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$\text{Pr}_2\text{BaNiMnO}_{7-\delta}$ double-layered Ruddlesden-Popper perovskite oxides as efficient cathode electrocatalysts for low temperature proton conducting solid oxide fuel cells

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Pr₂BaNiMnO_{7-δ} double-layered Ruddlesden–Popper perovskite oxides as efficient cathode electrocatalysts for low temperature proton conducting solid oxide fuel cells†

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The performance of low-temperature solid-oxide fuel cells (LT-SOFCs) is heavily dependent on the electrocatalytic activity of the cathode toward the oxygen reduction reaction (ORR). To overcome the obstacles of the poor activity and stability of traditional cathode materials, a Pr₂BaNiMnO_{7-δ} double-layered Ruddlesden–Popper structural oxide was developed that exhibits high ORR activity, exceptional low-temperature cell performance, long-term stability, and excellent chemical compatibility with a BaZr_{0.1}Ce_{0.7}Y_{0.1}Yb_{0.1}O_{3-δ} (BZCYYb) proton-conducting electrolyte. When Pr₂BaNiMnO_{7-δ} is used as the cathode electrocatalyst for BZCYYb-based SOFCs, it demonstrates a peak power density of 1070 mW cm⁻² at 700 °C with excellent stability under 0.7 V after 100 h of discharging. Even at 500 and 400 °C, the peak power densities still reach 259 and 135 mW cm⁻², respectively. The area-specific polarization resistance of this cell is 0.084 Ω cm² at 700 °C under open-circuit voltage (OCV) conditions. Interestingly, the activation energy (*E*_a) of the polarization resistance derived from the assembled single cell is lower than that in the reported literature, corresponding to a value of 0.96 eV. The excellent performance is higher than those of the state-of-the-art Ruddlesden–Popper structure materials used as cathode electrocatalysts for LT-SOFCs. Thus, these results suggest that the double-layered Ruddlesden–Popper perovskite oxide Pr₂BaNiMnO_{7-δ} is a preeminent highly active low-temperature cathode material.

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1. Introduction

Solid-oxide fuel cells (SOFCs) can directly convert the chemical energy of fuels into electricity, and have attracted special attention for their high fuel conversion efficiency, low environmental impact, and excellent fuel flexibility.^{1–6} To overcome the construction and durability limitations of the stacking system that accompanies the high operating temperatures (800–1000 °C) of conventional SOFCs, lowering the operating temperature to a low temperature (LT, below 600 °C) is the inevitable choice of research direction for an SOFC development regime.^{6–8} However, the oxygen reduction reaction (ORR) at the cathode is thermally activated and the exponentially increased cathode polarization resistances directly lead to

drastically decreased performances of the SOFCs. In this case, cathode resistance is a serious drawback for operation at low temperature. Therefore, cathode materials showing high performance at low temperature are required for the development of LT-SOFCs. And thus a good cathode should possess enough electrical conductivity (above 100 S cm⁻¹), excellent electrocatalytic activity, good chemical compatibility, a thermal expansion coefficient (TEC) compatible with the electrolyte and excellent stability.^{9–12}

To achieve a feasible, alternative cathode, research efforts have concentrated on developing a novel cathode material with good properties. Traditional cathode materials, such as La_{0.6}Sr_{0.4}MnO₃ (LSM), show a relatively high area specific resistance (ASR) compared to the available anode materials.¹³ A layered LnBaCo₂O_{5+δ} perovskite oxide cathode suffers from various stability issues during long-term operation, including A-site segregation, CO₂ poisoning to form carbonates and unmatched TEC compared to those of typical electrolytes.^{14,15} As an alternative cathode material system, Ruddlesden–Popper (R–P) perovskite oxides with layered structures have attracted attention, in consideration of their extremely high oxygen ion conductivities and electronic conductivity inside the rock salt layer.^{11,16} R–P series materials have promising ORR applications

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for high-temperature SOFC electrodes. As reported in the literature, one layered R–P oxides have been studied extensively, such as La_2NiO_4 and Pr_2NiO_4 ,^{17–26} and Pr_2NiO_4 has better ORR activity than La_2NiO_4 or Nd_2NiO_4 .^{27,28} In addition, according to the calculated and experimental results, the double-layered R–P phase structure $\text{La}_3\text{Ni}_2\text{O}_7$ exhibits better oxygen ion and proton transport behaviour than single-layered La_2NiO_4 .²⁹ In the double-layered $\text{Ln}_3\text{Ni}_2\text{O}_7$, the transition dopant metals (Mn, Fe, Co and Cu) are favourable for enhancing oxygen diffusion and proton diffusivity to some extent at the same time. Oxygen ion conduction is found to be closely related to the microelectronic structure and charge density gradients generated from the chemical bonding between O and the B-site atoms along the oxygen migration pathway. While, for proton diffusion, the dopants can weaken the proton association and enlarge the capacity of the ‘electron pocket’ around the Fermi level, which is beneficial to fast proton diffusivity in the R–P phase structure.²⁹ Intuitively, the typological transfer mode for the R–P cathode is shown in Fig. 1, in which the proton electrolyte SOFC cathode allows simultaneous oxygen ion, electron and proton transportation. The ORR routes are similar to those reported in the literature,³⁰ and a recent report³¹ demonstrated that oxygen vacancy is not the key point for R–P oxides to realize high ORR activity at high temperature. Instead, a high concentration and fast migration of the interstitial oxygen (O_i'') and lattice oxygen with high activity are favourable for high-temperature catalytic activity. High-valence ion doping can enhance the O_i'' concentration and the lattice oxygen activity.

Inspired by previous research on the R–P phase cathode, in this study we have developed a novel double-layered R–P structure $\text{Pr}_2\text{BaNiMnO}_{7-\delta}$ cathode material. Normally, the structural stability of ABO_3 perovskite is related to the ionic radii of the A- and B-sites and the stability is usually evaluated by the Goldschmidt tolerance factor ‘ t ’ (eqn (1)).^{32–34} Consideration is given to the ionic radii of Ba^{2+} (12-coordination with oxygen, 1.61 Å) and $\text{Pr}^{3+}/\text{Pr}^{4+}$ (8-coordination, 1.126/0.96 Å) compared with Ni^{3+} (6-coordination with oxygen, high spin, 0.6 Å) and Ni^{2+} (6-coordination with oxygen, 0.69 Å). If the A-site is $\text{Pr}^{3+}/\text{Pr}^{4+}$, the ‘ t ’ value is about 0.80–0.86, which is lower than 1. If the A-site is changed to Ba^{2+} , the ‘ t ’ value is very close to 1 and Ba^{2+} can easily form a 12-coordination structure with oxygen. In this case, the stability of the perovskite structure layer is significantly improved when the $\text{Pr}^{3+}/\text{Pr}^{4+}$ are partially replaced

with Ba^{2+} . In the B-site, the ionic radii and valence state of doped $\text{Mn}^{3+}/\text{Mn}^{4+}$ (6-coordination, 0.645/0.53 Å) is lower than that of $\text{Ni}^{2+}/\text{Ni}^{3+}$. The Mn substitution in the B-site lattice in the perovskite structure layer could cause some distortion to the BO_6 octahedra. Further, the changed microelectronic structures of perovskite may improve the oxygen ion conduction.²⁹ Hence, in the selected $\text{Pr}_3\text{Ni}_2\text{O}_7$ system, the barium element is doped into the A-site for considerations of structural stability, and the aliovalent Mn ($\text{Mn}^{3+}/\text{Mn}^{4+}$) cation doping in the B-site is an effective strategy for modifying the catalytic activity. $\text{Pr}_2\text{-BaNiMnO}_{7-\delta}$ (PrBaNiMn) was synthesized *via* a facile citric acid–nitrate combustion process. The physicochemical and electrical properties of the powders and the anode-supporting single-cell $\text{NiO-BZCYYb/AFL/BZCYYb/PrBaNiMn}$ were also investigated using corresponding techniques. Finally, the electrochemical performance in terms of the power output and the polarization impedance of the SOFC with the PrNaNiMn cathode was evaluated to demonstrate the feasibility of the materials as promising ORR catalysts for LT-SOFCs.

$$t = \frac{r_A + r_O}{\sqrt{2}(r_B + r_O)} \quad (1)$$

2. Experimental

2.1. Material synthesis

BZCYYb and PrBaNiMn powders were synthesized *via* a citric acid–nitrate gel combustion method.³⁵ For PrBaNiMn powder, Pr_6O_{11} , $\text{Ba}(\text{NO}_3)_2$, $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ and $\text{Mn}(\text{NO}_3)_2$ at a stoichiometric ratio of 2 : 1 : 1 : 1 were dissolved and well mixed, with citric acid as the chelating agent $n(\text{citric acid})/n(\text{metals}) = 1.5$ in the raw material solution. Then, the solution was heated to evaporate under continuous stirring until it changed into a sol-gel and finally ignited into a flame. The electrolyte powder BZCYYb was synthesized using BaCO_3 , $\text{Zr}(\text{NO}_3)_4 \cdot 5\text{H}_2\text{O}$, $\text{Ce}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$, $\text{Y}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$, and $\text{Yb}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$. After combustion, the two as-prepared ash-like precursors were calcined at 1250 and 1000 °C for 5 h in air to obtain PrBaNiMn and BZCYYb powders, respectively.

2.2. Fabrication of anode-supported single cells

The anode substrate composite powder NiO-BZCYYb (65 : 35 weight ratio) was also prepared by the one-step gel combustion process and calcined at 1000 °C for 5 h. The 80 wt% composite powder NiO-BZCYYb and pore-forming material (20 wt% starch) were well mixed to prepare a porous anode powder. The anode supported half cells ($\text{NiO-BZCYYb/AFL/BZCYYb}$) with a tri-layered structure were fabricated by a co-pressing method³⁶ and then co-sintered at 1350 °C for 5 h at a 3 °C min^{-1} heating rate. The cathode paste was obtained by mixing the PrBaNiMn powder and a 10 wt% ethylcellulose–terpineol binder to get PrBaNiMn ink. Then, the ink was painted onto a dense BZCYYb electrolyte membrane surface with a 0.28 cm^2 effective area and about 20 μm thickness, and sintered at 1100 °C for 3 h in air to get a porous cathode layer. Ag paste and wire were applied as a current collector and the conducting wire, respectively. Then,



Fig. 1 Schematic diagram of R–P cathode with different transportation routes (including e^- , O^{2-} , H^+).

the button anode supported single cells were installed on an alumina supporting tube for further measurements. A scheme of the fabrication process for anode-supported single cells is shown in Fig. S1.†

2.3. Characterization and electrochemical measurements

X-ray diffraction (XRD) analysis was performed to investigate the crystalline structure of the electrode and electrolyte powders using a SmartLab diffractometer with Cu K α radiation. For the PrBaNiMn structural refinement, the test angular range was 10 to 135 degrees, and the step size and counting times were varied to ensure the required data quality and resolution. Diffraction data was analyzed using professional software and the peak shape was described by a pseudo-Voigt function, and the background level was inserted with linear interpolation. The chemical stability of PrBaNiMn and BZCYYb was investigated using a PrBaNiMn/BZCYYb mixture at a weight ratio 1 : 1 calcined at 1000 °C for 5 h. Then, the mixture was studied to characterize the crystalline structure *via* XRD.

The valence states and the composition of the elements on the PrBaNiMn surface were investigated using an X-ray photon spectroscopy (XPS, Thermo ESCALAB 250) method. The thermal expansion coefficient (TEC) of the PrBaNiMn sample was measured using a thermal expansion instrument (DIL402C). For this measurement, 2 g of PrBaNiMn powder were dry-pressed into a rectangular bar of dimensions 2.50 × 0.45 × 0.30 cm (length × width × height) after sintering at 1450 °C for 10 h in air. The performance of the button single fuel cells installed on an alumina supporting tube was measured at 400–700 °C with wet hydrogen (~3% H₂O) as fuel and stationary air as oxidant. The linear sweep voltammetry (LSV) and electrochemical impedance spectroscopy (EIS) characteristics of the

cells were measured using an electrochemistry workstation (Solartron 1287 and 1260). The EIS measurements were carried out under open circuit conditions at 5 mV with AC amplitude 0.1–100 kHz. The cell ohmic and polarization resistances were clearly obtained from the EIS under open circuit conditions. The morphology, microstructure, and mapping of the tested single cell were examined using a scanning electron microscope (SEM, Hitachi, SU-70). The HRTEM and lattice fringes of the cathode material PrBaNiMn were measured by JEM-F200 at 200 kV accelerating voltage.

3. Results and discussion

3.1. Structural analysis

Fig. 2a shows the Rietveld refinement of the XRD pattern of the PrBaNiMn powder carried out using the FullProf program. It shows a tetragonal phase structure with *I4/mmm* symmetry, $a = b = 3.8746(1)$ Å and $c = 20.3245(3)$ Å. The reliability factors of the refinement are $R_{wp} = 8.70$, $R_{exp} = 6.02$ and $\chi^2 = 5.95$. The tetragonal phase structural obtained based on a Ruddlesden-Popper-type A₃B₂O₇ model is in good agreement with the values of La_{1.4}Sr_{1.6}Mn₂O₇ on the JCPDS card (PDF#01-089-9022).³⁷ Fig. 2b shows the crystal structure of PrBaNiMn according to the Rietveld analysis result, which consists of alternating rock-salt (A₂O₂) layers and perovskite-like (BO₆) layers along the *c*-axis. The Ni/Mn atoms located in the octahedron centers with corner-shared BO₆ build the perovskite-like layers and are then connected with two A₂O₂ layers. The rock-salt A₂O₂ layers have abundant transporting pathways for interstitial oxygen (O_i') along the (*a*–*b*) plane. And the perovskite-like sheets have rich oxygen vacancies and excellent electrical conductivity which are beneficial for the ORR and electron transportation. In this case,



Fig. 2 (a) Rietveld refinement plot of PrBaNiMn powder using X-ray powder diffraction data, R_{wp} and χ^2 represent the weighted profile factor and reduced chi-square; (b) the crystal structure of Pr₂BaNiMnO_{7.8}; (c) XRD patterns of PrBaNiMn, BZCYYb fired at 1250, 1000 °C and the dry-mixed composite powder BZCYYb–PrBaNiMn (5 : 5) fired at 1000 °C for 5 h, respectively.

the obtained powder PrBaNiMn should be a good cathode material for SOFCs. In addition, the XRD patterns of the powder mixture of PrBaNiMn and BZCYYb (50 : 50 wt%) after annealing at 1000 °C for 5 h (Fig. 2c), with no detectable impurity peaks, suggests good chemical compatibility between the cathode and the electrolyte phases.

Fig. 3a displays a TEM image of PrBaNiMn powder with an average particle size of ~ 300 nm. Corresponding energy dispersive X-ray spectroscopy (EDS) mapping images of PrBaNiMn for Pr, Ba, Ni, Mn and O elements exhibit a homogeneous distribution, and no observable elemental segregation could be detected (Fig. S2†). All this evidence suggests that PrBaNiMn double-layered R-P perovskite oxides have been successfully prepared without a secondary phase or elemental segregation, which is essential for the R-P structural cathodes to take part in an ORR in the fuel cell operating process. In addition, from the high-resolution TEM image (Fig. 3b and c) of the powder, the interplanar crystal spacing is calculated to be 3.804 Å, which corresponds to the (101) plane for the R-P structure (space group $I4/mmm$). The SEM image of the powder indicates the porous structure and good dispersibility of the prepared PrBaNiMn, which is beneficial for oxygen adsorption and transportation (Fig. 3d).

The elemental compositions and valence states of PrBaNiMn were investigated by XPS. Table 1 shows the elemental compositions (Pr, Ba, Ni, Mn, O), valence states and content of the elements with multiple valence states (Pr, Ni, Mn) which are calculated from the peak fitting by XPSPEAK4.1 software. The elemental compositions are close to the stoichiometric ratio of the designed material. In A-sites, the Pr 3d spectrum of PrBaNiMn (Fig. 4a) comprises four intense peaks at 928.5 (Pr³⁺ 3d_{5/2}), 948.4 (Pr³⁺ 3d_{3/2}), 932.8 (Pr⁴⁺ 3d_{5/2}) and 952.8 (Pr⁴⁺ 3d_{3/2}), respectively, with a splitting energy of about 20 eV between 3d_{5/2} and 3d_{3/2} core-levels, in agreement with the reported literature.³⁸ The spectrum of the satellite located at 956.5 eV corresponds to Pr₆O₁₁ (Fig. 4a) which is associated with the multiple valence

Table 1 Surface elemental percentage composition and relevant parameters of the prepared PrBaNiMn measured by XPS

The sample PrBaNiMn surface elemental composition (at%)								
Pr 3d		Ba 3d		Ni 2p		Mn 2p		O 1s
14.42		7.10		5.44		6.22		66.82
Pr ³⁺	Pr ⁴⁺	Ni ²⁺	Ni ³⁺	Mn ³⁺	Mn ⁴⁺	O _{latt}	O _{ads}	H ₂ O
30.59	69.41	30.09	69.91	81.12	18.88	44.11	48.55	7.34

effect of the Pr and oxygen O KLL Auger peak at 971.5 eV.^{38–40} The tetravalent Pr atoms are the charge compensation for the Ba atoms with bivalence. For the B-site atoms Ni and Mn, both have two oxidation states: these are 854.2 eV (Ni²⁺ 2p_{3/2}) and 855.5 eV (Ni³⁺ 2p_{3/2}) for Ni atoms (Fig. 4b), and 642.1 eV (Mn³⁺ 2p_{3/2}), 653.8 eV (Mn³⁺ 2p_{1/2}), 645.6 eV (Mn⁴⁺ 2p_{3/2}) and 658.2 eV (Mn⁴⁺ 2p_{1/2}) for Mn atoms (Fig. 4c).^{41,42} The discrepancy between the Ni²⁺/Ni³⁺ and Mn³⁺/Mn⁴⁺ atomic ratios at the B-sites in the surface of the sample reflect the charge and structural adjustments. Under these conditions, the percentage of O_{ads} (adsorbed oxygen) at 531.2 eV is higher than the O_{latt} (lattice oxygen) at 529.0 eV, which is beneficial for oxygen ion transportation and ORR at the surface of the samples (Fig. 4d). What is more, the rich O_{ads} can increase the proton (H⁺/OH⁻) conduction, which can enhance the cathode activity.²⁹ The 7.34% oxygen species at 532.8 eV for O 1s indicates the porous surface in the contaminants (hydroxyl/carbonyl groups).⁴³ The Ba 3d_{5/2} peaks show that two chemical states are present (Fig. S3†). The lower binding energy (BE) peak at 778.2 eV can be related to PrBaNiMn while the higher BE peak at 779.8 eV is typical of BaCO₃ as a result of the adsorption of CO₂ by the sample in an ambient environment.⁴⁴

Along the *ab*-plane in the R-P structure, the rock-salt A₂O₂ layers leave favorable transportation pathways for O_i' and the

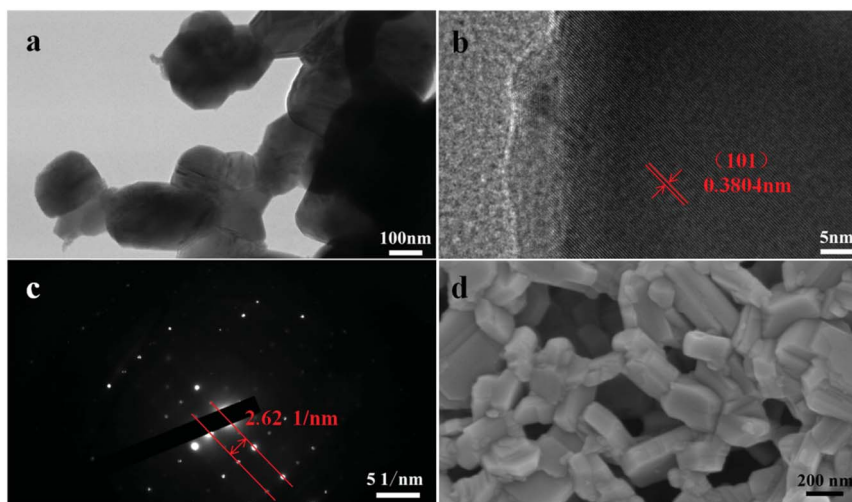


Fig. 3 (a) Bright-field TEM of PrBaNiMn powder; (b) the high-resolution TEM (HRTEM) images of PrBaNiMn at the (101) lattice plane; (c) the FFT of the (101) lattice plane; (d) the SEM image of PrBaNiMn.

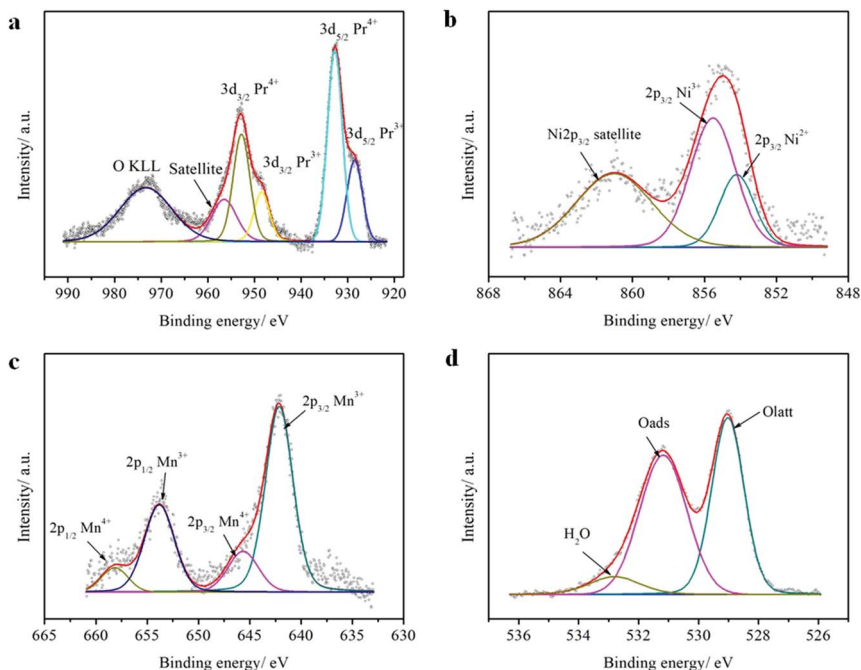


Fig. 4 (a) Pr 3d; (b) Ni 2p; (c) Mn 2p and (d) O 1s core level XPS spectra of PrBaNiMn powder.

electron transportation occurs predominantly along the perovskite-like layers. Because of the variable oxidation state in both the A- and B-site cations of the R-P structure, the O^{2-} can transport *via* the 3D channels in the perovskite-like layers by the hopping mechanism and in the rock-salt layers by the O_i' migration mechanism. The formation of oxygen vacancies (V_O^\times) can be expressed by eqn (2)–(4). Although the perovskite-like layers do not allow for the existence of interstices, the O^{2-} ions can diffuse *via* the BO_6 octahedra with a corner-shared structure between perovskite-like layers and the rock-salt layers (shown in Fig. 2b). As mentioned above, the obtained PrBaNiMn should be a good cathode material in SOFC with nice ORR activity.



These three redox couples accelerate the ORR reaction, which could be described in Kröger-Vink notation as follows:^{45,46}



It is generally accepted that the ORR at the cathode of H-SOFC could be described with the most plausible rate-limiting steps 1–4, as follows:

Step 1: $O_2 \rightarrow 2O_{ad}$ (dissociative adsorption).

Step 2: $O_{ad} + e^- \rightarrow O_{ad}^-$ (charge transfer).

Step 3: $O_{ad}^- \rightarrow O_{TPB}^-$ (surface diffusion, TPB, three-phase boundary).

Step 4: $O_{TPB}^- + e^- \rightarrow O_{TPB}^{2-}$ (charge transfer at TPB).

The adsorbed O_{ad} , O_{ad}^- and O_{ad}^{2-} could be incorporated into the PrBaNiMn phase, combining with the oxygen vacancies directly in the double-layered R-P structure cathode PrBaNiMn, which could be written as steps 5–7.

Step 5: $O_{ad} + 2e^- + V_{O,PrBaNiMn}^{\bullet\bullet} \rightarrow O_{O,PrBaNiMn}^\times$

Step 6: $O_{ad}^- + e^- + V_{O,PrBaNiMn}^{\bullet\bullet} \rightarrow O_{O,PrBaNiMn}^\times$

Step 7: $O_{ad}^{2-} + V_{O,PrBaNiMn}^{\bullet\bullet} \rightarrow O_{O,PrBaNiMn}^\times$

Furthermore, the O_{TPB}^{2-} at the TPB of PrBaNiMn-BZCYYb-gas could be injected into the PrBaNiMn phase (step 8) and react with H_{TPB}^+ conducted from the electrolyte (steps 9–12).

Step 8: $O_{TPB}^{2-} + V_{O,PrBaNiMn}^{\bullet\bullet} \rightarrow O_{O,PrBaNiMn}^\times$

Step 9: $H_{electrolyte}^+ \rightarrow H_{TPB}^+$

Step 10: $O_{TPB}^{2-} + H_{TPB}^+ \rightarrow OH_{TPB}^-$

Step 11: $OH_{TPB}^- + H_{TPB}^+ \rightarrow H_2O_{TPB}$

Step 12: $H_2O_{TPB} \rightarrow H_2O(g)$

3.2. Microstructures of the fuel cell

As shown in Fig. 5, the cross sectional images of the single cell have four apparent layers (PrBaNiMn cathode, BZCYYb electrolyte, AFL and anode support) and no layers show any sign of delamination or cracking after a long-term test for 100 hours, suggesting that the four-layered cell structure is able to retain chemical and thermal stability with no thermal mismatch occurring during the thermal cycles. The cathode PrBaNiMn undergoes no reaction with the electrolyte BZCYYb after long-term operation according to the EDS mapping shown in Fig. S4,[†] which further verifies the chemical compatibility of the



Fig. 5 Cross-sectional SEM images of the single cell. (a) The four-layer single cell with an anode functional layer (AFL) and PrBaNiMn cathode after testing; (b) PrBaNiMn cathode layer; (c) the cathode/BZCYYb; (d) BZCYYb electrolyte; (e) AFL/BZCYYb; (f) the porous anode NiO-BZCYYb and anode functional layer (AFL). AFL provides abundant triple-phase boundaries (TPBs) with the electrolyte allowing fast dissociation of the fuel gas and the rapid occurrence of charge transfer after the reduction of NiO (Fig. 5e). The larger pores in the anode support obtained from the pore-forming materials offer rapid diffusion of fuel gas to the AFL layer and then to the TPBs (Fig. 5f). The pore size distribution of the anode support plates is measured by the mercury porosimeter method described in the ESI.†⁴⁷ As shown in Fig. S5 and S6,† the cumulative intrusion of mercury has three stages as the pressure increases and the corresponding pore size distributions are about 100–200 μm , 1–0.4 μm and 50–250 nm. The rational distributions of pore sizes for the anode support accelerate the fuel gas diffusion, transmission and reaction. On the basis of the superior single-cell components and microstructures, intensive electrochemical performance in an intermediate temperature range should be achieved when a PrBaNiMn cathode is applied to BZCYYb-based solid-oxide fuel cells.

cathode material with the electrolyte after the XRD results in Fig. 1c. The thicknesses of the electrolyte and AFL are around 12 and 15 μm (Fig. 5a), respectively. Under SOFC working conditions, the dense BZCYYb electrolyte can prevent gas leakage, allow the efficient transportation of protons and retain a stable open-circuit voltage (Fig. 5d). Moreover, the uniform nano particles (~ 300 nm) with a continuous porous structure of the PrBaNiMn cathode accelerate gas diffusion and electrochemical reactions (Fig. 5b and c). Apart from the cathode, the firm adhered anode.

3.3. Electrochemical performance of the single cells

The button single-cell NiO-BZCYYb/AFL/BZCYYb/PrBaNiMn was assembled and then measured under conventional conditions (3% H_2O hydrogen as the fuel gas and static air as the oxidant) to assess the cathode performance of H-SOFC at 400–700 $^\circ\text{C}$. Fig. 6a and b show the typical V-I and P-I curves of the single cell obtained at 400–700 $^\circ\text{C}$. The open circuit voltage

(OCV) of the cell using the PrBaNiMn cathode were found to be 1.091, 1.079, 1.068, 1.059, 1.047, 1.017 and 1.002 V at 400, 450, 500, 550, 600, 650 and 700 $^\circ\text{C}$, respectively. And the corresponding peak power densities (PPDs) were 135, 201, 259, 407, 570, 776 and 1070 mW cm^{-2} from 400 to 700 $^\circ\text{C}$ with 50 $^\circ\text{C}$ intervals (Table S1†). The close-to-theoretical OCV values indicated that the BZCYYb electrolyte layer is dense enough to prevent gas leakage with no leakage current. Meanwhile, the single cell with a PrBaNiMn cathode shows the highest PPD among the R-P structured single-phase cathode materials reported in the literature under similar testing conditions, as shown in Table 2. Fig. 6c shows the typical electrochemical impedance spectra (EIS) plots of the single cell with a PrBaNiMn cathode at 400–700 $^\circ\text{C}$. The high-frequency intercept and low-frequency intercept correspond to the ohmic resistance (R_0) and the total resistance (R_T) of the cell, respectively. The low-frequency intercepts for 400 $^\circ\text{C}$ and 450 $^\circ\text{C}$ EIS are obtained from the simulated plots (Fig. S7†) according to the equivalent circuits using the model $LR(R_H Q_H)(R_M Q_M)(R_L Q_L)$ presented as an inset in Fig. 6d. In the equivalent circuit curves, the ohmic contribution and the inductive process are considered by the

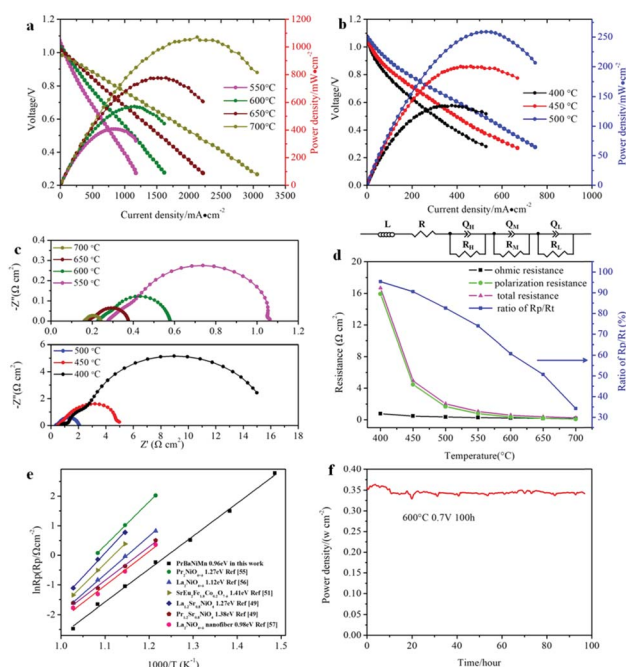


Fig. 6 Typical V-I and P-I curves of a NiO-BZCYYb/AFL/BZCYYb/PrBaNiMn single cell obtained at (a) 500–700 $^\circ\text{C}$ and (b) 400–450 $^\circ\text{C}$; (c) EIS of the NiO-BZCYYb/AFL/BZCYYb/PrBaNiMn single cell measured under open-circuit conditions from 400 to 700 $^\circ\text{C}$; (d) the temperature dependence of the ohmic resistance (R_0), polarization resistance (R_p) and total resistance (R_T), as well as the ratios R_p/R_T of the single cell with a PrBaNiMn cathode, with the equivalent circuits $LR(R_H Q_H)(R_M Q_M)(R_L Q_L)$ in the inset image; (e) the Arrhenius plots for R_p of the PrBaNiMn cathode estimated from the EIS in this study and the R-P phase cathodes reported in the literature under similar fuel gas testing conditions; (f) the long-term stability of the single-cell NiO-BZCYYb/AFL/BZCYYb/PrBaNiMn under a cell voltage of 0.7 V at 600 $^\circ\text{C}$ with hydrogen (3% H_2O) as the fuel.

Table 2 Comparison of the PPD (mW cm^{-2}) performance of single-phase cathodes below $700\text{ }^\circ\text{C}$ based on BaCeO_3 -based cells under similar fuel gas testing conditions reported in the literature and in the present study

Year	Cathode	Electrolyte (thickness, μm)	700	650	600	550	500	450	400	Ref.
2009	$\text{Pr}_2\text{NiO}_{4+\delta}$	$\text{BaCe}_{0.9}\text{Y}_{0.1}\text{O}_{3-\delta}$ (40)		132	96	53				55
2014	$\text{La}_2\text{NiO}_{4+\delta}$	$\text{BaZr}_{0.1}\text{Ce}_{0.7}\text{Y}_{0.2}\text{O}_{3-\delta}$ (20)	398	283	196	120				56
2017	$\text{La}_3\text{Ni}_{1.6}\text{Co}_{0.4}\text{O}_{7-\delta}$	$\text{BaZr}_{0.3}\text{Ce}_{0.5}\text{Y}_{0.2}\text{O}_{3-\delta}$ (20)	398	293	215					50
2018	$\text{SrEu}_2\text{Fe}_{1.8}\text{Co}_{0.2}\text{O}_{7-\delta}$	$\text{BaZr}_{0.1}\text{Ce}_{0.7}\text{Y}_{0.2}\text{O}_{3-\delta}$ (15)	562	365	210					51
2018	$\text{La}_{1.2}\text{Sr}_{0.8}\text{NiO}_4$	$\text{BaZr}_{0.1}\text{Ce}_{0.7}\text{Y}_{0.2}\text{O}_{3-\delta}$ (30)	461	330	223					49
2018	$\text{Pr}_{1.2}\text{Sr}_{0.8}\text{NiO}_4$	$\text{BaZr}_{0.1}\text{Ce}_{0.7}\text{Y}_{0.2}\text{O}_{3-\delta}$ (30)	352	212	127					49
2019	$\text{La}_2\text{NiO}_{4+\delta}$ nanofiber	$\text{BaZr}_{0.1}\text{Ce}_{0.7}\text{Y}_{0.2}\text{O}_{3-\delta}$ (15)	508	349	246	175				57
2019	$\text{La}_{1.2}\text{Sr}_{0.8}\text{Ni}_{0.6}\text{Fe}_{0.4}\text{O}_{4+\delta}$	$\text{BaZr}_{0.1}\text{Ce}_{0.7}\text{Y}_{0.2}\text{O}_{3-\delta}$ (15)	782	658	421	257	139			58
This work	PrBaNiMn	$\text{BaZr}_{0.1}\text{Ce}_{0.7}\text{Y}_{0.1}\text{Yb}_{0.1}\text{O}_{3-\delta}$ (12)	1070	776	570	407	259	245	135	

introduction of a resistance (R) and an inductance (L) in series with three RQ elements corresponding to the electrode processes involved (R and Q are the resistance and the constant phase element, respectively). And the difference between the two intercepts represents the interfacial polarization resistance (R_p). All resistances containing R_o , R_p , R_T and the ratios of R_p/R_T are shown in Fig. 6d and Table S1.† It is clear from the relationship between impedance and temperature that the electrochemical reaction processes are thermally activated. The R_p of the PrBaNiMn cathode cell decreases from 15.915 to $0.084\ \Omega\ \text{cm}^2$ along with the R_o alone from 0.759 to $0.162\ \Omega\ \text{cm}^2$ at temperatures from $400\text{ }^\circ\text{C}$ to $700\text{ }^\circ\text{C}$. The R_p values are 0.084 , 0.191 , 0.350 , 0.785 , 1.675 , 4.473 and $15.915\ \Omega\ \text{cm}^2$ and the corresponding R_o values are 0.162 , 0.185 , 0.227 , 0.275 , 0.354 , 0.468 and $0.759\ \Omega\ \text{cm}^2$ at 700 , 650 , 600 , 550 , 500 , 450 and $400\text{ }^\circ\text{C}$, respectively. In addition, the ratios of R_p/R_T are 34.24% , 50.72% , 60.69% , 74.03% , 82.57% , 90.54% and 95.45% when the temperature decreases from 700 to $400\text{ }^\circ\text{C}$. And R_p obviously plays a predominant role in determining the total resistance and the performance of the single cell, especially at low temperatures, which is also similar to the reported literature.⁴⁸ Therefore, under these circumstances, more attention should be paid to an exploration of electrode materials with lower R_p and high activity at low temperatures.

In detail, the activation energy E_a of the assembled single cell in this work was calculated with the Arrhenius equation and compared with various R–P single-phase cathodes for BaCeO_3 -based proton electrolytes under the same conditions (hydrogen with about 3% H_2O as fuel gas).

As shown in Fig. 6e, the E_a of the R_p of the PrBaNiMn cathode is lower than that in the reported literature, corresponding to the value of $0.96\ \text{eV}$, being comparable with the single-phase cathode with a one-layer R–P structure $\text{La}_{1.2}\text{Sr}_{0.8}\text{NiO}_{4+\delta}$ and $\text{Pr}_{1.2}\text{Sr}_{0.8}\text{NiO}_{4+\delta}$ with E_a values of 1.27 and $1.38\ \text{eV}$, respectively.⁴⁹ In addition, the PrBaNiMn cathode also has a relatively lower E_a than double-layered R–P structure cathode materials, such as $\text{La}_3\text{Ni}_{1.6}\text{Co}_{0.4}\text{O}_{7-\delta}$ or $\text{SrEu}_2\text{Fe}_{1.8}\text{Co}_{0.2}\text{O}_{7-\delta}$.^{50,51} Although the $\text{La}_2\text{NiO}_{4+\delta}$ nano-fiber presents relatively lower E_a at $0.98\ \text{eV}$, which is also little higher than the PrBaNiMn cathode in this study. Hence, it is clear that PrBaNiMn is a novel single-phase cathode material for H–SOFC combined with the compatibility analysis by XRD and EDS mapping mentioned above. And the thermal expansion coefficient (TEC)



Fig. 7 The thermal expansion coefficient of PrBaNiMn over the temperature range of $100\text{--}800\text{ }^\circ\text{C}$.

of the prepared PrBaNiMn is $10.35 \times 10^{-6}\ \text{K}^{-1}$ (Fig. 7), which is close to that of the BaCeO_3 -based electrolyte.⁵² In this case, it possesses better compatibility with the electrolyte than conventional perovskite materials. From the XPS study, the variable valence of the cations in the R–P structure can accelerate the oxygen transfer ability and oxygen reduction reaction catalytic activity. The lower E_a of the PrBaNiMn cathode can mitigate the performance degradation of the cell with a reduction in operation temperature. As expected, the performance of the PrBaNiMn cathode may be improved further when it is prepared by special synthesis methods or the particle size is decreased by reducing the roasting temperature with the guarantee of a single R–P phase structure. The molten salt,⁵³ electrostatic spinning⁷ and microwave sintering⁵⁴ methods may provide a new approach to improve the properties of the cathode further. In the stability test, the single cell with the PrBaNiMn cathode remains stable for 100 hours with no degradation and a power output of around $350\ \text{mW cm}^{-2}$ under a cell voltage of $0.7\ \text{V}$ at $600\text{ }^\circ\text{C}$ (Fig. 6f). This demonstrates that the PrBaNiMn cathode possesses fine chemical stability and compatibility with the electrolyte layer against water vapor and CO_2 under working condition. Combined with the higher peak power density and lower R_p compared with other reported cathodes under similar testing conditions, PrBaNiMn could be an outstanding alternative cathode material for proton-conducting SOFCs (H–SOFCs).

4. Conclusions

A novel double-layered R–P oxide of $\text{Pr}_2\text{BaNiMnO}_{7-\delta}$ was developed as an efficient cathode electrocatalyst for low-temperature H–SOFCs. Polycrystalline PrBaNiMn constitutes two members of a homologous series, the essential feature of which is the existence of two connected Ni/Mn octahedral layers with a perovskite-like structure, linked by a PrO/BaO rock-salt-like layer. Random distributions of 3d-metals, variable valence of the cation and oxygen vacancies in the perovskite blocks and interstitial oxygen in the rock-salt layers are directly associated with high ionic transformation and ORR activity. Moreover, the tetragonal PrBaNiMn with $I4/mmm$ space group symmetry has excellent chemical compatibility and similar TEC to the BaCeO_3 -based electrolyte. The electrochemical study shows that the peak power density of the anode supported single cell with PrBaNiMn is 1070 mW cm^{-2} at 700°C , with stable performance at 600°C under 0.7 V without any degradation after 100 hours. Even at 500 and 400°C , the peak power density of the cell reached 259 and 135 mW cm^{-2} , respectively. The area-specific polarization resistance of this cell is $0.084 \Omega \text{ cm}^2$ at 700°C under OCV conditions. Interestingly, the activation energy (E_a) for the polarization resistance of the assembled single cell is lower than that reported in the literature, corresponding to a value of 0.96 eV . The excellent performance is higher than those of state-of-the-art R–P structure materials used as cathodes in LT-SOFCs. Thus, the double-layered Ruddlesden–Popper perovskite oxide $\text{Pr}_2\text{BaNiMnO}_{7-\delta}$ is a preminent highly active low-temperature cathode material.

Conflicts of interest

There are no conflicts to declare.

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