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In situ surface/interface generation on Cu₂O nanostructures toward enhanced electrocatalytic CO₂ reduction to ethylene using *operando* spectroscopy†

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Electrocatalytic CO₂ reduction reactions (CO₂RRs), an efficient method of converting carbon dioxide into valuable fuels and chemicals, are attractive as well as challenging. In this work, Cu₂O nanostructures with active facets (face-raised cubic structures (F-Cu₂O) with the (100) facet, octahedral structures (O-Cu₂O) with the (111) facet and edge- and corner-truncated octahedral structures (T-Cu₂O) with both the (100) and (111) facets) were synthesized by a wet chemical reduction method. The surface of Cu₂O nanostructures was reconstructed *in situ* to form Cu₂O/Cu with a highly active interface during the conversion of CO₂ into C₂H₄, which is named F-Cu₂O/Cu, O-Cu₂O/Cu and T-Cu₂O/Cu. The C₂H₄ selectivity on Cu₂O/Cu catalysts follows the order of O-Cu₂O/Cu < F-Cu₂O/Cu < T-Cu₂O/Cu, and the faradaic efficiencies of C₂H₄ are 11.2%, 24.9%, and 58.0% at -1.1 V versus the reversible hydrogen electrode, respectively. The experimental results combined with *operando* surface-enhanced Raman spectroscopy reveal that the Cu₂O/Cu interface enhances *CO adsorption and decreases the activation energy of C–C coupling, which is also supported by density functional theory (DFT) calculations. This study will pave a feasible pathway for electrochemical energy storage and conversion by crystal facet engineering and interface engineering.

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Introduction

Carbon dioxide (CO₂) is greatly responsible for global warming, rising sea levels and other extreme weather patterns, making it imperative to reduce the amount of CO₂ released into the environment by human activities.^{1–3} Electrocatalytic CO₂ reduction reactions (CO₂RRs) have received widespread attention due to their functions including but not limited to efficient conversion of CO₂ into value-added chemical feedstocks with high efficiency, providing an opportunity for clean renewable energy storage.^{4–6} However, the activity and selectivity of multi-carbon (C₂₊) products with high commercial values and high energy densities will be severely limited due to the slow kinetics of the C–C coupling step during CO₂RRs.^{7,8} The design of catalysts with high activity and selectivity for C₂₊ products is the key to promote the development of this field.

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Among the various electrocatalysts, copper is a distinct metal catalyst, which can produce considerable amounts of hydrocarbons and alcohols,^{9–13} because it can adjust the adsorption energy of intermediates and then promote the C–C coupling to form C₂₊ products.^{14–16} C₂H₄ is the main C₂₊ product and an important organic raw material, which is widely used in various industries.¹⁷ Thus far, how to improve the selectivity of Cu-based catalysts for the conversion of CO₂ into C₂H₄ and inhibit the generation of H₂ and C₁ species is the focus of research in terms of experimental and theoretical aspects.^{18–22} Extensive research has focused on optimizing compositions,^{23–25} morphologies,^{26,27} crystal facets^{28,29} and other aspects^{30–32} of Cu-based catalysts to improve the Faraday efficiency of C₂H₄. For example, Cu nanocubes with three different sizes were synthesized by a colloidal chemistry method to investigate the influence of Cu nanocrystal size on the selectivity and activity of electrocatalytic CO₂ reduction products.³³ The 44 nm Cu nanocubes were optimal for ethylene production with a maximum FE of 41%. Moreover, Cu₂O NPs are more favorable to the selective formation of ethylene with high selectivity as compared to Cu NPs. The controllable construction of Cu⁰ and Cu⁺ sites was achieved by controlling the loading of cupric oxide on copper phyllosilicate lamella to steer CO₂ electroreduction toward C₂H₄ production with high

performance,³⁴ which proves that Cu⁺ sites are more beneficial to produce ethylene.

For the metal oxide catalyst, the exposed facet surface not only determines the geometry of catalysts but also has a great effect on the electrocatalytic property of catalysts.³⁵ Cu₂O NPs with different crystal facets show different stabilities and catalytic activities.^{36,37} The product of C₂H₄ on Cu₂O NPs depends on diverse crystal facets, which determine the active sites that stabilize crucial intermediates during CO₂RRs. Therefore, crystal facets should be particularly considered in designing efficient CO₂RR catalysts. The studies revealed that Cu⁰/Cu⁺ sites play a key role in improving C₂₊ products on Cu₂O catalysts.³⁸ However, there are still no systematic studies on the effect of the Cu₂O/Cu interface with highly active facets *in situ* generated for electrocatalytic CO₂ reduction to C₂H₄ on Cu₂O nanostructures.

In this work, we prepared Cu₂O catalysts with active facets (F-Cu₂O, O-Cu₂O, T-Cu₂O) using diverse surfactant templates. High-resolution transmission electron microscopy (HR-TEM) exhibits that Cu₂O is enclosed with different facets, which are F-Cu₂O structures with the (100) facet, O-Cu₂O structures with the (111) facet and T-Cu₂O structures with the (111) and (100) facets, respectively. The surface of Cu₂O was reconstructed *in situ* to form a Cu₂O/Cu interface (F-Cu₂O/Cu, O-Cu₂O/Cu and T-Cu₂O/Cu) during the CO₂RR. The experimental results indicated that the C₂H₄ activity and selectivity are intensely influenced by the surface reconstruction and exposed active facets of Cu₂O catalysts. The C₂H₄ selectivity on Cu₂O/Cu catalysts follows the order of O-Cu₂O/Cu < F-Cu₂O/Cu < T-Cu₂O/Cu, and the faradaic efficiencies of C₂H₄ are 11.2%, 24.9%, and 58.0% at -1.1 V *vs.* RHE, respectively, relating to the exposure of different highly active facets and *in situ* generated Cu⁺/Cu interface. The experimental results combined with the *operando* surface-enhanced Raman spectroscopy and DFT calculations confirmed that the presence of Cu⁺/Cu interfaces and highly active facets enhances *CO adsorption and decreases the adsorption energy of C-C coupling, thus improving the C₂H₄ selectivity.

Experimental section

Materials

Sodium citrate tribasic dihydrate (C₆H₅Na₃O₇·2H₂O), ascorbic acid (AA), sodium hydroxide (NaOH), cupric sulfate pentahydrate (CuSO₄·5H₂O), copper chloride dihydrate (CuCl₂·2H₂O), lauryl sodium sulfate (SDS) and polyvinyl pyrrolidone (PVP, M_w = 58 000) were all purchased from Aladdin. Glucoses were obtained from Tianli Chemical Reagents. Nafion (5 wt%) were obtained from Aldrich. All gases such as carbon dioxide and nitrogen were obtained from Airgas.

Catalyst preparation

Synthesis of F-Cu₂O. A F-Cu₂O catalyst was prepared by a wet chemical reduction method on the basis of previous reports.³⁹ Specifically, C₆H₅Na₃O₇·2H₂O (0.1940 g) was first dissolved in

400 mL deionized water and stirred for 20 min. Then, 1 mL CuSO₄·5H₂O (0.77 M) aqueous solution was dropped into this solution. After stirring for 5 minutes, 1 mL NaOH (4.8 M) aqueous solution was slowly added to this mixed solution at room temperature, and 1 mL ascorbic acid (1.2 M) was added under stirring for 30 min to form a yellow solution. The solution was centrifuged after standing aged for 6 hours, washed three times with ethanol and deionized water and finally dried in a vacuum dryer.

Synthesis of O-Cu₂O. In a typical process,⁴⁰ 9.67 g PVP was added to a round-bottom flask (250 mL) containing 100 mL CuCl₂·2H₂O (1 mM) aqueous solution and stirred continuously in a 60 °C water bath. Then, 10 mL NaOH (2 M) aqueous solution was subsequently added to the round-bottom flask and stirred continuously for 30 min. Glucose (1.2 g) was added to this mixture and stirred vigorously for 3 h. All of the processes were maintained at 60 °C. The precipitates were centrifuged three times in deionized water and anhydrous ethanol, and dried under vacuum at 60 °C for 6 h.

Synthesis of T-Cu₂O. In a typical synthesis,⁴⁰ 0.085 g CuCl₂·2H₂O (5.65 mM) was added to 88.2 mL solution containing 0.87 g SDS (34.01 mM) and then stirred vigorously at 60 °C for 10 min. After that, 1.8 mL NaOH (1 M) and 5 mL glucose (0.1 M) were rapidly added to this solution and maintained under magnetic stirring for 1 h. The color of the suspension gradually changed to orange. The orange product was collected *via* centrifugation, washed several times with ethanol and deionized water to remove excess SDS, and finally dried under vacuum for further use.

Characterization of the catalysts

TEM was performed using a JEM 2100 to characterize the morphologies and size of the as-synthesized Cu₂O catalysts. An X'Pert3 Powder instrument at 45 kV and 40 mA was used to analyze the powder X-ray diffraction (XRD) pattern of Cu₂O catalysts. X-ray photoelectron spectroscopy (XPS) and Cu LMM spectra were recorded using a Thermo Scientific K-Alpha instrument to obtain the structure of catalysts. The chemical structures of Cu₂O samples were analyzed by Infrared Spectroscopy (IR).^{41,42}

Electrocatalytic activity measurements

The catalyst ink was prepared by dispersing 20 mg Cu₂O and 5 μ L of Nafion solution (5 wt%) in 1 mL isopropanol for at least 30 min by ultrasonication.⁴³ Subsequently, the ink was coated onto the polished glassy carbon electrode (diameter: 3 mm; area: 0.07 cm²) surface. The electrode was then dried in ambient air to obtain the working electrode for later electrochemical performance tests. Electrochemical performance tests were operated on a workstation (CHI 760E) equipped with an air-tight three-electrode cell, which used a glassy carbon (GC) electrode coated with catalysts as the working electrode. A Pt sheet and a Ag/AgCl (saturated KCl) electrode were used as the counter and reference electrodes, respectively. First, 0.1 M KHCO₃ solution was used as the electrolyte for all electrochemical CO₂RRs. The solution in the cathodic cell was satu-

rated with N_2 or CO_2 before electrochemical testing and 20 sccm flow rate was maintained during the CO_2 RR. The potential was converted into the reversible hydrogen electrode (RHE) as follows:

$$E(\text{vs. RHE}) = E(\text{vs. Ag/AgCl}) + 0.197 \text{ V} + 0.0591 \text{ V} \times \text{pH}$$

The gaseous products (*i.e.*, H_2 , CO , CH_4 and C_2H_4) were quantified using a gas chromatograph (GC, Panna) equipped with a thermal conductivity detector (TCD) and a flame ionization detector (FID). The GC was directly linked to an electrochemical cell for online analysis. The faradaic efficiency of gaseous products was calculated using the following equation:⁴⁴

$$\text{FE} = \frac{n \times F \times C_i \times G \times p}{R \times T \times j}$$

where n is the number of electrons required to produce a molecular product (*e.g.*, 2, 2, 8, and 12 e^- for CO , H_2 , CH_4 and C_2H_4), F is the Faraday constant ($96\,485 \text{ C mol}^{-1}$), C_i is the measured concentration of the products by GC, G is the gas flow rate, j is the current density, p is the atmospheric pressure, $1.013 \times 10^5 \text{ Pa}$, $R = 8.314 \text{ J mol}^{-1} \text{ K}^{-1}$, and $T = 273.15 \text{ K}$.

The liquid mixture was analyzed by 1H nuclear magnetic resonance, which was recorded using a Bruker Avance NEO 400 MHz spectrometer in deuterium oxide- d_2 with DMSO as internal standards.⁹

Double-layer capacitance (C_{dl})

The C_{dl} value was relative to the electrochemical active surface area. The C_{dl} value was estimated by cyclic voltammetry (CV) to measure the relationship between the scanning rate and capacitive current density. The potential of CV ranged from 0.4 V to 0.5 V *vs.* RHE. The C_{dl} value was estimated by plotting Δj ($j_a - j_c$) at -0.15 V *vs.* RHE against the scan rates (j_a = anodic current density and j_c = cathodic current density). The slope of C_{dl} was estimated to be twice that of C_{dl} .⁴¹

In situ surface-enhanced Raman spectroscopy (SERS)

The potential-dependent SERS was conducted by combining an *in situ* surface enhanced Raman spectrometer²⁵ with an optical microscope (excitation wavelength 633 nm, sample power 3 mW). A glass carbon electrode, a Pt wire and a Ag/AgCl (saturated KCl) electrode were used as the working, counter and reference electrodes, respectively. During the SERS test, 0.1 M $KHCO_3$ saturated by high-purity CO_2 was continuously fed into the electrolytic cell. Raman spectra were recorded in the range of 100 to 3000 cm^{-1} using a 633 nm laser. The Raman spectra were acquired at about 10 min after the potential was initially applied.

DFT calculations

CASTEP calculation of Materials Studio was used for DFT calculations. We used the Perdew-Burke-Ernzerhof (PBE) exchange correlation functional of the generalized gradient approximation (GGA) with a cutoff energy of 450 eV. A custom-

ized ($3 \times 3 \times 1$) k -point grid was adopted for all the calculations.⁴⁵ The convergence criterion of residual force and energy was set to 0.03 eV \AA^{-1} and 10^{-5} eV in order to avoid the interaction between periodic units during structural relaxation, and the vacuum space in the z direction is larger than 20 \AA . The Cu_2O/Cu interface model is supported by a two-layer Cu (100)-(3 \times 3), four-layer $Cu_2O(100)-(2 \times 2)$ slab or nine-layer $Cu_2O(111)-(2 \times 2)$ slab with 15 \AA vacuum space. The change in free energy was calculated by the computational hydrogen electrode (CHE) method.⁴⁶

Results and discussion

Composition and morphology of Cu_2O nanocatalysts

Cu_2O nanostructures with highly active facets were successfully prepared by a wet chemical reduction method with diverse surfactants. In this process, surfactants play a key role in regulating the exposed crystal facets of Cu_2O by changing the crystallization agent, especially meaning that different types and amounts of surfactant applications lead to crystal growth differential rate and direction, thus laying the foundation for the ultimate morphology of Cu_2O nanostructures. The morphology of as-synthesized Cu_2O was investigated by TEM. As shown in representative TEM images, the as-synthesized F- Cu_2O , O- Cu_2O , and T- Cu_2O nanostructures exhibit the desired face-raised cubic structure (Fig. S1a, ESI†), octahedral structure (Fig. S2a, ESI†) and edge- and corner-truncated octahedral structure (Fig. S3, ESI†). In detail, Fig. S1b† shows the HR-TEM image of the F- Cu_2O catalyst enclosed with excellent crystallinity of the (100) facets. Besides, the F- Cu_2O catalyst possesses uniform particle size distribution, as shown in Fig. S1c.† Similarly, the O- Cu_2O catalyst is composed of the (111) facet (Fig. S2b, ESI†) and the T- Cu_2O catalyst is composed of the (100) and (111) facets (Fig. 1a and d), which are related to the types and amounts of surfactants (PVP and SDS) during the synthesis process. The different d -spacing values of lattice fringes from HR-TEM images also confirm the existence of the abovementioned crystal facets. Fig. 1a, d, and S3† give the TEM, high HR-TEM, and EDS-elemental mapping images of T- Cu_2O viewed along the different zone axis directions, from which it could be found that the T- Cu_2O catalyst is composed of 18 (100) facets and 8 (111) facets. Fig. S3b and e† show the HR-TEM images of the T- Cu_2O catalyst and show the distinct lattice fringes with d spacings of 2.13 and 2.45 \AA , which correspond to the (100) and (111) lattice facets of T- Cu_2O . The lattice plane directions are also in compliance with the respective particle orientation. For the F- Cu_2O catalyst, it shows a cubic shape, which can be assumed that the shape of F- Cu_2O is enclosed with 6 protruded (100) facets with 12 edges. The lattice fringe of the F- Cu_2O catalyst is 2.13 \AA and matches the (100) facet, as shown in Fig. S1b.† For the O- Cu_2O catalyst, it is enclosed with 8 (111) facets, with a lattice spacing of 2.45 \AA corresponding to the (111) facet. Cu_2O nanostructures with different morphologies and facets were characterized by EDS-elemental mapping technique. Fig. S1c, 2c and 3† indicate

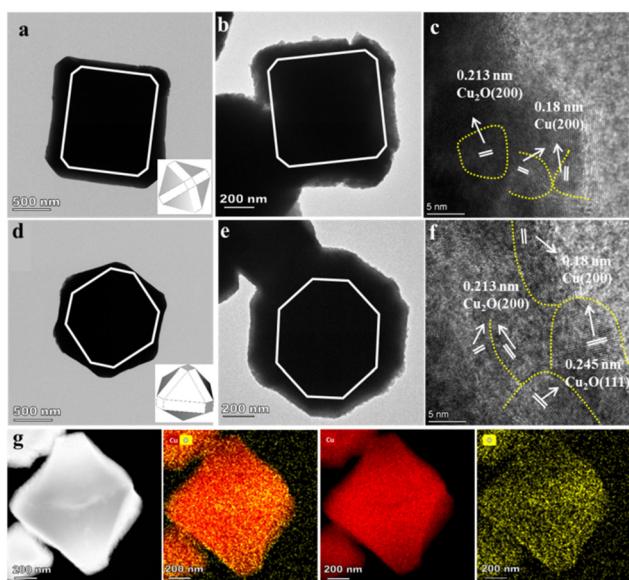


Fig. 1 Structural characterization of catalysts. The TEM images of T-Cu₂O viewed along the (a) [100] and (d) [111] directions, and the (b and e) TEM images, (c and f) HR-TEM images, (g) HAADF-STEM and elemental mapping images (Cu species were in red, and O species were in yellow) of surface-reconstructed T-Cu₂O samples after reduction at -1.1 V vs. RHE.

that Cu and O elements are averagely distributed through Cu₂O catalysts.

The catalysts are reduced at -1.1 V vs. RHE to investigate the surface reconstruction of Cu₂O and the formation of Cu⁺/Cu⁰ interface during CO₂RRs. TEM, HR-TEM and EDS-elemental mapping images of F-Cu₂O, O-Cu₂O and T-Cu₂O catalysts after stability test during CO₂RRs are shown in Fig. 1, S1d-f and S2d-f.† It is clear that Cu₂O structures are well preserved and the Cu⁺/Cu⁰ interface was formed, as revealed from the lattice fringes (Fig. S1e, S2e, 1c and f†). The surface reconstruction of F-Cu₂O, O-Cu₂O and T-Cu₂O catalysts is named F-Cu₂O/Cu, O-Cu₂O/Cu and T-Cu₂O/Cu.

XRD and XPS techniques were used to investigate the crystalline state and chemical valence states of Cu₂O before and after surface reconstruction. As shown in Fig. 2a-c, the three

samples with different exposed active facets are in good agreement with the simulated diffraction patterns of Cu₂O (PDF#05-0667) in the range of 29.55°–77.32°, and the XRD results also show that all the as-prepared Cu₂O catalysts manifest two intensive peaks at 36.4° and 42.3°, which belong to the (111) and (200) facets of Cu₂O before CO₂RRs. In addition, all these peaks are almost unchanged after CO₂RRs and two new peaks appeared at 43.3° and 50.43°, corresponding to the (111) and (200) facets of metallic Cu (PDF# 04-0836). The XRD results demonstrate that the structure of the as-synthesized Cu₂O catalyst is relatively stable, and partial Cu₂O is reduced to Cu, which is consistent with the TEM images. The chemical state of F-Cu₂O, O-Cu₂O, and T-Cu₂O catalysts was further studied by XPS measurement. The XPS results supported by XRD before CO₂RRs show that there are O and Cu elements in all three samples, among which Cu⁺ species appeared in the Cu 2p spectrum, as shown in Fig. S4.† Fig. S4a† reveals that Cu₂O catalysts have a similar sharp Cu⁺ peak at 932.5 eV. The presence of satellite peaks at 945.8 eV also proves the presence of Cu⁺.⁴⁷ In addition, low-intensity characteristic peaks at 933.5 eV and 953.0 eV are associated with Cu²⁺ 2p_{3/2} and Cu²⁺ 2p_{1/2}, respectively, which indicates that there is a small amount of CuO in the Cu₂O nanostructure, due to the natural surface oxidation during the *ex situ* XPS measurement.⁴⁸ Subsequently, the valence states of samples immediately after CO₂RRs was characterized by XPS. After CO₂RRs, the weak peak of Cu²⁺ disappeared (Fig. 2d) and had a main Cu 2p_{3/2} feature at 932.5 eV, which can be vested in either Cu₂O (Cu⁺) or Cu (Cu⁰) but is not distinguishable, as the binding energies between Cu⁺ and Cu⁰ differ by only 0.1 eV (Fig. 2d).⁴⁹ The characteristic peak at 531 eV is related to the existence of lattice oxygen and oxygen vacancies (Fig. 2e). In addition, the Raman spectra (Fig. S5†) of the reconstructed Cu₂O catalysts exhibit an absorption peak around 150 cm⁻¹, which could be ascribed to an oxygen defect excited mode. Fig. 2f provides the Cu LMM spectra to further distinguish Cu⁺ and Cu⁰. The characteristic peak of Cu⁰ at 568.0 eV is presented in the Cu LMM spectrum (Fig. 2f) and the main peak of Cu⁺ is retained (569.9 eV), which further indicates that Cu₂O is reduced only on the surface, but the bulk structure is relatively stable. The surface compositions of Cu⁺ and Cu⁰ on the different Cu₂O catalysts after CO₂RRs are clearly distinguished by Cu LMM spectra and XPS analysis, as shown in Table S1.† The Cu⁺ content of T-Cu₂O catalyst is significantly higher than that of F-Cu₂O and O-Cu₂O catalysts after surface reconstruction.

Catalyst performance

The electrocatalytic CO₂RR performances of F-Cu₂O/Cu, O-Cu₂O/Cu and T-Cu₂O/Cu were also investigated in CO₂-saturated 0.1 M KHCO₃ (pH = 6.8) aqueous solutions in a typical air-tight three-electrode electrochemical system. The electrocatalytic activity of Cu₂O/Cu for CO₂RRs is assessed in a N₂ and CO₂-saturated 0.1 M KHCO₃ solution by linear sweep voltammetry (LSV), respectively, and the LSV curves are recorded with a sweep speed of 20 mV s⁻¹ in the potential range from 0 to -1.4 V (vs. RHE). Obviously, the total current densities of

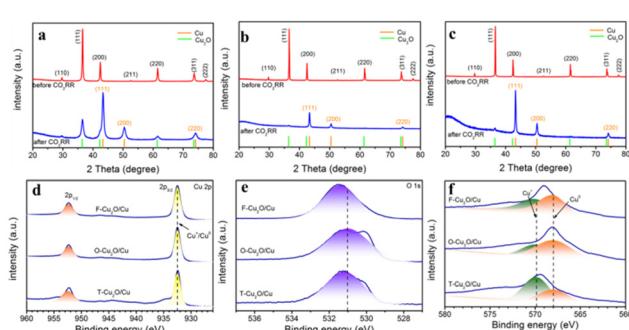


Fig. 2 XRD patterns of catalysts: (a) F-Cu₂O, (b) O-Cu₂O and (c) T-Cu₂O. XPS spectra of (d) Cu 2p, (e) O 1s and (f) Cu LMM of F-Cu₂O, O-Cu₂O and T-Cu₂O after CO₂RRs at -1.1 V vs. RHE until stable.

three $\text{Cu}_2\text{O}/\text{Cu}$ catalysts are all higher in CO_2 -saturated electrolytes than those in N_2 -saturated electrolytes, as shown in Fig. S6,† which suggests that the electrocatalytic activity of the catalysts for CO_2 RRs is better than that for hydrogen evolution reactions (HERs).⁵⁰ In addition, the LSV curves (Fig. 3a) exhibit the onset potentials decreasing following the order of $\text{T-Cu}_2\text{O}/\text{Cu} > \text{F-Cu}_2\text{O}/\text{Cu} > \text{O-Cu}_2\text{O}/\text{Cu}$, indicating that the onset potential and the electrocatalytic activity of $\text{T-Cu}_2\text{O}/\text{Cu}$ catalyst are higher than those of the other two catalysts. Moreover, the electrochemical double-layer capacitance measurement was implemented to evaluate the electrochemical surface area (ECSA) of $\text{Cu}_2\text{O}/\text{Cu}$ catalysts. According to CV curves at different scanning rates, the ECSA of catalysts was obtained through calculating the double-layer capacitance (C_{dl}) of the catalysts. $\text{T-Cu}_2\text{O}/\text{Cu}$ exhibits the largest ECSA value among the three catalysts (Fig. S7†), which indicates that $\text{T-Cu}_2\text{O}/\text{Cu}$ can provide a more accessible active site as compared with the other catalysts. Gas chromatography (GC) and ^1H NMR spectroscopy (Fig. S8, S9 and Table S2†) are used to analyze the effluent gaseous products and liquid products formed in CO_2 RRs at different applied potentials between -0.8 and -1.2 V vs. RHE. The products from CO_2 RR and the relevant faradaic efficiencies are displayed in Fig. 3b. Compared with the electrocatalytic performances of $\text{Cu}_2\text{O}/\text{Cu}$ catalysts, $\text{T-Cu}_2\text{O}/\text{Cu}$ exhibits better activity and electrocatalytic conversion efficiency than those of $\text{F-Cu}_2\text{O}/\text{Cu}$ and $\text{O-Cu}_2\text{O}/\text{Cu}$. Specifically, the total faradaic efficiency reaches 97.8% over $\text{T-Cu}_2\text{O}/\text{Cu}$ at -1.1 V vs. RHE. Notably, the C_{2+} products of CO_2 RRs are mainly C_2H_4 and $\text{C}_2\text{H}_5\text{OH}$ on the three $\text{Cu}_2\text{O}/\text{Cu}$ samples and the maximum FE of C_{2+} products achieve 69.0% at $\text{T-Cu}_2\text{O}/\text{Cu}$. The FE values of C_2H_4 and H_2 on $\text{T-Cu}_2\text{O}/\text{Cu}$ as a function of applied potential are compared in Fig. 3c. As presented, $\text{T-Cu}_2\text{O}/\text{Cu}$ displays the highest selectivity to C_2H_4 , achieving 58.0% at -1.1 V vs. RHE, while $\text{F-Cu}_2\text{O}/\text{Cu}$ and

$\text{O-Cu}_2\text{O}/\text{Cu}$ reach 24.9% and 11.2%, respectively. The evolution of H_2 is inhibited by $\text{T-Cu}_2\text{O}/\text{Cu}$, and the FE of H_2 is less than 30% in the whole potential range. Therefore, the $\text{T-Cu}_2\text{O}/\text{Cu}$ catalyst has high selectivity for CO_2 RRs to C_{2+} products. The detailed faradaic efficiencies for all products at various potentials are listed in Fig. S10.† It is apparently noted that the selectivity of the products varied with the applied potentials. CO was found to be the major product at relatively low overpotentials (from -0.8 to -0.9 V vs. RHE). With the applied potential being more negative, the FEs for CO production decrease and the FEs for ethylene production increase. This is consistent with the widely accepted hypothesis that the adsorbed CO is an intermediate in the formation of C_{2+} products.^{51,52} In addition, the electrocatalytic performance of $\text{T-Cu}_2\text{O}/\text{Cu}$ is significantly better than that of Cu-based catalysts reported in the literature under similar experimental conditions (Table S3†).^{53–61}

To gain more accurate facet features of the Cu_2O catalysts, we applied electrochemical adsorption of OH^- on the Cu_2O catalysts before and after reconstruction, which take into account their facet-dependent OH^- adsorption behaviors.⁶² As shown in Fig. S11a,† the cyclic voltammetry (CV) curves of the three Cu_2O catalysts before reconstruction did not exhibit the OH^- adsorption/desorption peaks. As for the reconstructed Cu_2O samples, the CV curves show OH^- adsorption peaks at -0.34 and -0.43 V vs. RHE for $\text{F-Cu}_2\text{O}/\text{Cu}$ and $\text{O-Cu}_2\text{O}/\text{Cu}$, which can be assigned to the OH^- adsorption on the $\text{Cu}(100)$ and $\text{Cu}(111)$ surfaces,⁶³ respectively. Such two adsorption peaks exist simultaneously on the $\text{T-Cu}_2\text{O}/\text{Cu}$ catalyst, manifesting that $\text{T-Cu}_2\text{O}/\text{Cu}$ is dominated by both the $\{100\}$ and $\{111\}$ facets (Fig. S11b†). Above all, it can be considered that metallic Cu with the corresponding crystal facets is generated on the surface of the reconstructed Cu_2O samples.

The stability is an important factor during CO_2 RRs in practical application. The electrocatalytic stability of the $\text{T-Cu}_2\text{O}/\text{Cu}$ catalyst for CO_2 RR was examined under -1.1 V vs. RHE for 10 h in 0.1 M KHCO_3 by chronopotentiometry technique. The stability result of $\text{T-Cu}_2\text{O}/\text{Cu}$ catalyst is given in Fig. 3d, which implies that the $\text{T-Cu}_2\text{O}/\text{Cu}$ catalyst has good working stability. It is also noticeable that the increase in $\text{FE}_{\text{C}_2\text{H}_4}$ is greatest between initial one and two hours and then decreases slightly. Furthermore, the FE for C_2H_4 reaches a maximum value of 58.0% when the reduction time is 2 h, indicating that CO_2 RR performance is stable in the long-term test. The electrocatalytic durability of the $\text{T-Cu}_2\text{O}/\text{Cu}$ catalyst was further valued by cycling 2000 cycles between -1.4 and 0 V vs. RHE at a scan rate of 50 mV s⁻¹. As shown in Fig. S12,† the test results showed only a slight decrease in activity at high potentials. The IR and PXRD patterns (Fig. S13 and 14†) of the recycled catalysts showed that the three catalysts can be well maintained during the catalytic reaction.

CO_2 electroreduction mechanisms on $\text{Cu}_2\text{O}/\text{Cu}$ catalysts

It is widely accepted that CO_2 RRs to multi-carbon products experience a critical CO dimerization step.^{64,65} We thus compared the coverage of surface-adsorbed CO (* CO) on $\text{T-Cu}_2\text{O}/\text{Cu}$

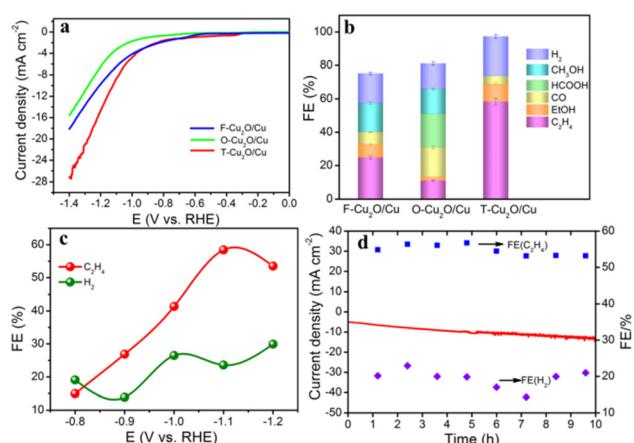


Fig. 3 Electrocatalytic CO_2 RR performance. (a) LSV curves in a 0.1 M KHCO_3 aqueous solution saturated with CO_2 for $\text{Cu}_2\text{O}/\text{Cu}$ catalysts; (b) faradaic efficiencies of various products at -1.1 V vs. RHE; (c) contrast of $\text{FE}_{\text{C}_2\text{H}_4}$ and FE_{H_2} for CO_2 RRs catalyzed by $\text{T-Cu}_2\text{O}/\text{Cu}$ at different applied potentials (-0.8 V to -1.2 V vs. RHE); and (d) stability of $\text{T-Cu}_2\text{O}/\text{Cu}$ at a potential of -1.1 V vs. RHE for 10 h.

Cu, F-Cu₂O/Cu, and O-Cu₂O/Cu catalysts by *in situ* Raman spectroscopy at an open circuit potential (OCP) and between -0.5 and -0.9 V vs. RHE from 250 to 650 cm^{-1} and 1550 to 2800 cm^{-1} , and this technique showed good sensitivity to *CO intermediates. In *in situ* Raman spectroscopy (Fig. S15†), low potentials were employed because the intermediate could be retained and there were not many bubbles on the electrode to affect the Raman spectral signal. As shown in Fig. 4a–c, the characteristic peaks were located at 218 , 527 and 623 cm^{-1} , corresponding to Cu₂O at the OCP. At the reduction potential from -0.5 V to -0.9 V vs. RHE, the peaks at 360 , 532 and 1070 cm^{-1} were assigned to the Cu–CO stretching mode, Cu–CO, the adsorbed OH group (vibration of Cu–OH), and CO₃²⁻ modes,⁶⁶ respectively, indicating the presence of Cu. XRD and XPS results also confirmed the existence of Cu peaks (Fig. 2). With the increase in applied potentials, two noticeable Raman peaks appeared on the T-Cu₂O/Cu electrode (Fig. 4d), where the peak at $\sim 2070\text{ cm}^{-1}$ originated from the stretching vibration mode of absorbed CO* at the top site.^{67,68} The peak at $\sim 1980\text{ cm}^{-1}$ could be attributable to the interaction between absorbed CO* intermediates,^{69,70} which benefited C₂₊ production. However, as for F-Cu₂O/Cu and O-Cu₂O/Cu, the *CO peak at a lower shift was so weak that could not be observed clearly. There was only the single mode at $\sim 2070\text{ cm}^{-1}$, manifesting a less favorable C–C coupling on the two electrodes (Fig. 4e and f), which was consistent with the electrochemical CO₂RR results that it mainly produced CH₃OH/H₂ and could not produce much C₂H₄ products.⁷¹ Moreover, both Raman signals disappeared on the T-Cu₂O/Cu electrode at high potentials, indicating that these intermediates reacted to CO₂ reduction kinetics at very fast rates.

DFT calculation

To gain deeper insights into the high selectivity of C₂H₄ on T-Cu₂O/Cu with the (111)/(100) facet compared with F-Cu₂O/Cu with the (100) facet and O-Cu₂O/Cu with the (111) facet catalysts, the DFT calculation was carried out to study the free energy of *CO intermediates on Cu₂O/Cu with the (111), (100) and (111)/(100) facet. F-Cu₂O/Cu(100), O-Cu₂O/Cu(111) and T-Cu₂O/Cu(111)/(100) models were built based on our HR-TEM

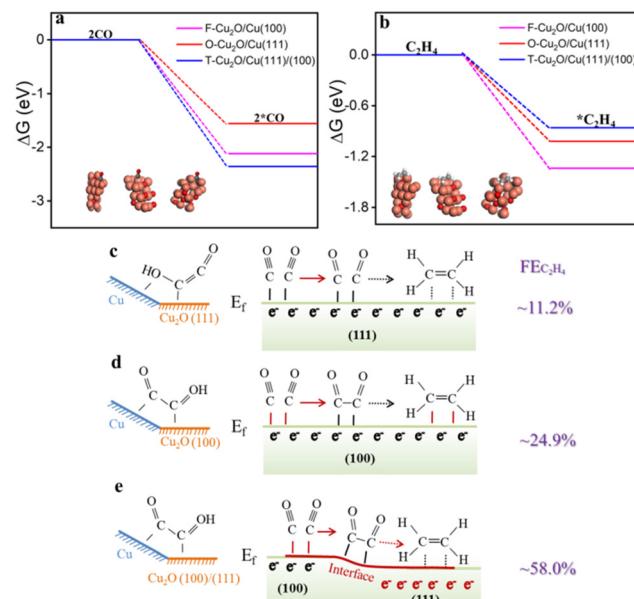


Fig. 5 Adsorption energies of (a) CO and (b) C₂H₄ on F-Cu₂O/Cu(100), O-Cu₂O/Cu(111) and T-Cu₂O/Cu(111)/(100) catalysts. Formation of C₂H₄ on (c) O-Cu₂O/Cu(111), (d) F-Cu₂O/Cu(100) and (e) T-Cu₂O/Cu(111)/(100) catalysts.

results to explore the mechanism of CO₂RRs in depth. Fig. 5 shows that the adsorption of *CO intermediate on the surface of Cu₂O/Cu(100) and Cu₂O/Cu(111)/(100) catalysts was stronger than that on Cu₂O/Cu(111), which would subsequently promote the C–C coupling to produce C₂₊ products in the CO₂RR process, and was consistent with the *in situ* Raman result (Fig. 4d–f). In addition, the adsorption of C₂H₄ on Cu₂O/Cu(111)/(100) and Cu₂O/Cu(111) was weaker than that on Cu₂O/Cu(100), indicating that Cu₂O/Cu(100) could promote the C–C coupling to generate C₂₊ products, but the C₂₊ products formed (e.g., C₂H₄) were difficult to escape from the surface of Cu₂O/Cu(100) due to the strong adsorption ability of C₂H₄. Associated with the experimental results, the synergistic effect of Cu⁰ and Cu⁺ was the activation of CO₂ on the Cu⁰ site to promote the following electron transfers, and strengthen the *CO adsorption on the Cu⁺ site to further facilitate C–C coupling. According to Cu LMM results after reconstruction (see Table S1, ESI†), the T-Cu₂O/Cu sample has more Cu⁺ active sites than the other two catalysts, so *CO adsorption on the T-Cu₂O/Cu catalyst is stronger and can further promote C–C coupling.³² Although the adsorption ability of the *CO intermediate on O-Cu₂O/Cu(100) was low, C₂H₄ could be desorbed from the surface of O-Cu₂O/Cu(100), due to its weak adsorption energy. Moreover, the *CO intermediate could not only be strongly adsorbed on the surface of T-Cu₂O/Cu(111)/(100) to facilitate the C–C coupling, but also C₂H₄ formed was easily desorbed from the surface of T-Cu₂O/Cu(111)/(100). Besides, T-Cu₂O/Cu(111)/(100) had better catalytic performance than F-Cu₂O/Cu(100) and O-Cu₂O/Cu(111), which might be related to the fact that the Fermi energy level of Cu₂O on the (111)

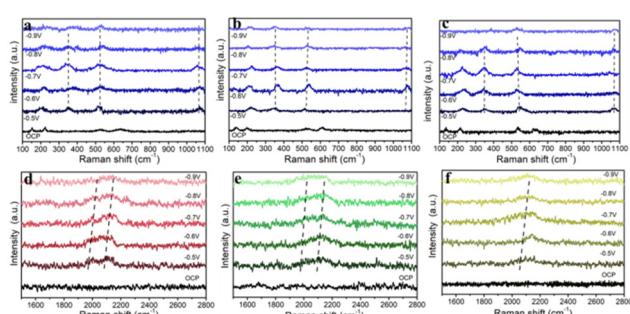


Fig. 4 *In situ* Raman spectra of CO₂RR over (a and d) T-Cu₂O/Cu, (b and e) F-Cu₂O/Cu and (c and f) O-Cu₂O/Cu as a function of the applied potentials.

facet was lower than that on the (100) facet, which promoted the charge transfer between the Cu₂O (111) and (100) facets and further facilitated the multi-electron participation kinetics of C₂H₄ formation (Fig. 5c–d).

Conclusion

In summary, F-Cu₂O, O-Cu₂O and T-Cu₂O catalysts enclosed with the (111), (100) and (111)/(100) facets have been synthesized by a wet chemical reduction method, which has been reconstructed *in situ* to form F-Cu₂O/Cu(100), O-Cu₂O/Cu(111) and T-Cu₂O/Cu(111)/(100) catalysts. The experimental results indicated that the T-Cu₂O/Cu catalyst shows maximum FE_{C₂H₄} values of 58.0% for CO₂RRs at -1.1 V *vs.* RHE, which is much better than those of the F-Cu₂O/Cu catalyst (24.9%) and O-Cu₂O/Cu catalyst (11.2%). The combination of *in situ* spectroscopy, electrochemical measurement and DFT calculation results revealed that the faradaic efficiencies of C₂H₄ on reconstructed Cu₂O catalysts is related to the exposure of highly active facets and the synergistic effect of Cu⁺ and Cu⁰ (Cu⁺/Cu⁰) generated *in situ*, which can enhance the *CO adsorption and decrease the activation energy of C–C coupling, thus improving the selectivity of the C₂H₄. This study will pave a feasible pathway for electrochemical energy storage and convention by crystal facet engineering and interface engineering.

Conflicts of interest

The authors declare no conflict of interest.

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