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ZSM-5-confined Cr₁–O₄ active sites boost methane direct oxidation to C1 oxygenates under mild conditions†

 Mengyu Zeng,^{‡,ab} Lu Cheng,^{‡,cd} Qingqing Gu,^{‡,e} Bing Yang,^{id e} Baiyang Yu,^{ab} Jing Xu,^f Ying Zhang,^{ab} Chengsi Pan,^{id ab} Xiao-Ming Cao,^{id *cd} Yang Lou^{id *ab} and Yongfa Zhu^g

Direct oxidation of methane (DOM) to value-added chemicals is of great significance but is still challenging under mild conditions. Herein, we report that Cr₁–O₄ as an active site in a ZSM-5 anchored Cr single atom catalyst (Cr₁/ZSM-5 SAC) can efficiently catalyse the DOM to form value-added C1 oxygenated products with a productivity of 21100 μmol g_{cat}⁻¹ h⁻¹ and a selectivity of 99.8% at 50 °C within 30 min, which outperforms most reported state-of-the-art catalysts. Density functional theory (DFT) calculations and experimental results show that Cr₁ atoms anchored on the wall of ZSM-5 micropores form the Cr₁–O₄ active sites, which boosts the formation of the reactive oxygen species (adsorbed OH species) and the activation of a C–H bond in CH₄. We believe that our atomic-level design strategy on a non-noble metal offers an approach to rationally design efficient catalysts for methane conversion.

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Broader context

Transforming methane to high-value oxygenated products (like CH₃OH, HCCOH *etc.*) is highly attractive. Traditionally, methane conversion can be achieved through an indirect process that couples methane reforming and a Fischer–Tropsch synthesis but such an indirect route normally requires high pressures (up to 30 bar) and temperatures (1100–1300 K) with large energy inputs. Alternatively, the direct oxidation of methane (DOM) to form value-added oxygenates is considered as a potential way to efficiently and economically convert methane into commercial chemicals and fuels but remains a major challenge to simultaneously obtain high activity and selectivity. In this present work, we report a ZSM-5 supported non-noble Cr single atom catalyst as a proof-of-concept catalyst (Cr₁/ZSM-5 SAC) with a unique Cr₁–O₄ entity as the active site to selectively and efficiently convert methane to HCOOH and other value-added C1 oxygenates under mild conditions.

Introduction

Transforming methane (the main composition of natural gas) into high-value oxygenated products (formic acid, methanol, *etc.*) is highly attractive.^{1–3} Traditionally, methane conversion can be achieved through an indirect process that couples methane reforming and a Fischer–Tropsch synthesis⁴ but such an indirect route normally requires high pressures (up to 30 bar) and temperatures (1100–1300 K) with large energy inputs.⁵ Alternatively, the direct oxidation of methane (DOM) to value-added oxygenated products by selective oxidation of CH₄ is a more economical and environmentally friendly route than that of the indirect route.⁶ However, the DOM remains highly challenging since it is very difficult to balance the activation of a C–H bond in CH₄ with the oxidation capability of the active oxygen species. As a result, the practical application of the DOM is inhibited by the low productivity and selectivity. Hence, designing novel catalysts with high productivity and selectivity for the DOM is highly important.

^a Key Laboratory of Synthetic and Biological Colloids, Ministry of Education, School of Chemical and Material Engineering, Jiangnan University, Wuxi, Jiangsu, 214122, China. E-mail: yang.lou@jiangnan.edu.cn

^b International Joint Research Center for Photoresponsive Molecules and Materials, Jiangnan University, Wuxi, Jiangsu 214122, China

^c Key Laboratory for Advanced Materials and Feringa Nobel Prize Scientist Joint Research Center, School of Chemistry and Molecular Engineering, East China University of Science and Technology, Shanghai, 200237, China. E-mail: xmcao@ecust.edu.cn

^d Centre for Computational Chemistry and Research Institute of Industrial Catalysis, East China University of Science and Technology, Shanghai, 200237, China

^e Dalian National Laboratory for Clean Energy, Dalian Institute of Chemical Physics, 457 Zhongshan Road, Dalian, 116023, China

^f School of Food Science and Technology, Jiangnan University, Wuxi, Jiangsu 214122, China

^g Department of Chemistry, Tsinghua University, Beijing 100084, China

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[‡] These authors contribute equally to the article.


Single-atom catalysts (SACs) that possess fully exposed active atoms and high homogeneity of the active site enable a significant boost in the selective conversion of various chemical transformations compared with nanocluster and nanoparticle catalysts.^{7,8} Especially, the M_1-O_x entity stabilized by the oxygen moieties of appropriate supports as active sites possesses a unique catalytic capability for methane selective conversion.^{9–11} For example, the Pd_1-O_4 entity anchored on the internal surface of microporous ZSM-5 can convert CH_4 to methanol or methyl peroxide.¹⁰ The Rh_1-O_5 entity decorated in ZSM-5 frameworks can efficiently catalyse CH_4 to CH_3COOH and CH_3OH by introducing CO and O_2 at 150 °C, which is around 1000 times higher than that of unsupported Rh cations.¹¹ However, non-noble metal based catalysts for the DOM with excellent catalytic performance under mild reaction are still rarely reported.^{12,13}

Herein, we report that atomically-dispersed chromium sites anchored on ZSM-5 can efficiently catalyse the DOM and achieve a yield of 21 100 $\mu\text{mol g}_{\text{cat}}^{-1} \text{h}^{-1}$ with a selectivity of 99.8% for value-added C1 oxygenated products ($HCOOH$, CH_3OH , CH_3OOH and $CH_2(OH)_2$) with H_2O_2 as the oxidant at 50 °C, which outperforms most reported state-of-the-art catalysts under similar reaction conditions (Table S1, ESI†). DFT and experimental results indicate that Cr_1-O_4 as the active site of the $Cr_1/ZSM-5$ SACs promotes the formation of the reactive oxygen species (adsorbed OH group) and the activation of a C–H bond in CH_4 , thereby enhancing the yield of the DOM.

Results and discussion

The $Cr_1/ZSM-5$ SAC was synthesized *via* a modified adsorption method by finely tuning the adsorption parameters of the metal precursors in the ethanol solution (details shown in the ESI†).¹⁴ The XRD patterns of the $Cr_1/ZSM-5$ SAC suggest that the original crystal structure of H-ZSM-5 is maintained, indicating that the metal species do not change the lattice structure of H-ZSM-5 (Fig. S1, ESI†). In addition, no characteristic peaks of Cr particles are observed from XRD, which reveals that the chromium species are highly dispersed in H-ZSM-5. To probe the morphology and structure information of the $Cr_1/ZSM-5$ SAC at the atomic level, aberration-corrected high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) was used. The low-dose HAADF-STEM images indicate that isolated Cr atoms are uniformly dispersed on ZSM-5 (Fig. 1a). No Cr particles or clusters can be observed in the fresh $Cr_1/ZSM-5$ SAC as shown in the low magnification HAADF-STEM images (Fig. S2, ESI†). The energy dispersive spectroscopy (EDS) elemental maps further confirm that the Cr species are atomically dispersed in selected regions of the $Cr_1/ZSM-5$ SAC (Fig. 1c and d). By examining numerous low/high magnification HAADF-STEM images and back-scattered electron images obtained from different areas of the $Cr_1/ZSM-5$ SAC, we conclude that the as-synthesized $Cr_1/ZSM-5$ SAC contains only isolated Cr atoms that are anchored onto ZSM-5. For the used $Cr_1/ZSM-5$ SAC (50 °C for 0.5 h), the atomically dispersed Cr species are still retained and no Cr clusters and nanoparticles are

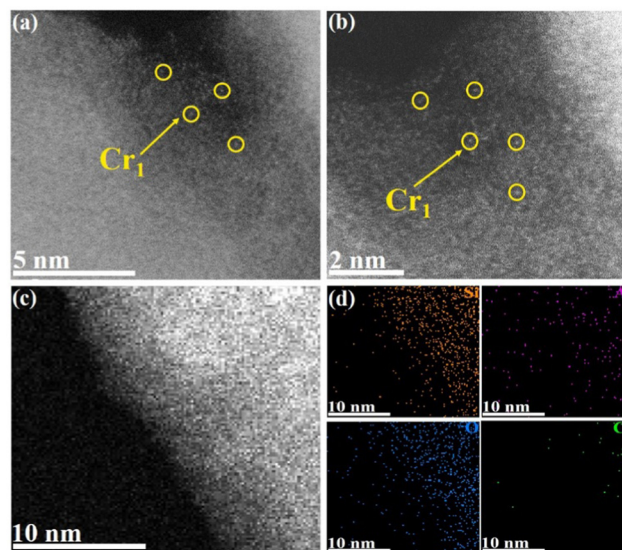


Fig. 1 Catalytic structural characterizations of the $Cr_1/ZSM-5$ SAC in methane oxidation under mild conditions. HAADF-STEM images of the synthesized $Cr_1/ZSM-5$ SAC at different magnifications (a–c) and once it had been used (b). The blue circles show single Cr atoms in the matrix of ZSM-5. Energy dispersive spectroscopy (EDS) mapping images of the $Cr_1/ZSM-5$ SAC in figure (d).

observed (Fig. 1b and Fig. S3, S4, ESI†), which reveals that the Cr_1 atoms are stably anchored on ZSM-5 and also supports the idea that the measured catalytic activity is originally from the isolated Cr atoms rather than the Cr clusters or particles.

For comparison studies, a $Cr/ZSM-5-NP$ sample composed of Cr particles dispersed on ZSM-5 was prepared (with a loading of 1.33 wt%). The average size of the Cr particles was 3.0 ± 0.6 nm, and the spatial distributions of the Cr particles in the $Cr/ZSM-5-NP$ are shown in Fig. S5 (ESI†).

To further explore the electronic state of Cr species, UV-Vis diffuse reflectance spectroscopy (DRS) was conducted as shown in Fig. S6 (ESI†). For the $Cr/ZSM-5$ NP, the broad absorption bands at ~ 458 nm and ~ 600 nm are associated with the $A_{2g}-T_{1g}$ and $A_{2g}-T_{2g}$ transitions of Cr(III) in octahedral symmetry respectively, which is the typical characteristic absorption band of the octahedral Cr^{3+} species in CrO_x clusters or in Cr_2O_3 .^{15–17} The absence of such an absorption band in the $Cr_1/ZSM-5$ SAC indicates that the Cr species are atomically dispersed on ZSM-5 (Fig. S2, ESI†), which corroborates the HAADF-STEM and elemental mapping results.

To investigate the chemical structure and electronic states of the Cr species in the $Cr_1/ZSM-5$ SAC, Fourier transform extended X-ray absorption fine structure (FT-EXAFS) in R space was performed (Fig. 2a). To accurately reveal the local coordination environment of the Cr species in the $Cr_1/ZSM-5$ SAC, the standard crystal model for the DFT simulations was used to fit the EXAFS data. The fitted data fits the original EXAFS data of Cr species well, which secures that the fitted results are reliable and enable us to accurately demonstrate the local structure of the Cr species in the $Cr_1/ZSM-5$ SAC. There is only a Cr–O peak located at 1.50 Å for the $Cr_1/ZSM-5$ SAC, without any Cr–Cr or



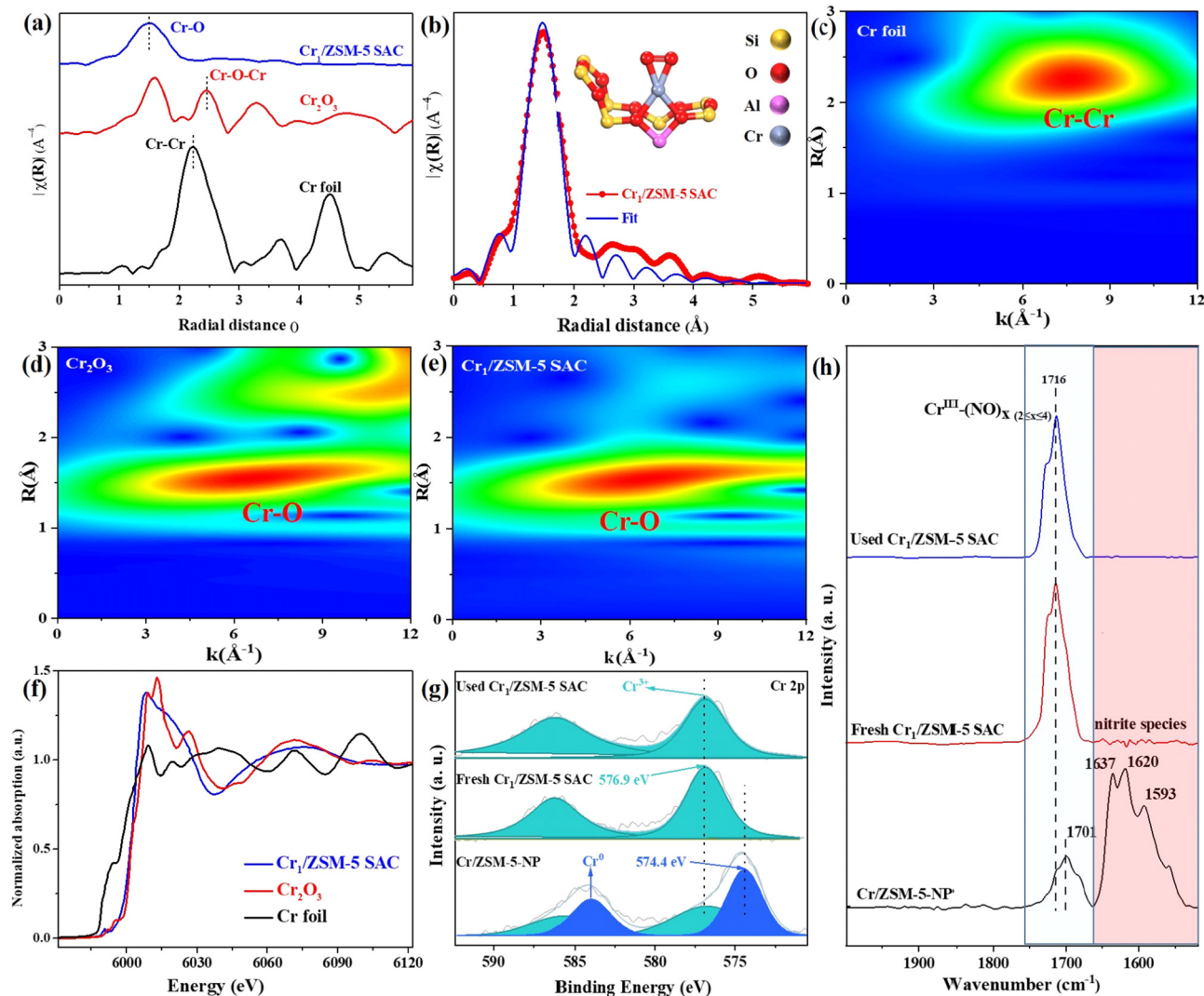


Fig. 2 Coordination structure and chemical state of the Cr/ZSM-5 catalysts. (a) The k^3 -weighted Cr K-edge Fourier transform EXAFS spectra of the Cr₁/ZSM-5 SAC as well as Cr foil and Cr₂O₃ references. (b) Experimental and fitting Cr K-edge EXAFS curves of the Cr₁/ZSM-5 SAC. (c) *In situ* NO-DRIFTS spectra adsorbed on Cr/ZSM-5-NP, the fresh Cr₁/ZSM-5 SAC and the used Cr₁/ZSM-5 SAC at 30 °C. (d) Cr K-edge X-ray absorption near-edge structure (XANES) spectra. (e) Cr K-edge XANES spectra of the fresh Cr₁/ZSM-5 SAC, the used Cr₁/ZSM-5 SAC after reaction and Cr/ZSM-5 NP. The WT-EXAFS plot of Cr foil (f), Cr₂O₃ (g), and the Cr₁/ZSM-5 SAC (h).

Cr–O–Cr peaks (from 2.00 Å to 3.00 Å), which suggests that the Cr₁/ZSM-5 SAC mainly contains atomically dispersed Cr atoms instead of nanoparticles or multi-core clusters, and further verifies the results of the HAADF-STEM, elemental mapping and UV-vis DRS. In addition, the detailed fitting data reveals that each Cr₁ atom is coordinated to four oxygen atoms (coordination number: 3.9 ± 0.1) as shown in Fig. 2b. Therefore, the Cr₁–O₄ configuration describes the nearest-neighbor environment of the Cr₁ atoms in the Cr₁/ZSM-5 SAC. The fitting details are displayed in Table S2 (ESI[†]).

To reveal the atomic dispersion of the Cr species in the Cr₁/ZSM-5 SAC more clearly, a wavelet transform (WT) of the Cr K-edge EXAFS oscillations was analyzed. For the Cr₁/ZSM-5 SAC, the strong WT maximum focuses at approximately 6.0 \AA^{-1} (Fig. 2c–e), which clearly distinguishes it from WT contour plots of Cr foil (Cr–Cr, $k = 8.0 \text{ \AA}^{-1}$) and Cr₂O₃

(Cr–O, $k = 6.3 \text{ \AA}^{-1}$). These results further confirm that the Cr species are atomically dispersed on the Cr₁/ZSM-5 SAC.

To probe the electronic states of the isolated Cr species in the Cr₁/ZSM-5 SAC, the X-ray absorption near edge structure (XANES) is investigated. The white-line intensity of the Cr species in the Cr₁/ZSM-5 SAC is slightly higher than that of Cr foil (Fig. 2f), which reveals that the Cr₁ atoms are in an oxidative state.¹⁸ Moreover, the absorption edge of the Cr₁/ZSM-5 SAC is higher than that of Cr foil and close to that of Cr₂O₃, which further indicates that the Cr species are in a high oxidation state (close to +3). X-ray photoelectron spectroscopy (XPS) was further used to probe the oxidation state of isolated Cr species (Fig. 2e). The detailed analysis of the XPS data indicates that the oxidation state of the Cr₁ atoms in the Cr₁/ZSM-5 SAC is +3 (peak centered at 576.9 eV in the spectra of Cr 2p_{3/2}), which is in line with the XANES data. The Cr



species in the Cr/ZSM-5 NP sample possess two oxidation states:¹⁸ a peak centered at 576.9 eV, assignable to Cr³⁺, and a peak centered at 574.4 eV, assignable to Cr⁰. The XPS data clearly confirms that the electronic state of the isolated Cr species in the Cr₁/ZSM-5 SAC is obviously different from that of the Cr particles/clusters in Cr/ZSM-5-NP. Furthermore, the binding energy of the Cr species in the used Cr₁/ZSM-5 SAC is similar to that of Cr species in the fresh Cr₁/ZSM-5 SAC, which further verifies that the Cr₁ atoms are stably anchored on ZSM-5.

In situ diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) of NO adsorption was used to further identify the microscopic properties of the active sites in the Cr/ZSM-5 samples. For NO adsorption on the Cr/ZSM-5-NP sample (Fig. 2f), the band centered at 1701 cm⁻¹ is associated with the stretching mode of NO on the isolated Cr sites (Cr₁-(NO)_{x≥2} nitrosyl species)^{19–21} and the peaks centered at 1637 cm⁻¹ (bridge nitrate), 1620 cm⁻¹ (monodentate nitrates) and 1593 cm⁻¹ (bidentate nitrate) are associated with the bridged adsorption mode of NO (bridging nitrate) on the multiple Cr sites.^{22–25} These results corroborate the TEM imaging results that the Cr species exist mainly in the form of nanometer-sized Cr particles (3.0 ± 0.6 nm) dispersed on ZSM-5 (Fig. S6, ESI†). For NO adsorption on the fresh Cr₁/ZSM-5 SAC sample, the peak at 1716 cm⁻¹ corresponds to the NO adsorption on isolated Cr sites (forming Cr₁-(NO)_{x≥2} nitrosyl species)^{19–21} and the bridged adsorption mode of NO is absent, which indicates that the Cr species are mainly in the form of single atoms in the Cr₁/ZSM-5 SAC. Compared with the Cr/ZSM-5-NP sample, the obvious blueshift

of Cr₁-(NO)_{x≥2} nitrosyl species by 15 cm⁻¹ on the Cr₁/ZSM-5 SAC reveals that the Cr₁ atoms possess a much higher oxidation state, which is in line with the XPS and XANES data. For NO adsorption over the used Cr₁/ZSM-5 SAC, there is only one peak at 1716 cm⁻¹ associated with the NO adsorption on isolated Cr sites and the bridging nitrate associated with the NO molecules adsorbed on multiple Cr sites is not observed (Fig. 2c), which further confirms that the Cr₁ atoms are stably anchored on ZSM-5.

To investigate the catalytic performance of the Cr₁/ZSM-5 SAC, the DOM is conducted in a batch reactor with H₂O₂ as the oxidant. By optimizing the DOM reaction conditions including Cr loading, temperature, methane pressure and amounts of H₂O₂, the highest catalytic performance was achieved for the Cr₁/ZSM-5 SAC at 3 MPa and 50 °C under the reaction conditions of 0.5 M H₂O₂ (Fig. S7, ESI†). For the DOM over the Cr₁/ZSM-5 SAC, the productivity of the C1 oxygenates that are mainly composed of HCOOH, CH₃OH, CH₃OOH and CH₂(OH)₂ is 21, 100 μmol g_{cat.}⁻¹ h⁻¹ with a total selectivity of 99.8% in all the products at 50 °C within 30 min (Fig. 3a), which surpasses most state-of-the-art catalysts reported in the literature (Table S1, ESI†). The compositions of gas-phase and liquid-phase products were analyzed and quantified by gas chromatography and nuclear magnetic resonance (Fig. S8 and S9, ESI†). The productivity of the C1 oxygenates over the Cr₁/ZSM-5 SAC is around 1.5 times higher than that of the highest catalyst (Cu-Fe/ZSM-5) under similar reaction conditions (50 °C) in the literature.²⁶

For the DOM reaction over H-ZSM-5 at 50 °C (Fig. 3a), the productivity of the C1 oxygenates is only 432 μmol g_{cat.}⁻¹ h⁻¹

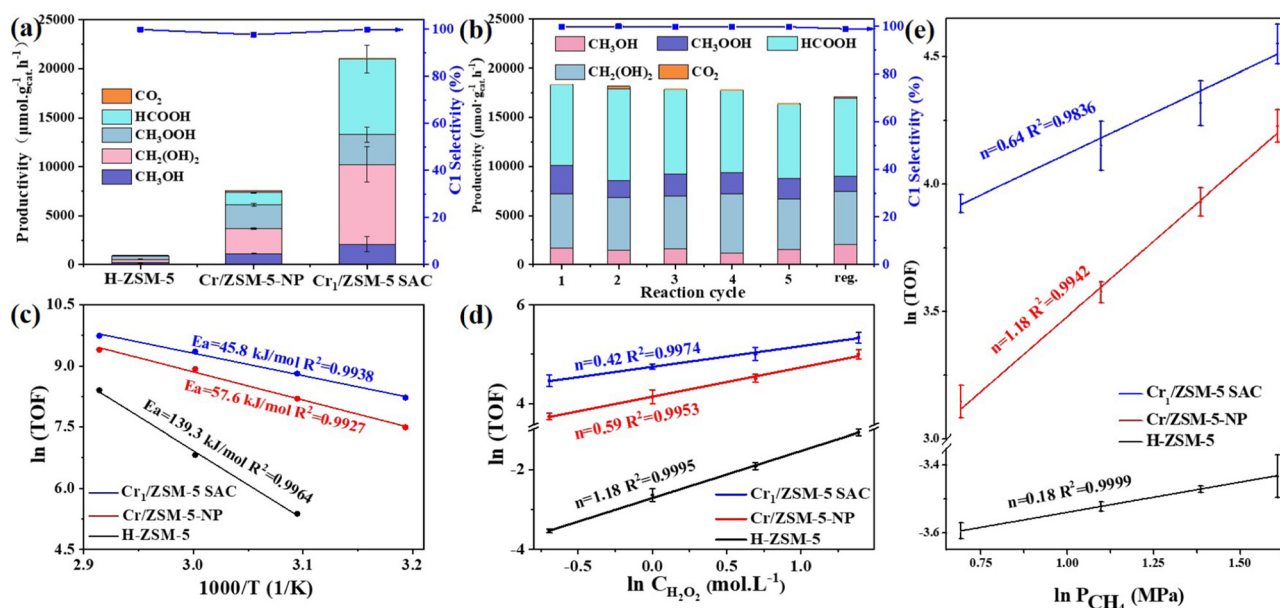


Fig. 3 Catalytic performances and kinetic parameters of the Cr/ZSM-5 samples for the DOM. The product distribution and selectivity of the DOM on pure H-ZSM-5, Cr/ZSM-5-NP and the Cr₁/ZSM-5 SAC (a); recycle performance and regeneration of the Cr₁/ZSM-5 SAC (b). (c) Arrhenius plots (apparent activation energy, E_a) of the Cr₁/ZSM-5 SAC (blue line), Cr/ZSM-5-NP (red line) and pure H-ZSM-5 (black line) in the temperature (T) range of 40 to 70 °C with 10 °C increments. (d) Reaction order (n) for the H₂O₂ on the Cr₁/ZSM-5 SAC (blue line), Cr/ZSM-5-NP (red line) and pure H-ZSM-5 (black line) in a H₂O₂ initial concentration range of 0.5 to 4 M. (e) Reaction order (n) for the CH₄ on the Cr₁/ZSM-5 SAC (blue line), Cr/ZSM-5-NP (red line) and pure H-ZSM-5 (black line) in a CH₄ pressure range of 20 to 50 bars with 10 bars increments. (Reaction condition: 10 mg catalysts; 40–70 °C; P(CH₄) of 20–50 bars; 0.5–4 M H₂O₂; 0.5 h; 10 mL; 1,500 rpm.) The error bars are defined as standard deviations of three experiments.



within 30 min and the major product is methyl hydroperoxide, around 48.9 times lower than that of the Cr₁/ZSM-5 SAC. To verify the existing form of the active Cr species, the DOM was conducted on commercial Cr₂O₃. The productivity of commercial Cr₂O₃ for C1 oxygenates that are mainly composed of methyl hydroperoxide is approximately 420 μmol g_{cat}⁻¹ h⁻¹ at 50 °C within 30 min (Fig. S9 and Table S1, ESI[†]), about 50 times lower than that of the Cr₁/ZSM-5 SAC, which indicates that the Cr₁ species are the main active species. For the DOM over Cr/ZSM-5-NP, the productivity of the C1 oxygenates that are mainly composed of CH₃OOH and CH₂(OH)₂ is 7249 μmol g_{cat}⁻¹ h⁻¹ with a total selectivity of 96.8% in all of the products at 50 °C within 30 min, about 3 times lower than that of the Cr₁/ZSM-5 SAC. Moreover, the turnover frequencies (TOFs) defined as the moles of the C1 oxygenates generated on one mole of Cr per hour are used to further characterize the intrinsic activity of the Cr species in the Cr/ZSM-5 samples.²⁷ The corresponding TOFs of the Cr species in Cr/ZSM-5-NP are 7.0 times lower than that of the Cr₁/ZSM-5 SAC (14.2 h⁻¹ vs. 99.8 h⁻¹) at 50 °C within 30 min (Fig. S10, ESI[†]), which further indicates that the Cr₁ species possess a much higher intrinsic activity for the DOM compared with nanometer-sized Cr species.

To demonstrate the efficiency of H₂O₂ utilization in the reaction, a gain factor defined as the molar ratio of formed C1 oxygenate products and consumed hydrogen peroxide²⁸ was measured as the standard (Fig. S11, ESI[†]). The gain factor of the Cr₁/ZSM-5 SAC (0.16) is 3.2-fold higher than that of Cr/ZSM-5-NP (0.05) at 50 °C. These results indicate that the Cr₁-O₄ as the active site in the Cr₁/ZSM-5 SAC significantly enhances the activation process of the oxygen species. In addition, no significant decrease in the selectivity and yield of the C1 oxygenates on the Cr₁/ZSM-5 SAC can be observed after five consecutive DOM cycles and the performance can be easily recovered after a simple calcination treatment (Fig. 3b), which indicates that the Cr₁-O₄ as the active site in the Cr₁/ZSM-5 SAC is highly stable for the DOM (Fig. S12, ESI[†]).

To better understand the kinetic behavior of the Cr₁/ZSM-5 SAC, the apparent activation energy (*E_a*) has been investigated. Under the conditions of kinetic control, the *E_a* of the Cr₁/ZSM-5 SAC (45.8 kJ mol⁻¹) is much lower than that of Cr/ZSM-5-NP (57.6 kJ mol⁻¹) and pure H-ZSM-5 (139.3 kJ mol⁻¹) as shown in Fig. 3c, which indicates that the catalytic process of the DOM is intrinsically boosted on the Cr₁/ZSM-5 SAC compared with that of Cr/ZSM-5-NP and H-ZSM-5. The reaction orders of CH₄ and H₂O₂ over the Cr₁/ZSM-5 SAC (0.64 for CH₄ and 0.42 for H₂O₂) are significantly different from that over Cr/ZSM-5-NP (1.18 for CH₄ and 0.59 for H₂O₂) and pure H-ZSM-5 (0.18 for CH₄ and 1.18 for H₂O₂) as shown in Fig. 3d, e and Table S3 (ESI[†]), which further reveals that the presence of the Cr₁ atoms significantly modulates the catalytic process of the DOM compared with that of Cr/ZSM-5-NP and pure H-ZSM-5.

We further computationally investigated the reaction mechanism of the DOM over the Cr₁/ZSM-5 SAC. After optimizing the structure of ZSM-5 (Fig. S13, ESI[†]), a series of potential mono-nuclear active sites coordinated with two framework oxygen anions (O_{fm}, Fig. S14, ESI[†]) were studied, including Z[CrO₂]⁺,

Z[Cr]⁺, Z[CrO]⁺, Z[Cr(OH)₂]⁺, Z[CrOH]⁺, and Z[Cr]²⁺. The sites of Z[Cr]⁺, Z[Cr]²⁺, Z[CrO]⁺, and Z[CrOH]⁺, which are not compatible with either the 4-fold coordinated Cr as confirmed by the EXAFS data or the trivalence of Cr as confirmed by the XPS results, were firstly excluded from the list of active site. The Z[Cr(OH)₂]⁺ was also excluded because of its low reactivity. The charge density analysis further revealed that both hydroxyls at the Cr sites of Z[Cr(OH)₂]⁺ are OH⁻ due to the strong electron-donating ability of the Cr species (Fig. S15 and Table S5, ESI[†]). The corresponding free energy barrier for the first C–H bond activation of methane is as high as 1.78 eV, which is formidable to activate a C–H bond of methane at the reaction temperature of 323 K. Moreover, even if the dissociative chemisorption of H₂O₂ could occur at the Z[Cr(OH)₂]⁺ site under the reaction conditions to generate Z[Cr(OH)₄]⁺, all of the hydroxyls at the Cr atom would be OH⁻ (Table S5, ESI[†]). The corresponding free energy barrier of the first C–H bond activation of methane is also as high as 1.44 eV, which is still insurmountable to activate methane. Hence, the sites of Z[Cr(OH)₂]⁺ and Z[Cr(OH)₄]⁺ were excluded because of their low reactivity.

Alternatively, the Z[CrO₂]⁺ site corresponds to an oxygen molecule chemisorbed at its Cr center *via* a π configuration, enabling the Cr₁ atom to be coordinated with two oxygen adatoms and two O_{fm} to form the Cr₁-O₄ coordination structure as presented in the inset picture of Fig. 2b. The O–O bond length of the chemisorbed O₂ is 1.424 Å, indicating that the O₂ presents as peroxide O₂²⁻ on Z[CrO₂]⁺.^{29–32} The spin charge density analysis further confirms that the peroxide O₂²⁻ and Cr³⁺ would exist at Z[CrO₂]⁺ (Fig. S15b, ESI[†]) since [CrO₂] needs to compensate a charge to the skeleton of the zeolite. It is in line with the XPS, XANES and NO-DRIFTS data. Based on the above experimental and DFT simulation results, the Z[CrO₂]⁺ site represents the local environment of the Cr₁ active site in the Cr₁/ZSM-5 SAC well and a mechanistic study was performed at the Z[CrO₂]⁺ site.

The DFT theoretical calculations prove that the reaction mechanism of the DOM by the Cr₁/ZSM-5 SAC can be divided into three stages (Fig. S16, ESI[†]): (i) pre-activation of the reaction site, (ii) oxidation of methane, and (iii) regeneration of the active sites. The first key step of the DOM using H₂O₂ as oxidant at Z[CrO₂]⁺ is the pre-activation of the reaction sites from Z[CrO₂]⁺ to Z[Cr(O)₂(OH)₂]⁺ with H₂O₂ as shown in Fig. 4a. H₂O₂ is likely to be intrinsically activated by the Z[CrO₂]⁺ site. It can chemisorb at the Z[CrO₂]⁺ site with a free adsorption energy of -0.52 eV followed by its O–O bond dissociation with a free energy barrier of 0.77 eV. Meanwhile, the Z[CrO₂]⁺ (IM1) turns into Z[CrO₂(OH)₂]⁺ (IM3). Interestingly, the presence of water molecules could significantly accelerate the H₂O₂ activation. As shown in Fig. 4a, in the presence of H₂O, the Z[CrO₂]⁺ site preferentially chemisorbs the H₂O with a stronger free adsorption energy of -0.87 eV. Then, the adsorbed H₂O can rapidly assist the O–O bond activation of H₂O₂ through H migration. It only needs to overcome a slight free energy barrier of 0.16 eV to generate the Z[CrO₂(OH)₂]⁺ (IM3) sites. Due to the strong electron-donating ability of Cr, the 4-fold Cr center is oxidized to the +5 valence state in the Z[CrO₂(OH)₂]⁺ configuration,



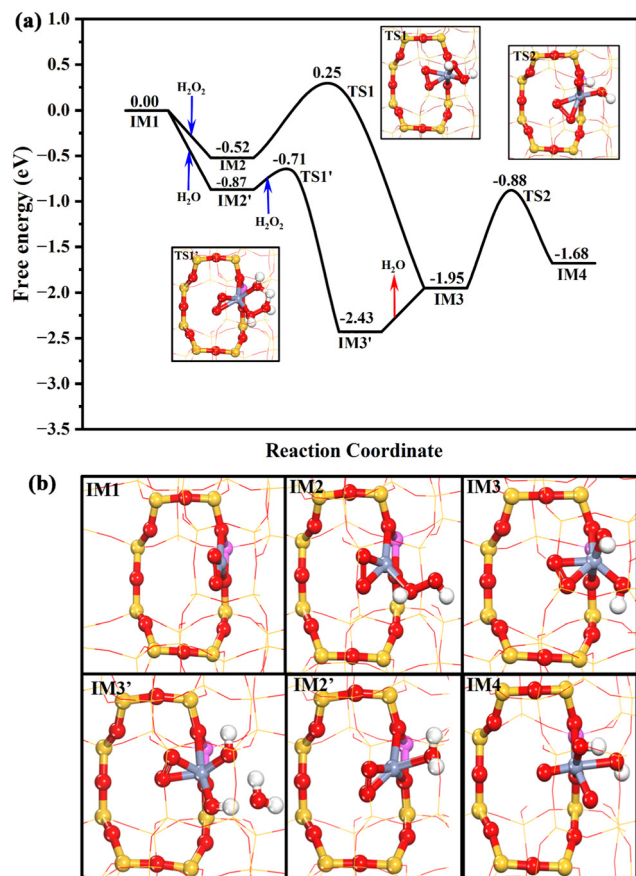


Fig. 4 The Gibbs free energy profile for the pre-activation of the reaction site over the $\text{Cr}_1/\text{ZSM-5}$ SAC with the geometry structures of key transition states (a); the geometry structures of all the intermediates in the whole catalytic cycle (b). The Gibbs energy profile was calculated under the reaction conditions of 30 bar CH_4 , 0.5 M H_2O_2 at 323 K. The H, O, Si, Al, and Cr atoms of the reaction sites are displayed in white, red, yellow, pink, and blue in a ball and stick style, respectively. The display settings were kept the same throughout the whole paper.

where two adsorbed hydroxyl anions (OH^{*-}) and two oxygen adatoms (O_2^{2-*}) are coordinated with the isolated Cr center. After forming the $\text{Z}[\text{CrO}_2(\text{OH})_2]^+$ configuration, the O–O bond of O_2^{2-*} at IM3 can be further broken by overcoming a free energy barrier of 1.07 eV (TS2). The addition of H_2O_2 lowers the free energy barrier by 0.14 eV (1.21 eV at IM1), indicating that the addition of H_2O_2 boosts the O_2^{2-*} dissociation. After the O_2^{2-*} dissociation, the formation of two O^{2-} anions results in the further oxidation of the $\text{Z}[\text{CrO}_2(\text{OH})_2]^+$ configuration (IM3) to Cr^{6+} , which forms the $\text{Z}[\text{Cr}(\text{O})_2(\text{OH})_2]^+$ configuration (IM4). The valence states of the chromium cations in these key intermediates are further demonstrated by Bader charge analysis as listed in Table S6 (ESI†). The Raman results fully support the dynamic transformation of Cr^{3+} to Cr^{6+} during the catalytic process of the DOM. The Cr^{6+} species (Raman characteristic peak at 875 cm^{-1}) would appear once the H_2O_2 interacts with the fresh and used $\text{Cr}_1/\text{ZSM-5}$ SACs (Fig. S17, ESI†), which indicates that the presence of H_2O_2 enables the efficient oxidization of the Cr^{3+} species to the active Cr^{6+}

species. The Bader charge density analysis (Fig. S15c and Table S5, ESI†) demonstrates that the formation of two O^{2-} anions renders one OH^{*-} at $\text{Z}[\text{CrO}_2(\text{OH})_2]^+$ (IM3) to be the radical state of OH^{*-} at $\text{Z}[\text{Cr}(\text{O})_2(\text{OH})_2]^+$ (IM4), which could be the reactive oxygen species for the DOM. It is very clear that the presence of H_2O_2 plays a crucial role in the O–O bond dissociation of O_2^{2-*} and the formation of the reactive oxygen species.

Due to the formation of Cr^{6+} , the reactive OH^{*-} is generated. As shown in Fig. 5, the OH^{*-} could significantly promote the CH_4 activation. The first C–H bond of CH_4 is activated by the OH^{*-} of IM4 through a radical-like mechanism,^{33,34} which only needs to climb over a free energy barrier of 0.68 eV (TS3). It is in good agreement with the previous reports that hexavalent Cr could be highly active.^{35,36} After methane activation, the generated free methyl radical could be readily captured by the O^{2-*} at $\text{Z}[\text{Cr}(\text{O})_2(\text{OH})]^+$ (IM6) to form $\text{Z}[\text{Cr}(\text{O})(\text{CH}_3\text{O})(\text{OH})]^+$ (IM7), which is significantly exothermic by 1.88 eV. Then, the OH^{*-} at IM7 could abstract one H atom of CH_3O^* to form H_2O^* and HCHO^* at $\text{Z}[\text{Cr}(\text{O})(\text{CH}_2\text{O})(\text{H}_2\text{O})]^+$ (IM8) by overcoming a free energy barrier of 1.02 eV. Subsequently, the HCHO and H_2O could be desorbed from the Cr center in sequence, which are respectively endothermic by 0.58 and 0.50 eV. Meanwhile, the $\text{Z}[\text{CrO}]^+$ (IM10) is formed and the valence state of the

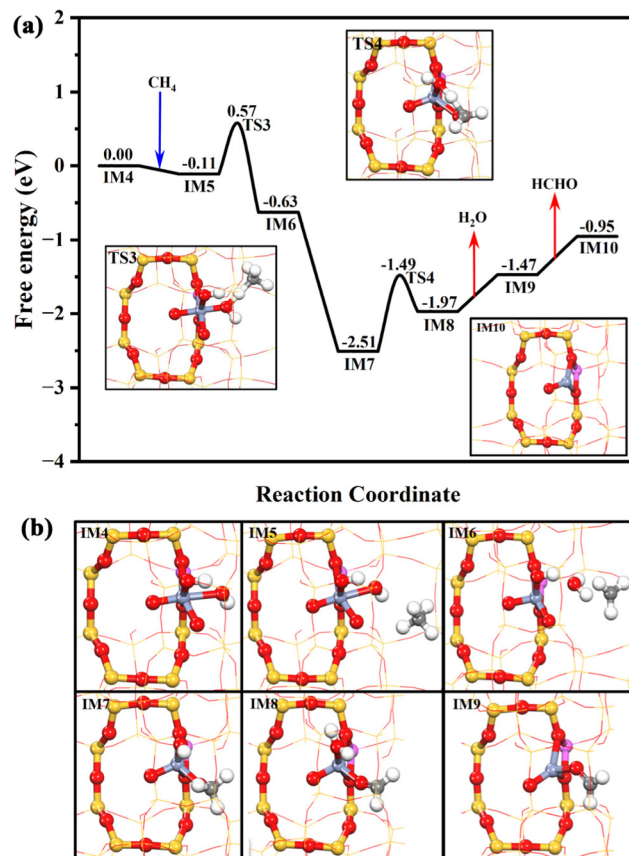


Fig. 5 The Gibbs free energy profile of the HCHO production branch over the $\text{Cr}_1/\text{ZSM-5}$ SAC with the geometry structures of key transition states (a); the geometry structures of all the intermediates in the whole catalytic cycle (b). The Gibbs energy profile was calculated under the reaction conditions of 30 bar CH_4 , 0.5 M H_2O_2 at 323 K.



Cr species returns to trivalent, which is consistent with the phenomenon detected by XPS (Fig. 2e). Hence, it is clear that the conversion of methane to formaldehyde catalyzed by the Cr₁/ZSM-5 SAC depends on the formation of hexavalent Cr ions and the surface reactive oxygen species.

To prove the above conclusion from DFT calculations, the adsorption behavior of OH* on the surface of the Cr₁/ZSM-5 SAC was explored by *in situ* H₂O₂-DRIFTS at 30 °C (Fig. S18). For the adsorption of H₂O₂ on the Cr₁/ZSM-5 SAC sample, the band at 3751 cm⁻¹ associated with the surface-adsorbed OH* is clearly observed as long as the H₂O₂ is introduced into the *in situ* chamber.³⁷ Alternatively, no significant OH* adsorption was observed on Cr/ZSM-5-NP and H-ZSM-5, which further reveals that the formation of surface-adsorbed OH* was promoted on the Cr₁ atoms. These results corroborate the conclusions of the DFT simulation results.

As shown in Fig. 6, Z[Cr(O)(CH₂O)]⁺ (IM9) is generated after methane and methoxy dehydrogenation. H₂O₂ can be easily chemisorbed at Z[Cr(O)(CH₂O)]⁺ (IM9) with a free adsorption energy of -0.88 eV. Interestingly, one OH of H₂O₂* could be

readily abstracted by the neighboring HCHO* to form Z[Cr(O)(OH)(H₂COOH)]⁺ (IM12), assisting the cleavage of the O–O bond of H₂O₂. This process only needs to climb over a subtle free energy barrier of 0.18 eV (TS5). Then, the HCOOH* (Z[Cr(O)(H₂O)(HCOOH)]⁺, IM13) is formed through the oxidative dehydrogenation of H₂COOH* by OH* with a free energy barrier of 1.21 eV. Then, the HCOOH is finally produced after overcoming a trivial desorption energy of 0.14 eV. The Z[CrO]⁺ (IM10) could also be formed in the pathway for HCOOH production after the desorption of H₂O (0.65 eV) from Z[Cr(O)(H₂O)]⁺ (IM14), which is the same as the reaction pathway of HCHO production.

As confirmed by the DFT simulation and experimental results, the active Cr species is hexavalent (Cr⁶⁺) in the presence of H₂O₂, and resulting reactive oxygen species trigger the DOM. Meanwhile, the Cr³⁺ species can be regenerated from the Cr⁶⁺ species after the desorption of the products, regardless of the HCHO or HCOOH production pathway. Since our Raman spectra prove that the hexavalent Cr could appear again when the used Cr₁/ZSM-5 SAC is treated with H₂O₂ (Fig. S17, ESI[†]), we further computationally investigate the pathway for the regeneration of the hexavalent Cr site (Fig. 7). Similar to the results above, the electron-donating trivalent Cr ion at Z[CrO]⁺ could

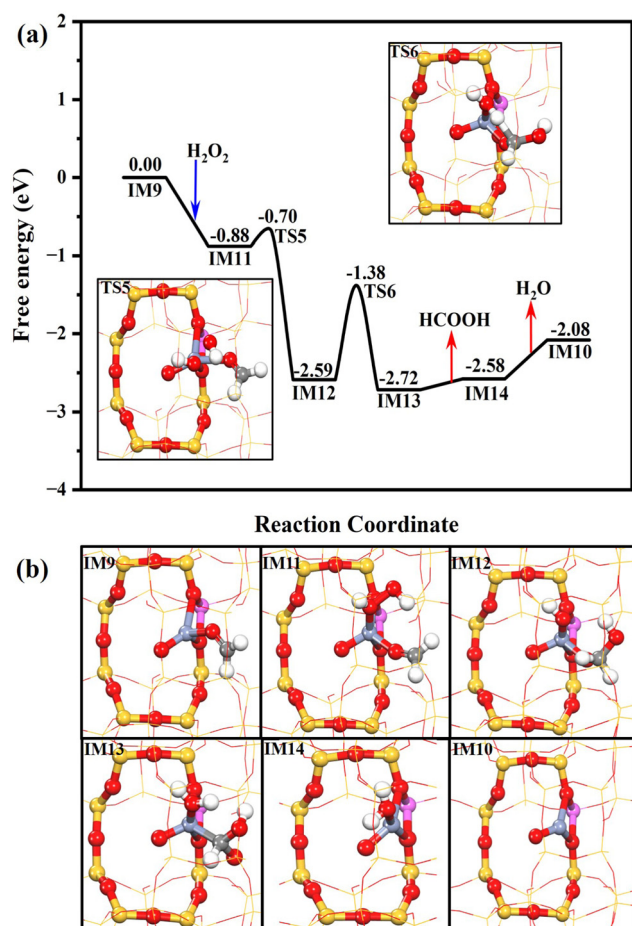


Fig. 6 The Gibbs free energy profile of the HCOOH production branch over the Cr₁/ZSM-5 SAC with the geometry structures of key transition states (a); the geometry structures of all the intermediates in the whole catalytic cycle (b). The Gibbs energy profile was calculated under the reaction conditions of 30 bar CH₄, 0.5 M H₂O₂ at 323 K.

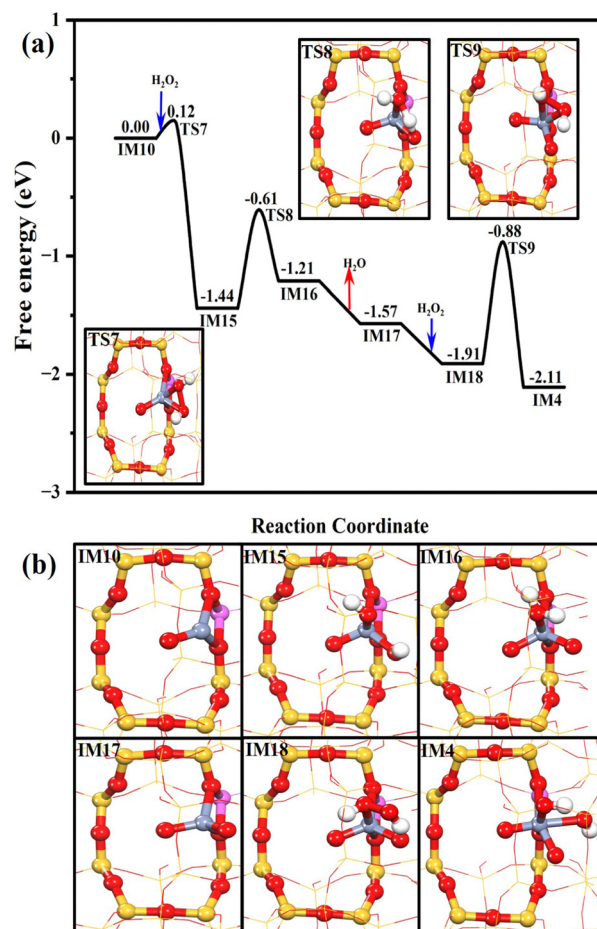


Fig. 7 The Gibbs free energy profile of the regeneration of the active sites with the geometry structures of key transition states (a); the geometry structures of all the intermediates in the whole catalytic cycle (b).



also break the O–O bond of H₂O₂ and form two OH[−]* readily (Z[Cr(O)(OH)₂]⁺, IM15) after overcoming a subtle free energy barrier of 0.12 eV. Then, the H migration between two OH* at IM15 could produce Z[Cr(O)₂(H₂O)]⁺ (IM16) with a free energy barrier of 0.83 eV, followed by the water desorption (−0.36 eV). The formed Z[Cr(O)₂]⁺ (IM17) could also chemisorb the H₂O₂ with the free adsorption energy of −0.34 eV. After its O–O bond has been broken (TS9, 1.03 eV), the hexavalent active site of Z[Cr(O)₂(OH)₂]⁺ (IM4) is regenerated. Therefore, the Cr₁ center would exhibit the trivalent status in the absence of H₂O₂, while it is transformed to the active hexavalent Cr center in the presence of H₂O₂, enabling the DOM to form the C1 oxygenates.

Conclusion

In summary, we demonstrate that the atomically-dispersed chromium sites anchored on ZSM-5 possess the excellent catalytic performance for the direct oxidation of methane to C1 oxygenated products with H₂O₂ as the oxidant at 50 °C. Compared with the low yield of C1 oxygenates from Cr/ZSM-5-NP, the yield of C1 oxygenates and selectivity are 21 100 μmol g_{cat}^{−1} h^{−1} and 99.8% on the Cr₁/ZSM-5 SAC at 50 °C, which, to our knowledge, outperforms most reported state-of-the-art catalysts. The *in situ* characterization and experimental results confirm that the transformation of the Cr³⁺ to Cr⁶⁺ species is the key to the high activity of the Cr₁/ZSM-5 SAC for the DOM. DFT theoretical calculations prove that the reaction mechanism of methane oxidation by the Cr₁/ZSM-5 SAC can be divided into three steps: (i) pre-activation of the reaction site; (ii) oxidation of methane; (iii) regeneration of the active sites. We believe that this study not only provides a new prospect for the efficient DOM under mild conditions but also promotes the design of non-noble metal SACs in heterogeneous catalysis.

Author contributions

Mengyu Zeng: data curation, formal analysis, writing-original draft. Lu Cheng: DFT data curation, investigation, formal analysis, writing-original draft. Qingqing Gu: STEM data curation, formal analysis. Bing Yang: STEM data curation, formal analysis. Baiyang Yu: investigation. Jing Xu: methodology, formal analysis. Ying Zhang: methodology, investigation. Chengsi Pan: methodology, formal analysis. Yang Lou: conceptualization, methodology, data curation, funding acquisition, writing-original draft, review & editing. Xiaoming Cao: DFT data curation, funding acquisition, supervision, writing – review & editing. Yongfa Zhu: funding acquisition, supervision, writing – review & editing.

Conflicts of interest

There are no conflicts to declare.

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