

Cite this: *Chem. Sci.*, 2024, 15, 6643

All publication charges for this article have been paid for by the Royal Society of Chemistry

Received 31st January 2024  
Accepted 21st April 2024

DOI: 10.1039/d4sc00746h

rsc.li/chemical-science

# Understanding electrochemical interfaces through comparing experimental and computational charge density–potential curves

Nandita Mohandas,<sup>†ab</sup> Sumit Bawari,<sup>†a</sup> Jani J. T. Shibuya,<sup>b</sup> Soumya Ghosh,<sup>a</sup> Jagannath Mondal,<sup>id</sup><sup>a</sup> Tharangattu N. Narayanan,<sup>id</sup><sup>a</sup> and Angel Cuesta<sup>id</sup><sup>\*bc</sup>

Electrode–electrolyte interfaces play a decisive role in electrochemical charge accumulation and transfer processes. Theoretical modelling of these interfaces is critical to decipher the microscopic details of such phenomena. Different force field-based molecular dynamics protocols are compared here in a view to connect calculated and experimental charge density–potential relationships. Platinum–aqueous electrolyte interfaces are taken as a model. The potential of using experimental charge density–potential curves to transform cell voltage into electrode potential in force-field molecular dynamics simulations, and the need for that purpose of developing simulation protocols that can accurately calculate the double-layer capacitance, are discussed.

## 1. Introduction

In electrochemistry, interfacial potential differences drive chemical reactions involving the transfer of charge. These interfacial charge transfer processes are reasonably well understood at a qualitative level and often require an electrocatalyst, *i.e.*, a material which, in addition to acting as a source or drain of electrons, can also act as a catalyst that lowers the apparent activation energy of the process by providing easy paths to the rupture and formation of bonds. Platinum group metals (PGM) are probably the most common components of such electrocatalysts, particularly regarding reactions relevant for energy conversion and storage.<sup>1</sup>

In recent years, experimental techniques have been able to probe much deeper into these processes at smaller spatial resolution and timescales. In parallel, computational approaches have also been optimised with new methods that can simulate larger system sizes and longer timescales. For electrocatalysts, the intrinsic activity is defined by the positioning of d-orbitals, bonding efficacy, or specific binding sites. However, to understand an overall electrochemical reaction, all aspects of it, including charging, chemical interactions, and solvent dynamics need to be considered. Classical and *ab initio* molecular dynamics (MD) have the potential to simulate an entire reaction, and in this perspective, we aim to discuss the

applicability of electrochemical force-field based MD approaches from an experimentalist's point of view.

In the absence of specific adsorption and at the Potential of Zero Free Charge (pzfc), the potential at the outer Helmholtz plane (OHP) is the same as in the bulk of the electrolyte,  $\phi_{\text{OHP}} = \phi_{\text{S}}$ , and there is no charge accumulation at the electrode–electrolyte interface.<sup>2</sup> The potential of zero charge (pzc) is a fundamental property of the electrode–electrolyte interface, whose knowledge is a key requirement for a detailed understanding of double layer phenomena and related properties. Accumulation of charge at the interface is the expected outcome if the electrode potential differs from the pzc. To rationally model electrochemical systems we need a fair experimental estimation of the pzc and of the capacitance that controls the magnitude of charge accumulation at the electrodes at any given potential away from it.

Although methods to describe ions and solvent in classical MD are well developed, modelling of the electrode is still quite challenging. The interfacial potential difference,  $\Delta\phi_{\text{S}}^{\text{M}}$ , can be controlled by the externally applied potential on the electrode. Depending on the sign and amount of this difference, mere charge accumulation, specific adsorption, or charge transfer reactions can take place at the interface, but such phenomena cannot be accurately described with a single set of force field parameters in force field-based MD simulations. In this perspective, we aim to understand electrode potentials (Section 2), how charge is induced on an electrode (Section 3) and how potentials and the charging process can be modelled using classical MD (Section 4). In force field-based MD simulations, certain methods exist to induce an electrochemical potential on the electrode.<sup>3</sup> In the simplest approximation, the Fixed Charge Method (FCM),<sup>4–8</sup> a partial charge can be added to the surface atoms of the electrode. In Section 4, we discuss and compare

<sup>a</sup>Tata Institute of Fundamental Research-Hyderabad, Hyderabad 500046, India<sup>b</sup>Advanced Centre for Energy and Sustainability (ACES), School of Natural and Computing Sciences, University of Aberdeen, AB24 3UE Aberdeen, Scotland, UK. E-mail: angel.cuestaciscar@abdn.ac.uk<sup>c</sup>Centre for Energy Transition, University of Aberdeen, AB24 3FX, Aberdeen, Scotland, UK

† Equal contributing authors.





work function,  $\Phi$ , which can be measured and differs from  $E_F$  by  $e\psi$ . This apparently trivial difference is very relevant, because it renders  $\Phi$  a magnitude sensitive to the atomic structure of the metal surface.<sup>12</sup> For example, the work function of Pt(111) is 5.9 eV, whereas that of Pt(100) is 5.75 eV. The absurdity of defining  $\Phi$  as the energy needed to extract an electron from the bulk of the metal to a point at infinity in vacuum (*i.e.*, of identifying  $\Phi$  with  $E_F$ ), as sometimes found even in textbooks, is easily shown by a simple gedankenexperiment (inset 2 of Fig. 1a): extracting an electron from the bulk of, say, platinum, through a (100) facet and then letting that electron fall to the Fermi level through a (111) facet would result in the net release of 0.15 eV, which violates the First Law of thermodynamics. Defining  $\Phi$  as the energy needed to extract an electron from the bulk of the metal to a point in vacuum just outside the metal surface also makes this magnitude insensitive to the state of charge of the metal surface, which is obviously not true for  $E_F$ . This can be shown with another simple gedankenexperiment (inset 3 in Fig. 1a): two metal pieces exposing to the vacuum initially uncharged surfaces are put in contact, forcing electrons to flow from the higher to the lower  $E_F$ , until both Fermi levels are aligned, and resulting in a net positive charge on the surface of the metal with the initially higher  $E_F$  and a net negative charge on the surface of the metal with the initially lower  $E_F$ .  $\Phi_1$  and  $\Phi_2$ , however, remain unaltered, and the difference between them can be measured by simply measuring the difference between the Volta potentials of the two surfaces when in contact:

$$\Phi_1 - \Phi_2 = e(\psi_2 - \psi_1) \quad (1)$$

Differences or changes in  $\Phi$  can therefore be measured very accurately, while absolute measurements of  $\Phi$  typically carry a large error due to the loose definition of the reference energy. In Fig. 1b, a metal surface is in direct contact with an electrolyte layer which is in contact with a UHV at the pzc (please note that because at the pzc the charge density on the electrode surface is zero,  $\psi = 0$ ). The energy necessary to extract an electron from the bulk of the metal to a point in vacuum just outside the surface of the electrolyte at the pzc is  $eE_{\text{pzc}}$ , and differs from  $\Phi$  by  $-\delta\chi_0^M + g^{\text{solv}}(\text{dip})_0$ , *i.e.*,<sup>13–15</sup>

$$eE_{\text{pzc}} = \Phi - \delta\chi_0^M + g^{\text{solv}}(\text{dip})_0 \quad (2)$$

where  $-\delta\chi_0^M$  is the change in the surface potential of the metal due to the presence of the electrolyte and  $g^{\text{solv}}(\text{dip})_0$  is an additional contribution due to the net orientation of the solvent dipoles at the interface at the pzc. This implies a proportionality between the pzc and  $\Phi$  that was suggested by Frumkin<sup>16</sup> nearly 60 years ago. The experimental evidence provided by Hansen and Kolb<sup>17</sup> that the double-layer survives emersion into UHV and that the work function of an immersed electrode depends linearly on the potential applied just before emersion is proof that eqn (2) holds.

The energy of an electron just outside the surface of the electrolyte provides a reference level for the definition of an absolute potential, for which a new gedankenexperiment, illustrated in Fig. 1c for the case of the standard hydrogen electrode (SHE), is needed. Thermodynamic cycles like that illustrated in Fig. 1c have

recently been used in the development of several computational reference electrodes as well as the calculation of pzc's.<sup>18–22</sup>

Take a piece of Pt immersed in and in equilibrium with an aqueous solution of pH 0 in equilibrium with 1 bar  $\text{H}_2$ . Because the system is in equilibrium,  $\Delta G$  for



is zero. Therefore, the net energy of a process in which (i) the  $\text{H}_2$  molecule is dissociated (requiring  $\Delta G_{\text{dis}}(\text{H}_2)$ , the dissociation energy of  $\text{H}_2$ ); (ii) the two resulting H atoms are ionised (requiring  $2I$ , with  $I$  the ionisation energy of H); (iii) the two resulting  $\text{H}^+$  ions are returned to the solution (requiring  $2\Delta G_{\text{solv}}(\text{H}^+)$ , where  $\Delta G_{\text{solv}}(\text{H}^+)$  is the solvation energy of protons); (iv) the two electrons are transferred from a point in vacuum just outside the surface of the solution ( $\text{e}^-(\text{vac}/\text{sol})$ ) to a point in vacuum just outside the Pt surface ( $\text{e}^-(\text{vac}/\text{Pt})$ , requiring  $-2e(\psi_{\text{Pt}} - \psi_{\text{sol}})$ , with  $\psi_{\text{Pt}}$  and  $\psi_{\text{sol}}$  the Volta potentials of Pt and the solution, respectively); and (v) the two electrons fall to the Fermi level of Pt (requiring  $-2\Phi_{\text{Pt}}$ , with  $\Phi_{\text{Pt}}$  the work function of Pt), must also be zero. Therefore:

$$\psi_{\text{Pt}} - \psi_{\text{s}} = \frac{-2\Phi_{\text{Pt}} - \Delta G_{\text{dis}}(\text{H}_2) - 2I - 2\Delta G_{\text{solv}}(\text{H}^+)}{2e} \quad (4)$$

By analogy with eqn (1), we can define the work function of the SHE (*i.e.*, the energy needed to extract an electron for the Fermi level of Pt to a point in vacuum just outside the surface of the electrolyte when reaction (3) is in equilibrium) as:

$$\Phi_{\text{SHE}} = \frac{1}{2}\Delta G_{\text{dis}}(\text{H}_2) + I + \Delta G_{\text{solv}}(\text{H}^+) \quad (5)$$

and the absolute potential of the SHE as  $E_{\text{abs}}(\text{SHE}) = \frac{\Phi_{\text{SHE}}}{e}$ . Please note that, as demonstrated by Hansen and Kolb,<sup>17</sup> the energy required to extract an electron from the Fermi level of Pt (or any other metal) to a point in vacuum just outside the surface of the electrolyte scales linearly with the applied potential.<sup>24</sup> Only when reaction (3) is in equilibrium will this energy coincide with  $\Phi_{\text{SHE}}$  (for example, at the pzc, it will correspond to  $eE_{\text{pzc}}$ , as shown above, with  $E_{\text{pzc}}$  the potential of zero charge in the absolute scale).

The accepted value of  $E_{\text{abs}}(\text{SHE})$  is  $4.5 \pm 0.2$  V. The large uncertainty is due to the error associated with the experimental determination of work functions and/or the computational calculation of the thermodynamic magnitudes included in the definition (see eqn (4) and (5)). It is also the reason why we keep using arbitrary reference potential scales like the SHE instead of the absolute potential scale. However, this definition of the absolute potential is crucial for the development of computational reference electrodes.

### 3. Experimental determination of the pzc and of the potential–charge relationship

The effect of the electrostatic potential difference between the electrode surface and the bulk of the electrolyte on the solvent



and ions constituting that electrolyte has been studied by Gouy,<sup>23</sup> Chapman,<sup>24</sup> Stern,<sup>25</sup> and Grahame,<sup>26</sup> resulting in increasingly complex models describing charge separation and distribution at the electrochemical interface. The difference ( $\Delta\phi_S^M$ ) between the Galvani or inner potential of the electrode ( $\phi_M$ ), and the Galvani or inner potential of the electrolyte ( $\phi_S$ ), accounts for the electrostatic contribution to the Gibbs free energy of any interfacial charge transfer reaction. This potential difference ( $\Delta\phi_S^M = \phi_M - \phi_S$ ) can be precisely changed by any desired amount and in either direction by externally controlling the difference between the electrochemical potential of electrons in our electrode (which is usually denoted as the working electrode, WE),  $\tilde{\mu}_e^{WE}$ , and the electrochemical potential of electrons in a reference electrode (RE),  $\tilde{\mu}_e^{RE}$ . The latter is pinned by an electrochemical equilibrium as determined by Nernst equation (e.g., in the SHE it is pinned by the  $H^+/H_2$  equilibrium when pH is 0 and  $P_{H_2} = 1$  bar). Because this potential difference,  $\Delta\phi_S^M$ , happens across a very short distance, it generates a huge electric field that can, for example, polarise any chemical species present in this spatial region, including interfacial water molecules. Please note that  $\tilde{\mu}_e = \mu_e^\circ - e\phi$  (where  $\mu_e^\circ$  is the standard chemical potential of electrons in the material,  $e$  is the elementary charge and  $\phi$  is the Galvani potential of the material) has both chemical ( $\mu_e^\circ$ ) and electrostatic ( $\phi$ ) contributions and, therefore, the measured or applied potential difference between WE and RE does not in general correspond to the difference in electrostatic Galvani potentials between them, unless both electrodes are made of the same material, in which case  $\mu_e^{\circ,WE} = \mu_e^{\circ,RE}$ .

The interfacial capacitance ( $C$ ), defined as the slope of a plot of the charge density on the electrode ( $\sigma_M$ ) vs. the applied potential ( $\Delta\phi_S^M$ ),

$$C = \frac{\partial\sigma_M}{\partial\Delta\phi_S^M} \quad (6)$$

describes the charging behaviour of the electrode. Please note that, because the interface must remain neutral,  $\sigma_M = -\sigma_S$ , where  $\sigma_S$  is the charge density in the electrolyte side of the interface. This description of the electrode–electrolyte interface as two parallel layers of opposed charge is the origin of the term electrical double layer. The electrical double layer models mentioned above have attempted to explain the capacitive behaviour of and the potential profile across the electrode–electrolyte interface at different ion concentrations using simple models of the electrolyte. The Grahame<sup>26</sup> modification to the Stern<sup>25</sup> model proposed the existence of three regions: Inner Helmholtz Plane (IHP), Outer Helmholtz Plane (OHP) and diffuse layer (Fig. 2). The IHP passes through the centres of the ions in direct contact with the electrode, the OHP passes through the centres of solvated ions at the distance of their closest approach to the electrode and the diffuse layer is the region beyond the OHP where the ions concentration is still not identical to that in the bulk. In the absence of specific adsorption, the IHP can be ignored. In such case, the total capacitance is that of two capacitors in series, one, the Helmholtz capacitance, describing charge accumulation at the OHP ( $C_H$ ), the



Fig. 2 Scheme depicting Stern's description of the electrochemical interface in the presence of specifically adsorbing anions for the particular case of a positively charged surface.

other one, the diffuse layer capacitance, describing accumulation of charge in the diffuse layer ( $C_{diffuse}$ ),

$$\frac{1}{C_T} = \frac{1}{C_H} + \frac{1}{C_{diffuse}} \quad (7)$$

If there is specific adsorption, accumulation of charge in the adsorption bond behaves as a third capacitor ( $C_{ad}$ ) in parallel to  $C_H$  and  $C_{diffuse}$ , and the  $C_T$  is given by:

$$C_T = \frac{C_H C_{diffuse} + C_H C_{ad} + C_{diffuse} C_{ad}}{C_H + C_{diffuse}} \quad (8)$$

Even though various general phenomena are successfully described by these theories, the quantitative study of the effect of ion concentration and type requires the explicit atomistic description of the electrolyte.

From the preceding paragraphs, it is evident that a good experimental estimation of the pzc and the interfacial capacitance is required, as they control the magnitude of charge accumulation at the interface, a clear understanding of which is essential for modelling electrochemical systems. At this point, the definition of two types of pzc results convenient (see Fig. 3):<sup>27,28</sup>

(1) The potential of zero free charge (pzfc), at which the free electronic excess charge density on the metal surface is zero.

(2) The potential of zero total charge (pztc), at which the sum of the free electronic charge density plus the charge density localised in polar adsorption bonds is zero. The pztc can also be defined as the potential at which no charge will flow in or out of the interface (i.e., no current would be measured) upon changing its area.<sup>28</sup> In the absence of specific adsorption, pztc = pzfc.

It must be noted that, because the presence of an adlayer on the electrode surface will modify its surface potential, and





Fig. 3 The pzfc and the pztc. In the absence of specific adsorption (A), the pztc and the pzfc coincide. When there are specifically adsorbed species on the metal surface (B and C), the free charge density on the metal surface is not zero at the pztc (B), while the total charge density is not zero at the pzfc (C).

therefore also its work function (see preceding section) the pzfc of an electrode surface in the absence of specific adsorption (Fig. 3A) will be different to the pzfc of the very same surface covered by specifically adsorbed species (even if those are neutral, e.g., the pzfc of Pt(111) is  $0.26 \pm 0.03$  V vs. SHE, while the pzfc of CO-covered Pt(111) is  $1.10 \pm 0.04$  V (ref. 29)). Specific adsorption can also lead to an electrode surface having two pzfc's. For example, Pt(111) has a pzfc around 0.26 V vs. SHE corresponding to the adsorbate-free metal surface,<sup>29</sup> and a second pzfc around 0.84 V vs. RHE corresponding to the OH-covered Pt(111) surface.<sup>30</sup> Obviously, as the charge density on Pt(111) must become increasingly positive when crossing over 0.26 V in the positive direction but then must return to zero at 0.84 V, at some point between these two potentials the positive free charge density on the surface of this electrode will reach a maximum after which it will start decreasing to then become zero at  $E = 0.84$  V (in other words, there will be a negative capacitance contribution to the total interfacial capacitance of Pt(111) in this potential region<sup>30</sup>).

Possibly the most classical method of determining the pzfc of an electrode–electrolyte interface is that based on the determination of the Gouy–Chapman capacitance minimum. As the name of the method implies, the method is based on Gouy–Chapman's theory of double-layer structure and, consequently, can only be applied under conditions in which Gouy–Chapman's model applies, i.e., sufficiently low electrolyte concentration and absence of specific adsorption, under which the distinction between pzfc and pztc is unnecessary. Using this method, significant differences between the experimentally measured capacitance and that calculated using Gouy–Chapman's theory were revealed in the 1980's for metals other than Hg, specifically, for Ag(111).<sup>31–33</sup> Similar differences have been found recently for Pt(111) and have reignited the interest in the topic.<sup>34–36</sup>

It is worth briefly discussing here two methods of determining the pztc, namely, the CO-charge displacement and the immersion methods, as both rely on the thermodynamic definition of the pztc as the potential at which no charge will flow in or out of the interface upon changing its area and can be considered as the two sides of the same coin (Fig. 4). The CO-charge displacement method, developed by the Alicante group,<sup>37,38</sup> can be considered as the reverse of the immersion method, as it attempts to measure the charge flowing across the interface when the double layer is quenched (Arrow 2 in Fig. 4a), rather than when it's formed (Arrow 1 in Fig. 4a). It does so by measuring the current transient resulting from the adsorption of CO on a metal electrode and works well with metals on which CO adsorbs strongly and forms a dense adlayer that completely separates the metal substrate from the electrolyte, like Pt<sup>37–40</sup> and the Pt-group metals.<sup>41</sup>

If the charge density on the CO-covered metal surface is much smaller than that present on the CO-free surface, the former can be neglected (i.e.,  $Q_2 = \sigma_{M/CO} - \sigma_M \approx -\sigma_M$ , see Fig. 4) and the charge obtained by integrating the current transient measured during the adsorption process corresponds to the total charge density on the metal surface at the potential at which the experiment is performed. The precision of the method can be improved by determining the charge density on the CO-covered metal (i.e.,  $Q_4 = \sigma_{M/CO}$ , Arrow 4 in Fig. 4a) and subsequently correcting  $Q_2$ .<sup>29,42</sup> Performing experiments at different potentials and/or integrating a current–potential curve using  $Q_2$  (if necessary, corrected by  $Q_4$ ) at a given potential as the integrating constant, allows to obtain a charge–potential curve, from which the pztc can be determined as the point at which the curve crosses through zero.

The immersion method involves measuring the current transient when immersing the electrode surface in the electrolyte at a constant applied potential (Arrows 1 and 4 in Fig. 4a).





**Fig. 4** (A) Schematic description of the immersion (Arrow 1) and CO-charge displacement (Arrow 2) methods for the determination of the pztc. Arrow 4 corresponds to the determination by the immersion method of the pzfc of an adlayer-covered electrode, a CO adlayer in this example (B) current transients measured during the potentiostatic immersion of a CO-covered Pt electrode in 0.1 M acetate buffer (pH 4.76) at 0.24 (black), 0.14 (red), 0.04 (purple), -0.06 (blue) and -0.16 V vs. SHE. The charge resulting from integrating each of the current transient is also provided. (C) CV at 50 mV s<sup>-1</sup> of polycrystalline Pt in 0.1 M acetate buffer (pH 4.76, black line) and charge density vs. potential curves (red lines) obtained by integrating the CV using the charge obtained from a CO-charge displacement experiment at 0.12 V vs. RHE (see inset) as the integration constant, before (dashed line) and after (solid line) correction with the charge present on the CO-covered Pt electrode at that potential as obtained from the corresponding potentiostatic immersion experiments shown in (B). The blue dots on the red dashed line correspond to the charge measured in CO-charge displacement experiments at 0.12 and 0.22 V vs. RHE, illustrating the internal consistency of the experiments. The uncorrected and corrected pztc's resulting from these curves are 0.254 and 0.270 V vs. RHE, respectively. (D) Cyclic voltammogram (black line) at 50 mV s<sup>-1</sup> of a CO-covered Pt electrode in 0.1 M acetate buffer (pH 4.76) and charge density vs. potential curve (blue line) obtained by integrating the CV using the charge obtained from a potentiostatic immersion experiment at -0.16 V vs. SHE as the integration constant. The black square symbols correspond to the charge density present of the CO-covered Pt electrode at the corresponding potential as obtained from the potentiostatic immersion transients in (B). The red solid line is an extrapolation of the charge density vs. potential curve to  $\sigma = 0$  and yields a pzfc for the CO-covered polycrystalline Pt electrode of 0.87 V vs. SHE.

When immersing a pristine, clean metal surface, the potential at which integration of the immersion current transient returns zero charge density corresponds to the pztc of that metal surface, because upon immersion species that can adsorb specifically will do so until the equilibrium coverage corresponding to the applied potential is reached, and the charge corresponding to the adsorption up to that coverage will be included in the transient (as discussed above, in the absence of specific adsorption, that pztc will also be the pzfc).

As all metals but gold are too reactive to remain free of any adsorbate when exposed to an atmosphere containing oxygen and/or water vapour, Au is the only metal for which its pzfc can be detected by this method. For example, no charge density flows when immersing a UHV-prepared clean and well-ordered reconstructed Au(111) surface in 0.1 M HClO<sub>4</sub> at 0.53 ± 0.04 V vs. SHE,<sup>43</sup> which is therefore the pzfc (ClO<sub>4</sub><sup>-</sup> does not adsorb specifically on Au, or does so very weakly) of reconstructed

Au(111), in good agreement with values obtained from the Gouy–Chapman capacity minimum. However, when the same group tried to determine the pzfc of Pt(111) in the same solution by the same method, they did not obtain the correct value of 0.26 V vs. SHE.<sup>29</sup> Instead, a zero charge transient was obtained at 0.78 V vs. SHE,<sup>43</sup> corresponding to the pzfc of Pt(111) covered by a complete OH adlayer, which must have formed when the Pt(111) electrode was extracted from the UHV chamber and put in contact with the atmosphere in the electrochemical cell.<sup>30</sup> The immersion method can be used to determine the charge density present at a specific potential ( $Q_4 = \sigma_{M/CO}$ , in Fig. 4a) on a CO-covered Pt electrode. Using this strategy, one of us<sup>29</sup> was able to determine that the charge density on a CO-covered Pt(111) electrode at 0.04 V vs. SHE is -16.6 μC cm<sup>-2</sup> ± 0.9, which results in an error of 0.05 V in the determination of the pztc of Pt(111) in 0.1 HClO<sub>4</sub> by the CO-charge displacement method if this charge density is not taken into account. Fig. 4b



shows transients measured upon immersion of a CO-covered polycrystalline Pt electrode (Pt(poly)) in 0.1 M acetate buffer (pH 4.76). The charge density obtained by integrating any of these transients can be used to correct the charge density–potential curve of Pt(poly) in the same solution obtained using the CO-charge displacement method. Fig. 4c shows the characteristic CV of Pt(poly) in 0.1 M acetate buffer together with the corrected (red solid line) and uncorrected (dashed solid lines) charge density *vs.* potential curves, which result, respectively in corrected and uncorrected pzfc's of 0.270 and 0.254 V *vs.* RHE.

Because any localised charge density associated to the formation of the CO adlayer is already present on the electrode surface before immersion, the charge that flows in the immersion transients necessarily has to be free charge. Therefore, extrapolation to zero charge density delivers the pzfc of the CO-covered electrode. Fig. 4d shows the CV (black line) of CO-covered Pt(poly) between  $-0.16$  V and the onset of the oxidation of the CO adlayer. The black squares correspond to the charge density on the CO-covered electrode at  $-0.16$ ,  $-0.06$ ,  $0.04$ ,  $0.14$  and  $0.24$  V *vs.* SHE as obtained from the transients shown in Fig. 4b. The blue line is the charge-density *vs.* potential curve of CO-covered Pt(poly) obtained by integrating the CV using the charge from the immersion transient at  $-0.16$  V as the integration constant. The excellent agreement between the interfacial capacitance obtained from a linear fit to the charge density as determined from the potentiostatic immersion transients with that obtained from integrating the CV is evidence of the internal consistency of our data. Extrapolation of the charge-density *vs.* potential curve to charge density zero delivers the pzfc of CO-covered Pt(poly), which is  $0.87$  V *vs.* SHE. This is, as expected, more negative than the pzfc of CO-covered Pt(111) ( $1.10$  V *vs.* SHE<sup>29</sup>), because the polycrystalline surface will contain a multiplicity of sites with different local atomic structures, all of which will have a work function smaller (and therefore, a more negative pzfc) than CO-covered Pt(111). Although, at the pzfc, the charge summed over the whole surface will add up to zero, locally the surface will have negatively and positively charged sites. Even if there were a considerable fraction of (111) terraces on the Pt(poly) surface, the presence of sites with a different local atomic structure, including a variety of steps, kinks and border grains, must necessarily shift the overall pzfc negatively. The immersion method has also been used to determine the pzfc's of Au(111) electrodes modified by alkanethiol<sup>44</sup> and mercaptoalkanoic acid SAMs.<sup>45</sup> As demonstrated by all this work, preparation in UHV is thankfully not always a prerequisite for the immersion method.

Some electrochemical reactions have proven to also be good pzfc probes. For example, the reduction of peroxodisulphate is strongly inhibited on Pt(111), Pt(100) and Pt(110) single-crystal electrodes except at potentials around the corresponding pzfc.<sup>46</sup> Much more interesting is the case of the reduction of  $N_2O$ , which has been shown to be an excellent probe of the local pzfc.<sup>47</sup>  $N_2O$  reduction has been used in combination with CO-charge displacement experiments to identify the pzfc of step and terrace sites of stepped Pt single-crystal electrodes and improve our understanding of the effect of introducing steps on the global pzfc.<sup>48,49</sup>

The determination of the pzfc by classical electrochemical methods is impossible when it falls within a potential region in which specific adsorption occurs and requires coupling with non-electrochemical methods. Probably the most successful of these is the measurement of coulometric potential transients after a laser-induced temperature jump (*T*-jump) at the electrode electrolyte interface.<sup>50–53</sup> The cartoon in Fig. 5 illustrates the interfacial processes generating the coulometric potential transient measured upon inducing an interfacial *T*-jump with a short laser pulse in an aqueous electrolyte. At any applied potential, interfacial water dipoles will orient to shield the charge density accumulated at the electrode surface, resulting in a potential drop across the electrode–electrolyte interface smaller than what would exist for the same charge density in the absence of interfacial dipoles. The *T*-jump resulting from a short laser pulse incident on the electrode surface randomises the orientation of the interfacial water dipoles, thereby decreasing the degree to which the charge density on the electrode surface can be screened by them. Because under coulometric conditions charge cannot flow to keep the potential drop across the interface constant during the experiment (this is what would happen if the experiment were done potentiostatically instead, and would result in a current transient), the interfacial drop will change during the *T*-jump and will return to the initial value when the interface cools down back to the initial temperature. Because the potential drop across the reference electrode–electrolyte interface remains constant, this results in a potential transient. If the electrode surface is negatively charged, as in the example in Fig. 5, a negative potential transient will occur, while a positive potential transient will be measured for a positively charged electrode surface. There will however be a potential at which the orientation of the interfacial water dipoles is as random as can be, and at which therefore the *T*-jump will not result in a coulometric potential transient. This will be the Potential of Maximum Entropy (pme). Because the orientation of the interfacial water dipoles must be determined by the free charge density on the electrode surface, the pme must be closely related to the pzfc. Actually, because in most metals interfacial water has a negative contribution to the interfacial potential drop at the pzfc,<sup>19</sup> the pme is slightly negative of the pzfc.<sup>52</sup>

Very recently, Xu *et al.*<sup>54</sup> have reported an optical method for the determination of the pzfc of metal electrodes based on measuring the phase shift of the electrode's second harmonic generation (SHG) signal, which must scale with the interfacial electric field. Therefore, by comparing the potential dependence of the phase of an electrode's SHG,  $\phi_1$ , with the phase of the SHG generated by the same, uncharged, surface (*e.g.*, the SHG of same surface either in vacuum or exposed to an inert atmosphere, instead of immersed in an electrolyte),  $\phi_0$ , the pzfc can be identified as the potential at which  $\phi_1 - \phi_0 = 0$ . Xu *et al.*<sup>54</sup> tested their method with a polycrystalline Pt electrode and, although they find the expected independence of the pzfc on pH and a  $-0.36$  V shift of the pzfc when Ni is deposited on Pt, the absolute value obtained for the pzfc of Pt(poly),  $0.231$  V *vs.* SHE  $\pm 0.076$  is essentially identical to that of Pt(111). As discussed above, due to the presence on the surface of Pt(poly) of sites



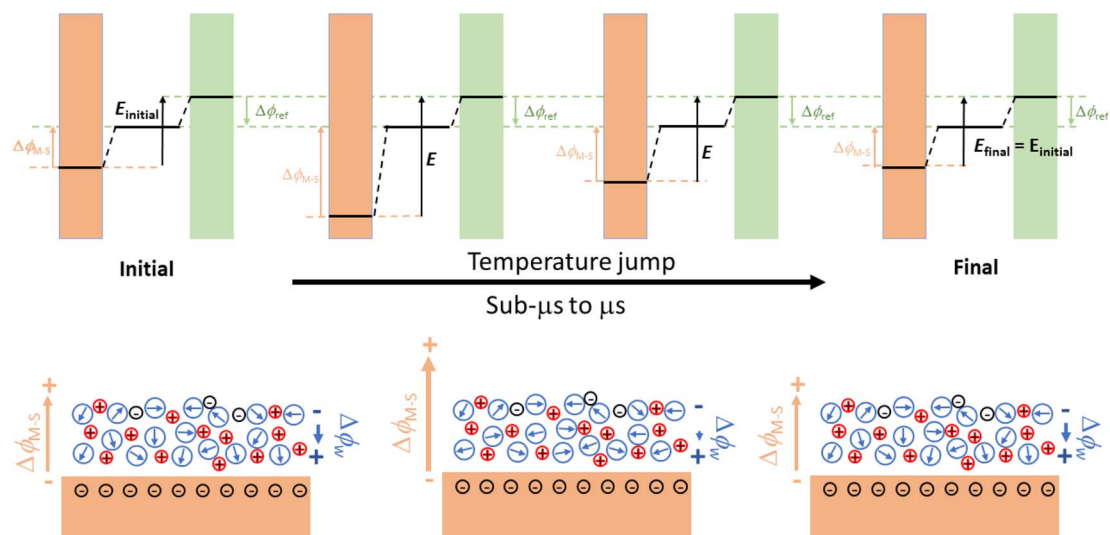


Fig. 5 Scheme describing the changes induced in the structure of interfacial water upon heating with a short laser pulse under coulостatic conditions. Initially, both the charge density at the electrode surface and the orientation of the interfacial water dipoles are determined by the applied potential. When the laser pulse hits the surface, the temperature of the interface increases, randomising the orientation of the interfacial water dipoles and decreasing the effectiveness with which they can screen the charge density on the electrode surface. Because under coulостatic conditions the charge density on the electrode cannot change to respond to the reduced screening of the surface potential by the interfacial water dipoles, the potential drop across the electrode changes during the experiment, and so does the potential measured with respect to the reference electrode. As the interface cools down again to the initial temperature, the initial structure of the interface is restored.

with a local work function necessarily smaller than that of Pt(111), the pzfc of Pt(poly) should be expected to be lower than that of Pt(111) (see, *e.g.*, the 0.23 V difference noted above between the pzfc of CO-covered Pt(poly), 0.87 V vs. SHE, and that of CO-covered Pt(111), 1.10 V vs. SHE). It must be noted, though, that even in perchloric acid solutions, only (111) terraces will be free of adsorbates in the so-called double-layer region of Pt(poly). For any other site with a different local atomic structure, hydrogen desorption is concomitant to OH adsorption.<sup>55</sup> Because the presence of adsorbed OH will lead to a different, probably more positive, pzfc (see discussion above noting that the pzfc of OH-covered Pt(111) is 0.84 V vs. RHE in 0.1 M HClO<sub>4</sub>), an overall pzfc of Pt(poly) very similar to that of Pt(111) is still possible. In any case, the validity of Xu *et al.*'s<sup>54</sup> method for the determination of the pzfc needs to be tested with model surfaces like Pt(111) and Au single-crystal electrodes, for which the pzfc's are well known and free of ambiguities.

## 4. Computational electrochemistry: modelling the electrode–electrolyte interface with classical force fields-based molecular dynamics

Force field-based Molecular Dynamics (MD) are versatile and powerful computational methods. Although the quantum mechanical *ab initio* alternative can provide a more detailed description of the electrode at the atomic level, we need to resort to force field-based MD simulations to study significantly larger spatial and temporal scales, at which the computational cost of *ab initio* MD becomes prohibitive.

In force field-based MD simulations of electrochemical systems, modelling the electrode, including an appropriate way of describing the electrode's charge density and potential, is a particular challenge of critical importance.<sup>3</sup> Here, we discuss three ways of including the voltage between the two electrodes enclosing the simulation cell in classical MD: (i) Electrochemical Dynamics with Implicit Degrees of freedom (EChemDID), (ii) the fixed charge method (FCM), and (iii) the constant potential method (CPM) (Fig. 6). Even though other methods have been reported,<sup>56</sup> we feel that these three are particularly important and more widely used among computational electrochemists. We then discuss the challenge of translating the cell voltage into individual electrode potentials and how comparison with experimental results like those discussed in the preceding sections can help in this task.

### 4.1 EChemDID

This method is applied particularly within the framework of reactive force-field (ReaxFF) type potentials, which are empirical.<sup>10,57–59</sup> In ReaxFF, bond breaking/formation and partial charges ( $q$ ) are described through the bond order, bonding and charge interactions.<sup>10</sup> Two atom-dependent electronic parameters are then introduced, electronegativity ( $\chi^0$ ) and hardness ( $H$ ), to describe the electronic energy of the system, which is then combined with the coulombic interactions to yield the total energy of the system,

$$E(q_i; R_i) = \sum_i \left( \chi_i^0 q_i + \frac{1}{2} H_i q_i^2 \right) + \sum_{i < j} q_i q_j J(|R_i - R_j|) \quad (9)$$

where  $J$  is the shielded coulomb interaction parameter between particles  $i$  and  $j$ , and  $R$  is their position.





Fig. 6 Scheme describing the three methods for including the electrode potential in classical MD discussed in the text. In the fixed charge method (FCM, left), partial charges are applied on the electrode surface, in the constant potential method (CPM, centre), electrode–solvent interactions are minimised to a fixed potential, and in the ElectroChemical Dynamics with Implicit Degrees of freedom (EchemDID) method, a change ( $\pm V$ ) is induced in the ReaxFF parameter for electronegativity ( $\chi$ ).

The method relies on the electronegativity parameter,  $\chi$ , to induce an external voltage. Onofrio *et al.*<sup>60</sup> introduced externally applied voltages using  $\chi + 1/2 V$  and  $\chi - 1/2 V$  for each one of the opposing slabs describing the two electrodes enclosing the simulation cell. This change in the electronegativity of the atoms in the slab changes the Fermi level of the metal electrode. This method was initially developed to elucidate the mechanism of potential-dependent contact formation/breaking in solid state electro-metallisation cells.<sup>61</sup> Surface chemical interactions can be studied in this framework because ReaxFF also describes bonding interactions. This method can, in principle, capture both the capacitive and faradaic responses corresponding to the various surface reactions that can take place in an aqueous electrolytic solution. As an example, a system consisting of two polycrystalline platinum electrodes (modelled as protruding conical electrodes) in a weakly acidic pH (carbonic

acid) in the electrochemical window between hydrogen and oxygen evolution is studied here. Using ReaxFF parameters for Pt/C/H/O, the EchemDID module is used to simulate an externally applied voltage  $V_{sim}$  between two platinum electrodes (Fig. 7),<sup>10</sup> which results in charge accumulation on the surfaces of the electrodes.

A maximum simulated bias of  $16 V_{sim}$  (between  $-8$  and  $+8 V$ ) is applied between the two electrodes, above which the interactions seen in simulations are deemed unrealistic. The charge accumulation across the surface of either one of the electrodes at positive and negative voltages is reported in Fig. 7a. An almost linear dependence of charge density on  $V_{sim}$ , that becomes exponential at high simulated voltage due to the contribution from surface reactions, is obtained. It is important to note that faradaic reactions, *e.g.*, hydrogen- and oxygen evolution reactions, cannot be simulated in force-field based



Fig. 7 (A) Charge accumulation upon application of an external simulated voltage ( $V_{sim}$ ). (B) Snapshot showing charge accumulation on the polycrystalline protruding electrode at  $\pm 7V_{sim}$ . (C) Bond order dependence of charge accumulated on the surface atoms on both electrodes at a bias of  $\pm 7V_{sim}$ .



MD. Nevertheless, it is interesting to note that the trend of the charge density–voltage relationship in Fig. 7a is consistent with the charge density–potential curve in Fig. 4c, even though the voltage range in the simulations is highly unrealistic.<sup>62,63</sup>

Another aspect that can be studied in simulations is the plane dependent behaviour of different interactions. Protruding conical electrodes are used to simulate a rugged surface which is closer to a real polycrystalline platinum surface, where the effect of edges and different planes can be studied. These polycrystalline surfaces contain local regions which can be ascribed to different Pt crystallographic orientations.<sup>63</sup> Fig. 7c shows a clear dependence of accumulated charges on the bond order of the platinum atom in question. Atoms buried inside the electrode, which form the bulk phase, have no charge on them, showing that, as expected for a metal, only the surface gets charged. Polarised charge is bond-order dependent and increases with decreasing bond order. Thus based on the bond order of surface atoms of different planes the following trend for charge accumulation can be inferred: Pt(110) > Pt(100) > Pt(111). This behaviour is entirely dependent on the bond order and surface chemical interactions, and any correlation with the pzc of these surfaces cannot be inferred from these results. The edges that form between these phases accumulate even more charge, as they have lower coordination. A notable difference in the spread of charge is also seen between the positive (anode) and negative (cathode) electrodes, where negative charge is more delocalised than positive charge.

## 4.2 FCM

This is the most straight-forward way to incorporate charges computationally on the electrode surface. The method applies a partial charge to the surface atoms of an electrode and neglects charge fluctuations on the electrode induced by local density fluctuations in the electrolyte solution. From the electrostatics point of view, two oppositely charged electrodes induce an electric field between them, and hence FCM, in principle, may be considered as an equivalent to directly applying an electric field to the electrochemical system. Even though FCM is fairly uncomplicated and relies on a crude approximation, the method has been successfully adapted to various systems,<sup>4–8,64–69</sup> where it is reported to give promising results in most of the cases.

## 4.3 CPM

CPM was developed initially by Reed *et al.*<sup>70</sup> to explicitly consider local charge fluctuations while maintaining the potential constant over the electrode surface.<sup>68</sup> The method is based on earlier work by Siepmann and Sprik,<sup>71</sup> in which the constraint of constant electrode potential was enforced on average using an extended Hamiltonian approach. This is similar to the Nosé method<sup>72</sup> for constant temperature, with the main difference that in CPM the constraint is applied instantaneously at every step. The electric potential  $\Psi_l$  on each electrode atom is constrained at each simulation step to be equal to the applied bias, which is constant for a given electrode. This constraint leads to the following equation:

$$V = \Psi_l = \frac{\partial U}{\partial Q_l} \quad (10)$$

where  $U$  is the total Coulomb energy of the system and  $Q_l$  is the charge on each electrode atom.

The interaction potential of an electrode/electrolyte system is given by:

$$\Psi_l = \sum_i^n a_{li} Q_i + \sum_j^m b_{lj} q_j \quad (11)$$

where  $a_{li}$  and  $Q_i$  describe the position and charge of the atoms at the electrode surface, respectively, and  $b_{lj}$  and  $q_j$  describe the position and charge of ions in the electrolyte, respectively. The term  $a_{li}$  is constant for each atom throughout the simulation, as all the electrode atoms are considered fixed, but  $b_{lj}$  is updated every timestep, as the ions in the electrolyte are allowed to move throughout the simulation. From eqn (10) and (11) we obtain:

$$\sum_i^n a_{li} Q_i = V - \sum_j^m b_{lj} q_j \quad (12)$$

For each electrode atom a similar linear equation can be obtained, and solving these well-determined linear equation systems, the explicit charge for all the electrode atoms can be determined. In CPM simulations, equal and opposite potentials were assigned on the positive and negative electrodes, so that  $\Delta\Psi = \Psi^+ - \Psi^- = 2\Psi^+ = 2\Psi^-$ .

In the simulations discussed here, two water models with nonpolarizable (SPC/E<sup>73</sup>) and polarisable (SWM4-NDP<sup>74</sup>) force fields are considered. While the SPC/E model contains constant charges on atomic positions, the SWM4-NDP water model is represented as a rigid object imposing the experimental gas phase molecular geometry, with four interaction sites: the oxygen, carrying the molecular polarizability but no net charge, the two hydrogens, and an additional site located along the HOH bisector. An isotropic polarizability is introduced by adding an auxiliary mobile charged particle attached to the oxygen atom by a harmonic spring, generally referred to as a classical 'Drude' oscillator. Comparison between a polarizable and a non-polarizable water models is essential because the electronic polarization of water is highly sensitive to its environment and polarizability has shown essential to accommodate the local disruption of the hydrogen bond network created by anions or to reproduce the polarization effects of small multivalent cations on the first hydration shell.<sup>75–80</sup> Studies have shown that polarization of water may play a crucial role for the specific water–water interactions near small nonpolar moieties.<sup>81–84</sup>

Charge vs. voltage curves can be obtained by simulating two Pt(111) surfaces with the CPM model, which is compared in Fig. 8 with results for the same system using EChemDID. In the CPM simulations the charge follows a linear response up to bias voltages of around 5 V, after which the charge appears to saturate. The maximum surface charge is found to be slightly higher for the polarisable SWM4-NDP water model. Nevertheless, the polarizability of the water model does not seem to have a huge





Fig. 8 Charge–potential relationship curves using classical MD simulations on Pt(111) surface, with the CPM using SWM4-NDP water model and SPC/E water models; and EChemDID method with reactive water.

impact on the charging of the electrode. The order of magnitude of charge density that we have calculated by employing the CPM,  $10 \mu\text{C cm}^{-2}$ , is comparable to the charge density that had been reported in previous studies employing the same method.<sup>85,86</sup> Even though the SWM4-NDP water model, partially accounts for the polarizability of water and better estimates the viscosity ( $\eta$ ) and hydration free energy ( $\Delta G$ ) within the range of experimental estimates, it is still unable to induce charging of the electrode any better than the non-polarizable SPC/E model. We find that the  $b_{ij}$  and  $q_j$  terms in eqn (12), which describe the position and charge of species, respectively, in the electrolyte in the CPM, were not altered as expected due to the polarization of water. We speculate that the origin of this result lies in the rigid setup of SWM4-NDP water model as well as in the rigid setup of the electrode. For this reason, the polarizability of water does not have a significant impact on the charge induced on the electrode, *i.e.*, on the  $Q_i$  term in eqn (12).

In the case of EChemDID, the accumulated charge on the electrode also increases linearly with the applied bias but with an larger slope (*i.e.*, a larger capacitance) which is likely due to the added contributions of surface reactions and water alignment in the vicinity of the electrode. This behaviour is similar to the experimental result, which contains capacitive and pseudo-capacitive contributions in and at both sides, respectively, of the double-layer region. In contrast to the CPM method, different charges were induced at positive and negative bias in EchemDID, because this model takes into account the intrinsic electronegativity difference of Pt–O and Pt–H interactions. In the FCM (fixed charge method) and CPM (constant potential method), the surface charge density increases with voltage through accumulation of non-specifically adsorbing ions in the double layer, which eventually reaches dielectric saturation as no other processes can be described. On the contrary, bond breaking is allowed in the EChemDID method, and surface bonds like Pt–O at the anode and Pt–H at the cathode allow for

a further increase in charge density at higher cell voltages. This effect mirrors experimental charge increment due to surface reactions, which is why the charge density–potential profile is consistent with experiments, even though the underlying computational voltages are unrealistic.

FCM and CPM have been previously compared for modelling electric double layer capacitors (EDLC). Laird and co-workers<sup>9</sup> reported that for an ionic liquid electrolyte system at a graphite electrode, at low voltage ( $\leq 2$  V), the two methods yield essentially identical results, but at higher voltages ( $>4$  V) significant differences appear. Another work by Merlet *et al.*<sup>87</sup> examined the differences between the two methods by examining the relaxation kinetics and the electrolyte structure at the interface in EDLC with nanoporous carbide-derived carbon electrodes and planar graphite electrodes. They showed that CPM predicted more reasonable relaxation time than FCM, while the qualitative features in the electrolyte structure remained unchanged in both cases. Yet another work on the same line by Yang *et al.*,<sup>88</sup> on a very similar system, also reported that both methods yielded essentially similar results for electric double layer (EDL) structures in the charged nanometre and sub-nanometre spaces, consistent with previous observations in bulk electrolytes. Their results also suggest that the dynamics of the formation of EDL, *i.e.*, the evolution of ion concentration with time during the charging process, is more reliable in CPM. In a recent work by Tee and Searles,<sup>89</sup> the theoretical framework of CPM-MD was extended to the case in which the total charge of each electrode is controlled, instead of their potential difference, with a typical ionic liquid–graphene supercapacitor. They too observed statistically identical plots of charge against bias voltage in both cases.

A recent review by Zeng *et al.*<sup>56</sup> discussed various scenarios where different classical MD approaches are applicable in modelling electrochemical systems. They review applications of MD to supercapacitors, capacitive deionization, batteries, and electrical double layer transistors. We refer the reader interested in the rationality and possible applicability of the three different ways of including the voltage in classical MD to this review. Surface reactions are routinely studied with EChemDID method, and voltage provides another descriptor for simulating surface chemistry. Some of us<sup>62,63</sup> have recently demonstrated, for the first time to the best of our knowledge, the possibility of modelling electrochemical interfaces using reactive force field-based EChemDID MD simulations.

## 5. Comparison of charge density–voltage curves computed using classical force fields-based MD with experiments

As mentioned in Section 4, all the force field-based MD methods discussed above allow inclusion of the electrode charge density in the simulation, but none of them allows to translate this into an electrode potential. The ability of experimental methods, as shown in Section 3, to determine very precise and accurate charge density *vs.* potential curves, however, offers the



Table 1 Comparing the double layer capacitance obtained experimentally and theoretically from various methods

Method	Electrode	Electrolyte	Capacitance/ $\mu\text{F cm}^{-2}$	Reference
Computation-CPM	Pt(111)	SPC/E water	4.705	This work
Computation-CPM	Pt(111)	SWM4-NDP water	4.475	This work
Computation-EChemDID	Pt(111)	Reactive water	8.584	This work
Computation-EChemDID	Pt(poly)	Reactive water & acetic acid	18.07	This work
Experiment-CO charge displacement	Pt(poly)	0.1 M acetic acid	82.11	This work
Experiment-CO charge displacement	Pt(111)	0.1 M HClO <sub>4</sub>	~65	Ref. 90

possibility to estimate the potential in force field-based MD, or at least to test the agreement of simulated interfacial capacitances with experimental values.

Double layer capacitances obtained computationally and experimentally in this work and a few others from the literature are summarised in Table 1. The computed interfacial capacitances were calculated in all the cases as the slope of the charge density vs. voltage plot in the region where the dependence is linear, taking into account that the cell voltage is composed of two potentials identical in magnitude but opposed in sign at each of the electrodes (*i.e.*, a cell voltage of 4 V corresponds to polarising the negative electrode  $-2$  V below and the positive electrode  $+2$  V above, the pzc). This is simply the capacitance as defined in eqn (6). We can clearly see that computational methods considerably underestimate the double layer capacitance. For example, the experimental double layer capacitance of Pt(111) in 0.1 M HClO<sub>4</sub> is  $\sim 65 \mu\text{F cm}^{-2}$  in the double layer region.<sup>90</sup> In contrast, our simulations with Pt(111) and pure water delivered  $4\text{--}5 \mu\text{F cm}^{-2}$  with CPM MD and  $\sim 8 \mu\text{F cm}^{-2}$  when reactive force fields were used. Similarly, if we compare the experimental double-layer capacitance of polycrystalline Pt in acetate buffer (see Fig. 4c and corresponding discussion) with the computational result (see Fig. 7a), the latter is more than four times smaller than the former.

Such a discrepancy between the experimental and computational double layer capacitance is majorly overlooked in most of the cases. In most of the simulation studies we can find unrealistically high potentials being used which do not make sense from the experimental point of view, without any clear justification or charge induced being discussed. Both computational and experimental electrochemists should have a clear understanding of this discrepancy and be very careful when using either computational results to explain experiments or experimental results to support computations. Rather than simply reporting applied voltages in the simulation results, the charge densities induced by those voltages also need to be discussed and compared with the experiments. This is extremely important because potentials in force field-based simulations are not referred to any reference electrode scale, but to the pzc of the electrode in question. In experimental conditions, the charge density on the electrode surface is zero only at the potential of zero charge (pzc), which is characteristic of each electrode and electrolyte combination. In both classical CPM and EChemDID simulations, the charge induced on the electrode is zero at a cell voltage of 0 V, a situation which has no equivalent in experiment. Furthermore, along with non-specific

ion adsorption, interfacial charge-transfer processes associated to bond breaking and formation (*i.e.*, specific adsorption) and reorientation of interfacial water are concomitant to charging the electrode surface. In CPM, none of the processes involved in specific adsorption are taken into consideration, thereby yielding the smallest double layer capacitance. In EChemDID method, bond breaking and formation is modelled, which leads to a better estimation of the double layer capacitance than CPM. However, charge transfer processes cannot be modelled, which leads to an underestimation of adsorption capacitance. This shows the limitations of the existing classical MD methods.

The problem of how to refer the computed electrode potentials to a reference electrode in MD simulations of electrode-electrolyte interfaces is non-trivial. There are several ways to solve this issue in the case of *ab initio* MD. The oldest of these methods implies, for aqueous electrolytes, explicitly modelling the water-vapour interface and the use of the vacuum potential as reference.<sup>91–94</sup> The work function (*i.e.*, the energy required to extract an electron from the metal to the water-vacuum interface, see Fig. 2b and the corresponding discussion), which corresponds to the electrode potential in the absolute scale, is converted to the SHE scale by subtracting the experimental value of the absolute SHE potential (see Fig. 2c and the corresponding discussion). A related approach, using surface dipole correction, has been employed to study systems under constant charge<sup>95</sup> or constant potential conditions.<sup>96</sup> An alternative is the computational reference electrode method developed by Cheng and Sprik for the SHE.<sup>20,21</sup> This method avoids the explicit modelling of the water-vapour interface and does not require any experimental input. It uses the free energy of solvation of aqueous H<sup>+</sup>, calculated using thermodynamic integration over a set of ensembles sampled by DFT-MD,<sup>97,98</sup> as reference. The method has been used to compute the pzc's of metal electrodes and can be used for reference electrodes other than the SHE<sup>18</sup> as well as for non-aqueous media.<sup>22</sup> The simulated electrode surface can be charged by adding explicit ions in the electrolyte to the simulation cell,<sup>99</sup> and has been successfully employed to study the double layer properties of metal-electrolyte interfaces.<sup>100–102</sup> A similar internal reference has been employed in simulations with implicit solvent environment.<sup>103</sup>

Similar methods are unfortunately not available for including a computational reference electrode in classical force field-based MD. However, because at zero simulated applied voltage the charge density on both electrodes in the simulation cell is zero, the potential of both electrodes can be identified with the experimental pzc. The electrode potential



corresponding to any other simulated applied bias can be identified then by comparing the simulated and experimental charge-density *vs.* potential curves, hence the critical relevance of accurately describing the capacitance of the electrode–electrolyte interface discussed above. This is needed because, while AIMD methods are now able to reliably simulate electrochemical surfaces, the allowed timescales and system sizes are still limited by the computational power required. Simulating double-layer dynamics in relevant time scales or non-planar geometries is only possible in classical force field-based MD.

## 6. Conclusions, outlook and perspective

Using the Pt-aqueous electrolyte system as a prototype, we compare in this perspective the charge density–potential relationships from three classical MD methods to experimental data. We stress the importance of understanding the charge–potential relationship obtained from simulations as well as experiments to get a better understanding of the proxy variable for potential used in the simulations. While each of the three classical MD methods analysed has its own merit, their limitations are equally important and should not be overlooked.

FCM is the simplest and fastest method to induce an electrochemical potential on the electrode, with little difference in terms of static properties when compared to CPM. FCM also allows for direct comparison with experimental charge values, while polarisation effects like charge inhomogeneity at the electrode surface and dynamic properties are better modelled with CPM. EChemDID allows to incorporate surface reactions and can be useful to model charged states of polarisable ions and reaction processes.

We found a consistent mismatch between the computed and experimental capacitance with all the simulation methods analysed. This is a serious problem, as this is a proxy variable commonly used to define potentials in classical force field-based MD. The situation in which the simulated applied voltage and charge density are zero can still be identified with the experimental *pzc*. However, determination of the potential of both the positive and negative electrodes at non-zero simulated applied voltages and charge densities requires as accurate a simulation of the interfacial capacitance as possible. Although it is promising that the computational methods reproduce the almost constant experimental capacitance in the double-layer potential window, their performance still requires further improvement if they are to provide sensible insights into the structure and dynamics of real electrode–electrolyte interfaces.

MD simulations are a robust method for exploring EDLs at solid–liquid interfaces, even though accurately simulating electrode polarization is a notable hurdle. Looking ahead, though the CPM is a promising strategy for capturing EDL behaviours precisely, further improvement is essential to provide valuable insights for optimizing electrochemical devices. Another critical aspect is integrating chemical reactions into MD simulations, by employing reactive force fields (ReaxFF) within CPM-MD framework. With the greater

timescales and system complexities available to classical MD, the effects of electrolytes, electrode geometry, *etc.* can be studied and these mechanistic insights can complement experiments. Despite significant advancements, it is important to be cautious to prevent erroneous results, by giving meticulous attention to system design, method selection, parameter accuracy, and data collection. Through these measures, even within its limitations, classical MD simulations can still offer valuable insights about EDL and electrochemical processes.

## 7. Methods

### 7.1 Experiments

The immersion and CO charge-displacement experiments were conducted using a polycrystalline Pt bead which was cut and polished with alumina paste of 1.0, 0.3, and 0.05  $\mu\text{m}$  particle size in succession. Contact with the electrolyte was made through a hanging meniscus so that only the polished flat surface of known area is covered by the solution.

For the CO charge-displacement experiments, the crystal was first annealed in an open propane flame then quickly placed in a clean flask containing CO-saturated ultra-pure water. The crystal was allowed to cool down for at least 10 seconds in the closed atmosphere of the flask, lowered into the water, then raised to form a drop on the surface to protect it during transfer to the electrochemical cell, which contained 0.1 M acetate buffer (0.1 M  $\text{CH}_3\text{COOH}$  + 0.1 M  $\text{Na}(\text{CH}_3\text{COO})$ ) deaerated with Ar (N5.0, supplied by BOC). Once transferred to the electrochemical cell, the CO-covered surface was immersed in the electrolyte at 0.1 V *vs.* RHE and Ar was bubbled for some minutes to remove excess CO present in the protecting drop before starting a cyclic voltammogram. Then, a CO-stripping voltammogram was done to oxidise the CO-adlayer and expose a clean polycrystalline Pt surface. The CO charge-displacement experiment was then performed by applying the desired potential and blowing CO through a Pasteur pipette into the meniscus, thus allowing rapid transport of CO to the electrode–electrolyte interface. The resulting current transient was recorded and the experiment was repeated at least four times per set potential. The data used, including those presented in Fig. 4c, are the average of these four measurements.

In the immersion experiments, after annealing the polycrystalline Pt bead was introduced directly in the electrochemical cell containing a CO atmosphere and a CO-saturated electrolyte solution. The electrode surface was then positioned directly over the tip of the Luggin capillary, which points upwards, and the desired potential was applied. A KCl-saturated Ag/AgCl reference electrode with a glass joint fitting created an overpressure in the Luggin capillary when inserted into the airtight joint that closes the compartment where the reference electrode is hosted. By slowly opening the Teflon or glass key separating that compartment from the capillary tip, a jet of solution was shot up directly to the crystal surface, allowing to form a hanging meniscus and to wet the electrode surface without wetting the walls of the bead. The current transient resulting from forming the electrode–electrolyte interface was recorded and integrated to obtain the charge density on the CO-



covered polycrystalline Pt electrode at that potential. As with the CO charge-displacement experiments, each transient was repeated at least four times per set potential. The charge densities presented in Fig. 4b and used in Fig. 4d, are the average of these four measurements. The experimental errors and error bars, respectively, presented in those figures, are the corresponding standard deviations.

Solutions were prepared using ultra-pure water (18.2 MΩ cm, 1–3 ppb TOC, from an ELGA-VEOLIA PURELAB Chorus 1 Life Science water purification system), Acetic acid (glacial) 100% Suprapur (Merck) and Sodium acetate (anhydrous 99.99%) Suprapur (Merck).

## 7.2 MD simulation

All the MD simulations employing FCM and CPM were performed using the LAMMPS<sup>104</sup> 2020 code. For EChemDID simulations LAMMPS<sup>105</sup> 2015 code was used. The MD system consists of water enclosed between two oppositely charged Pt electrodes. Each electrode is modelled as three layers of Pt (111) sheets with an area of 9.8582 nm<sup>2</sup>, with the distance between the innermost layers of the two electrodes 75.4 Å. Simulations were performed in the NVT ensemble with the electrolyte temperature maintained at 300 K using the Nose–Hoover<sup>106</sup> thermostat. A cut-off length of 1.2 nm was used in the calculation of electrostatic interactions in the real space. The electrostatic potential is treated using the particle–particle particle–mesh approach. The Pt sheets were treated with fix command, so as to make them immobile. To reach equilibrium, the NVT simulation was first run for 200 ps and then a 20 ns production run was performed. For modelling water SPC/E<sup>73</sup> parameters were used in the non-polarizable case. The polarizable SWM4-NDP<sup>74</sup> model was constructed as an explicit 4-point model, with the Drude oscillator added by the Python tool polarizer.py.<sup>104</sup> A rectangular simulation box of dimension 34 × 30 × 80 Å<sup>3</sup> used in all the simulations, was periodically replicated in the *x* and *y*-directions while a fixed boundary condition was employed for the *z*-direction containing the platinum electrodes. The constant potential method implemented in the LAMMPS code by Wang *et al.*<sup>9</sup> was used. For the EChemDID simulations, LAMMPS 2015 code was used as it is compatible with the USER-EChemDID package.<sup>60,61</sup> A similar system as described above (Pt(111) with water) and a system consisting of two conical electrodes with 3–4 passive Pt layers were simulated with a solvent containing water and carbonic acid (as HCO<sub>3</sub><sup>−</sup> and H<sub>3</sub>O<sup>+</sup>) to simulate a pH ~5. Up to 320 ps were run at a particular applied potential, in an NVT ensemble where a temperature of 300 K is maintained using the Berendsen<sup>107</sup> thermostat.

## Data availability

The experimental and computational datasets generated for this article are available from the authors on reasonable request.

## Author contributions

NM: conceptualization, investigation, methodology, MD simulations, writing – original draft. SB: conceptualization, investigation, methodology, MD simulations, writing – original draft. JJTS: electrochemical experiments and corresponding analysis – CO-charge displacement and immersion transients. SG: supervision, writing – editing. JM: conceived the idea, conceptualization, resources, supervision. TNN: conceived the idea, conceptualization, funding acquisition, resources, supervision, writing – original draft. AC: conceptualization methodology, resources, supervision, writing – review and editing.

## Conflicts of interest

There are no conflicts of interest to declare.

## Acknowledgements

N. M., S. B., S. G., J. M. and T. N. N. acknowledge the support of the Department of Atomic Energy, Government of India, under Project Identification No. RTI 4007. J. J. T. S. and A. C. thank the University of Aberdeen for continued support.

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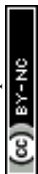
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