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Cobalt–zinc carbides embedded in N-doped porous carbon nanospheres as polysulfide mediators for efficient lithium–sulfur batteries†

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Developing high-efficiency interlayer catalysts is a promising tactic for improving the cycling performance of rechargeable lithium–sulfur (Li–S) batteries. Herein, using the Prussian blue analogue as the precursor, cobalt–zinc carbide nanocrystal-embedded N-doped porous carbon (Co₃ZnC@NC) is synthesized *via* simple post-carbonization. The obtained Co₃ZnC@NC nanospheres exhibit a robust core–shell structure showing good conductivity, high porosity and available metal active sites, favoring the interfacial charge transfer and the electron transport upon electrochemical reactions. The results demonstrate that the Co₃ZnC@NC catalyst is quite suitable for boosting the adsorption and redox conversion kinetics of soluble polysulfides. When acting as the separator interlayer, Co₃ZnC@NC contributes to improved Li–S batteries with a high discharge specific capacity of 1659.8 mA h g^{−1} at 0.1C and superior cycling stability of over 250 cycles at 1.0C (high capacity retention of 84.1% after 100 cycles at 0.5C). Furthermore, the Co₃ZnC@NC-based battery can maintain a high discharge capacity of 734.0 mA h g^{−1} at 5.0C, along with delivering a stable reversible capacity of 805.4 mA h g^{−1} (~5 mA h cm^{−2}) after 50 cycles even under a high sulfur loading of 6.2 mg cm^{−2}. This study affords a viable way to construct highly dispersed bimetal/carbon composites for efficient catalysts and renewable energy devices.

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1. Introduction

The ubiquitous application of numerous portable electronics and the continued success of plug-in electric vehicles have increasingly motivated the exploration of high-performance and safe electrochemical battery systems.¹ In addition to traditional ion-intercalation batteries, rechargeable lithium–sulfur (Li–S) batteries have become one of the preferred solutions for advancing current energy storage devices.² Based on the electrocatalytic sulfur chemistry, Li–S batteries possess outstanding theoretical energy density (2600 W h kg^{−1}) and high theoretical specific capacity (1675 mA h g^{−1}), along with the merits of naturally abundant sulfur and eco-friendliness.^{3,4} However, today's Li–S electrochemistry is inherently plagued by

several drawbacks, including the poor inherent conductivity of the active sulfur and the insoluble lithium sulfide, the volumetric expansion of the sulfur cathode, and the notorious shuttling of soluble polysulfide lithium (Li₂S_x, LiPSs).^{5,6} More importantly, the lithium metal anode has high reactivity and often tends to form unstable structures on its surface during prolonged electrochemical reactions.⁷ Moreover, the shuttling of LiPSs could cause unnecessary side reactions on the lithium metal surface and induce the formation of more lithium dendrites, seriously affecting the long-term cycling stability, especially the safety of Li–S batteries.⁸

To inhibit the shuttling effect of LiPSs for improved Li–S batteries, tremendous efforts have been made to elucidate the reaction mechanism of Li–S electrochemistry.⁹ Thus, designing suitable high-activity electrocatalysts has become a primary option that can speed up the slow reaction kinetics of lithium polysulfides involving a complex multi-electron transfer process.¹⁰ As an indispensable part of the electrochemical energy device, the separator could play a crucial role in modulating the complicated “solid–liquid–solid” interfacial reactions during lithium storage, thus largely impacting the performance of Li–S batteries.¹¹ Accordingly, modifying commercial separators with functional interlayer electrocatalysts has been a feasible strategy for promoting battery performance.¹² Those functional separators can generally mitigate LiPS shuttling by trapping the dissolvable LiPSs at the cathode side and

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effectively reducing the corrosion of the lithium anode.¹³ Among diverse interlayer catalysts, various porous carbon materials have been adopted to obtain functional separators, limiting the shuttle of polysulfides by physically blocking the LiPSs with abundant and appropriate pores.¹⁴ Taking advantage of electronegative heteroatom (*e.g.* N, S, and P) doping, the physical adsorption and binding ability of the carbon surface toward the LiPSs can be increased.¹⁵ However, the chemical affinity and electrochemical properties of most carbon catalysts toward sulfur electrocatalysis are still restricted, leaving sufficient room to improve the cycling capacities and the long-term stability of corresponding Li-S batteries.¹⁶

To address these issues, polar metal compounds (*e.g.* sulfides, nitrides, oxides and phosphides of non-precious metals) with strong chemical affinity and abundant electro-active sites are introduced as catalysts for boosting the sluggish redox conversion of LiPSs at the multiphase interfaces.^{17–19} By rationally hybridizing metal compounds with porous carbon matrix, desirable catalysts with good conductivity, high selective permeability and excellent electrocatalytic activities can be achieved.^{20–23} Such hybridized catalysts are promising to use fully the synergistic effects between the porous carbon nano-structure and the metal active sites, which considerably accelerates the adsorption and catalytic conversion of LiPSs during reversible battery reactions.^{24,25} Intriguingly, transition metal carbides have attracted much attention in (electro-)catalytic fields due to their electroactivity, prominent electronic conductivity, high stability and good compatibility with carbon supports.^{26–28} By constructing desired transition metal carbide-based hybrid catalysts, one major challenge is to ensure homogeneously dispersed and sufficient metal active sites in the carbon matrix.²⁹ Moreover, the different valence changes in the metal centers are often conducive to manipulating the charge transfer as well as the adsorption/desorption behavior between the active sites and the LiPS intermediates, which ultimately influence the redox kinetics of Li-S electrochemical reactions.^{30,31} In early 2016, Wang *et al.* hybridized exfoliated-metal carbide ($\text{Ti}_3\text{C}_2\text{T}_x$) nanosheets with mesoporous carbon to host sulfur. Profiting from the effective trapping of sulfur and polysulfides by metal carbides, the sulfur cathode contributed to improved Li-S batteries with a discharge capacity of $1225.8 \text{ mA h g}^{-1}$ and stable cycling of over 300 cycles at 0.5C .³² Zhang *et al.* used nitrogen-doped carbon-supported $\text{Co}_3\text{Mo}_3\text{C}$ to modify the commercial separator. The results demonstrated that bimetallic $\text{Co}_3\text{Mo}_3\text{C}$ could provide more binding sites for polysulfide adsorption and catalysis compared with monometallic Mo_2C , thus leading to highly stable Li-S batteries with greatly increased sulfur utilization.³³ Hong *et al.* proposed $\text{Ni}_3\text{ZnC}_{0.7}/\text{Ni}/\text{NCNTs}$ -functionalized separators for high-performance Li-S batteries with excellent rate capabilities. The study illustrated the advantageous properties of the bimetal carbides with sulfophilic Ni sites and lithophilic Zn sites to regulate the redox kinetics of polysulfides.³⁴ Despite this encouraging progress, it is still essential to develop high-efficiency bimetal carbide-based interlayer catalysts through simpler, low cost, and scalable syntheses to better increase sulfur utilization toward practical Li-S batteries.³⁵

In consideration of the above, in this work, we designed nitrogen-doped porous carbon-encapsulated cobalt–zinc carbides ($\text{Co}_3\text{ZnC@NC}$) nanospheres through a simple one-pot synthesis. The $\text{Co}_3\text{ZnC@NC}$ composite was derived from the post-carbonization of the Prussian blue analogue precursor. Benefiting from the core–shell structure that comprises highly dispersed bimetal carbide nanocrystals and thin N-doped carbon shells, $\text{Co}_3\text{ZnC@NC}$ was endowed with hierarchical pores, good conductivity and abundant metal catalytic sites. Experimental results demonstrated the key role of $\text{Co}_3\text{ZnC@NC}$ in boosting the adsorption and reversible catalytic conversion of LiPSs during electrochemical reactions. By modifying the commercial polypropylene separator with $\text{Co}_3\text{ZnC@NC}$, corresponding rechargeable Li-S batteries achieved high discharge capacities ($1144.6 \text{ mA h g}^{-1}$ at 0.5C), superior cyclic stability (long cycling of over 250 cycles at 1.0C) and good high-rate performance ($734.0 \text{ mA h g}^{-1}$ at 5.0C), showing inhibited shuttling of polysulfides upon charge/discharge cycling.

2. Experimental

2.1 Synthesis of materials

2.1.1 Synthesis of $\text{Co}_3\text{ZnC@NC}$. Note that 1.3293 g of potassium–cobalt cyanide was added to 100 mL of deionized water and labeled as solution A. A total of 0.2920 g of $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ and 1.4875 g of $\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ were added to 100 mL of deionized water to form solution B. Then, solution B was slowly dropped into solution A under an agitated state. The mixture underwent continuous stirring for 10 min at room temperature and was then left to age for 24 h . After centrifugation, pink precipitates were obtained, washed, and further dried in a vacuum at 60°C to form the pink precursor of the Prussian blue analogue (PBA). The precursor was then placed in a tube furnace for post carbonization at 700°C for 1 h under the protection of the N_2 atmosphere at a heating rate of 3°C min^{-1} . After cooling to room temperature, the powder sample was collected and labeled as $\text{Co}_3\text{ZnC@NC}$.

2.1.2 Preparation of the modified separators. The inter-layer catalyst ($\text{Co}_3\text{ZnC@NC}$), the conductive carbon black (Super P) and the polymeric binder (polyvinylidene fluoride, PVDF) were weighed at a mass ratio of $8:1:1$, respectively, while *N*-methylpyrrolidone (NMP) was used as the solvent and stirred for 12 h to obtain a uniform mixture. Then, the resulting slurry was coated onto one side of the commercial separator (Celgard 2500) by applying the doctor blading method. The modified separators were then dried overnight in a vacuum oven at 60°C , generating the $\text{Co}_3\text{ZnC@NC}/\text{PP}$ separators. Typically, $\text{Co}_3\text{ZnC@NC}/\text{PP}$ separators were cut into 19 mm discs with a catalyst loading amount of approximately 0.8 mg cm^{-2} . In comparison, the Super P modified separator (Super P/PP) was prepared according to the same procedures without incorporating $\text{Co}_3\text{ZnC@NC}$.

2.2 Preparation of the electrodes

2.2.1 Preparation of the sulfur cathode. The carbon/sulfur composites were prepared using the hot melting method.



Sublimed sulfur and Ketjen black (ECP-200L) were ground, evenly mixed in an agate mortar with a mass ratio of 3 : 1 for 15 min, and then placed into a tube furnace. The powder was heated at 155 °C for 12 h under N₂ atmosphere and further sublimated at 200 °C for 30 min at a heating rate of 2 °C min⁻¹. The sample collected after cooling was the active carbon/sulfur composite. The preparation of the sulfur cathode pieces was as follows. 80 wt% of the carbon/sulfur composite, 10 wt% of Super P and 10 wt% of the LA133 binder (5 wt% in water) were evenly mixed with deionized water and fully stirred in deionized water for 12 h, and the acquired slurry was uniformly coated onto the carbon-coated side of aluminum foil using the doctor blading method. As-fabricated cathode pieces were dried overnight in a vacuum oven at 60 °C and finally cut into cathode discs with a diameter of 12 mm and a specific sulfur loading of 1.2–1.3 mg cm⁻².

2.2.2 Preparation of the symmetrical electrodes. The carbon/sulfur composite was replaced with the active material (Co₃ZnC@NC), and the other procedures were the same as those above to produce the final Co₃ZnC@NC-based working electrodes and counter electrodes of the symmetrical cells.

2.3 Material characterization

X-ray diffraction (XRD, Rigaku Ultima IV) with Cu K α radiation (λ = 0.154 nm) was used to analyze the crystal structure and composition of the composite. The microstructure of the samples was analyzed by applying a scanning electron microscope (SEM, ZEISS) and transmission electron microscope (TEM, FEI-Talos F200S). X-ray photoelectron spectroscopy (XPS, Thermo Scientific K-Alpha) was used to characterize the composition and valence states of the elements in the composites. The carbon content in the composite was analyzed by thermogravimetric analysis (TGA, Rigaku TG/DTA8122) under an air atmosphere. The Brunauer–Emmett–Teller (BET) method was used to assess the specific surface area and the pore size distribution of the sample through Micromeritics ASAP 2460. For the static adsorption test, a 10 mg sample (Super P or Co₃ZnC@NC) was added into 2 mL of Li₂S₆ solution (5 mmol L⁻¹, DoDo Chem, LS-243) and left for 24 h. The obtained supernatant after adsorption was diluted to measure the UV-vis absorption behavior on a UV-2600 spectrophotometer.

2.4 Battery assembly and electrochemical measurement

2.4.1 Assembly of Li–S batteries and symmetrical cells. Battery assembly was carried out in a glove box filled with argon gas to fabricate CR 2032 button cells. Typically, to assemble Li–S batteries, a high-purity lithium plate acted as the anode while the above-mentioned sulfur electrode acted as the cathode. The catalyst-modified separator or commercial separator (Celgard 2500) is assumed to be the separator. The electrolyte was composed of 1.0 M lithium bis(trifluoromethanesulphonyl) imide (LiTFSI) dissolving in mixed 1,2-dimethoxyethane (DME) and 1,3-dioxolane (DOL) solvent (DME : DOL = 1 : 1 vol%) by incorporating 1.0 wt% lithium nitrate (LiNO₃) as the additive. For the assembly of symmetrical cells, two identical Co₃ZnC@NC-based electrodes acted as the working electrode and

the counter electrode, respectively. A commercial separator (PP, Celgard 2500) was used as the separator, and the electrolyte (20 μ L) was composed of 0.2 mol L⁻¹ Li₂S₆, 1.0 M LiTFSI and 1.0 wt% LiNO₃ in the mixed solvent of DME and DOL ($V_{\text{DME}}/V_{\text{DOL}}$ = 1 : 1).

2.4.2 Electrochemical characterizations. Several electrochemical tests were performed on the CHI660E and NEWARE battery systems for the assembled coin cells. Charging–discharging tests were performed under constant current to determine the specific capacities, cyclic stability and rate performance. Cyclic voltammetry (CV) tests used an operating voltage range of 1.7–2.8 V and a scanning rate of 0.1–0.5 mV s⁻¹. The AC electrochemical impedance spectroscopy (EIS) responses were recorded over the frequency range of 0.01 Hz to 100 kHz. CV curves of the symmetric cells were obtained at a scanning rate of 5 mV s⁻¹ and a voltage window of –1.0 to 1.0 V. For the lithium sulfide deposition/nucleation experiments, the coin cell was first discharged at a constant current of 0.112 mA to 2.12 V and then kept at a constant potential of 2.05 V until the current was below 0.01 mA to ensure that Li₂S was completely nucleated. For the Li₂S dissolution experiment, the battery was first discharged to 1.80 V at a constant current of 0.01 mA and then charged at a constant potential of 2.40 V until the current was down to 0.01 mA such that Li₂S was completely dissolved to obtain the current–time curve.

3. Results and discussion

The schematic of the synthesis of the bimetal carbide-embedded composite is shown in Fig. 1a. Particularly, Co₃ZnC@NC was derived from the formation and post-pyrolysis of the PBA precursor. Following a simple one-pot process, Co(CN)₆³⁻ reactants were spontaneously coordinated with Co²⁺ and Zn²⁺ for co-precipitation in the dispersion according to a suitable stoichiometric ratio. After sufficient aging and separation/purification, the cobalt–zinc PBA precursor was received, as evident by the series of characteristic diffraction peaks belonging to Zn₃[Co(CN)₆]₂·(H₂O)₁₂ (PDF #89-3739) (Fig. 1b). Finally, the PBA precursor turned to carbon-wrapped metal compounds after high-temperature calcination under an inert atmosphere, forming the Co₃ZnC@NC composite. As demonstrated by the XRD pattern in Fig. 1b, there is a convex peak near 2θ of 26.5°, which results from the characteristic graphitic plane of the nitrogen-doped carbon component in the composite. Moreover, the set of characteristic peaks centered at 2θ of 34.0°, 41.9°, 48.8° and 71.5° corresponds to the (110), (111), (200) and (220) planes of the Co₃ZnC phase (PDF #29-0524).³¹ In addition, the composition of the composite was further distinguished by thermogravimetric analysis (TGA) conducted in an air atmosphere. Fig. 1c shows the thermogravimetric curve of Co₃ZnC@NC. This demonstrates two obvious steps for mass loss upon calcination. The first weight decline occurs in the range of 300–400 °C, which accounts for a loss portion of 28.6% and can be attributed to the oxidation decomposition of the nitrogen-doped carbon species in the outer layer of the composite. The second weight loss appears in the range of 550–650 °C largely caused by the oxidation of the



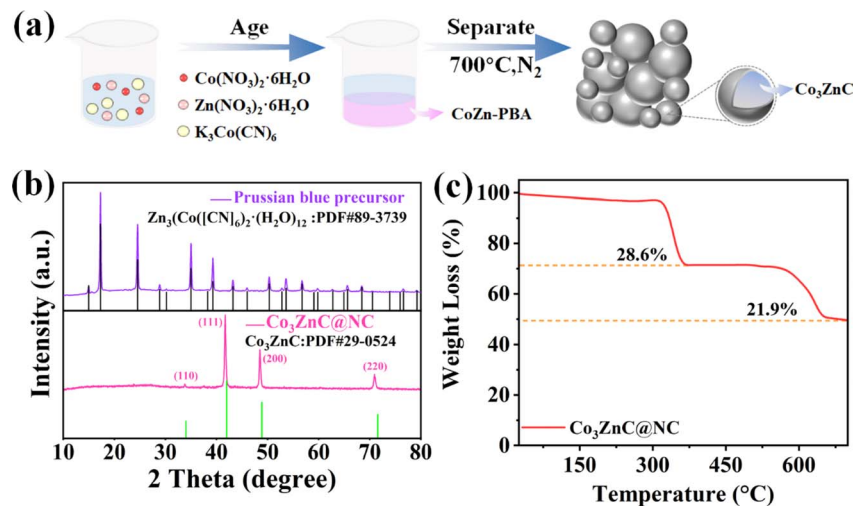


Fig. 1 (a) Schematic preparation of the $\text{Co}_3\text{ZnC@NC}$ composite, (b) XRD patterns of different samples, and (c) thermogravimetric curve of $\text{Co}_3\text{ZnC@NC}$.

inner carbonaceous species and metal carbides component, leading to a loss rate of 21.9%. The results indicate that there are considerable amounts of carbon components in the $\text{Co}_3\text{ZnC@NC}$ composite.

SEM images of the as-synthesized composite are shown in Fig. 2a and b. It can be observed that $\text{Co}_3\text{ZnC@NC}$ is basically composed of relatively dispersed and uniform nanoparticles. Some of these densely packed nanoparticles are connected by a few short carbon nanotubes (Fig. 2c), which is not uncommon

because the presence of active cobalt-based species can often catalyze the growth of carbon nanotubes under high-temperature carbonization.³⁶ The fine structure of $\text{Co}_3\text{ZnC@NC}$ is illustrated in Fig. 2d, revealing that $\text{Co}_3\text{ZnC@NC}$ mainly comprises irregular nanoparticles with particle sizes of 30–50 nm. According to Fig. 2e and f, $\text{Co}_3\text{ZnC@NC}$ demonstrates a typical core-shell nanostructure, where the internal Co_3ZnC nanocrystals are stably surrounded by thin N-doped carbon shells. Moreover, the lattice spacing of the inner nanoparticles is about 0.217 nm and

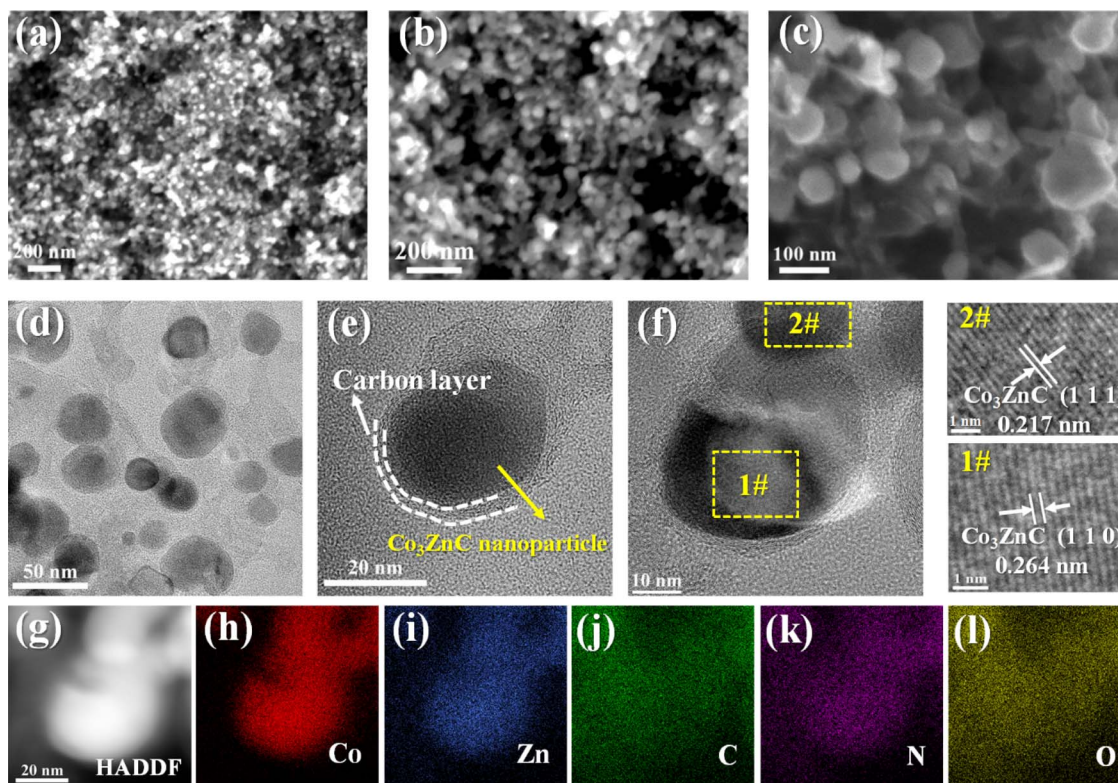


Fig. 2 SEM (a–c), HR-TEM (d–f), and EDS mapping (g–l) images of $\text{Co}_3\text{ZnC@NC}$.

0.264 nm, corresponding to the characteristic (110) and (111) faces of the Co_3ZnC nanocrystals. Fig. 2g–l displays the energy disperse spectroscopy (EDS) mapping images of $\text{Co}_3\text{ZnC@NC}$, showing that Co, Zn, C, N, and O elements are homogeneously distributed in the core/shell structured nanoparticles. Obviously, Co and Zn species are dominantly concentrated in the core of the nanoparticle, while C and N elements exhibit aggregated distribution in the outer layer of the nanoparticle along with apparent spreading over the entire nanoparticle. Unavoidably, the uniform distribution of O element in the composite is reasonable because many active nanocarbon or metal nanoparticles often endure slight oxidation to introduce oxygen-containing groups on the surfaces upon synthesis and utilization.³⁷ All the above results confirm the effective hybridization of Co_3ZnC nanocrystals and N-doped carbon to form core-shell structured $\text{Co}_3\text{ZnC@NC}$.

Fig. 3a demonstrates the N_2 adsorption/desorption isotherms of $\text{Co}_3\text{ZnC@NC}$. The BET surface area of $\text{Co}_3\text{ZnC@NC}$ is determined to be $53.40 \text{ m}^2 \text{ g}^{-1}$. Thus, the pore volume of the $\text{Co}_3\text{ZnC@NC}$ composite is $0.202 \text{ cm}^3 \text{ g}^{-1}$ with an average pore size of 16.26 nm. The pore size distribution reveals that $\text{Co}_3\text{ZnC@NC}$ is characterized by a hierarchical structure consisting of considerable micropores and sufficient mesopores. These hierarchical pores can ensure the appropriate penetration of the electrolyte into the catalyst to improve ion diffusion. Moreover, more exposed active sites are available to positively anchor/adsorb the soluble LiPSSs to accelerate the catalytic conversion rate of LiPSSs³⁸ to confine the LiPSSs at the cathode reaction interfaces with reduced shuttling effect.

To investigate the surface chemical composition and electronic state of the $\text{Co}_3\text{ZnC@NC}$ catalyst materials, X-ray photoelectron spectroscopy (XPS) characterization was

performed. The full spectrum further verified the coexistence of the main characteristic peaks of C 1s, N 1s, O 1s, Co 2p, and Zn 2p. The contents of C, N, O, Co, and Zn elements on the surface of $\text{Co}_3\text{ZnC@NC}$ were 74.32%, 12.69%, 8.31%, 1.35% and 3.33%, respectively. Fig. 3b shows the high-resolution Co 2p spectrum of $\text{Co}_3\text{ZnC@NC}$. The pair of sharp peaks at 778.1 and 793.1 eV can be ascribed to the characteristic Co^0 species, suggesting the adequate proportion of metallic Co present in the bimetal carbides under pyrolysis. This result agrees well with the above-mentioned observation that minor carbon nanotubes were generated by Co-catalyzed growth during the carbonization synthesis of $\text{Co}_3\text{ZnC@NC}$.³⁹ The prominent peaks at 778.8 and 793.7 eV correspond to the Co^{2+} species, along with two satellite peaks occurring at 781.9 and 796.8 eV. It is rational that the coexistence of Co^0 and Co^{2+} could effectively balance the valence states of Co active sites, which is beneficial for enhancing the chemical adsorption and targeted anchoring of LiPSSs by the active electrocatalyst during battery reactions.³⁵ In the high-resolution Zn 2p spectrum (Fig. 3c), two featured peaks at 1021.8 and 1044.9 eV can be assigned to Zn^{2+} . Previous findings have illustrated that the presence of a second metal species (*e.g.* Zn^{2+}) can cooperate with Co^{2+} to act as a reservoir, achieving synergistic adsorption and catalytic conversion of LiPSSs.^{40,41} For the C 1s spectrum illustrated in Fig. 3d, the diffraction peaks are C–C (284.8 eV), C–N (285.7 eV) and C=O (288.3 eV), indicating that the carbon layer on the surface of $\text{Co}_3\text{ZnC@NC}$ is rich in abundant C–N bonding. Such electro-negative nitrogen-rich carbon coating can introduce more disordered defects, increase the surface chemical affinity of the $\text{Co}_3\text{ZnC@NC}$ composite toward LiPSSs, and stabilize the internal bimetal carbides nanocrystals upon electrochemical cycling.

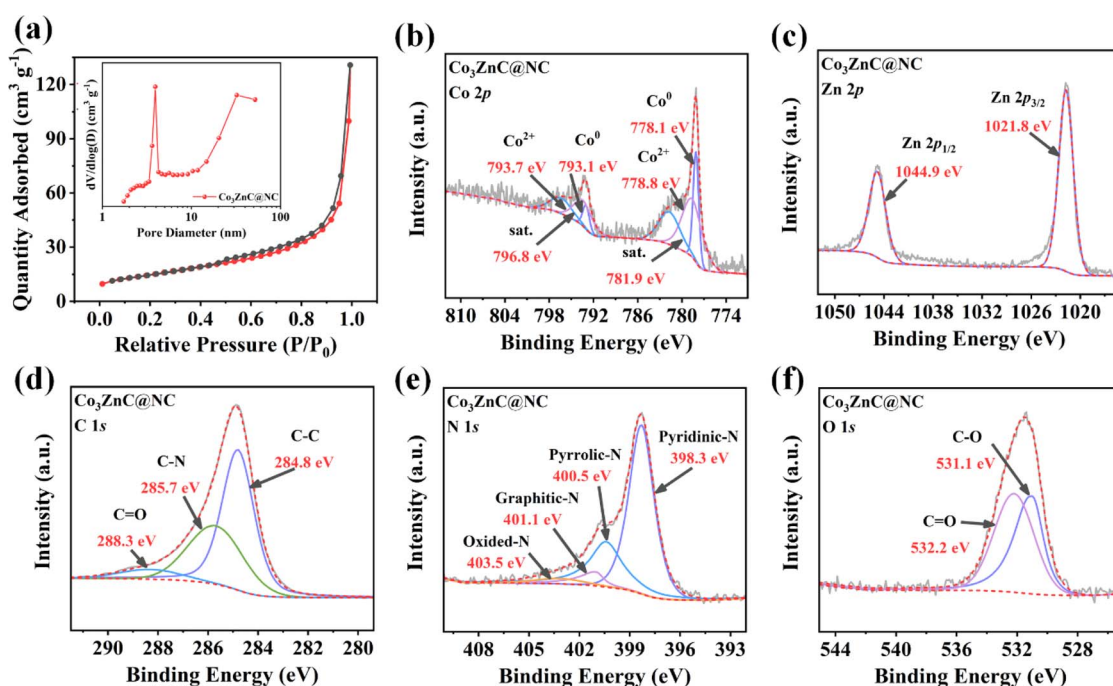


Fig. 3 (a) Nitrogen adsorption/desorption curves and pore size distribution (inset) of $\text{Co}_3\text{ZnC@NC}$; Co 2p (b), Zn 2p (c), C 1s (d), N 1s (e) and O 1s (f) spectrum of $\text{Co}_3\text{ZnC@NC}$.



According to Fig. 3e of the N 1s spectrum, the peak corresponds to pyridinic N (398.3 eV), pyrrolic N (400.5 eV), graphitic N (401.1 eV) and N oxides (403.5 eV). Conformably, the apparently high content of pyridinic N and pyrrolic N promoted electron transfer on the surface of the hybrid electrocatalyst, favoring the redox reactions of long-chain LiPSs.⁴² For the O 1s spectrum (Fig. 3e), the C–O bond at 531.1 eV and the C=O bond at 532.2 eV further infer the partial oxidation on the surface of Co₃ZnC@NC.

Fig. 4a shows the UV-vis absorption curves and corresponding optical photos of different samples after the static adsorption of Li₂S₆. Compared to Super P and the blank samples, Co₃ZnC@NC exhibited obviously increased adsorption capacity and high trapping ability toward polysulfides, which can be verified by the cleared color and the almost disappeared characteristic peaks of the Li₂S₆ solution in the UV-vis absorption spectrum.²⁵ To verify the electrocatalytic performance of Co₃ZnC@NC for LiPSs, cyclic voltammetry (CV) tests of symmetric cells were performed with Li₂S₆ solution as the electrolyte across the operating voltage range of −1.0 V to 1.0 V. In addition, a control cell using an electrolyte without Li₂S₆ was

investigated as the reference. As shown in Fig. 4b, the reference cell basically produces a negligible current contribution, while the symmetric cell containing Li₂S₆ exhibits obvious current response and significant redox peaks at −0.06 V and 0.06 V, indicating the adorable electrochemical properties of the Co₃-ZnC@NC composite for catalyzing the redox conversion of soluble LiPSs.

To further examine the electrochemical performance of the designed catalyst in actual batteries, Co₃ZnC@NC was used as an interlayer catalyst to modify the commercial PP separator, obtaining the Co₃ZnC@NC/PP-based Li–S battery. Unless otherwise mentioned, all the assembled Li–S batteries adopted a cathode with a sulfur loading of 72 wt% (Fig. S1†). Fig. 4c shows the Nyquist plots of fresh batteries based on Co₃-ZnC@NC/PP and PP separator through electrochemical impedance spectroscopy (EIS) characterization. It is reasonable that the entire internal resistance of the battery significantly decreases after the involvement of Co₃ZnC@NC. Thus, the charge transfer resistance (R_{ct}) of the Co₃ZnC@NC/PP battery (24.2 Ω) is much smaller than that of the PP battery (47.5 Ω), suggesting that the Co₃ZnC@NC interlayer catalyst can

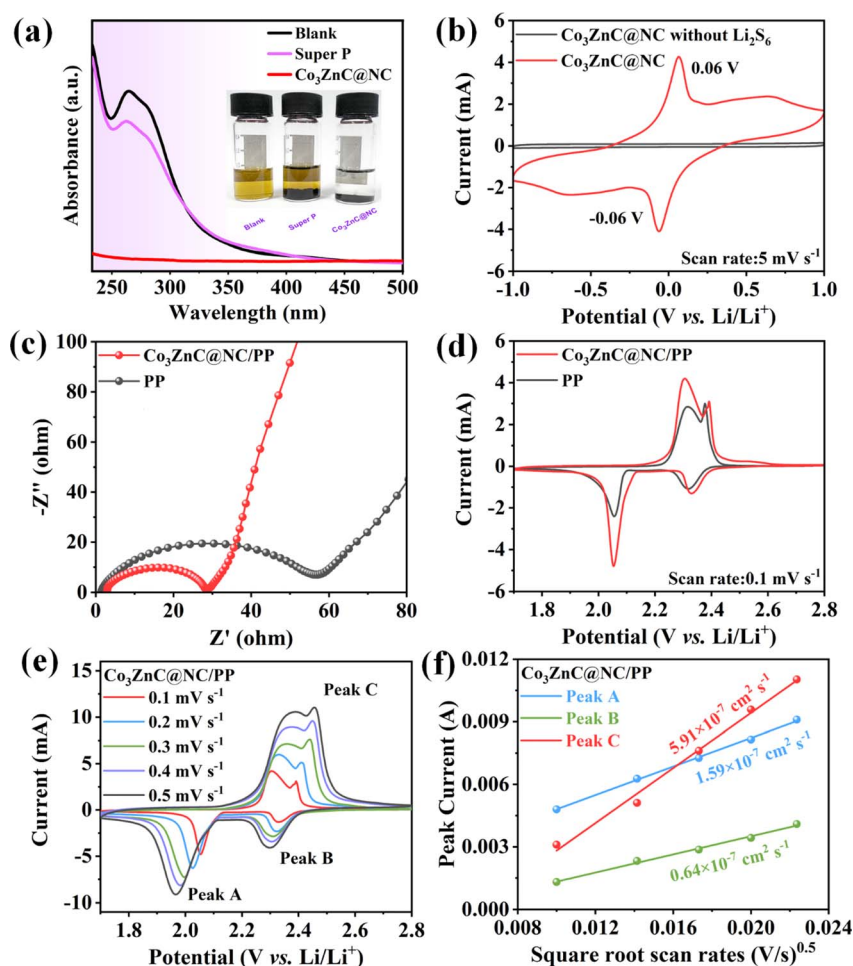


Fig. 4 (a) UV-vis absorption curves of different samples after Li₂S₆ adsorption and correlated photos of the static adsorption experiment of Li₂S₆ solution (inset); (b) CV curves of Co₃ZnC@NC-based symmetrical cells at a scan rate of 5 mV s^{−1}; (c) EIS curves of fresh Co₃ZnC@NC/PP and the PP batteries before cycling; (d) CV curves of Co₃ZnC@NC/PP and PP-based Li–S batteries at a scanning rate of 0.1 mV s^{−1}; (e) CV curves of the Co₃ZnC@NC/PP battery at different scanning rates; and (f) linear fitting plots of the three peak currents for the Co₃ZnC@NC/PP battery.

dramatically improve the interfacial charge-transfer by simultaneously providing sufficient electrocatalytic sites and a good conductive network, leading to accelerated redox kinetics of sulfur species, especially on the cathode side of the battery.^{43,44} Moreover, the redox reaction process of Li-S batteries was investigated in the operating voltage range (1.7–2.8 V) using CV at a low sweep rate of 0.1 mV s⁻¹. As shown in Fig. 4d, two separate reduction peaks centered at 2.34 and 2.05 V appear in the cathodic sweeping process, while two distinct peaks (2.3–2.5 V) in the anodic sweeping process can be observed. The former results from the stepwise production of long-chain Li₂Sn (4 ≤ *n* < 8) and short-chain polysulfides (1 ≤ *n* < 4) by reducing the elemental sulfur.⁴⁵ The latter corresponds to the backward oxidation of lithium sulfide to Li₂Sn (2 ≤ *n* ≤ 8). With the incorporation of Co₃ZnC@NC, the relevant battery delivers much stronger peak currents and reduced polarization potentials. It can be concluded that Co₃ZnC@NC exhibits a superior catalytic ability to facilitate reaction kinetics and improve the redox conversion of LiPSs during the battery charge/discharge process. Moreover, CV tests were performed on the PP battery and Co₃ZnC@NC/PP battery under different scanning rates. As demonstrated in Fig. 4e, the peak current and electrode polarization of the Li-S battery gradually increase as the scanning rate increases. Using the Randles-Sevcik equation, we analyzed the relationship between the peak current (*I*_p) of the characteristic redox peaks and the square root of the scanning rate (*v*^{0.5}).⁴⁶ As displayed in Fig. 4f, there is a certain linear relationship between *I*_p and *v*^{0.5}. In particular, the lithium ion diffusion coefficients (*D*_{Li⁺}) of peaks A, B and C are calculated to

be 1.59 × 10⁻⁷, 0.64 × 10⁻⁷ and 5.91 × 10⁻⁷ cm² s⁻¹, respectively, which are obviously higher than those of the PP battery (Fig. S2 and S3†), further confirming the favorable ion transport and electrochemical reversibility by the Co₃ZnC@NC catalyst. Notably, the *D*_{Li⁺} of the oxidation peak is significantly higher than the others. This infers that Co₃ZnC@NC could behave better at the catalytic conversion of short-chain Li₂Sn to long-chain LiPSs rather than the opposite reduction pathway.⁴⁷

Fig. 5a shows the cycling performances of Li-S batteries based on Co₃ZnC@NC/PP, Super P/PP and PP separator under a current density of 0.5C. Compared to the other two counterparts, the Co₃ZnC@NC/PP exhibits extremely improved discharge capacities and cycling stability. In particular, the initial discharge specific capacity of the Co₃ZnC@NC/PP battery is 1144.6 mA h g⁻¹ higher than that of Super P/PP (1003.6 mA h g⁻¹) and PP battery (635.1 mA h g⁻¹). After 100 continuous charge/discharge cycles, the Co₃ZnC@NC/PP battery can maintain a high discharge capacity of 962.6 mA h g⁻¹, yielding a retention rate of 84.1%, which is superior to that of the Super P/PP (79.6%) and PP battery (61.6%) with much lower retention capacity. Moreover, the high coulombic efficiencies of the Co₃ZnC@NC/PP battery during cycling demonstrate its excellent reversibility and durability during charge/discharge reactions.^{48,49} Correspondingly, the initial galvanostatic charge–discharge curves of batteries with different separators are compared, as depicted in Fig. 5b, which magnifies the relatively low electrode polarization of the Co₃ZnC@NC/PP battery. Further, after 100 successive cycles, the electrode polarization of the Co₃ZnC@NC/PP battery did not

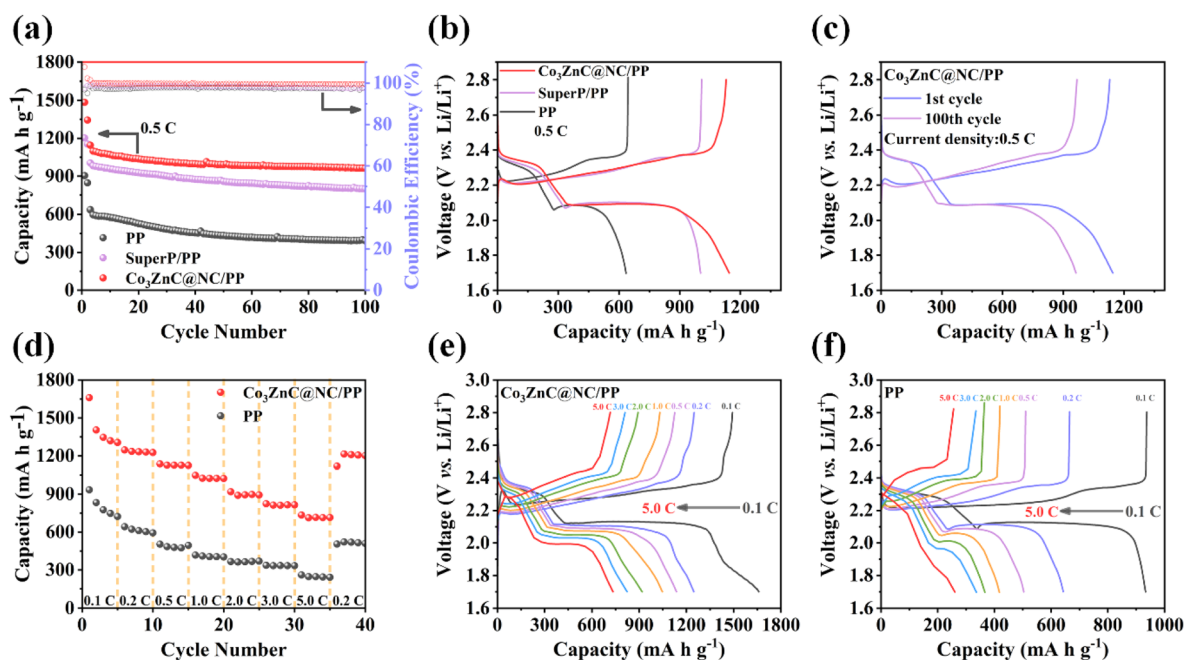


Fig. 5 (a) Cycling capacities and coulombic efficiencies of Li-S batteries with Co₃ZnC@NC/PP, Super P/PP and PP separator at 0.5C. The batteries were measured at 0.1C for the initial two cycles. (b) Comparison of the initial charge/discharge voltage–capacity curves of different batteries at 0.5C; (c) comparison of the first and 100th galvanostatic charge–discharge curves of Co₃ZnC@NC/PP-based Li-S battery at 0.5C; (d) rate performances of Li-S batteries with different separators; and (e and f) galvanostatic charge and discharge curves of Li-S batteries with different separators under different current densities.

change much (Fig. 5c). This suggests that the $\text{Co}_3\text{ZnC}/\text{NC}$ interlayer catalyst can effectively improve the electrochemical reversibility and capacity performance of Li-S batteries. According to the S 2p spectrum of $\text{Co}_3\text{ZnC}/\text{NC}$ after cycling at 0.5C for 50 cycles (Fig. S4a†), the prominent Co-S bonding further infers the strong chemical affinity and anchoring ability of $\text{Co}_3\text{ZnC}/\text{NC}$ toward polysulfides. Moreover, the evident negative shift of the N 1s peaks along with the positive shifts of both Co 2p peaks and Zn 2p peaks indicates the redistributed electron density of the metal centers or the metal-N moieties (Fig. S4b-d†), which could act as active sites for enhanced polysulfide interaction and catalytic conversion.

The rate performance of the Li-S batteries is demonstrated in Fig. 5d. $\text{Co}_3\text{ZnC}/\text{NC}/\text{PP}$ -based battery delivers a specific discharge capacity of $1659.8 \text{ mA h g}^{-1}$ at 0.1C. As the current density incrementally increases to 0.2C, 0.5C, 1.0C, 2.0C, 3.0C and 5.0C, the corresponding specific capacity is 1246.9, 1136.7, 1047.3, 918.4, 823.4 and $734.0 \text{ mA h g}^{-1}$, greatly surpassing that of the PP battery. Then, when the current density returns to 0.2C, the discharge specific capacity can still be restored to $1201.7 \text{ mA h g}^{-1}$ for the $\text{Co}_3\text{ZnC}/\text{NC}/\text{PP}$ battery. This indicates

that the active sites of the $\text{Co}_3\text{ZnC}/\text{NC}$ composite can achieve stable adsorption and electrocatalytic promotion of LiPSs upon lithium storage at different current densities, thus contributing to the high specific capacities and excellent rate capability of the battery at high rates. Based on the charge-discharge curves illustrated in Fig. 5e and f, the increases in the voltage gap of the $\text{Co}_3\text{ZnC}/\text{NC}/\text{PP}$ battery are significantly smaller than those of the PP battery at different current densities, further proving the efficient utilization of active sulfur and superb cycling stability by involving the $\text{Co}_3\text{ZnC}/\text{NC}$ interlayer as a polysulfide mediator in Li-S batteries during battery operation.

Furthermore, the long-term cyclic stability of the designed Li-S batteries was investigated. As presented in Fig. 6a, the $\text{Co}_3\text{ZnC}/\text{NC}/\text{PP}$ -based battery delivers an initial discharge capacity of $996.6 \text{ mA h g}^{-1}$ at 1.0C. After 250 charge/discharge cycles, the battery can well maintain a reversible specific capacity of $695.8 \text{ mA h g}^{-1}$, exhibiting capacity retention of 69.8% and an average decay rate per cycle of about 0.121%. Additionally, the coulombic efficiencies of the battery are stably above 96%. The results demonstrate the distinctly enhanced battery stability and excellent cycling performance by the

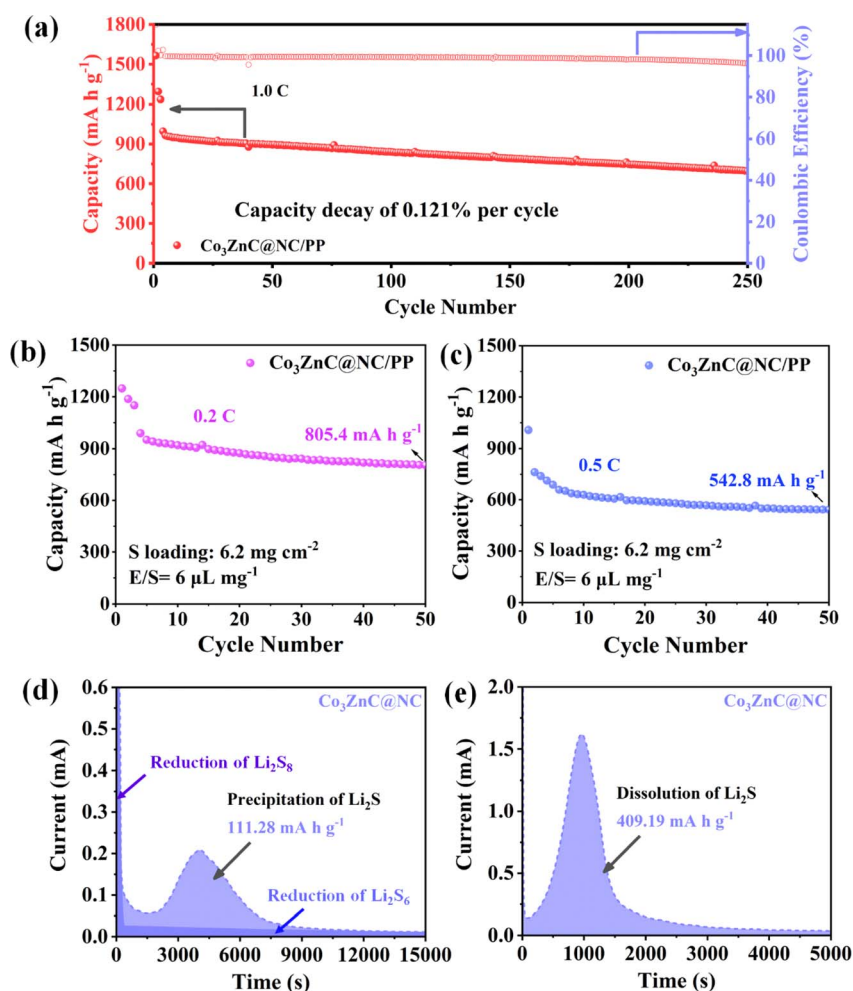


Fig. 6 (a) Long-cycle capacities and coulombic efficiencies of the $\text{Co}_3\text{ZnC}/\text{NC}/\text{PP}$ battery at 1.0C. The battery was measured at 0.1C for the initial two cycles. Cycling performance of the $\text{Co}_3\text{ZnC}/\text{NC}/\text{PP}$ battery with high sulfur loading at 0.2C (b) and 0.5C (c). (d) Potentiostatic discharge current-time plot of $\text{Co}_3\text{ZnC}/\text{NC}$. (e) Potentiostatic charging current-time plot of $\text{Co}_3\text{ZnC}/\text{NC}$.

Co₃ZnC@NC-modified functional separator upon long cycling. When the sulfur loading of the cathode was drastically elevated to 6.2 mg cm⁻² (*i.e.* E/S of 6 μ L mg⁻¹), the corresponding Co₃-ZnC@NC/PP battery can maintain a high discharge capacity of 805.4 mA h g⁻¹ (areal capacity of $\sim$ 5 mA h cm⁻²) at 0.2C (Fig. 6b) and 542.8 mA h g⁻¹ at 0.5C (Fig. 6c) even after 50 continuous cycles, shedding light on its superior cycling stability and promising practical potential toward high-specific energy output with lean electrolyte (Table S1†).

To further elucidate the positive role and key electrocatalytic performance of the Co₃ZnC@NC/PP catalyst for the redox conversion of LiPSs, typical nucleation/dissolution experiments were performed by assembling the coin battery with the Co₃-ZnC@NC electrode and the Li₂S₈-contained electrolyte.^{50,51} Fig. 6d illustrates the potentiostatic discharge current–time plot of Co₃ZnC@NC at an operating voltage of 2.05 V. The specific capacity of the Co₃ZnC@NC electrode toward Li₂S nucleation is calculated to be 111.28 mA h g⁻¹. Furthermore, by fitting the charging current–time plot of the Co₃ZnC@NC electrode operating at 2.40 V, a high specific capacity of 409.19 mA h g⁻¹ is achieved for Co₃ZnC@NC toward Li₂S dissolution (Fig. 6e). The relatively adorable nucleation/dissolution ability of Li₂S strongly confirms the chemical affinity and superior catalytic activity of the functional Co₃ZnC@NC layer. Co₃ZnC@NC could dominantly inhibit polysulfide shuttling by facilitating the interfacial charge transfer process and reducing the activation barrier for the phase nucleation of polysulfides^{52,53} to achieve accelerated redox kinetics of LiPSs and improved sulfur utilization of correlated Li–S batteries.

4. Conclusion

In summary, a hybrid electrocatalyst of Co₃ZnC-embedded nanospheres was developed as an efficient separator interlayer for rechargeable Li–S batteries. Using one-pot synthesis combined carbonization of Prussian blue analogue precursor, core–shell-structured Co₃ZnC@NC composite was obtained, showing advantages of high conductivity, hierarchical porosity, excellent adsorption properties and rich active sites toward LiPSs. Results demonstrated that Co₃ZnC@NC could act as a suitable polysulfide mediator by effectively lowering the interfacial charge-transfer resistance and improving the catalytic reversibility, thus contributing to enhanced redox kinetics of LiPSs upon battery reactions. Consequently, Co₃ZnC@NC/PP-based Li–S batteries achieved superior rate capabilities (734.0 mA h g⁻¹ at 5.0C), excellent cyclic durability (capacity retention rate of 84.1% after 100 cycles at 0.5C) and significant sulfur utilization efficiency even under a high sulfur loading of 6.2 mg cm⁻². This study illustrates a simple and cost-effective strategy for constructing advanced bimetal compound/carbon-based hybrid catalysts for high-performance renewable energy devices.

Data availability

The raw/processed data used in this study cannot be shared at this time, as the data also form part of an ongoing study.

Conflicts of interest

The authors declare no conflict of interest.

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