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Design and simulation of biomimetic microfluidic designs to achieve uniform flow and DNA capture for high-throughput multiplexing†

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High-throughput multi-analyte point-of-care detection is often constrained by the limited number of analytes that can be effectively monitored. This study introduces bio-inspired microfluidic designs optimized for multi-analyte detection using 38–42 biosensors. Drawing inspiration from the human spinal cord and leaf vein networks, these perfusion-oriented designs ensure uniform flow velocity and consistent molecular capture while maintaining spatial separation to prevent cross-talk. *In silico* optimizations achieved velocity profile uniformity with coefficients of variance of 0.89% and 0.86% for the spine- and leaf-inspired designs, respectively. However, simulations revealed that velocity uniformity alone is insufficient for accurate molecular capture prediction without consistent reaction site channel dimensions. The bio-inspired designs demonstrated superior performance, stabilizing—coefficient of variance below 20%—in DNA capture within 10 minutes, compared to 68 minutes for a simple branched design. This work underscores the potential of bio-inspired microfluidics to enable scalable, uniform, and high-performance systems for multi-analyte detection.

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Introduction

Multiplexing, which refers to either generating multiple signals for a single analyte¹ or detecting multiple analytes simultaneously, plays a critical role in advancing diagnostics across various fields.² In health monitoring and disease diagnostics, the continuous multiplexed measurement of biomarkers such as glucose,³ lactate,³ urea,⁴ citrate,⁵ metal ions,⁶ and small proteins such as enzymes, hormones, and cytokines provides invaluable information about physiological health.⁷ Similarly, profiling microRNA (miRNA) biomarkers has gained prominence for diagnosing, assessing prognosis, and monitoring diseases, including cancer, neurodegenerative disorders, and cardiovascular conditions.^{8,9} Thousands of miRNAs are screened to obtain accurate profiles of pathogenic expressions, with focused panels typically requiring 20–42 analytes for precise diagnosis.⁸ In environmental and food safety monitoring, multiplexing is

required for the detection of well over 100 pathogens (*e.g.* bacteria¹⁰ and viruses¹¹), contaminants, and harmful chemicals¹⁰ in a single sample. Identification of different species, as well as determination of antibiotic resistance can inform effective treatment strategies and reduce response times, potentially saving lives.¹² These diverse biomarkers can be detected by immobilizing biorecognition elements such as aptamers,¹³ oligonucleotides, enzymes, antibodies, and peptides¹⁴ onto sensing surfaces designed to selectively bind to their targets.¹⁵ Integrating a large number of biosensors, often rely on the amalgamation of biorecognition elements into a single device which presents significant technical challenges, requiring multiple readout labels, cross-contamination, and signal interference.¹⁶

Conventional diagnostic methods that have been designed for operation at centralized laboratories are not suitable for rapid clinical decision making at or near the patient, which adds delays in diagnosis, especially for those in remote and resource-poor areas.^{17,18} This has fueled the development of portable, simple, rapid, and multiplexed point-of-care (POC) diagnostics.¹⁹

Microfluidic systems offer several advantages for the development of fully-integrated biosensors for POC diagnostics and health monitoring.⁷ These include reducing sample and reagent volumes,²⁰ increasing local analyte concentrations,²¹ enabling multiplexing,²² and providing reproducible reaction conditions at the detection zones,²³ all of which are essential for optimizing sensor performance.

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Electrochemical transduction, in particular, has been widely adopted within microfluidic platforms due to its compatibility with miniaturization while maintaining sensitivity and reliability.^{24–27} However, current electrochemical microfluidic systems are typically limited to detecting 2–4 analytes simultaneously,²⁸ falling short of the demands for modern diagnostics. The primary challenge lies in integrating the detection of multiple analytes within a single device.

A key challenge in multi-analyte detection within passive flow channel designs—especially without the use of valves—is maintaining consistent biochemical environments and ensuring uniform interaction times across the channels. This is particularly critical in multiplexed affinity-based biosensors. Achieving consistent target capture efficiency across multiple biosensors integrated into a single system, while ensuring distinct signal readout without interference from neighboring electrodes, often demands precise assay^{29,30} and channel¹⁶ designs. Surface treatments between electrodes are commonly employed in electrochemical arrays within a single channel to isolate adjacent electrodes.³¹ However, in the absence of such advanced assay designs and surface treatments, these systems are prone to issues such as cross-contamination during immobilization and capture,³¹ signal interference from adjacent electrodes, and cross-talk caused by lateral movement of electroactive species between electrodes.¹⁶ To address challenges that compromise high-fidelity performance, spatial separation techniques employing separate detection zones either by mechanical separators³² or air pockets (hydrophobic areas),³³ parallel channels,³⁴ or bifurcating designs¹⁴ have been proposed. These approaches promote uniformity by maintaining consistent channel resistance and equal distances from the sample introduction point. Despite their advantages, majority of these designs are typically limited to detecting 2–4 analytes,^{14,28,34} due to the increased complexity of scaling for high-throughput multiplexing.

Scaling up microfluidic designs while maintaining spatial separation poses significant challenges due to the need for uniform flow velocity, analyte distribution, and target capture efficiency. Improper channel design can result in stagnation or dead zones, areas with little to no flow, that are particularly prevalent in branched systems.³⁵ Similarly, suboptimal channel configurations can result in flow deformation, where uneven flow distributions and secondary flow patterns can disrupt efficient analyte transport.³⁶ While such effects can be exploited for particle separation and entrapment,³⁷ unintended use may contribute to significant non-uniformity across different channels or outlets. Additionally, neglecting pressure drops at junctions can worsen energy losses and result in unwanted flow patterns, reducing channel consistency.^{38,39} These limitations can be mitigated by biomimetic designs and the use of computational approaches such as finite element analysis that are well-suited for predicting and optimizing the performance metrics of multiplexed microfluidic systems.⁴⁰

In silico methods enable the development of multiplexed biosensors with uniform flow velocities and consistent chemical reaction conditions, thereby reducing reliance on experimental trial and error.⁴⁰ Recent studies have explored novel designs *in silico* including manifold and biomimetic designs to address flow velocity uniformity while maintaining spatial separation. Biomimetic structures are particularly interesting because of their high functionality in flow velocity and distribution profiles.⁴¹ A manifold channel network inspired by the human circulatory system was optimized to achieve a flow velocity uniformity with 2.5% standard deviation across four channels, though experimental validation using microparticle image velocimetry indicated an approximately 10% standard deviation.⁴² While promising for velocity profile uniformity, this design lacked capture efficiency modeling and was limited in the number of reaction sites. In another study, a tentacles-like device inspired by many invertebrates demonstrated flow velocity uniformity *in silico* in simultaneous multi-analyte detection.⁴³ This design successfully addressed velocity uniformity and cross-talk prevention by employing spatial separation across six detection zones. Similarly, a rhombus tree-like device with a series of bifurcations achieved a uniform velocity profile, culminating in a chamber with a 10% standard deviation through *in silico* optimization; however, the design is prone to signal interference due to the lack of spatial separation.⁴⁰

As demonstrated in previous studies, most multi-analyte microfluidic designs are constrained by the limited number of analytes they can effectively detect. To overcome this limitation, we developed biomimetic microfluidic systems inspired by the spinal cord and staghorn plant leaf vein networks, incorporating 38–42 biosensors into a single microfluidic system. These bio-inspired designs were optimized *in silico* to achieve uniform flow velocity and consistent analyte capture across different channels while maintaining spatial separation to prevent cross-talk between reaction sites. The performance of these designs was further validated through direct comparison with a simpler branched microfluidic design.

Methods

Theory

We simulated the fluid dynamics within the microfluidic channels using COMSOL Multiphysics® software (version 6.2, COMSOL AB, Stockholm, Sweden). To apply the computational finite element analysis from the hydrodynamic equations module, we assumed laminar flow of an incompressible fluid, governed by the Navier–Stokes eqn (1). This equation governs the motion of fluids, representing the conservation of momentum, where u is the velocity of fluid, ρ is the density of fluid, p is pressure, K is the viscous stress tensor, and F denotes the external force applied to the fluid. For incompressible flow, where the density remains constant, the continuity eqn (2) converges to



zero. This assumption is valid based on the properties of the fluid and the scale of the microfluidic channels.⁴⁴

$$\rho(u \cdot \nabla u) = \nabla \cdot [-pI + K] + F \quad (1)$$

$$\rho \nabla \cdot u = 0 \quad (2)$$

In summary, (1) represents the balance between inertial, pressure, viscous, and external forces, while (2) ensures fluid incompressibility by enforcing that the velocity field is divergence-free.

To study DNA–DNA hybridization in the reaction sites, we used the transport of diluted species module in COMSOL 6.2, which models the diffusion and convection of diluted species in a liquid, as described by Fick's law, when flow is present.⁴⁵

$$\frac{\partial c_i}{\partial t} + \nabla \cdot J_i + u \cdot \nabla c_i = R_i \quad (3)$$

$$J_i = -D_i \nabla c_i \quad (4)$$

The species transport eqn (3), where the term $\frac{\partial c_i}{\partial t}$ represents the rate of change of the concentration of species i over time, $\nabla \cdot J_i$ is the divergence of the flux accounting for the net rate of species i entering or leaving the volume due to diffusion, $u \cdot \nabla c_i$ term represents convection, which is the transport of species i due to the bulk movement of the fluid at velocity u , and R_i is the reaction term of the rate of production or consumption of species i due to the chemical reaction. By substituting the flux term with Fick's law of diffusion (4), the flux of species i is proportional to the gradient of its concentration and moves from high to low concentration, governed by the diffusion constant D_i .⁴⁵

$$\frac{\partial c_{s,i}}{\partial t} + \nabla_t \cdot (-D_i \nabla_t c_{s,i}) = R_{s,i} \quad (5)$$

$$N_{s,i} = -D_i \nabla_t c_{s,i} \quad (6)$$

$$\theta_i = \frac{c_{s,i} \sigma_i}{\Gamma_s} \quad (7)$$

$$\frac{\partial c_{s,i}}{\partial t} = R_{s,i} \quad (8)$$

Surface species transport eqn (5)–(8) are used to model and describe the surface reaction, desorption, and adsorption process into a surface of species i . The $\frac{\partial c_{s,i}}{\partial t}$ term represents the rate of change of surface concentration, $\nabla_t \cdot (-D_i \nabla_t c_{s,i})$ represents surface diffusion of species i , and $R_{s,i}$ is the surface transport term representing the rate of production or consumption of species i on the surface. The surface coverage fractional occupancy is represented by (7), where θ_i is fractional occupancy, Γ_s is the total surface site density, and σ_i is the molecular surface area of species i .

Approach to simulations

The microfluidic designs were created using AutoCAD (version 2024, Autodesk Inc., San Rafael, CA, USA), and subsequently imported into COMSOL Multiphysics. The designs were then used to model and analyze the fluid dynamics within the microchannels under various conditions. The simulations employed the Navier–Stokes equations to model laminar flow, providing insights into the velocity and pressure profiles within the microchannels. The boundary conditions included a no-slip condition at the walls, representing the adherence of fluid to the channel surfaces. At the outlet, a zero-pressure boundary condition suppressing backflow was used to simulate an open-ended flow, allowing fluid to exit the microchannels without resistance. At the inlet, a fully developed flow profile was applied with flow rate set at $100 \mu\text{L min}^{-1}$ unless otherwise stated, which assumes that the fluid entering the channel had a uniform velocity distribution characteristic of steady-state flow. The initial conditions defined the starting state of the fluid, ensuring consistency in the velocity and pressure fields before simulation steps began. Solver settings included a time-dependent solver for transient analysis with a range of 0–600 s with 10 s increments.

Additionally, the model was used to study the transport of diluted species and surface reactions to simulate and understand the DNA–DNA hybridization on the surface of reaction sites. The conditions for the transport of diluted species contained a boundary condition set with an initial concentration of zero, followed by a gradual inflow of different target concentrations using a step function from 0 to 1 and a diffusion coefficient of small molecules in water defined as $1 \times 10^{-9} \text{ m}^2 \text{ s}^{-1}$ (ref. 45) (Table S1†). A general inward flux was modeled as ($R = K_{\text{on}} \times \text{concentration}$), coupled with a surface reaction rate defined by R . The K_{on} ($0.96 \times 10^6 \text{ M}^{-1} \text{ min}^{-1}$) and K_{off} (0.09 min^{-1}) values are extracted from our previous work.⁴⁶ Furthermore, we introduced Multiphysics coupling of laminar flow and transport of diluted species models to consider how the flow velocity affects DNA transport and hybridization, reflecting realistic behavior in a microfluidic system. Surface reactions parameters were set at zero initial concentration and site occupancy, with a surface probe density of 4.55×10^{12} molecules per cm^2 , and surface reaction rate of R . Solver conditions were set at stationary for laminar flow and time-dependent with a range from 1–10 000 s with 800 s increments and physics-controlled tolerance.

The meshing strategy for 2D simulation were adjusted to ensure accurate results while maintaining computational efficiency. Normal, fine, and extremely fine meshes were tested using the staghorn sumac leaf inspired design to demonstrate mesh independency (Fig. S1†). Fine and extremely fine meshing showed identical flow velocity uniformity (coefficient of variance 0.86%), while normal demonstrate slightly higher variability (coefficient of variance 2.4%). Therefore, the meshing



strategy for laminar flow used the default fine mesh option. Additionally, we tested the chosen fine mesh under varies flow rates ($10\text{--}1000\ \mu\text{L}\ \text{min}^{-1}$), demonstrating no difference in the coefficient of variance measurement (Fig. S2†). In the 3D simulation, the meshing strategy was designed to achieve accurate results while maintaining computational efficiency. We employed a combination of physics-defined and user-defined approaches, utilizing a fine mesh for the reaction sites, a

fine mesh for the boundaries, and a coarse mesh for the remaining geometry. Further increase of mesh refinement showed no improvement in capture kinetics.

The fraction of free sites was obtained by using boundary probes that are assigned to measure the fractions of free sites at each of the reaction sites. The fractions are then converted into capture efficiency using eqn (9):

$$\text{Capture efficiency (\%)} = 100\% \times (1 - \text{fraction of free sites}) \quad (9)$$

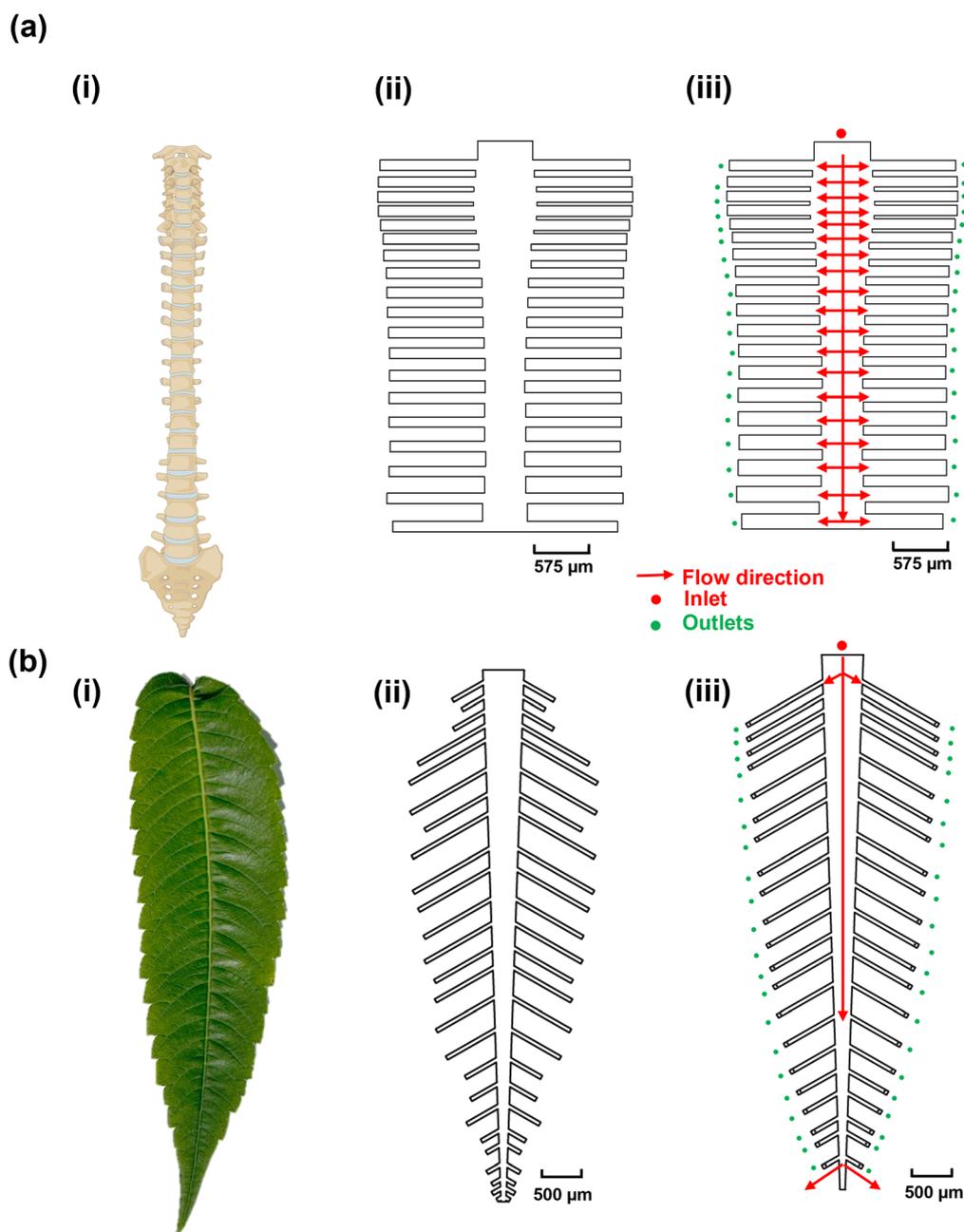


Fig. 1 Design of the bio-inspired multiplexed microfluidics. (a) Human spine-inspired design, (i) human spine schematic, (ii) the original scaled down design of a healthy human spinal vertebrae for microfluidics, (iii) the optimized design of the healthy human spinal vertebrae for microfluidics. (b) Staghorn sumac leaf-inspired design, (i) staghorn sumac leaf, (ii) the original scaled down design of the staghorn sumac leaf for microfluidics, (iii) the optimized design of the staghorn sumac leaf for microfluidics.



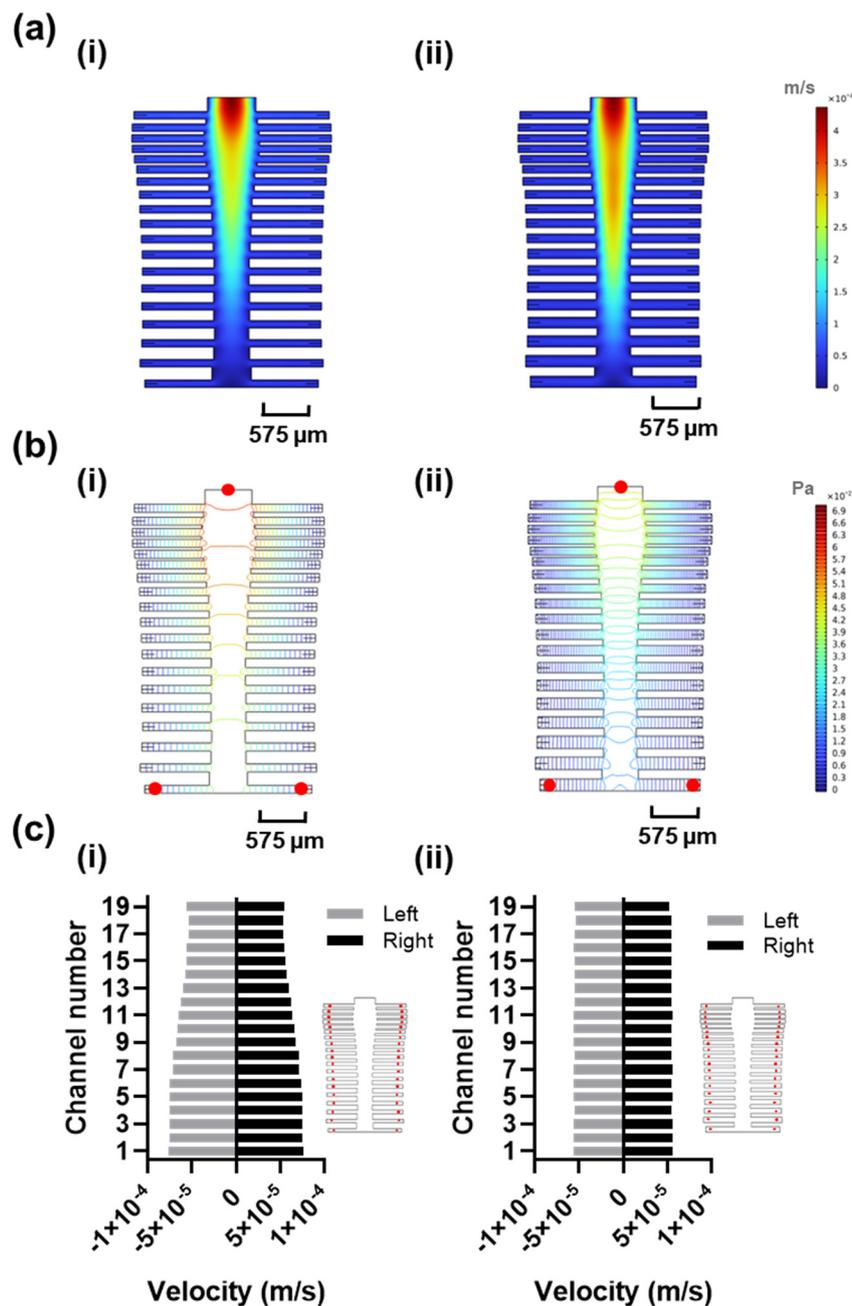


Fig. 2 Redesign of the spine-inspired design. (a) Velocity profile of the original (i) and optimized (ii) design. (b) Pressure profile of the original (i) and optimized (ii) design. (c) Velocity vector in each reaction site (red circles) for the original (i) and optimized (ii) design. Simulations are run using fully developed laminar flow at $100 \mu\text{L min}^{-1}$ flow rate.

10 , 50 and $100 \mu\text{L min}^{-1}$. As the concentration of target is higher in the bulk solution than the reaction sites, molecules diffuse from the bulk to the reaction sites through the diffusion layer⁵⁴ (Fig. 4b). We expect the capture efficiency of the reaction sites within different subchannels to be the same because of the reduced coefficient of variance of the velocity vector at the reaction sites (Fig. 2c-ii and 3c-ii), which ensures uniform convection and target transport. However, coupling convection, diffusion, and surface reactions in the simulation of capture

efficiency will achieve a more accurate prediction than convection alone of the performance of the bio-inspired designs for biosensing.

The original and optimized spine-inspired designs show the same capture efficiency over time in all the 38 capture reaction sites and minimal drop in hybridization efficiency between the reaction sites in the first and last channels (Fig. 4c and d), with a coefficient of variance of 0.43% and 0.59% at $100 \mu\text{L min}^{-1}$, 1.14% and 1.49% at $50 \mu\text{L min}^{-1}$, and 3.20% and 3.61% at $10 \mu\text{L min}^{-1}$ for the original and



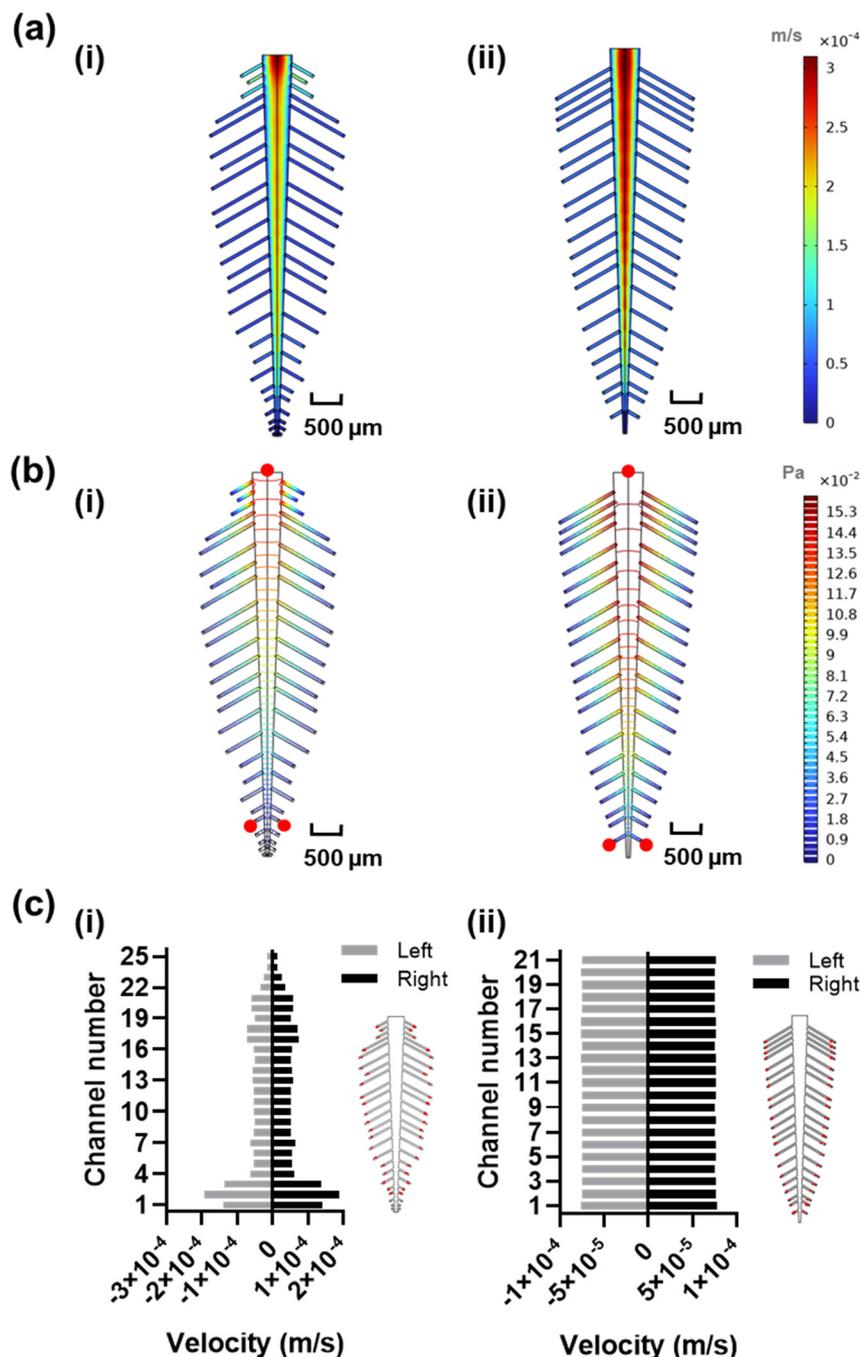


Fig. 3 Redesign of the leaf-inspired design. a) Velocity profile of the original (i) and optimized (ii) design. b) Pressure profile of the original (i) and optimized (ii) design. c) Velocity vector in each reaction site (red circles) for the original (i) and optimized (ii) design. Simulations are run using fully developed laminar flow at $100 \mu\text{L min}^{-1}$.

optimized spine-inspired designs at 20 minutes, respectively (Fig. S4a†). While both original and optimized spine-inspired designs demonstrate uniform capture across all 38 subchannels, it is interesting to observe that the original spine-inspired design has marginally lower coefficient of variance in all the tested flow rates ($10, 50, 100 \mu\text{L min}^{-1}$) (Fig. S4a†). We hypothesize that the optimized spine-inspired design is more variable due to variable widths (ranging from $98.5\text{--}153.5 \mu\text{m}$) of the subchannels, creating variable amount

of target diffused DNA within each subchannel.⁵⁵ While in the original spine-inspired design with uniform subchannel widths ($100 \mu\text{m}$), the distance between the centerline of the flow and the reaction sites (diffusion path) is equal, allowing target DNA to reach the reaction site uniformly through sideways (lateral) diffusion.⁵⁴ Furthermore, as flow rate increases, convection becomes more dominant, reducing the effect of diffusion, resulting in less difference between the original and optimized spine-inspired systems (Fig. S4a†). At



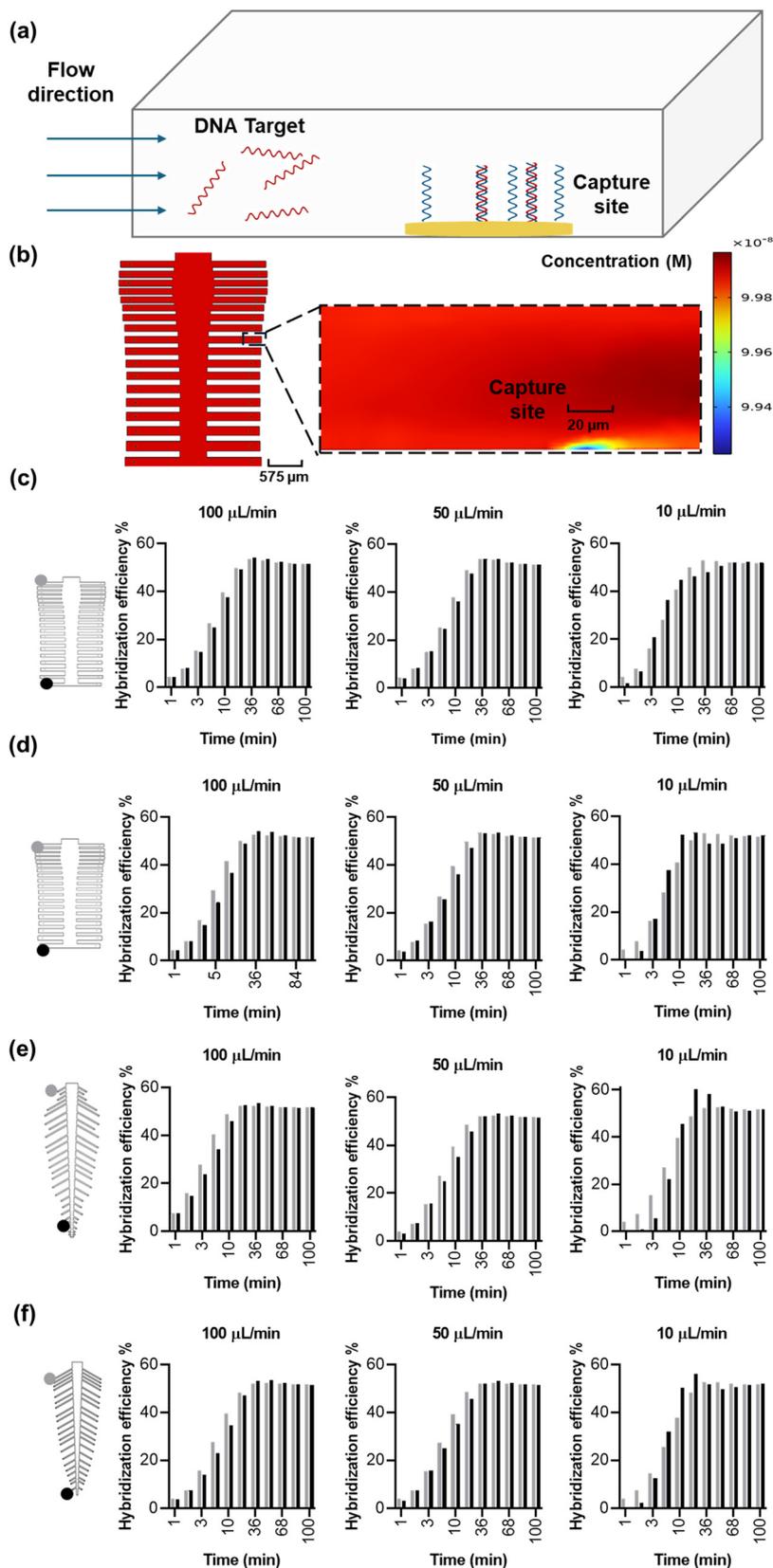


Fig. 4 DNA–DNA hybridization of the bio-inspired designs. (a) Schematics of the flowing DNA target and capture at the reaction/capture site using single stranded DNA probes. (b) Simulated channel cross section, showing the bulk target concentration of 100 nM and a reaction site. Hybridization efficiency of the original (c) and optimized (d) spine designs for the first (gray) and last (black) reaction sites. Hybridization efficiency of the original (e) and optimized (f) leaf designs for the first (gray) and last (black) reaction sites. Simulated laminar flow was set for a target concentration of 100 nM under a range of flow rates (10, 50, and 100 $\mu\text{L min}^{-1}$).



flow rates of 10, 50, and 100 $\mu\text{L min}^{-1}$, the average Peclet numbers for the original design are 0.62, 3.09, and 6.19, compared to 0.53, 2.63, and 5.26 for the optimized design, confirming the dominance of diffusion at lower flow rates.

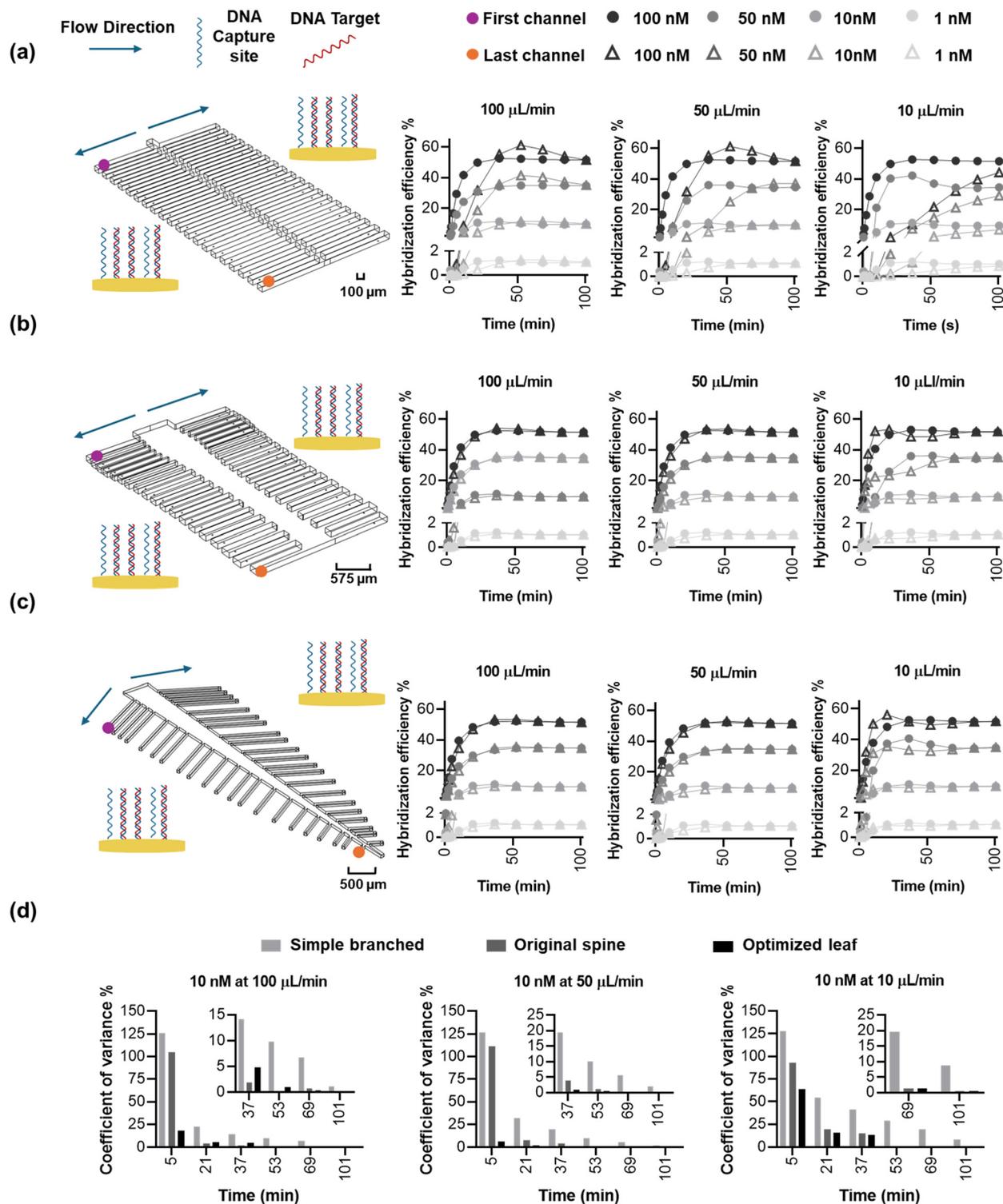


Fig. 5 Comparison of DNA-DNA hybridization kinetics of a simple branched design and the bio-inspired designs. The schematic and the hybridization efficiency at the first (purple) and last (orange) reaction sites for the simple branched (a), original spine-inspired (b), and optimized leaf-inspired (c) designs, along with a coefficient of variance analysis (d) across all the reaction sites for a target concentration of 10 nM at 100 $\mu\text{L min}^{-1}$ flow rate for the simple branched, original spine-inspired, and optimized leaf-inspired designs. Insets in (d) demonstrate rescaled y-axis versus time. Results show various DNA target concentrations (1, 10, 50, 100 nM), under a range of flow rates (10, 50, 100 $\mu\text{L min}^{-1}$).



To evaluate the efficacy of these designs, we first analyzed the velocity and pressure profiles in the original designs, followed by optimizing their dimensions to improve flow uniformity at the reaction sites through computational simulations. We then compared the original and optimized designs in terms of molecular capture at a target concentration of 100 nM, under varying flow rates (10, 50, and 100 $\mu\text{L min}^{-1}$). Notably, the original spine-inspired design exhibited less variability than the optimized design, suggesting that a combined approach—optimizing flow dynamics, mass transport, and surface reaction modeling—better predicts DNA capture uniformity than flow dynamics alone.

In further validation, we compared a simple branched design with the bio-inspired designs to assess the variability in target capture in the different reaction sites. The capture kinetics in both designs initially exhibited high variability more than 35% at 36 minutes for the simple branched and 5 minutes for the bio-inspired designs, transitioning to moderate variability between 10% and 35% at 84 and 36 minutes for the simple branched and bio-inspired designs respectively, then eventually both designs stabilizing with less than 10% variability as adsorption–desorption and mass transport reached steady-state. Notably, the bio-inspired designs demonstrated significantly lower variability compared to the simple branched design, achieving stabilization (coefficient of variance <20%) within 10 minutes, compared to up to 68 minutes for the simple branched design under varying flow rates and target concentrations. Furthermore, the bio-inspired systems were tested using various probe densities and complex media (plasma, whole blood, and saliva), demonstrating low variability across all conditions, highlighting the benefits of bio-inspired designs for biosensing.

The findings underscore the advantages of bio-inspired methodologies in the creation of multiplexed and multi-analyte sensing devices. We anticipate that these designs will find practical applications in areas requiring multiplexing, such as organ-on-a-chip platforms, monitoring food and water for various contaminants, and diagnostic panels. Future research will concentrate on refining these designs through experimental validation to develop optimized multiplexed systems for the aforementioned applications.

Data availability

The data supporting this article have been included as part of the ESI.†

Author contributions

E. O. designed the study, conducted the simulation, data analysis, and manuscript writing. J. L. H. contributed to the surface reactions simulations and manuscript writing. P. L. contributed to design optimizations and manuscript editing. L. S. contributed to the design and conceptualization of the

study and manuscript writing. All authors have approved the final version of the manuscript.

Conflicts of interest

The authors declare no competing financial interest.

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