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Molecular recognition and adsorptive separation of *m*-xylene by trianglimine crystals†

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The separation of xylene isomers is one of the most challenging tasks in the petrochemical industry. Herein, we developed an efficient adsorptive molecular sieving strategy using crystalline trianglimine macrocycle (**1**) to separate the elusive *m*-xylene isomer from an equimolar xylenes mixture with over 91% purity. The selectivity is attributed to the capture of the preferred guest with size/shape selectivity and C–H... π interactions. Moreover, the trianglimine crystals are readily recyclable due to the reversible transformation between the guest-free and guest-loaded structures.

The energy intensive separation and purification of petrochemical isomers currently consumes 10–15% of the world's total energy production. Separation of C₈ aromatics, *o*-xylene (OX), *p*-xylene (PX), *m*-xylene (MX) and ethylbenzene (EB), is considered as one of the 'seven chemical separations that will change the world'.¹ Xylenes are obtained from crude oil by catalytic reforming and pyrolysis of gasoline. Each of the isomers is an important building block in the production of polymer fibers, films, plasticizers, resins, *etc.*^{2–4} Separation of MX from a mixture of OX/MX/PX is highly demanding as these isomers have overlapping physical properties.^{5,6} Chromatographic separation and other processes such as enclathration can be considered as energy saving options however, they are labor and time intensive.^{7–10}

Employing porous materials especially for C₈ aromatics separation has recently gained a lot of attention.¹¹ Zeolites and metal organic frameworks (MOFs) have shown effective industrial separation of OX and PX but more efforts are needed to obtain desired separation performance.^{12–17} Porous organic cages, with complementary geometry suitable for specific host molecules, were also employed for energy-demanding separations but showed modest performance for the separation of isomers.^{18–20} Nonporous adaptive crystals (NACs) based on macrocyclic building blocks such as pillar[6]arene have been successfully utilized for the separation of *p*-xylene and other isomer from their mixtures in the vapor phase.^{4,21,22} Nonetheless, pillar[6]arene crystals can work only *via* vapor-based adsorption as they are soluble in xylenes, which dramatically limits the possibility for their industrial translation. In this context, our group has recently reported the selective separation of OX and PX by CB[7] and crystalline azo cages, respectively.^{6,23} Interestingly, separation of the MX isomer has so far been illusive as host–guest interactions using the molecular sieving approach has mainly preferred PX and OX isomers.

Trianglimine macrocycles have emerged as a novel class of intrinsically porous molecular hosts that can be specifically tailored for selective separations.²⁴ Herein, we report that macrocycle **1** can be used as a host for the encapsulation and separation of MX from the xylene isomers both in the liquid and vapor phases through shape selective crystallization and the adsorption based approach (Fig. 1a and Fig. S1, ESI†). To the best of our knowledge, no systematic investigation was reported thus far on the use of organic macrocycles for the separation of MX from xylene isomers by the molecular sieving approach.

The synthesis and crystal structure of the macrocyclic host **1** have already been reported by our group.^{25,26} It crystallizes in a monoclinic system, chiral space group *P*2₁ and the asymmetric unit contains one unit of trianglimine and disordered solvent molecules (Table S1, ESI†). The structural analysis also revealed that two trianglimines are nearly perpendicular and stacked in

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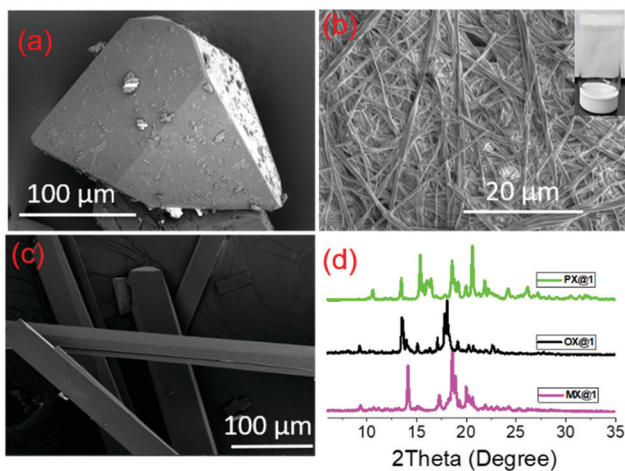


Fig. 3 SEM images of the products formed: (a) crystal obtained from **MX@1**. (b) Organogel obtained from OX and their self-assembly structure. (c) Crystal obtained from PX. (d) PXRD pattern of different forms of xylenes product.

These host-guest interactions and shape/size selectivity prompted us to test whether **1** could discriminate one isomer from a mixture of isomers in the liquid state. Crystallization of **1** in DCM/ACN (2:1) in the presence of a ternary equimolar mixture of *o*-/*m*-/*p*- xylenes (1:1:1 v/v/v) resulted in block prism shaped single crystals after 3 days and SCXRD analysis revealed the selective adsorption of MX over other isomers (Fig. 3 and Fig. S6b, S7, ESI[†]). The structure was exactly similar to that of **MX@1** crystals, which indicates that this system is also effective for crystallization-based separation with a purity over 99% in the solid-liquid state as verified by GC analysis (Table S4 and Fig. S8, ESI[†]). The competitive experiments were further tested for binary compositions of xylenes, which also supported the selectivity towards MX (Fig. S6c, ESI[†]).

Being prompted by the outstanding host-guest properties (as observed in SCXRD), we envisioned the applicability of this system in vapor phase and so we tested the positional sorting effect of xylene isomers. Activated guest free crystals **1** were obtained upon heating **1** at 70 °C for 24 h under high vacuum. After removing the solvent molecules by activation, the crystals exhibited high stability and crystallinity which indicates that the lattice voids are imprinted as verified by SCXRD (Fig. S2, ESI[†]). ¹H NMR spectra, TGA and PXRD experiments were performed to confirm the adsorption selectivity towards MX over other isomers. To reveal the detailed mechanistic pathway for the separation of MX, a time dependent solid-vapor experiment for equimolar mixture containing three xylene isomers (*o*-/*p*-/*m*- 1:1:1 v/v) was performed by **1** to measure the rate of the uptake process. It was found that the uptake of MX in **1A** increased over time and reached a saturation at 24 h; whereas the uptake of OX was competitive over the first three hours and then decreased to negligible quantity. The adsorption of PX was almost negligible throughout the entire period (Fig. 4a). It is possible that MX and OX are both adsorbed in the beginning (kinetically favored), and then when the material is almost

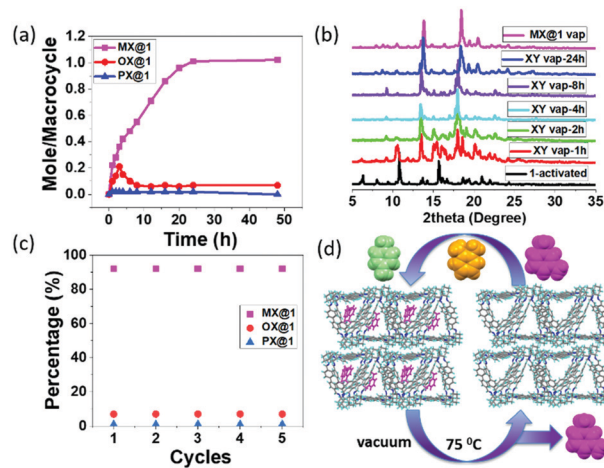


Fig. 4 (a) Solid-vapor sorption of **1** in OX/MX/PX (1:1:1 v/v) xylenes. (b) Time dependent PXRD of **1** to **MX@1** in the presence of OX/MX/PX (1:1:1 v/v) vapor. (c) Relative uptakes of MX after five recycles. (d) Schematic representation of MX release from **MX@1** to **1** upon heating and uptake of MX again from the mixture vapor.

saturated, OX is gradually replaced by MX due to thermodynamic stability. This implies a remarkably selective adsorption of MX from the xylene mixtures through guest capture by the host (Fig. S9–S12, ESI[†]). Further, PXRD experiments were carried out to monitor the structural transformation of **1** to **MX@1** after exposure to xylene isomers. The PXRD pattern suggests that apohost **1A** transforms to **MX@1** phase after 24 h from exposure to the equimolar mixture of xylene vapors (*o*-/*p*-/*m*- 1:1:1 v/v), while the preferentiality towards the other isomers (OX and PX) were negligible (Fig. 4b, Scheme S1 and Fig. S13a, ESI[†]). This further confirmed the preference towards MX over PX and OX in the vapor phase. The traditional porous crystalline materials do not change the structures upon guest capture,^{29,30} while the “intrinsic porosity” in triaglimine crystals could be induced by preferred guest molecules such as MX. Gas chromatography (GC) showed that **1A** can selectively capture MX over PX and OX in the intrinsic pores of crystalline solids with more than 91% selectivity (Fig. S14, ESI[†]).

Once we have established that **1A** is selective towards MX, we thought of looking into its performance on commercially relevant samples such as the C₈ aromatic fraction of xylene mixture and ethylbenzene isomer through both liquid and solid-vapor phase. Consistently, it revealed to be selective towards MX from the commercial samples (Fig. S6b and S13b, ESI[†]). In industrial production processes, the major problems associated with the adsorptive separation is decreasing performance of porous materials over time, because of the instability of the porous framework during heating. To be practically useful, an adsorbent must perform well over multiple cycles without any degradation. Recyclability and reversibility was accordingly verified over five cycles without any loss of selectivity as confirmed by GC (Fig. 4c, d and Fig. S14, S15, ESI[†]). We then investigated the selectivity of **1** for binary mixtures and again found the formation of **MX@1** from a



mixture of either MX and PX or MX and OX, as confirmed from PXRD (Fig S6c and S16, ESI†).

To estimate the thermochemistry of the formation of **MX@1**, **OX@1** and **PX@1**, density functional theory (DFT) calculations were performed at ω B97xD(SMD)/Def2-TZVP//PBE0-D3/Def2-SVP level of theory. The calculated energy values indicated that the formation of all the **MX@1**, **OX@1** and **PX@1** are exergonic by -24.6 , -13.2 and -10.7 kJ mol $^{-1}$ respectively ($\Delta G_{298}^{\text{Sol}}$, Scheme S2, ESI†). Therefore, in agreement with the experimental observation, the selectivity order of adsorption is $\text{MX} > \text{OX} > \text{PX}$. We also performed the distortion-interaction analysis on the electronic structure of **MX@1**, **OX@1** and **PX@1**. This analysis indicated that the ΔE of **MX@1** is in favor of 10.5 kJ mol $^{-1}$ and 13.1 kJ mol $^{-1}$ than that of **OX@1** and **PX@1** respectively (Table S5, ESI†). The highest ΔE values of **MX@1** corresponds to the lowest contribution of ΔE_{dis} of the host fragment **1**, which is disfavored by 17.3 kJ mol $^{-1}$ and 16.6 kJ mol $^{-1}$ relative to that of **OX@1** and **PX@1**. A minor distortion of **1** in **MX@1** with RMSD (root-mean-square deviation) of heavy atoms is 0.25 Å, while a clear deviation have been observed in **OX@1** and **PX@1** with RMSD values of 0.66 Å and 0.68 Å respectively. Therefore, the computational studies clearly support that the cavity of **1** is tailored to incorporate the MX molecule, while the adsorption of OX and PX requires a substantial deformation of the macrocycle cavity.

In conclusion, we have demonstrated a new class of intrinsically porous trianglimine macrocycle crystals with shape selective adsorptive molecular sieving of MX from the xylene isomers in both liquid and solid-vapor phase with selectivity over 91% for the multiple times. The present approach relies on the ability of **1** to preferentially capture a guest with “the best fit” and superior host-guest interactions, which was corroborated by DFT calculations. Considering the easy and cheap accessibility, low operating temperature, higher separation efficiency and high recyclability, this material holds a great potential for energy intensive separations through a tailored molecular recognition approach.

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Conflicts of interest

There are no conflicts to declare.

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