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Association of Zn- and Mg-based chain transfer agents in coordinative chain transfer polymerizations of olefins for enhanced control and activity†

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Based on DFT-level computational studies, ZnEt₂ was implemented as a chain transfer agent (CTA) to promote the coordinative chain transfer (co)polymerization of ethylene for the first time with a metallocene complex of Nd. The use of ZnEt₂ in combination with Mg(⁷Bu)_{1.5}(⁷Oct)_{0.5} compared to the use of Mg(⁷Bu)_{1.5}(⁷Oct)_{0.5} alone, improves several key aspects of the polymerization process. When ethylene is polymerized, an increase of catalytic activities is observed and narrower molar mass distributions are obtained due to reduced β -H transfer and faster reversible chain transfer reactions. In copolymerization of ethylene with butadiene, the presence of ZnEt₂ has no impact on the polymerization process in terms of polymerization kinetics and microstructure of the final copolymer. Nevertheless, it acts as an excellent CTA. Using ZnEt₂ in combination with MesMgBr rather than Mg(⁷Bu)_{1.5}(⁷Oct)_{0.5} enables selective chain transfer between neodymium and zinc and promotes a nearly quantitative chain-end functionalization with acyl chloride.

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Introduction

Polyolefins represent the most significant family of polymers in the industry. They are produced in large volumes and at low cost through radical polymerization or coordination catalysis and serve a broad spectrum of applications. A long-standing challenge in this field has been achieving the control of the chain growth to allow the formation of more complex architectures such as block copolymers. Both radical and coordination

polymerizations can achieve this by utilizing systems leading to controlled and/or living polymerizations. For instance, recent advancements have applied reversible deactivation radical polymerizations and controlled coordination polymerizations to successfully control the polymerization of ethylene. Although not applied to the high-pressure and high-temperature gas-phase process used for producing low-density polyethylene (LDPE), recent studies have demonstrated that reversible deactivation radical polymerization of ethylene is achievable.^{1–4} Besides, since the early 1990s, the development of coordinative chain transfer polymerization (CCTP)^{5–8} has garnered increasing interest from both academia and industry. For example, Dow Chemical marketed olefin block copolymers (OBC) produced by this approach.⁹ CCTP is a polymerization catalysis based on a degenerative transfer mediated by an organometallic compound such as AlR₃, MgR₂, ZnR₂ that acts as a reversible chain transfer agent (CTA).¹⁰ Polymer chains grow on the catalyst and are reversibly transferred to the CTA, where they become intermittently dormant. In the absence of β -H elimination and with an excess of CTA relative to the catalyst, the polymerization process becomes controlled—meaning the number of polymer chains is fixed and directly proportional to the amount of CTA. As a result, the degree of polymerization is predictable based on the ratio of monomer consumed to the initial amount of CTA used. Since the chains

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produced by CCTP remain connected to a metal center throughout the polymerization, this method not only allows for the production of precision polyolefins,^{11–13} but also facilitates the introduction of functional groups at their chain ends¹⁴ and gives access to diverse macromolecular architectures.^{15–20} Interestingly, the CTA itself can be active under polymerization conditions. In the case of (co)polymerization of 1,3-dienes and styrene mediated by lanthanide borohydride complexes, it is possible to adjust the microstructure of the (co)polymers by regulating the amount of MgR_2 .^{21–23} In the same works, Zinck *et al.* have also shown the beneficial use of ternary systems based on the association of MgR_2 and AlR_3 to control the stereospecificity of 1,3-diene polymerization by CCTP.

Neodymium-based metallocenes enable coordinative chain transfer (co)polymerization (CCT(co)P) of ethylene and butadiene using MgR_2 as the CTA such as $Mg(^7Bu)_{1.5}(^7Oct)_{0.5}$ (BOMAG) (Scheme 1).^{24–26} The unique properties of MgR_2 in this CCTP process has been elucidated through a theoretical mechanistic study.²⁵ $ZnEt_2$ is commonly used in association with a large panel of olefin polymerization catalysts resulting from the combination of Fe-, Hf- or Zr-based complexes with borate activators or methylaluminoxane (MAO).^{7,8} In these systems, the underlying reaction mechanisms remain intricate. In addition, the group of Sita suggested that $ZnEt_2$ can mediate the chain transfer between the active catalyst and the second co-catalyst.¹³

In light of these results, developing more efficient and versatile conditions for Nd-based CCTP is of significant interest, especially when compared to those achieved with MgR_2 as a lone CTA. However, a major challenge in using $ZnEt_2$ as a CTA with Nd-based pre-catalysts is its inability to activate the Nd precursor.²⁷

In this communication, we circumvent this issue by combining $ZnEt_2$ and MgR_2 or $RMgX$ with $\{((Me_2Si(C_{13}H_8)_2)Nd(\mu-BH_4)(\mu-BH_4)Li(THF))_2\}$ Nd-based complex **1** (Scheme S1†). Building on our previous expertise with MgR_2 as an efficient CTA for the CCTP of ethylene and the CCT(co)P of ethylene and butadiene using a Nd-based catalyst,^{28–30} and supported

by preliminary DFT-level computational investigations, we evaluated the potential of $ZnEt_2$ as a CTA in MgR_2 -mediated CCTP systems. The resulting ternary Nd/Mg/Zn catalysts were then investigated for the polymerization of ethylene and its copolymerization with butadiene.

Results and discussion

Insights from molecular modelling

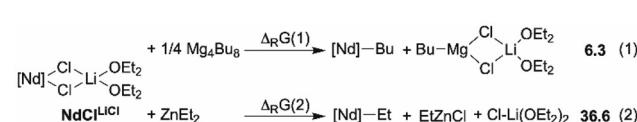
Before implementing the experimental design for the ternary catalytic system **1**/BOMAG/ $ZnEt_2$, we first obtained structural and mechanistic insights through DFT-level molecular modelling. This study presents several challenges, including the large size of the system (>100 atoms), the presence of three different metals, and multiple polymer chains. To address these challenges, we relied on our previous theoretical modelling strategies for speciation of heteropolymetallic complexes and the exploration of chain exchange reactions.^{25,31} To reduce computational costs, BOMAG was modelled using $Mg(^7Bu)_2$ clusters, with the rhombohedral tetramer being selected as the most stable configuration.²⁵ Regarding $ZnEt_2$, optimization of a dimer consistently leads to its dissociation into monomers. Since $ZnEt_2$ is purchased and used in a hydrocarbon solution, the most stable form present in this context is considered to be the monomer. The fully detailed computational method is described in the ESI.†

To validate the computational method, the thermodynamics of the formation of alkylated monometallic species $[Nd]-R$ ($R = ^7Bu$ or Et, $[Nd] = Me_2Si(C_{13}H_8)_2Nd$) from the Nd precursor $Me_2Si(C_{13}H_8)_2Nd(\mu-Cl)_2Li(OEt_2)_2$ ($NdCl^{LiCl}$) was computed for both Zn and Mg alkylating agent (Scheme 2). This precursor has been taken as both as model and analog of **1**. While the activation reaction of $NdCl^{LiCl}$ is endergonic by 6 kcal mol^{−1} in the case of $Mg(^7Bu)_2$, it is endergonic by 37 kcal mol^{−1} in the case of $ZnEt_2$. This is in line with experimental results for this specific system,²⁷ but also matches with the activation conditions reported for other polymerization catalytic systems.^{32,33}

As suggested in the literature and mentioned above, $ZnEt_2$ may mediate the chain transfer between the catalyst and a second CTA, namely AlR_3 .¹³ This mechanism hypothesis has been considered and will be compared to the chain transfer mechanism previously reported for the CCTP of ethylene mediated by BOMAG and $[Nd]-^7Bu$.²⁵ Of note, the latter revealed that the chain exchange reaction proceeds *via* a two-

Previous methodology, binary Nd / Mg CCT(co)P catalysts			
PE	$200 \text{ kg mol}^{-1} \text{ h}^{-1}$, $D 2.1$		
or			
PE	$220 \text{ kg mol}^{-1} \text{ h}^{-1}$, $D 1.4$		
This work, ternary Nd / Mg / Zn CCT(co)P catalysts			
PE	$9\,200 \text{ kg mol}^{-1} \text{ h}^{-1}$, $D 1.2$		
or			
PE	$230 \text{ kg mol}^{-1} \text{ h}^{-1}$, $D 1.4$		
or			

Scheme 1 Implementation of the CCTP of ethylene and CCTCoP of ethylene and butadiene mediated by binary or ternary Nd-based catalysts. $[Nd]$ corresponds to the metal center and its ligands ($Me_2Si(C_{13}H_8)_2$), $[Nd]X = \{((Me_2Si(C_{13}H_8)_2)Nd(\mu-BH_4)(\mu-BH_4)Li(THF))_2\}$.



Scheme 2 Thermodynamics ($\Delta_R G$, kcal mol^{−1}) of $[Nd]-R$ species formation ($R = ^7Bu$ or Et) as a function of the alkylating agent. $[Nd]$ corresponds to the metal center and its $Me_2Si(C_{13}H_8)_2$ ligand. Gaussian 09, B3PW91/D3BJ(SP), SMD(TolH), 298 K, 1 atm.

step association/dissociation transmetalation in which the intermediate heterotrimetallic complex $[\text{Nd}]-(\mu\text{-}^n\text{Bu})_2\text{Mg}_2\text{-}^n\text{Bu}_3$ (NdMg_2) is the resting state of the polymerization catalyst.²⁵

Considering now the addition of ZnEt_2 as a third component of the catalytic system, the speciation of thermodynamically accessible complexes has been performed. Relative to NdMg_2 and ZnEt_2 , a set of complexes can be formed with an endergonicity ranging from 1 to 10 kcal mol⁻¹ (Scheme 3). As a general trend, relative to separated NdMg_2 and ZnEt_2 , the formation of complexes in which zinc is the β position to neodymium is endergonic by at least 10 kcal mol⁻¹. Interestingly, the formation of the heterobimetallic dimer NdZn is almost as endergonic as the release of the NdBu complex from which monomer coordination-insertion mechanism takes place.²⁵

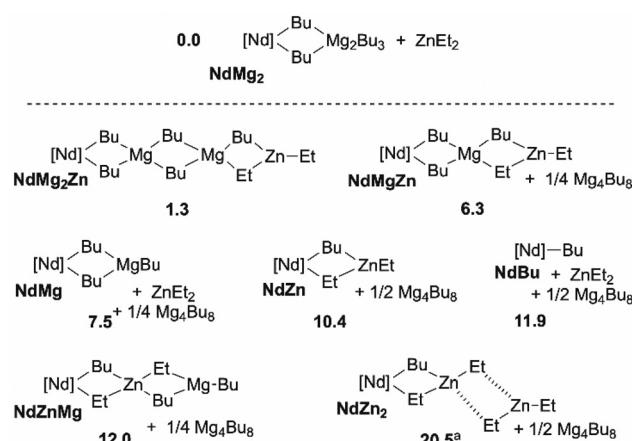
From a kinetic point of view, the Gibbs energy barrier for ethylene insertion in the Nd-C bond of the NdBu complex is computed to 10.7 kcal mol⁻¹. Concerning, the Nd/Mg binary system, in presence of Mg_4Bu_8 , the overall Gibbs energy barrier is raised to 22.6 kcal mol⁻¹ relative to NdMg_2 and ethylene due to the formation of the NdMg_2 dormant complex.²⁵ In the Nd/Mg/Zn ternary system, the presence of zinc leads to the formation of the bimetallic species NdZn as an intermediate that can become the most abundant Nd-based complex along with NdMg if ZnEt_2 is added in large excess relative to

BOMAG, the amount of NdMg_2 becoming small. NdZn and NdMg becoming the most abundant resting state of the catalyst, the overall Gibbs energy barrier for ethylene insertion is decreased from 22.6 kcal mol⁻¹ in a window ranging from 12.2 to 15.1 kcal mol⁻¹. Thereof, adding an excess of ZnEt_2 to the catalytic mixture would lead to a significant boost in catalytic activity. Regarding the influence on the chain transfer, we were unable to adequately converge the geometry of the transition states(s) as it relies on association/dissociation processes, coupled with re-orientation of the chain end carbanion doublet by rotations.^{25,26} However, an energy barrier of less than 5 kcal mol⁻¹ can be roughly estimated leading to an overall fast exchange between Nd and Zn, this barrier is thereof lower than the one computed between Nd and Mg by 8 kcal mol⁻¹,²⁵ thus enabling a much faster chain shuttling. Finally, as ZnR_2 and presumably $\text{Zn}(\text{polymer})_2$, do not aggregate, a more straightforward chain transfer between Nd and Zn may be inferred.

Polymerization of ethylene and copolymerization of ethylene with butadiene

Preliminary experimental observations. Molecular modelling highlights that though ZnEt_2 is not capable of alkylating the complex **1**, its addition in excess relative to MgR_2 would enhance both the catalytic activity and the chain transfer leading to a fastest polymerization producing chains with more narrowly distributed molar masses. Thereof, we compared ethylene polymerization mediated by **1**/BOMAG catalyst with that mediated by **1**/BOMAG/ ZnEt_2 ternary system, keeping the $[\text{CTA}]/[\text{Nd}]$ ratio constant (Table 1). 4 g of PE was targeted corresponding to a theoretical M_n of 2000 g mol⁻¹.

In a first blank experiment, ethylene was polymerized with the **1**/BOMAG catalyst ($[\text{Nd}]/[\text{Mg}] = 1/80$, run 1, Table 1). In agreement with our previous works,²⁵ the catalyst meets the requirement of CCTP but the chain exchange rate is low compared with the propagation rate as indicated by a dispersity value of 2.1. This has been attributed to a high-energy barrier for dissociation of the heterobimetallic species formed between the active species and BOMAG.²⁵ When the ternary system **1**/BOMAG/ ZnEt_2 ($[\text{Nd}]/[\text{Mg}]/[\text{Zn}] = 1/5/75$) was used (run 2, Table 1), complex **1** was first activated by BOMAG in a separate vial and the mixture was transferred in a solution containing ZnEt_2 before starting the polymerization. A strong decrease of D from 2.1 to 1.1 (Table 1 and Fig. 1) is observed and the content of vinyl-terminated chains resulting from β -H elimination drops from 10 to 2%.



Scheme 3 Speciation of the alkylated species yielded from $[\text{Nd}]\text{-}^n\text{Bu}$, $\text{Mg}_4\text{-}^n\text{Bu}_8$ and ZnEt_2 . Only the most stable species are shown, the fully detailed speciation is provided in ESI.† ΔG in kcal mol⁻¹. ^aIn NdZn_2 , interaction between the ZnEt_2 fragments is weak, the endergonicity results from the entropy cost of the association of free and separated ZnEt_2 . Gaussian 09, B3PW91/D3BJ(SP), SMD(TolH), 298 K, 1 atm.

Table 1 Investigation of the influence of ZnEt_2 on **1**/BOMAG catalyst during ethylene polymerization

Run	$[\text{Nd}]/[\text{Mg}]/[\text{Zn}]$	Yield g	Activity kg mol ⁻¹ h ⁻¹	M_n^{theo} g mol ⁻¹	$M_n (D)^a$ g mol ⁻¹	$\text{PE}^{\text{vinyl}} b$ %
1	1/80/0	3.6	200	1800	2400 (2.1)	10
2	1/5/75	4.1	3700	2050	2200 (1.1)	2

80 °C, toluene, $[\text{Nd}] = 62.5 \mu\text{M}$, $M_n^{\text{theo}} = \text{yield}/2 \times (n\text{Mg} + n\text{Zn})$. ^a Determined by HT-SEC with PE standards. ^b Determined by ¹H NMR.

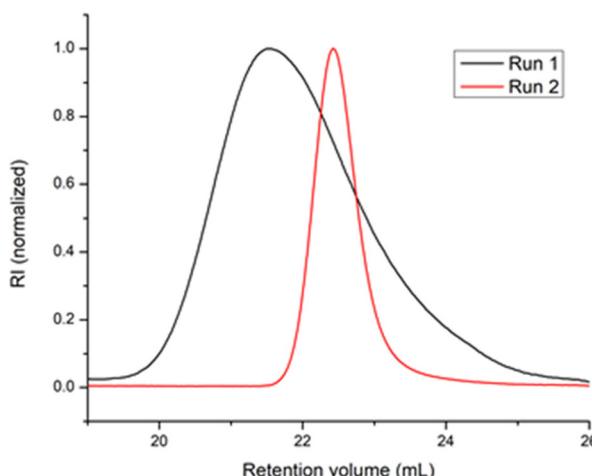


Fig. 1 SEC traces of polyethylene obtained with 1/BOMAG (run 1, Table 1) and 1/BOMAG/ZnEt₂ (run 2, Table 1) catalysts.

We also observe a good agreement between the theoretical number-average molar mass (M_n^{theo}) calculated considering that ZnEt₂ is concomitantly acting as chain transfer agent with BOMAG and the experimental M_n confirming that ZnEt₂ definitely acts as a CTA in this CCTP.

In addition, a sharp increase in activity from 200 to 3700 kg mol⁻¹ h⁻¹ is obtained, in good agreement with the modelling study. Indeed, the formation of a heterobimetallic NdZn₂ (Scheme 3) formed between the active species Me₂Si(C₁₃H₈)₂NdR and ZnEt₂ is exergonic by only 1.5 kcal mol⁻¹, whereas the heterobimetallic NdMg₂ (Scheme 3) species formed with BOMAG is exergonic by 11.9 kcal mol⁻¹. Consequently, the overall energy barrier of the ethylene insertion is lowered in the presence of ZnEt₂ and chain exchange is much faster between Nd and zinc than between Nd and magnesium. However, at this stage of our study, chain exchange between magnesium and zinc is not demonstrated. To evaluate a potential chain transfer between magnesium and zinc, a model reaction was performed in an NMR tube. The ¹H NMR analysis of BOMAG (Mg(ⁿBu)_{1.5}(ⁿOct)_{0.5}) and ZnEt₂ was carried out (Fig. S1 and S2†), followed by that of a BOMAG/ZnEt₂ mixture ([Mg]/[Zn] = 0.8, Fig. S3–S7†). Three new signals are

observed: two triplets at 0.23 and 0.27 ppm respectively, and a quadruplet at 0.13 ppm (Fig. S4†). An assignment of the two triplets is better performed when the NMR analysis is carried with a spectrometer operating at 500 MHz (Fig. S5†). As the signals are as well defined as those of ZnEt₂, it is reasonable to assume the formation of ZnEtR (R = ⁿBu and ⁿOct respectively) and to confirm an exchange of alkyl groups between zinc and magnesium under these conditions.

Investigation of the 1/BOMAG/ZnEt₂ catalyst system for ethylene polymerization. A series of experiments was further carried out by varying the [Nd]/[Mg]/[Zn] ratio. The overall concentration in Mg and Zn was kept constant, while [1] and [Mg]/[Zn] ratio were varied (Table 2). Given the low percentage of PE-vinyl observed at 80 °C when ZnEt₂ is used, the polymerization temperature was set at 90 °C to improve polyethylene solubility and reach higher molar masses while keeping the control of the polymerization. As expected, a higher yield resulted in higher molar masses (runs 7 and 8 in Table 2). Besides, considering the strong increase in activity observed when ZnEt₂ is used, lower concentrations of **1** could be used (run 4, Table 2) emphasizing that neodymium metallocene catalysts offer performances close to that of the best molecular catalysts for ethylene polymerization.³⁴

In the present case, ZnEt₂ increases the quantity of active neodymium as shown by the computational investigation. The good agreement between theoretical and experimental M_n indicates that polymerizations are controlled according to CCTP. The final PE show narrow molar mass distributions and the content of PE-vinyl chains decreases when the amount of ZnEt₂ increases. Decreasing the [Mg]/[Zn] ratio (runs 5–7, Table 2) leads to an increase in activity. When the lowest [Mg] is used (run 9, Table 2), a sudden deactivation of the catalyst is observed at the end of polymerization (Fig. S8†). The deactivation process appears to be linked to the increase in [Nd]-P active species in the presence of ZnEt₂. This deactivation might occur from inter- or intra-molecular reactions between the active species, reactions that are not identified yet even by molecular modelling. In summary, the dialkylmagnesium compound not only acts as an alkylating agent for **1** but also brings stability to the catalytic system *via* a mechanism that still not understood at the molecular level. Building on these promising results on the PE chain transfer ability when additional ZnEt₂ is employed, the

Table 2 Investigation of the ternary catalyst 1/BOMAG/ZnEt₂ in ethylene polymerization

Run	[Nd]/[Mg]/[Zn]	Yield g	Time min	Activity kg mol ⁻¹ h ⁻¹	M_n^{theo} g mol ⁻¹	M_n^{expt} g mol ⁻¹	D	PE-vinyl %
3	1/255/0	3.9	207	290	1950	2000	2.2	17
4	1/15/240	4.8	8	9200	2400	1900	1.2	5
5	1/60/20	4.1	48	410	2050	1400	1.6	29
6	1/40/40	4.9	14	1700	2450	2000	1.4	17
7	1/20/60	5.3	6	4600	2650	1800	1.4	5
8	1/20/60	9.7	12	3100	4850	4900	1.2	11
9	1/5/75	3.6	7	2500 ^c	1800	1400	1.2	5

^a [Nd] = 20 μ M (runs 3 and 4), 62.5 μ M (runs 5 to 9), 200 mL toluene, 4 bar, 90 °C (run 8 at 80 °C), M_n^{theo} = yield/2*(nMg + nZn). ^b Determined by ¹H NMR. ^c Total deactivation of the catalytic system at the end of polymerization.

combination of **1** and mixed CTA based on Mg and Zn was further evaluated in the coordination chain transfer copolymerization (CCT(co)P) of ethylene and butadiene for the synthesis of ethylene butadiene rubber (EBR).

Investigation of 1/BOMAG/ZnEt₂ catalyst system for the copolymerization of ethylene (E) and butadiene (B). A first preliminary test was performed with ZnEt₂ alone combined with **1** ([Zn]/[Nd] = 5) and a [B]/[E] monomer feeding ratio of 20/80, at 70 °C in toluene but as expected no polymerization was observed. Nevertheless, the addition of 4 equivalents of Mg (Bu)_{1.5}(Oct)_{0.5} (BOMAG) in the polymerization medium activates the metallocene and an EBR was isolated. The determination of the M_n highlighted that both BOMAG and ZnEt₂ acted again as CTAs.

Copolymerizations of ethylene and butadiene were then carried out with a ([Mg] + [Zn])/[Nd] ratio fixed to 10 and targeting 15 g of polymer, corresponding under these conditions to a theoretical M_n^{theo} of 15 000 g mol⁻¹ (Table 3). Very similar molar masses (between 12 500 and 14 200 g mol⁻¹) consistent with the targeted value were obtained for various [Mg]/[Zn] ratios showing again here that both BOMAG and ZnEt₂ are acting as CTAs.

For CCTcoP of ethylene and butadiene, the number of polymer chains is fixed by the number of magnesium-alkyl and zinc-alkyl bonds. For both binary and ternary catalytic systems, similar molar mass distributions are obtained (Fig. S9†), but contrary to ethylene homopolymerization, the use of ZnEt₂ as co-CTA in CCTcoP of ethylene and butadiene does not raise the catalytic activity nor narrow the molar mass distribution that respectively remain around 200 kg mol⁻¹ h⁻¹

Table 3 Copolymerization of ethylene with butadiene using 1/BOMAG/ZnEt₂ ternary catalytic system

Run	[Nd]/[Mg]/[Zn]	Yield g	Time min	Activity kg mol ⁻¹ h ⁻¹	M_n^a g mol ⁻¹	D
10	1/10/0	14.9	81	220	13 800	1.4
11	1/8/2	15.4	87	210	14 200	1.5
12	1/5/5	14.8	94	190	13 800	1.5
13	1/4/6	14.8	76	230	12 500	1.4
14 ^b	1/2/8	1.6	35	60 ^b	—	—

[Nd] = 250 μ M, 4 bar (ethylene/butadiene = 80/20), 90 °C, 200 mL toluene. ^a Determined by SEC in THF using an universal calibration.

^b Low activity then total deactivation of the catalytic system after 35 minutes of polymerization.

Table 4 Microstructure of EBR obtained with 1/RMgX/ZnEt₂ ternary catalysts (X = Bu or Mes) determined by ¹H NMR

Run	[Nd]/[Mg]/[Zn]	E/B	Vinyl (%)	trans-1,4%	1,2-Cyclohexyl (%)	Ethylene ^a (%)
10	1/10/0	80.0/20.0	7.7	6.0	10.4	75.9
11	1/8/2	81.2/18.8	6.3	5.9	10.7	77.2
12	1/5/5	80.7/19.3	6.6	6.2	10.7	76.6
13	1/4/6	81.0/19.0	6.4	6.0	10.7	76.9
17	1/16/10	79.7/20.3	8.6	5.8	9.9	75.8

^a Except those included in cyclic units.

Table 5 Optimization of **1**/MesMgBr/ZnEt₂ catalyst for ethylene polymerization or ethylene and butadiene copolymerization and subsequent chain end functionalization by reaction with an acyl chloride

Run	[Nd]/[Mg]/[Zn]	Yield g	Time min	Activity kg mol ⁻¹ h ⁻¹	M_n^{theo} g mol ⁻¹	M_n^{c} g mol ⁻¹	D	PE-vinyl %	PE(EBR)-C(O)C ₆ H ₄ X %
1 ^a	1/80/0	3.6	82	200	1800	2400	2.1	10	—
15	1/20/80	4.2	31	690	2010	2000	1.1	3	79 ^d
16	1/8/80	3.5	35	500 ^e	1750	1700	1.1	4	86 ^d
17 ^b	1/16/10	10.3	174	70	10 000	16 400	1.3	—	34 ^f

[Nd] = 62.5 μ M, 4 bar, 80 °C, 200 mL toluene. ^a Reference test with BOMAG. ^b [Nd] = 250 μ M, 4 bar (ethylene/butadiene feed ratio: 80/20), 80 °C, 200 mL toluene. ^c Determined by HT-SEC with PE standards for PE samples and by SEC-THF with universal calibration for the EBR sample. ^d Determined by ¹H NMR. ^e Partial discoloration of the solution, loss of exotherm and decrease of ethylene consumption. ^f Functionalization yield = $M_n^{\text{SEC}}/M_n^{\text{RMN}}$.

the number of chains formed, *i.e.* all chains were initiated by an ethyl group (Table 5). Whatever the reaction conditions used, polymerization takes place. Considering that ZnEt₂ does not alkylate **1** and that the Nd-Mes was previously shown not to initiate ethylene polymerization,⁴⁰ initiation of the polymerization presumably proceeds *via* an arylation of the Nd center by MesMgBr followed by a transmetalation between Nd-Mes and Zn-Et bonds. This was indeed confirmed by a good agreement between experimental and theoretical M_n . The reversibility of the chain transfer between Nd and Zn centers is also confirmed by lower the dispersity values obtained ($D < 1.3$) compared to the one obtained when the experiment was conducted with BOMAG alone ($D = 2.1$, run 1, Table 5).

Concerning chain-end functionalization, preliminary results gathered on the reactivity of MgPE₂ prepared with (C₅Me₅)₂NdCl₂Li(OEt)₂/BOMAG binary catalyst reveals that functionalization upon the reaction with two equivalents of *p*-toluoyl chloride does not provide the expected ketone functionalized PE chains. Instead, a mixture of secondary and tertiary alcohols (PE-CH(OH)-(C₆H₄Me): 25%, PE₂-C(OH)-(C₆H₄Me): 27%), PE-vinyl (30%) et PE-CH₃ (16%) (Scheme S2 and Fig. S10†) is obtained. Using **1**/MesMgBr/ZnEt₂ ternary system, chain-end functionalization with two equivalents of *p*-toluoyl chloride relative to Zn was performed (runs 15 and 16, Table 1). A representative ¹H NMR spectrum of the final PE obtained is shown on Fig. 2 for run 16 (Table 5). The assign-

ment of the signals performed on Fig. 2 strongly supports the selective formation of the targeted *p*-methylphenone-PE and shows the absence of any other signals including those related to chains initiated by a mesityl moiety. High functionalization yields from 79 to 86% were obtained using only one equivalent of acyl chloride per Zn-alkyl bond. This selectivity outcome reinforces the role played by Zn in mostly supporting PE chains and eludes an efficient chain transfer reactions between Nd or Zn with Mg. Eventually, run 16 (Table 5), with [Mg]/[Nd] = 8, shows a slowdown in polymerization rate over time. As already mentioned in the case of BOMAG (Table 2), an excess of magnesium compound compared to neodymium is required to achieve stable activity.

1/MesMgBr/ZnEt₂ catalyst system was further tested for the copolymerization of ethylene and butadiene (run 17, Table 5). An EBR (20.3% of inserted butadiene) with a similar microstructure (Table 4) to that obtained when BOMAG is used (run 10, Table 3) was isolated however with lower activity. The polymerization medium was deactivated by addition of 4-dimethylaminobenzoyl chloride. The ¹H NMR spectrum shows the characteristic signal of methyl groups from $-\text{NMe}_2$ group in agreement with the formation of *p*-dimethylaminophenone chain end (Fig. S11†). A functionalization rate of 34% was measured. This relatively low functionalization efficiency in comparison to functionalization reaction conducted on PE chains can be ascribed to the different nature of the chain ends in the two systems²⁶ and their respective reactivity but also to the higher molar mass obtained for EBR.⁴¹

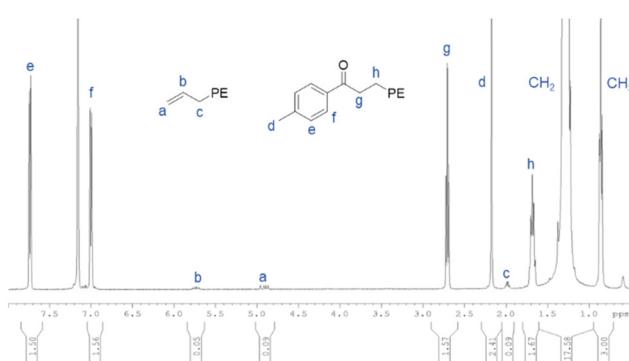


Fig. 2 ¹H NMR spectrum of the *p*-methylphenone-PE obtained with the ternary catalytic system **1**/MesMgBr/ZnEt₂ after deactivation with *p*-toluoyl chloride (run 16, Table 5).

Conclusions

In this work, we have demonstrated that ZnEt₂ is an effective CTA when used in combination with **1** for CCTP of ethylene or CCTcoP of ethylene and butadiene to produce EBR. However, being unable to alkylate **1** when used alone, the effectiveness ZnEt₂ as CTA depends on the additional presence of an organomagnesium compound that additionally stabilize the resulting catalyst. Compared to magnesium, the storage of the polymer chains on zinc modifies the reactivity of the chain ends, enabling a selective terminal ketone formation through deactivation reactions of the polymerization medium with acyl

chlorides. Despite this, the functionalization rate remains low for EBR, making the synthesis of highly functionalized EBRs with high molar masses a future challenge. Additionally, combining ZnR_2 and MgR_2 CTA could open new avenues for integrating Nd metallocenes in original catalyst combinations for the production of original OBC. This approach holds the potential to combine the properties of polyolefins exclusively accessible with Nd metallocene with other polyolefins.

Author contributions

The original ideas were conceived by the corresponding authors FdA, MEP, and CB in collaboration with industrial partners FJBdD and RN. Experimental work was carried out by AD, VL and NB, while the computational studies were conducted by LV. The manuscript was written collectively by all the authors.

Data availability

The data supporting this article have been included as part of the ESI.†

Conflicts of interest

There are no conflicts to declare.

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