194\text{ mA cm}^{-2}$  (Fig. 5B) with a high FE towards  $CH_4$  of 64.5% at  $300\text{ mA cm}^{-2}$  (Fig. 5C). This is attributed to the alloying of Cu with La, which not only stabilizes the  $^*CHO$  intermediates, but also promotes the splitting of the C–O bond in the  $^*CH_3O$  reaction intermediate by forming a stable La–O bond (Fig. 5D). Similar conclusions were found through the introduction of Bi into a Cu aerogel,<sup>105</sup> which resulted in the variation of the  $Cu^{2+}/Cu^+$  ratio on the electrocatalyst surface and in turn led to different FEs towards  $ECO_2RR$  products (Fig. 6A). In particular, the highest FE towards  $CH_4$  was obtained for a  $Cu_{50}Bi$  material that displayed a FE towards  $CH_4$  of 26% at a total current density of  $150\text{ mA cm}^{-2}$ . Additionally, as observed in Fig. 6B, the tuning of the  $Cu_xBi$  composition leads to a significant modification of the  $ECO_2RR$  selectivity, with FEs towards CO above 80% in the case of  $Cu_{100}Bi$ , or 60% FE towards formate with  $Cu_5Bi$ . Interestingly, the higher  $Cu^{2+}/Cu^+$  ratio increased significantly the selectivity for  $CH_4$  formation, hypothetically due to favoring of the hydrogenation of reaction intermediates.

Another interesting study tried to integrate H-affine elements within Cu. Although platinum-group elements are known for their high HER-selectivity, when atomically

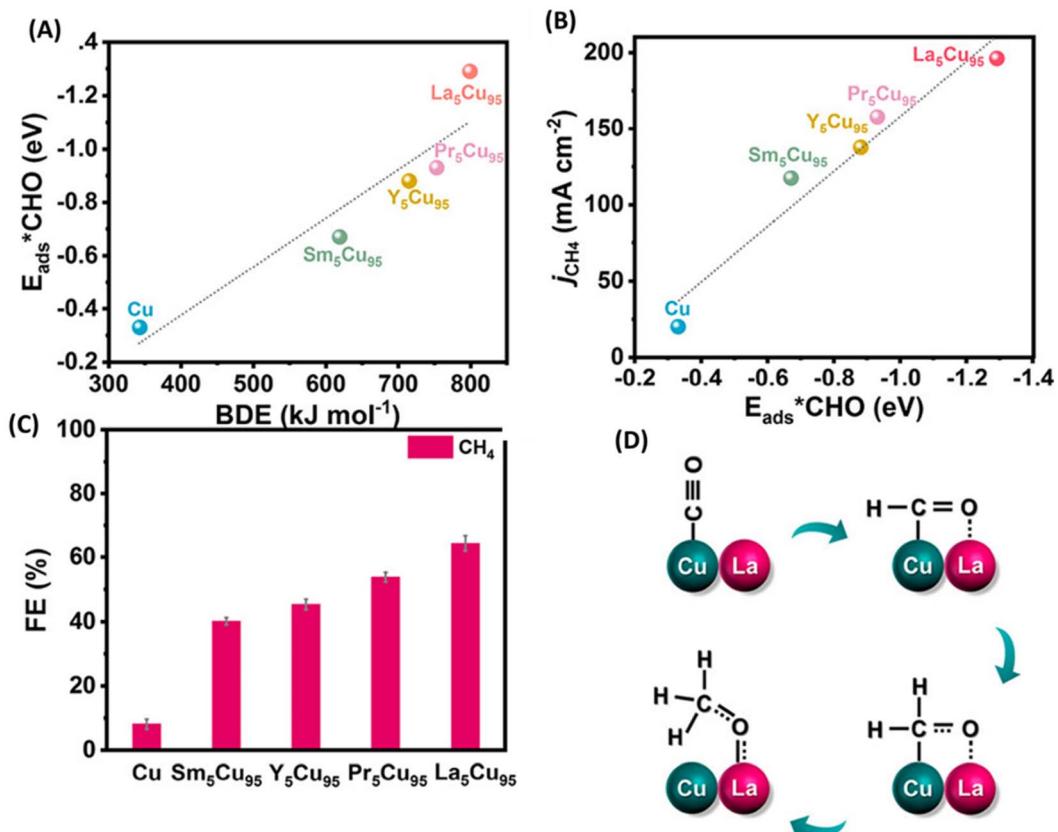


Fig. 5 (A) Relationship between calculated  $*CHO$  adsorption energy (energy required to convert one molecule from the lowest adsorbed state to the lowest gaseous state) and the bond dissociation enthalpy (BDE) of the metal–oxygen bond. (B) Relationship between the partial current density of  $CH_4$  at a total current density of  $300\text{ mA cm}^{-2}$  (in  $CO_2$ -saturated  $1\text{ M KOH}$  solution) and the adsorption energy of  $*CHO$  for Cu and  $M_5Cu_{95}$  electrocatalysts. (C) FE of  $CH_4$  on Cu and  $M_5Cu_{95}$  electrocatalysts at a total current of  $300\text{ mA cm}^{-2}$ . (D) Proposed reaction pathways of the  $ECO_2RR$  to  $CH_4$  on the  $La_5Cu_{95}$  surface. Reproduced from ref. 102 with permission from the American Chemical Society, copyright 2023.



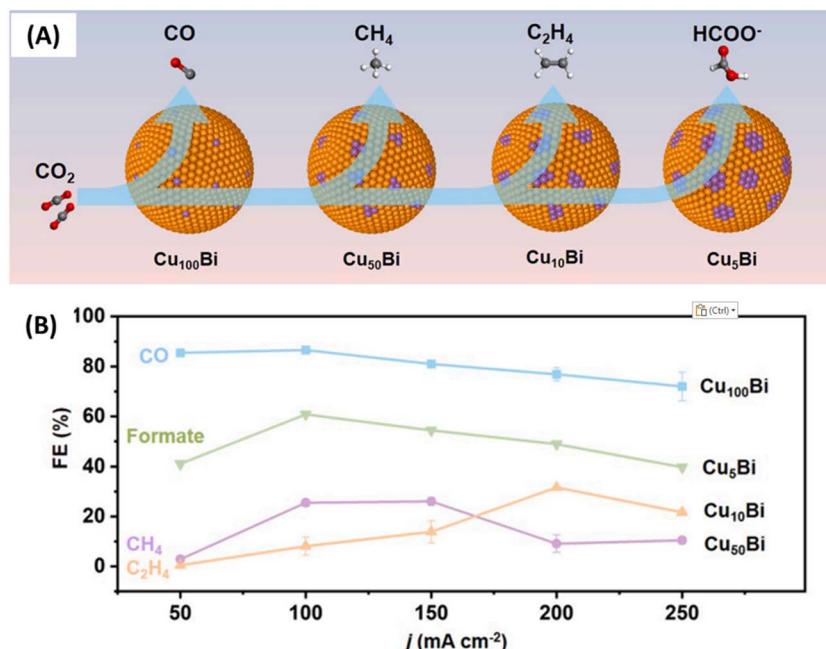


Fig. 6 (A) Product distribution of the ECO<sub>2</sub>RR with different Cu<sub>x</sub>Bi compositions. (B) Electrocatalytic performance (in CO<sub>2</sub>-saturated 1 M KOH solution) of the corresponding Cu<sub>x</sub>Bi aerogels, showcasing the FE (%) for ECO<sub>2</sub>RR products at different applied current densities for Cu<sub>100</sub>Bi, Cu<sub>50</sub>Bi, Cu<sub>10</sub>Bi and Cu<sub>5</sub>Bi. Reproduced from ref. 105 with permission from Elsevier, copyright 2022.

dispersed platinum atoms are integrated into a shape-controlled Cu catalyst, they increase the selectivity towards hydrocarbon products. For instance, Pt-group single atoms act as H\* donors and facilitate the hydrogenation of \*CO intermediates in polycrystalline Cu surfaces.<sup>106</sup> The incorporation of Pd single atoms into Cu-based electrocatalysts led to an increase in the CH<sub>4</sub> partial current density from 2.3 to 118 mA cm<sup>-2</sup> (Fig. 7A), with an improvement of FE towards CH<sub>4</sub> from 2 to 60% at  $-1.1$  V vs. RHE (Fig. 7B). Moreover, the alloy phase morphology is also relevant, since spherical or cubic structures resulted in high C<sub>2+</sub> yields, whereas octahedral structures promoted CH<sub>4</sub> formation (Fig. 7C). Chiefly, this strategy of adjusting the metal nature and metal doping to tune the \*CHO adsorption energy can be extended to increase the hydrocarbon selectivity of Cu electrocatalysts towards products other than CH<sub>4</sub>.<sup>107,108</sup>

**3.1.2. Silver-based electrocatalysts.** Ag-based electrocatalysts are of the greatest interest for CO production because of this metal's relatively low cost (particularly when compared with noble metals) and high selectivity for this product.<sup>109</sup> This is why most of the studies that focus on Ag electrocatalysts for the ECO<sub>2</sub>RR do so with a strong focus on CO production. However, the size, crystal structure and morphology of silver (nano)catalysts can further tune their ECO<sub>2</sub>RR performance. As a result, Ag-based electrocatalysts in which the properties of the pristine metal have been tuned through the addition of a second metal phase have recently emerged as a promising approach for the electrochemical conversion of CO<sub>2</sub> into CH<sub>4</sub>.

As an example of this, a 2017 study showed that Ag-Co bimetallic electrocatalysts with electronic properties different

from those of the monometallic Ag counterpart featured a methane FE of 20% at an applied voltage of 2.0 V (vs. nearly 0% for the monometallic catalyst) thanks to the atomic rearrangement and concomitant tuning of the binding strength of the \*CO intermediate, which favors CH<sub>4</sub>.<sup>110</sup> Specifically, Co atoms provide free electrons to the vacant orbitals in Ag, forming Ag-Co bonds that induce large changes in the electron density of the metals and shift ECO<sub>2</sub>RR selectivity towards CH<sub>4</sub> instead of CO. Similarly, the deposition of a N<sub>x</sub>C shell surrounding the Ag nanoparticles also serves to tune product selectivity,<sup>111</sup> in this case not through a modification of silver's electronic properties, but by prolonging the residence time of the \*CO intermediate on the catalyst's surface and increasing the number of hydrogenation reactions. As a result, the FE for CH<sub>4</sub> formation was enhanced above 44% after the creation of the N<sub>x</sub>C nanoshell, as compared to nearly 0% in the absence of the latter (*i.e.*, for bare Ag nanoparticles).

In summary, although there are not many studies that focus on modifying the ECO<sub>2</sub>RR selectivity of Ag electrocatalysts, the few studies discussed above demonstrate that tuning silver's properties can also be a promising strategy towards CH<sub>4</sub> formation.

**3.1.3. Cobalt-based electrocatalysts.** DFT computations indicate that the chemisorption of the \*CO<sub>2</sub> intermediate is the rate-limiting step for the ECO<sub>2</sub>RR on Co<sub>4</sub>N sites.<sup>112</sup> While CO is the main product for such Co-based electrocatalysts,<sup>113</sup> CH<sub>4</sub> is eventually produced in minor amounts due to the hydrogenation of the \*CO intermediate. This is confirmed experimentally, since a FE towards CO of 97–99% was obtained when investigating Co phthalocyanine as the ECO<sub>2</sub>RR active site, and



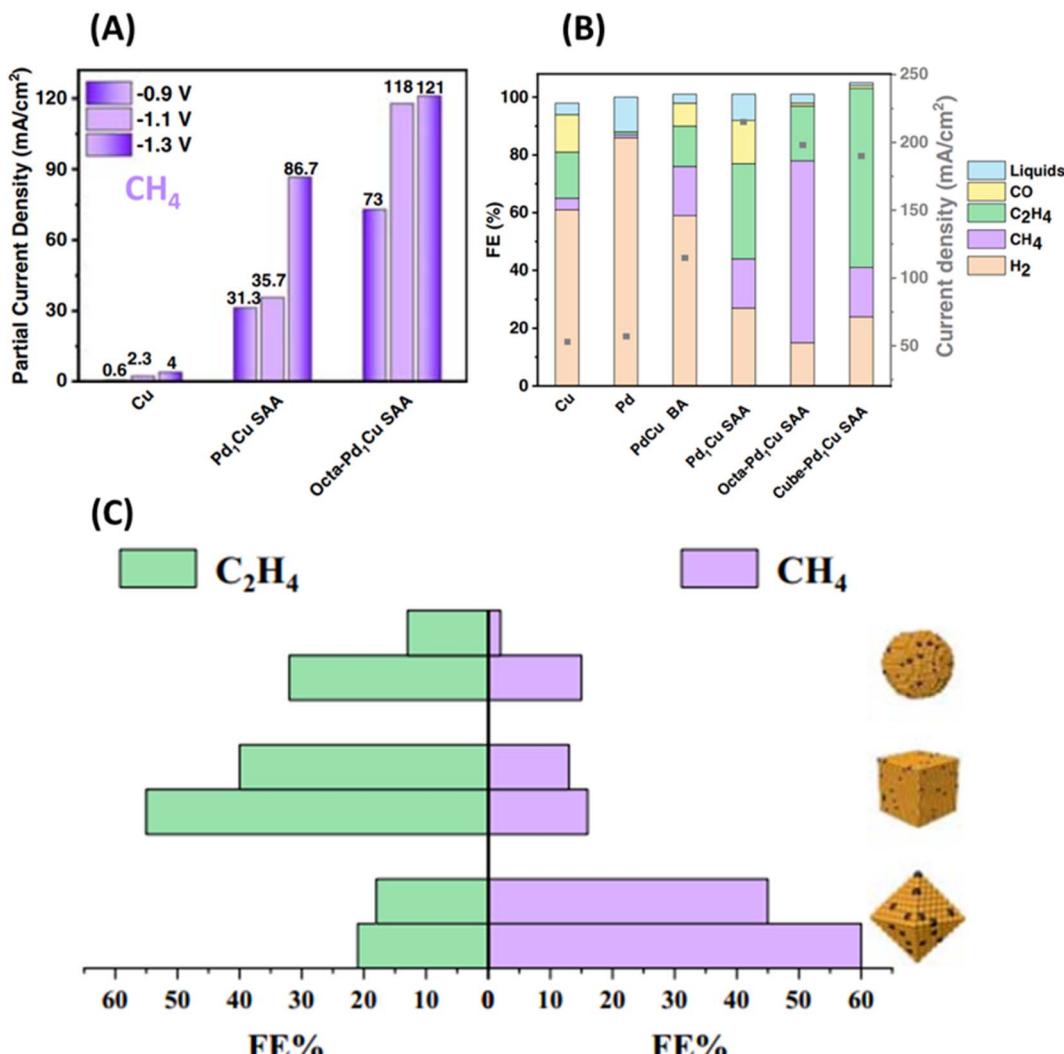


Fig. 7 (A) Partial current density for CH<sub>4</sub> at different voltages for polycrystalline Cu, polycrystalline Pd<sub>1</sub>Cu configuration and shape-controlled Octa-Pd<sub>1</sub>Cu configuration. SAA stands for single-atom alloys. (B) Comparison of CO<sub>2</sub> reduction FE (%) and current densities of Pd<sub>1</sub>Cu configuration and analogues. The FE was obtained from amperometric *i*-*t* curves at -1.1 V vs. RHE (in a CO<sub>2</sub>-saturated 0.5 M KHCO<sub>3</sub> solution) and quantifying the products over 30 min. (C) FE distribution of CH<sub>4</sub> and C<sub>2</sub>H<sub>4</sub> obtained using Cu and shape controlled Pd<sub>1</sub>Cu materials. Reproduced from ref. 106 with permission from Springer Nature, copyright 2023.

negligible formation of CH<sub>4</sub> was observed.<sup>76,114</sup> Nevertheless, even if the majority of Co-based ECO<sub>2</sub>RR electrocatalysts are designed for CO production, strategies again exist to improve their selectivity towards CH<sub>4</sub>.

For instance, electrochemical CO<sub>2</sub>-to-CH<sub>4</sub> conversion has been achieved when employing photo-assisted electrochemical methods.<sup>115</sup> The addition of light illumination during electrocatalysis promotes the stabilization of the \*CO intermediate adsorbed on the Co-N<sub>4</sub> sites, allowing its subsequent hydrogenation to yield CH<sub>4</sub>. Along these lines, the incorporation of Co phthalocyanine into Zn-N-C materials caused a 100-fold enhancement in the selectivity of the latter materials towards CH<sub>4</sub> formation.<sup>116</sup> DFT calculations revealed that the first reduction of CO<sub>2</sub> molecules occurs at the Co-N<sub>4</sub> sites, but the resulting \*CO intermediate is transferred onto the Zn-N<sub>4</sub> sites for further conversion into CH<sub>4</sub>.<sup>116</sup>

Interestingly, a strong effect of the supporting electrolyte was also observed in Co porphyrins.<sup>117</sup> Cation size affects the reaction in two ways: large cations, such as K<sup>+</sup>, enhance the HER because smaller cations retain more water, creating steric hindrance that slows H<sup>+</sup> diffusion. Conversely, small cations, such as Li<sup>+</sup>, stabilize the key intermediate of CO<sub>2</sub> reduction through ion pairing, facilitating the conversion of CO<sub>2</sub> into CO and CH<sub>4</sub>.<sup>117</sup>

**3.1.4. Fe-based electrocatalysts.** Fe is among the most promising transition metals for catalyzing many electrochemical reactions due to its high abundance and corresponding low cost.<sup>118-121</sup> This means that tuning the electronic properties of Fe electrocatalysts is not a new strategy in materials science, but how this approach affects these materials' ECO<sub>2</sub>RR performance is still unknown. Furthermore, the poor HER activity of Fe-based electrocatalysts (typically requiring



overpotentials  $> 400$  mV (ref. 82)) underscores the capabilities of these electrocatalysts for promoting  $\text{CO}_2$  electroreduction over  $\text{H}_2$  production.

Iron, especially in the form of single atoms with an  $\text{FeN}_4$  coordination, is known to electrochemically reduce  $\text{CO}_2$  to CO with high selectivity (*i.e.*, a FE  $> 90\%$ ).<sup>122–124</sup> The correspondingly poor selectivity towards  $\text{CH}_4$  formation is mainly associated with the isolated nature of the  $\text{FeN}_4$  active sites. Computations indicate that the  $\text{ECO}_2\text{RR}$  in  $\text{FeN}_4$  sites can indeed proceed beyond CO.<sup>125</sup> Specifically, since  $\text{FeN}_4$  sites are excellent CO producers and therefore can form a large amount of \*CO intermediates, these reaction intermediates can be further reduced until yielding hydrocarbons. However, this work suggested that highly active  $\text{CH}_4$  formation may require an extended surface or nearby proton source to lower the protonation barrier.<sup>125</sup>

We are only aware of one study in which Fe exhibited  $\text{CH}_4$  formation.<sup>126</sup> This work explored structure–activity relations in  $\text{FeN}_4$  catalysts, revealing that the catalytic activity is strongly influenced by the nitrogen functionalities. Specifically, XPS data suggested that pyridinic N and  $\text{FeN}_4$  moieties serve as active sites, as they promote  $\text{CO}_2$  adsorption and facilitate electron transfer. *Operando* EXAFS results indicated a change in the Fe oxidation state from  $\text{Fe}^{2+}$  to  $\text{Fe}^{1+}$  at potentials of approximately  $-0.9$  to  $-1.1$  V *vs.* RHE, coinciding with the onset of  $\text{CH}_4$  production. The authors attributed this  $\text{CH}_4$  formation to the  $\text{FeN}_4$  sites with the Fe atom in the +1 oxidation state. While  $\text{CH}_4$  production remained very low (<1%), this redox transition offers a potential pathway to enhance the  $\text{CO}_2$ -to- $\text{CH}_4$  activity of  $\text{FeN}_4$  sites by tuning their electronic configuration.

### 3.2 Metal-free carbon-based electrocatalysts

In the pursuit of low-cost  $\text{ECO}_2\text{RR}$  electrocatalysts, metal-free carbon-based materials have emerged as an excellent alternative to those containing metals.<sup>28,127,128</sup> Nevertheless, even if these metal-free electrocatalysts have been extensively proven to be effective for other electrochemical reactions such as oxygen reduction<sup>129,130</sup> and hydrogen evolution,<sup>130,131</sup> their  $\text{ECO}_2\text{RR}$  performance is still far from that of metal-containing materials. Pristine, undoped carbon materials exhibit minimal catalytic activity towards the  $\text{ECO}_2\text{RR}$  because the electron density across their carbon layers is homogeneously distributed.<sup>132</sup> A common strategy to improve this poor catalytic performance involves altering and tuning their electronic properties through the introduction of heteroatoms, surface functionalities, and defect engineering and curvature. Incorporating functional groups or defects into the basal plane of the carbon layers usually induces a redistribution of electron density through electron withdrawal-donation effects that localize the charge in carbon atoms adjacent to defects or heteroatoms. This electron delocalization near heteroatoms tends to attract the reagent molecule more easily, and when the molecule is chemically adsorbed at the active sites, the polarization of the carbon electrode induces its subsequent reduction.

Nitrogen is the most commonly studied heteroatom when it comes to doping carbon materials due to its similar size to

carbon, but also because of its larger electronegativity (3.04 for N and 2.55 for C). N-doped carbon materials have proven to be effective electrocatalysts for multiple electrochemical reactions, including the  $\text{ECO}_2\text{RR}$ . Nitrogen atoms can be incorporated into carbon materials in the form of different functionalities that can be classified according to their binding energies:<sup>133–135</sup> pyridinic-N (398.4 eV), pyrrolic/pyridonic-N (400.3 eV), graphitic-N (also called quaternary-N, 401.2 eV) and oxidized-N (402.9 eV). In general, the defects located at the edge of the carbon layers are assumed to be more active than those at the basal plane, with N-doped zigzag species being the most active site among these.<sup>136</sup> Fig. 8a shows HRTEM images of N-doped graphene quantum dots (NGQDs) 1–3 nm in size that were prepared through exfoliating and cutting graphene oxide with *in situ* N doping. The N 1s XPS spectrum confirmed the N doping in the form of pyridinic, pyrrolic and graphitic N species (Fig. 8B). Pristine non-doped GQDs showed indeed moderate  $\text{ECO}_2\text{RR}$  activity thanks to their large edge density, with a current density of around  $10 \text{ mA cm}^{-2}$  at  $-0.85 \text{ V}$  *vs.* RHE and high selectivity towards CO (FE = 10%) and  $\text{HCOO}^-$  (FE = 6%).<sup>137</sup> However, the high N content at the basal plane of NGQDs resulted in a significant improvement of the catalytic activity with a current density of  $100 \text{ mA cm}^{-2}$  at the same potential and enhanced selectivity for  $\text{CH}_4$  and  $\text{C}_2\text{H}_4$  products (Fig. 8C and D).<sup>137</sup> Among such N species, pyridinic functional groups appear to be responsible for variations in the selectivity in metal-free carbon-based electrocatalysts, as this edge-type N species substantially decreases the energy barrier for the formation of the \*COOH intermediate, which mainly leads to CO production.<sup>138,139</sup> For high  $\text{CH}_4$  or  $\text{C}_2\text{H}_4$  production, N species located in the basal plane, such as graphitic N, appear to be the most promising in terms of selectivity. However, for graphitic N, the extra electron located in the  $\pi^*$  antibonding orbital is less accessible for  $\text{CO}_2$  chemisorption, as proved by the 1 eV higher chemisorption energy of graphitic N when compared to pyridinic N.<sup>140</sup> Nevertheless, even with this thermodynamic barrier, graphitic N remains better than the N-free, pristine carbon, as demonstrated by its better  $\text{ECO}_2\text{RR}$  activity.<sup>140</sup>

Here it is worth noting that both graphitic and pyridinic N induce an electron withdrawal effect in the adjacent carbon atoms, which leads to a redistribution of the charge density in the carbon matrix.<sup>139–141</sup> This results in a negative electron density in the N atom and a corresponding positive charge density in the first neighbor carbon atoms. These negatively charged sites act as active centers onto which the positively charged C atoms from the  $\text{CO}_2$  molecules chemisorb, forming a N– $\text{CO}_2$  intermediate. In the case of pyridines, the chemisorption occurs *via*  $\text{sp}^2$ -to- $\text{sp}^3$  hybridization, facilitating  $\text{CO}_2$  chemisorption. However, graphitic N already forms three chemical bonds with adjacent carbon atoms, making the creation of an additional chemical bond with the  $\text{CO}_2$  molecule highly energy demanding. This is why the carbon atoms in the vicinity of the N functionality are considered the active sites in the case of graphitic N groups. However, in modelling graphitic N, C– $\text{CO}_2$  chemisorption is often proposed on the carbon atom located in the *ortho* position,<sup>142</sup> which appears unlikely when considering these C atoms' positive charge



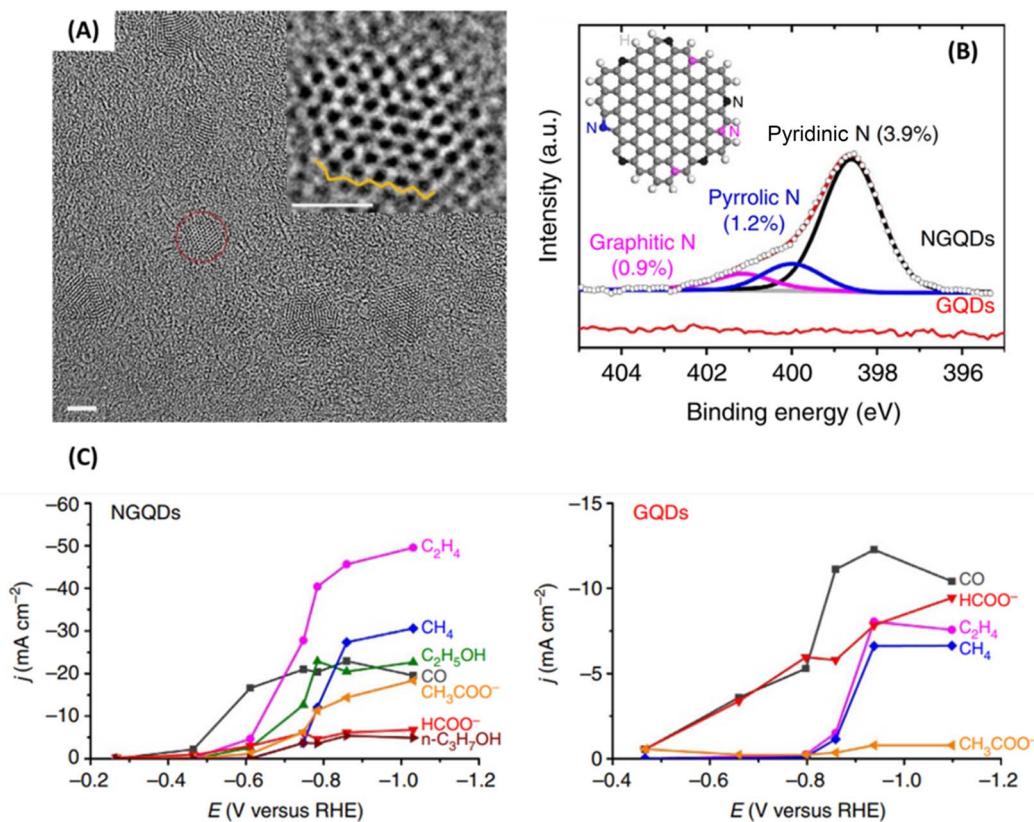


Fig. 8 (A) TEM image of NGQDs (scale bar, 2 nm), with the inset showing a high magnification image of a single NGQD containing zigzag edges outlined by the yellow line (inset scale bar, 1 nm). (B) N 1s XPS spectrum of the NGQD sample, deconvoluted into pyridinic, pyrrolic and graphitic N. The value in parentheses is the corresponding N atomic concentration. (C) Partial current densities as a function of the cathode potential for various electrochemical  $\text{CO}_2$  reduction products when using NGQDs (left) and GQDs (right) as the electrocatalysts. Reproduced from ref. 137 with permission from Springer Nature, copyright 2016.

induced by the N functionality. Therefore, it is anticipated that the active sites involve the C atom in the *meta* position to the N through a C– $\text{CO}_2$  interaction or the C atom in the *ortho* position through interaction with the oxygen atoms of the  $\text{CO}_2$  molecule through a C–OCO intermediate. As such, further studies are mandatory to unravel the mechanisms behind the ECO<sub>2</sub>RR in N-doped carbon materials.

Other heteroatom elements have also been studied as doping agents in carbon materials, such as B,<sup>143–145</sup> F,<sup>146,147</sup> P<sup>148–151</sup> or S.<sup>152,153</sup> Furthermore, heteroatom doping with these elements has also been carried out with the aim of tuning the electronic structure of the carbon layers and inducing larger electron delocalization for further ECO<sub>2</sub>RR studies. One particularly interesting article claimed to reach a FE towards  $\text{CH}_4$  formation of 99% with an F- and N-codoped carbon material.<sup>154</sup> However, this high selectivity was only reached with a very low current density of 0.2 mA cm $^{-2}$ . Recently, adjacent N and B atoms in N- and B-codoped carbon materials have also demonstrated high  $\text{CH}_4$  selectivity (*i.e.*, a FE of 68%) and a current density of  $\approx$ 15 mA cm $^{-2}$  at  $-0.5$  V vs. RHE.<sup>155</sup>

In summary, metal-free heteroatom-doped carbon materials are still at the earliest stage of development as ECO<sub>2</sub>RR-electrocatalysts. As observed in Table 2, their overall current density remains far below that of metal-containing

electrocatalysts, with the best reported current density reaching 40 mA cm $^{-2}$  so far. This large performance gap raises critical questions regarding their practical scalability. Nevertheless, an intriguing characteristic emerges when comparing both families of catalysts. While metal-containing electrocatalysts require very negative potentials to achieve  $\text{CH}_4$  formation, metal-free electrocatalysts can achieve high FE for  $\text{CH}_4$  already at moderate potentials between  $-0.5$  and  $-0.9$  V vs. RHE. This suggests that, although less active in absolute terms, metal-free catalysts may intrinsically demand lower overpotentials to trigger efficient C–H bond formation. Importantly, long-term stability under operating conditions has not yet been demonstrated for metal-free catalysts, which remains a major barrier for their practical applications. Further advances in catalyst design and mechanistic understanding are therefore mandatory to assess whether such features can be leveraged for scalable and competitive implementation.

## 4 Electrochemical $\text{CO}_2$ electrolyzers

The ECO<sub>2</sub>RR performance is not only influenced by the selection of the electrocatalyst, but also by the design of the electrochemical reactor (commonly referred to as a  $\text{CO}_2$  electrolyzer) where  $\text{CO}_2$  is converted into a value-added product. From an industrial perspective, one of the most crucial

requirements for the practical deployment of  $\text{CO}_2$  electrolyzers is their ability to operate at high current densities, typically at least  $200 \text{ mA cm}^{-2}$ . Achieving such high current densities is essential for ensuring economically viable reaction rates and maximizing  $\text{CO}_2$  conversion efficiency at scale. However, maintaining high activity while preserving selectivity and stability poses significant engineering challenges, as it requires optimizing not only the catalyst, but also the overall reactor architecture (including the balance of plant), mass transport properties and ion management.

The geometry of the  $\text{CO}_2$  electrolyzer, including the electrode and electrolyte configurations, plays a crucial role in determining the mass transfer efficiency of the gaseous reactant and the reaction products. These factors have a direct impact on key performance metrics, such as electrocatalytic selectivity, long-term stability and overall  $\text{CO}_2$  conversion efficiency. While extensive research has been dedicated to the development and optimization of electrocatalysts to enhance  $\text{CO}_2$  reduction activity and selectivity, less attention has been paid to the practical implementation of these catalysts in application-relevant  $\text{CO}_2$  electrolyzers, and comparatively fewer studies can be found on this important topic.

Before delving into the different types of  $\text{CO}_2$  electrolyzers, it is important to highlight the critical role of membranes, which are an essential yet often overlooked component in these systems. Membranes serve multiple key functions, such as enabling ion transport between the electrodes, preventing unwanted product crossover, and maintaining system stability, all of which directly impact the overall efficiency and selectivity of the electrolyzers. Since membranes are an essential component in  $\text{CO}_2$  electrolyzers and exist in various types, it is important to first explain their nature and functions to understand their application in different electrolyzer types.

#### 4.1 Ion exchange membrane (IEM) $\text{CO}_2$ electrolyzers

A fundamental component of any  $\text{CO}_2$  electrolyzer is the membrane, which acts as a selective barrier that regulates the transport of ions between the electrode compartments while preventing the undesired crossover of reactants and products, which can lead to efficiency losses and reduced selectivity.<sup>156</sup> Depending on their ion transport properties, membranes can be classified into three main types: cation exchange membrane (CEM), anion exchange membrane (AEM) and bipolar membrane (BPM). Each of these membrane types has different characteristics that influence the reaction environment and can significantly influence electrolyte pH, ionic conductivity, and product separation, ultimately affecting the performance and feasibility of the system under industrially relevant conditions.<sup>156</sup>

Beyond their electrochemical role, membranes also have a significant economic impact on the viability of  $\text{CO}_2$  electrolyzers. The choice of IEM not only dictates performance metrics but also plays a crucial role in determining operational costs, particularly in large-scale applications. Importantly, these costs are not limited to the intrinsic price of the membrane itself but extend to the entire system configuration that each membrane

requires. Certain membranes impose operational constraints that necessitate additional infrastructure or system modifications to compensate for their drawbacks. A holistic approach was developed to assess and optimize the economic factors involved in the electrochemical conversion of  $\text{CO}_2$  to  $\text{CO}$  based on different IEMs.<sup>157</sup> Although that study did not focus on  $\text{CH}_4$  production, we believe that it properly illustrates the costs associated with each IEM type for electrochemical  $\text{CO}_2$  conversion. Mass and energy balances were computed using state-of-the-art literature data and revealed that 75 to 84% of the total production costs can be attributed to the electrolyzer cost. According to the study,<sup>157</sup> AEMs are expected to be the most suitable membranes for  $\text{ECO}_2\text{RR}$  electrolysis due to the low electricity and capital costs associated with their use, leading to an estimated  $\text{CO}$ -production cost of  $\approx 800 \text{ € t}_{\text{CO}}^{-1}$ . This is closely followed by BPMs, which feature a competitive cost of  $\approx 840 \text{ € t}_{\text{CO}}^{-1}$ , and CEMs with a higher cost of  $\approx 1100 \text{ € t}_{\text{CO}}^{-1}$ .

Given the importance of the membrane choice in both economic and performance terms, it is essential to delve into the specifics of each IEM type. In the following section, we will analyze the characteristics, advantages and challenges associated with each IEM category, providing a comprehensive understanding of how this influences  $\text{CO}_2$  electrolysis systems.

**4.1.1. Cation exchange membranes (CEMs).** Cation exchange membranes (CEMs) are a class of IEMs that selectively allow the passage of cations, such as  $\text{H}^+$  or  $\text{K}^+$ , while blocking the movement of anions. These membranes are widely used in electrochemical systems, including  $\text{CO}_2$  reduction electrolyzers, due to their ability to maintain ionic conductivity and decrease the extent of unwanted crossover of reactants and products.

One of the major challenges of CEMs is the acidic pH at the cathode electrode, which promotes the competitive HER over  $\text{CO}_2$  reduction. To mitigate this limitation, CEM-based  $\text{CO}_2$  electrolyzers, in particular those with electrolyte fed at the anode compartment, can also be operated with a high concentration of  $\text{K}^+$  cations from the electrolyte solution, such as  $\text{KHCO}_3$  or  $\text{K}_2\text{CO}_3$ . The high concentration of  $\text{K}^+$  in the electrolyte leads to the diffusion of  $\text{K}^+$  through the membrane, replacing  $\text{H}^+$  ions at the cathode, and consequently suppressing HER and improving the selectivity for  $\text{CO}_2$  reduction.<sup>158</sup> The resulting pH-buffer effect strongly correlates with the hydration shell of the electrolyte cation, which is in turn associated with its permeability and diffusion coefficients.<sup>159</sup> Considering an inverse relationship between the diffusion coefficient and cation hydration radii, the diffusion coefficient for alkali cations follows the order  $\text{Cs}^+ > \text{K}^+ > \text{Na}^+ > \text{Li}^+$ .<sup>159</sup> This implies that, from a device-operation perspective, maintaining high selectivity towards  $\text{CO}_2$  reduction requires precise control over the electrolyte composition and ion concentration. However, as we will explain later in the  $\text{CO}_2$  electrolyzers section, this strategy is only useful for  $\text{CO}_2$  electrolyzers that employ liquid electrolytes, which introduces several challenges, such as high electrical resistance, limited  $\text{CO}_2$  solubility and concomitantly low current densities.

Another critical concern in CEM-based  $\text{CO}_2$  electrolysis is the crossover of  $\text{CO}_2$  products during operation, which leads to the need for including additional separation and regeneration



processes and would increase these devices' operational complexity. Although  $\text{CO}_2$  crossover is not a significant issue,  $\text{CO}_2$ -derived alcohols, such as methanol and ethanol, are more problematic with regard to crossover due to their high diffusion coefficients in CEMs.<sup>160,161</sup>

**4.1.2. Anion exchange membranes (AEMs).** Anion exchange membranes (AEMs) serve as a key alternative to CEMs in  $\text{CO}_2$  electrolyzers, offering the advantage of selectively allowing the migration of anions, such as  $\text{OH}^-$ ,  $\text{HCO}_3^-$  and  $\text{CO}_3^{2-}$ , while blocking cations. AEMs are particularly advantageous in  $\text{CO}_2$  electrolysis because they create a neutral-to-alkaline environment at the cathode, which promotes the  $\text{CO}_2$  reduction reaction over the HER.<sup>162</sup> As for the nature of the anionic species, while  $\text{OH}^-$  anions are produced from the reduction of  $\text{H}_2\text{O}$  and/or  $\text{CO}_2$  in the cathodic catalyst layer, their reaction with  $\text{CO}_2$  results in carbonate and bicarbonate anions (with the distribution of these species' concentrations being determined by the local pH), and all three species get transported through the AEM to the anode to yield  $\text{H}_2\text{O}$ ,  $\text{O}_2$  and  $\text{CO}_2$  molecules resulting from the oxidation of  $\text{HCO}_3^-$  and/or  $\text{CO}_3^{2-}$ .<sup>163-165</sup> This  $\text{CO}_2$  regeneration at the anode decreases the electrolyzer's net carbon dioxide consumption and makes it mandatory to put into place additional separation steps that substantially increase the electrolyzer cost<sup>166</sup> and can be more energy-demanding than the  $\text{CO}_2$  electrolyzer itself.<sup>163-165</sup> Indeed, the separation of the  $\text{CO}_2$  that has crossed the membrane to the anode compartment is estimated to be  $\approx 1.6$  times more energy demanding than the  $\text{ECO}_2\text{RR}$  step.<sup>167</sup>

Similar to what was discussed above for CEM-based  $\text{CO}_2$  electrolyzers, the crossover of products from the cathode to the anode is a major bottleneck for AEM  $\text{CO}_2$ -electrolysis development. Indeed, it has been reported that more than 30% of all cathodic liquid products cross the AEM to the anode compartment.<sup>168</sup> This crossover increases linearly with current density and  $\text{CO}_2$  flow rate and makes it significantly difficult to obtain high energy efficiencies. However, this product crossover is minimized when the targeted product is not a liquid but a gas, such as  $\text{CH}_4$ , although crossover of volatile products through the GDE can also occur through evaporation.<sup>168</sup> Nevertheless, the high selectivity and efficiency of AEM-based electrolyzers compared to CEM-based ones nearly compensate for such a substantial extra cost of recycling  $\text{CO}_2$  from the anode.<sup>162</sup> This advantage stems from AEM electrolyzers' neutral-to-alkaline operative pHs in the cathode electrode, which mitigate the acidic conditions that facilitate the HER over the  $\text{CO}_2\text{RR}$  in CEM-based devices (*vide supra*).<sup>169</sup> This is also advantageous for the counter reaction in the anode, the oxygen evolution reaction (OER), since CEMs' acidic conditions limit the choice of OER electrocatalytic materials to scarce and expensive Ir oxides, which would jeopardize the system's upscale potential due to their high costs.<sup>170</sup> Instead, such medium-to-high pHs at the anode allow the use of OER electrocatalysts based on non-precious metals such as Co or Ni, which drastically reduces the electrolyzer price.<sup>171-173</sup>

Palladium-based and Cu-based electrocatalysts were tested as cathode electrodes for the  $\text{ECO}_2\text{RR}$  in AEM-based flow cell electrolyzers.<sup>174</sup> The Pd electrocatalysts showed a FE towards CO

of 98% with a current density of  $200 \text{ mA cm}^{-2}$ . Similarly, Cu electrocatalysts were evaluated under the same conditions, with a FE of 82% towards hydrocarbons with a current density of  $350 \text{ mA cm}^{-2}$ . The electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  reduction reaction is, however, less studied in AEM-type electrolyzers. Nevertheless, a few studies have proven that the alkaline pH of AEM-type electrolyzers can also lead to high selectivity towards  $\text{CH}_4$  formation, with FEs of 62 to 73%.<sup>88,175</sup>

**4.1.3. Bipolar membranes (BPMs).** The above limitations regarding product and ion crossover have recently been reported to be reduced through the use of bipolar membranes (BPMs), which in their simplest version consist of an AEM and a CEM laminated against each other.<sup>156,171,176,177</sup> It is worth mentioning that two configurations can be applied when implementing a BPM in a  $\text{CO}_2$  electrolyzer. First, in the so-called reverse bias (RB) mode that has become the most common configuration in  $\text{CO}_2$  electrolysis, the anion- and cation-exchange layers (AEL and CEL) are disposed at the anode and cathode compartments, respectively (Fig. 9). Moreover, water is split at the CEM-AEM interface, which therefore acts as a  $\text{H}^+$  and  $\text{OH}^-$  donor. The protons obtained from the water splitting are transported through the CEL to the  $\text{ECO}_2\text{RR}$  electrocatalyst and react with the reduced species obtained from the  $\text{ECO}_2\text{RR}$ . On the other side,  $\text{OH}^-$  anions obtained from the water split at the BPM junction are transported by the AEL to the OER electrocatalysts, where they react with the oxidized species of the anode electrode.

Large current densities have been obtained in the RB-BPM mode. Co phthalocyanine was reported as an excellent electrocatalyst for the  $\text{ECO}_2\text{RR}$  in a RB-BPM-type electrolyzer, reaching a CO FE of 62% at a current density of  $200 \text{ mA cm}^{-2}$  with aqueous  $\text{CO}_2$ -saturated 1 M KOH anolyte.<sup>178</sup> The use of KOH as the anode electrolyte produces cation crossover that can damage the electrochemical devices. If KOH is substituted with pure water, the current density is reduced to  $100 \text{ mA cm}^{-2}$  for a similar FE at the same potential. Ni-based electrocatalysts were also tested in RB-BPM mode, with lower CO selectivity (FE of 30%) with a high current density of  $100 \text{ mA cm}^{-2}$ .<sup>179</sup> Interestingly, Cu-based electrocatalysts were also evaluated in this configuration,<sup>180</sup> with significant selectivity towards multi-carbon products ( $\text{C}_{2+}$  FE of 25%) at a current density of  $100 \text{ mA cm}^{-2}$ . At higher current densities, the HER predominates over CO or multicarbon selectivity.

The second configuration of the BPM electrolyzer is the so-called forward bias (FB) mode, in which the CEM is located in the anode and the AEM is in the cathode, thus contrary to the RB-BPM case (see Fig. 9). This approach has gained attention in the last few years due to the suppression of  $\text{CO}_2$ -crossover drawbacks and the elimination of low pHs in the cathode. Regarding the former, the carbonate and bicarbonate anions generated at the cathode are transported by the BPM's AEM towards the CEM-AEM interface, where they recombine with  $\text{H}^+$  obtained from the anodic water electrolysis and transported by the CEM to form water and  $\text{CO}_2$ . Experiments showed the absence of  $\text{CO}_2$  gas in the anode electrode, implying that the gas formed at the AEM-CEM interface diffuses back to the cathode compartment, thus successfully inhibiting net  $\text{CO}_2$  crossover, as



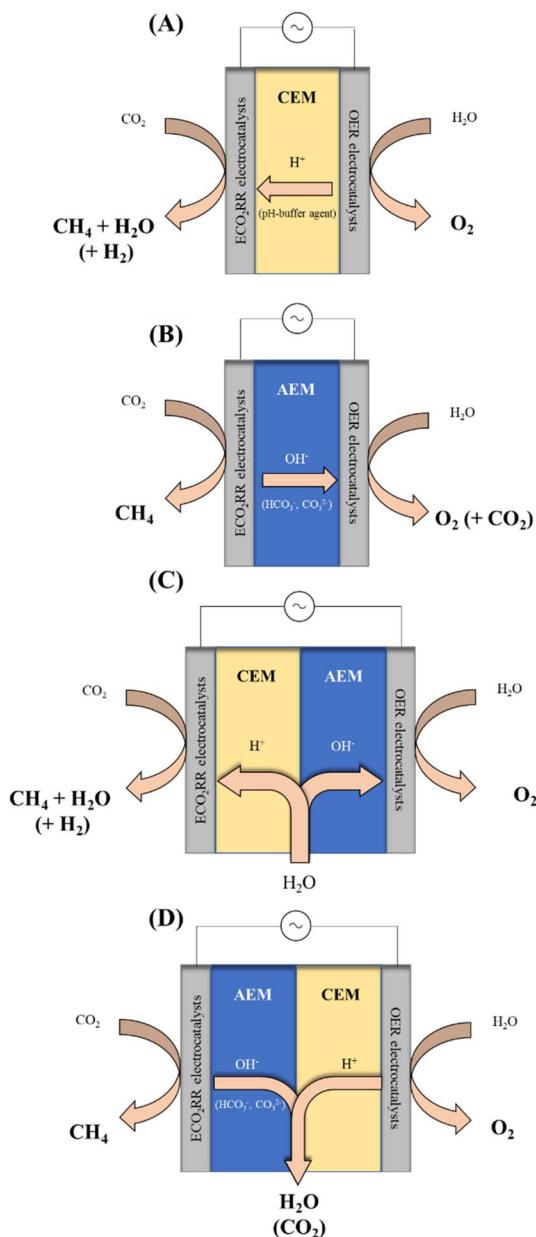


Fig. 9 Schematic representation of an ion exchange membrane in  $\text{CO}_2$  electrolyzers. (A) Cation exchange membrane (CEM)-type electrolyzer, (B) anion exchange membrane (AEM)-type electrolyzer, (C) reverse bias bipolar membrane (RB-BPM)-type electrolyzer and (D) forward bias bipolar membrane (FB-BPM)-type electrolyzer.

observed in Fig. 10A.<sup>165</sup> However, it is important to note that this suppression of  $\text{CO}_2$  crossover may not always be at play. The  $\text{CO}_2$  generated at the BPM junction can also diffuse towards the anode, where it accumulates and transitions into the gas phase at the membrane–anode catalyst layer interface.<sup>181</sup> Over time, this accumulation can lead to structural damage, including catalyst layer perforation and BPM delamination, raising concerns about the stability of BPMs in  $\text{CO}_2$  electrolyzers.<sup>181,182</sup> Nevertheless, larger current densities were obtained for the FB-BPM configuration ( $-150 \text{ mA cm}^{-2}$  at  $1.7 \text{ V}$ ) compared to those of the RB-BPM ( $-80 \text{ mA cm}^{-2}$ ) using the same cell components

(Fig. 10B). Additionally, at a fixed current density of  $-100 \text{ mA cm}^{-2}$ , a higher selectivity towards CO was obtained with the FB-BPM configuration ( $\approx 6\%$ , compared to  $\approx 4\%$  for the AEM or RB-BPM – Fig. 10C).<sup>165</sup> The stability of this FB mode was also measured at  $50 \text{ mA cm}^{-2}$ , revealing a substantial decrease in CO selectivity within the first 5 h due to water accumulation at the cathode, which progressively blocked  $\text{CO}_2$  diffusion towards the electrocatalyst. However, after drying the cathode electrode for 24 h, the CO selectivity returned again to the initial values, confirming that excess water was responsible for the blockage (operation 2, blue region in Fig. 10D).<sup>165</sup>

In another study in which  $1 \text{ M KOH}$  was fed at the anode, it was shown that the dominant ion transport mechanism is water dissociation at the layer's interface in RB mode,<sup>183</sup> while the absence of water dissociation in FB mode reduces the applied voltage by around  $3 \text{ V}$ .<sup>183</sup> However, after an operation time of 10 min, a drop in the cathodic potential is observed, which correlates with a decrease in CO selectivity. The authors hypothesize that this effect is due to the formation of potassium-based (bi)carbonate at the AEL-CEL interface.<sup>183</sup>

It is worth pointing out that the FB-BPM configuration is significantly less studied than AEM or CEM  $\text{CO}_2$  electrolysis, as it has only been under study for a few years. In particular, studies on the use of BPMs for the  $\text{CO}_2\text{RR}$  have only been published since 2016,<sup>184,185</sup> while FB-BPM research dates back to 2021,<sup>183,186</sup> highlighting the novelty of this approach. In general, only a few studies have focused on the development of BPMs for  $\text{CO}_2$  electrolyzers since then, but interesting results have already been obtained. BPMs have quickly achieved similar FEs and current densities to AEM and CEM. In such a short period, a few studies have reported  $\text{FE}_{\text{CO}}$  values of  $80\text{--}100\%$  at  $100\text{--}300 \text{ mA cm}^{-2}$ .<sup>187\text{--}189</sup> We therefore believe that bipolar membranes possess the greatest potential for improvement due to their very early stage of development, but substantial advancements are still needed to render them fully applicable, especially with regard to their stability.

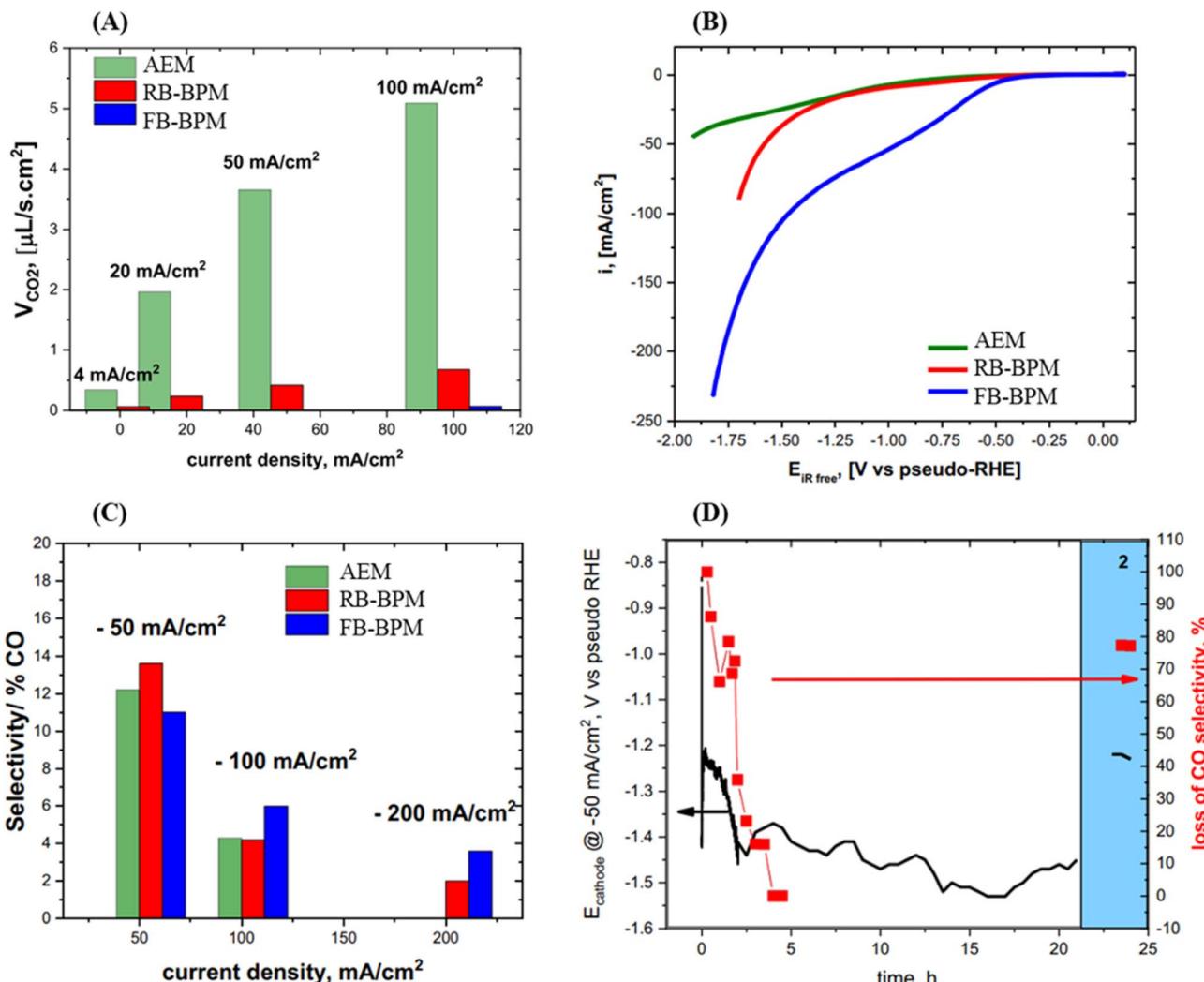
## 4.2 $\text{CO}_2$ electrolyzers

The design of the  $\text{CO}_2$  electrolyzer plays a crucial role in determining the overall performance of the electrochemical reaction, as it directly affects mass transport, ion management, and the system's stability. Different electrolyzer configurations have been developed to address key challenges such as achieving high current densities, optimizing gas–liquid interactions, and ensuring long-term operational stability.

$\text{CO}_2$  electrolyzers can be broadly classified into three main categories (Fig. 11):<sup>190</sup> H-type and parallel plate cells, flow cells and zero-gap cells. In the following sections, each of these electrolyzer types will be discussed in detail, highlighting their operating principles, advantages, limitations and recent advancements.

**4.2.1. H- and parallel-plate cell.** H- and parallel-plate type electrolyzers are broadly used as lab-scale reactors for  $\text{ECO}_2\text{RR}$  studies due to their straightforward operation and simplicity. Both electrolyzers consists of a two-compartment electrochemical cell, where the cathode electrode is set in one





**Fig. 10** (A) Volume flows of  $\text{CO}_2$  produced on the anode side of a  $\text{CO}_2$ -electrolyzer cell with an Au-based cathode and an  $\text{IrO}_2\text{-TiO}_2$  anode catalyst using different membrane configurations. The anode gas composition was analyzed using mass spectrometry at various cell current densities in galvanostatic mode. Cells were operated at 40 °C under ambient pressure. The cathode was fed with pure, humidified  $\text{CO}_2$  and the anode with humidified Ar. (B) Cathode polarization curves of  $\text{CO}_2$ -electrolysis cells with an AEM (Fumasep AA30), RB-BPM (Fumatech FBM, 130  $\mu\text{m}$  thickness), and FB-BPM (Fumatech FBM, 130  $\mu\text{m}$  thickness) at 50  $\text{mV s}^{-1}$ , 40 °C and ambient pressure. (C) CO selectivities obtained in galvanostatic experiments at various fixed current densities. (D) Chronoamperometric measurements at  $-50 \text{ mA cm}^{-2}$  (black line) and corresponding CO selectivity measured by *online* MS (red data) for the FB-BPM. The cathode was fed with 50/50 vol%  $\text{CO}_2/\text{Ar}$ , while the anode consisted of a Pt/C catalyst fed with pure  $\text{H}_2$ . Reproduced from ref. 165 with permission from ECS, copyright 2019.

compartment and the anode and reference electrodes are located in the other.<sup>171,176,191,192</sup> These cathodic and anodic compartments are separated by an IEM, which prevents the crossover and possible recombination of products during operation. During electrolysis,  $\text{CO}_2$  gas is continuously fed into the cathodic reservoir solution, where it is reduced on the electrode surface. The gas output is subsequently directed to a gas chromatograph or a mass spectrometer for accurate product analysis and quantification. Liquid products, such as  $\text{CH}_3\text{OH}$ , are collected from the cathode compartment electrolyte post-reaction and analyzed using techniques such as nuclear magnetic resonance or high-performance liquid chromatography.

This electrolyzer design mainly relies on the dissolution of  $\text{CO}_2$  into the cathode compartment electrolyte, whereby the use

of a liquid solution limits the concentration of  $\text{CO}_2$  and its accessibility to the electrode surface. More precisely, aqueous electrolytes possess a  $\text{CO}_2$  solubility of  $\approx 30 \text{ mM}$ , which restricts the attainable current densities to values  $\ll 100 \text{ mA cm}^{-2}$  that cannot be considered as industrially relevant.<sup>171,193</sup>

Instead, H- and parallel plate type  $\text{CO}_2$  electrolyzers serve as effective tools for evaluating the kinetics of ECO<sub>2</sub>RR electrocatalysts, which is in turn extremely useful when comparing the catalytic performance of different materials. However, this cell design is not up-scalable due to its high electric resistance (typically around 5  $\Omega \text{ cm}^2$  (ref. 194)), inefficient mass transfer and low  $\text{CO}_2$  solubility, which as discussed above severely limit the currents attainable with such setups. As shown in Table 2, the highest current densities reported with the H-type cell design rarely surpass 40  $\text{mA cm}^{-2}$ , and stability tests typically

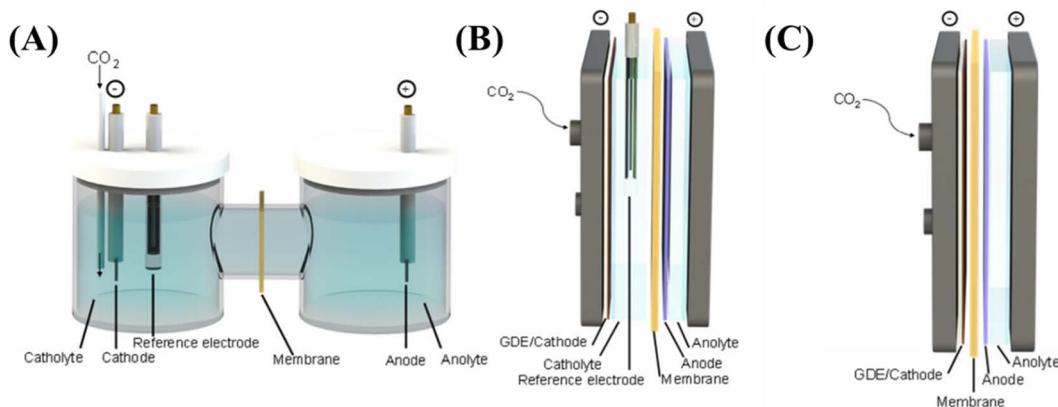


Fig. 11 Schematic illustration of different CO<sub>2</sub> electrolyzers: (A) H-type cell, (B) flow cell, and (C) zero-gap cell. Reproduced from ref. 190 with permission from the American Chemical Society, copyright 2024.

extend only for a few hours. Since this type of reactor is designed exclusively for the fundamental evaluation of catalyst potential, it is not meaningful to perform long-term durability studies, as H-type cells are not envisioned for industrial implementation. Therefore, degradation processes of membranes, catalysts, or other cell components are generally not investigated in these systems.

**4.2.2. Flow cell CO<sub>2</sub> electrolyzers.** In light of the limitations of H-type electrolyzers, flow cells have emerged as a promising solution to enhance CO<sub>2</sub> mass transfer.<sup>195</sup> These cells are structured into three compartments: a gas chamber, a cathodic compartment and an anodic compartment. The cathode electrode is typically constructed with a porous carbon gas diffusion layer (GDL) coated with the ECO<sub>2</sub>RR electrocatalyst, located between the gas chamber and the cathodic compartment.<sup>196</sup> Moreover, an ion-exchange membrane separates cathode and anode electrolytes.<sup>156</sup> In contrast to the conventional H-type CO<sub>2</sub> electrolyzer, the gas diffusion medium provides pathways for gaseous CO<sub>2</sub> to directly access the cathode catalyst layer, thus avoiding the above discussed limitations in CO<sub>2</sub> availability intrinsic to its provision as a dissolved species in the electrolyte. As such, the electrolyte in the cathode compartment is also in contact with the ECO<sub>2</sub>RR electrocatalysts, so that the electrochemical reduction of CO<sub>2</sub> proceeds at a solid-liquid-gas interface. This design substantially improves mass transport efficiency and enables higher currents, particularly for the production of CO,<sup>197–200</sup> for which current densities of 500–1000 mA cm<sup>−2</sup> with catalysts of different chemical compositions (Ni-, Co-, Cu- or Fe-based, among others) and electrolytes (such as CO<sub>2</sub>-saturated KHCO<sub>3</sub> or KOH solutions) have been demonstrated.<sup>197–200</sup> Furthermore, additional studies have shown the potential for hydrocarbon production when selecting appropriate Cu-based electrocatalysts, with current densities reaching more than 1000 mA cm<sup>−2</sup>.<sup>201–205</sup>

Concerning electrochemical CO<sub>2</sub>-to-CH<sub>4</sub> conversion, flow cells have demonstrated large current densities with high CH<sub>4</sub> FE. As previously described, Cu nanoparticles supported on N-doped carbon materials were found to exhibit excellent catalytic performance for the ECO<sub>2</sub>RR to CH<sub>4</sub>.<sup>88</sup> The electrolyzer

configuration consisted of an anion exchange membrane separating anodic and cathodic chambers. For electrochemical measurements, 1 M KOH was used as the electrolyte. At −1.1 V vs. RHE, the FE towards CH<sub>4</sub> formation was around 70% with a current density of 230 mA cm<sup>−2</sup>.<sup>88</sup> As demonstrated in the following section, the authors also conducted electrochemical measurements in zero-gap cells, with lower FEs but long stability (50 h). Additionally, a Cu(i)-based coordination polymer (NNU-33(S)) underwent a substitution of hydroxyl radicals for sulfate radicals during the ECO<sub>2</sub>RR that resulted in an *in situ* dynamic crystal structure transformation to NNU-33(H), which reached a current density of 391 mA cm<sup>−2</sup> with a FE towards CH<sub>4</sub> of 82% at −0.9 V vs. RHE.<sup>206</sup> These results were obtained in a 1 M KOH solution and slightly decreased to 350 mA cm<sup>−2</sup> and 75% after 5 h of continuous electroconversion.

Despite these encouraging results, there are still big challenges for the widespread implementation of large-scale CO<sub>2</sub> flow cells. One notable issue involves the flooding of the electrolyte in the GDL at the cathode gas chamber, causing channel blockages that limit CO<sub>2</sub> transfer from the gas chamber to the catalyst layer. This limitation significantly impacts the ECO<sub>2</sub>RR performance and leads to increased HER selectivity after only a few hours of operation.<sup>176,207</sup> Furthermore, many of the used electrolytes, especially KOH, tend to produce carbonates and bicarbonates that precipitate during operation, hindering again the exposure to CO<sub>2</sub> through the blockage of the diffusion channels.<sup>208</sup> To address the flooding issue, three main strategies have been proposed.<sup>209</sup> The first is the control of the interface at the GDL catalyst by using polymeric or hydrophobic substrates that reduce wettability and limit water penetration. The second is to design GDLs with adapted structures that allow excess electrolyte to drain through the electrode and be carried out of the cell with the gas flow. A third approach involves tuning the membrane thickness and CO<sub>2</sub> feed conditions (*i.e.* humidity) to control water transport and minimize salt precipitation.<sup>210,211</sup>

**4.2.3. Zero-gap cells.** The high resistance caused by the liquid electrolytes circulated between the cathode and the anode in flow cells lowers the overall energy efficiency of these electrochemical systems.<sup>208</sup> Alternatively, zero-gap cells, also

known as catholyte-free or membrane electrode assembly (MEA) cells, have been developed to eliminate the liquid electrolyte in the cathode compartment, thus addressing issues such as electrode flooding and ohmic resistance. The ohmic resistance is significantly reduced, reaching values as low as  $0.3 \Omega \text{ cm}^2$ .<sup>212</sup> The zero-gap cell consists of a compact, sandwich-like design with the anode and cathode separated only by an IEM. One of the most promising qualities of zero-gap cells is the scalability of MEA technology, as multiple individual MEA cells can be assembled into a  $\text{CO}_2$  electrolyzer stack, making it extremely relevant for industrial-scale processes.<sup>208</sup> In zero-gap cells, gaseous  $\text{CO}_2$  (often humidified to enhance the membrane's ionic conductivity) is fed into the cathode through a GDE, and the anode electrode is exposed to the electrolyte. It is worth mentioning that zero-gap cells equipped with AEMs are the most commonly used configuration.<sup>116,175</sup>

Few studies have addressed  $\text{CO}_2$  conversion to  $\text{CH}_4$  in zero-gap cells. The previously mentioned work about Cu nanoparticles supported on N-doped carbon materials showed a  $\text{CH}_4$  selectivity above 70% at  $-230 \text{ mA cm}^{-2}$  in a flow cell reactor.<sup>88</sup> However, this methane FE dropped below 60% after conducting measurements at the same current density in a  $\text{CO}_2$  zero-gap electrolyzer. Both  $\text{CO}_2$  electrolyzers employed an anion exchange membrane. Nevertheless, it is worth pointing out that the  $\text{CH}_4$  selectivity and the current density in a zero-gap cell did not change substantially for 50 h at a voltage of 4 V, indicating excellent stability.

Another exciting study can be found about electrochemical  $\text{CO}_2$  conversion into  $\text{CH}_4$  in zero-gap cells, using again Cu nanoparticles in a MEA configuration with an anion-exchange membrane.<sup>175</sup> The authors demonstrated that low coordination number Cu nanoparticles are beneficial for reducing the hydrogenation energy requirement towards  $\text{CH}_4$  production under alkaline conditions, counteracting the traditionally low energy requirements for C-C coupling. This MEA-catalyst combination operated for 110 h at a current density of  $190 \text{ mA cm}^{-2}$  with an average FE for  $\text{CH}_4$  of 56%, which is the longest operating time for  $\text{CO}_2$ -to- $\text{CH}_4$  conversion so far.

Despite these advantages, one of the most critical challenges of the zero-gap systems is the precipitation of carbonates and bicarbonates within the catalyst layer and the GDL. Salt precipitation originates from the interplay of  $\text{CO}_2$ , hydroxide ions and alkali cations (from the anolyte). Carbonates and bicarbonates accumulate within the catalyst layer, GDL and membrane, progressively blocking gas transport, increasing cell resistance and leading to higher HER selectivity. While dilute electrolytes greatly improve stability, as demonstrated by thousands of hours of continuous operation at moderate current densities,<sup>213,214</sup> they also increase cell resistance and limit performance at higher currents. This means that operating without cations prevents precipitation but drastically lowers activity.<sup>213,214</sup> Beyond avoiding precipitation, other strategies aim to remove salts once formed, typically through regeneration protocols. In these approaches, solvents are periodically injected into the cathode to dissolve the precipitated carbonates and restore  $\text{CO}_2$  transport, although this inevitably complicates system operation and questions the viability for

continuous industrial processes.<sup>215</sup> In the same line, some authors have proposed electrochemical pulse strategies, where the applied potential is periodically altered to redistribute ions and reverse salt precipitation.<sup>215</sup> Alternating between cell potentials of  $-3.8 \text{ V}$  during operation and  $-2.0 \text{ V}$  during regeneration enabled a 15-fold increase in stability compared to continuous operation without regeneration.<sup>215</sup>

## 5 Future perspectives

A comprehensive overview of the historical and current landscape of the electrochemical  $\text{CO}_2$  reduction reaction has been provided in this review, with particular attention to electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  conversion. The  $\text{ECO}_2\text{RR}$  emerges as a straightforward solution for mitigating anthropogenic  $\text{CO}_2$  in the atmosphere while producing value-added products.  $\text{CH}_4$ , among all  $\text{CO}_2$ -derived products, has arisen as a promising chemical due to the already existing industrial infrastructure for its rapid implementation and utilization. Technoeconomic analyses underscore the near-term viability of electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  conversion, although significant improvements are imperative to compete effectively with traditional  $\text{CH}_4$  synthetic routes. The design of electrocatalysts and advancements in  $\text{CO}_2$  electrolyzers stand as crucial milestones in the competitiveness of the  $\text{ECO}_2\text{RR}$ . Future perspectives and challenging targets for the successful implementation of electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  conversion are outlined below.

- Metal electrocatalysts, in our assessment, hold promise for the near-term advancement in electrochemical  $\text{CO}_2$ -to- $\text{CH}_4$  conversion due to their competitive performance. Using Cu as the active site has proven to be the most straightforward strategy to obtain high selectivity towards  $\text{CH}_4$  production. However, special emphasis should be placed on tuning the chemical environment of Cu with other metal electrocatalysts to enhance selectivity in  $\text{CH}_4$  production.

- Understanding why active sites, such as  $\text{CuN}_4$ , exhibit such varied selectivity in the  $\text{ECO}_2\text{RR}$  remains a challenge. Cu single atoms have demonstrated remarkable selectivity towards  $\text{CH}_4$ ,  $\text{CH}_3\text{OH}$  and  $\text{CO}$ , with FE above 70%, in similar carbon materials. Nonetheless, comprehending the disparities in  $\text{ECO}_2\text{RR}$  results among studies using comparable materials remains elusive. We understand that most of the studies in electrocatalyst design prioritize outcomes over delving into the chemistry involved; however, fine chemistry is clearly playing a definitive role in  $\text{ECO}_2\text{RR}$  activity and selectivity. To design better electrocatalysts, the understanding of electrochemistry that is behind these results is imperative.

- Metal-free carbon-based electrocatalysts have been proposed as promising materials for the  $\text{ECO}_2\text{RR}$ . However, their  $\text{ECO}_2\text{RR}$  performance is still far from competitive results. Despite its promising perspective, further efforts are still mandatory for carbon materials to compete with the state-of-the-art metal-containing electrocatalysts.

- Although DFT is often used to support experimental data with contrasted theory methods, its usage is often biased and partial. Authors typically focus solely on determining the electrocatalytic mechanisms that align with experimental



results, disregarding potential alternative reaction pathways. Here, the complexity of evaluating all potential mechanisms is worth noting, given the varied possibilities in the ECO<sub>2</sub>RR. However, we believe that it is crucial to emphasize that DFT results, as presented in these studies, should not be regarded as absolute truths but rather as thermodynamic validations of specific ECO<sub>2</sub>RR routes.

- Faradaic efficiency (FE) denotes selectivity towards a particular product in the ECO<sub>2</sub>RR. Despite the emphasis on FE in numerous studies, there must exist a crucial need to place greater scrutiny on energy efficiency (EE). EE, expressing the FE per voltage efficiency, provides a more meticulous indicator, especially for techno-economic aspects. In the case of pathways with a high number of electrons transferred, such as CH<sub>4</sub> (8-electron pathway), high voltages are usually required to obtain high selectivity. This is not reflected in FE but becomes essential in EE.

- We noticed a significant gap between fundamental and cell design researchers, which needs to be overcome to fulfill the cost and energy requirements for the electrochemical conversion of CO<sub>2</sub> into not only CH<sub>4</sub>, but all CO<sub>2</sub>-derived products. Fundamental research is imperative for understanding kinetics and thermodynamics, while producing the most active ECO<sub>2</sub>RR electrocatalysts but lacks practical applications. On the other hand, design of highly efficient electrochemical cells is useless if state-of-the-art electrocatalysts cannot be used in them.

- Advancements in CO<sub>2</sub> electrolyzers are crucial to bringing electrochemical CO<sub>2</sub>-to-CH<sub>4</sub> to competitive levels. H-type electrolyzers are useful electrochemical devices that provide valuable insights into mechanisms and fundamentals when comparing different electrocatalysts. However, the limited solubility of CO<sub>2</sub> in aqueous solution hampers the industrial applications of these devices. More attention should be directed to flow or zero-gap electrolyzers, capable of providing current densities above 100 mA cm<sup>-2</sup>.

- Progress in ion exchange membranes is essential for the future electrochemical production of CH<sub>4</sub> from CO<sub>2</sub>. Both CEMs and AEMs have been widely studied in CO<sub>2</sub> electrolysis, showing significant drawbacks that hinder their worldwide application. CEMs exhibit high HER activity in the cathode electrode, which reduces the ECO<sub>2</sub>RR selectivity. At the same time, AEMs display a large crossover issue, allowing CO<sub>2</sub> products to cross the membranes and recombine at the anode electrode, reducing the energy efficiency.

- Recently, BPMs have emerged as a promising alternative to mitigate crossover and pH challenges. However, the low stability under working conditions remains a key factor for the feasibility of these membranes. Particular relevance should be given to FB-BPMs, as despite their novelty, they have reached comparable current densities to AEMs and RB-BPMs. Moreover, in alignment with technoeconomic assessments, BPMs are postulated as the most feasible membranes for the next generation of flow electrolyzers.

## Conflicts of interest

The authors declare no competing financial interest.

## Data availability

No primary research results, software or code have been included and no new data were generated or analyzed as part of this review.

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