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Ring-opening terpolymerisation of phthalic thioanhydride with carbon dioxide and epoxides†

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In seeking to expand the portfolio of accessible polymer structures from CO₂ waste, we report the ring-opening terpolymerisation (ROTERP) of phthalic thioanhydride with CO₂ and epoxides, forming statistical poly(ester-thioester-carbonates) by employing heterobimetallic catalysts. Both metal choice and ligand chemistry modulate the amount of CO₂ incorporated into the polymer microstructure. Terpolymerisation occurs when maintaining polymerisation rates of the faster parent ring-opening copolymerisation and this finding led us to develop the formation of CO₂-derived terpolymers with butylene oxide at low CO₂ pressure under bicomponent catalysis. Tetrapolymerisation with added phthalic anhydride leads to the preferential polymerisation of phthalic anhydride before the polymerisation of sulfur derivatives with CO₂ and epoxides. Finally, we show that the presence of sulfur-containing thioester links leads to polymers with degradability benefits compared to those from all-oxygen derivatives.

Introduction

Heteroatom-containing polymers have great potential as degradable replacements for polymers based on backbones made up of –C–C– bonds.^{1–4} An increasingly popular synthetic methodology for accessing heteroatom-containing polymers is the copolymerisation of three- or four-membered heterocycles **A** with heteroallenes or cyclic anhydrides **B** to generate alternating copolymers (AB)_n in the so-called ring-opening copolymerisation (ROCOP).⁵ Prominent examples include CO₂/epoxide ROCOP forming polycarbonates or cyclic anhydride/epoxide ROCOP forming polyesters.^{6–8} Consequently, ROCOP has been identified as a promising methodology for the utilization of globally accumulating CO₂ waste.⁹ However, sulfur-containing variants also exist, such as cyclic thioanhydride/epoxide ROCOP forming poly(ester-*alt*-thioesters) or CS₂/epoxide ROCOP yielding poly(thiocarbonates) with improved photochemical and oxidative degradability compared to their related all-oxygen analogues.^{10–22} Thermal properties can also be improved by formal sulfuration as recently reported for CS₂/oxetane copolymers, which are semi-crystalline, whereas the CO₂/oxetane analogues are amorphous.^{23–25} Moving to more complex monomer mixtures comprising three monomers **A**, **B** and **C** (e.g. epoxide

A, phthalic anhydride (PA) **B** and CO₂ **C**) yield either statistical terpolymers (poly(ester-carbonates), [(AB)_r(AC)_n]_m) or block terpolymers (polyester-*b*-polycarbonates, (AB)_r(AC)_m).^{26–30} In these cases, the monomer sequences usually depend on catalyst selection. In the cases of sulfurated monomers, further insights into new terpolymerisation processes have been made. We, for example, recently realised sequence selective ring-opening terpolymerisation (ROTERP) of ternary monomer mixtures comprising phthalic thioanhydride (PTA), CS₂ or PhNCS and monosubstituted epoxide (propylene oxide PO and butylene oxide BO).^{31–34} Here, a simple lithium catalyst (e.g. lithium benzyloxide LiOBn) selectively forms poly(ester-*alt*-ester-*alt*-heterocarbonates). In another work directly relevant to this report, we achieved statistical terpolymerisation of CS₂ and CO₂ with epoxides by employing heterobimetallic Cr(III)Rb catalysts.³⁵ Here, CO₂ insertion into alkoxide intermediates formed from epoxide ring-opening appeared to be kinetically favourable over CS₂ insertion, so that the resulting terpolymers mostly contained all-oxygen carbonates and few sulfur-containing thiocarbonate links. Although there was some control over the amount of CS₂ vs. CO₂ incorporation by adjusting the amount of initially supplied CS₂ in the starting monomer feed, the obtained molecular weights deteriorated particularly with higher CS₂ loadings.

Aiming to expand the monomer scope of CO₂ terpolymerisation with sulfurated monomers, we hypothesized that PTA/CO₂/epoxide ROTERP could be possible, which we investigate here, particularly in relation to the parent CO₂/epoxide and PTA/epoxide ROCOPs (Fig. 1).

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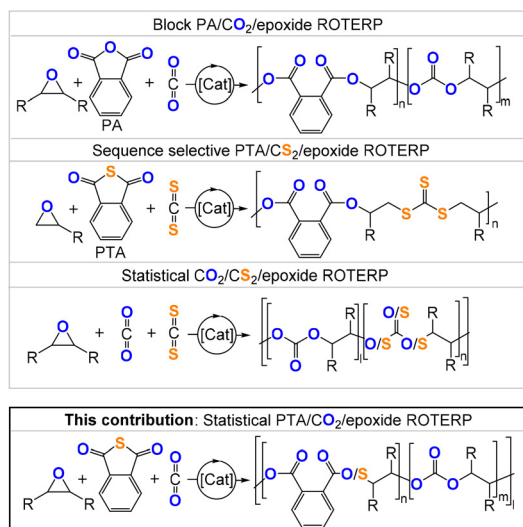


Fig. 1 Comparison of the literature-reported ROTERP and the ROTERP presented in this contribution; [Li] = LiOCH₂Ph (LiOBn), R = Me, Et, -(C₄H₉)_n.

Results and discussion

We hypothesized that in order to achieve the terpolymerisation of PTA, CO₂ and epoxides, a catalyst needs to be active in the parent copolymerisations of CO₂ with epoxides and PTA with epoxides, respectively. Given the precedence for heterobimetallic and Cr(III)-containing catalysts in CO₂/epoxide and PTA/epoxide ROCOP, we decided to employ a series of Cr(III)AM (AM = Li, Na, K, Rb, Cs) L^XCr^{AM} complexes based on binucleating ligands L^XH₂ (Fig. 2) in an easy-to-perform, low-pressure PTA/CO₂/cyclohexene oxide (CHO) ROTERP.^{36,37}

To explore how catalyst selection influences the new ROTERP, we synthesized a range of different ligands L^XH₂ fea-

turing aromatic backbones bearing electron-donating and electron-withdrawing substituents, and aliphatic backbones of varying rigidity. Metalation was achieved in a straightforward fashion by following our recently published procedure.³⁵ The treatment of L^XH₂ with Cr(OAc)₂ in acetonitrile at room temperature, followed by aerobic oxidation in the presence of additional acetic acid, yields L^XCr, *i.e.*, ligands L^X coordinated to a CrOAc moiety, which we could crystallographically verify for L²Cr (Fig. 2). A consecutive reaction with alkali metal acetates AMOAc (AM = Li, Na, K, Rb, Cs) in refluxing MeOH yields L^XCr^{AM} (ESI section S2†) as brown or red powders after the removal of all solvents, which were characterised by HR-ESI MS, IR and elemental analyses confirming their heterobimetallic nature. With a series of L^XCr^{AM} catalysts in hand, we then turned towards their application in PTA/CO₂/CHO ROTERP with 1 eq. of L^XCr^{AM}:100 eq. of PTA:1000 eq. of CHO, 4 bar CO₂ pressure and 100 °C (ESI section S3†). Under these conditions, terpolymerisation can be performed in screw-cap glass vessels, which obviates the need for steel reactor set-ups as are commonplace in CO₂ ROCOP. At the end of the reaction, ROTERP was terminated by the addition of MeOH to the cooled-down reaction mixture. All polymers were then isolated from DCM/MeOH and THF/pentane by repeated precipitation, yielding off-white colourless powders in typical yields of 50–60% with respect to the consumed CHO.

The analysis of the precipitated polymers by ¹H, ¹³C and 2D NMR spectroscopy reveals the formation of terpolymers comprising carbonate, ester and thioester links, as exemplified in Fig. 3. The ¹H NMR spectrum shows tertiary CH resonances between δ = 5.35 and 4.90 ppm, which correlate to the R-(C=O)-O-R ester units at δ = 164.4 and 168.8 ppm in the ¹³C NMR spectrum, as determined by ¹H-¹³C HMBC spectroscopy. Similarly, the tertiary CH resonances between δ = 4.90 and 4.50 ppm correlate to R-O-(C=O)-O-R carbonate groups at δ = 151.0 and 156.0 ppm, while the resonances between δ = 4.10 and 3.80 ppm correlate to R-(C=O)-S-R thioester groups at δ = 190.0 and 194.0 ppm. Only trace amounts of poly(thio) ether links from CHO (or CHS *vide infra*) homopolymerisation could be observed as being part of the polymers for all catalysts comprising Na–K. However, for the Li-containing catalyst (Table 1, run #7), *ca.* 21% (thio)ether links are formed in the terpolymerisation. Notably in all cases, the respective carbonyl regions in the ¹³C NMR spectrum for the quaternary ester, thioester, and carbonate carbons are highly complex, showing multiple, ill-defined, and overlapping resonances in the diagnostic regions, which suggest statistical terpolymer formation. This notion could be confirmed by following the polymerisation by ¹H NMR analysis of aliquots removed at regular time intervals, which indeed revealed continuous PTA consumption and uniform generation of ester, carbonate and thioester links in the same ratio as observed in the final isolated polymers. Finally, IR spectroscopy of the isolated polymers further supports the presence of carbonate and ester ($\tilde{\nu} \approx 1734.0 \text{ cm}^{-1}$) in addition to thioester ($\tilde{\nu} \approx 1676.0 \text{ cm}^{-1}$) links. The materials are amorphous with *T*_g values between 118 and 128 °C with no clear trend between composition and glass transition. GPC

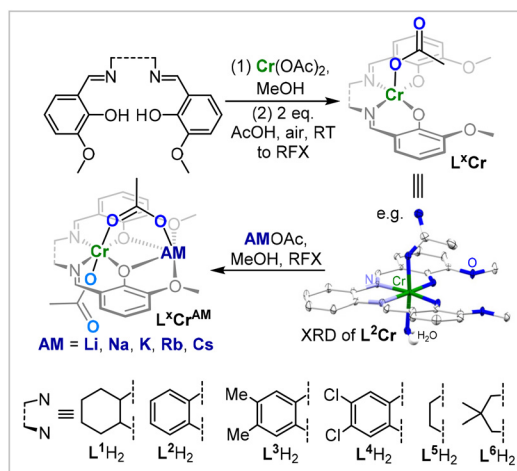


Fig. 2 Synthesis of L^XCr^{AM} as well as the solid-state structure of L²Cr, with H atoms apart from co-crystallised H₂O and co-crystallised MeOH omitted for clarity; ellipsoids set at 40% probability.



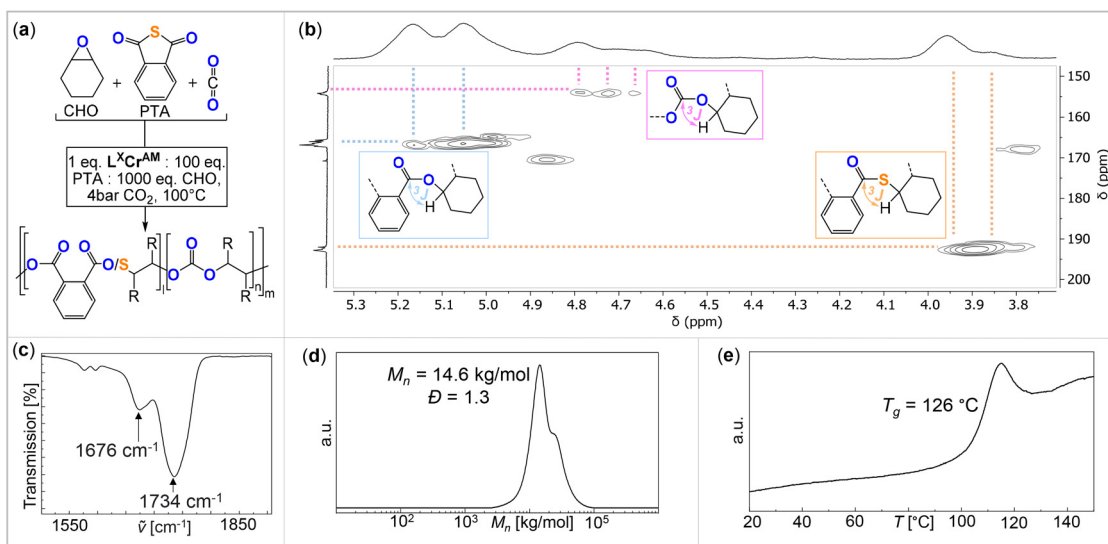


Fig. 3 (a) Schematic representation of the ROTERP reaction. (b) ^1H - ^{13}C HMBC NMR spectrum (25 °C, CDCl_3), (c) IR spectrum, (d) SEC trace calibrated against a narrow polystyrene standard and (e) DSC thermogram of the polymer corresponding to Table 1, run #1.

Table 1 PTA/ CO_2 /CHO ROTERP polymerisation table and comparison with parent ROCOPs

Run	Cat. ^a	TOF ROTERP ^b [h ⁻¹]	Final TON ^c	Ester : thioester : carbonate ^d (%)	M_n^e [kg mol ⁻¹]	D^f	TOF (CHO/ CO_2) ^g [h ⁻¹]	TOF (CHO/PTA) ^h [h ⁻¹]	LC ⁱ
#1	$\text{L}^1\text{Cr}^{\text{Rb}}$	200 ± 5	520	14 : 9 : 77	14.6	1.3	161 ± 1	51 ± 3	136 ± 1
#2	$\text{L}^2\text{Cr}^{\text{Rb}}$	189 ± 7	570	16 : 9 : 75	10.3	1.2	149 ± 20	70 ± 6	129 ± 17
#3	$\text{L}^3\text{Cr}^{\text{Rb}}$	122 ± 8	460	16 : 12 : 72	7.9	1.2	110 ± 2	85 ± 8	103 ± 4
#4	$\text{L}^4\text{Cr}^{\text{Rb}}$	111 ± 9	280	52 : 19 : 23	5.1	1.3	40 ± 4	40 ± 5	40 ± 5
#5	$\text{L}^5\text{Cr}^{\text{Rb}}$	367 ± 32	440	23 : 11 : 66	12.1	1.3	273 ± 17	144 ± 9	229 ± 14
#6	$\text{L}^6\text{Cr}^{\text{Rb}}$	223 ± 13	550	17 : 7 : 76	13.3	1.3	261 ± 7	41 ± 1	208 ± 5
#7	$\text{L}^1\text{Cr}^{\text{Li}}$	84 ± 4	270	55 : 18 : 27 ^k	5.5	1.4	38 ± 4 ^j	84 ± 5	72 ± 5
#8	$\text{L}^1\text{Cr}^{\text{Na}}$	66 ± 2	260	16 : 13 : 71	6.4	1.2	76 ± 3 ^j	32 ± 4	63 ± 3
#9	$\text{L}^1\text{Cr}^{\text{K}}$	360 ± 15	500	15 : 20 : 65	16.9	1.2	127 ± 4 ^j	33 ± 1	94 ± 3
#10	$\text{L}^1\text{Cr}^{\text{Cs}}$	195 ± 8	400	19 : 20 : 61	13.0	1.3	162 ± 15 ^j	58 ± 2	121 ± 10

^a Terpolymerisation at 1 eq. cat.:100 eq. PTA:1000 eq. CHO, $T = 100$ °C, 4 bar CO_2 . ^b Turnover frequency (TOF) determined by a linear fit to the eq. of CHO conversion per eq. of catalyst vs. time plot. Data points are excluded once conversion vs. time plots deviate from linearity. ^c Final turnover number (TON) at the specific endpoints of the polymerisations as depicted in the conversion vs. time plots of ESI section S3. ^d Relative ratio of ester (4.9–5.2 ppm) versus thioester (3.7–4.2 ppm) versus carbonate (4.4–4.9 ppm) linkages assessed by the relative integrals of the tertiary CH resonances in the corresponding ^1H NMR spectrum of the precipitated polymers. ^e Determined by SEC measurements conducted in THF using narrow MW polystyrene standards to calibrate the instrument. ^f $D = M_w/M_n$. ^g CHO/ CO_2 copolymerisation at 1 eq. of Cat.:1000 eq. of CHO, $T = 100$ °C, 4 bar CO_2 . ^h CHO/PTA copolymerisation at 1 eq. of Cat.:100 eq. of PTA:1000 eq. of CHO, $T = 100$ °C. ⁱ Proportionate linear combination (LC) of the TOFs of the parent ROCOPs. ^j According to ref. 35. ^k ca. 21% of ether and thioether links are part of the final polymer.

analysis of the isolated polymers reveals molecular weights of $M_n = 5.1$ – 16.9 kg mol⁻¹ and bimodal distributions with $D = 1.2$ – 1.4 . We observed linearly increasing molecular weights with reaction progress, indicative of a controlled ROTERP process, albeit with bimodal molecular weight distributions formed from the beginning of the polymerisation (Fig. 4(a)). The bimodal distribution in each case comprises two narrow overlapping distributions of which one exhibits approximately half the molecular weight of the other, and the ratio of the two remains constant throughout the polymerisation. It is well established that bimodality in epoxide ROCOP catalysis stems chain transfer with protic impurities.^{38,39} Usually one distribution of chains is formed from an ROCOP process initiated by monofunctional initiators X, which are part of the catalyst,

yielding α -X, ω -OH-chains, while the second distribution of chains is formed *via* ROCOP initiated from either H₂O or diol impurities in the monomers *via* chain-transfer processes yielding α , ω -OH-telechelic chains. Indeed, in all our catalysts $\text{L}^X\text{Cr}^{\text{AM}}$, acetate coligands, which can be expected to serve as monofunctional initiators, are introduced which would produce aliphatic ester chain ends and these were identified to be part of the isolated polymers by ^{13}C NMR ($\delta(\text{C}^q) = 171$ ppm). To test whether chain transfer with diol impurities is the origin of bimodality, we deliberately added the bifunctional alcohol 1,4-benzenedimethanol (BDM) to an ROTERP run (employing 1 eq. of $\text{L}^1\text{Cr}^{\text{Cs}}$:20 eq. of BDM:100 eq. of PTA:1000 eq. of CHO, 4 bar CO_2 and identical reaction time and temperature). Compared to the run without BDM, we



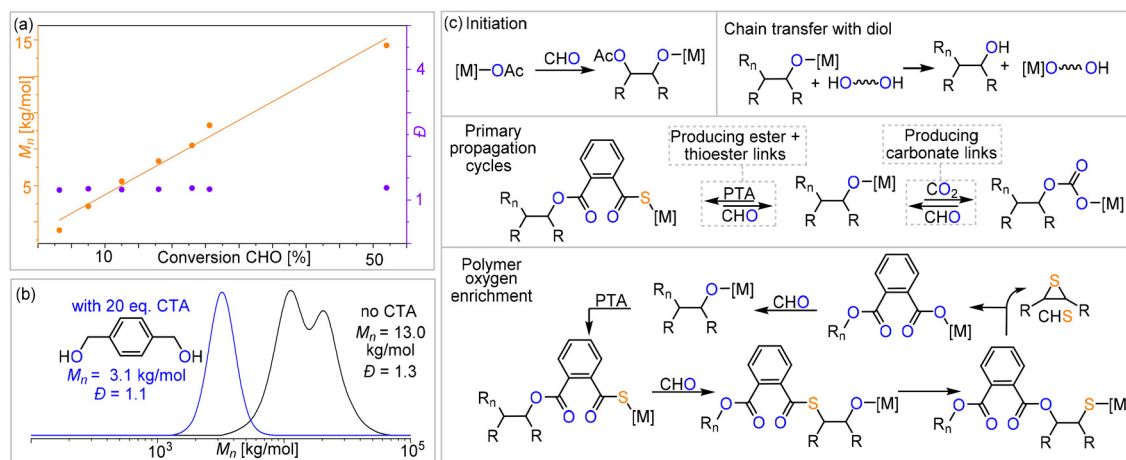


Fig. 4 (a) Plot of conversion vs. M_n and D for Table 1 run #1 ROTERP; note that due to the viscosity of the reaction mixture, no aliquots could be taken between 25% and 55% conversions. (b) Overlaid GPC traces of Table 1 run #10 with and without the addition of 20 equiv. of 1,4-benzendi-methanol as a chain transfer agent. (c) The proposed PTA/ CO_2 /CHO ROTERP mechanism and intermediate speciation. [M] = metal catalyst, R_n = polymer chain, and $R = -(\text{C}_4\text{H}_8)-$.

observed a clear decrease of the obtained M_n from 13.0 to 3.1 kg mol^{-1} and furthermore, a narrowed monomodal distribution in the latter case with $D = 1.1$. NMR analysis of this polymer unambiguously shows that BDM has been incorporated into the polymer structure. All findings support that BDM acts as a chain transfer agent by increasing the number of telechelic chains formed so that the polymer samples predominantly comprise α,ω -OH telechelic chains. This leads to apparent monomodality with decreased molecular weights at comparable monomer conversion, as now a similar number of monomers have to be distributed across more initiators. On a side note, our experiments also show that our new ROTERP tolerates chain-transfer agents to control the molecular weights and the chain-end chemistry. Our finding suggests that bimodality in the first place is caused by diol or H_2O impurities in the liquid monomers at the beginning of the polymerization, impurities introduced during the setup of the reaction, or impurities in the CO_2 supplied throughout the reaction since the degree of bimodality remains constant throughout ROTERP. This variable is intrinsically hard to control between monomer batches and reactions although all reaction parameters and purification methods are kept identical. Accordingly, the degree of bimodality varies between runs, as shown in Table 1. This variability furthermore extends to repeat runs although reaction rates, polymer compositions and molecular weights are reproducible. In terms of catalyst dependence, the precise ratio of ester:carbonate:thioester links depends on both the alkali metal and the backbone choice with regards to $\text{L}^{\text{X}}\text{Cr}^{\text{AM}}$ (Table 1), although no obvious trends could be identified. This suggests that an interplay, rather than a simple combination, of the electronic and steric nature of the chromium coordination site alongside the one imposed through alkali metal choice determines the respective insertion events. However, regardless of the catalyst employed, the ester:thioester ratio observed is always lower than the

perhaps expected 1:1 ratio resulting from PTA insertion following propagation, implying the loss of sulfur centres and concurrent oxygen enrichment of the polymer during ROTERP. Confirming that “sulfur-loss” is an inherent side-process of the PTA-CHO insertion events, we performed a separate PTA/CHO ROCOP reaction (1 eq. of $\text{L}^{\text{1Cr}^{\text{CS}}}$:1000 eq. of PTA:1000 eq. of CHO) and observed an ester to thioester ratio of *ca.* 1.8:1 deviating substantially from the ideal 1:1 ratio. The broadened polydispersity of the obtained polymer ($M_n = 19.8 \text{ kg mol}^{-1}$ and $D = 1.6$) also suggests that PTA/CHO insertion events during ROTERP could contribute to bimodality and the different extents to which this occurs for different catalysts could also cause different degrees of bimodality between different catalysts, as shown in Table 1. In fact, we observed a similar oxygen enrichment process of the polymer in our previous study on CS_2 /CHO ROCOP and were able to conclusively show that O/S exchange processes at the chain end and consecutive thiirane elimination cause this.¹⁸ Accordingly, ^1H NMR aliquot analysis of the ROTERP process reveals steadily increasing amounts of thiirane cyclohexene sulfide (CHS) being generated alongside propagation, which accounts for the apparent sulfur loss and oxygen enrichment of the polymer. Given all our observations above, we propose the following mechanism (Fig. 4) in which initiation either happens from acetate coligands generating an alkoxide *via* CHO insertion or from deprotonated diol impurities after which two primary propagation cycles occur. Among them, CO_2 *versus* PTA insertion from the common alkoxide intermediate determines the (thio)ester:carbonate linkage ratio. Analogous to our previous report on CS_2 /CHO ROCOP, polymer oxygen enrichment is proposed to originate from an O/S rearrangement step from alkoxide chain ends adjacent to thioester links that eliminate CHS to create a carboxylate chain end, which then inserts CHO to generate a diester link.³⁵ This effectively turns PTA and 2 equivalents of CHO into a diester link and



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