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# Techno-economic assessment of aluminum as a clean energy carrier to decarbonize remote industries†

Pascal Boudreau,<sup>id</sup>\*<sup>a</sup> Michael Johnson<sup>b</sup> and Jeffrey M. Bergthorson<sup>a</sup>

The energy sector is transitioning to a low-carbon era requiring the wide use of renewable energy sources, mainly wind and solar. In this context, aluminum could serve as a sustainable energy carrier as it stores energy in a safe and compact way. It could be used to help decarbonize remote communities and industries, trade energy on a global scale, or provide seasonal energy storage. The Hall–Héroult process, reducing aluminum oxides to aluminum, is already a technology deployed at an industrial scale. The maturity of this industry could therefore be leveraged to store electricity. To convert aluminum back to power, it can be fully oxidized with high-temperature liquid water. The hydrogen and high-temperature heat produced can then be converted to power using a combination of heat engines and/or fuel cells. For this concept to be viable, the oxides produced must be collected and reduced in a sustainable way. In this work, aluminum recharging costs were evaluated by reviewing the current reduction process and the literature available on the development of inert anodes, a technology enabling carbon-free smelting. Results show that aluminum can be cost-competitive on a chemical energy basis with most common hydrogen carriers discussed in the literature. To contextualize the findings, a remote mine case study integrates transportation, storage and power generation costs for aluminum, compared to liquefied hydrogen and ammonia. The analysis reveals that aluminum is comparable to other carbon-free solutions, although they all currently remain more expensive than diesel fuel at an input electricity price of \$30/MWh<sub>e</sub>. Aluminum emerges as marginally more expensive than the direct use of ammonia, while avoiding concerns related to toxicity and NO<sub>x</sub> emissions. This study thus positions aluminum as a promising energy carrier that merits further consideration in various other applications.

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## 1 Introduction

As electrical grids expand and rely more heavily on variable renewable electricity sources to meet a growing demand, some changes in energy management will occur on a global scale. Cheap and efficient storage will be needed on a wide range of sizes and time scales to ensure energy can be dispatched when and where it's needed. Chemical energy carriers are likely to be needed to smooth out seasonal variations in renewable power generation, decarbonize hard to abate sectors and remote communities and industries, or to facilitate the exchange of clean energy on a global scale.<sup>1,2</sup> Some countries, such as

Germany and Japan, have already recognized their future need to import clean energy in order to reach full decarbonization.<sup>3,4</sup>

As an alternative to widely discussed hydrogen-based energy carriers, some metals have been proposed as promising candidates, since they store energy in a compact and stable form.<sup>5–8</sup> These metals, such as iron, aluminum, magnesium, or zinc, are safe and can be easily handled and shipped to end-users. They can be stored inexpensively and, ultimately, can be either combusted in air to produce heat, or reacted with water to generate heat and hydrogen, both of which can be used for power generation.<sup>9,10</sup> The other byproducts are solid oxide particles that must be collected, returned to the metal producer, and reduced back into fuel to ensure the sustainable utilization of these resources. Provided that the reduction step is carbon-free, this has the potential to create a clean utilization cycle, facilitating the use of renewable energy in sectors, such as remote industries, in need of a clean fuel to decarbonize.

Among metal fuels candidates, aluminum represents a promising option due to its high energy density, safety, and

<sup>a</sup> Alternative Fuels Laboratory, Department of Mechanical Engineering, McGill University, Rm 270 Macdonald Engineering Building, 817 Sherbrooke Street West, Montréal, H3A 0C3, Canada. E-mail: pascal.boudreau@mail.mcgill.ca

<sup>b</sup> Siemens Energy Canada Limited, 2200 rue Courval, Lachine, H8T 3H1, Canada

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abundance. However, to challenge other alternatives, the clean aluminum fuel cycle must not only be technically viable but, most importantly, cost competitive and sustainable. Previous work studying aluminum as an energy carrier employed a simplified approach when estimating production costs. These studies considered only the costs associated with oxides and electricity as inputs,<sup>11</sup> or omitted capital costs from their analysis.<sup>12</sup>

This work presents a comprehensive assessment of the cost of the aluminum fuel cycle. An in-depth analysis of the reduction process provides insights on the production cost of current aluminum smelting, and the economic impact of using a novel carbon-free reduction process is estimated. Cost models for storage, transportation, and power generation are formulated to assess the overall cost for each cycle. A similar analysis is then performed for two alternative carbon-free energy carriers, liquefied hydrogen and ammonia, both extensively studied in previous work. This enables aluminum to be compared to two widely discussed energy carriers within the framework of supplying clean electricity to remote industries in need of an alternative to diesel fuel.

## 2 Aluminum as an energy carrier

As demonstrated by its use in rocket propulsion, aluminum is of particular interest as a fuel because of its high energy content with respect to both mass and volume, storing around 8.6 MWh<sub>ch</sub>/tonne.<sup>13</sup> Aluminum is inherently safe due to a thin oxide layer that forms on its surface upon contact with air, making it effectively inert to water at ambient conditions. This contrasts with other metals, such as the alkalis, which are prone to react violently in such conditions. This passivating oxide layer is a few nanometers thick and protects the bulk material from further oxidation at ambient conditions, which simplifies storage requirement and avoids energy losses over time.

Aluminum can be oxidized with water to release approximately half of its stored energy in the form of heat and the other half as hydrogen, offering the potential for a wide range of utilization schemes.<sup>10,14–16</sup> The complete reaction of coarse aluminum particles has been recently demonstrated with the use of high-temperature liquid water without the need for any catalyst.<sup>17</sup> Operating at higher temperatures enables the production of heat that can be recuperated for power generation, thereby increasing the efficiency of the cycle. As storing electricity in any energy carrier leads to significant losses (and costs), it is necessary to maximize the conversion back to electricity to make any cycle viable. Moreover, a high-temperature high-pressure reaction regime enables the use of bigger particles as the fuel, which, in turn, lowers the risk of dust explosions, identified as a safety hazard for fine metal powders.<sup>18</sup>

## 3 Aluminum production

Aluminum reduction, performed industrially using the Hall-Héroult electrowinning process, is a critical step when assessing

the cost and sustainability of the aluminum fuel cycle. In this process, smelter grade alumina (SGA) is fed to a molten cryolite (Na<sub>3</sub>AlF<sub>6</sub>) electrolytic bath where it dissolves and is reduced using an electric current. In modern pots, up to 600 kA flow from the carbon anodes, through a cryolite bath kept at around 940–970 °C, onto the cathode where aluminum is reduced.<sup>19,20</sup> SGA is added to the bath periodically to maintain proper alumina concentration, therefore achieving maximal energy efficiency. Low alumina concentration also induces the occurrence of the so-called “anode effect”, a phenomenon characterized by a sudden surge in pot voltage that results in thermal instability and the emissions of harmful perfluorocarbon (PFC).<sup>19,21</sup> Modern smelters use dozens of pre-baked carbon anodes per cell, which are fixed to a rod and attached to the busbar delivering the current. Anodes are consumed during the process, producing CO<sub>2</sub>, and need to be replaced every 20 to 25 days.<sup>19</sup>

From Faraday's law of electrolysis, the specific electrical energy consumption of the aluminum electrowinning process can be derived to yield eqn (1). The energy consumption EC, in MWh<sub>e</sub>/t, is calculated from the voltage *V*, the number of electrons transferred in the reaction *n* (3 moles of e<sup>-</sup> per mole of Al), the Faraday constant *F*, the current efficiency CE, and aluminum molar mass *M*<sub>Al</sub> (26.98 g mole<sup>-1</sup>).

$$EC = \frac{V \cdot n \cdot F}{CE \cdot M_{Al} \cdot 3600} = \frac{2.98 V}{CE} \quad (1)$$

The energy consumption, or efficiency, of the cell is therefore a function of the voltage requirement and the current efficiency, defined as the mass ratio of the metal reduced to the theoretical value. This efficiency is over 95% in modern smelters and is less than 100% due to the inevitable back reaction of anodic products (CO<sub>2</sub>) with cathodic products (Al) which reverses the reduction reaction.<sup>22</sup>

Thermodynamically, the theoretical minimum cell voltage required to drive a reaction can be calculated using the change in standard Gibbs energy *G*<sup>0</sup>, as described in eqn (2). For alumina reduction, this amounts to 2.25 V as shown in eqn (3).

$$E^0 = \frac{-\Delta G^0}{nF} \quad (2)$$

In practice many losses add up, making this voltage significantly higher. The first 1.22 V is required to drive the alumina reduction using a carbon anode, as shown by eqn (3)–(5). Ohmic losses due to gas bubbles, external equipment, the anode, and the cathode are responsible for around 1.10 V.<sup>23</sup> The bath resistive loss, dependent on the anode to cathode distance (ACD), represents around 1.33 V.<sup>23</sup> These losses contribute to heating the cell to maintain the bath in its liquid state, since thermal losses are inevitable through the sides of the cells. This is crucial to keep a side ledge of frozen cryolite to protect the cell lining from the highly corrosive electrolyte.<sup>24</sup> Overpotentials losses, which are required to achieve an increase in the reduction reaction kinetics, account for the remaining





Fig. 1 Voltage breakdown of current electrolytic cell using carbon anodes (left) compared to an hypothetical inert anode cell benefiting from low overvoltage losses (middle), and to the same inert anode cell with a wettable cathode allowing for a lower ACD (right). Assuming a current efficiency of 95%, these voltages result in an electrical consumption of 13, 15 and 13.3 MWh<sub>e</sub>/t<sub>Al</sub> respectively. When comparing to the energy stored in aluminum, this corresponds to efficiencies of 66.2%, 57.4%, and 64.7%, when only considering electricity as the energy input.

voltage required. The total voltage breakdown for carbon-anode reduction can be seen in Fig. 1.



## 4 Aluminum-fuel cycle cost assessment

The aluminum-fuel cycle consists of four main components: aluminum production, transportation, storage, and power generation as shown in Fig. 2. Generic cost assessment models for each of component are outlined in Sections 4.1–4.3. These models can be further customized to accommodate various case studies, for example by varying the input electricity cost for specific regions, varying the size of the power generation



Fig. 2 Aluminum fuel cycle consisting of four main components: aluminum production, transportation, storage, and power generation.

system, or removing transportation costs to study localised long-duration energy storage use-cases.

### 4.1 Aluminum recharging costs: Power-to-Al

**4.1.1 Alumina cost.** The SGA fed to the smelters is produced from bauxite refined using the Bayer process. The ore is first ground and digested in a solution of caustic soda (NaOH) at temperatures of 100–260 °C.<sup>25</sup> Following the filtration of insoluble red mud residues, the resulting liquor is cooled to allow aluminum trihydrates (Al(OH)<sub>3</sub>) to precipitate. The recovered crystals are then washed, classified, and calcined at temperature of 950–1100 °C, which yields alumina (Al<sub>2</sub>O<sub>3</sub>).<sup>25</sup>

The alumina transformed in smelters today shifted from being finer “floury” α-Al<sub>2</sub>O<sub>3</sub> to coarser “sandy” γ-Al<sub>2</sub>O<sub>3</sub> over the years.<sup>26,27</sup> This change mainly resulted from the adoption of point-feeders to inject alumina in the cryolite baths, which require better flowability to control the injection and thus the concentration of alumina in the reduction cells. SGA must also exhibit a low attrition index which quantifies its breakdown during handling.<sup>26</sup> A high attrition index can lead to a higher concentration of fines (% < 45 μm) and super fines (% < 20 μm) in the alumina, which are linked to low current efficiency and an increase in anode effects.<sup>28</sup> Specific surface area is also of particular importance as SGA is used in dry scrubbers to filter toxic hydrogen fluoride (HF) emissions from the pot exhaust gases and help recycle the fluoride back to the cryolite bath.<sup>29</sup> HF emissions have been identified to mainly come from the presence of structural hydroxide (–OH) in the alumina, which underlines the importance of the calcination process to reach the desired aluminum oxide form. Loss on Ignition (LOI) is used to quantify the amount of structural –OH present in a sample, as it characterizes the alumina weight loss observed when heated from 300 °C to 1000 °C.<sup>30</sup>

The direct recyclability of the oxides produced by the aluminum–water reaction will therefore depend on their type and morphology. Reacting aluminum with water close to its critical point (373 °C) showed that boehmite (γ-AlOOH) was formed as the product.<sup>17</sup> In that case, calcination would likely be needed prior to each reduction step, to obtain the desired SGA composition. Calcination alone requires around 1.6 MWh of thermal energy per tonne of aluminum produced, which is currently provided using natural gas.<sup>31</sup> Alumina processing should eventually be decarbonized, either through direct electrification, the use of clean fuels, or even concentrated solar power.<sup>32</sup>

Used in a closed cycle, the alumina only needs to be purchased once at a certain market price  $P_{\text{Al}_2\text{O}_3}$ . Although it can also be eventually be sold back to the market once it’s no longer needed, this revenue discounted to present value is negligible compared to the initial purchase cost, and has been neglected in this study. As losses throughout the cycles are inevitable, an oxide collection efficiency  $\eta_{\text{coll}}$  is defined as the ratio of alumina recuperated from one cycle to the next. This is used to determine the amount of alumina required to be purchased to offset losses. A fixed market price is assumed over the years although the price might change due to alumina market fluctuations. The number of cycles  $N_{\text{cyc}}$  performed over



a year will also affect the recharging cost, as the initial cost of alumina is amortized annually, using a capital recovery factor CRF defined by eqn (6), where  $i$  is the annual interest rate, and  $n$  is the period of use, in years.

$$\text{CRF} = \frac{i(1+i)^n}{(1+i)^n - 1} \quad (6)$$

This period,  $n_{\text{Al}_2\text{O}_3}$ , represents the time required to deplete the initial alumina purchased, and is a function of  $\eta_{\text{coll}}$  and  $N_{\text{cyc}}$ , defined by eqn (7).

$$n_{\text{Al}_2\text{O}_3} = \frac{1}{(1 - \eta_{\text{coll}}) \cdot N_{\text{cyc}}} \quad (7)$$

The alumina cost per cycle  $C_{\text{Al}_2\text{O}_3}$ , in  $\$/\text{t}_{\text{Al}}$ , is therefore calculated using eqn (8).

$$C_{\text{Al}_2\text{O}_3} = 1.9 \cdot P_{\text{Al}_2\text{O}_3} \left( \frac{\text{CRF}}{N_{\text{cyc}}} + (1 - \eta_{\text{coll}}) \right) \quad (8)$$

**4.1.2 Aluminum production cost.** Aluminum production costs can vary depending on the smelter's reduction technology, its location, the availability of cheap electricity and the integration of supply chain operations, such as alumina refining or bauxite mining. To estimate the production cost of aluminum, cost breakdowns from Alcoa<sup>33</sup> and Norsk Hydro<sup>34</sup> were compared to Rio Tinto's 2021 total cash cost for their Canadian smelters.<sup>35</sup> By combining this information with calculations guided by knowledge of the aluminum production process, estimates have been derived for each cost category, as shown in Fig. 3, and detailed in Sections 4.1.2.1 to 4.1.2.3. Rio Tinto's total cost includes all expenses incurred before casting, excludes depreciation of assets, and assumes alumina is purchased at a market price of  $\$271/\text{t}$ .<sup>35</sup> With around 1.9 tonnes of alumina needed per tonne of aluminum produced, alumina accounts for

$\$515/\text{t}_{\text{Al}}$  of this production cost. In the context of the aluminum-fuel cycle, this alumina purchasing cost needs to be replaced by the amortized cost per cycle, shown in eqn (8).

**4.1.2.1 Electricity.** The electricity consumption of the most-efficient Hall-Héroult cells can currently reach around  $12 \text{ MWh}_e/\text{t}_{\text{Al}}$ <sup>20,36</sup> but the average modern smelters consume closer to  $13 \text{ MWh}_e/\text{t}_{\text{Al}}$ , consistent with the voltage drop and current efficiency presented in Fig. 1.<sup>37</sup> This energy consumption, at an estimated electricity rate of  $\$23/\text{MWh}_e$ , yields  $\$300/\text{t}_{\text{Al}}$  and represents 26% of the total production cost. Such an electricity rate is realistic considering Rio Tinto's operations in Canada are powered by privately owned hydropower plants.<sup>38,39</sup> Furthermore, this is consistent with electricity rates for large industries in the province of Quebec, mostly supplied by hydropower, that were  $\$26/\text{MWh}_e$  in 2022.<sup>40</sup>

**4.1.2.2 Anodes.** Approximately 400–450 kg of carbon anodes are consumed per tonne of aluminum produced.<sup>19,37</sup> They are made of around 80% of petroleum coke and 20% coal tar pitch,<sup>41</sup> having a market price of about  $\$300/\text{t}$  and  $\$620/\text{t}$  respectively.<sup>34</sup> The resulting material cost is rounded to  $\$170/\text{t}_{\text{Al}}$  to account for baking loss and other conversion costs.<sup>42</sup>

**4.1.2.3 OPEX.** The operational expenditure (OPEX) category includes insurance, maintenance, and labour costs. This can vary from one smelter to another depending on location and equipment used. This category also covers additional material costs for cryolite and aluminum fluoride, as around 19 kg of bath material are lost per tonne of aluminum produced.<sup>19</sup> Pot relining costs, accounting for an estimated  $\$30\text{--}50/\text{t}_{\text{Al}}$  for an average lifetime of 1600 to 2500 days and a cost of around  $\$300\,000$  per cell, can also be included in this category.<sup>43</sup> Differentiating what falls into the OPEX and Other categories is however difficult, and some overlaps are probable from one source to the other. Costs of  $\$132/\text{t}_{\text{Al}}$  and  $\$45/\text{t}_{\text{Al}}$  were respectively estimated for these two categories to approximately fit the industry cost breakdowns.

**4.1.3 Plant depreciation cost.** Aluminum smelting is a capital-intensive industry and the investment needed to build smelters must also be considered in the total aluminum cost. The depreciation cost of assets, or capital expenditure (CAPEX), for this industry is, however, hard to estimate since values found in literature vary widely. The variation can be explained from regional differences in costs, mainly between western countries and China, but also from the year of construction and the plant capacity. Based on publicly available data (see ESI,† Fig. S1), a capital cost of  $\$5000$  per tonne per year of production is assumed in this study. From this CAPEX, an annualized capital cost is calculated using a CRF, defined by eqn (6). The annual interest rate  $i$  is taken to be 8%, to reflect the cost of debt used in Lazard's leveled cost of energy analysis.<sup>44</sup> Assuming the smelter has a lifetime,  $n$ , of 50 years, the amortized CAPEX yields a cost of  $\$409/\text{t}_{\text{Al}}$ . This lifespan is assumed since smelters can operate on many decades as demonstrated by the Kitimat plant commissioned in the 1950s.<sup>45</sup> Additionally, the annualized CAPEX shows a rather



Fig. 3 Aluminum production cost breakdown estimated based on Rio Tinto's total production cost for Canadian smelters,<sup>35</sup> and cost breakdowns from Alcoa<sup>33</sup> and Norsk Hydro.<sup>34</sup> All costs are in US dollars.



low sensitivity to plant life, since reducing it to 40 years (−20%) results in a \$11/t<sub>Al</sub> increase in CAPEX cost (+2.6%).

**4.1.4 Carbon-free aluminum production.** To be sustainable, the aluminum fuel cycle must be free of carbon emissions. To do so, the electricity powering the smelter needs to be clean, which can be achieved using renewable sources, such as wind, solar or hydro. The upstream emissions generated from alumina mining and processing also need to be mitigated. Assuming a large number of cycles with a high collection efficiency and minimal addition of fresh alumina for each cycle, alumina emissions can be amortized to a negligible value. Consequently, carbon anodes would be responsible for the only remaining CO<sub>2</sub> emissions in aluminum fuel production. These emissions imperatively need to be eliminated since they range from 170 to 190 kg of CO<sub>2</sub> per MWh<sub>ch</sub> of stored energy, close to the natural gas emission intensity.

**4.1.4.1 Inert anodes technology.** Using inert anodes would cut all carbon from the electrolytic process, thereby eliminating CO<sub>2</sub> and PFC emissions. Research on the topic has gained momentum in the last few decades and such anodes are currently being developed by Elysis. The company hopes to reach commercialization by 2024 and has already built a pilot-scale demonstration cell.<sup>46</sup> The challenge in making inert anodes lies in the development of a material enabling stable operation and low wear rate in a high temperature corrosive environment, while avoiding the contamination of the aluminum produced.<sup>47</sup> Another technology that could be employed to decarbonize aluminum production involves converting alumina to aluminum chloride before the reduction process, maintaining a closed loop for chlorine and carbon and only emitting oxygen. Norsk Hydro is currently developing this process, aiming to achieve pilot-scale production volume by 2030.<sup>48</sup>

**4.1.4.2 Costs reductions.** Apart from reducing carbon emissions, using inert anodes will likely impact aluminum production costs. This technology could have the benefit of increasing cell productivity by 15% while reducing operating costs by 15%.<sup>46</sup> This is due to the reduced frequency at which anodes need to be replaced if a low wear rate is achieved, therefore reducing labor requirements.<sup>42</sup> The cost of anodes could also be significantly cut down, although this will depend on materials and manufacturing methods used, which remain uncertain. Production cost of anodes on a commercial scale were estimated to range as low as \$47–57/t<sub>Al</sub>.<sup>49</sup> The need to build a carbon anode baking plant would also be eliminated for new smelters, which could represent a total CAPEX reduction of up to 30%.<sup>37,50</sup> Table S1 in the ESI† provides a summary of various sources regarding the potential impact of inert anodes on aluminum production costs.

**4.1.4.3 Wettable cathodes.** Removing carbon from the process would, however, increase the energy requirement, as the contribution of eqn (4) to the reduction process would no longer be present. This increase, which could be compensated in part by a reduction in the kinetic overvoltages at the anode,

would result in an overall voltage increase of around 0.63 V, as shown in Fig. 1.<sup>23</sup> To keep the energy requirement close to the initial level, inert anodes would need to be implemented in combination with a wettable cathode. This consists in the use of an inert ceramic coating on the cathode, such as titanium diboride (TiB<sub>2</sub>), to ensure better electrical contact with the reduced aluminum pad sitting at the bottom of the cell. This enables the possibility of operating with a thinner metal pad, thereby reducing the height of the waves formed at its surface due to magnetohydrodynamic effects.<sup>19</sup> The cell could then operate at a smaller anode to cathode distance while avoiding short circuits, reducing the electrolyte resistive losses and increasing reduction efficiency, as seen in Fig. 1. This change in resistive losses and the elimination of carbon oxidation from the process would, however, present a challenge for the cell's thermal balance. Adding better insulation would likely lead to the melting of the frozen side ledge needed to protect the walls from corrosion.<sup>51</sup> New cell designs, such as a vertical anode arrangement, may be required to harness the full potential of both inert anodes and wettable cathodes.<sup>24,37,42</sup>

**4.1.5 Power-to-Al costs.** The total aluminum recharging cost can be obtained by summing the amortized CAPEX, OPEX, anode cost, electricity cost, and alumina cost per cycle. To account for the potential calcination of oxides, an additional 1.6 MWh<sub>e</sub>/t<sub>Al</sub> was also added to the energy requirement. The total recharging cost can therefore be seen with respect to the input renewable electricity cost in Fig. 4. Since inert anodes cells have not been commercialized yet, their impact on the recharging cost is still uncertain and is presented as a range. CAPEX and anodes cost exhibit the greatest potential to reduce fixed costs. The figure shows that with sufficiently low electricity input cost, aluminum fuel could be in the range of \$100/MWh<sub>ch</sub> which roughly compares to diesel fuel at \$1/L.

## 4.2 Transportation and storage costs

To assess the delivered energy cost of aluminum, the storage and shipping costs must be added to the recharging cost.



Fig. 4 Aluminum recharging cost plotted with respect to input electricity cost. Conventional carbon anode recharging cost corresponds to the black line, and is compared to the range in which inert anode smelting technology could fall. The contribution of each cost category is shown with their respective boundaries.



Aluminum fuel is assumed to be transported using a Panamax dry-bulk carrier having a cargo capacity of 80 000 DWT. The cost of such a vessel is estimated around \$40m,<sup>52,53</sup> amortized using a CRF of 9.4%, corresponding to a 8% interest rate  $i$  for an average lifetime  $n$  of 25 years, which is reasonable for dry-bulk carriers.<sup>54</sup> Daily fuel cost  $F$  is calculated assuming a 50% efficient engine running 24 hours per day at a continuous power rating of 10 MW, typically used for Panamax dry-bulk carriers cruising at their design speed of 14.5 knots.<sup>54</sup> Heavy fuel oil (HFO) is assumed to provide the energy for powering the carrier, therefore increasing aluminum's carbon footprint. However, the use of clean fuels is expected to contribute to decarbonizing shipping in the future, with the International Maritime Organization having pledged to reach net-zero by 2050.<sup>55</sup> Although canal fees  $C_{\text{canal}}$  might not be necessary depending on the shipping route, a passage fee of \$188 000 every 12 000 km on average was included as a proxy for this cost in this generic model. This fee corresponds to a 80 000 DWT dry-bulk super vessel crossing the Panama canal.<sup>56</sup> Around half the cargo capacity  $Q$  is used to ship aluminum, to ensure the same vessel can bring back the corresponding amount of oxide to be recycled on the return trip, according to the 1.9 molar mass ratio between alumina and aluminum. The volumetric ratio was not considered, as it was assumed the ship was limited by the weight of the cargo and not by its volume. The shipping duration,  $t_s$ , is calculated by doubling the shipping distance to account for the return trip, and a total of 4 days of downtime per trip is added for handling cargo at the ports  $t_h$ , necessary to load and unload aluminum and aluminum oxide both at the import and export sites. The shipping cost is normalized using the amount of aluminum fuel transported as described by eqn (9), therefore decoupling the analysis from the size of the carrier used. The parameters used are listed in Table 1 and results are shown later in Fig. 7.

$$C_{\text{ship}} = \frac{\left( \frac{CPX_V(\text{CRF} + OPX_V)}{365} + L \right) (t_s + t_h) + (F + C_{\text{canal}})t_s + C_{\text{port}}}{Q/1.9} \quad (9)$$

Regarding storage, aluminum should have minimal requirements if its size is kept over 420 microns,<sup>18,58</sup> as it is already

Table 1 Assumption used for aluminum shipping cost

Parameters	Unit	Value
Vessel CAPEX, $CPX_V$	\$m	40
Vessel lifetime, $n$	Years	25
Vessel capacity, $Q$	DWT	80 000
Vessel speed	Knots	14.5
Maintenance cost, $OPX_V$	% of CAPEX	4 <sup>57</sup>
Labor cost, $L$	\$ per day	7000 <sup>57</sup>
Fuel consumption	$t_{\text{HFO}}$ per day	40
HFO cost	\$ per $t_{\text{HFO}}$	500 <sup>57</sup>
Load/unload duration, $t_h$	Days per trip	4
Port charges, $C_{\text{port}}$	\$ per trip	100 000
Canal costs, $C_{\text{canal}}$	\$ per day on average	10 000

Table 2 Properties of the energy carriers considered in this study

Energy carrier	Specific energy (kWh kg <sup>-1</sup> )	Density (kg m <sup>-3</sup> )	Energy density (kWh L <sup>-1</sup> )
LH <sub>2</sub> (−253 °C)	33.3	70	2.3
NH <sub>3</sub> (−33 °C)	5.2	682	3.5
Diesel	11.8	850	10.0
Aluminum	8.6	2700	23.2
Al (SGA bulk density)	4.5	1000	4.5

protected by its natural oxide layer. Handling and storage of powders below that size should be done with caution due to some fire and explosion hazards. Coarse aluminum particles are however considered safe, and dry bulk storage for grain was deemed to be a reasonable comparable reservoir cost, with grain silos ranging from \$1–5 per bushel.<sup>59–61</sup> Aluminum can store 10 times more energy per unit volume than cryogenic hydrogen, and over 6 times more than liquid ammonia, as shown in Table 2. However, it is assumed that the same tanks would be used to store both the metal and the oxide powder byproduct. Doing so, the effective storage density of aluminum is significantly reduced to account for the volume of the oxides collected, which are expected to have a bulk density similar to that of SGA, *i.e.* around 1 g cm<sup>-3</sup>.<sup>26</sup>

With aluminum fuel expected to require around 2 m<sup>3</sup>/t<sub>Al</sub>, the storage cost would fall in the range of \$58–284/t<sub>Al</sub>. Operating costs of 4% of the CAPEX are assumed to account for loading and unloading procedures, maintenance, and cleaning, and the equipment is amortized over 25 years at 8% interest rate. With those assumptions, the yearly storage cost would fall in the range of \$7.6–38/t<sub>Al</sub> or \$0.9–4.4/MWh<sub>ch</sub>, therefore of the same order of magnitude as shipping costs for a 5000 km round trip.

### 4.3 Power generation costs: Al-to-Power

Once at destination, aluminum is assumed to be fed to a metal-water reactor to release heat and hydrogen, which can both be used for power generation. This reactor is expected to operate in the range of 450–600 °C and 250 bar, as supercritical water was shown to efficiently oxidize coarse aluminum particles without the need for any catalyst.<sup>17</sup> The cost of such a reactor was estimated from economic analyses conducted for supercritical water oxidation (SCWO) sewage treatment plants operating under similar conditions. Few studies provide such numbers, and results can vary significantly from one source to another,<sup>62,63</sup> which explains the large uncertainty used in this study. Additionally, to translate these results to a metal-water reactor, many assumptions are needed due to the many differences between the two technologies. The reactor, pumps and separation unit to collect the oxides are therefore estimated to account for \$140 ± \$110 per kW<sub>ch</sub>, referring to the chemical energy input of the aluminum fuel. Since operating the reactor at supercritical conditions is likely to increase corrosion issues and the use of a solid fuel might induce faster wear rate on many components the OPEX is set as 8% of CAPEX, and the lifetime is set at a maximum of 10 years.

In the current analysis, it is assumed that the stoichiometric heat-to-hydrogen ratio produced by the aluminum–water





while an air separation unit supplying nitrogen and a Haber-Bosch synthesis loop are needed for the production of  $\text{NH}_3$ . Storage is omitted at the production site, prior to shipping, assuming the same production plant would serve many customers, therefore amortizing this storage facility to a negligible value per shipment. Block diagrams illustrating the processing steps to produce, ship and store  $\text{LH}_2$  and  $\text{NH}_3$  are presented in Fig. S3 and S4 of the ESI.†

Regarding power generation, the optimal utilization of ammonia as an energy carrier remains unclear. Direct combustion is challenging because of its low flame speed and high ignition temperature, not to mention issues associated with high  $\text{NO}_x$  emissions.<sup>71</sup> To avoid this, the molecule can be cracked in part, or in full, to either produce a pure hydrogen stream or  $\text{H}_2/\text{NH}_3$  blends. Bearing some similarities with steam-methane reforming, this cracking process is endothermic and requires a high-temperature heat input, typically around 550 °C or above depending on the catalysts.<sup>67</sup> This high-temperature requirement prevents the use of waste heat in most cases. Additionally, the hydrogen conversion efficiency is highest at low pressure, therefore adding a need for compression prior to being fed to a power generation system or being stored. A purification step might also be needed, depending on the fuel requirements of the power generation equipment used.

In an effort to encompass all possible scenarios for ammonia as fuel, this study assumes two different scenarios as shown in Fig. S4 (ESI†): direct utilization, or ammonia cracking using heat from hydrogen combustion. Direct utilization is the most favorable scenario as it does not require post-processing, but prevents the use of PEMFC which typically operates on pure hydrogen.<sup>67</sup> For ammonia cracking, the heat needed is considered to be supplied by hydrogen combustion, at 100% efficiency. In that case, electricity is also needed for the compression and purification stages. It is assumed that this electricity is generated by diverting some of the hydrogen produced to a 50% efficient power generation system, simplifying the analysis by ignoring any capital or operational costs for this step. Both the heat and electricity needed decrease the overall X-to-Power efficiency for this scenario, making it the least favorable.

The various parameters used for modeling production costs of each carrier are outlined in Table 3. A wide range of values are found for most parameters, reflecting differences in technologies considered, their maturity, the anticipated cost and performance improvements according to learning rates, the effect of size and economies of scale, and the impact of inflation on costs. While accounting for all of these effects is outside the scope of this study, some lower and upper bounds were defined for most parameters to capture some of this uncertainty. Unless otherwise stated, the plant life used to amortize the capital investment is assumed to be 25 years, and the OPEX is taken to be 4% of the CAPEX.

As for  $\text{LH}_2$  and  $\text{NH}_3$  shipping, the assumptions used are consistent with the aluminum case. A similar size carrier, with a cargo volume of 160 000  $\text{m}^3$ , was assumed to be full on the outward trip, and to come back empty. Boil-off losses are

Table 3  $\text{H}_2$  carriers PtX assumptions

Parameter	Low	High
<b>Hydrogen electrolyser<sup>65,66,72,73</sup></b>		
CAPEX (\$ per $\text{kW}_e$ )	700	1500
OPEX (% of CAPEX)	1.5	4
Electricity consumption ( $\text{kWh kg}_{\text{H}_2}^{-1}$ )	50	54
<b>Hydrogen liquefaction<sup>67,74,75</sup></b>		
CAPEX (\$ per $\text{t}_{\text{H}_2}$ per year)	5100	6400
Electricity consumption ( $\text{kWh kg}_{\text{H}_2}^{-1}$ )	9	12
<b>Ammonia synthesis<sup>65–67,71,72,76</sup></b>		
CAPEX (\$ per $\text{t}_{\text{NH}_3}$ per year)	220	900
OPEX (% of CAPEX)	1.5	4
Electricity consumption ( $\text{kWh kg}_{\text{NH}_3}^{-1}$ )	0.58	1.46
Conversion efficiency	0.98	0.97
<b>Ammonia cracking<sup>66,67,77,78</sup></b>		
CAPEX (\$ per $\text{t}_{\text{NH}_3}$ per year)	310	1000
Plant life <sup>a</sup> (years)	10	—
Heat requirement ( $\text{kWh kg}_{\text{NH}_3}^{-1}$ )	1.58	1.71
Electricity requirement ( $\text{kWh kg}_{\text{NH}_3}^{-1}$ )	0.18	0.26
Conversion efficiency	1	0.9

<sup>a</sup> The ammonia cracker depreciation period should match that of the power generation and storage equipment installed at the mine site.

assumed to displace some of the fuel consumption on the outward journey, thereby reducing fuel cost, but also lowering the transportation efficiency. Details on the model and the assumptions are presented in Section S5 of the ESI.† Storing hydrogen in its liquid state requires a temperature of  $-253$  °C, which is significantly lower than for liquefied natural gas at  $-163$  °C or ammonia at  $-33$  °C, therefore making it harder to limit boil-off losses while keeping costs low. Unlike ammonia, which is already being transported on a large scale, large hydrogen carrier ships do not exist yet, which explains the wide range of values found in Table 4 and seen in Fig. 7.

## 5.2 Recharging costs: Power-to-X

Based on the analysis presented above, the costs of producing aluminum, ammonia and liquefied hydrogen are presented in Fig. 8 as a function of input electricity price. From this figure, information on fixed costs can be obtained from the y-intercepts, when electricity is free, while the slopes provide insights into the energy storage efficiency of each carrier. It can be observed that  $\text{LH}_2$  and  $\text{NH}_3$  have similar production cost, while aluminum has higher fixed cost while being the most efficient Power-to-X (PtX) option at 57.6% for the average case. It can also be seen that cracking ammonia significantly reduces its efficiency as an energy carrier.

To visualize the effect of each parameter on the PtX cost, a stacked bar chart is presented in Fig. 9. In this figure, and for the remaining analysis, the input electricity price is set

Table 4  $\text{H}_2$  carriers shipping and storage assumptions<sup>66–68</sup>

Parameter	$\text{LH}_2$	$\text{NH}_3$
Vessel CAPEX (\$ per kg)	30–90	1.5–2.0
Storage CAPEX (\$ per kg)	30–90	0.8–1.7
Boil-off rate (% per day)	0.1–0.3	0.04





Fig. 7 Shipping cost breakdown for a 5000 km trip. Both the low and high assumptions of Table 4 are considered for LH<sub>2</sub>, while an average case is used for NH<sub>3</sub>. Crosses show the total boil-off losses per trip, providing insights into the overall transportation efficiency for each pathway.



Fig. 8 PtX cost for all carriers versus electricity cost. The input parameters are set as the average value within their respective range from Table 3. The shaded area for aluminum illustrates the effect of varying the input parameters from the low to high scenario (see Fig. 4), with the number of cycles per year set at 2. Diesel commodity price in the range of \$50–100 per bbl<sup>11</sup> is shown as an indication for the energy cost.

at \$30/MWh<sub>e</sub> at the production plant, which is in the range of the industrial rate in Quebec mostly supplied by hydropower.<sup>40</sup> It shows that the heat necessary to crack the ammonia molecule is the main factor increasing the cost compared to direct ammonia utilization. The higher overall efficiency of the aluminum process is illustrated by its lower electricity cost share, compared to the hydrogen carriers. Aluminum, however, has higher fixed costs, which are mainly driven by high CAPEX.

### 5.3 Transportation and storage costs

The effect of shipping and storing the different energy carriers can be observed in Fig. 10. The results illustrate that shipping costs represent a small portion of the delivered energy cost for all options. This cost would increase with distance but should stay fairly negligible in all cases except for LH<sub>2</sub>. On the other hand, storage cost is significant for all hydrogen carriers because, assuming only two trips per year, half of the energy

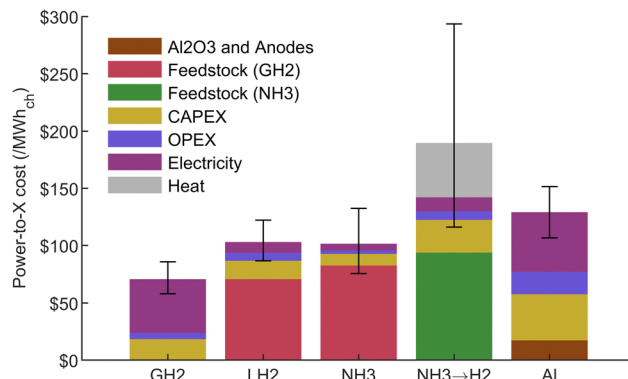


Fig. 9 PtX cost distribution for all carriers at \$30/MWh<sub>e</sub> electricity cost. Error bars reflect the uncertainty from all PtX input parameters (see Table 3). The gaseous hydrogen (GH<sub>2</sub>) stack refers to the hydrogen production cost from the electrolyser then used as a feedstock for LH<sub>2</sub> and NH<sub>3</sub>, which totals \$70.5/MWh<sub>ch</sub> or \$2.35/kgH<sub>2</sub>.



Fig. 10 Delivered energy cost at 5000 km for 2 trips a year assuming the storage equipment is amortized over the mine's operational lifespan. Error bars reflect the uncertainty from all shipping and storage input parameters (see Table 4).

consumed yearly must be stored at the remote location. This effect is significant for LH<sub>2</sub> and NH<sub>3</sub> since their storage cost is expensive compared to aluminum. This storage cost is inversely proportional to the number of trips per year and would lead to maximizing the fuel shipment frequency for LH<sub>2</sub> and NH<sub>3</sub> in order to minimize cost. It should also be noted that boil-off losses at the final location are neglected since, for the six-months long storage scenario, the amount consumed for power generation would be of 0.5% per day, which is higher than the maximum boil-off value considered in this study.

### 5.4 Power generation costs: X-to-Power

For the hydrogen carriers, the power generation system was selected as the least-cost power generation option among the different equipment considered: GT, ICE, PEMFC and SOFC. Details on the assumptions used in for CAPEX, OPEX and efficiency can be found in the ESI,<sup>†</sup> Section S6. For aluminum, a combination of a ST and a PEMFC was found to minimize the power generation cost in this specific case, as presented





**Fig. 11** Electricity generation cost for each options compared to the baseline diesel case. Excluding transportation energy, the overall round-trip efficiencies for all carbon-free pathways are 25.4%, 13.5%, 24.1% and 18.7% respectively from left to right. In the same order, the electricity cost is \$623/MWh<sub>e</sub>, \$504/MWh<sub>e</sub>, \$336/MWh<sub>e</sub>, \$453/MWh<sub>e</sub> and \$228/MWh<sub>e</sub> for diesel fuel. The thick error bands refer to the power generation equipment uncertainty on CAPEX and efficiency, while the main error bars show the effect of the total uncertainty (PtX, storage, shipping) on power generation cost. The aluminum case is compared to the diesel case to get the break-even CO<sub>2</sub> price. This price was calculated based solely on the emissions from the diesel combustion process.

in Fig. 5. The results for all scenarios are presented in Fig. 11, where they are compared with the diesel fuel case, which represents the current situation. Diesel commodity price is used as the fuel cost for comparison to the current system, since no profit margin is assumed for the clean energy carriers. This cost, including shipping and storage, is set at \$83/MWh<sub>ch</sub>, which roughly leaves a \$0.2/L margin for profits assuming a purchasing price of \$1/L.

These results show that aluminum is cost-competitive with hydrogen carriers in this application. The only cheaper scenario is the direct utilization of NH<sub>3</sub>, which benefits from the use of a high-efficiency ICE. In practice, a dual-fuel strategy might be required to reach suitable performances for ammonia combustion,<sup>79</sup> and an aftertreatment system would be needed to reduce NO<sub>x</sub> emissions. A SOFC could be used instead, but it is unclear at what efficiency. In all cases, safety measures would need to be implemented to mitigate toxicity hazards for NH<sub>3</sub>. Nevertheless, for aluminum to break-even with current diesel fuel cost, a CO<sub>2</sub> price of \$360/tCO<sub>2</sub> would be required. This is high compared to the current carbon pricing policies implemented in certain countries. To close the gap and rival with diesel in this application, aluminum's power generating cost, shown in Fig. 11, would need to fall within the lower end of its uncertainty range.

The LH<sub>2</sub> and the NH<sub>3</sub> → H<sub>2</sub> cracking scenarios both employ a PEMFC at 49.1% efficiency, while the direct NH<sub>3</sub> and the diesel scenarios use a 41.7% efficient ICE. These equipment are significantly more efficient than the 32% efficient aluminum-water power generation system, which suffers from a low-efficiency ST. This explains the higher fuel cost for aluminum seen in Fig. 11, although its delivered energy cost is similar to that of NH<sub>3</sub> (seen in Fig. 10). The main factors influencing the final electricity cost in this study are the delivered energy cost

and the power generation efficiency, which drive the fuel cost shown in Fig. 11. The power generation system is assumed to run as a baseload with a 100% capacity factor therefore spreading the CAPEX over a large number of operating hours and keeping its proportion low in the total electricity cost. Lowering the capacity factor, for example by integrating some wind turbines at the mine site, would affect the results by increasing the CAPEX share of the electricity cost.

The mass, volume and total CAPEX needed at the mine are presented for each option in Fig. S8 in the ESI.† All carbon-free scenarios require a similar storage size, approximately 3 to 4 times bigger than for diesel. The CAPEX at the mine, including the power generation equipment and storage, is significantly more important for the LH<sub>2</sub> and the NH<sub>3</sub> → H<sub>2</sub> cracking cases, totalling \$76m and \$140m respectively. Expensive storage tanks are responsible for the difference in the LH<sub>2</sub> case, while the cost of the cracker needed to release hydrogen from NH<sub>3</sub> makes up the majority of the initial investment for this scenario. Direct NH<sub>3</sub> utilization, the aluminum, and the diesel cases all have similar total CAPEX in the range of \$38–\$50m.

## 6 Conclusions

This study presents a comprehensive techno-economic assessment of aluminum as a sustainable energy carrier. The aluminum fuel recharging cost analysis relied on publicly available data compiled from investors' presentations of aluminum producers, complemented by insights from the modern aluminum smelting process. Since the smelting process must be decarbonized to enable a sustainable use of aluminum fuel, the potential impact of inert anode technology was also reviewed to project its effects on costs. Transportation, storage and power generation costs were also evaluated to assess the entire energy cycle. Similar cost estimates were conducted for LH<sub>2</sub> and NH<sub>3</sub> in an effort to compare aluminum to other alternative often discussed as potential energy carriers. A case study was finally used to contextualize this comparison in the context of a remote mine requiring a continuous power supply of 25 MW<sub>e</sub>.

Results indicate that aluminum has the potential to be cost competitive with diesel fuel on a chemical energy basis. To do so, aluminum must benefit from low electricity prices while a carbon pricing system needs to be implemented to account for the cost of emissions. Aluminum could also reach similar costs as both LH<sub>2</sub> and NH<sub>3</sub> if inert smelting can help to reduce fixed costs, as PtX efficiencies are similar for all three pathways. The remote mine case study, integrating the costs of the entire cycle, demonstrates that aluminum can provide electricity at a cost comparable to these more widely discussed hydrogen carriers. Direct use of ammonia is shown to be marginally cheaper, but would require mitigating the high NO<sub>x</sub> emissions from combustion, and dealing with the corrosion and toxicity hazards. This positions aluminum as a promising and viable option for consideration in various other applications.

This study also shows that limited access to a location, which increases the storage size requirement, is particularly



detrimental to  $\text{LH}_2$  and  $\text{NH}_3$  which need specialized storage tanks. Shipping costs are generally not a significant cost driver. The prohibitive storage cost of  $\text{LH}_2$ , and the necessity for a cracking unit for  $\text{NH}_3$ , incurring significant cost and complexity, are the main factors making these options more expensive.

The 25  $\text{MW}_e$  aluminum power generation system, despite being comparable to the diesel case in terms of total installed CAPEX at the mine, is facing a drawback due to its lower efficiency, estimated to be approximately 10 percentage points lower than that of other scenarios. Higher efficiencies could be achieved in applications in need of more power which could benefit from a higher steam turbine efficiency, or the use of a combined cycle to recuperate some waste heat. The development of a reactor capable of converting aluminum to hydrogen while efficiently converting heat to power is essential for the viability of this metal-fuel cycle.

Finally, the commercialization of inert anode smelting is key to make the aluminum fuel viable and should help gain more certainty on the recharging cost in the coming years. Future studies should focus on evaluating the potential of the aluminum fuel cycle for seasonal energy storage and its ability to facilitate global trade of clean energy. This should help in assessing the economic viability of integrating smelters as energy storage facilities and metal-water power generation in renewable-heavy electricity grids.

## Author contributions

P. Boudreau: conceptualization, methodology, formal analysis, investigation, visualization, writing – original draft, writing – review & editing. M. Johnson: conceptualization, methodology, writing – review & editing. J. M. Bergthorson: conceptualization, methodology, resources, writing – review & editing, supervision, funding acquisition.

## Conflicts of interest

There are no conflicts to declare.

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