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# Study on the performance and mechanism of a p–n type $\text{In}_2\text{O}_3/\text{BiOCl}$ heterojunction prepared using a sacrificial MOF framework for the degradation of PFOA†

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In this study, an  $\text{In}_2\text{O}_3/\text{BiOCl}$  p–n heterojunction was prepared using a co-calcination method. By utilising the built-in electric field formed near the heterojunction interface, photoinduced electron–hole pairs can be effectively separated, thereby enhancing the photocatalytic activity of the photocatalyst. Experimental results indicate that the p–n heterojunction photocatalyst significantly enhanced photocatalytic activity in the degradation of PFOA under UV light irradiation. Within 2 h, the defluorination rate of PFOA achieved by the heterojunction photocatalyst reached 84.01%, while the pure  $\text{BiOCl}$  and  $\text{In}_2\text{O}_3$  photocatalysts exhibit defluorination rates of 61.82% and 56.69%, respectively. The degradation mechanism of PFOA was studied through free radical capture experiments, VB-XPS, FT-IR, and LC-MS. Mechanistic studies show that the main active substances in the heterojunction are holes ( $h^+$ ) and superoxide radicals ( $\cdot\text{O}_2^-$ ). The holes in the valence band of  $\text{In}_2\text{O}_3$  are transferred to  $\text{BiOCl}$  under the effect of the built-in electric field, and the defluorination of PFOA mainly occurs on the  $\text{BiOCl}$  component of the heterojunction. This highlights the superiority of heterojunctions over pure photocatalysts in terms of their photocatalytic efficiency and provides insights into the photocatalytic degradation mechanism of PFOA.

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## 1. Introduction

Perfluorooctanoic acid (PFOA) is a type of synthetic perfluorinated organic compound that can be almost completely ionized in water. As a strong organic acid, it can corrode the skin and has a molecular weight of  $414.06 \text{ g mol}^{-1}$ .<sup>1</sup> Since 1950, Minnesota Mining and Manufacturing Company (3M) has been developing perfluorinated compounds, which have been widely used in various fields, such as refrigerants, polymers, flame retardants, surfactants, and pharmaceuticals.<sup>2</sup> However, PFOA is commonly detected in groundwater, soil, and biota owing to its persistent and bioaccumulative nature.<sup>3,4</sup> Moreover, some studies have found a close relationship between PFOA and human health, including increased cholesterol and liver enzyme levels, significantly increased incidence of kidney cancer and testicular cancer, reduced fertility, developmental effects on children's lungs, decreased immunity, and induction of thyroid disease.<sup>5,6</sup> Some studies have shown that PFOA can have an impact on fetal development through maternal exposure.<sup>7,8</sup> Therefore, it is urgent to develop efficient technology for

eliminating PFOA pollutants in water using photocatalysis to protect human health.

In recent years, researchers worldwide have conducted numerous studies on the degradation of PFOA, including those based on reverse osmosis,<sup>9</sup> adsorption,<sup>10</sup> electrochemistry,<sup>11</sup> advanced oxidation/reduction<sup>12</sup> and photocatalytic degradation.<sup>13–15</sup> Although adsorption and reverse osmosis methods can effectively remove PFOA from wastewater, further treatment is required for the removal of residual substances. In the processes of electrochemical and advanced oxidation degradation of PFOA, hydrogen atoms on the carbon chain of PFOA molecules are completely replaced by fluorine atoms. This results in the carbon atoms being surrounded by fluorine atoms in the spatial structure, making it impossible for external active groups to directly attack the carbon chain.<sup>16</sup> Moreover, thermodynamically, owing to the high bond energy of the C–F bond ( $485 \text{ kJ mol}^{-1}$ ),<sup>17</sup> the C–F bond is very stable, resulting in the low efficiency of these two methods in PFOA degradation. Photocatalytic degradation technology has strong oxidative ability compared with the commonly used degradation technologies and exhibits particularly strong selectivity towards refractory organic compounds.<sup>18</sup> Therefore, scholars worldwide are currently employing photocatalytic degradation techniques to study the degradation of PFOA. However, as shown in Table 1, most of the previous studies were time-consuming with low degradation rates, and the degree of

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Table 1 Photocatalysis technologies for PFOA degradation

Photocatalyst	Light wavelength	Conditions	Reaction time	Degradation & mineralization ratio	Ref.
BiOHP/CS	254 nm UV lamp	$C_0 = 0.12 \text{ mM}$ $C_{\text{catalyst}} = 0.5 \text{ g L}^{-1}$ $\text{pH} = 5$	4 h	99% & 32.5%	19
In-MOF/BiOF	254 nm UV lamp	$C_0 = 15 \text{ mg L}^{-1}$ $C_{\text{catalyst}} = 0.5 \text{ g L}^{-1}$	3 h	99% & 34%	20
BiOI@Bi <sub>5</sub> O <sub>7</sub>	Solar irradiation	$C_0 = 15 \text{ mg L}^{-1}$ $C_{\text{catalyst}} = 0.5 \text{ g L}^{-1}$ $\text{pH} = 3$	6 h	80% & 60%	21
BiOF	UV lamp	$C_0 = 15 \text{ mg L}^{-1}$ $C_{\text{catalyst}} = 0.5 \text{ g L}^{-1}$	6 h	99% & 26%	22
ZIF67/MIL-100(Fe)@C <sub>3</sub> N <sub>4</sub>	Iodine-tungsten lamp	$C_0 = 10 \text{ mg L}^{-1}$ $C_{\text{catalyst}} = 1 \text{ g L}^{-1}$ $\text{pH} = 4.6$	8 h	79.2% & —	23
BiOCl	UV lamp	$C_0 = 20 \text{ mg L}^{-1}$ $C_{\text{catalyst}} = 1 \text{ g L}^{-1}$ $\text{pH} = 3.8$	4 h	— & 29.93%	24
In <sub>2</sub> O <sub>3</sub> /BiOCl	UV lamp	$C_0 = 20 \text{ mg L}^{-1}$ $C_{\text{catalyst}} = 0.2 \text{ g L}^{-1}$ $\text{pH} = 5.0$	2 h	— & 84.01%	This work

mineralization of PFOA was not obvious. Thus, it is necessary to further develop a photocatalyst that can efficiently degrade PFOA.

BiOCl is a common p-type semiconductor material.<sup>25</sup> Due to its unique layered structure, its electronic transition is an indirect bandgap transition. The [Bi<sub>2</sub>O<sub>2</sub>] atom-staggered layered structure provides enough space to polarize atoms and orbitals,<sup>26,27</sup> thereby forming internal electric fields perpendicular to each layer, and effectively separating the generated electron-hole pairs. It has been reported that BiOCl exhibits exceptional degradation performance for the photocatalytic degradation of PFOA.<sup>28–30</sup> However, during its degradation process, the generated short-chain perfluoro carboxylic acids (PFCAs) resulting from the incomplete mineralization of PFOA still can pose a threat to the ecological environment,<sup>31</sup> so further research is needed to achieve complete defluorination and mineralization. The construction of heterojunctions can effectively improve the photocatalytic performance of semiconductors.<sup>32</sup> The reason is that in a heterojunction, the establishment of the heterojunction interface enhances the transfer of photo-generated charges, thereby enhancing the photocatalytic activity of the heterojunction.

In<sub>2</sub>O<sub>3</sub> is an n-type semiconductor that is commonly used in photocatalytic oxidation studies due to its narrow bandgap (2.7 eV) and simple, low-cost preparation method.<sup>33</sup> However, the photocatalytic efficiency of In<sub>2</sub>O<sub>3</sub> is low due to the easy recombination of its photo-generated electron-hole pairs. To enhance the photocatalytic efficiency of In<sub>2</sub>O<sub>3</sub>, it can be combined with other p-type semiconductors to form a p-n heterojunction. An internal electric field will be generated near the interface of the heterojunction, which will guide the photogenerated electrons produced in the heterojunction to transfer a conduction band (CB) in the n-type semiconductor,<sup>25</sup> while the photogenerated holes will remain in the valence band (VB) of the p-type semiconductor. Therefore, the internal electric field near the

interface will improve the separation efficiency and activity of the photogenerated electron-hole pairs.

In this study, an In<sub>2</sub>O<sub>3</sub>/BiOCl composite material was prepared by a simple mixing-calcination method. The formation of a p-n heterojunction for the composite material In<sub>2</sub>O<sub>3</sub>/BiOCl significantly improved the photocatalytic degradation of PFOA. The photocatalytic performance of the prepared p-n heterojunction In<sub>2</sub>O<sub>3</sub>/BiOCl was systematically investigated by defluorination mineralization of refractory organic pollutants PFOA under ultraviolet light. The roles of various active species in the photocatalytic degradation process were identified, and the pathways of electron transfer, photocatalytic degradation mechanism, and degradation pathway of PFOA in the p-n heterojunction were revealed.

## 2. Experimental

### 2.1 Chemical reagents

Perfluorooctanoic acid (PFOA, Shanghai Adamas Reagent Co., Ltd, 96.0%), hydrated indium(III) nitrate (In(NO<sub>3</sub>)<sub>3</sub>·xH<sub>2</sub>O, Adamas, 99.9%), *p*-phthalic acid (C<sub>8</sub>H<sub>6</sub>O<sub>4</sub>, Adamas, 99.0%) sodium chloride (NaCl, Chengdu Cologne Chemical Co., Ltd, 99.5%), acetic acid (CH<sub>3</sub>COOH, Adamas, 99.0%), potassium bromate (KBrO<sub>3</sub>, Cologne, 99.8%), bismuth nitrate hydrate (Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O, Cologne, 99.0%), methanol (CH<sub>3</sub>OH, Cologne, 99.5%), ascorbic acid (C<sub>6</sub>H<sub>8</sub>O<sub>6</sub>, Cologne, 99.7%), ethylenediaminetetraacetic acid disodium salt (C<sub>10</sub>H<sub>14</sub>N<sub>2</sub>Na<sub>2</sub>O<sub>8</sub>, Cologne, 99.0%), sodium hydroxide (NaOH, Cologne, 98.0%), ethanol (C<sub>2</sub>H<sub>5</sub>OH, Cologne, 99.7%) and nitric acid (HNO<sub>3</sub>, East Sichuan Chemical Group Co., Ltd, 65.0–68.0%). Deionized water was used in all experiments.

### 2.2 Preparation of photocatalysts

**2.2.1 Preparation of BiOCl.** The BiOCl photocatalyst was prepared by hydrothermal method using bismuth nitrate and NaCl as raw materials. 0.01 mol Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O and 0.01 mol



NaCl were dissolved in glacial acetic acid and deionized water, respectively, and then an appropriate amount of methanol was added to an acetic acid solution containing bismuth nitrate. NaCl solution was added dropwise to the above solution, and the mixture was stirred for 0.5 h, transferred to a polytetrafluoroethylene reactor, and reacted at 160 °C for 24 h. The above reaction products were cooled to room temperature, filtered, and washed three times with deionized water and ethanol, respectively. The obtained solid product was dried at 80 °C for 12 h, and the final sample was obtained.

**2.2.2 Preparation of  $\text{In}_2\text{O}_3$ .** First, 0.60 g of  $\text{In}(\text{NO}_3)_3 \cdot x\text{H}_2\text{O}$  (0.2 mol) and 0.33 g of PTA were dissolved in 50 mL *N,N*-dimethylformamide solution, and then irradiated for 20 min under ultrasonication. The reaction solution was transferred to a reaction kettle lined with polytetrafluoroethylene, and maintained at 130 °C for 4 h. After cooling to room temperature and filtering, the product was washed with ethanol three times, and then dried in a vacuum drying oven at 50 °C for 12 h to obtain the precursor. The precursor was thoroughly ground and transferred to a crucible, and calcined at 550 °C in a muffle furnace at a heating rate of 3 °C per min for 1 h. The final product,  $\text{In}_2\text{O}_3$ , was obtained by cooling down to room temperature at a rate of 5 °C per min.

**2.2.3 Preparation of the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction.** The prepared  $\text{In}_2\text{O}_3$  and  $\text{BiOCl}$  were weighed according to the mass ratio. The two materials were dispersed in 5 mL of EtOH, and then the mixture was sonicated for 20 min. The resulting suspension was dried at 60 °C for 12 h until completely dry. The reaction product was ground thoroughly and then transferred into an alumina crucible. The crucible was heated at a heating rate of 5 °C per min to 300 °C, and calcined for 3 h. The final product was named according to the different mass ratios, such as 20%  $\text{In}_2\text{O}_3/\text{BiOCl}$ , 25%  $\text{In}_2\text{O}_3/\text{BiOCl}$ , 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$ , 35%  $\text{In}_2\text{O}_3/\text{BiOCl}$ , and 40%  $\text{In}_2\text{O}_3/\text{BiOCl}$ .

### 2.3 Characterization

The XRD pattern of the catalyst was determined using a D2 Phaser X-ray diffractometer (XRD,  $\text{Cu K}\alpha = 1.5406 \text{ \AA}$ , Bruker). The specific surface area ( $S_{\text{BET}}$ ) of the samples was measured by SSA-4200 (Builder, Beijing). The morphology of the catalyst was analyzed by scanning electron microscopy (SEM, Tescan Vega 3 SBU). X-ray photoelectron spectroscopy (XPS) (Escalab 250Xi, Thermo Fisher Scientific) was used to investigate the surface chemical composition of the heterojunction. The diffuse reflectance spectroscopy (DRS) of the catalyst was recorded using a UV-visible spectrophotometer (UV-2550, Shimadzu). The  $e^-/h^+$  recombination rate was tested on a fluorescence spectrometer (PL, PICOQuant FT-300). Electrochemical impedance spectroscopy (EIS) and transient photocurrent ( $I-t$ ) tests were performed on an electrochemical workstation (CHI660E). An ion chromatography (Essentia IC16, Shimadzu) system coupled with an ion meter (PXSJ-216F) was employed to quantify the fluoride ion ( $\text{F}^-$ ) concentrations during the experimental analysis. A TOC analyzer (TOC-L, Shimadzu) was used to determine the removal efficiency of organic carbon in PFOA. The electron spin resonance spectrometer (ESR, Bruker MX-PLUS) was used to test the free radicals produced by the

samples. The adsorption of the catalyst for PFOA was tested by Fourier transform infrared spectrometer (FT-IR, Bruker).

The detection and analysis of the intermediate products generated during the degradation of PFOA were carried out using high-performance liquid chromatography/quadrupole time-of-flight mass spectrometry (HPLC/QTOF/MS). MassLynx V4.1 was used for data analysis. The specific testing parameters included an ACQUITY UPLC BEH C18 column (1.7  $\mu\text{m}$ , 2.1 mm  $\times$  50 mm) with a column temperature of 40 °C and injection volume of 3  $\mu\text{L}$ . An acetic acid ammonium solution (2.5 mmol  $\text{L}^{-1}$ ) was used as mobile phase A, while acetonitrile was used as mobile phase B for elution. In the gradient elution mode, mobile phase A accounts for 90–58%, 58–30%, 30–25%, and 25–90% of the total eluent volume at 0–3 min, 3–5 min, 5–8 min, and 8–12 min, respectively. The flow rate is set at 0.4 mL per minute. Mass spectrometry employs electrospray ionization (ESI) as an ion source, utilizing the negative ion mode and leucine enkephalin as an online calibration substance. The cone voltage is set at 40 V, with the collision energy ranging from 20–45 V for LC-MS. The ion source temperature is set at 100 °C and the desolvation temperature at 300 °C. The capillary voltage is set at 3 kV, and the desolvation gas flow rate is 600 L per h. Data acquisition is acquired through the MSE mode.

### 2.4 Photocatalytic defluorination of PFOA

To achieve enhanced degradation of PFOA, various light sources were systematically evaluated, with ultraviolet (UV) irradiation being ultimately selected as the optimal condition for PFOA decomposition. UV light irradiation was provided by a 500 W mercury lamp. In order to reduce the heat generated by the lamp during the degradation of PFOA, the lamp was placed in a cylindrical quartz water jacket and completely wrapped by a quartz water jacket. The degradation temperature was maintained by cooling water. Before the mercury lamp was turned on, 50 mL PFOA solution was prepared and stirred by magnetic stirring in the dark for half an hour to reach adsorption–desorption equilibrium. At fixed intervals throughout the degradation process, equal samples of degradation solution were taken out. To investigate the effect of the preparation conditions on heterojunctions, the degradation effect of heterojunctions prepared under different conditions was tested under the same conditions. The influence of factors such as the dosage of the photocatalyst, pH, and initial concentration of PFOA on the degradation of PFOA was investigated. The experiments for capturing the reactive species were similar to the previous photocatalytic activity tests. Different scavengers, including ethylenediaminetetraacetic acid disodium salt (EDTA), benzoquinone (BQ), and isopropanol (IPA), were added to the PFOA solution to capture holes ( $h^+$ ), superoxide radicals ( $\text{O}_2^-$ ), and hydroxyl radicals ( $\text{OH}^-$ ).

## 3. Results and discussion

### 3.1 Characterization and analysis of $\text{In}_2\text{O}_3/\text{BiOCl}$ heterojunction

The XRD pattern of the prepared photocatalyst is shown in Fig. 1. The diffraction peaks at  $2\theta = 21.5$  (211), 30.6 (222), 35.5



(400), 51.0 (440), and 60.7 (622) in the  $\text{In}_2\text{O}_3$  sample spectrum are in good agreement with the standard pattern of the cubic phase  $\text{In}_2\text{O}_3$  (PDF #71-2194).<sup>34</sup> In the  $\text{BiOCl}$  sample spectrum, all diffraction peaks are similar to those of the diffraction peaks of the pure tetragonal phase structure  $\text{BiOCl}$  standard (PDF #82-0485).<sup>35</sup> The XRD spectra of the pure  $\text{In}_2\text{O}_3$  and  $\text{BiOCl}$  samples do not exhibit any impurity peaks, indicating the high purity of the samples.<sup>36</sup> However, it can be observed that the diffraction peaks of the prepared  $\text{In}_2\text{O}_3$  are broad and weak, indicating that the crystallinity of the sample is slightly inferior to that of  $\text{BiOCl}$ . The XRD spectra of the  $\text{In}_2\text{O}_3/\text{BiOCl}$  photocatalysts with different composite ratios show the characteristic diffraction peaks of  $\text{In}_2\text{O}_3$  and  $\text{BiOCl}$  (marked in Fig. 1), indicating the successful preparation of the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction. Furthermore, according to the changing trend of peaks in the X-ray diffraction (XRD) spectra, it can be observed that as the proportion of  $\text{In}_2\text{O}_3$  in the composite material increases, the characteristic peak of  $\text{In}_2\text{O}_3$  gradually becomes stronger.

The morphology of the prepared photocatalyst was observed using SEM to reveal its microstructure. The morphologies of  $\text{BiOCl}$ ,  $\text{In}_2\text{O}_3$ , and 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  are shown in Fig. 2. SEM images of  $\text{BiOCl}$  and  $\text{In}_2\text{O}_3$  are presented in Fig. 2(A) and (B), respectively.  $\text{BiOCl}$  is represented in the form of small flakes and round-ball aggregates. Meanwhile,  $\text{In}_2\text{O}_3$  exhibits an irregular shape of hollow rods with uneven sizes and a smooth surface, and some small particles adhere to its surface, which might cause detachment during calcination. SEM images of the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  composite material, shown in Fig. 2(C and D), reveal that the combination between  $\text{BiOCl}$  and the  $\text{In}_2\text{O}_3$  materials was mediated by the small flake-shaped  $\text{BiOCl}$  coating on the surface of the hollow rod-shaped  $\text{In}_2\text{O}_3$  (Fig. 2(C)) or by

particle-shaped  $\text{In}_2\text{O}_3$  adhering to  $\text{BiOCl}$  that has fractured (Fig. 2(D)).

In order to understand the microstructure of the catalyst, the prepared materials were probed using transmission electron microscopy (TEM). Fig. 3(A) and (E) show the TEM images of  $\text{In}_2\text{O}_3$  and  $\text{BiOCl}$ , respectively. Fig. 3(A) further confirms the hollow rod-like morphology of  $\text{In}_2\text{O}_3$ . Fig. 3(F–G) presents the TEM images of the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  composite material prepared in this study. Compared with Fig. 3(B) ( $\text{In}_2\text{O}_3$ ) and Fig. 3(C and D) ( $\text{BiOCl}$ ), it is confirmed again that the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction was successfully constructed, indicating the proper combination of these two different materials in the heterojunction. The HRTEM images of  $\text{BiOCl}$  and  $\text{In}_2\text{O}_3$  are displayed in Fig. 3(I, J and K). The lattice spacings of the (101) and (003) crystal planes of  $\text{BiOCl}$ , with values of 0.334 nm and 0.245 nm, respectively, are consistent with that reported in the literature for  $\text{BiOCl}$  (PDF #82-0485). The HRTEM image in Fig. 3(K) shows the lattice spacing of the (222) and (211) crystal planes of  $\text{In}_2\text{O}_3$ , with values of 0.292 nm and 0.413 nm, respectively, which is in good agreement with the standard values of  $\text{In}_2\text{O}_3$  (PDF# 71-2194). Fig. 3(L) shows an HRTEM image of the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterostructure, where the (222) crystal plane of  $\text{In}_2\text{O}_3$  intersects and overlaps with the (001) and (003) crystal planes of  $\text{BiOCl}$ , providing further evidence for the successful preparation of the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterostructure.

**3.1.1 BET specific surface area and pore size analysis of the photocatalyst.** The specific surface area ( $S_{\text{BET}}$ ) and pore size of  $\text{BiOCl}$ ,  $\text{In}_2\text{O}_3$ , and 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  were analyzed using  $\text{N}_2$  adsorption/desorption, and the results are presented in Table 2. It can be observed from this table that the specific surface area of  $\text{BiOCl}$  increases significantly from  $3.42 \text{ m}^2 \text{ g}^{-1}$  to  $13.87 \text{ m}^2$

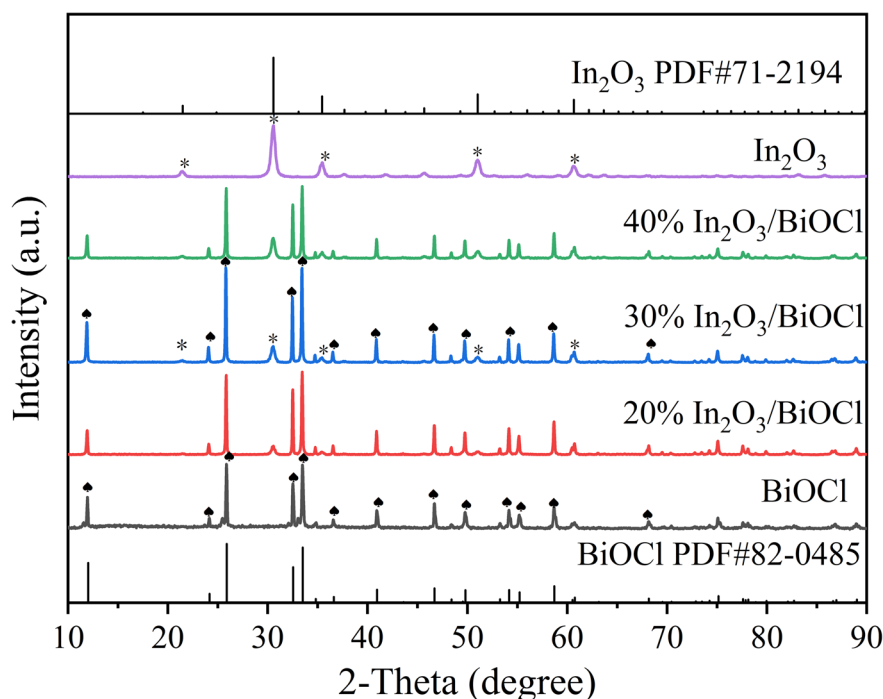


Fig. 1 XRD spectra of  $\text{In}_2\text{O}_3$ ,  $\text{BiOCl}$ , and the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction with different mass ratios.



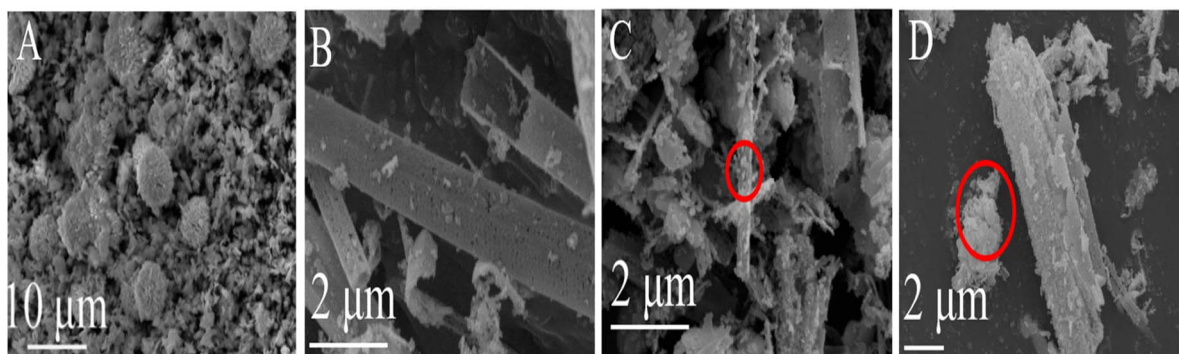


Fig. 2 SEM images of the photocatalyst. (A) BiOCl; (B) In<sub>2</sub>O<sub>3</sub>; (C and D) 30% In<sub>2</sub>O<sub>3</sub>/BiOCl.

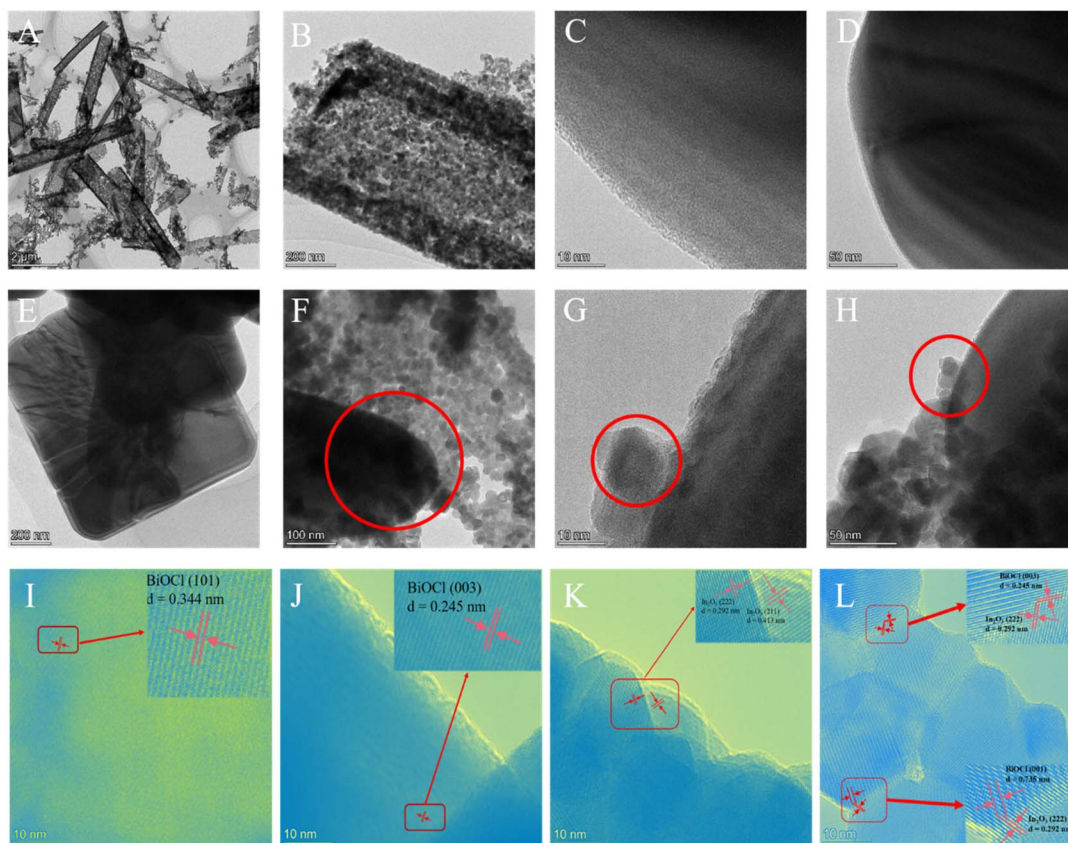


Fig. 3 TEM (A–H) and HRTEM (I–L) images of the photocatalyst. (A, B, and K) In<sub>2</sub>O<sub>3</sub>; (C–E, I and J) BiOCl; (F–H and L) 30% In<sub>2</sub>O<sub>3</sub>/BiOCl.

$\text{g}^{-1}$  after the introduction of In<sub>2</sub>O<sub>3</sub>. This increase in the specific surface area effectively enhances the adsorption of reactants on the catalytic surface, thereby promoting their absorption of light and enhancing the catalytic activity.

The nitrogen adsorption–desorption isotherms and pore size distribution curves of the prepared photocatalyst are shown in Fig. 4. It can be seen from Fig. 4(A) that the N<sub>2</sub> adsorption–desorption isotherms of the three prepared samples match the trend of the type IV isotherm. Moreover, when the ratio of  $P/P_0$  is between 0.6 and 1.0, the hysteresis loops of the H3 adsorption can be observed according to the different sizes classified by

IUPAC. So, it can be concluded that all three samples have spaces of different pore sizes. As shown in Fig. 4(B), the pore size of the prepared BiOCl, In<sub>2</sub>O<sub>3</sub>, and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl are

Table 2 Average crystallite size and specific surface area of samples

Sample	Specific surface area ( $\text{m}^2 \text{g}^{-1}$ )	Pore diameter (nm)	VP ( $\text{mL g}^{-1}$ )
BiOCl	3.42	21.06	0.0182
30% In <sub>2</sub> O <sub>3</sub> /BiOCl	13.87	20.39	0.0707
In <sub>2</sub> O <sub>3</sub>	33.09	20.00	0.1655



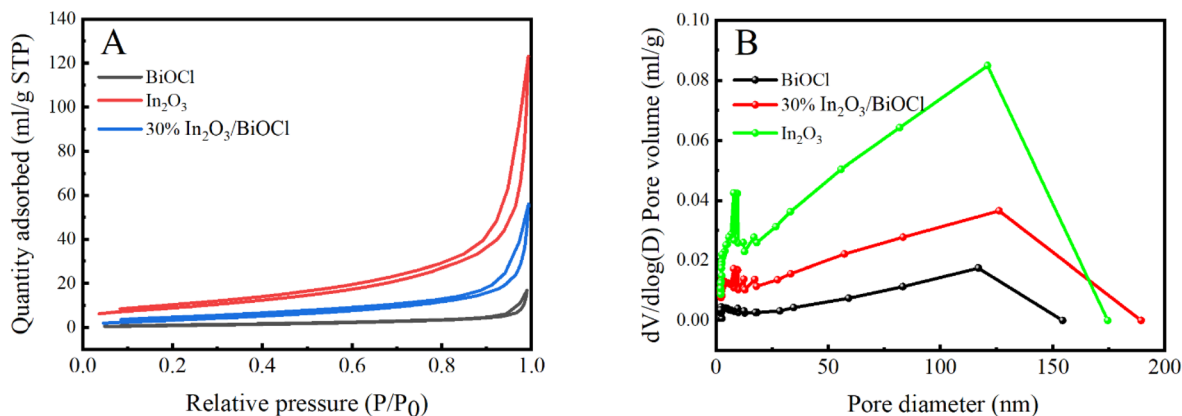


Fig. 4 Nitrogen adsorption–desorption diagram of the photocatalyst (A), and micropore distribution diagram of the photocatalyst (B).

mainly distributed in the range of 50–150 nm. By comparison, the pore volume of BiOCl is the smallest, while the presence of the large pore volume in In<sub>2</sub>O<sub>3</sub> and the heterojunction is conducive to the diffusion of photogenerated holes, which can effectively improve its photocatalytic activity. Compared with the BET specific surface area (33.09 m<sup>2</sup> g<sup>-1</sup>) and pore volume (0.1655 mL g<sup>-1</sup>) of In<sub>2</sub>O<sub>3</sub>, the BET-specific surface area (13.87 m<sup>2</sup> g<sup>-1</sup>) and pore volume (0.0707 mL g<sup>-1</sup>) of 30% In<sub>2</sub>O<sub>3</sub>/BiOCl are slightly reduced. However, it overcomes the drawback of In<sub>2</sub>O<sub>3</sub>, which can only absorb light above 360 nm without any PFOA degradation activity (verified by experimental exploration in subsequent mechanism research studies).

**3.1.2 XPS analysis of photocatalysts.** The surface chemical composition and valence state of the heterojunction were extensively studied using X-ray photoelectron spectroscopy (XPS), as shown in Fig. 5. Fig. 5(A) displays the XPS spectra of In<sub>2</sub>O<sub>3</sub>, 30% In<sub>2</sub>O<sub>3</sub>/BiOCl, and BiOCl. The presence of elements In, Bi, Cl, and O is distinctly observed in the XPS spectrum of the 30% In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction. Fig. 5(B) displays the high-resolution XPS spectrum of Bi 4f. These two dominant peaks at 164.6 eV and 159.4 eV correspond to the Bi 4f<sub>5/2</sub> and Bi 4f<sub>7/2</sub> signals of BiOCl, respectively.<sup>37–39</sup> The two characteristic peaks of Bi 4f on In<sub>2</sub>O<sub>3</sub>/BiOCl shift to 164.7 eV and 159.5 eV, respectively, which may be attributed to the coupling interface interaction between the heterogeneous components. Fig. 5(C) shows the high-resolution XPS spectrum of Cl 2p. The binding energies of the two strong peaks at 198.1 eV and 199.7 eV are assigned to Cl 2p<sub>1/2</sub> and Cl 2p<sub>3/2</sub> of Cl in BiOCl, respectively.<sup>40,41</sup> Compared with pure BiOCl, the binding energies of both characteristic peaks from In<sub>2</sub>O<sub>3</sub>/BiOCl slightly shifted towards higher energy, providing evidence of the coupling interface interaction caused by the formation of the heterojunction. As shown in Fig. 5(D), In 3d of In<sub>2</sub>O<sub>3</sub> is located at 451.9 eV and 444.3 eV, corresponding to the In 3d<sub>3/2</sub> and In 3d<sub>5/2</sub> peaks, respectively.<sup>42,43</sup> The two In 3d peaks of the In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction are located at 451.5 eV and 443.9 eV, respectively, which shifts towards lower binding energy compared to pure In<sub>2</sub>O<sub>3</sub>. This indicates that electrons on In<sub>2</sub>O<sub>3</sub> transfer to BiOCl, forming an interface electric field at the coupling interface. Moreover, a small peak appears at 442.3 eV in Fig. 5(D) for

In<sub>2</sub>O<sub>3</sub>/BiOCl, which can be attributed to Bi 4d<sub>5/2</sub> of BiOCl and further confirms the formation of the heterojunction.<sup>44</sup> From Fig. 5(E), it can be observed that each O 1s peak can be deconvoluted into three peaks. The peak with the lowest binding energy can be attributed to the Bi–O and In–O chemical bonds, oxygen atoms in the lattice of a molecule (O<sub>L</sub>). The peak with higher binding energy corresponds to an oxygen atom in the hydroxyl group of the adsorbed molecule (O<sub>H</sub>). The peak with the highest binding energy is typically associated with oxygen ions that contain defects in the imperfect lattice (O<sub>M</sub>).<sup>45–47</sup> It is observed that the O 1s fitting peaks in the heterojunction shifted towards lower binding energies to a certain extent, indicating the intimate interfacial contact between neighboring components. This is consistent with the result from the XRD spectroscopic analysis, which confirms the successful fabrication of the In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction. Furthermore, as shown in the fitting curves and Table 3, the percentage of the oxygen-vacancy-rich region in the In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction is higher than that in BiOCl, indicating an abundance of oxygen vacancies. These vacancies can serve as adsorption sites and facilitate the chemical adsorption of oxygen molecules at relatively low temperatures. Furthermore, the appropriate oxygen vacancies can enhance the photocatalytic performance by capturing electrons and suppressing the recombination of photo-generated electron–hole pairs,<sup>48</sup> thereby improving the utilization of light.

**3.1.3 Adsorption of PFOA.** The adsorption performance of the photocatalyst on PFOA was investigated because having strong adsorption is beneficial for the photocatalytic reaction.<sup>49</sup> The adsorption of PFOA on In<sub>2</sub>O<sub>3</sub>, In<sub>2</sub>O<sub>3</sub>/BiOCl, and BiOCl is shown in Fig. 6(A and B). Adsorption experiments were conducted by adding 25 mg of different photocatalysts to 50 mL (20 ppm) of PFOA solution. Fig. 6(A and B) demonstrates that the initial 20 min correspond to the rapid adsorption stage, followed by a decrease in the adsorption rate of PFOA by photocatalysts. The rapid adsorption can be attributed to two factors: (1) the abundance of oxygen vacancies on the BiOCl material surface allows for the adsorption of carboxyl oxygen atoms of PFOA, and the formation of chemical bonds; (2) In<sub>2</sub>O<sub>3</sub> prepared by the sacrificial MOF framework contains numerous inner



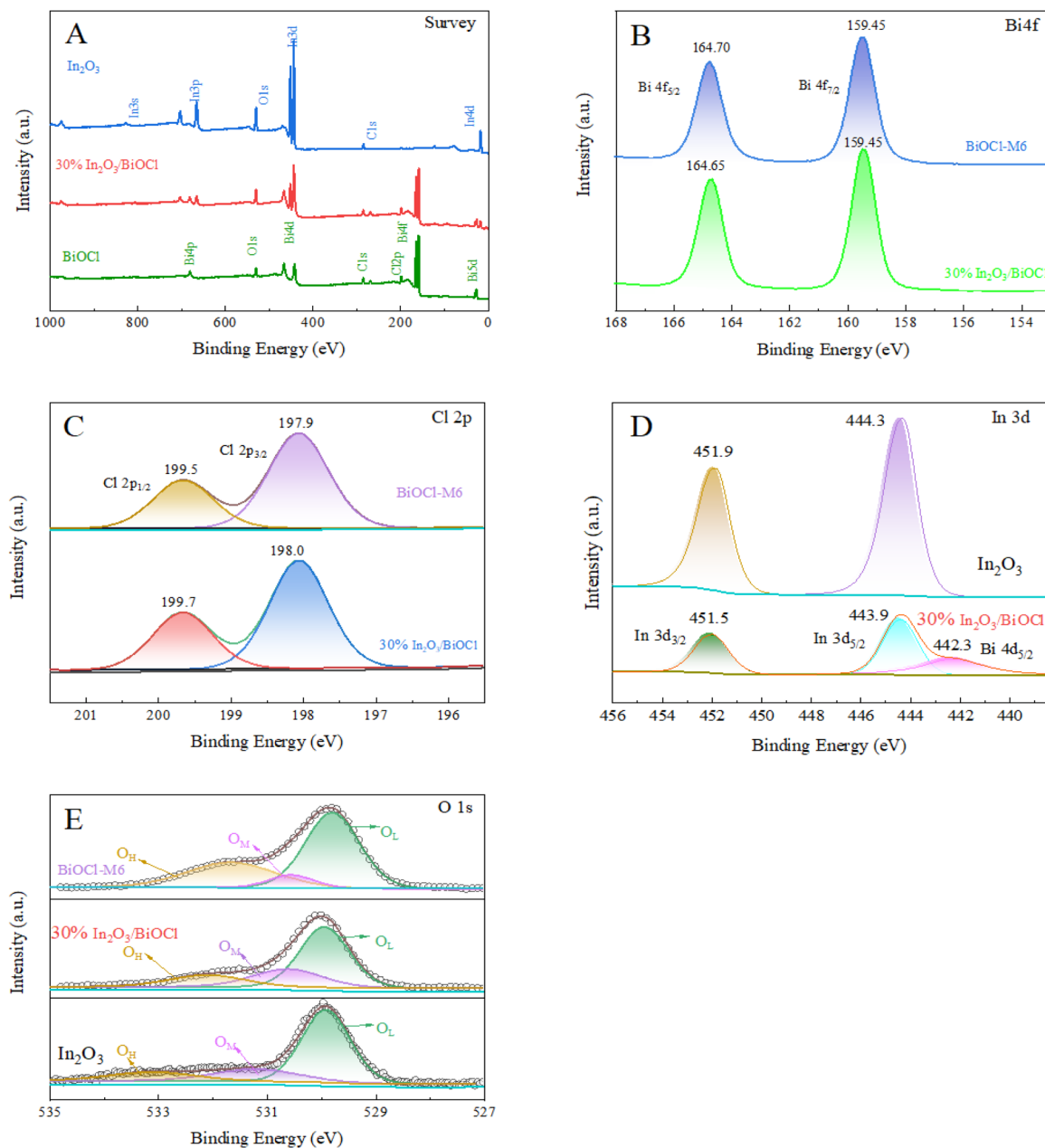


Fig. 5 XPS spectra of the photocatalysts. (A) XPS spectra of BiOCl, In<sub>2</sub>O<sub>3</sub>, and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl; (B) Bi 4f spectra of BiOCl and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl; (C) Cl 2p spectra of BiOCl and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl; (D) In 3d spectra of In<sub>2</sub>O<sub>3</sub> and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl; and (E) O 1s spectra of BiOCl, In<sub>2</sub>O<sub>3</sub>, and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl.

channels, which facilitates the adsorption and diffusion of molecules and possession of a high specific surface area, promoting the interaction between the material and reactants.<sup>50</sup>

Table 3 Sample O 1s peak fitting results

Sample	O <sub>L</sub> atomic (%)	O <sub>M</sub> atomic (%)	O <sub>H</sub> atomic (%)	O <sub>M</sub> /O <sub>L</sub>
In <sub>2</sub> O <sub>3</sub>	61.69	7.21	31.10	0.12
BiOCl	65.12	19.06	15.82	0.29
In <sub>2</sub> O <sub>3</sub> /BiOCl	57.87	25.01	17.12	0.43

After 60 min, the maximum adsorption capacities of BiOCl, In<sub>2</sub>O<sub>3</sub>, and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl are 17.0%, 68.2%, and 51.0%, respectively. The corresponding maximum adsorption capacities are determined to be 6.815 mg g<sup>-1</sup>, 27.272 mg g<sup>-1</sup>, and 20.404 mg g<sup>-1</sup>, respectively. To gain a better understanding of the adsorption mechanism, fitting analysis was performed on Fig. 6(B). The rate constants and correlation coefficients for the pseudo-first-order and pseudo-second-order kinetics models were calculated for different photocatalysts based on the experimental data, as shown in Table 4. The high values of the correlation coefficient *R*<sup>2</sup> in the table indicate that the adsorption of PFOA on the surface of the photocatalyst of BiOCl



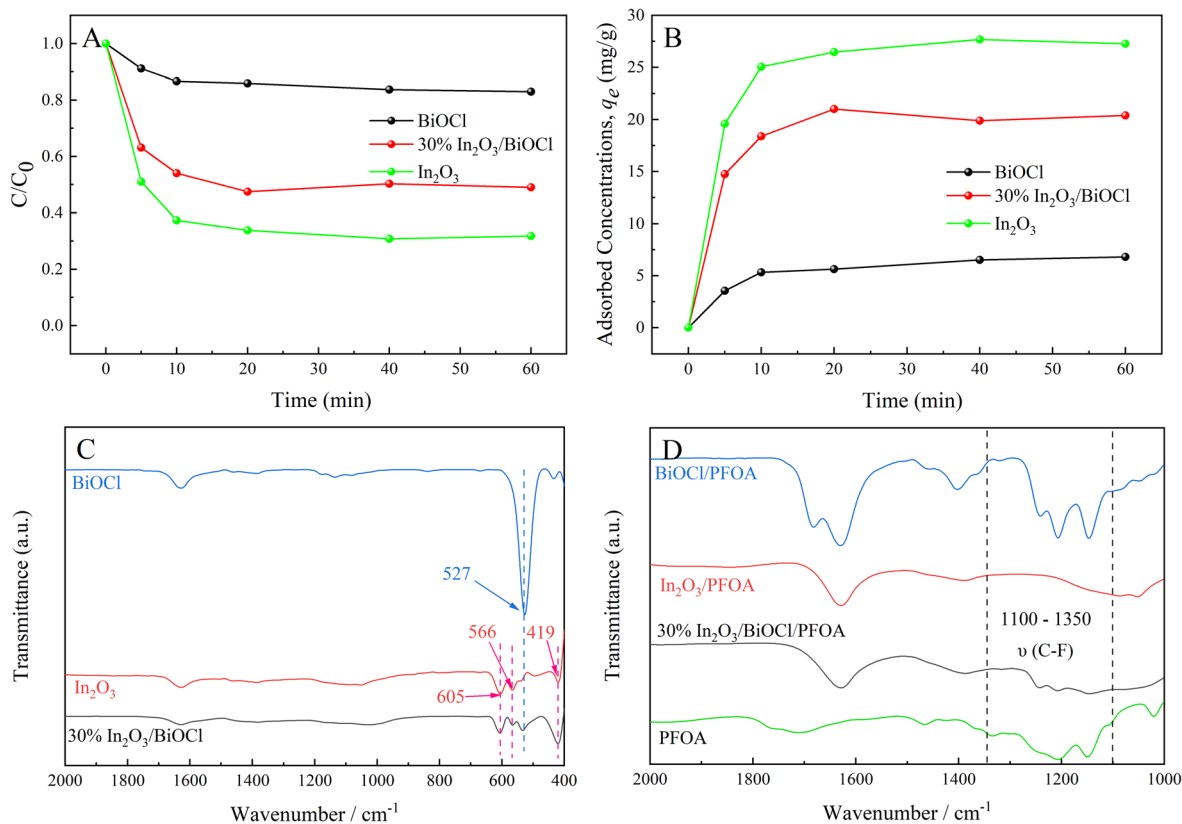


Fig. 6 Adsorption curve and FT-IR spectra. (A) Adsorption curve of different photocatalysts. (B) Adsorption volume change curve. (C) FT-IR spectra of BiOCl, In<sub>2</sub>O<sub>3</sub>, and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl. (D) FT-IR spectra of BiOCl/PFOA, In<sub>2</sub>O<sub>3</sub>/PFOA, and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl/PFOA.

involves both physical and chemical adsorption. For BiOCl, the correlation coefficients ( $R^2$ ) obtained from the fitting analysis for pseudo-first-order and pseudo-second-order kinetics are 0.985 and 0.992, respectively. The pseudo-second-order kinetics model shows a higher correlation coefficient. The adsorption process of PFOA on BiOCl is more accurately described by the pseudo-second-order kinetic model, indicating that the adsorption of PFOA on the photocatalyst mainly occurs through chemical adsorption. However, in the case of 30% In<sub>2</sub>O<sub>3</sub>/BiOCl and In<sub>2</sub>O<sub>3</sub>, the correlation coefficient of the pseudo-first-order kinetic model is greater than that of the pseudo-second-order kinetic model, suggesting that the pseudo-first-order kinetic model can more accurately describe the adsorption process of both photocatalysts on PFOA, and physical adsorption is the main mechanism. Moreover, the corresponding kinetic model equations can be used to more accurately calculate the adsorption capacity of photocatalysts for PFOA at equilibrium.<sup>49</sup>

FT-IR spectroscopy was utilized to further determine the composition of BiOCl, In<sub>2</sub>O<sub>3</sub>, and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl and their adsorption capacity for PFOA, and the results are shown in Fig. 6. Fig. 6(C) reveals that the characteristic peak of pure BiOCl at 527 cm<sup>-1</sup> is attributed to the stretching vibration of the Bi-O bond.<sup>51</sup> The characteristic peaks of pure In<sub>2</sub>O<sub>3</sub> at 605 cm<sup>-1</sup>, 566 cm<sup>-1</sup>, and 419 cm<sup>-1</sup> can be attributed to the asymmetric stretching of In-O bond.<sup>52-54</sup> Furthermore, the distinctive peaks of pure BiOCl and In<sub>2</sub>O<sub>3</sub> can be observed in the FT-IR spectra of the 30% In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction, indicating the successful preparation of heterojunction, which is consistent with the XRD results. In order to investigate the adsorption of PFOA on the photocatalyst, the infrared spectra of the photocatalyst after PFOA adsorption were analyzed. As shown in Fig. 6(D), the peaks from 1100 cm<sup>-1</sup> to 1350 cm<sup>-1</sup> are attributed to the vibrations of the -CF<sub>3</sub> and -CF<sub>2</sub> groups of PFOA.<sup>55</sup> Upon adsorption of PFOA onto BiOCl and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl

Table 4 Adsorption kinetic parameters of PFOA on BiOCl, 30% In<sub>2</sub>O<sub>3</sub>/BiOCl and In<sub>2</sub>O<sub>3</sub>

Adsorbent	Pseudo first-order			Pseudo second-order		
	q <sub>e</sub> (mg g <sup>-1</sup> )	K <sub>1</sub> (min <sup>-1</sup> )	R <sup>2</sup>	q <sub>e</sub> (mg g <sup>-1</sup> )	K <sub>2</sub> (g mg <sup>-1</sup> min <sup>-1</sup> )	R <sup>2</sup>
BiOCl	6.487	0.157	0.985	7.295	0.029	0.992
30% In <sub>2</sub> O <sub>3</sub> /BiOCl	20.401	0.252	0.997	21.640	0.023	0.987
In <sub>2</sub> O <sub>3</sub>	27.209	0.253	0.999	28.999	0.016	0.994



heterojunction, the corresponding peaks for the  $-\text{CF}_3$  and  $-\text{CF}_2$  groups of PFOA are observed from  $1100\text{ cm}^{-1}$  to  $1350\text{ cm}^{-1}$ . However, after PFOA is adsorbed onto  $\text{In}_2\text{O}_3$ , no corresponding vibration peak is found from  $1100\text{ cm}^{-1}$  to  $1350\text{ cm}^{-1}$ . This may be attributed to the removal of the MOF framework during the preparation of  $\text{In}_2\text{O}_3$ , which creates a significant number of porous structures that facilitate the internal adsorption of most PFOA molecules in the photocatalyst. Consequently, the concentration of residual PFOA on the surface of  $\text{In}_2\text{O}_3$  is relatively low, making it undetectable by infrared spectroscopy. The reaction rate of the pollutant adsorbed in the internal pores of the photocatalyst is limited by diffusion, leading to a lower reaction rate. Surface adsorption leads to the proximity of the reactant molecules to the active sites on the photocatalyst surface, and establishes an adsorption-desorption equilibrium state. This proximity and equilibrium state can promote the reaction rate. These results provide a foundation for the high efficiency of BiOCl in the degradation of PFOA.

### 3.2 Investigation of the catalytic activity and stability of the heterojunction

The photodegradation of PFOA was investigated under the fixed initial PFOA concentration of  $20\text{ mg L}^{-1}$ , pH of 4, and photocatalyst dosage of  $0.1\text{ g L}^{-1}$ , as presented in Fig. 7. To obtain the complete PFOA degradation process, the photocatalytic activity

of the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction was studied under a different light source, as illustrated in Fig. 7(A). Results show that the defluorination efficiency and rate of PFOA both decrease with increasing light source wavelength. At  $420\text{ nm}$  wavelength, the PFOA degradation becomes negligible due to the photocatalyst's excessively wide bandgap, which hinders the efficient utilization of visible light. Therefore, a mercury lamp with an emission wavelength of  $360\text{ nm}$  was adopted as a light source for subsequent experiments. The photocatalytic activity of BiOCl,  $\text{In}_2\text{O}_3$ , and different composite ratios of  $\text{In}_2\text{O}_3/\text{BiOCl}$  under UV light was investigated. As shown in Fig. 7(B), it can be seen that the defluorination rate of PFOA by BiOCl and  $\text{In}_2\text{O}_3$  is  $61.82\%$  and  $56.69\%$ , respectively, while the defluorination efficiency of PFOA exceeds  $75\%$  by the heterojunction photocatalyst. Especially, the defluorination rate of the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  photocatalyst reaches  $80.81\%$ , indicating that the photocatalytic activity is significantly enhanced. The amount of fluoride generated during the degradation increases linearly within  $30\text{ min}$  (Fig. 7(C)). The reaction is determined to be the pseudo-zero-order reaction. The slope of the graph calculates the fluoride generation rate of  $23.04\text{ }\mu\text{mol L}^{-1}\text{ min}^{-1}$  in the heterojunction photocatalyst  $\text{In}_2\text{O}_3/\text{BiOCl}$  system, which is  $3.23$  times ( $7.14\text{ }\mu\text{mol L}^{-1}\text{ min}^{-1}$ ) and  $2.09$  times ( $11.00\text{ }\mu\text{mol L}^{-1}\text{ min}^{-1}$ ) higher than the fluoride generation rate of pure BiOCl and the pure  $\text{In}_2\text{O}_3$  photocatalyst, respectively. Compared

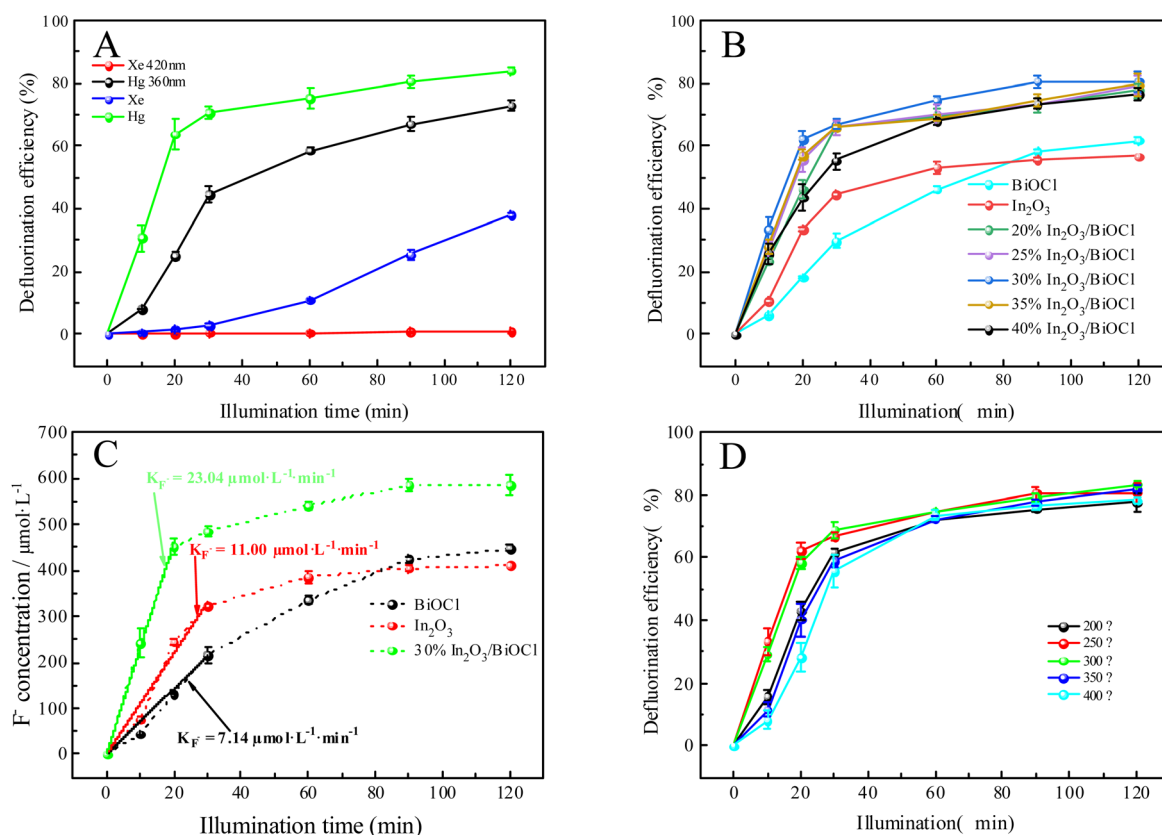


Fig. 7 Effect of preparation conditions of the photocatalyst on its photocatalytic activity. (A) The effect of different wavelengths of light source on the catalytic activity. (B) The effect of different composite ratios on the activity of the photocatalyst. (C) Pseudo-first-order defluorination rates of different photocatalysts. (D) The effect of calcination temperature on the catalytic activity.

with the pure BiOCl and pure  $\text{In}_2\text{O}_3$  photocatalysts, the heterojunction system does not possess any special active sites. Moreover, the specific surface area of the heterojunction ( $13.87 \text{ m}^2 \text{ g}^{-1}$ ) is inferior to that of  $\text{In}_2\text{O}_3$  ( $33.09 \text{ m}^2 \text{ g}^{-1}$ ). Nevertheless, the excellent defluorination performance of the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction photocatalysts toward PFOA is attributed to the establishment of an internal electric field, which enhances the utilization of light by the photocatalyst. Fig. 7(D) illustrates the photocatalytic activity of the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction photocatalyst prepared by different calcination temperatures. It can be observed that the activity significantly increases when the calcination temperature is increased from  $200 \text{ }^\circ\text{C}$  to  $300 \text{ }^\circ\text{C}$ , which may be attributed to the more stable interface coupling between BiOCl and  $\text{In}_2\text{O}_3$  at a higher calcination temperature. However, the activity of the heterojunction somewhat decreases when the calcination temperature further increases to  $400 \text{ }^\circ\text{C}$ , owing to the limited thermal stability of BiOCl. Its activity decreases when the calcination temperature exceeds  $300 \text{ }^\circ\text{C}$ , leading to the decreasing photocatalytic activity of the heterojunction.

To investigate the optimal catalytic degradation process of the photocatalyst, PFOA was used as the reaction substrate, and the effect of the photocatalyst dosage, initial pH value of pollutant and concentration of the degradation product on the degradation efficiency of the heterojunction photocatalyst were

systematically investigated, as shown in Fig. 8. When the initial concentration of PFOA is  $20 \text{ mg L}^{-1}$  and pH is 4, different dosages of the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction photocatalyst are used to degrade PFOA. As shown in Fig. 8(A), the degradation efficiency continuously increases with increasing catalyst dosage within the range of  $0.05 \text{ g L}^{-1}$  to  $0.2 \text{ g L}^{-1}$ . This phenomenon can be attributed to the fact that with a few photocatalysts, the availability of the catalytically active sites is limited, whereas with increasing dosage of photocatalyst, the quantity of active sites becomes more abundant.<sup>56</sup> However, upon increasing the dosage of the photocatalyst, the degradation efficiency of PFOA presents a downward trend. The reason is that the excessive amount of photocatalyst results in photocatalyst aggregation, which increases the solution turbidity, hinders the transmission of radiation to the interior of the solution, and scatters light, thereby reducing the efficiency of the photocatalytic degradation.<sup>57</sup> Therefore,  $0.2 \text{ g L}^{-1}$  is chosen as the optimal dosage of the photocatalyst.

The pH of the degradation solution plays a critical role in determining the surface charge properties of the catalyst and affects the adsorption of reactants on the catalyst surface, thereby influencing the efficiency of the photocatalytic reactions.<sup>58</sup> Therefore, in the process of the photocatalytic degradation of PFOA, the initial concentration of PFOA was fixed at  $20 \text{ mg L}^{-1}$ , the catalyst dosage was  $0.2 \text{ g L}^{-1}$ , and the pH was

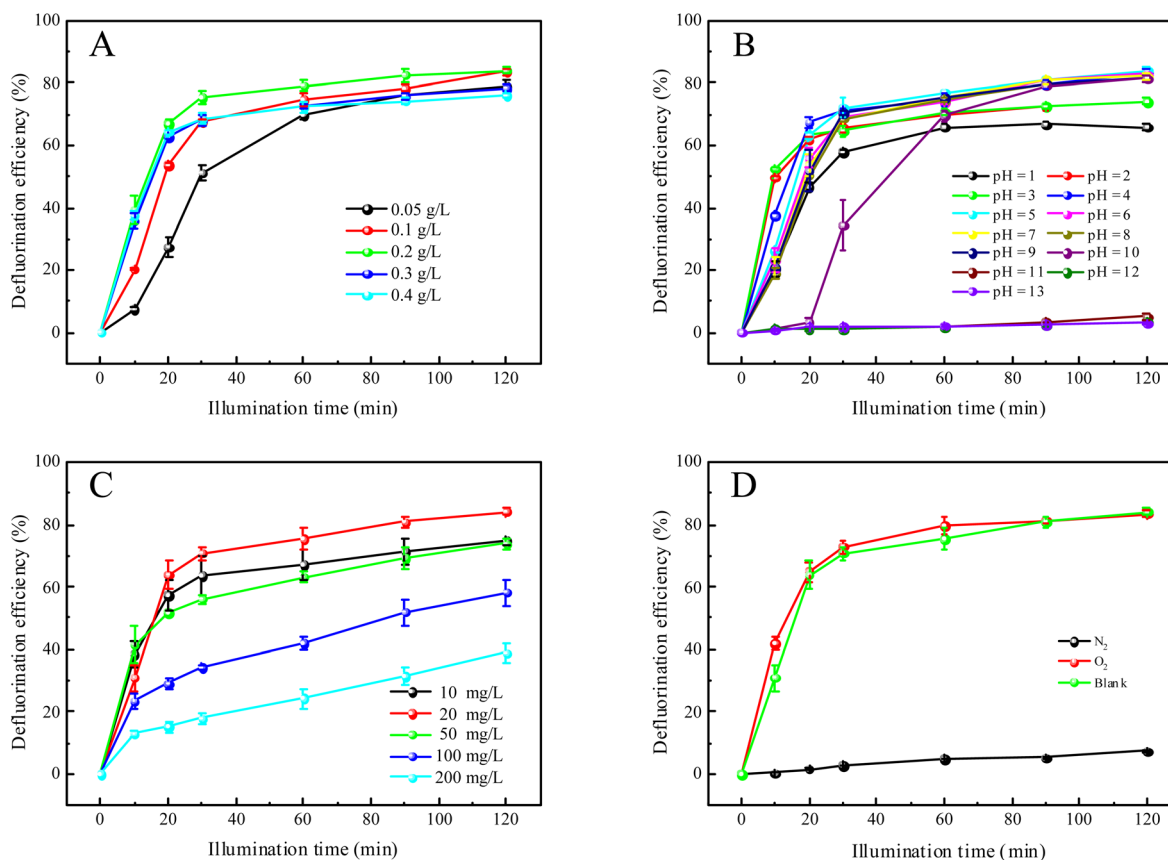


Fig. 8 Effect of photocatalytic degradation conditions on the defluorination rate of PFOA. (A) The effect of catalyst loading on the defluorination rate. (B) The effect of degradation solution pH on the defluorination rate. (C) The effect of the concentration of the degradation product on the defluorination rate. (D) The effect of different environmental atmospheres on the defluorination rate.



adjusted from 1 to 13. The defluorination efficiency of PFOA is shown in Fig. 8(B). As the pH of the PFOA solution increases from 1.00 to 13.00, the degradation rate of the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction photocatalyst firstly increases and then decreases, while the defluorination rate in the first 20 min decreases gradually with the increase of pH. It suggests that the acidic conditions are conducive to the degradation of PFOA. When the pH value is between 1.0 and 3.0, the defluorination effect is poor. This is attributed to the influence of  $\text{NO}_3^-$  in the nitric acid solution used to adjust the pH. Furthermore, the evaporation of HF gas caused by the combination of desorbed  $\text{F}^-$  and  $\text{H}^+$  in solution results in a lower measured concentration of fluoride ion. The photocatalytic degradation of PFOA reaches its optimum effect when the pH value is 5.0. Therefore, 5.0 is selected as the pH of the degradation solution.

During photocatalytic degradation, the substrate concentration and environmental atmosphere are important factors that influence the degradation. The impact of different initial concentrations of PFOA solutions on the defluorination rate was investigated when the catalyst dosage was  $0.2 \text{ g L}^{-1}$  and the pH value was 5, as shown in Fig. 8(C). The defluorination rate increases when the concentration of PFOA is increased from 10 to  $50 \text{ mg L}^{-1}$ . This may be attributed to the slow diffusion of PFOA in the solution under a low initial concentration, which makes it difficult to be adsorbed onto the surface of the catalyst. As a result, the defluorination rate increases when the PFOA concentration increases. When the initial concentration of PFOA is in the range of  $50\text{--}200 \text{ mg L}^{-1}$ , the defluorination rate decreases with the increase of the initial concentration. This phenomenon may be attributed to the saturation of active sites on the catalyst surface under the low solution concentration. As the solution concentration increases, the relative reduction of active sites leads to a decrease in the defluorination rate. This study also shows that the defluorination rate decreases when the initial concentration increases from 20 to  $200 \text{ mg L}^{-1}$ . The reason is that some  $\text{F}^-$  generated during the reaction will be adsorbed on the active sites, leading to a decrease in the defluorination rate.<sup>28</sup> The environmental atmosphere during the photocatalytic degradation also affects the reaction efficiency. As shown in Fig. 8(D), it can be seen that the photocatalytic efficiency is enhanced in the presence of a sufficient amount of oxygen, while PFOA is hardly degraded in the nitrogen atmosphere. This suggests that oxygen plays an indispensable role in the degradation process of PFOA.

To demonstrate the superior performance of the heterojunction photocatalyst compared to pure  $\text{BiOCl}$  and  $\text{In}_2\text{O}_3$ , the degradation of PFOA was carried out under acidic ( $\text{pH} = 3.0$ ), neutral ( $\text{pH} = 7.0$ ), and alkaline ( $\text{pH} = 10.0$ ) conditions using different photocatalysts. As shown in Fig. 9(A), the heterojunction exhibits excellent degradation efficiency towards PFOA under acidic ( $\text{pH} = 3.0$ ), neutral ( $\text{pH} = 7.0$ ), and alkaline ( $\text{pH} = 10.0$ ) conditions, while pure  $\text{BiOCl}$  only shows good degradation efficiency towards PFOA under acidic ( $\text{pH} = 3.0$ ) conditions, with a significant reduction in the degradation activity under neutral ( $\text{pH} = 7.0$ ) conditions, and almost complete suppression of degradation activity under alkaline ( $\text{pH} = 10.0$ ) conditions. For the pure  $\text{In}_2\text{O}_3$  photocatalyst, the pH of the

degradation solution has a greater impact on the degradation activity of PFOA, exhibits degradation activity towards PFOA only under acidic conditions ( $\text{pH} = 3.0$ ), and the photocatalytic activity is severely suppressed under neutral ( $\text{pH} = 7.0$ ) and alkaline ( $\text{pH} = 10.0$ ) conditions. To demonstrate the applicability of the heterojunction in a wider pH range,  $\text{HNO}_3$  and  $\text{NaOH}$  solutions are utilized to adjust the pH of the degradation solution. The zeta potential of pure  $\text{BiOCl}$  and 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  is measured within the pH range of 1.00–11.00. As shown in Fig. 9(B), it can be observed that the zeta potential of pure  $\text{BiOCl}$  and 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  varies at different pH values, but the overall trend in the potential change is consistent between these two materials. However, the zero point of the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  photocatalyst is 6.25. This is lower than the zero point of pure  $\text{BiOCl}$  (7.60), and inconsistent with the result shown in Fig. 9(A). To explain this phenomenon, the pH is measured during the PFOA degradation process. As shown in Fig. 9(C), it can be observed that the pH of the PFOA solution gradually decreases during the degradation process. Furthermore, the pH of the degradation solution decreases faster in the alkaline environment. This might be because  $\text{OH}^-$  in the degradation solution is oxidized to form  $\cdot\text{OH}$  by hole, and there are more  $\text{OH}^-$  in the alkaline environment, which is more easily oxidized, thus resulting in a faster decrease in pH of the degradation solution. The comparison of different photocatalysts revealed that the pH of the solution in the heterojunction decreases the fastest, while the pH of the pure  $\text{In}_2\text{O}_3$  decreases the slowest. This suggests that the heterojunction photocatalyst exhibits the highest light utilization efficiency and the strongest photocatalytic activity. Based on Fig. 9(A), the degradation of PFOA by the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction photocatalyst begins after irradiating for 20 min when the pH value is 10.0. This is because in the first 20 min of irradiation, the pH of the solution is greater than 7.0. Negative charges accumulate on the surface of the catalyst under this condition, making it difficult for the carboxyl groups to be adsorbed with the negative charges at the end of PFOA. When the irradiation time reaches 30 min and the pH value is 6.0, the catalyst surface carries positive charges, allowing them to effectively adsorb PFOA with a negatively charged carboxyl group at the end, resulting in its degradation. However, under the same conditions,  $\text{BiOCl}$  cannot degrade PFOA until the pH of the degradation solution is lower than 7.0. This may be because the recombination of  $\text{BiOCl}$ 's photogenerated electron-hole pairs is too fast, resulting in a low utilization efficiency of light, so the degradation of PFOA requires a lower pH environment.

To investigate the applicability of  $\text{In}_2\text{O}_3/\text{BiOCl}$  in real environments, the effect of common anions ( $1 \text{ mM Cl}^-$ ,  $\text{CO}_3^{2-}$ ,  $\text{NO}_3^-$ ,  $\text{SO}_4^{2-}$ , etc.) on the photocatalytic degradation of PFOA in water was examined. As shown in Fig. 9(D), all anions exhibit inhibitory effects on PFOA degradation. The weakest inhibitory effect is observed for  $\text{Cl}^-$  and  $\text{F}^-$ , while  $\text{SO}_4^{2-}$  showed a relatively strong inhibitory ability. The inhibition of PFOA degradation by all three anions can be understood, as these anions occupy part of the active sites and inhibit the degradation process by competing with PFOA for photoinduced holes. The inhibition of the PFOA degradation by  $\text{NO}_3^-$  is attributed to its



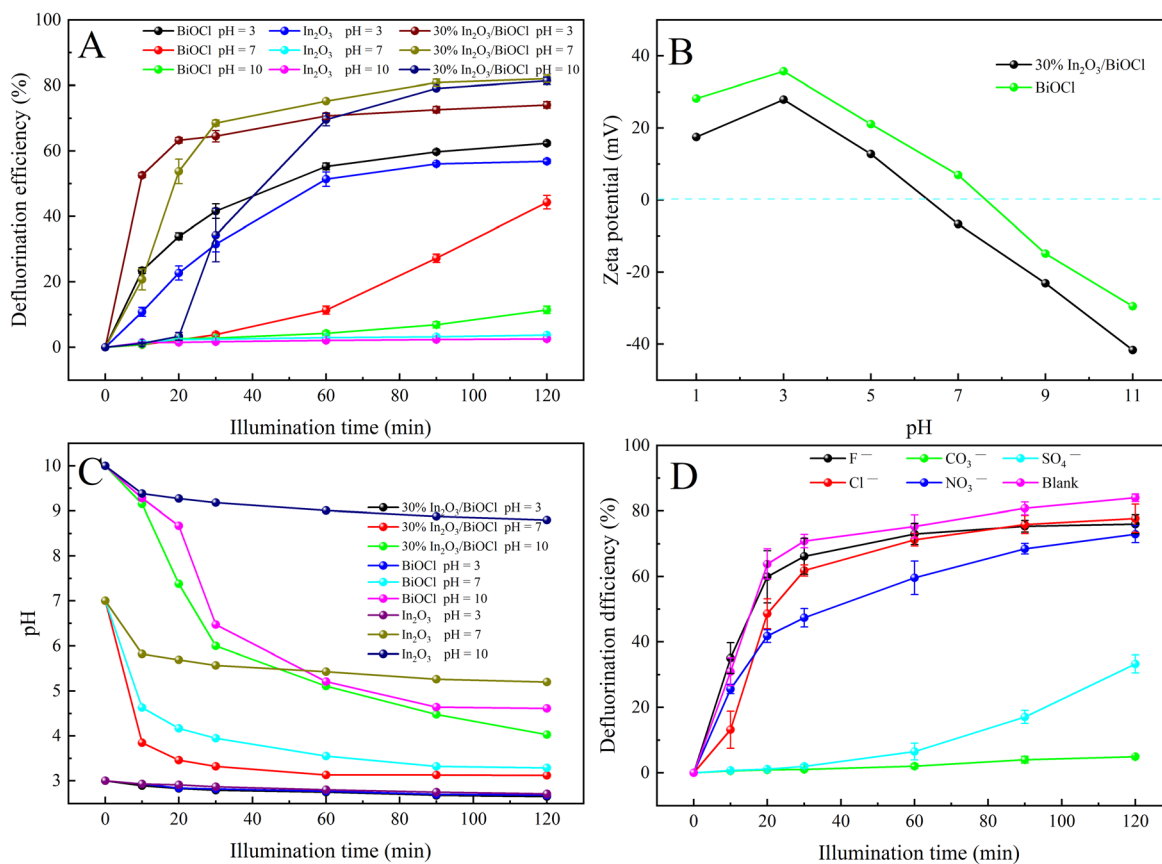


Fig. 9 Comparison of PFOA defluorination by different photocatalysts. (A) The influence of various photocatalysts on the defluorination rate under different acidic conditions. (B) Zeta potential at pH 1.00–11.00. (C) pH variation during PFOA degradation with different photocatalysts under different initial pH conditions. (D) The impact of different anions on the defluorination rate.

ability to capture part of the electrons,<sup>59–61</sup> while  $\text{CO}_3^{2-}$  almost completely inhibits the degradation of PFOA. This may be attributed to  $\text{CO}_3^{2-}$  having a carboxyl group and small molecular size, which can almost completely occupy these active sites that the carboxyl end of PFOA can bind on the surface of the catalyst, resulting in ineffective degradation for PFOA. This indirectly indicates that PFOA is connected to the catalyst through the carboxyl end of PFOA.

The stability of 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  for the photocatalytic degradation of PFOA was investigated, and the results are shown in Fig. 10. The results showed that even after the catalyst is used four times, the defluorination efficiency of PFOA still reaches 76.44%. Compared with the first use of a catalyst, the defluorination rate of PFO is only reduced by 7.00%, reaching 84.01%. At the same time, the defluorination rate is significantly increased during the first 10 min when 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  is reused, which may be related to the increase in the oxygen vacancies in part of  $\text{BiOCl}$  within the heterojunction under UV-light illumination, leading to a decrease in the recombination rate of the photogenerated electron–hole pairs.

### 3.3 Research on the degradation mechanism of PFOA

**3.3.1 Degradation mechanism of PFOA.** To investigate the photodegradation mechanism of PFOA by the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$

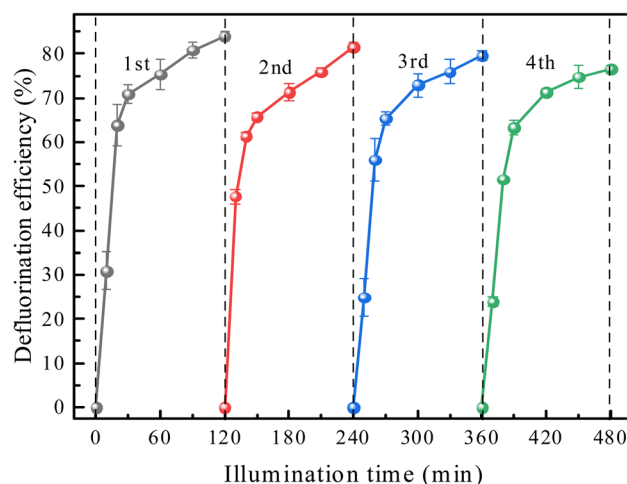


Fig. 10 Effect of the reuse of 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  on PFOA defluorination.

heterojunction, the active species were studied using electron spin resonance (ESR) with 5,5-dimethyl-1-pyrroline-*N*-oxide (DMPO) as a spin trap agent. As shown in Fig. 11(A) and (B), there is almost no ESR signal observed for  $\text{BiOCl}$  and 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  under dark conditions. However, the four-line



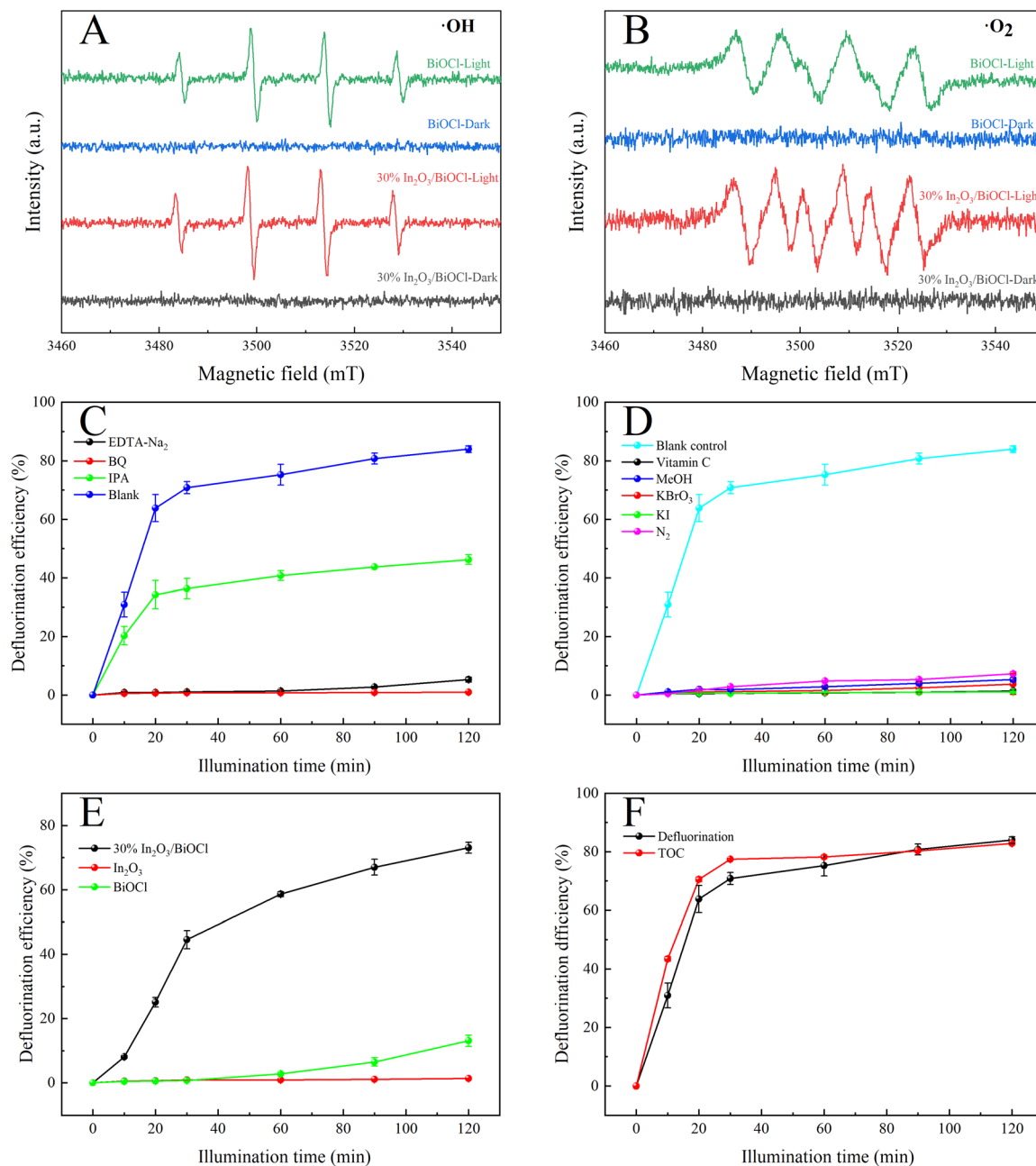


Fig. 11 (A and B) ESR spectra of  $\cdot\text{OH}$  and  $\cdot\text{O}_2^-$  of BiOCl and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl. (C) Free radical capture experiment. (D) Control experiment of  $\cdot\text{O}_2^-$  inhibition and  $\text{h}^+$  generation. (E) Degradation efficiency of different photocatalysts on PFOA under a 360 nm filter. (F) TOC removal rate of PFOA.

characteristic ESR signal of the DMPO- $\cdot\text{OH}$  and DMPO- $\cdot\text{O}_2^-$  spin adducts is observed under simulated solar light irradiation, indicating that both catalytic systems can generate  $\cdot\text{OH}$  and  $\cdot\text{O}_2^-$ . Furthermore, all ESR signals produced by the 30% In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction are significantly stronger than those produced by BiOCl, which indicates that more active species can be generated in a 30% In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction photocatalytic system. To explore the main active substances in the degradation process of PFOA, various scavengers are added to the degradation reaction to study their roles in photocatalysis. Among them, 1 mM EDTA-Na<sub>2</sub> is used as a hole ( $\text{h}^+$ )

scavenger, 1 mM IPA is used as a hydroxyl radical ( $\cdot\text{OH}$ ) scavenger, and 1 mM BQ is used as a scavenger of superoxide radicals ( $\cdot\text{O}_2^-$ ). From Fig. 11(C), it can be seen that when EDTA-Na<sub>2</sub> and BQ are added as scavengers, the defluorination rate of PFOA decreases significantly under the same conditions from 84.01% without any scavenger to 5.23% and 0.95%, respectively, indicating a significant reduction in the defluorination rate and nearly complete inhibition of the PFOA degradation. This suggests that  $\text{h}^+$  and  $\cdot\text{O}_2^-$  play a major role in the photocatalytic degradation of PFOA. When IPA is introduced as a capture agent under identical experimental conditions, the defluorination

efficiency only decreases to 46.23%, indicating that  $\cdot\text{OH}$  only plays a supporting role in the PFOA defluorination process. However, in a photocatalytic system, even though  $\cdot\text{O}_2^-$  can be produced through an electronic reduction pathway, the oxidation ability of  $\cdot\text{O}_2^-$  is too weak to decompose the PFOA molecules.<sup>45</sup> Therefore, it can be inferred that the defluorination of PFOA occurs under the joint action of  $\text{h}^+$  and  $\cdot\text{O}_2^-$ .

Given the influence of substances (such as quinones) on the color of the solution, their presence may obstruct light and thus impact the degradation of PFOA. To investigate this phenomenon,  $\cdot\text{O}_2^-$  scavenger (1 mM ascorbic acid) is selected and utilized to eliminate  $\cdot\text{O}_2^-$ , as shown in Fig. 11(D). In addition, by adding 2.5 mM  $\text{KBrO}_3$  to capture electrons and indirectly suppress the formation of  $\cdot\text{O}_2^-$ , the control experiments are conducted under an anaerobic  $\text{N}_2$  environment. The results demonstrate significant inhibition of PFOA degradation in all scenarios. The impact of the hollow structure on PFOA degradation is further confirmed through the addition of 1 mM KI and 1 mM MeOH. Fig. 11(E) shows the degradation efficiency of three different materials towards PFOA under UV light above 360 nm. Compared with Fig. 7(B), it can be observed that under irradiation with light at wavelengths above 360 nm, the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction still achieves a defluorination efficiency exceeding 70%, while the degradation efficiency of  $\text{BiOCl}$  is significantly inhibited. In particular, the degradation efficiency of  $\text{In}_2\text{O}_3$  is completely inhibited. This indicates that under light irradiation above 360 nm, the holes generated by  $\text{In}_2\text{O}_3$  cannot degrade PFOA. Therefore, in the heterojunction, the degradation of PFOA occurs on the surface of the  $\text{BiOCl}$  component, and the holes generated by  $\text{In}_2\text{O}_3$  will transfer to the  $\text{BiOCl}$  component. The increase in the degradation efficiency is due to the improvement of the separation efficiency of photo-generated electron-hole pairs, effectively preventing their recombination, and is consistent with the FT-IR, EIS, and PL results.

The removal efficiency of the total organic carbon (TOC) of the PFOA solution was analyzed, and the mineralization rate was also calculated, which is of great importance for avoiding secondary pollution in wastewater treatment. As shown in Fig. 11(F), the removal efficiency of TOC increased with the increase in the irradiation time and reached 82.87%. At the

same time, after ultraviolet irradiation for 2 h, the defluorination rate reached 84.01%, which is consistent with the removal efficiency of TOC.

### 3.3.2 The separation efficiency of photo-generated electron-hole pairs

**3.3.2.1 UV-vis DRS and VB-XPS of the heterojunction.** UV-vis DRS was employed to reveal the optical properties of  $\text{BiOCl}$ . To compare the light absorption characteristics of  $\text{BiOCl}$ ,  $\text{In}_2\text{O}_3$ , and the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction, they were measured by UV-vis DRS (Fig. 12(A)).  $\text{In}_2\text{O}_3$  shows good absorption performance in the UV and visible light regions, and its absorption edge is 500 nm. Pure  $\text{BiOCl}$  only shows good light absorption ability in the UV region, with an absorption edge at 360 nm. The  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction demonstrated absorption in the visible light region as well, with an absorption edge at 470 nm. Compared to pure  $\text{BiOCl}$ , the  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction exhibits a significantly red-shifted absorption wavelength, which indicates that a broader light absorption range can increase the absorption intensity. The Tauc plot of  $\text{BiOCl}$  and  $\text{In}_2\text{O}_3$  is calculated and plotted based on the UV-vis DRS data, and the relationship curve between  $(\alpha h\nu)^{n/2}$  and  $h\nu$  is shown in Fig. 12(B). The bandgap width ( $E_g$ ) of the semiconductor can be determined according to its bandgap derivation formula:

$$(\alpha h\nu)^{n/2} = A(h\nu - E_g) \quad (1)$$

where  $\alpha$ ,  $h$ ,  $\nu$ ,  $A$ , and  $E_g$  are the absorption coefficient, Planck's constant, optical frequency, constant, and bandgap energy, respectively. For the bandgap derivation formula,  $n = 1$  in indirect bandgap semiconductors, while  $n = 4$  in direct bandgap semiconductors. This graph shows that the bandgap widths of  $\text{BiOCl}$  and  $\text{In}_2\text{O}_3$  are 3.29 eV and 3.18 eV, respectively. X-ray photoelectron spectroscopy (XPS) can provide information on the electronic structure of the solid material because it is related to the energy band structure of a solid. The valence bands (VB) of  $\text{BiOCl}$  and  $\text{In}_2\text{O}_3$  photocatalysts are determined by VB-XPS, as shown in Fig. 12(C). The VB edges of  $\text{BiOCl}$  and  $\text{In}_2\text{O}_3$  are confirmed to be 2.23 and 2.20 eV, respectively. The conduction band position can be estimated according to eqn (2):

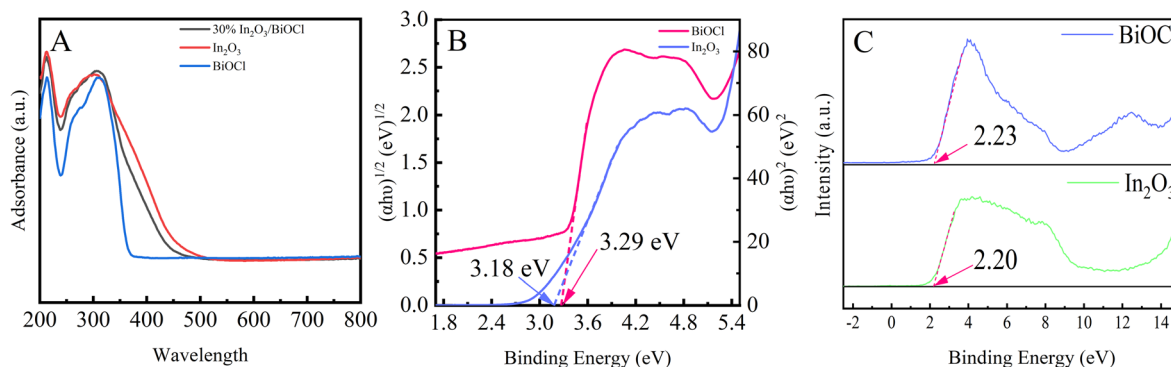


Fig. 12 (A) UV-vis DRS spectra of ( $\text{BiOCl}$ ,  $\text{In}_2\text{O}_3$ , and 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$ ); (B)  $(\alpha h\nu)^{n/2}$  vs. photon energy ( $h\nu$ ) diagrams of ( $\text{BiOCl}$ ,  $\text{In}_2\text{O}_3$ ); (C) VB-XPS diagrams of ( $\text{BiOCl}$ ,  $\text{In}_2\text{O}_3$ ).



$$E_{CB} = E_{VB} - E_g \quad (2)$$

The respective conduction band minima of BiOCl and In<sub>2</sub>O<sub>3</sub> are found to be approximately  $-1.06$  and  $-0.98$  eV.

It is widely believed that p-n heterojunctions can accelerate the separation of photogenerated electron-hole pairs. In the BiOCl@In<sub>2</sub>O<sub>3</sub> p-n heterojunction, the flow and transfer of electrons can occur at the coupled interface of two semiconductors (Fig. 13). The Fermi energy levels of BiOCl (p-type) and In<sub>2</sub>O<sub>3</sub> (n-type) are located near VB and CB, respectively. When the interface between the semiconductor materials contacts, the Fermi energy levels of BiOCl (p-type) and In<sub>2</sub>O<sub>3</sub> (n-type) move upward and downward, respectively, until the Fermi energy level reaches equilibrium, thus establishing an internal electric field. When the BiOCl@In<sub>2</sub>O<sub>3</sub> p-n heterojunction is exposed to light, photogenerated electrons on the BiOCl conduction band will be transferred to the In<sub>2</sub>O<sub>3</sub> conduction band, while holes will remain on the VB of BiOCl, thereby effectively separating the photogenerated electron-hole pairs.

**3.3.2.2 Electrochemical properties and PL spectra of the heterojunction.** To verify the aforementioned assumption, the transient photocurrent intensity ( $I-t$ ), electrochemical impedance spectroscopy (EIS), and photoluminescence spectroscopy (PL) of photocatalysts under simulated visible light irradiation were measured. Fig. 14(A) reflects the photocurrent intensity of these three materials. Generally speaking, the higher the photocurrent response intensity, the higher the separation efficiency of the photo-generated electron-hole pairs.<sup>62</sup> The photogenerated current intensity of 30% In<sub>2</sub>O<sub>3</sub>/BiOCl is the highest, as indicated in the graph, demonstrating that the formation of the heterojunction effectively enhances the separation efficiency of the photo-generated electron-hole pairs.

Conversely, the pure BiOCl material exhibits the lowest photo-generated current intensity, which may be attributed to its wide bandgap that cannot be excited by visible light. This is consistent with the UV-vis diffuse reflectance spectral results. Additionally, all samples have similar trends in the EIS signals. Generally speaking, the smaller the arc radius of the EIS Nyquist plot, the higher the separation efficiency of the photogenerated charge carriers, and the higher the photocatalytic activity.<sup>63,64</sup> As shown in Fig. 14(B), the EIS Nyquist plot of the 30% In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction photocatalyst exhibits the smallest arc radius, indicating that 30% In<sub>2</sub>O<sub>3</sub>/BiOCl possesses the highest efficiency for the separation of photogenerated electron-hole pairs. However, in Fig. 14(A) and (B), the test results of In<sub>2</sub>O<sub>3</sub> and BiOCl show the opposite trend. This discrepancy may be attributed to the larger specific surface area of In<sub>2</sub>O<sub>3</sub>, which can generate more photogenerated carriers and consequently result in a higher transient photocurrent response. Additionally, the larger specific surface area might increase the path length of charge transfer, leading to higher charge transfer resistance. As displayed in Fig. 14(C), the fluorescence spectra of BiOCl, In<sub>2</sub>O<sub>3</sub> (n-type), and 30% In<sub>2</sub>O<sub>3</sub>/BiOCl were analyzed under the excitation wavelength of 350 nm. All three kinds of materials show emission intensity peaks in the wavelength range between 350–400 nm, which can be attributed to a near-band edge (NBE) UV emission peak resulting from excitonic recombination. Among these materials, the fluorescence intensity of the 30% In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction is the lowest, suggesting that the rate of the photogenerated electron-hole pair recombination is the slowest for 30% In<sub>2</sub>O<sub>3</sub>/BiOCl. This result is consistent with the results of  $I-t$  and EIS, which demonstrate that the construction of the 30% In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction effectively inhibits the recombination of the photogenerated electron-hole pairs. The peak located near 550–750 nm may be the deep-level (DL) visible

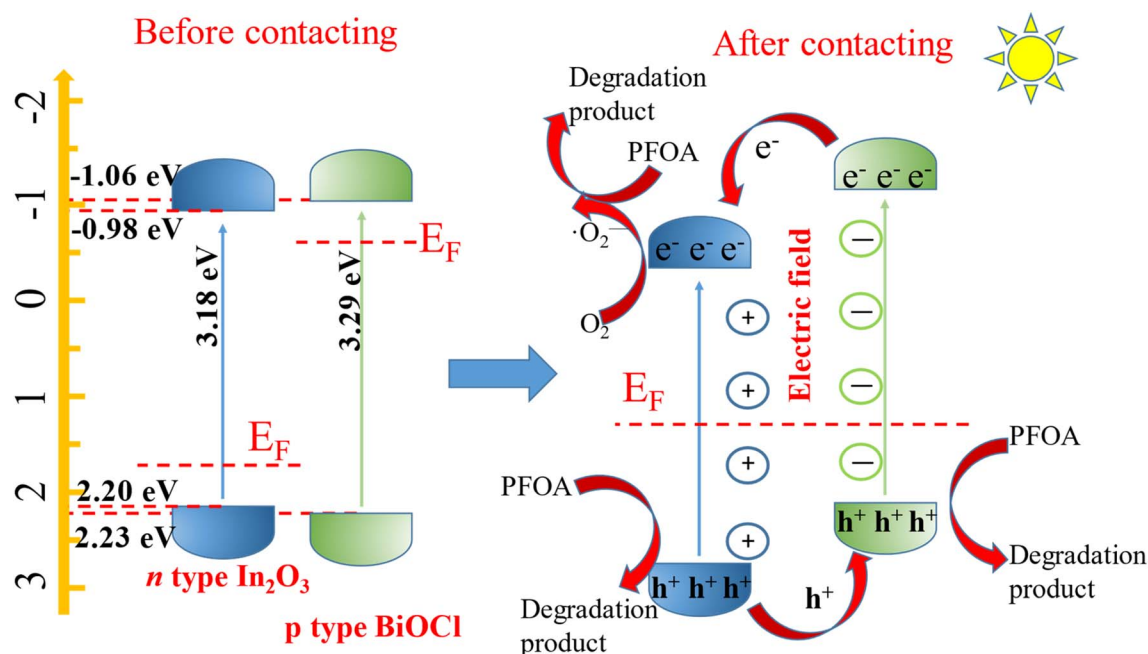


Fig. 13 Banded structure of the In<sub>2</sub>O<sub>3</sub>/BiOCl heterojunction.



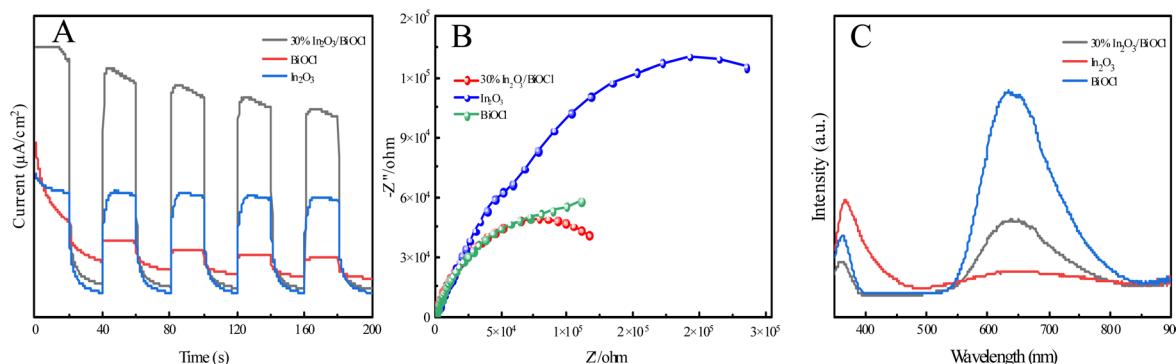


Fig. 14 (A)  $I-t$  spectra of (BiOCl,  $\text{In}_2\text{O}_3$ , and 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$ ); (B) EIS diagrams of (BiOCl,  $\text{In}_2\text{O}_3$ , 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$ ); (C) PL spectra of (BiOCl,  $\text{In}_2\text{O}_3$ , 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$ ).

luminescence peak related to structural defects and impurities.<sup>65–67</sup> It can be observed that the fluorescence intensity of the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction is relatively weak compared to that of BiOCl, which also confirms that the effective construction of the 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  heterojunction suppresses the recombination of the photo-generated electron-hole pairs.

**3.3.3 Detection of intermediate products in PFOA and analysis of the degradation pathways.** High-performance liquid chromatography/quadrupole time-of-flight mass spectrometry (HPLC/QTOF/MS) was employed to analyze and detect the intermediate products of PFOA degradation. The initial concentration of PFOA was controlled at  $20 \text{ mg L}^{-1}$ , with a degradation solution pH of 4.00 and catalyst dosage of  $0.2 \text{ g L}^{-1}$ . Sampling was conducted for 10 min and 2 h, respectively. The peak-to-peak voltage of 22 kV was utilized to identify the intermediate products using HPLC-QTOF/MS, with molecular weights ranging from 100 to 450. The total ion chromatogram (TIC) is shown in Fig. 15. By selecting the intermediate product peaks with retention times of 0.85, 1.40, 3.10, 4.19, 4.81, 5.28, 5.66, and 6.25 min (other retained peaks may be impurities), it can be seen from the total ion chromatogram of the intermediate products that with the continuous increase in irradiation time from 10 min to 2 h, the intensity and peak area of the intermediate product peaks with elution times of 0.85, 1.40, and 3.10 min have significantly increased, while the intermediate product peaks with elution times of 4.81, 5.28, and 5.66 min have significantly decreased and nearly disappeared. This indicates that molecular ions with elution times of 4.81, 5.28, and 5.66 min are almost completely degraded during the degradation process.

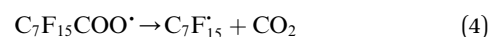
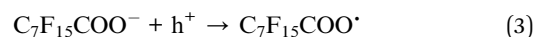
Analysis of the elution peaks on the total ion chromatogram was conducted. The mass spectrometry results are shown in Table 5, where the main chemical substances are 7 kinds of perfluorocarboxylic acids in  $A_1$ , the degradation intermediates in  $A_2$  and  $A_3$ , and the substances with  $m/z$  ratios of 141, 361, 217, and 285 in  $A_4$  to  $A_7$ . The other  $m/z$  ratios in  $A_4$  to  $A_7$  correspond to substances with the same main characteristic peaks, but differ by adding or reducing one  $\text{CF}_2$  unit.  $A_8$  and  $A_9$  show low peak intensity in the mass spectrometry of each elution peak. However, evidence of possible substances can be found in

multiple peaks, and their low intensity can be attributed to low molecular concentration. The mass peaks with  $m/z$  ratios of 113, 163, 213, 263, 313, 363, and 413 in the mass spectrum correspond to elution times of 0.85, 1.40, 3.10, 4.19, 4.81, 5.28, and 5.66 min, respectively. Combined with Fig. 15, it can be seen that after an irradiation time of 2 h, elution peaks with elution times of 4.81, 5.28, and 5.66 min almost disappear, indicating that PFOA in the solution is almost completely degraded. Both perfluoroheptanoic acid (PFHpA) and perfluorohexanoic acid (PFHxA), which are degradation intermediates, also disappear, indicating that the heterojunction material 30%  $\text{In}_2\text{O}_3/\text{BiOCl}$  exhibits excellent performance during the degradation and defluorination of PFOA.

Based on the experimental and characterization analysis results, three kinds of degradation pathways of PFOA are proposed:

(1) The main intermediate product is  $\text{C}_n\text{F}_{2n+1}^*$ .

Route 1: due to the experimental evidence of free radical capture,  $\cdot\text{OH}$  only plays an auxiliary role during the degradation of PFOA, so there should be only one path for generating  $\text{C}_7\text{F}_{15}^*$ , the reason is that the electrons on the carboxyl end of PFOA adsorbed on the surface of the photocatalyst are captured by  $\text{h}^+$  on the heterogeneous junction surface under light irradiation conditions, generating  $\text{C}_7\text{F}_{15}\text{COO}^*$  (eqn (3)), and then the Photo-Kolbe reaction occurs to remove the carboxyl groups and produce the free radical  $\text{C}_7\text{F}_{15}^*$  (eqn (4)).<sup>68</sup>



In the further degradation of  $\text{C}_7\text{F}_{15}^*$ , three reaction pathways have been proposed by scholars. This includes hydrolysis with  $\text{H}_2\text{O}$ , resulting in the production of  $\text{C}_7\text{F}_{15}\text{OH}$ , attacked by  $\cdot\text{OH}$ , resulting in the formation of  $\text{C}_7\text{F}_{15}\text{OH}$ , and reaction with  $\text{O}_2$  to generate  $\text{C}_7\text{F}_{15}\text{O}_2^*$ . However, considering previous research that PFOA cannot be defluorinated in a nitrogen atmosphere, these two pathways for  $\text{C}_7\text{F}_{15}^*$  defluorination through hydrolysis by water and attack by  $\cdot\text{OH}$  are excluded. Therefore,  $\text{C}_7\text{F}_{15}^*$  can only react with  $\text{O}_2$ , resulting in the production of the perfluoroperoxyl radical  $\text{C}_7\text{F}_{15}\text{OO}^*$  (eqn (5)), and the subsequent



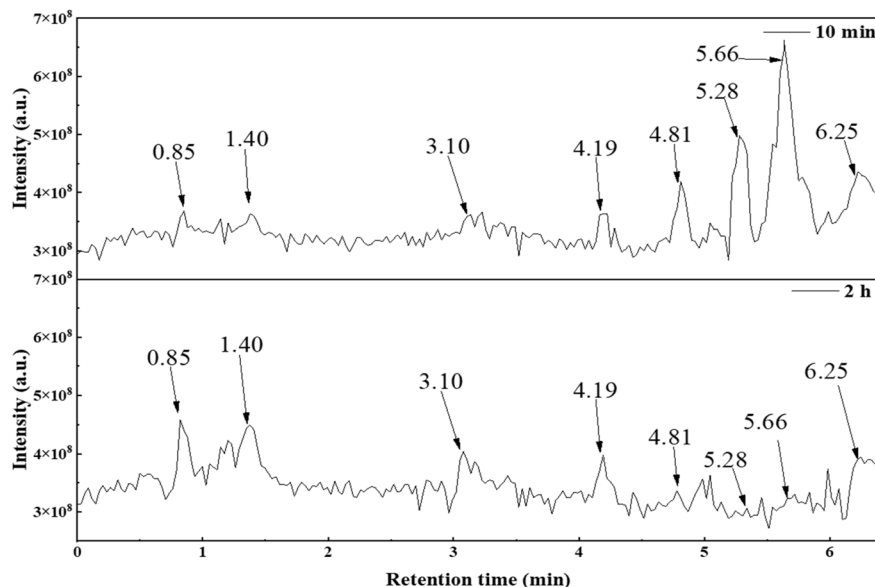
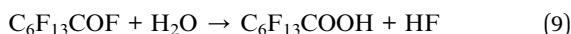
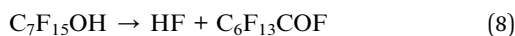
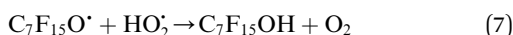
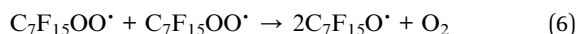


Fig. 15 Total ion flow diagram (TIC) of the degradation products of PFOA for different degradation times.

combination of two  $C_7F_{15}OO\cdot$  molecules to generate oxygen and two kinds of perfluoroalkoxy radicals  $C_7F_{15}O\cdot$  and  $O_2$  (eqn (6)).<sup>69</sup> However, the generated perfluoroalkoxy free radicals can easily react with hydrogen peroxide radicals ( $HO_2\cdot$ ) to form unstable alcohols (eqn (7)), which can easily lose one HF moiety to form  $C_6F_{13}COF$  (eqn (8)).  $C_6F_{13}COF$  is unstable and easily hydrolyzes to form HF and  $C_6F_{13}COOH$  (eqn (9)).

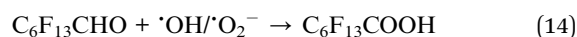
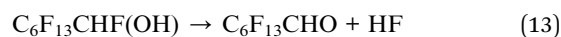
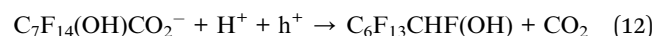
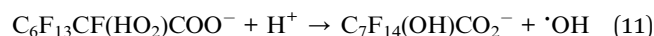
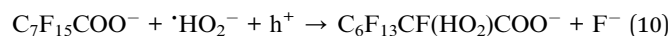


(2) The main intermediate product is  $C_nF_{2n+1}CO$ .

Route 2: in mass spectrometry analysis, several substances represented by  $A_3$  are peaks with the highest relative abundance, indicating that they are probably the main intermediates during the degradation of PFOA. As shown in Table 5, the terminal functional group of substances represented by  $A_3$  is  $C=O$ . In order to confirm the origin of the  $C=O$  functional group, ion searching was conducted on the total ion chromatograms (TIC) of samples for 10 min and 2 h. It was found that no ion peak with a ratio of mass to charge 397 is detected, which indicates that the  $C=O$  functional group in intermediate  $A_3$  during degradation is not formed by direct dehydroxylation of the carboxyl group at the end of perfluorocarboxylic acid, but by  $\alpha$ -C defluorination.

Evidence of free radical capture experiments suggests that both  $\cdot O_2^-$  and  $h^+$  play a major role during the degradation of PFOA, in addition to its oxidation capacity.  $\cdot O_2^-$  is a kind of

weakly reducing substance, nucleophilic free radicals that can easily attack low electron density areas in molecules.<sup>70</sup> Therefore, holes on the surface of the photocatalyst can be seen as electron-withdrawing groups. Under the action of holes, the electron cloud on the alpha carbon moves towards the carboxyl groups, while the electron density on the alpha carbon decreases, making it susceptible to being attacked by nucleophilic free radicals such as  $\cdot O_2^-$ . This leads to a nucleophilic substitution ( $S_N2$ ) reaction.<sup>71,72</sup> The specific process involves the pairing of electrons on  $\cdot O_2^-$  with electrons on  $C_7F_{15}CO_2^-$ , followed by electron transference on  $C_7F_{14}CO_2^-$  to F atoms attached, resulting in the cleavage of the C-F bond. Additionally,  $H^+$  provided by the solution leads to intermediates converting into  $C_6F_{13}CF(HO_2)COO^-$  (eqn (10)).<sup>72</sup> Then, hydrogen peroxide decomposes, and the solution provides another  $H^+$  to generate  $\cdot OH$  and  $C_7F_{14}(OH)CO_2^-$  (eqn (11)). This is one of the reasons why PFOA is more easily degraded under acidic conditions. Then, the end of the carboxyl group is removed to form the unstable  $C_6F_{13}CHF(OH)$  (eqn (12)), which easily loses one HF to generate  $C_6F_{13}CHO$  (eqn (13)). Finally, it is oxidized by  $\cdot OH$  and  $\cdot O_2^-$  to form the corresponding carboxylic acid,  $C_6F_{13}COOH$  (eqn (14)).



Route 3: the generated  $C_6F_{13}CFO_2HCOO^-$  directly eliminates HF to form perfluorooctanoic acid ( $C_6F_{13}COCO_2H$ , eqn (15)),<sup>73</sup>

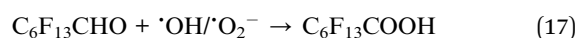
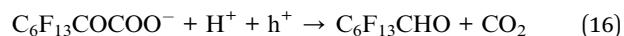


Table 5 Determination of intermediates formed at different reaction times using LC/MS

Possible substances	$m/z$ ( $[M + H]^-$ )	Molecular formula	Molecular structural formula
A <sub>1</sub>	413, 363, 313, 263, 213, 163, 113	$C_nF_{2n+1}COOH$	
A <sub>2</sub>	369, 319, 269, 219, 169 <sup>a</sup> , 119	$C_nF_{2n+1}$	
A <sub>3</sub>	347 <sup>a</sup> , 297 <sup>a</sup> , 247 <sup>a</sup> , 197 <sup>a</sup>	$C_nF_{2n+1}CO$	
A <sub>4</sub>	391, 341, 141 <sup>a</sup>	$C_nF_{2n+1}C_2O_3$	
A <sub>5</sub>	361, 311	$C_nF_{2n+1}C_2FO_3H$	
A <sub>6</sub>	367, 217 <sup>a</sup>	$C_nF_{2n+1}CFOH$	
A <sub>7</sub>	335, 285, 235, 185	$C_nF_{2n+1}O$	
A <sub>8</sub>	401, 301, 201, 151	$C_nF_{2n+1}O_2$	
A <sub>9</sub>	409, 359, 309, 259, 209, 109	$C_nF_{2n+1}C_2O_4H_2$	

<sup>a</sup> Peaks of the base ion in each elution time are indicated.

which further loses the carboxyl group at the end to produce perfluorooctanal ( $C_6F_{13}CHO$ , eqn (16)). Eventually, it is oxidized by  $\cdot OH$  and  $\cdot O_2^-$  to form the corresponding carboxylic acids ( $C_6F_{13}COOH$ , eqn (17)).



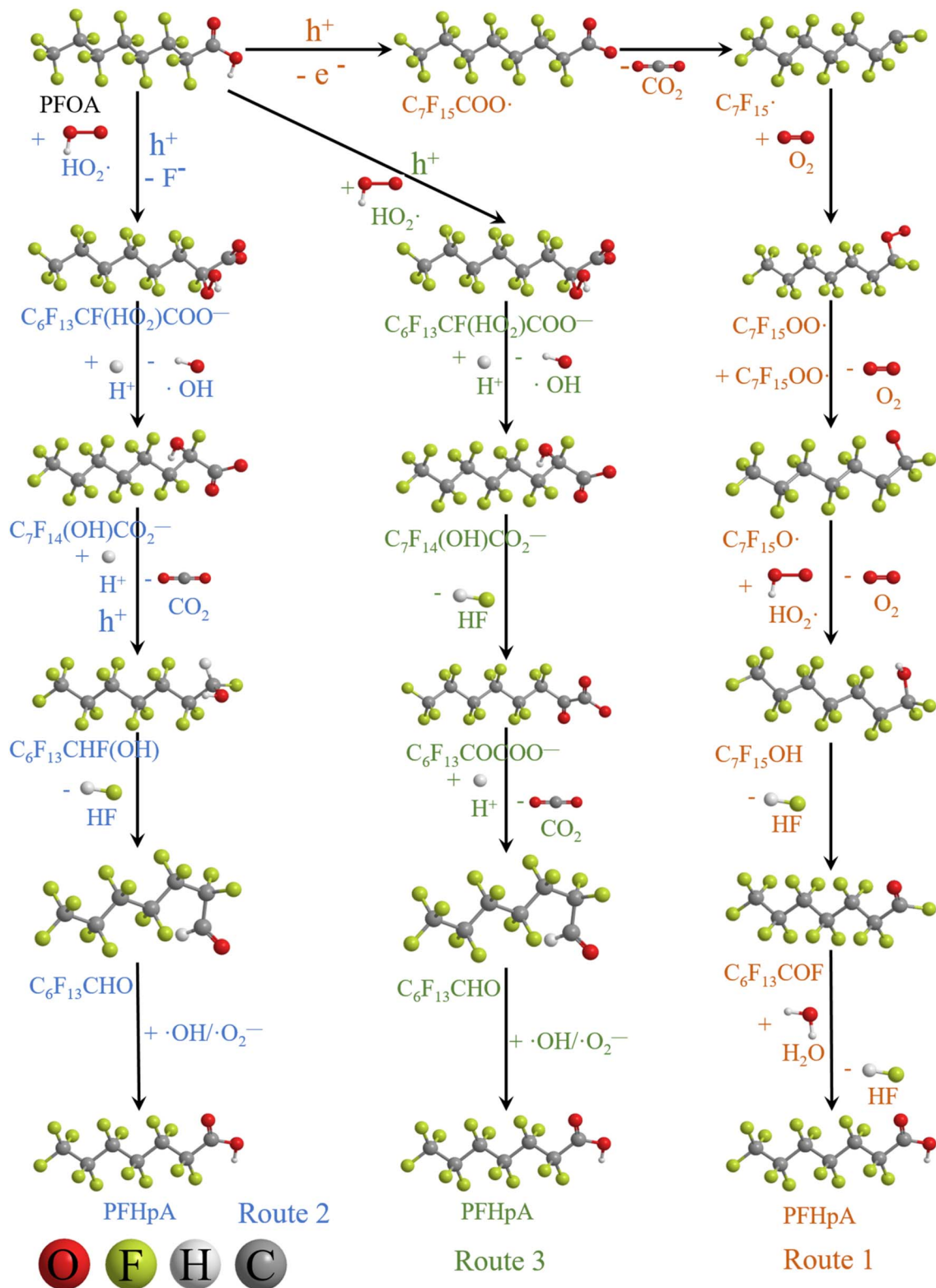


Fig. 16 Possible paths of PFOA degradation.

During the photocatalytic degradation of PFOA by the  $In_2O_3/BiOCl$  heterojunction, the defluorination process is mainly driven by  $\cdot O_2^-$  and  $h^+$ , with  $\cdot OH$  playing a secondary role. Based on these intermediates that are produced, the degradation pathway of

PFOA can be divided into three routes (as shown in Fig. 16): route 1, proton ( $H^+$ ) abstraction from perfluorooctanoic acid (PFOA) leads to the formation of  $C_7F_{15}COO\cdot$ , which subsequently undergoes the Photo-Kolbe decarboxylation reaction to generate



$C_7F_{15}^{\cdot}$ , a perfluoroalkyl radical. The radical reacts with molecular oxygen ( $O_2$ ) through a series of oxidative reactions to produce perfluoroheptanoic acid ( $C_6F_{13}COOH$ ). In route 2, under the assistance of  $h^+$ ,  $^{\cdot}O_2^-$  undergoes nucleophilic substitution ( $S_N2$ ) on the  $\alpha$ -C of PFOA, causing the cleavage of one  $F^-$  on  $\alpha$ -C. This reaction is followed by the Photo-Kolbe reaction, which results in decarboxylation and the formation of  $C_6F_{13}CHF(OH)$ . After dehydration, the corresponding fully fluorinated heptaldehyde,  $C_6F_{13}CHO$ , is produced. Finally, under the activity of  $^{\cdot}OH$  and  $^{\cdot}O_2^-$ , heptaldehyde is oxidized to the corresponding perfluorocarboxylic acid,  $C_6F_{13}COOH$ . In route 3, based on the replacement of the second pathway *via* the generation of  $C_6F_{13}CFO_2HCOO^-$  by  $F^-$ , followed by substitution of another  $F^-$ , the corresponding perfluorooctanoic acid  $C_6F_{13}COCO_2H$  is produced after dehydration, and then it is decarboxylated by Photo-Kolbe reaction to form the corresponding perfluorooctanal  $C_6F_{13}CHO$ . Finally, under the action of  $^{\cdot}OH$  and  $^{\cdot}O_2^-$ , it is oxidized to the corresponding carboxylic acid  $C_6F_{13}COOH$ .

## 4. Conclusion

In this study,  $In_2O_3$  was prepared from indium nitrate and the  $In_2O_3/BiOCl$  p-n heterojunction was synthesized by combining it and  $BiOCl$ . The preparation process and photodegradation process of  $In_2O_3/BiOCl$  were investigated using the defluorination efficiency of PFOA under UV illumination as a performance indicator. The results showed that when the prepared  $In_2O_3/BiOCl$  p-n heterojunction was excited under illumination, the photogenerated electrons on the conduction band of  $BiOCl$  would transfer to the CB of  $In_2O_3$ , while holes would still remain on the VB of  $BiOCl$ , resulting in effective separation of photo-generated electron-hole pairs, thereby enhancing its catalytic activity. Moreover, the prepared heterojunction exhibits less sensitivity to pH and demonstrates excellent degradation activity for PFOA in the wider range of acidic and alkaline environments (up to  $pH \leq 10$ ).

The photocatalyst that was prepared under the condition of  $m(In_2O_3) : m(BiOCl) = 3 : 7$  and calcined at  $300\text{ }^{\circ}C$  exhibits the highest efficiency in PFOA defluorination. At a catalyst dosage of  $0.2\text{ g L}^{-1}$ , degradation solution pH value of 5.00, and PFOA concentration of  $20\text{ mg L}^{-1}$ , the defluorination rate of PFOA reached 84.01%. Even after the catalyst was used four times, the defluorination efficiency of PFOA still exceeded 76.44%, which demonstrated its excellent stability.

In the photodegradation process of PFOA by the  $In_2O_3/BiOCl$  p-n heterojunction,  $h^+$  and  $^{\cdot}O_2^-$  play a primary role, while  $^{\cdot}OH$  plays a minor role in the defluorination process of PFOA. The degradation of PFOA is aided by these two components of  $In_2O_3$  and  $BiOCl$  in the heterojunction. PFOA molecules are adsorbed on  $BiOCl$  with plentiful oxygen vacancies and then gradually lose  $CF_2$  units under the action of  $^{\cdot}O_2^-$  produced by the CB reduction of  $In_2O_3$ , and are ultimately degraded into  $H_2O$  and  $CO_2$ .

## Data availability

The data supporting this article have been included as part of the ESI.†

## Conflicts of interest

There are no conflicts to declare.

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