


Cite this: *J. Mater. Chem. A*, 2024, **12**, 11332

# Spatial tuning of adsorption enthalpies by exploiting spectator group effects in organosilica carbon capture materials†

Mario Evers,<sup>a</sup> Karin Hauser,<sup>b</sup> Wolfgang G. Hinze,<sup>b</sup> Nele Klinkenberg,<sup>b</sup> Yasar Krysiak,<sup>b</sup> Daniel Momers†<sup>a</sup> and Sebastian Polarz <sup>†\*a</sup>

Functional gradient materials can process more complex tasks than a mixture of their homogeneous analogs. Generating such materials is difficult as it necessitates spatial control over chemical and/or structural properties. A gradient is a unique degree of freedom in hierarchical material architectures, and as such, biology has managed exploiting the full potential of graded structures. For instance, despite being present at a comparably low concentration (approaching 420 ppm in 2023), plants are capable of capturing carbon dioxide from the air. Binding occurs in the carboxysome, a complex entity characterized by pores with engineered surfaces composed of shell proteins that create a concentration gradient of CO<sub>2</sub> towards an enzyme responsible for the first conversion step. The current paper hypothesizes that porous organosilica materials can mimic some of the features of the mentioned biological paragon. Primary amines as sites for interacting with CO<sub>2</sub> are surrounded by spectator groups on bifunctional surfaces. It is found that the proper choice of the spectator group almost doubles the adsorption enthalpy. Above a critical density, the hydrophobic moieties create a quasi-solvent layer on the surfaces in which CO<sub>2</sub> molecules dissolve. When the density of the spectator groups gradually changes inside a graded organosilica monolith, one obtains zones varying systematically in adsorption enthalpy. Directionality in affinity towards CO<sub>2</sub> and controlled transport properties are realized.

Received 28th February 2024  
Accepted 3rd April 2024

DOI: 10.1039/d4ta01381f

rsc.li/materials-a

## Introduction

Scientific investigations in different fields clearly show that the atmosphere's composition, the abundance of so-called greenhouse gases such as carbon dioxide (CO<sub>2</sub>), correlates with the medium temperature at the earth's surface. With growing populations and economies, one cannot foresee when there will be a turning point in the increase in the CO<sub>2</sub> concentration which has already reached 419 ppm in the meantime. Given that industrial plants, transportation, and animal husbandry will continue to emit greenhouse gases for the next few decades, it is obvious that trapping those gases before they reach the atmosphere represents an indispensable step in all future climate management scenarios. An even larger challenge is to reduce the atmospheric concentration by adsorption of CO<sub>2</sub> despite it being only a minor constituent of air. This is where carbon capture materials (CCMs) become important.<sup>1,2</sup> The

optimization of the uptake capacity for CO<sub>2</sub> is one important task in the development of CCMs, and impressive progress has been made and is reported in the literature.<sup>3</sup> As expected, the specific surface area combined with the density of CO<sub>2</sub>-binding functionalities determines the uptake capacity. For instance, microporous materials such as metal-organic frameworks (MOFs) have proven highly valuable CCMs.<sup>4</sup> However, considering the huge amount of CO<sub>2</sub>, it is questionable that the long-term storage of solid, gas-loaded adsorbents is the best way. This poses the question of whether uptake capacity is a CCM's most important aspect. For sure, it is not the only aspect.

To learn about what other features beyond capacity are important for future technical solutions to the problem, it is worth considering how nature deals with atmospheric CO<sub>2</sub>. Plants can bind CO<sub>2</sub> from the air under ambient conditions. Fixation occurs in the carboxysome and is succeeded by the redox-activated conversion of CO<sub>2</sub>.<sup>5,6</sup> Overall, the carboxysome acts as a specialized compartment that creates a concentration gradient of CO<sub>2</sub> around the enzyme responsible for the conversion reaction.<sup>7</sup> Carbon dioxide from the surrounding environment diffuses into the carboxysome through small pores with engineered surfaces composed of shell proteins. Once inside the carboxysome, carbon dioxide reacts with water to form bicarbonate ions. This reaction is facilitated by the enzyme carbonic anhydrase. The bicarbonate ions are

<sup>a</sup>Institute of Inorganic Chemistry, Leibniz-University of Hannover, Callinstrasse 9, 30167 Hannover, Germany. E-mail: sebastian.polarz@aca.uni-hannover.de<sup>b</sup>Department of Chemistry, University of Konstanz, Universitaetsstrasse 10, 78457 Konstanz, Germany† Electronic supplementary information (ESI) available. See DOI: <https://doi.org/10.1039/d4ta01381f>

‡ SP and DM contributed equally to this work.



channeled towards succeeding enzymes. An alternative enzyme is crotonyl-CoA carboxylase/reductase (CCR).<sup>8</sup> The newest results have shown that the enzyme contains a hydrophobic CO<sub>2</sub>-binding pocket in the active site.<sup>9</sup> The surface of the cavity is characterized by four amino acids, most importantly phenylalanine which efficiently excludes water from the active site and therefore limits unwanted irreversible side reactions.

Multiple conclusions can be drawn from those biological examples for effectively removing CO<sub>2</sub> from a gas phase, which are also relevant for developing and improving technical systems. The biological approach indicates that capacity can be a minor aspect. In essence, the chemical structures of the surfaces of the adsorbent material have to be engineered much more precisely. For capturing CO<sub>2</sub> close to ambient conditions, preferably even from normal air, and for transportation of the loaded CCM, the adsorption enthalpy  $\Delta H_{\text{ads}}$  must not be too low. However, even for a CCM with high uptake capacity, at a certain point, its regeneration is vital and must be possible without significant energy consumption. Thus, strongly bound carbon dioxide is not always preferred. The range in which the CO<sub>2</sub> medium is strongly attached to the surface is between physisorption and chemisorption, corresponding to  $-100 \text{ kJ mol}^{-1} > \Delta H_{\text{ads}} > -50 \text{ kJ mol}^{-1}$ . The precise adjustment of  $\Delta H_{\text{ads}}(\text{CO}_2)$  cannot be managed by pore-size engineering alone, but rather control over active surface functionalities attached to the pore-walls is necessary. The chemical structure of the surfaces in a CCM has many more implications, most importantly regarding selectivity. In a mixture, different compounds compete for adsorption sites, and it is particularly difficult to separate weakly interacting and low concentrated species. CO<sub>2</sub> can interact with Lewis-basic centers, such as primary amine groups, as do water molecules (H<sub>2</sub>O) *via* hydrogen binding.<sup>10</sup>

Special adsorbent materials with bifunctional surfaces have already been discussed in the literature.<sup>11</sup> In the so-called synergistic approach, bifunctional surfaces can exhibit special effects, where different functional groups work cooperatively to enhance CO<sub>2</sub> adsorption. For example, combining amine groups (such as primary, secondary, or tertiary amines) with other functional groups such as carboxyl (–COOH), hydroxyl (–OH), or imidazole (–NH) on a surface can create more favorable interactions with CO<sub>2</sub>. The amine groups can form chemical bonds (amine–CO<sub>2</sub> adducts), while the other functional groups provide additional sites for physical interactions (such as hydrogen bonding) with CO<sub>2</sub> molecules. The presence of a secondary group can also affect the adsorption capacity. Bifunctional surfaces can serve as both adsorbents and catalysts for CO<sub>2</sub> conversion. The functional groups on the surface can activate CO<sub>2</sub> molecules, making them more reactive for subsequent chemical transformations. This allows the possibility of utilizing the adsorbent–catalyst synergy to capture and convert CO<sub>2</sub> simultaneously.

For the current paper, the most important aspect is that bifunctional surfaces can also enhance the recyclability of the adsorbent, *i.e.*, the release of adsorbed CO<sub>2</sub>, which can be facilitated by controlling the desorption temperature or exploiting the functional groups' reversible nature. It is well

known in the literature that modifying surfaces with non-polar groups such as hydrocarbons results in hydrophobicity.<sup>12</sup> However, how these groups affect  $\Delta H_{\text{ads}}(\text{CO}_2)$  has not been investigated in-depth. The latter aspect represents the focus of the paper presented herein. Because the mentioned hydrophobic groups cannot interact with CO<sub>2</sub> *via* Lewis acid-base pair formation or hydrogen bonding, we call them spectator groups. How do spectator groups change  $\Delta H_{\text{ads}}(\text{CO}_2)$ ?

Nanoporous CCMs with bifunctional surfaces are required to investigate the formulated question. Although porous organosilica materials may not have specific surface areas as high as those for microporous materials such as zeolites, MOFs, or charcoal and consequently fall behind regarding uptake capacity, it has been proven that an extremely rich surface chemistry is possible.<sup>13–16</sup> A special approach involves the use of sol–gel precursors containing a bridging organic (functional) unit R<sub>F</sub>: (RO)<sub>3</sub>Si–R<sub>F</sub>–Si(OR)<sub>3</sub>.<sup>15</sup> The undiluted precursor is converted to organosilica materials R<sub>F</sub>Si<sub>2</sub>O<sub>3</sub> with a very high content of organic functionality. The sol–gel process can be performed in the presence of a template which generates porosity after removal. Bi- and multifunctional materials can be prepared by mixing different precursors containing R<sub>F1,2</sub>, in the sol. This approach is known in the literature as the co-condensation route. Several years ago, we were able to show that the distribution of two different functionalities R<sub>F1</sub> = –NH<sub>2</sub> and R<sub>F2</sub> = –COOH is statistical.<sup>17</sup> The composition of the material (R<sub>F1</sub>)<sub>x</sub>(R<sub>F2</sub>)<sub>1–x</sub> Si<sub>2</sub>O<sub>3</sub> can be varied freely from  $x = 0$  to  $x = 1$ , directly affecting the distance between R<sub>F1</sub> and R<sub>F2</sub> and their intermolecular interaction. Another approach to introduce bifunctionality into a porous organosilica material is the so-called post-modification. If R<sub>F1</sub> is reactive and can be converted to R<sub>F2</sub>, one can also obtain (R<sub>F1</sub>)<sub>x</sub>(R<sub>F2</sub>)<sub>1–x</sub> Si<sub>2</sub>O<sub>3</sub>. The composition depends on the degree of conversion and, thus, on parameters such as the concentration of reactants, temperature, *etc.* In our research, we could establish R<sub>F1</sub> (=–N<sub>3</sub>, –CH = CH<sub>2</sub>, –C≡CH, –SH, *etc.*) representing a group capable of undergoing click-chemistry, which was used for the preparation of a multitude of mono- and bifunctional organosilica materials.<sup>18–23</sup>

Although many papers exist in the literature on bifunctional organosilica materials,<sup>24–27</sup> only a few papers deal with the importance of the secondary group in adsorption processes and CCM applications in particular. In a recent paper, we investigated the role of R<sub>F1</sub> = –COOH next to combined surface-bound primary amines R<sub>F2</sub> = –NH<sub>2</sub> for the properties of porous organosilica materials in CO<sub>2</sub> adsorption.<sup>28</sup> It was found that there is a cooperative binding of CO<sub>2</sub> if R<sub>F1</sub> and R<sub>F2</sub> are next to each other on the surface. R<sub>F1</sub> = –COOH is obviously not a spectator group as it interacts directly with surface-bound CO<sub>2</sub> molecules. In the latter paper, we have already recognized that passive neighboring groups also seem to influence  $\Delta H_{\text{ads}}(\text{CO}_2)$ , but the effect was not studied in detail.

Here, we propose a porous organosilica material with regions differing in the presence of the spectator group. These regions would then be connected to different  $\Delta H_{\text{ads}}(\text{CO}_2)$  values. So-called functional gradient materials (FGMs) are expected to fulfill more complex tasks compared to homogeneous materials





Chart 1 Two-step synthesis of amine-modified organosilica materials containing hydrophobic moieties ( $R_{F2}$ ) as spectator groups.

as discussed in the nice review article by Pragya *et al.*<sup>29</sup> FGMS have also been proposed for their large potential in carbon capture applications,<sup>3,30–33</sup> but there are only a few experimental realizations yet. We could already show that organosilica materials containing chemical and/or structural gradients can be prepared using click-chemistry.<sup>18,22,28</sup> For instance, ref. 18 described the attachment of dye molecules to the surfaces of azide-functionalized organosilica molecules using the copper-catalyzed Huisgen cycloaddition reaction. The conversion of the azide groups was managed to depend on the position of the materials, and this allowed the introduction of the chemical gradient.

The current paper is organized as follows. In the first section, we present the preparation and characterization of amine-functionalized organosilica materials with aerogel structures containing a broad selection of spectator groups (see Chart 1). The adsorption properties of the materials are investigated with particular emphasis on identifying connections between the nature of the spectator groups and  $\Delta H_{\text{ads}}(\text{CO}_2)$  will be identified. In the final section of the paper, we approach a gradient material and want to prove that there is a spatial dependency of  $\Delta H_{\text{ads}}(\text{CO}_2)$ .

## Results and discussion

### Preparation of bifunctional materials

Starting from the azide-modified organosilica aerogel (=AzSil; for characterization, see ESI Fig. S1†)<sup>18,28,34</sup> the target materials were prepared in a two-step process shown in Chart 1; see also the experimental part. The first step involves the attachment of primary amine groups from the copper-catalyzed click reaction of AzSil with a *tert*-butyloxycarbonyl (boc) protected propargylamine. After deprotection, one obtains  $\text{Am}_x\text{Sil}$  with the subscript defining the degree of conversion of the azide groups. The analytical data of this reference material are given in ESI Fig. S2.† The residual azide groups in  $\text{Am}_x\text{Sil}$  were then reacted in a second step with terminal alkynes to introduce  $R_{F2}$ . At this point, all accessible azide groups will be consumed. However, a small portion might still be present, for instance, inside the pore walls. Depending on the spectator group (=  $R_{F2}$ ), those materials are denoted as  $\text{Am}_x\text{Sp}(\text{a-f})_y\text{Sil}$ .

Data for the materials  $\text{Am}_x\text{Sp}(\text{a-g})_y\text{Sil}$  are summarized in the ESI Fig. S1–3–8.† The analysis of the chemical composition of  $\text{Am}_x\text{Sp}(\text{d})_y\text{Sil}$  is discussed as a representative case. The total degree of azide functionalization ( $x + y$ ) can be determined from Fourier-transform infrared (FT-IR) spectroscopy and thermogravimetric analysis (TGA). Fig. 1a shows the FT-IR fingerprint region of  $\text{Am}_x\text{Sp}(\text{d})_y\text{Sil}$  in comparison to AzSil and  $\text{Am}_{0.57}\text{Sil}$  as references. The spectra were referenced to the intensity of the Si–O–Si band. Because the siloxane network is not affected by the chemical reactions (Chart 1), the band is suitable for comparing the samples among each other. The assignment of the bands is shown in more detail in ESI Fig. S6† as  $\text{Am}_x\text{Sp}(\text{d})_y\text{Sil}$  contains all relevant groups, residual azide, the triazole ring, the amine group and *tert*-butylphenyl as a SG. The signal at  $2115\text{ cm}^{-1}$  is characteristic of the azide group. It can be seen that the band is very weak for  $\text{Am}_x\text{Sp}(\text{d})_y\text{Sil}$ . The decrease in the intensity (peak area) indicates that 80% ( $= x + y$ ) of the azide groups have been converted. Thermogravimetric analysis (TGA) can be used as an independent method to determine the sum  $x + y$ . Fig. 1b shows the TGA analysis of  $\text{Am}_x\text{Sp}(\text{d})_y\text{Sil}$  performed in an atmosphere containing 50%  $\text{O}_2$  and 50%  $\text{N}_2$ . After loss of residual water in the temperature range below  $T = 120^\circ\text{C}$ , one sees two main steps with a maximum in the first derivative of the TGA data at  $T_1 = 416^\circ\text{C}$  and  $T_2 = 546^\circ\text{C}$ . The first main decomposition step is at the same temperature compared to  $\text{Am}_x\text{Sil}$  materials. The missing decomposition step at  $T = 295^\circ\text{C}$  agrees with the almost quantitative conversion of the azide functionalities, which has been deduced from IR spectroscopy. We conclude that  $T_2$  corresponds to the presence of SP(d) and a ratio of Am to Sp(d) equal to  $\approx 1 : 1$ . The conversion of  $\text{Am}_x\text{Sp}(\text{d})_y\text{Sil}$  to  $\text{SiO}_2$  corresponds to a mass-loss of 60.8% and thus  $x + y = 0.77$ . Because the separate values of  $x$  and  $y$  cannot be determined from TGA data with absolute precision, we adopted a method developed by us in the past to determine the composition by liquid nuclear magnetic resonance (NMR) spectroscopy.<sup>35</sup> Organosilica materials ( $\text{Am}_x\text{Sp}_y\text{Az}_{1-x-y}\text{Si}_2\text{O}_3$ ) can be dissolved quantitatively at elevated pH values ( $>10$ ) resulting in deprotonated silicic acid species  $\text{AmSi}_2(\text{OH})_n(\text{O}^-)_m$ ,  $\text{SPSi}_2(\text{OH})_n(\text{O}^-)_m$ ,  $\text{AzSi}_2(\text{OH})_n(\text{O}^-)_m$  (Fig. 1c). These species are soluble in deuterated water,  $\text{D}_2\text{O}$ , and the quantitative evaluation of the  $^1\text{H}$ -NMR spectra allows us to deduce the values for  $x$





**Fig. 1** (a) FT-IR spectra of AzSil (black), AmSil (red) and Am<sub>x</sub>Sp<sub>y</sub>(d)Sil (blue; R<sub>F2</sub> = *tert*-butyl phenyl). (b) TGA trace (solid line) for the oxidative decomposition of AmSp(d)Sil (black) and the first derivative (dashed line) in comparison to the decomposition steps of AmSil (grey). (c) <sup>1</sup>H-NMR spectrum (aromatic region) of the dissolved Am<sub>x</sub>Sp<sub>y</sub>(d)Sil sample. (d) Results for the composition analysis of the different samples; squares (x + y determined from IR), circles (x + y determined from TGA), hashes (x determined from NMR), triangles (y determined from NMR), hexagons (x + y determined from NMR), and pentagons (x + y; averaged value).

and y. For instance, the signals at  $\delta = 8.04$  can be assigned to the R<sub>F1</sub> = Am group, at 7.38 to R<sub>F1</sub> = SP(d) and at 7.83 to residual Az. For the concrete assignment of the signals in the aromatic region, refer to ESI Fig. S6.† The described analysis results in a composition Am<sub>0.48</sub>Sp<sub>0.42</sub>Si and agrees with the values obtained from the TGA measurement. The results for the analysis of the composition for the other samples Am<sub>x</sub>-SP(a,b,c,e,f) are shown in Fig. 1d and the original data are shown in ESI Fig. SI-3–8.†

The total conversion (x + y) is quite constant for all bifunctional samples. Because the first click-reaction was performed under the same conditions, the number of amine groups also varies only a little. Because of the different kinetics with the second click-step for the attachment of the different R<sub>F2</sub> groups, it is very hard to avoid that there is a certain variance. In particular, sample AmxSP(c) is distinct from the others.

The structure of the materials and effects of the functionalization process were investigated by scanning electron microscopy (SEM) as shown in Fig. 2a–c and ESI Fig. S3–8.†

The starting material, the monolithic AzSil body (ESI Fig. S1†), possesses an aerogel structure after supercritical drying. The first postmodification step to AmSil has no marked effects on the pore structure, as can be seen from Fig. 2b, and

the monolithic shape is retained (ESI Fig. S2†). However, introducing the hydrophobic *tert*-butyl phenyl group in AmSp(d)Sil during the second modification step (Chart 1) leads to partial densification. The material is still highly porous, but in particular, fewer pores with diameters >100 nm seem to be present.

The material's porosity can be characterized by nitrogen physisorption measurements shown in Fig. 2d. All materials feature a type II isotherm. In interpreting those isotherms, one has to consider that the attachment of organic groups to the existing pore walls increases the mass of the aerogels. Because the density of the material enters the calculations of values from isotherm plots, for parameters such as the specific surface area, for instance, it is expected that the curves for AmSil and AmSp(d)Sil are shifted to lower values. In agreement with this, lower values for the specific surface area  $A_{\text{spec}}$  are also expected (Fig. 2e). However, the drop in  $A_{\text{spec}}$  from 527 m<sup>2</sup> g<sup>−1</sup> for AmSil to 330 m<sup>2</sup> g<sup>−1</sup> for AmSp(d) as an example cannot be explained by the gain of mass alone. As we have already assumed based on the SEM measurements, the post-functionalization process seems to cause a certain degree of compaction of the aerogel. Another consequence of the described compaction is that the micropores in the system almost vanish. The values for  $V_{\text{ads}}$



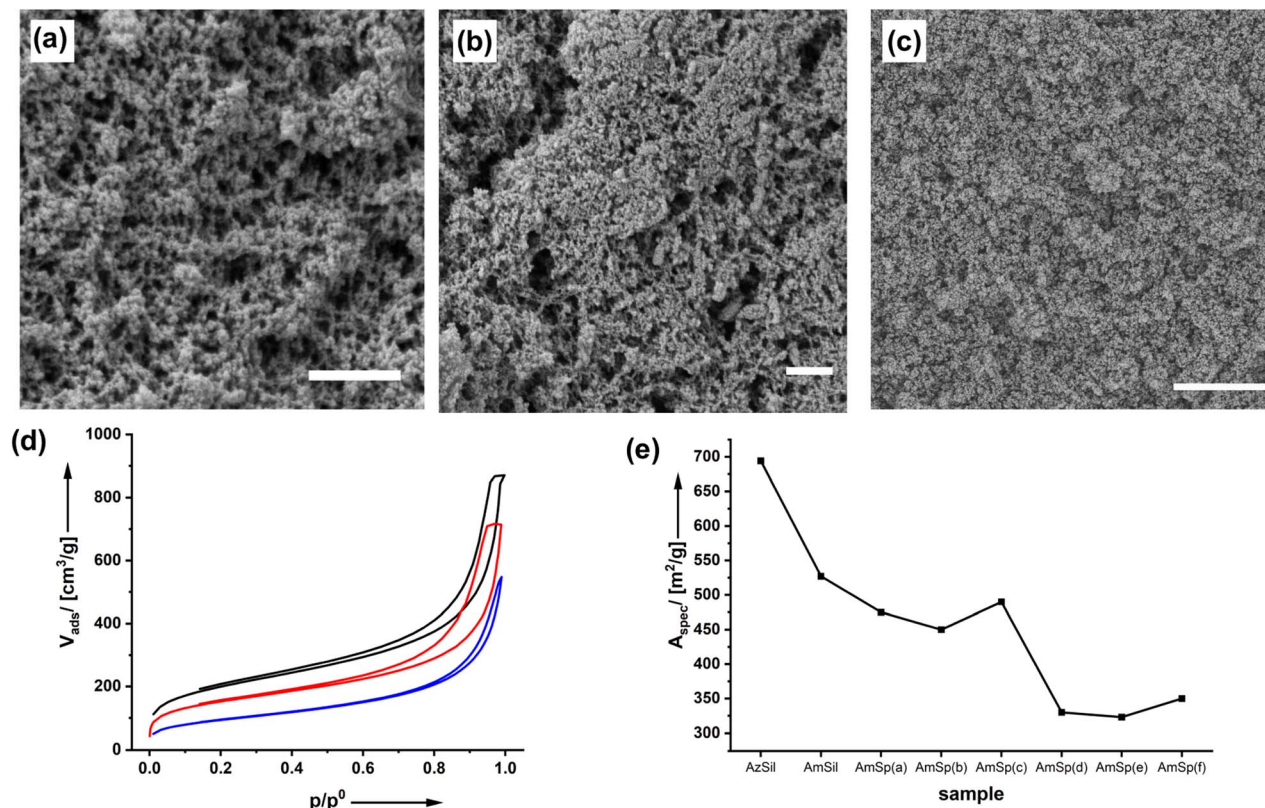


Fig. 2 SEM micrograph of AzSil (a; scalebar = 1  $\mu\text{m}$ ), AmSil (b; scalebar = 1  $\mu\text{m}$ ) and Am<sub>0.48</sub>Sp(d)<sub>0.42</sub>Sil (c; scalebar = 5  $\mu\text{m}$ ). (d) Nitrogen physisorption isotherms (adsorption and desorption) of AzSil (black), AmSil (red) and Am<sub>0.48</sub>Sp(d)<sub>0.42</sub>Sil (blue). (e) Specific surface area of the different organosilica samples as determined by N<sub>2</sub> physisorption measurements.

close to  $p/p^0 = 0$  are indicative of the presence of micropores. One can see in Fig. 2d that there are notable micropores in AzSil. In comparison, the amount of micropores is much lower in AmSil and AmSp(d)Sil. One can also see from Fig. 1e that sample AmxSP(c) shows a little bit different behavior compared to the others.

### Hydrophobicity of materials containing spectator groups

All spectator groups shown in Chart 1 are hydrophobic, and the uptake of water (H<sub>2</sub>O) indicates the prepared materials' hydrophobicity. Therefore, we have measured H<sub>2</sub>O vapor adsorption curves (Fig. 3; ESI Fig. S9<sup>†</sup>). One can see that the introduction of amino groups does not change the hydrophobicity/hydrophilicity of the material. The H<sub>2</sub>O uptake isotherms for AzSil and AmSil are almost identical. Because all spectator groups (a–f) are non-polar, we expect that the water uptake will be reduced because of enhanced hydrophobicity. From chemical intuition, one would sort the samples  $a \rightarrow f \rightarrow d \rightarrow e \rightarrow b \rightarrow c$  in an order of increasing hydrophobicity. Neither the latter nor the order of the van der Waals volumes reflect the empirical order of the water uptake capacities (Fig. 3b). The attachment of the *tert*-butyl phenyl groups leads to an overall lowest water uptake at all pressures. If the adsorption of water is an indication of the hydrophobicity of the material, one can conclude that AmSp(d)Sil is the most hydrophobic material within the series presented here.

### Carbon capture properties of amine-modified organosilica materials containing spectator groups

It is expected that the presence of a hydrophobic group on the surfaces of amine-modified organosilica materials will have consequences for water adsorption. However, none of the spectator groups can interact specifically with carbon dioxide. Thus, the current paragraph addresses how the presence of spectator groups influences the adsorption of CO<sub>2</sub>.

Fig. 4a shows the adsorption isotherm of CO<sub>2</sub> on AmSp(d)Sil. The data for the other samples are given in ESI Fig. S10.<sup>†</sup> The isotherms display a Henry-type behavior. The adsorbed volume at  $p = 1 \text{ atm} = 760 \text{ mm Hg}$  at  $T = 0^\circ \text{C}$  was used to compare the uptake capacity. With values of  $\text{cap} = 1.0\text{--}1.75 \text{ mmol CO}_2 \text{ per gram of material}$  (Fig. 4b), the organosilica aerogels' storage capacity is only average. Materials known in the literature with much higher specific surface area, such as MOFs, possess much better values up to  $5 \text{ mmol g}^{-1}$  under analogous conditions.<sup>36</sup> As stated in the paper's introductory section, the uptake capacity is not the focus of the current work.

The ideal model system would display a constant  $R_{F1} : R_{F2}$  ratio whilst also the internal surface area  $A_{\text{spec}}$  is the same for all materials. The differences in kinetics when using different click reagents lead to a variation in both parameters as documented in Fig. 1d and 2e. It is thus difficult to compare the results directly. Therefore, in Fig. 4b, a second graph shows where  $\text{cap}$  was divided by  $A_{\text{spec}}$  and  $\chi_{\text{amine}}$ . Compared to AmSil, the



Fig. 3 (a) H<sub>2</sub>O vapor adsorption of AzSil (black), AmSil (red) and Am<sub>0.48</sub>Sp(d)<sub>0.42</sub>Sil (blue). (b) Water uptake at  $p/p^0 = 0.86$  for different organosilica materials.

spectator groups have a positive effect on the uptake capacity of the material.

To determine the effectiveness of a CO<sub>2</sub> molecule binding to an amine when the spectators are next to it, we have used  $T$ -dependent adsorption measurements (ESI Fig. S10†) to determine the isosteric adsorption enthalpy  $\Delta H_{\text{ads}}(\text{CO}_2)$ . Fig. 4c shows the results of three materials as an example (AmSil; AmSp(c); AmSp(d)). One sees that there is a pronounced effect of the spectator groups on the adsorption enthalpy. The highest values for  $\Delta H_{\text{ads}}$  are always found at low surface coverage, corresponding to low  $V_{\text{ads}}$  values at STP (standard temperature and pressure). This behavior is nothing unusual because, for most adsorbents, the most reactive sites are typically occupied first. However, one can see that the presence of R<sub>F2</sub> = *tert*-butyl phenyl in AmSP(d)Sil almost doubles  $\Delta H_{\text{ads}}(\text{CO}_2)$  compared to AmSil.

Even for higher surface coverages, there is a notable difference in  $\Delta H_{\text{ads}}(\text{CO}_2)$  between AmSil and AmSP(d)Sil (Fig. 4c). We tried to identify a systematic correlation between the nature of the spectator group and  $\Delta H_{\text{ads}}(\text{CO}_2)$ . One idea is that the hydrophobicity next to the amine site can be a deciding factor. The adsorption of water (Fig. 3) is a good way to quantify the hydrophobicity. The material with the highest tendency to adsorb water is the least hydrophobic in the series (AmSil), and its adsorption value  $V_{\text{ads,H}_2\text{O}}(\text{max})$  at  $p/p^0 = 0.86$  is used as a reference point for the calculation of the relative hydrophobicity index  $I_{\text{hyph}}^{\text{rel}} = 1 - V_{\text{ads,H}_2\text{O}}/V_{\text{ads,H}_2\text{O}}(\text{max})$ . The values for  $\Delta H_{\text{ads}}(\text{CO}_2)_{V_{\text{ads}} \rightarrow 0}$  is then plotted as a function of  $I_{\text{hyph}}^{\text{rel}}$  in Fig. 4d. Interestingly, there is a linear correlation between the hydrophobicity and  $\Delta H_{\text{ads}}(\text{CO}_2)$ . Again, one has to consider that the samples are not absolutely constant in R<sub>F1</sub>:R<sub>F2</sub>, and sample AmxSP(c) deviates more than the others. However, taking into account the large error bars, the correlation is still reliable. What are the possible reasons for the unusual behavior? we propose two alternative hypotheses.

(a) The initial step in the chemisorption of the CO<sub>2</sub> molecules is the Lewis-acid-base reaction with lone pairs at the amine groups, which attack the carbon atom as an electrophilic center. If the nucleophilicity of the amine group is influenced in some way by the spectator groups, one could explain differences in  $\Delta H_{\text{ads}}(\text{CO}_2)$ . More specifically, if the amine becomes more nucleophilic, the bond between C–N becomes stronger. However, one would then expect that the stretching frequency in the IR spectra of the resulting carbamic acid species should differ from material to material and should be shifted to higher wavenumbers the higher the  $\Delta H_{\text{ads}}(\text{CO}_2)$  value is. However, after close inspection of the IR data, we cannot see any frequency shift of the carbamate signals. An alternative explanation for the observed phenomena has to be found.

(b) CO<sub>2</sub> is an unpolar molecule; thus, its solubility is higher in less polar media. We hypothesize that the hydrophobic groups on the surface of the organosilica material act as a quasi-solvent, which may even increase the local concentration of CO<sub>2</sub> and allow the molecule to bind more tightly to the amine functionalities. Similar effects are known in the literature, for instance, for films formed by ionic liquids on the surfaces of porous hosts.<sup>37</sup> In our case, the additional van der Waals (vdW) interactions with the quasi-solvent layer contribute to the adsorption enthalpy.

Molecular modeling calculations (Fig. 5b) support the view that the amine functionality is integrated inside a quite dense phase of the spectator groups forming the outer surface of the pores. Because a carbon dioxide molecule approaching the surface goes through different stages in the adsorption process, we expect that effects can be seen spectroscopically.

Fig. 5a shows DRIFTS (diffuse reflectance infrared Fourier transform spectroscopy) spectra of the sample AmSp(d)Sil, which has shown the strongest spectator group effect in the determination of the adsorption enthalpies (Fig. 4d). The sample was treated with carbon dioxide ( $p = 1$  bar) first. Because the CO<sub>2</sub>

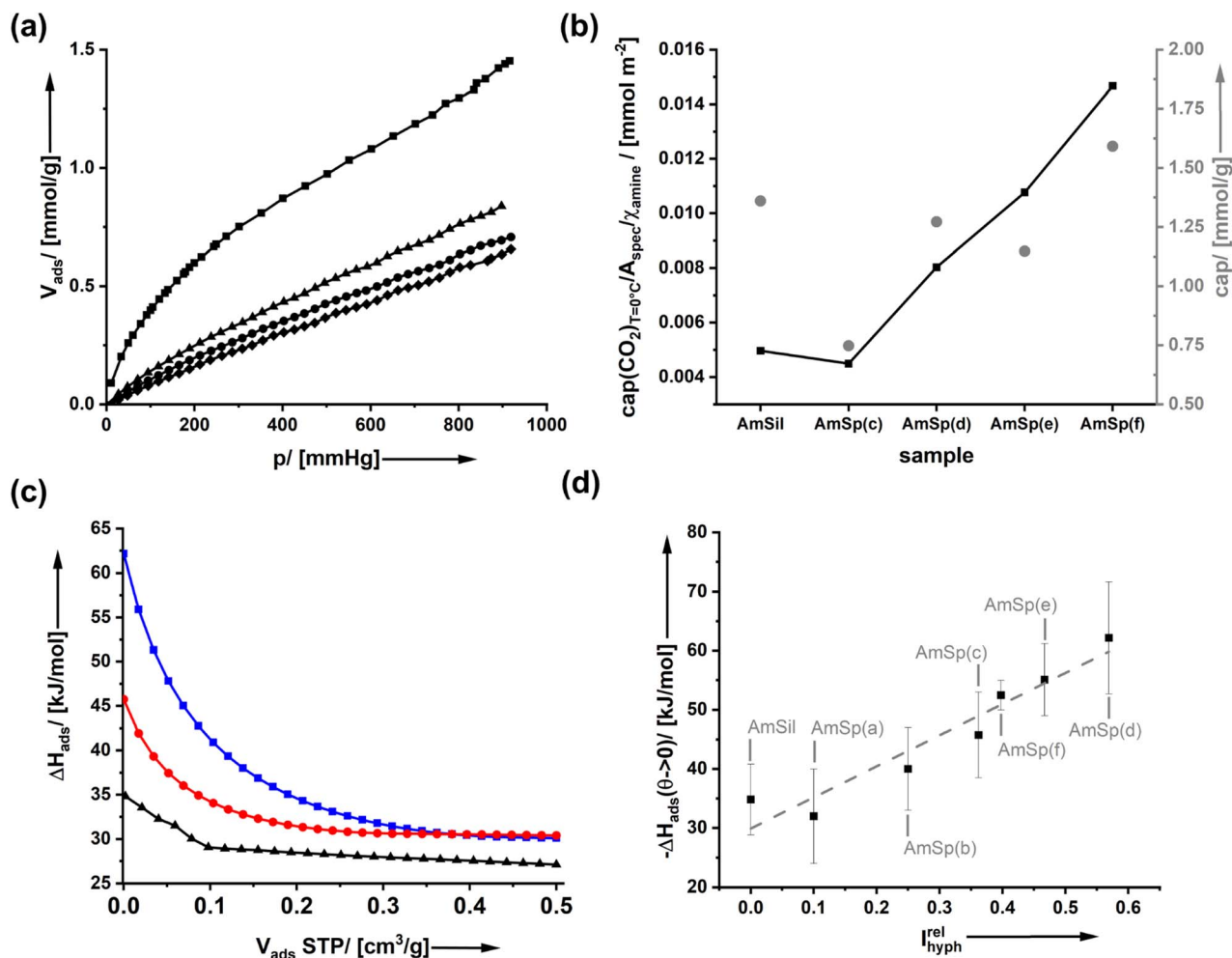


Fig. 4 (a) CO<sub>2</sub> adsorption isotherms of AmSp(d)Sil measured at  $T = 0^\circ\text{C}$  (squares),  $30^\circ\text{C}$  (triangles),  $40^\circ\text{C}$  (circles) and  $50^\circ\text{C}$  (hashes). (b) Comparison of the CO<sub>2</sub> uptake capacity between different organosilica materials; grey circles = capacity in mmol CO<sub>2</sub> per gram material; black line = data referenced to  $A_{\text{spec}}$  and  $\chi_{\text{amine}}$  of the respective sample. (c) isosteric heat of CO<sub>2</sub> adsorption determined from  $T$ -dependent adsorption measurements for three exemplary materials; black triangles = AmSil; red circles AmSp(c); blue squares AmSp(d). (d) Correlation between the isosteric adsorption heat of CO<sub>2</sub> on different organosilica aerogels and the correlation with the relative hydrophobicity index  $I_{\text{hyph}}^{\text{rel}}$ .

in the chamber's atmosphere is irrelevant and interferes with the signals for bound CO<sub>2</sub>, the system was flushed with dry nitrogen. Spectra were recorded at different times and are shown in Fig. 5a. The decrease in the intensity of a reflection signal, indicated by the grey, downward arrows, means that there is more absorption and the corresponding species is forming. *Vice versa*, signals with increasing reflection intensity (upward arrows) stand for species that disappear. Signal assignment was performed according to the extensive literature on amine-modified materials used for carbon dioxide adsorption.<sup>38–40</sup> In good agreement with the literature is the existence and formation of carbamic acid species (see also Fig. 5b), or carbamate-ammonium pairs seen in the region 1750–1550 (signals '1' and '2'). Because those species are more tightly bound, there is only a small change in the corresponding DRFITS signals with time. The region of  $2340\text{ cm}^{-1}$  is characteristic of physically adsorbed species '3'. The reflectance increases, which is not a surprise as physisorbed CO<sub>2</sub> is only weakly bound in such large pores as those present in the organosilica aerogels presented here.

However, we see one more signal in the same spectral region but shifted to slightly higher wavenumbers ('4';  $2377\text{ cm}^{-1}$ ). It seems that this species forms with time as its reflectance decreases. We assume that the vdW interactions with the spectator groups change the vibrations of CO<sub>2</sub> slightly, which would result in a small signal shift to higher wavenumbers. This carbon dioxide species could be the one that resides in a quasi-solvated state in the hydrophobic domain close to the silica surface (Fig. 5b, left image). The latter interpretation is consistent with the intensity changes seen in the fingerprint region ('5'). The signals in this region are present in the pure, carbon-dioxide free AmSp(d)Sil material and correspond to the *tert*-butyl-CH<sub>3</sub> groups. A change in this signal is not expected unless the presence of carbon dioxide has an influence.

There is now sufficient evidence that the quasi-solvation of CO<sub>2</sub> in the hydrophobic domain of the organosilica surfaces (Fig. 5b) is associated with an enthalpy  $\Delta H_{\text{qsolv}}$ .  $\Delta H_{\text{qsolv}}$  depends on the hydrophobicity of the spectator group and contributes to the adsorption enthalpy.





Fig. 5 (a) DRIFTS measurements performed for AmSp(d)Si;  $t = 1$  min (yellow) to 15 min (blue). (b) Molecular modelling of the surfaces of one pore in an organosilica material. The spectator group extends the primary amine function, and the *tert*-butyl phenyl groups in AmSp(d) Si form a disordered layer that is liquid-like. (c) Schematic representation of the  $\text{CO}_2$  uptake proposed for amine-modified organosilica surfaces containing spectator groups ( $\text{R}_{\text{F}2} = \text{tert-BuPh}$ ; AmSp(d)Si). The first step is the quasi-solvation of  $\text{CO}_2$  in the surface's hydrophobic domains, which is associated with  $\Delta H_{\text{qsolv}}$ . The following Lewis-acid reaction between the amino group and carbon dioxide followed by carbamic acid formation is also known from the literature and contributes to  $\Delta H_{\text{chemisorb}}$ . Both enthalpies contribute to  $\Delta H_{\text{adsorb}}$ . However, only  $\Delta H_{\text{qsolv}}$  depends on the nature of the spectator group, respectively, and its hydrophobicity.

### Materials consisting of zones of different adsorption enthalpies

The van der Waals interactions associated with  $\Delta H_{\text{qsolv}}$  can be strong, but due to the distance ( $d$ ) dependency ( $\propto 1/d^6$ ) only when the surface-bound  $\text{CO}_2$  and the spectator groups are close to each other. From our previous work on bifunctional organosilica materials, which were investigated by electron spin resonance (ESR) spectroscopy,<sup>17</sup> we know that the distribution of the functionalities on the pore-surfaces is statistical. This means that the average distance between equal groups e.g.  $\text{R}_{\text{F}1}$ , is a function of composition  $x,y$ . The modification of organosilica materials *via* click-chemistry allows the preparation of monolithic materials with controlled chemical gradients as we showed in several past papers.<sup>18,22,28</sup> We adopted the method here and have prepared a material containing a gradient in the *tert*-butyl phenyl spectator group. Fig. 6a–d demonstrate this for

an exemplary, fixed amine density in  $\text{Am}_{x=0.5}\text{SP(d)}_y\text{Si}$  materials. One can see that the probability is very high that each amine group has at least one further amine group as a next neighbor. However, for a low density of the spectator groups ( $x \ll 0.5$ ) one can see that only a few amine groups have a spectator as a neighbour. For moderate densities ( $x < 0.5$ ), the probability is high that most amines have at least one neighbouring spectator. For  $x = 0.5$ , most amines are surrounded by two spectator groups. *Vice versa*, lowering  $x$  and increasing  $y$  further would reduce the amine–amine contacts and increase the number of spectator groups in the direct vicinity.

For characterization, different areas of the resulting monolith (Fig. 6b) were characterized by IR spectroscopy (see Fig. 6c and ESI S11†). The decreasing intensity of the azide vibration demonstrates the successive presence of the spectator group at the surfaces. The more *tert*-butyl phenyl groups are present, the weaker the vibration of bands ( $3382\text{ cm}^{-1}$ ) associated with the

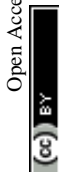






Fig. 6 (a–d) Schematic representation of the chemical nature of the pore-surfaces of  $\text{Am}_{x=0.5}\text{Sp(d)}_y\text{Sil}$  materials which are constant in the amine density (red squares) and vary systematically in the spectator group (blue). For high  $y$ -values every amine has a spectator group as a neighbor and many have even two neighbors. (e) Schematic representation of a monolithic organosilica material containing a gradient in the spectator group  $R_{F2} = \text{tert-butyl phenyl}$ . (f) Evaluation of FT-IR spectra of different segments associated with an increasing ratio of  $R_{F2}$ . (g)  $\text{CO}_2$  adsorption enthalpies of materials associated with an increasing ratio of  $R_{F2}$ .

presence of water. The latter result proves that the zones containing the spectator groups are more and more hydrophobic. Next, we have investigated the  $\text{CO}_2$  adsorption isotherms for materials differing in the ratio of amine functionalities to *tert*-butyl phenyl groups  $R_{F1} : R_{F2}$  (ESI Fig. S11† and 6d). According to our current knowledge, each composition of  $\text{Am}_x\text{Sp(d)}_y\text{Sil}$  should lead to a different  $\text{CO}_2$  adsorption enthalpy. Starting from the value of a material containing no spectator groups

$\text{Am}_{0.48}\text{Sp(d)}_0\text{Sil}$  ( $\Delta H_{\text{ads}} \approx 30 \text{ kJ mol}^{-1}$ ), we see that a low density of the spectator group (Fig. 6b) has only a minor effect. The *tert*-butyl phenyl sites are more or less isolated on the surface, which is insufficient to induce the quasi-solvent effect. A higher density of spectator groups seems necessary (Fig. 6c and d), and then the quasi-solvent effect manifests by increasing values for  $\Delta H_{\text{ads}}$ .

## Experimental

### Chemical synthesis

All starting chemicals and solvents have been purchased from Sigma Aldrich or TCI and were used after purification and drying.

**1,3-Bis-tri-isopropoxysilylphenyl-5-azide as a sol-gel precursor was prepared as described in the literature.<sup>18,28</sup>**

**AzSil material.** 117.2  $\mu\text{L}$  (0.22 mmol, 116 mg) 1,3-bis-tri-isopropoxysilylphenyl-5-azide are dissolved in 1 mL ethanol. 50  $\mu\text{L}$  aqueous HCl is added and left stirring for 1 h. Then, 50  $\mu\text{L}$  aqueous  $\text{NH}_3$  (25 wt%) is added under vigorous stirring. The solution is transferred into a sealed 3 mL vial. Gelation takes place within 15 minutes. The gel is aged for 20 h at room temperature, after which the monolith is removed from the vial. Solvent exchange is performed by placing the monolith in acetone for 3 days. Fresh solvent is used multiple times a day. Finally, an aerogel is prepared by supercritical extraction with liquid  $\text{CO}_2$ .

**Supercritical drying.** A monolith is placed into a sample holder filled with acetone. The holder was transferred into a dryer chamber and closed. The chamber was filled with liquid  $\text{CO}_2$  ( $p \sim 60$  bar). The acetone was exchanged with liquid  $\text{CO}_2$  by removing the acetone through the release valve. After complete removal of acetone from the chamber, it was heated to 42  $^\circ\text{C}$  ( $p \sim 90$  bar). The  $\text{CO}_2$ , which is supercritical under these conditions, was released throughout 4–5 h. After completely releasing  $\text{CO}_2$ , the dried monoliths were removed from the dryer chamber.

**AmSil material.** Depending on the desired degree of azide functionalization and the mass of the dry monolith, one can use different amounts of the catalyst and the alkyne (0.5–2 eq.). For instance, (0.2–0.4 mmol, = 1–2 eq.) copper(i)-tetrakis(acetonitrile) hexafluorophosphate is dissolved in 10 mL acetone. *N*-Boc-propargylamine (0.11–0.44 mmol, = 0.5–2 eq.) is added to the solution. The AzSil monolith (0.2 mmol, = 1 eq.) is then placed in the reaction solution. While stirring for 48 hours, one has to be careful that there is no mechanical damage from the stirring bar. For removal of the Boc protection group, the monolith was added to a 4 M HCl in acetone solution for two days. This solution was exchanged once after 24 h. After another washing step with acetone the monolith was placed in a solution of 500  $\mu\text{L}$   $\text{NH}_3$  (25%) in 10 mL acetone for 24 h. This step was repeated twice. An aerogel is prepared by supercritical extraction with liquid  $\text{CO}_2$ .

**AmSp(x) bifunctional materials.** The general procedure is similar to the one described before. However, the AmSil monolith still containing the Boc-group is used for the second post-functionalization step. The corresponding alkyne (1–3 eq.) was added together with the new catalyst dissolved in 30 mL acetone, and the mixture was reacted for 90 hours at room temperature. Afterward, deprotection and supercritical drying are performed as described before.

**Gradient materials.** A boc-protected AmSil material is the starting point. Ethanol is added to obtain a wet monolith. The monolith is placed inside a shrinking tube to avoid accessing

the reaction solution from the side.<sup>28</sup> One side of the tube is sealed and the other side is placed inside the reaction solution containing the catalyst and the spectator group alkyne. After the completion of the reaction the monolith was removed from the shrinking tube by dipping it into dichloromethane for 15 min. Thereby, the shrinking tube was swollen, and the monolith was removed. The solvent was exchanged for acetone. Afterward, deprotection and supercritical drying are performed as described before.

### Analytical methods

ATR-IR spectroscopy was performed on a Bruker Tensor with an ATR unit. All spectra were background corrected and normalized to the Si–O–Si vibration at 1044  $\text{cm}^{-1}$ . Thermogravimetric analysis measurements were performed using a Netzsch STA 409 PC LUX with a heating rate of 5  $\text{K min}^{-1}$  until 300  $^\circ\text{C}$  and 10  $\text{K min}^{-1}$  for 300–1000  $^\circ\text{C}$ . NMR measurements ( $^1\text{H}$ ,  $^{13}\text{C}$ ) were performed on a Bruker Ascend 400 MHz spectrometer. Scanning electron microscopy was performed on a Hitachi Regulus SU8200. Before conducting any gas adsorption measurement, the samples were degassed at 85  $^\circ\text{C}$  with the build-in degas system of an ASAP 2020 for 6 h. For temperature-dependent measurements the samples were degassed in between each measurement. The  $\text{N}_2$  measurements were performed at 77 K using liquid nitrogen and the  $\text{CO}_2$  measurements were performed at 0–50  $^\circ\text{C}$  using a Micromeritics Iso Controller Sub-Ambient to maintain a constant temperature. The equilibration interval was 10 s. The measurements were blank corrected by subtracting the blank measurement of an empty sample tube measured under identical conditions. The heat of adsorption was determined with the plugin of the MicroActive (4.06) software using the Clausius–Clapeyron-equation and isotherms at 0–50  $^\circ\text{C}$ .

For the DRIFT measurements, a Vertex 80v FTIR spectrometer from Bruker was used, equipped with a reaction chamber (Praying Mantis, DRP-M-16) and a gas flow cell (CHC-CHA-4), both from Harrick. To produce the samples, the silica material was ground with a pestle and mortar. The resulting powder was mixed with KBr to yield a mixture with 1% weight of the material. The mixture was again ground to minimize the size of the silica and the KBr grains. This is necessary to prevent artifact formation in the DRIFT spectra. KBr for infrared spectroscopy from Roth was used. A stock of the sample was produced, but each experiment was conducted with a new sample from the stock. The stocks were kept at 80  $^\circ\text{C}$  in a drying oven over night and desiccated for at least 15 min prior to the measurements, to remove crystal water from KBr. For the measurement, a set of three grids was placed in a CHC gas cell to prevent the powder from leaking out of the sample holder when the gas flow was applied. The pore size of the smallest grid (from Plano) was approximately 4  $\mu\text{m}$ . To stabilize this fragile grid, it was placed between the two others with bigger pore sizes (from Harrick). To apply the gas flow, two mass flow controllers (Bronkhorst, El Flow Select F-201CV) were used, one for  $\text{N}_2$  and one for  $\text{CO}_2$ . First, the sample was purged with nitrogen for 15–30 min and afterward the background signal was recorded. Gas mixtures of



N<sub>2</sub> and CO<sub>2</sub> with different partial pressures were then applied for five minutes each. Each of the CO<sub>2</sub>-adsorption steps was followed by a purging step, conducted with pure nitrogen for 15 min. The total flow rate was always 0.5 L min<sup>-1</sup>. For the gas mixtures, the rates of the two gases were adjusted to result in partial pressures of 0.2, 0.4, 0.6, 0.8 and 1 bar of CO<sub>2</sub>. IR measurements were performed with a spectral resolution of 4 cm<sup>-1</sup> and baseline correction.

## Conclusions

Porous materials containing primary amine groups are well known in the literature for their capability to adsorb and reversibly bind carbon dioxide. For any adsorbent, co-adsorption of competing molecules is a problem, and in the case of carbon-capture materials, the presence of water is an issue. One expects that the more hydrophobic a surface is, the less the co-adsorption of water contributes. We have shown here that the relevance of hydrophobic groups goes much further.

Organosilica materials characterized by bifunctional materials have been prepared using click-chemistry. The active group, a primary amine responsible for the interaction with CO<sub>2</sub>, is next to the hydrophobic group. We found that the density of this so-called spectator group, as well as its nature, is used to determine the adsorption enthalpy  $\Delta H_{\text{ads}}(\text{CO}_2)$ . The presented data indicate that it is not the aliphatic or aromatic character of the hydrophobic entities that is the most important factor, nor is it a steric influence. The capability of a spectator group to make the surface more hydrophobic is essential. Above a certain density of the spectator groups on the surface, they act like a quasi-solvent. The solvation enthalpy  $\Delta H_{\text{solv}}(\text{CO}_2)$  contributes and is higher the more hydrophobic the spectator group is. The effect allows for almost doubling the adsorption enthalpy. The latter observation represents the first main result of our study: one can now precisely adjust the adsorption enthalpy of CO<sub>2</sub> on amine-modified materials. The described findings agree with research by others on the solubility of CO<sub>2</sub> in ionic liquids (ILs), where hydrophobicity is also an important factor and influences enthalpic factors directly.<sup>40–43</sup> Considering the latter work and the fact that liquid CO<sub>2</sub> shows preferable interactions with perfluorinated groups, it is promising for the future to prepare a material containing more extended fluorinated alkyls compared to Am<sub>x</sub>SP(b,c).

Our definition of a spectator group is that it does not directly interact with CO<sub>2</sub>. As a consequence, one would expect that the effects on the adsorption enthalpy are only weak. However, the current results show that the seemingly “spectator” groups are equally important compared to the active CO<sub>2</sub> binding site (the amine groups). Unlike chemisorption, where one can also increase the adsorption enthalpy, the described quasi-solvent effects are fully reversible.

We developed an additional approach based on our experience with gradient materials. An organosilica monolith comprising a fixed amine “background” and a gradient in the hydrophobic spectator group was prepared. It can be shown that the  $\Delta H_{\text{solv}}(\text{CO}_2)$  becomes a function of the location. The different zones of the material correlate with different

adsorption enthalpies. We expect a material associated with a high value for  $\Delta H_{\text{ads}}(\text{CO}_2)$  to have a high affinity and can exhibit selectivity. In contrast, low values for  $\Delta H_{\text{ads}}(\text{CO}_2)$  mean the opposite. Thus, we hope to be able to show in the future that the gradient material is capable of separating gas mixtures and transporting the different species in opposite directions.

## Author contributions

ME: investigation (materials); KH: funding acquisition, supervision (DRIFTS); WGH: investigation (DRIFTS), formal analysis (DRIFTS); YK: project administration, supervision (materials); DM: investigation (materials), formal analysis; NK: methodology (materials); SP: conceptualization, data curation, funding acquisition, methodology, project administration, supervision (materials), visualization, writing – original draft.

## Conflicts of interest

There are no conflicts to declare.

## Acknowledgements

This project was funded by a grant from the Deutsche Forschungsgemeinschaft (DFG): Grant numbers PO 780/23-1 and HA 5142/6-1. We thank Marvin Träger, Katharina Rütther and Andreas Schneider for the molecular modelling calculations.

## Notes and references

- 1 D. D'Alessandro, B. Smit and J. Long, *Angew. Chem., Int. Ed.*, 2010, **49**, 6058–6082.
- 2 R. Ben-Mansour, M. Habib, O. Bamidele, M. Basha, N. Qasem, A. Peedikakkal, T. Laoui and M. Ali, *Appl. Energy*, 2016, **161**, 225–255.
- 3 Z. Zhang, Z. Cano, D. Luo, H. Dou, A. Yu and Z. Chen, *J. Mater. Chem. A*, 2019, **7**, 20985–21003.
- 4 B. Chen, S. Xiang and G. Qian, *Accounts Chem. Res.*, 2010, **43**, 1115–1124.
- 5 J. Borden and D. Savage, *Curr. Opin. Microbiol.*, 2021, **61**, 58–66.
- 6 S. Tanaka, C. Kerfeld, M. Sawaya, F. Cai, S. Heinhorst, G. Cannon and T. Yeates, *Science*, 2008, **319**, 1083–1086.
- 7 S. Bierbaumer, M. Nattermann, L. Schulz, R. Zschoche, T. J. Erb, C. K. Winkler, M. Tinzl and S. M. Glueck, *Chem. Rev.*, 2023, **123**, 5702–5754.
- 8 T. Schwander, L. Schada von Borzyskowski, S. Burgener, N. S. Cortina and T. J. Erb, *Science*, 2016, **354**, 900–904.
- 9 G. M. M. Stoffel, D. A. Saez, H. DeMirci, B. Vögeli, Y. Rao, J. Zarzycki, Y. Yoshikuni, S. Wakatsuki, E. Vöhringer-Martinez and T. J. Erb, *Proc. Natl. Acad. Sci. U. S. A.*, 2019, **116**, 13964–13969.
- 10 S. Choi, J. H. Drese and C. W. Jones, *ChemSusChem*, 2009, **2**, 796–854.
- 11 I. S. Omodolor, H. O. Otor, J. A. Andonegui, B. J. Allen and A. C. Alba-Rubio, *Ind. Eng. Chem. Res.*, 2020, **59**, 17612–17631.



- 12 X. Zhang, F. Shi, J. Niu, Y. Jiang and Z. Wang, *J. Mater. Chem.*, 2008, **18**, 621–633.
- 13 F. Hoffmann and M. Froeba, *Chem. Soc. Rev.*, 2011, **40**, 608–620.
- 14 W. Wang, J. E. Lofgreen and G. A. Ozin, *Small*, 2010, **6**, 2634–2642.
- 15 P. Van der Voort, D. Esquivel, E. De Canck, F. Goethals, I. Van Driessche and F. J. Romero-Salguero, *Chem. Soc. Rev.*, 2013, **42**, 3913–3955.
- 16 Y. Chen and J. Shi, *Adv. Mater.*, 2016, **28**, 3235–3272.
- 17 A. Kuschel, M. Drescher, T. Kuschel and S. Polarz, *Chem. Mater.*, 2010, **22**, 1472–1482.
- 18 A. Schachtschneider, M. Wessig, M. Spitzbarth, A. Donner, C. Fischer, M. Drescher and S. Polarz, *Angew. Chem., Int. Ed.*, 2015, **54**, 10465–10469.
- 19 J. Gehring, D. Schleheck, M. Luka and S. Polarz, *Adv. Funct. Mater.*, 2014, **24**, 1140–1150.
- 20 J. Gehring, D. Schleheck, B. Trepka and S. Polarz, *ACS Appl. Mater. Interfaces*, 2015, **7**, 1021–1029.
- 21 J. Gehring, B. Trepka, N. Klinkenberg, H. Bronner, D. Schleheck and S. Polarz, *J. Am. Chem. Soc.*, 2016, **138**, 3076–3084.
- 22 H. Bronner, A.-K. Holzer, A. Finke, M. Kunkel, A. Marx, M. Leist and S. Polarz, *RSC Adv.*, 2020, **10**, 17327–17335.
- 23 D. Kollofrath, M. Geppert and S. Polarz, *Chemsuschem*, 2020, **13**, 5100–5111.
- 24 N. Pal, J. Lee and E. Cho, *Nanomaterials*, 2020, **10**, 2122.
- 25 E. Cho, D. Kim and M. Jaroniec, *J. Phys. Chem. C*, 2008, **112**, 4897–4902.
- 26 P. Bhanja, A. Modak, S. Chatterjee and A. Bhaumik, *ACS Sustainable Chem. Eng.*, 2017, **5**, 2763–2773.
- 27 T. Asefa, M. Kruk, M. MacLachlan, N. Coombs, H. Grondy, M. Jaroniec and G. Ozin, *J. Am. Chem. Soc.*, 2001, **123**, 8520–8530.
- 28 N. Klinkenberg, A. Klaiber, M. Müller and S. Polarz, *Microporous Mesoporous Mater.*, 2020, **294**, 109879.
- 29 A. Pragma and T. K. Ghosh, *Adv. Mater.*, 2023, 2300912.
- 30 P. Kortunov, L. Heinke, S. Vasenkov, C. Chmelik, D. Shah, J. Karger, R. Rakoczy, Y. Traa and J. Weitkamp, *J. Phys. Chem. B*, 2006, **110**, 23821–23828.
- 31 Z. Liu, M. Meyers, Z. Zhang and R. Ritchie, *Prog. Mater. Sci.*, 2017, **88**, 467–498.
- 32 C. Zhang, Y. Xie, C. Xie, H. Dong, L. Zhang and J. Lin, *MRS Bull.*, 2022, **47**, 432–439.
- 33 E. Lopez-Maya, C. Montoro, V. Colombo, E. Barea and J. Navarro, *Adv. Funct. Mater.*, 2014, **24**, 6130–6135.
- 34 N. Klinkenberg, S. Kraft and S. Polarz, *Adv. Mater.*, 2021, **33**, 2007734.
- 35 M. Luka and S. Polarz, *Microporous Mesoporous Mater.*, 2013, **171**, 35–43.
- 36 S. Mahajan and M. Lahtinen, *J. Environ. Chem. Eng.*, 2022, **10**, 108930.
- 37 M. Ramdin, T. W. de Loos and T. J. H. Vlugt, *Ind. Eng. Chem. Res.*, 2012, **51**, 8149–8177.
- 38 Z. Bacsik, N. Ahlsten, A. Ziadi, G. Zhao, A. E. Garcia-Bennett, B. Martín-Matute and N. Hedin, *Langmuir*, 2011, **27**, 11118–11128.
- 39 N. Hedin and Z. Bacsik, *Curr. Opin. Green Sustainable Chem.*, 2019, **16**, 13–19.
- 40 Z. Bacsik and N. Hedin, *Vib. Spectrosc.*, 2016, **87**, 215–221.
- 41 A. Yokozeki, M. B. Shiflett, C. P. Junk, L. M. Grieco and T. Foo, *J. Phys. Chem. B*, 2008, **112**, 16654–16663.
- 42 M. J. Muldoon, S. N. V. K. Aki, J. L. Anderson, J. K. Dixon and J. F. Brennecke, *J. Phys. Chem. B*, 2007, **111**, 9001–9009.
- 43 L. A. Blanchard and J. F. Brennecke, *Ind. Eng. Chem. Res.*, 2001, **40**, 287–292.

