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# Matrix effects on the performance and mechanism of Hg removal from groundwater by MoS<sub>2</sub> nanosheets†

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Mercury (Hg) contamination in groundwater has been recognized as a serious threat to human health and ecological systems all over the world. This study demonstrated that two-dimensional (2D) molybdenum disulfide (MoS<sub>2</sub>) nanosheets can efficiently remove Hg in groundwater, with high Hg uptake capacity, ultrafast removal kinetics, and excellent selectivity. Interestingly, we found that the groundwater matrix has profound implications on the Hg removal efficiency and mechanisms by MoS<sub>2</sub> nanosheets. Specifically, surface adsorption is the dominant removal mechanism for Hg in DI water owing to the high affinity between Hg(II) and MoS<sub>2</sub> via strong Lewis acid/base soft-soft interactions. In groundwater, however, the presence of Cl<sup>-</sup> renders HgClOH the dominant species, which can undergo adsorption onto MoS<sub>2</sub> and homolytic cleavage to form the <sup>•</sup>HgCl radical. As an intermediate radical, <sup>•</sup>HgCl could either dimerize to form Hg<sub>2</sub>Cl<sub>2</sub> or further reduce to Hg<sup>0</sup>. This reduction-based mechanism enhanced the overall removal capacity of Hg to 6288 mg g<sup>-1</sup>, which is among the highest values reported to date. Additionally, our desorption tests revealed the high stability of immobilized Hg on MoS<sub>2</sub> nanosheets over conventional adsorbents in various extractant fluids. These impressive features render MoS<sub>2</sub> nanosheets a promising candidate for remediation of Hg-contaminated groundwater.

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## Environmental significance

Mercury (Hg) contamination is a serious threat to human health and ecological systems, and requires efficient remediation methods. Two-dimensional MoS<sub>2</sub> has emerged as a promising material for Hg remediation. Investigation for the matrix effects on Hg removal efficiency by MoS<sub>2</sub> nanomaterials is imperative and a precondition for the application in various water systems (e.g., groundwater). This study employed chemically exfoliated MoS<sub>2</sub> nanosheets to remove Hg(II) in groundwater, and demonstrated that the coexisting Cl<sup>-</sup> has largely promoted the removal performance through the reductive formation of Hg<sub>2</sub>Cl<sub>2</sub>. The highest capacity reported so far has further advanced the potential of utilizing MoS<sub>2</sub>-based nanomaterials in Hg remediation and highlighted the significance of matrix effects in the nano-enabled remediation processes.

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† Electronic supplementary information (ESI) available: Schematic illustration of the chemical exfoliation of bulk MoS<sub>2</sub> (Fig. S1); particle size distribution of the as-exfoliated MoS<sub>2</sub> nanosheets (Fig. S2); S 2p XPS spectra of the as-prepared MoS<sub>2</sub> nanosheets (Fig. S3); Hg uptake kinetics by MoS<sub>2</sub> nanosheets in groundwater (Fig. S4); Hg uptake kinetics model fitting curve (Fig. S5); determination of MoO<sub>4</sub><sup>2-</sup> in solution by ion chromatography (Fig. S6); Ca(II) and Mg(II) uptake by MoS<sub>2</sub> nanosheets (Fig. S7); XPS survey scan spectra of Hg-laden MoS<sub>2</sub> formed in DI water and groundwater (Fig. S8); TEM images and EDS-mapping of Hg-laden MoS<sub>2</sub> nanosheets in groundwater (Fig. S9) and DI water (Fig. S10); mass distribution of Mo in groundwater and DI water (Fig. S11); oxidation of MoS<sub>2</sub> nanosheets in the presence of Cl<sup>-</sup> at various concentrations (Fig. S12); the percentage of Hg species in simulated groundwater (Fig. S13); effects of pH on Hg removal efficiency by MoS<sub>2</sub> (Fig. S14); Hg uptake by AC in groundwater (Fig. S15). See DOI: 10.1039/d1va00035g

## 1. Introduction

Mercury (Hg) is recognized as one of the most remarkably toxic contaminants and widely present in environmental matrices such as soil and groundwater.<sup>1,2</sup> Generally, Hg in the environment is generated from industrial activities, agriculture, and natural sources.<sup>3-6</sup> In groundwater, Hg mainly exists as inorganic species (an average of 84% of soluble Hg)<sup>7</sup> and Hg pollution occurs via deep-well disposal of liquid wastes, the leachate from a number of contaminated sources such as landfills, sewage, mine tailings, and industrial waste lagoons.<sup>8</sup> Exposure to Hg has been reported to cause various adverse health effects on the nervous, renal, and endocrine systems.<sup>9</sup> Based on surrounding environmental conditions, the environmental and health risk of Hg in groundwater can be intensified by the microbial transformation of inorganic Hg to the more toxic methylmercury, which can be biomagnified with



a bioaccumulation factor of up to  $10^6$  in the food chain.<sup>10</sup> Consequently, the United States Environmental Protection Agency (EPA) has established a maximum contaminant level (MCL) of  $2 \mu\text{g L}^{-1}$  for Hg, and the guideline value from the World Health Organization (WHO) is set to be  $1 \mu\text{g L}^{-1}$ .<sup>11</sup> Nowadays, exposure to Hg-contaminated drinking water is still a serious concern in some small and rural communities, where groundwater is directly used for self-supply domestic purposes without standard treatment.

Available techniques for removing Hg from aqueous solutions include chemical precipitation,<sup>12,13</sup> ion exchange,<sup>14</sup> coagulation,<sup>15</sup> membrane filtration,<sup>16</sup> and adsorption.<sup>17</sup> Among these techniques, adsorption is a favored option for small-sized communities, because of feasible operation, low expertise requirement, and regeneration potential. Conventional adsorbents (*e.g.*, carbon-based materials,<sup>18,19</sup> iron-based minerals,<sup>20,21</sup> and oxide nanomaterials<sup>11</sup>) generally have low specificity and affinity to Hg, which leads to the low effectiveness of Hg removal. Particularly in the case of Hg removal from groundwater, co-existing cations at elevated concentrations relative to Hg may compete with Hg cations for the sorption sites and therefore increase the necessary sorbent dose and costs. For instance, the typical concentrations of Ca and Mg ions in groundwater can range from  $\sim 10$  to  $200 \text{ mg L}^{-1}$ , a few orders of magnitude higher than that of the Hg species found in contaminated groundwater.<sup>22,23</sup> Additionally, the presence of various anions (*e.g.*,  $\text{Cl}^-$ ,  $\text{NO}_3^-$ ,  $\text{OH}^-$ , and  $\text{SO}_4^{2-}$ )<sup>24,25</sup> and negatively-charged natural organic matter (NOM) may form various stable coordination complexes with Hg(II), which may reduce the overall removal efficiency of Hg from groundwater.

Two dimensional molybdenum disulfide (2D-MoS<sub>2</sub>), an emerging nanomaterial, consists of covalently bonded atomic trilayers of S–Mo–S and has been extensively studied with demonstrated excellent removal performance towards various heavy metals including Hg.<sup>26–28</sup> Generally, the highly efficient and selective Hg removal by MoS<sub>2</sub> nanosheets stems from their large surface area and abundant active sulfur sites that have strong Lewis acid/base soft–soft interactions with Hg.<sup>29–31</sup> Liu *et al.*<sup>32</sup> used hydrothermally-synthesized MoS<sub>2</sub> to simultaneously remove Hg(II), Pb(II) and Cd(II) from the aqueous phase, and MoS<sub>2</sub> exhibited the highest removal efficiency for Hg(II) among the tested ions with a maximum adsorption capacity of  $2409 \text{ mg g}^{-1}$ . Jia *et al.*<sup>33</sup> reported multi-layer adsorption of Hg(II) onto MoS<sub>2</sub> nanosheets *via* Hg–S complexation and electrostatic interactions. Additionally, MoS<sub>2</sub>-based complex architectures have been developed for enhanced exposure of the sorption sites and feasible regeneration of the sorbent materials. For instance, MoS<sub>2</sub> nanoflowers were immobilized onto eco-friendly aerogels and exhibited excellent removal efficiency of methylmercury and also extremely low toxicity to aquatic species.<sup>34–36</sup> MoS<sub>2</sub>-loaded carbon nanofibers were employed to maximize the exposure of MoS<sub>2</sub> surface to Hg for enhanced decontamination while minimizing the release of loaded MoS<sub>2</sub> into the treated water.<sup>37</sup> Despite superb Hg removal performance by MoS<sub>2</sub>, previous studies mainly focused on Hg removal in deionized (DI) water or buffered solutions.<sup>32,37–39</sup> Considering limited pretreatment approaches for rural communities to moderate

the impacts of groundwater constituents, we believe it is of great importance to study the matrix effects on the Hg removal from groundwater, and to unravel the applicability of MoS<sub>2</sub> in the remediation of Hg-contaminated groundwater.

The overall goal of this work was to determine the mechanisms governing removal of Hg(II) from groundwater by 2D MoS<sub>2</sub> nanosheets and examine the effects of the groundwater matrix on the Hg(II) removal efficacy. In this work, monolayer MoS<sub>2</sub> nanosheets were prepared by a chemical exfoliation method and employed for evaluating the Hg(II) removal performance of MoS<sub>2</sub> nanosheets in groundwater. The Hg removal kinetics and isotherms of MoS<sub>2</sub> were studied in batch tests and compared in groundwater and DI water to reveal any matrix effects. The Hg-laden MoS<sub>2</sub> formed in groundwater and DI was extensively characterized to understand the underlying Hg removal mechanisms in each water matrix. Lastly, the stability of Hg immobilized by MoS<sub>2</sub> nanosheets was tested in various extractant solutions to test the Hg anchoring capability in groundwater remediation.

## 2. Materials and methods

### 2.1 Preparation and characterization of MoS<sub>2</sub> nanosheets

The detailed information of chemicals used in this study is listed in the ESI.† MoS<sub>2</sub> nanosheets were prepared by an established chemical exfoliation method following the approach reported previously, and the schematic illustration of the exfoliation process is shown in Fig. S1.†<sup>40</sup> Briefly, 5 mL of 1.6 M *n*-butyllithium in hexane solution was added to  $\sim 300 \text{ mg}$  of bulk MoS<sub>2</sub> powder ( $\sim 2 \mu\text{m}$ , Sigma-Aldrich) and the suspension was stirred gently in a nitrogen-filled glovebox for 2 d. Then 40 mL hexane was added to the resulting solution mixture, and the excess organic reactants and byproducts were removed by centrifugation at 4000 rpm for 15 min to obtain the Li-intercalated MoS<sub>2</sub> sample. About 100 mL DI water was added to the collected Li-intercalated MoS<sub>2</sub> and incubated in an ultrasonic water bath for 1 h to facilitate hydration and exfoliation to obtain individual MoS<sub>2</sub> nanosheets. The resulting dispersion of MoS<sub>2</sub> nanosheets was dialyzed in DI water for 1 d using a dialysis bag (BEF 88244, Thermo Fisher Scientific, Waltham, MA, U.S.A.) to remove inorganic byproduct LiOH. Finally, the MoS<sub>2</sub> stock solution was purged with purified N<sub>2</sub> ( $>99.9\%$ ) for 1 h to remove dissolved oxygen and stored in a nitrogen-filled glovebox. To determine the nanosheet concentration, the MoS<sub>2</sub> suspension was completely digested with 2% HNO<sub>3</sub> and 30% H<sub>2</sub>O<sub>2</sub>, followed by the measurement of soluble Mo species concentration with ICP-OES (iCAP 7000 SERIES, Thermo Fisher Scientific, Waltham, MA, U.S.A.).

The hydrodynamic size and zeta potential ( $\zeta$ ) of MoS<sub>2</sub> nanosheets were obtained using a Zetasizer Nano ZS instrument (NanoBrook Omini, Brookhaven, NY, U.S.A.). An atomic force microscope (AFM, MFP-3D Stand Alone, Asylum Research, Oxford, UK) was used to observe the flake-like structure of MoS<sub>2</sub> nanosheets. Transmission electron microscopy (TEM, Talos F200X, FEI, MA, U.S.A.) with energy dispersive spectroscopy (EDS) was used to monitor the morphology of the as-exfoliated MoS<sub>2</sub> and exhibit the elemental distribution of Hg-laden MoS<sub>2</sub>



nanosheets. Raman spectroscopic measurements were performed on a LabRAM HR Evolution (HORIBA, Kyoto, Japan). X-ray photoelectron spectroscopy (XPS, PHI 5000 Versaprobe III, ULVAC-PHI, Japan) was employed to identify the chemical composition of the MoS<sub>2</sub> nanosheets before and after Hg removal. The composition and crystallographic structure of Hg-laden MoS<sub>2</sub> nanosheets were examined by powder X-ray diffraction (XRD, Rigaku Smartlab 9 kW, Tokyo, Japan) with Cu-K $\alpha$  radiation ( $\gamma = 1.5406 \text{ \AA}$ ).

## 2.2 Mercury removal by MoS<sub>2</sub> nanosheets

Batch tests were used to study the Hg(II) removal capacity, kinetics, and selectivity of MoS<sub>2</sub> nanosheets in groundwater. A solution of pH 8.3 containing 230 mg L<sup>-1</sup> Na<sup>+</sup>, 32 mg L<sup>-1</sup> Ca<sup>2+</sup>, 234 mg L<sup>-1</sup> Cl<sup>-</sup>, 183 mg L<sup>-1</sup> HCO<sub>3</sub><sup>-</sup>, and 96 mg L<sup>-1</sup> SO<sub>4</sub><sup>2-</sup> was prepared to represent the simulated groundwater.<sup>41</sup> To evaluate the removal kinetics, the simulated groundwater was spiked with 20 mg L<sup>-1</sup> Hg, and 4 mg L<sup>-1</sup> MoS<sub>2</sub> dispersion was then added to initiate the remediation. The mixture was continuously mixed on an end-over-end rotator at 60 rpm at room temperature (25  $\pm$  1  $^{\circ}$ C). At predetermined time intervals (0–48 h), the samples were filtered through 0.22  $\mu$ m PTFE filters and the remaining Hg concentrations in the filtrates were measured with a direct mercury analyzer (DMA-80, Milestone, Italy). The pH of the mixture was stable at 7.9  $\pm$  0.2 throughout the entire removal process. The Hg uptake isotherm was determined with the initial concentration of MoS<sub>2</sub> nanosheets at 4 mg L<sup>-1</sup> and varying initial Hg(II) concentrations from 2 to 42 mg L<sup>-1</sup>. Upon equilibration for 2 d, the samples were processed in the same manner as described in the sorption kinetics tests. To reveal the groundwater matrix effects on Hg capture, the Hg uptake isotherm was also measured in DI water for comparison. The equilibrium Hg removal capacity ( $q_e$ , mg Hg/g MoS<sub>2</sub>) and the distribution coefficient ( $K_d$ ) were calculated *via* the following equations:

$$q_e = (C_0 - C_e)V/m \quad (1)$$

$$K_d = (V[(C_0 - C_e)/C_e])/m \quad (2)$$

where  $C_0$  and  $C_e$  are the initial and equilibrium Hg concentrations (mg L<sup>-1</sup>) after Hg removal by MoS<sub>2</sub>, respectively,  $V$  is the solution volume (L), and  $m$  is the mass (g) of MoS<sub>2</sub>.

In addition, to demonstrate the selectivity of MoS<sub>2</sub> towards Hg among various typical heavy metal cations, batch experiments were performed under the same conditions except for the addition of Ni(II), Cd(II), Cu(II), and Zn(II) at 1 mg L<sup>-1</sup> as co-existing cations. All experiments were conducted in duplicate. To investigate the effects of pH on Hg immobilization, the initial pH was adjusted in the range of 3–8 with the addition of HNO<sub>3</sub> and NaOH solutions. In order to probe the competing ion effects on Hg removal, Ca(NO<sub>3</sub>)<sub>2</sub> and Mg(NO<sub>3</sub>)<sub>2</sub> were spiked in the sorption tests with Ca(II) or Mg(II) concentrations up to 200 mg L<sup>-1</sup> to mimic groundwater with high hardness. The effects of NOM on the Hg removal were tested in the presence of various concentrations of NOM (0–50 mg L<sup>-1</sup>).

## 2.3 Mechanistic investigation of groundwater matrix effects

To reveal the removal mechanisms, we investigated the mass distribution of Hg in the remaining solution (*i.e.*, unremoved Hg), with the MoS<sub>2</sub> sorbent (*i.e.*, Hg sorbed), and in the vapor state (*i.e.*, reduced Hg<sup>0</sup>). First, the Hg concentration in solution at equilibrium was measured following the filtration stage as described before. The Hg-laden MoS<sub>2</sub> was collected on the membrane surface and freeze-dried to drive off water and Hg<sup>0</sup>. Freeze-drying was performed under vacuum conditions at  $-45 \text{ }^{\circ}$ C using a vacuum freeze-dryer (Scientz-12N, Ningbo Xinzhi Biotech Co., Ltd., China) for 36 h. A solution made of 30% H<sub>2</sub>O<sub>2</sub> and 68% HNO<sub>3</sub> was then used to completely digest the Hg-laden MoS<sub>2</sub> to enable quantification of the Hg (and Mo) content on the adsorbent. Finally, the amount of Hg<sup>0</sup> was obtained by subtracting the amount of Hg remaining in the solution and on the sorbents from the total amount of Hg added. All experiments were conducted in triplicate to ensure reproducibility.

## 3. Results and discussion

### 3.1 Characterization of MoS<sub>2</sub> nanosheets

The dispersion of MoS<sub>2</sub> nanosheets was prepared by chemical exfoliation of bulk MoS<sub>2</sub> reported previously (Fig. S1†).<sup>35</sup> After exfoliation, the lateral size of the as-prepared MoS<sub>2</sub> nanosheets was estimated to be  $\sim$ 230 nm (Fig. S2†), and the zeta potential was  $-44.7 \text{ mV}$  at pH 6.0. The MoS<sub>2</sub> suspension was able to maintain colloidal stability (Fig. S1†) for over 6 months due to strong electrostatic repulsion forces between the negatively charged nanosheets, which is critical to allow the contact between MoS<sub>2</sub> and the target Hg cations. TEM and AFM images (Fig. 1a and b) exhibited the flake-like structure of exfoliated MoS<sub>2</sub> nanosheets, and the thickness measured by AFM implied that most nanosheets existed as monolayers or bi-layers. The phase composition of the as-exfoliated MoS<sub>2</sub> was characterized by XPS and Raman spectroscopy. As shown in Fig. 1c, the deconvolution of Mo 3d XPS spectra implied that 1T-MoS<sub>2</sub> was the dominant phase at 228.5 and 231.6 eV, corresponding to Mo 3d<sub>5/2</sub> and Mo 3d<sub>3/2</sub>, respectively.<sup>42</sup> 2H phase MoS<sub>2</sub>, as a minor component in the exfoliated nanosheets, exhibited a binding energy  $\sim$ 1 eV higher than that of the 1T phase. The mixed phase in the as-exfoliated MoS<sub>2</sub> was also confirmed with S 2p XPS spectra (Fig. S3†) and Raman spectra (Fig. 1d), which exhibited characteristic peaks of 1T (*i.e.*, 149.1, 214.2, and 323.5 cm<sup>-1</sup>) and 2H phases (*i.e.*, 377.2 and 402.0 cm<sup>-1</sup>).<sup>43,44</sup> The partial phase conversion from pure 2H in bulk MoS<sub>2</sub> to mixed 1T/2H in the exfoliated MoS<sub>2</sub> was caused by lithium intercalation in chemical exfoliation.<sup>45</sup>

### 3.2 Hg removal performance by MoS<sub>2</sub> nanosheets

Batch experiments were performed to examine the effectiveness of the as-prepared MoS<sub>2</sub> nanosheets in the removal of Hg in the groundwater matrix. As shown in Fig. 2a, MoS<sub>2</sub> nanosheets exhibited fast Hg(II) removal kinetics with a removal efficiency of 95% achieved within 5 min. More importantly, at a moderate MoS<sub>2</sub> dose of 8 mg L<sup>-1</sup>, the concentration of Hg was reduced



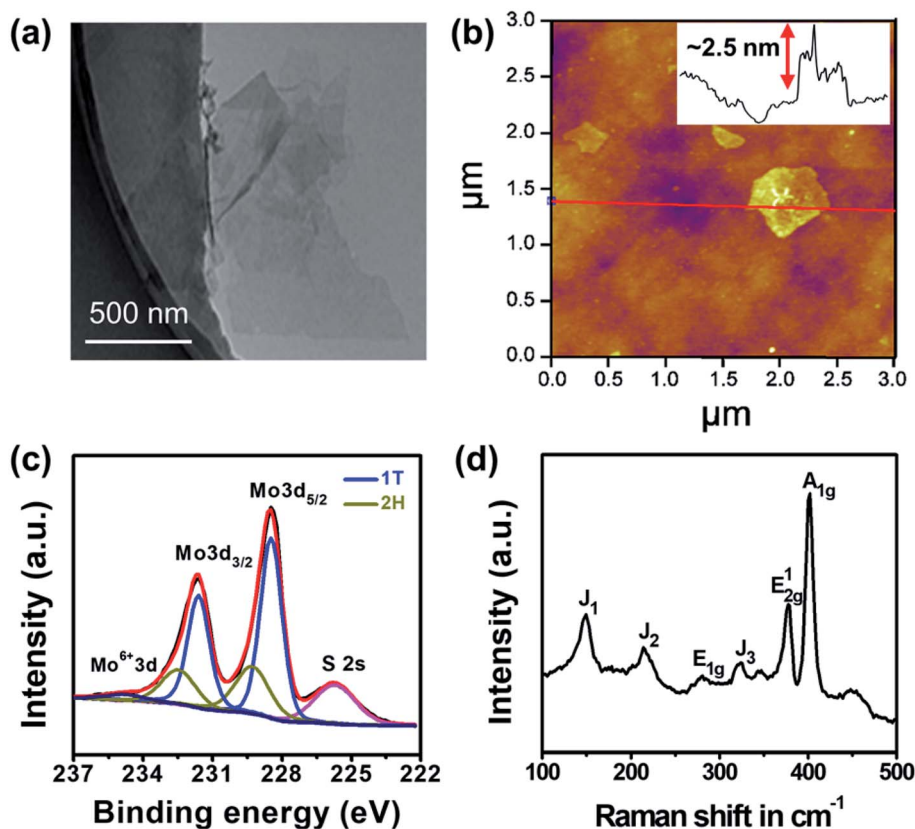


Fig. 1 Characterization of the as-exfoliated MoS<sub>2</sub> nanosheets. (a) TEM and (b) AFM images of MoS<sub>2</sub> nanosheets, and the inset shows the line profile; (c) Mo 3d XPS and (d) Raman spectra.

from 5 mg L<sup>-1</sup> to 0.92 µg L<sup>-1</sup> (Fig. S4†), far below the drinking water standard regulated by the US-EPA (2 µg L<sup>-1</sup>). The distribution coefficient ( $K_d$ ) of MoS<sub>2</sub> nanosheets for Hg is also

calculated to be  $1.02 \times 10^8$  mL g<sup>-1</sup>, which is much higher than  $1.0 \times 10^5$  mL g<sup>-1</sup>, the criterion for excellent adsorbents.<sup>31</sup> This value is also superb among engineered nanomaterials targeted

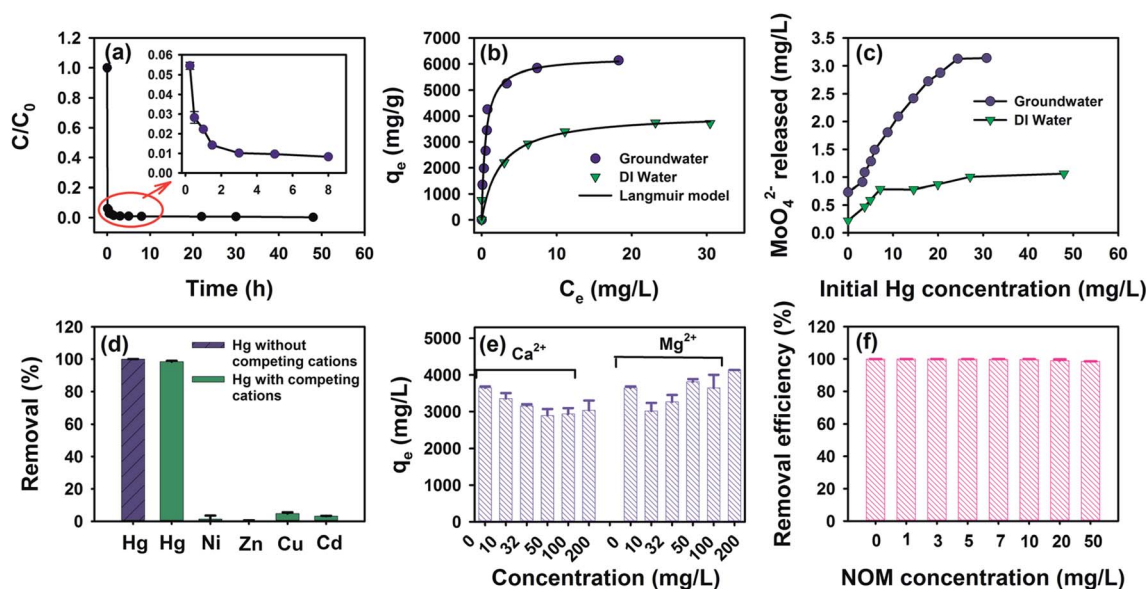


Fig. 2 Hg(II) removal by MoS<sub>2</sub> nanosheets. (a) Kinetics of Hg(II) uptake by MoS<sub>2</sub> nanosheets,  $C_{\text{Hg}} = 5$  mg L<sup>-1</sup> and  $C_{\text{MoS}_2} = 4$  mg L<sup>-1</sup>; (b) isotherm of Hg(II) uptake by MoS<sub>2</sub> fitted with Langmuir model,  $C_{\text{Hg}} = 0$ –42 mg L<sup>-1</sup>; (c) the concentration of MoO<sub>4</sub><sup>2-</sup> in the solution after reaction between MoS<sub>2</sub> and Hg ions; (d) removal efficiency of various heavy metals by MoS<sub>2</sub> nanosheets in a mixture containing all cations at equal concentrations of 1 mg L<sup>-1</sup>; (e) effects of Ca(II) and Mg(II) on Hg removal by MoS<sub>2</sub> nanosheets; (f) effects of NOM on Hg removal by MoS<sub>2</sub>,  $C_{\text{Hg}} = 20$  mg L<sup>-1</sup> and  $C_{\text{MoS}_2} = 15$  mg L<sup>-1</sup>.





at Hg removal reported previously including M-Ti<sub>3</sub>C<sub>2</sub> nanosheets ( $\sim 5.46 \times 10^6$  mL g<sup>-1</sup>),<sup>46</sup> GO@SnS<sub>2</sub> ( $8.68 \times 10^5$  mL g<sup>-1</sup>),<sup>47</sup> LHMS-1 ( $>1 \times 10^6$  mL g<sup>-1</sup>),<sup>48</sup> and polymeric chelating fibers ( $3.0 \times 10^5$  to  $3.8 \times 10^6$  mL g<sup>-1</sup>).<sup>49</sup> The kinetic data were fitted with pseudo-first-order and pseudo-second-order models (Fig. S5†),<sup>50</sup> and fitting parameters and the results are summarized in Table S1.† As shown in Fig. S5b,† the pseudo-second-order kinetic model provided the better fitting with the higher  $R^2$  (0.9999), which indicated that the rate-limiting step might be chemisorption between Hg and MoS<sub>2</sub> nanosheets.<sup>51</sup>

The removal isotherm in Fig. 2b shows that the Hg uptake density of MoS<sub>2</sub> nanosheets increased promptly at low equilibrium Hg concentrations and approached a constant value at high concentrations. The isotherm was better fitted with the Langmuir model ( $R^2 = 0.9801$ ) than Freundlich model ( $R^2 = 0.9145$ , Table S2†), which suggested that removal of Hg was likely achieved *via* a monolayer coverage on homogeneous sites of the MoS<sub>2</sub> nanosheet surface.<sup>52</sup> According to the fitting, the maximum Hg uptake capacity by MoS<sub>2</sub> nanosheets in groundwater was determined to be 6288 mg g<sup>-1</sup>, which is among the highest removal capacities for Hg reported to date and also higher than those of MoS<sub>2</sub> nanosheets synthesized by other methods (*i.e.*, 425–1991 mg g<sup>-1</sup> in Table S3†). The superb remediation performance of MoS<sub>2</sub> nanosheets in our study stems from the good dispersity and monolayer structure, which give rise to maximum exposure of active sulfur sites for anchoring Hg ions. More interestingly, the removal capacity determined in this study also exceeds the theoretical Hg removal capacity by monolayer MoS<sub>2</sub> (*i.e.*, 2506 mg g<sup>-1</sup>) if surface adsorption *via* Hg–S bonding is the sole removal mechanism.<sup>31</sup> Thus, other removal mechanisms (*e.g.*, reduction, electrostatic interactions, or complexation) might exist in the Hg removal by the MoS<sub>2</sub> nanosheets employed in this study. Considering the high redox potential of the Hg<sup>2+</sup>/Hg<sup>0</sup> couple ( $E^0 = 0.85$  V),<sup>53</sup> we measured the concentrations of the oxidation product of MoS<sub>2</sub>, namely MoO<sub>4</sub><sup>2-</sup>, after Hg removal to reveal if reductive removal of Hg occurred. The oxidation of MoS<sub>2</sub> to MoO<sub>4</sub><sup>2-</sup> has been observed in previous studies and also validated experimentally in our own test (Fig. S6†).<sup>37</sup> As shown in Fig. 2c, the extent of oxidative dissolution of MoS<sub>2</sub> nanosheets was closely related to initial Hg concentrations. Specifically, if Hg was absent, the concentration of released MoO<sub>4</sub><sup>2-</sup> was very low at 0.22 and 0.73 mg L<sup>-1</sup> in DI water and groundwater, respectively, indicating that the extent of oxidation of MoS<sub>2</sub> by dissolved oxygen was insignificant; when the initial Hg addition was 25–30 mg L<sup>-1</sup>, the concentration of released MoO<sub>4</sub><sup>2-</sup> was  $\sim 3.1$  mg L<sup>-1</sup> amounting to  $\sim 80\%$  of the total MoS<sub>2</sub> added, which indicates that Hg promoted the oxidation of MoS<sub>2</sub>. The correlation of Hg removal and MoO<sub>4</sub><sup>2-</sup> release indicates that a portion of Hg in the groundwater was likely removed *via* a redox reaction with MoS<sub>2</sub> nanosheets.

To evaluate the potential of using MoS<sub>2</sub> nanosheets in practical groundwater remediation, we also investigated the selectivity of MoS<sub>2</sub> nanosheets towards Hg cations in the presence of various ionic species found in groundwater. In the groundwater containing mixed heavy cations at the same concentration (Fig. 2d), MoS<sub>2</sub> nanosheets exhibited nearly

complete removal of Hg(II) with an efficiency of 98.4%. In comparison, the removal efficiency was much lower (<5%) for other heavy metals such as Cu(II), Cd(II), Ni(II) and Zn(II). Additionally, the presence of concentrated competing Ca and Mg cations does not impact the Hg removal (Fig. 2e), because of the high affinity of MoS<sub>2</sub> to Hg ions and thus favorable removal of Hg over other competing cations. Meanwhile, Ca and Mg cations were not adsorbed noticeably by MoS<sub>2</sub> (Fig. S7†), in line with the low affinity of MoS<sub>2</sub> to hard Lewis acids. Moreover, the presence of NOM up to 50 mg L<sup>-1</sup> has no influence on the Hg removal by MoS<sub>2</sub> (Fig. 2f), which is an advantage for MoS<sub>2</sub> compared to the inhibited Hg removal by NOM observed in other adsorbents previously (*e.g.*, FeS, oxide/Fe-Mn).<sup>54,55</sup>

It is interesting to note in Fig. 2b that a large Hg removal capacity by MoS<sub>2</sub> was observed in DI water (*i.e.*, 4043 mg g<sup>-1</sup>), which is however slightly lower than that in groundwater (*i.e.*, 6288 mg g<sup>-1</sup>). The oxidative dissolution of MoS<sub>2</sub> was apparently inhibited in DI water (Fig. 2c). Collectively, the decreased capacity and inhibited MoS<sub>2</sub> oxidation imply that the reduction-based Hg removal was weakened in DI water and also indicates that the groundwater matrix plays an important role in varying the efficiency and mechanism of Hg removal by MoS<sub>2</sub>. Interestingly enough, the groundwater matrix has been reported to have negative impacts on the removal of heavy metals *via* competitive sorption of other cations and complexation of heavy metals with anions.<sup>56,57</sup> The contrary, enhanced Hg removal in groundwater by MoS<sub>2</sub> nanosheets is yet to be reported and is therefore investigated by using various characterization tools to assess the role of the matrix on the removal nature and extent.

### 3.3 Matrix-dependent Hg removal by MoS<sub>2</sub>

To unravel the matrix-dependent Hg removal, the Hg-laden MoS<sub>2</sub> nanosheets were characterized by XRD, Raman, XPS and TEM after Hg removal in groundwater and DI water. As shown in Fig. 3a, Hg-laden MoS<sub>2</sub> formed in DI water exhibited no apparent peaks in the XRD spectra. In the groundwater matrix, however, the characteristic reflections of Hg<sub>2</sub>Cl<sub>2</sub> (PDF #73-1247) were observed in the Hg-laden MoS<sub>2</sub>. The formation of Hg<sub>2</sub>Cl<sub>2</sub> in the groundwater was also confirmed with Raman spectra, in which the Raman band that is specific to Hg(I)–Hg(I) was observed at  $\sim 166$  cm<sup>-1</sup> (Fig. 3b).<sup>58</sup> Such a characteristic Raman peak for Hg(I) was absent for Hg-laden MoS<sub>2</sub> formed in DI water, and instead only MoS<sub>2</sub> peaks at 380 cm<sup>-1</sup> and 405 cm<sup>-1</sup> were observed. Both XRD and Raman spectra indicate that the reduction of Hg(II) by MoS<sub>2</sub> and precipitation of Hg(I) with the Cl ion (a major constituent in groundwater) were involved in the Hg removal from groundwater,<sup>46</sup> and Hg removal in DI water might occur by different Hg removal mechanisms.

XPS analysis was performed to characterize chemical compositions and oxidation states of Hg-laden MoS<sub>2</sub> formed in DI water and groundwater. The composition of Hg-laden MoS<sub>2</sub> shown in Fig. S8† confirmed the association of Cl with the Hg removal in the groundwater. Based on the deconvolution of Mo 3d XPS spectra (Fig. 3c), the Hg removal in DI water caused the partial oxidation of MoS<sub>2</sub> to Mo(v), which exhibits the



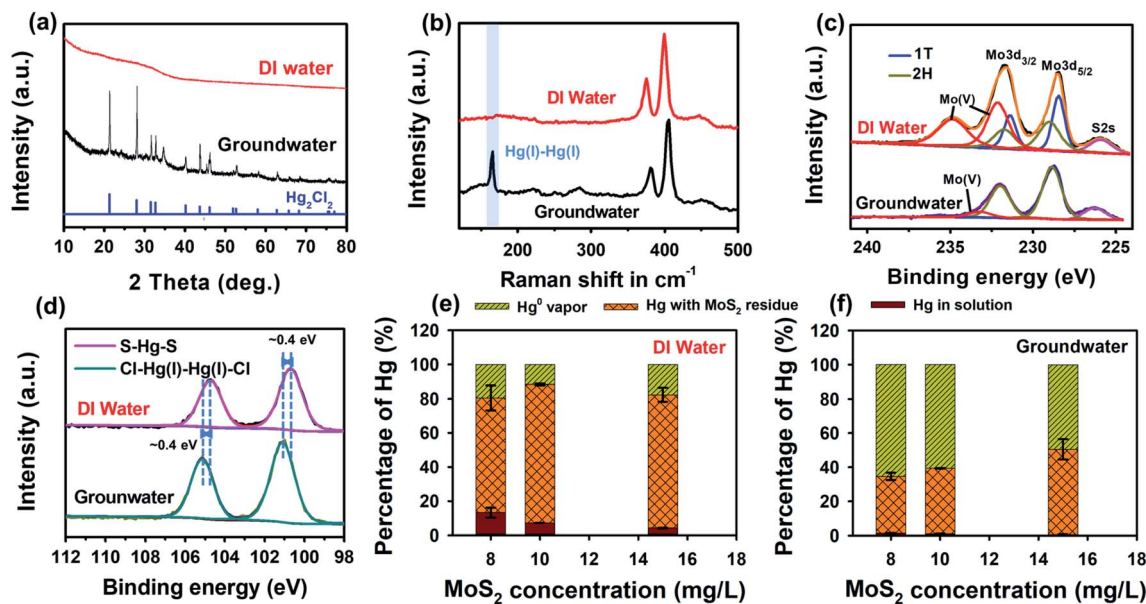


Fig. 3 Mechanistic investigation of Hg(II) removal by MoS<sub>2</sub> nanosheets in groundwater and DI matrices. (a) XRD patterns, (b) Raman spectra, (c) Mo 3d and (d) Hg 4f XPS spectra of Hg-laden MoS<sub>2</sub> formed in DI water and groundwater; Hg species distribution in the Hg-laden MoS<sub>2</sub> nanosheets formed in (e) DI water and (f) groundwater.

characteristic peaks of Mo 3d<sub>5/2</sub> and Mo 3d<sub>3/2</sub> at 232.1 and 234.8 eV, respectively. In groundwater, however, 1T-phase MoS<sub>2</sub> was completely degraded as shown in Fig. 3c, and 2H-phase MoS<sub>2</sub> became the main Mo residue after Hg remediation. The oxidation product of MoS<sub>2</sub> formed in groundwater could not be observed in the XPS spectra, because it existed as soluble MoO<sub>4</sub><sup>2-</sup> species released into the groundwater solution (Fig. 2c). Hg 4f XPS spectra showed the Hg 4f<sub>7/2</sub> and Hg 4f<sub>5/2</sub> peaks of Hg<sub>2</sub>Cl<sub>2</sub> formed in the groundwater were located at ~101.1 and 105.1 eV (Fig. 3d), respectively.<sup>59</sup> The appearance of Hg 4f peaks in Hg-laden MoS<sub>2</sub> formed in DI water was observed at even lower binding energy with a ~0.4 eV shift relative to those in groundwater, implying the complexation of Hg ions with multiple electron-donating S atoms on the MoS<sub>2</sub> surface. Actually, a downward shift of binding energy has been observed in the case of Pb(II) removal by MoS<sub>2</sub>, in which Pb(II) binds to two neighboring S atoms with an equal bond length.<sup>40</sup> Hg(II) as a larger and softer Lewis acid is more likely to form a multi-bonding structure with S, in a similar manner to S–Hg–S arranged in a square planar configuration on the galena surface.<sup>60</sup> The TEM elemental mapping (Fig. S9†) of Hg-laden MoS<sub>2</sub> formed in groundwater exhibited similar element distribution patterns of Hg and Cl because of the formation of Hg<sub>2</sub>Cl<sub>2</sub>. Meanwhile, the overlap of Hg and S elements in the Hg-laden MoS<sub>2</sub> samples formed in DI water also confirms surface adsorption as one of the dominant removal mechanisms when chloride is absent (Fig. S10†).

It is worth noting that Hg<sup>0</sup>, as the possible reduction product of Hg(II), was not observed in the XPS spectra of Hg-laden MoS<sub>2</sub>. This might be due to the ultra-high vacuum conditions we employed in the XPS measurements, which could vaporize Hg<sup>0</sup>. Thus we investigated the mass distribution of Hg species in different physical states to reveal the amount of Hg<sup>0</sup> generated

during the Hg removal by MoS<sub>2</sub> nanosheets in the groundwater and DI water. After Hg removal in both water matrices, Hg species distribution—in solution, with the MoS<sub>2</sub> residue, and in the vapor phase—was calculated to represent the un-removed Hg, the Hg removed *via* surface adsorption or formation of Hg<sub>2</sub>Cl<sub>2</sub>, and reduction product Hg<sup>0</sup>, respectively. The measurements of the mass content of Hg in each phase are described in the Methods, and the species distributions are shown in Fig. 3e and f for the removal in DI water and groundwater, respectively. In DI water, the adsorbed Hg was the major species amounting to ~70–80% of the total Hg (Fig. 3e), which confirmed that surface adsorption played the dominant role in the Hg removal by MoS<sub>2</sub> in the DI water. In the groundwater, the removed Hg predominantly existed as Hg<sup>0</sup> with percentages at 50–65% of the total Hg, and the remaining 35–50% of Hg species existed in the form of Hg<sub>2</sub>Cl<sub>2</sub>. Additionally, almost no residual Hg was detected in the groundwater as compared to ~10% residual Hg found in DI water, which is in line with the enhanced Hg removal performance associated with the groundwater matrix.

The Mo mass distribution results (Fig. S11†) revealed that the dissolved portion in the groundwater accounts for 57–82% of the total Mo added (8–15 mg L<sup>-1</sup>), which is much larger than that in DI water (0.16–2.83%). The significantly enhanced oxidative dissolution of MoS<sub>2</sub> in the Hg-containing groundwater is in good agreement with the observation in Fig. 2c. Overall, the characterization and mass distribution of Hg-laden MoS<sub>2</sub> demonstrated that the groundwater matrix (*i.e.*, the presence of Cl) could promote the redox reactions between Hg and MoS<sub>2</sub>, induce vast generation of reduced Hg species (*i.e.*, Hg<sup>0</sup> and monovalent Hg), and thus enhance the overall removal capacity of Hg by MoS<sub>2</sub> nanosheets as compared to the removal in DI water.



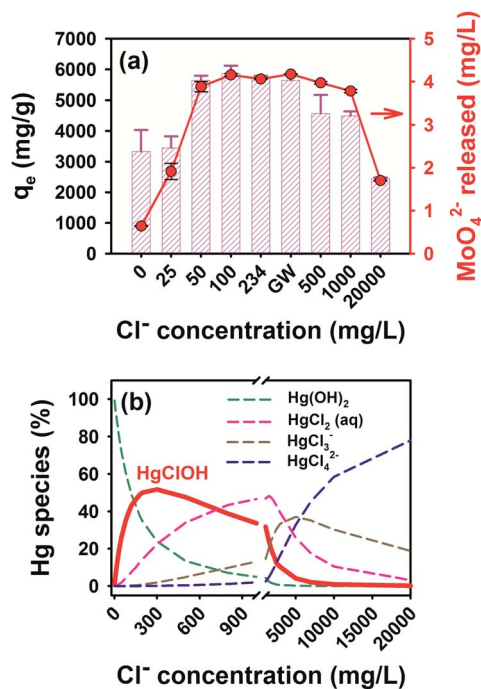


Fig. 4 Speciation-dependent Hg removal efficiency varied by  $\text{Cl}^-$  concentrations. (a) Effects of  $\text{Cl}^-$  on Hg removal by  $\text{MoS}_2$ ,  $C_{\text{Hg}} = 35 \text{ mg L}^{-1}$  and  $C_{\text{MoS}_2} = 4 \text{ mg L}^{-1}$ . (b) Hg speciation as a function of  $\text{Cl}^-$  concentration determined by using Visual MINTEQ.

### 3.4 $\text{Cl}^-$ effect on Hg removal efficiency and mechanisms

To reveal the role of chloride in the case of Hg removal by  $\text{MoS}_2$ , we measured the Hg removal capacities by  $\text{MoS}_2$  in solutions containing various concentrations of  $\text{Cl}^-$ . As shown in Fig. 4a, the Hg uptake density of  $\text{MoS}_2$  increased from  $\sim 3331 \text{ mg g}^{-1}$  to  $\sim 5723 \text{ mg g}^{-1}$  with increasing concentrations of  $\text{Cl}^-$  from 0 to  $\sim 234 \text{ mg L}^{-1}$ , the typical  $\text{Cl}^-$  concentration in groundwater. Further increase of  $\text{Cl}^-$  to  $500 \text{ mg L}^{-1}$  and above would decrease the uptake density, eventually down to  $2445 \text{ mg g}^{-1}$  when the  $\text{Cl}^-$  concentration was  $20\,000 \text{ mg L}^{-1}$ , typically found in seawater. The profile of  $\text{MoS}_2$  oxidative release was in line with the Hg uptake trend, in which moderate  $\text{Cl}^-$  concentrations enhanced the release and the high  $\text{Cl}^-$  content inhibited the  $\text{MoS}_2$  oxidative dissolution (Fig. 4a). The control test without Hg addition indicated that  $\text{Cl}^-$  alone did not change the  $\text{MoS}_2$  oxidation and Mo release behavior (Fig. S12†).

To explain inverted U-shaped Hg removal as a function of  $\text{Cl}^-$  concentration, the distribution of soluble Hg species as a function of  $\text{Cl}^-$  concentration was calculated by using Visual Minteq (Fig. 4b).<sup>55</sup> At the concentration of  $\text{Cl}^-$  in the chosen groundwater, soluble Hg predominantly exists as  $\text{HgClO}(\text{H})$  at  $\sim 51\%$  (Fig. S13†).  $\text{HgClO}(\text{H})$  species exhibit a similar inverted U-shaped pattern to the Hg removal in response to various  $\text{Cl}^-$  concentrations: the formation of  $\text{HgClO}(\text{H})$  was promoted at moderate  $\text{Cl}^-$  concentrations (0 to  $300 \text{ mg L}^{-1}$ ) but was inhibited at high  $\text{Cl}^-$  concentrations ( $800 \text{ mg L}^{-1}$  above), where the dominant Hg species shifted to  $\text{Cl}^-$  complexed Hg such as  $\text{HgCl}_2$ ,  $\text{HgCl}_3^-$ , and  $\text{HgCl}_4^{2-}$  (Fig. 4b). The inhibition of these

stable aqueous  $\text{Hg}(\text{II})$  complexes in the Hg reductive and adsorptive removal has been observed previously.<sup>55,61–63</sup>

Considering the strong correlation between Hg removal capacity and  $\text{HgClO}(\text{H})$  percentages, we proposed the following steps that may account for the enhanced Hg removal in groundwater. First,  $\text{HgClO}(\text{H})$  was adsorbed onto the surface of  $\text{MoS}_2$  via Hg–S bonding owing to the high affinity of S atoms as a soft Lewis base to Hg species, followed by the split of adsorbed  $\text{HgClO}(\text{H})$  into  $\cdot\text{OH}$  and  $\cdot\text{HgCl}$  radicals on the  $\text{MoS}_2$  surface.<sup>46</sup> The homolytic cleavage of the Hg–O bond has been found to be a spontaneous step with a small energy barrier if any to overcome in the previous study.<sup>46</sup> Consequently,  $\cdot\text{HgCl}$  radicals could either dimerize into the  $\text{Hg}_2\text{Cl}_2$  precipitate ( $K_{\text{sp}} = 5 \times 10^{-20}$ )<sup>64</sup> or accept another electron from  $\text{MoS}_2$  and reduce to  $\text{Hg}^0$ .<sup>65</sup> Owing to the stability of  $\text{Hg}(\text{I})$  associated with Cl, the stepwise reduction of  $\text{Hg}(\text{II})$  by  $\text{MoS}_2$  was favored leading to the enhanced total Hg removal. Meanwhile the resulting  $\cdot\text{OH}$  radicals caused nearly complete oxidation of  $\text{MoS}_2$  to soluble Mo and S species.<sup>66</sup> In DI water, however, the reductive removal of Hg is slow because uncomplexed  $\text{Hg}(\text{I})$  is not stable and direct two-electron reduction is kinetically inhibited.<sup>53</sup> Thermodynamically, the formation of  $\text{Hg}_2^{2+}$  associated with Cl is also favored over direct reduction to  $\text{Hg}^0$  because the redox potential  $E^\circ$  for the  $\text{Hg}_2^{2+}/\text{Hg}_2^{2+}$  couple (0.91 V) is greater than that for the  $\text{Hg}^{2+}/\text{Hg}^0$  couple (0.85 V).<sup>53</sup>

The importance of  $\text{HgClO}(\text{H})$  in the reductive removal of  $\text{Hg}(\text{II})$  by  $\text{MoS}_2$  can also be demonstrated by the pH-varied Hg removal. Fig. S14† exhibits the declined Hg removal efficiency by  $\text{MoS}_2$  nanosheets under lower pH conditions, which could be partially explained by the decreased amounts of  $\text{HgClO}(\text{H})$  formed under these conditions. Specifically, the Hg removal efficiency decreased from 94.2% to 33.2% as the equilibrium pH was adjusted from 7.9 to 3.0. The Hg species distribution as a function of pH is shown in Fig. S14b,† which clearly shows the conversion of the dominant Hg species from  $\text{HgClO}(\text{H})$  to  $\text{HgCl}_2$  when the pH was lowered. The correlation of  $\text{HgClO}(\text{H})$  dominance with the highest Hg removal efficiency at pH 8 supports the finding that the  $\text{HgClO}(\text{H})$  species contribute to the reductive removal and thus enhance the overall removal efficiency. In addition, low pH conditions would decrease the Hg removal efficiency via the protonation and charge-neutralization of  $\text{MoS}_2$  nanosheets.<sup>55,67</sup>

### 3.5 Toward practical application of $\text{MoS}_2$ in Hg remediation

For engineered remediation use, immobilization of Hg on materials is of great importance to minimize the migration, bioavailability and toxicity of Hg.<sup>50</sup> Activated carbon (AC), as a common adsorbent for heavy metal remediation in groundwater,<sup>68</sup> was chosen as a reference for comparison. The Hg removal capacity by AC was determined to be  $55.5 \text{ mg g}^{-1}$  (Fig. S15†), much lower than that of  $\text{MoS}_2$ . Consequently, significantly high dosage of AC ( $\sim 200$  times as much as  $\text{MoS}_2$  used) has to be employed to achieve a similar Hg loading mass onto the remediation materials. The Hg release behavior of the Hg-laden  $\text{MoS}_2$  nanosheets and AC was examined with fresh groundwater, acid solution (mass ratio of  $\text{H}_2\text{SO}_4$  and  $\text{HNO}_3$  at





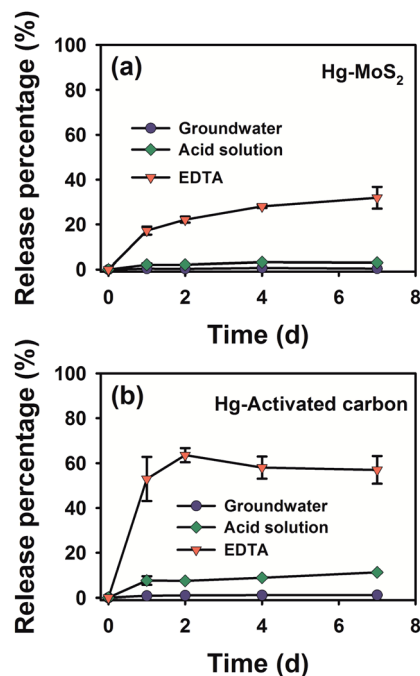


Fig. 5 Desorption kinetics of Hg from (a) MoS<sub>2</sub> and (b) activated carbon in the groundwater, acid solution, and EDTA solution, initial  $C_{\text{Hg}} = 20 \text{ mg L}^{-1}$ ,  $C_{\text{MoS}_2} = 8 \text{ mg L}^{-1}$ ,  $C_{\text{AC}} = 1.67 \text{ g L}^{-1}$ .

2 : 1,  $\text{pH} = 3.20 \pm 0.05$ ), and EDTA solution, to simulate the natural state fluid, acid rain, and strong metal complexing agent, respectively.<sup>69,70</sup> Generally, as shown in Fig. 5a and b, the amount of released Hg from MoS<sub>2</sub> or AC increased slowly over 1 d, and then gradually reached an equilibrium in 2–4 d. Upon equilibrium, the desorption efficiencies of Hg-laden MoS<sub>2</sub> were 0.4%, 3.0%, and 28% (the ratio of desorbed Hg over the actual amount of Hg immobilized by MoS<sub>2</sub> estimated from Fig. 3f) in the simulated groundwater, acid solution, and EDTA solution, respectively, as compared to apparently higher desorption degrees of 1.2%, 12%, and 60% in the case of AC (Fig. 5b). These results indicated that MoS<sub>2</sub> has stronger Hg immobilization capability against release in various types of extractants, which is more conducive to the remediation of Hg pollution in the groundwater environment.

Despite the strong immobilization of Hg by MoS<sub>2</sub>, the redox reactions between Hg(II) and MoS<sub>2</sub> nanosheets are potential concerns towards the practical applications of MoS<sub>2</sub> in the remediation of Hg-containing groundwater. Hg reduction could decrease the content of soluble Hg(II) that is readily available for conversion to more toxic MeHg by microbial activities. However, it may also unintentionally lead to the generation of toxic Hg<sup>0</sup> vapor.<sup>71</sup> Additionally, MoS<sub>2</sub> overdose and the oxidative release of MoO<sub>4</sub><sup>2-</sup> may cause secondary pollution. To address these concerns, the concentration of MoS<sub>2</sub> should be optimized in practical applications, and the fate and transport behaviors of the remaining MoS<sub>2</sub> should be investigated to evaluate the environmental risks. Phase engineering of MoS<sub>2</sub> is also suggested for future studies to enhance the chemical stability of MoS<sub>2</sub> and to minimize the redox reactions between oxidants (e.g., Hg(II) and

dissolved oxygen) and 1T-MoS<sub>2</sub>, and thus eliminate the release of potential hazardous secondary species.<sup>35</sup> Also, the *ex situ* treatment of Hg-containing groundwater with MoS<sub>2</sub> is suggested at the current stage to better manage the remediation process and avoid the uncontrollable release.

## 4. Conclusions

Our study demonstrated that the groundwater matrix has profound implications on the Hg removal efficiency and mechanisms by MoS<sub>2</sub> nanosheets. In DI water free of Cl<sup>-</sup>, MoS<sub>2</sub> nanosheets remove Hg with a moderate capacity *via* adsorption as the dominant mechanism. In this mechanism, Hg ions are selectively removed over other divalent cations because of the strong affinity to MoS<sub>2</sub> *via* Lewis soft–soft interactions and are likely to complex with multiple S atoms on the MoS<sub>2</sub> surface. In groundwater containing Cl<sup>-</sup>, the formation of HgClOH, as the major species, kinetically and thermodynamically promotes the reduction of Hg(II) to Hg<sub>2</sub>Cl<sub>2</sub> and Hg<sup>0</sup>, which becomes the predominant removal mechanism. This reduction-based removal further enhances the total Hg removal capacity of MoS<sub>2</sub> nanosheets to  $\sim 6288 \text{ mg g}^{-1}$ , which is among the highest values reported for Hg to date. Considering the excellent dispersity of MoS<sub>2</sub>, stability of Hg-laden MoS<sub>2</sub>, and low toxicity of MoS<sub>2</sub>,<sup>72</sup> we believe that MoS<sub>2</sub> nanosheets have great potential in the remediation of Hg-contaminated groundwater. Additionally, our work suggests that future studies should consider matrix effects on the performance of remediation materials in the groundwater environment.

## Author contributions

Mengxia Wang: methodology, investigation, data analysis, visualization, writing – original draft; Qi Han: investigation, data analysis; Yufei Shu: investigation, data analysis; Kunkun Wang: investigation, data analysis; Li Wang: investigation, data analysis; Bei Liu: investigation, data analysis, writing – review & editing; Ines Zucker: writing – review & editing; Zhongying Wang: supervision, project administration, writing – review & editing.

## Conflicts of interest

There is no conflict of interest for this research.

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