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# Unveiling the particle size effect and surface reactivity of Pt/C nanoparticles for ammonia electrooxidation using *in situ* infrared spectroscopy†

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The ammonia electrooxidation reaction (AmER) has attracted considerable attention due to its potential for hydrogen storage and transportation, as well as its possible application in direct ammonia fuel cells. In the present work, we studied ammonia electrooxidation on carbon-supported Pt/C nanoparticles (NPs) of four average sizes of 1.3, 2.2, 2.8, and 4.2 nm. Carbon-supported Pt NPs with a 20 wt% metal loading were synthesized using the polyol method, and the control of the synthesis solution pH allowed the formation of Pt NPs of different average sizes, which was confirmed by TEM. The onset potential was more negative for the smallest nanoparticles (1.3 nm) compared to those for the larger ones. Pt/C with a mean particle size of 2.2 nm showed better stability while exhibiting comparable activity to the 1.3 nm particles. As revealed by *in situ* polarization modulation infrared reflection absorption spectroscopy (PM-IRRAS), the oxidation products included N-H species, azide ions, and nitrate and nitrite compounds. The N-H stretching peak was observed at about 2800 cm<sup>-1</sup> on the Pt surface and in the bulk of the electrolyte. However, the intensity of peaks corresponding to the reaction products was different on the surface of Pt and in the bulk of the electrolyte. NO<sub>2</sub><sup>-</sup> was mostly observed in the bulk of the electrolyte. In contrast, NO<sub>3</sub><sup>-</sup> was present on the Pt surface. PM-IRRAS demonstrated that the particle size affected the catalytic activity of Pt/C NPs but not their selectivity. In addition, the PM-IRRAS technique allowed, for the first time, distinguishing both symmetric and asymmetric N-O bonds that were not observed previously using IR spectroscopy during ammonia electrooxidation.

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## 1 Introduction

Ammonia is a promising candidate for high hydrogen storage and utilization in transportation not only because of its high hydrogen content (121 kg H<sub>2</sub> m<sup>-3</sup>) but also because it is the most cost-effective source of energy compared to other fuel sources like methanol and gasoline, at approximately 6.30 \$ per 100 km.<sup>1</sup> The low cost of ammonia is approximately 0.54 \$ per kg H<sub>2</sub> per unit of stored energy compared to that of hydrogen energy (14.95 \$ per kg H<sub>2</sub>),<sup>2,3</sup> and in addition, it is a CO<sub>2</sub>-free energy system. Ammonia can be liquefied under

moderate pressures and temperatures of around 8–10 bar and 20 °C and stored as a liquid for further applications and easy transport.<sup>4</sup> Furthermore, ammonia can be used as a suitable fuel source in direct ammonia fuel cells (DAFCs).<sup>5–8</sup>

The electrochemical oxidation of ammonia has been investigated on several mono- and bimetallic electrocatalysts to improve the reaction kinetics and find active catalysts such as Pt, Pt–Ir, Pt–Ir–Ni, *etc.*<sup>9–18</sup> As compared to some active catalysts, platinum has been reported to be the most effective catalyst with reversibility against surface poisoning in the ammonia electrooxidation reaction (AmER).<sup>19,20</sup>

Several studies have been conducted to investigate the use of transition metals (Pt, Pd, Rh, Ru, Au, Ag, Cu, Ni, and Ir) as ammonia oxidation electrocatalysts.<sup>8–17,21–25</sup> They reported that Pt and Ir catalysts with the lowest binding energy towards adsorbed atomic nitrogen (N<sub>ads</sub>) have increased ammonia oxidation reaction activity.<sup>12,13</sup> Pt is the most investigated and promising metal catalyst for the ammonia oxidation reaction,

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capable of generating high current densities at lower overpotentials.<sup>26,27</sup>

The mechanism of ammonia electrooxidation on Pt in alkaline solution proposed by Oswin-Salomon and Gerischer-Mauerer consists of several hydrogenation steps.<sup>28–30</sup> After being adsorbed on the catalyst surface, ammonia molecules undergo dehydrogenation into various N–H species and finally to N<sub>2</sub>. The last dehydrogenation step of NH produces N<sub>ads</sub> atoms, strongly binding intermediates that poison Pt active surface sites.<sup>28</sup>

Ammonia electrooxidation on the Pt surface is a highly structure-sensitive reaction that also depends on the size and the surface and bulk structure of nanocatalysts.<sup>28,31</sup> A change in the nanoparticle size could lead to changes in the Pt crystallographic orientation, and also to changes in the oxidation state, which results in the alteration of the Pt electronic structure.<sup>26,32</sup> It has been reported that the most active crystallite plane of Pt for ammonia electrooxidation is (100), followed by (111) and (110).<sup>26,31,33</sup> Several studies have been conducted to investigate this facet effect.<sup>31,33,34</sup> The higher Pt (100) activity is linked to its ability to stabilize adsorbed active NH<sub>2</sub> intermediates and not N<sub>ads</sub>, compared to the fcc Pt (111) surface.<sup>35,36</sup> Furthermore, the adsorption energy of the poisonous product N<sub>ads</sub> is lower on Pt (100) compared to that on the Pt (111) facets.<sup>19,37</sup> As a result, cubic Pt nanoparticles with a high number of Pt (100) facets have a substantially higher peak current density for the AmER than those with more Pt (111) surfaces.<sup>27,38</sup>

Studies on single Pt crystal electrodes, as well as electrochemically prepared (100) surfaces, revealed that the particle size of nanostructured catalysts could have a significant effect on the electrocatalytic performance of Pt, as the distribution and number of crystal planes depend on the particle size and the catalyst fabrication method.<sup>39,40</sup>

*In situ* infrared (IR) spectroscopy and Raman spectroscopy are powerful techniques for studying reaction mechanisms and product analysis.<sup>41,42</sup> Although the IR spectroscopy technique is efficient for analyzing solid-liquid interfaces, several obstacles, like strong IR absorption by aqueous electrolytes, may conceal the reaction products and intermediates.<sup>43</sup> In an early work, ammonia electrooxidation was studied on Pt electrocatalysts using the infrared reflection absorption spectroscopy (IRRAS) technique.<sup>44</sup> It is well-known that adsorbed N–H species are major intermediates of the AmER;<sup>30</sup> however, they could not be observed using infrared spectroscopy due to the huge peak overlaps in the water and nitrogen wavenumber regions. In a recent study using attenuated total reflection infrared reflection absorption spectroscopy (ATR-IRRAS), N<sub>2</sub>H<sub>4</sub> was observed during ammonia electrooxidation as an intermediate formed on Pt.<sup>42,45</sup> An N–O peak was also observed at relatively higher anodic potentials. Furthermore, surface-enhanced Raman spectroscopy (SERS) was used to detect N-containing products on the surface of platinum group metals (PGMs).<sup>46</sup> Adsorbed azide anions were found to

form on a Pt catalyst due to interaction between adsorbed ammonia molecules and generated N<sub>2</sub>H<sub>4</sub>.<sup>46</sup>

Polarization modulation infrared reflection absorption spectroscopy (PM-IRRAS) is a powerful technique to investigate solid/liquid and solid/gas interfaces and, in recent years, has attracted significant attention in electrochemistry and electrocatalysis.<sup>43,48</sup> This technique can simultaneously distinguish reaction species directly on the electrode surface and in the electrolyte in immediate contact with the electrode surface while suppressing signals from water.<sup>49</sup> In recent years, we have used *in situ* PM-IRRAS to study the electrooxidation of ethanol and glycerol on various Pd- and Ni-based nanoparticles.<sup>50,53–55</sup>

In the present study, we applied PM-IRRAS to study the AmER in alkaline media on size-defined Pt/C nanoparticles to elucidate the surface reactivity, oxidation products and catalyst selectivity. To this end, we fabricated carbon-supported Pt nanoparticles of four average sizes using the polyol synthesis method. To investigate the particle size effect and product distribution, we applied cyclic voltammetry, chronoamperometry, and the *in situ* PM-IRRAS technique. First, the detailed electrochemical characterization of Pt/C for the AmER is shown, and then optimization of the PM-IRRAS experimental approach for ammonia electrooxidation in 1 M KOH is presented, followed by *in situ* reaction product analysis under various anodic polarizations.

## 2 Results and discussion

Fig. 1 shows the TEM images and size distribution histograms of Pt/C NPs synthesized at various pH values. The resulting nanoparticles are spherical in shape, and show a narrow size distribution and no agglomeration. The average particle size ranges between 1.3 and 4.2 nm. The TEM results confirm that the size of the Pt nanoparticle catalysts was adjusted by changing the NaOH content from 0.08 to 0.25 M, corresponding to a pH increase from 5 to 8.2.<sup>46,47</sup> Table 1 summarizes the NaOH concentrations, as well as the initial and final pH values of the synthesis solution along with the average particle size.

### 2.1 Electrooxidation of ammonia

Fig. 2 shows the cyclic voltammograms of Pt/C nanoparticles in 1 M KOH in the presence and absence of 0.5 M NH<sub>4</sub>OH in the potential range of –0.9 to 0.0 V *vs.* Hg/HgO at 20 mV s<sup>–1</sup>. The current was normalized by the electrochemically active surface area (ECSA) obtained from the integration of the surface under the CV in the hydrogen adsorption/desorption region in 1 M KOH, Fig. S1.† The ECSA values (Table 1) do not show a clear trend with the particle size increase. This could be attributed to the change in the surface oxidation state of Pt NPs with increasing size. Earlier,<sup>47</sup> the XPS analysis of Pt/C NPs synthesized in ethylene glycol showed that the smallest (~1 nm) Pt/C NPs were mostly metallic, whereas for 2.2 nm NPs and larger ones, the existence of platinum atoms in the higher oxidation states of 2+ and 4+





Fig. 1 (Left) TEM images and (right) corresponding size distribution histograms of carbon-supported Pt nanoparticles of various mean particle sizes: – (a) 1.3 nm, (b) 2.2 nm, (c) 2.8 nm, (d) 4.2 nm.



**Table 1** Summary of the mean particle size of Pt/C catalysts, corresponding NaOH concentrations, and initial and final pH values during the nanoparticle synthesis, as well as the electrochemically active surface area (ECSA) of Pt/C

| Pt/C particle mean size <sup>a</sup> (nm) | NaOH concentration | Initial pH | Final pH | ECSA <sup>b</sup> (cm <sup>2</sup> ) |
|---|--------------------|------------|----------|--------------------------------------|
| 1.3                                       | 0.25               | 11.6       | 8.2      | 0.17                                 |
| 2.2                                       | 0.15               | 11.4       | 8        | 0.21                                 |
| 2.8                                       | 0.1                | 11         | 7        | 0.17                                 |
| 4.2                                       | 0.08               | 10         | 5        | 0.09                                 |

<sup>a</sup> From TEM images. <sup>b</sup> From the hydrogen adsorption/desorption region of CVs, Fig. S1 in the ESI†

was detected, indicating that the Pt surface consists of metal and oxides. This in turn will affect the active surface area and NP activity.

The CV scans in Fig. 2 are in agreement with studies on ammonia electrooxidation on carbon-supported Pt.<sup>51–53</sup> In 1 M KOH, the CVs show a PtO<sub>x</sub> formation peak at  $\sim -0.1$  V and the corresponding reduction peak between  $-0.1$  and  $-0.35$  V depending on the particle size. Hydrogen adsorption starts past  $-0.4$  V in the cathodic scan. In the presence of ammonia, the large oxidation peak (red line) at  $\sim -0.2$  V

corresponds to ammonia electrooxidation on Pt. The current decrease past  $-0.2$  V is due to the formation of inactive PtO<sub>x</sub> and surface poisoning by reaction intermediates, *e.g.*, N<sub>ads</sub>. In ammonia containing solution, hydrogen evolution occurs at around  $-0.8$  V compared to  $\sim -0.85$  V in 1 M KOH. The presence of ammonia also affects the hydrogen adsorption/desorption region, which shows a shift to higher potentials of  $-0.35$  V compared to it being in the  $-0.4$  V to  $-0.83$  V region in the absence of ammonia. This shift indicates that ammonium cations affect the binding energy of hydrogen, leading to a change in the corresponding potential. The observed small anodic peak prior to the ammonia oxidation peak has been attributed to the arrangement of ammonia molecules on the surface of Pt nanoparticles.<sup>23,54</sup> The current density reaches  $0.18$  mA cm<sup>-2</sup> for Pt/C with a  $1.3$  nm mean particle size as the highest and  $0.15$  mA cm<sup>-2</sup> for  $4.2$  nm Pt/C as the lowest (Fig. S2 in the ESI†).

Fig. 3a shows a comparison of the forward scan of CVs in ammonia-containing solution. The activity decreases as the particle size increases, demonstrating the relationship between the particle size and the catalytic activity of Pt nanoparticles. Smaller Pt particles generally have a larger surface area, resulting in a higher catalytic output. In the literature, some



**Fig. 2** Cyclic voltammograms of Pt/C catalysts of various average sizes as indicated in the figure in 1 M KOH (blue line) and in 1 M KOH + 0.5 M NH<sub>4</sub>OH (red line) at 20 mV s<sup>-1</sup>.





Fig. 3 (a) A comparison of the forward CV scans of Pt/C catalysts at  $v = 20 \text{ mV s}^{-1}$  and (b) chronoamperograms of Pt/C catalysts at  $-0.3 \text{ V}$  in  $1 \text{ M KOH} + 0.5 \text{ M NH}_4\text{OH}$ .

disagreement exists regarding the Pt particle size effect on electrochemical reactions, where, in addition to the size, the synthesis procedure and as a result the surface and bulk composition, and in some cases the particle shape, influence the reactivity. For instance, it has been reported that decreasing the catalyst particle size below  $3 \text{ nm}$  or increasing the specific surface area reduces the Pt catalytic activity.<sup>55,56</sup>

The current density normalized by the ECSA is lower for the  $4.2 \text{ nm}$  Pt/C catalyst compared to that of the smaller nanoparticles. This is due to the surface structural differences and the amount of surface  $\text{PtO}_x$ , also observed in the hydrogen region (Fig. 2). The onset potential is more

negative for the smallest Pt nanoparticles and nearly equal for the two intermediate sizes.

Fig. 3b shows the chronoamperometric measurements of Pt/C catalysts of various average sizes at  $-0.3 \text{ V}$ . As can be observed, the two largest particles,  $2.8$  and  $4.2 \text{ nm}$ , were rapidly deactivated without reaching steady state. The steep decline could be attributable to the formation of passive atomic  $\text{N}_{\text{ads}}$  intermediates that block Pt active sites.<sup>23,57</sup> The surface poisoning by  $\text{N}_{\text{ads}}$  could also be responsible for the observed current density noise for Pt/C of  $1.3$ ,  $2.8$  and  $4.2 \text{ nm}$  sizes (Fig. 3b). The noise decreases as the stability of Pt/C nanoparticles increases.



Fig. 4 PM-IRRAS spectra in the bulk of electrolyte (left hand side) and on the surface (right hand side) obtained on Pt/C catalysts of  $1.3 \text{ nm}$  average size (a and b) and  $2.2 \text{ nm}$  average size (c and d) in  $1 \text{ M KOH} + 0.5 \text{ M NH}_4\text{OH}$ . The applied potentials, as indicated in the figure, are  $-0.45$ ,  $-0.43$ ,  $-0.4$ ,  $-0.35$ ,  $-0.3$ , and  $-0.25 \text{ V}$  for  $5 \text{ min}$ . The spectra were processed considering ammonia at  $-0.5 \text{ V}$  as a reference.



## 2.2 *In situ* PM-IRRAS measurements

PM-IRRAS enables distinguishing between oxidation species adsorbed on the catalyst surface and those released into the electrolyte. Chronoamperometry experiments were coupled with PM-IRRAS in 1 M KOH to collect reference spectra before switching the electrolyte to 1 M KOH + 0.5 M NH<sub>4</sub>OH.

Fig. 4 depicts the spectra collected during ammonia electrooxidation for the two Pt/C catalysts with the highest activity and the best short-term stability, *i.e.*, 1.3 and 2.2 nm. The applied potentials ranged from the double layer region at  $\sim -0.5$  V to the ammonia oxidation potential at  $-0.25$  V vs. Hg/HgO. Depending on the potential, different peaks with varying intensities were observed (Fig. 4), and the corresponding band assignments are listed in Table 2. After applying specific potentials, four distinct bands emerged at 1290–1360, 1475–1550, 2000–2120, and 2700–3000 cm<sup>-1</sup>.

The peak at 3000–2700 cm<sup>-1</sup> is related to N–H species and starts appearing at around  $-0.35$  V for 1.3 nm and at a more positive potential of  $-0.3$  V for 2.2 nm Pt/C, which is in agreement with the onset potentials in the CVs, Fig. 3a. The intensity of this peak increases as the potential becomes more positive. The peak confirms the AmER on the Pt electrode and the peak intensity reaches its maximum at around  $-0.25$  V. The differences in the intensity of the peaks in the bulk and on the surface shows that N–H compounds desorb from the surface and diffuse into the bulk of the solution.

The peak at around 2010 cm<sup>-1</sup> observed during ammonia electrooxidation on the Pt surface and in the bulk of the electrolyte corresponds to azide ions, N<sub>3</sub><sup>-</sup>, according to surface-enhanced Raman spectroscopy.<sup>28,54</sup> The interaction of hydrazine (N<sub>2</sub>H<sub>4</sub>) and ammonia molecules produces azide ions. The asymmetric and symmetric N–O bonds in the bulk of the electrolyte correspond to nitrate and nitrite compounds with peaks at 1550–1475 cm<sup>-1</sup> and 1360–1290 cm<sup>-1</sup>, respectively.<sup>58,59</sup> As seen, the symmetric nitrite components are not visible on the 1.3 and 2.2 nm Pt surfaces, which could be due to the immediate desorption of these species from the surface after formation. Overall, all IR peaks have a higher intensity and appear earlier for the smallest 1.3 nm Pt/C catalyst, confirming its higher reactivity and earlier onset potential observed in Fig. 3.

Fig. 5 and 6 show the collected spectra on the Pt/C catalysts of 1.3 nm and 2.2 nm, respectively. The left hand side corresponds to spectra in the electrolyte and the right hand side spectra are recorded on the Pt surface. In these experiments, the reference spectra to process the data are

acquired in 1 M KOH at  $-0.4$  V in order to see the effect of the ammonia electrolyte. Fig. 5a and b and 6a and b show the PM-IRRAS spectra at  $-0.3$ ,  $-0.2$ , and  $-0.1$  V in 1 M KOH in the absence of ammonia, and as expected, no oxidation species are observed.

Fig. 5c and 6c show the existence of ammonia peaks at 2900 cm<sup>-1</sup> at the start of the experiment at  $-0.5$  V, reflecting the effect of the ammonia electrolyte on both bulk and surface spectra. In comparison to those in Fig. 4, the peaks are more intense because the effect of the electrolyte has not been omitted. As can be seen, N–O species centered at 1500 cm<sup>-1</sup> are mostly present in the electrolyte and were observed only at high anodic potentials on the surface. It also seems that there is less N–O formation for larger NPs and only at high potentials based on the peak intensity.

Fig. 7 shows the spectra obtained at  $-0.35$ ,  $-0.3$ , and  $-0.25$  V for 30 min to study the accumulation of products and intermediates. Like in Fig. 4 to 6, the larger Pt/C NPs of 2.2 nm do not show N–H and N–O peaks at  $-0.35$  V in the electrolyte (Fig. 7c) or on the surface (Fig. 7d), indicating the absence of ammonia electrooxidation at this potential. The smallest sized catalyst shows the highest peak intensities at a given potential. In addition, the formation of OH<sup>-</sup> at 3600 cm<sup>-1</sup> on the surface of 1.3 nm Pt/C NPs was clearly observed. This peak was only seen on the surface but not in the electrolyte nor on the larger NPs. The coverage of the Pt surface by OH<sup>-</sup> could be a potential reason for the short-term stability difference between 1.3 and 2.2 nm nanoparticles. It was reported that OH<sup>-</sup> ions could be strongly attached to the surface of Pt catalysts and cover the active sites competing with ammonia molecules.<sup>24,60</sup> It is therefore assumed that oxygenated ions also play a negative role in blocking active surface sites, in addition to the N<sub>ads</sub> atoms.

## 3 Conclusions

The influence of the Pt nanoparticle size on the ammonia electrooxidation reaction was investigated. PM-IRRAS was combined with electrochemical measurements to explore ammonia electrooxidation on carbon-supported Pt/C NPs in alkaline environments. The study demonstrated a clear relationship between the nanocatalyst size and catalytic activity. The smallest sized Pt particles, 1.3 nm, displayed better activity and a lower onset potential, while the 2.2 nm Pt particles showed better durability and reasonable activity. Various oxidation potentials were applied to detect the oxidation species using *in situ* PM-IRRAS. N–H species, azide ions, and nitrate and nitrite compounds have been identified as the main reaction products. At higher anodic potentials of  $-0.3$  V and  $-0.25$  V, when Pt oxidation takes place, the formation of N–O species was also observed. NO<sub>2</sub><sup>-</sup> was mostly observed on the catalyst surface. In contrast, NO<sub>3</sub><sup>-</sup> was mostly identified in the bulk indicating its fast desorption. PM-IRRAS allowed the detection of both symmetric and asymmetric N–O bonds, as well as N–O linked to surface NO<sub>2</sub><sup>-</sup>, which was not possible with the ATR-FTIR technique.

**Table 2** Band assignment of IR peaks during the AmER on Pt/C in 1 M KOH + 0.5 M NH<sub>4</sub>OH

| Wavenumber (cm <sup>-1</sup> ) | Bond  | Assignment  |
|--------------------------------|-------|---|
| 3000–2700                      | N–H   | N <sub>2</sub> H <sub>4</sub> , N <sub>2</sub> H <sub>2</sub> , NH <sub>2</sub> , NH, ... |
| 2120–2000                      | N=N=N | Azide ion   |
| 1550–1475                      | N–O   | NO <sub>3</sub> <sup>-</sup>  |
| 1360–1290                      | N–O   | NO <sub>2</sub> <sup>-</sup>  |





**Fig. 5** PM-IRRAS spectra (considering KOH at  $-0.4$  V as reference for processing the spectra) on Pt/C of 1.3 nm. (a and b) Spectra in 1 M KOH and (c and d) spectra in 1 M KOH + 0.5 M  $\text{NH}_4\text{OH}$ . The applied potentials in (c) and (d), as indicated in the figure, are  $-0.5$ ,  $-0.45$ ,  $-0.43$ ,  $-0.4$ ,  $-0.35$ ,  $-0.3$ , and  $-0.25$  V. The left hand side corresponds to the bulk of the electrolyte and the right hand side corresponds to the Pt surface.



**Fig. 6** PM-IRRAS spectra (considering KOH at  $-0.4$  V as reference for processing the spectra) on Pt/C of 2.2 nm. (a and b) Spectra in 1 M KOH and (c and d) spectra in 1 M KOH + 0.5 M  $\text{NH}_4\text{OH}$ . The applied potentials in (c) and (d), as indicated in the figure, are  $-0.5$ ,  $-0.45$ ,  $-0.43$ ,  $-0.4$ ,  $-0.35$ ,  $-0.3$ , and  $-0.25$  V. The left hand side corresponds to the bulk of the electrolyte and the right hand side corresponds to the Pt surface.

In addition,  $\text{OH}^-$  species were detected on the surface of 1.3 nm Pt in the oxidation potential region of  $-0.35$  to  $-0.25$

which could not be seen in the spectra corresponding to the electrolyte side. It has been reported that  $\text{OH}^-$  can become





Fig. 7 PM-IRRAS spectra (considering ammonia at  $-0.5$  V as reference) on Pt/C of (a), (b) 1.3 nm size and (c), (d) 2.2 nm particle size during ammonia electro-oxidation in 1 M KOH + 0.5 M  $\text{NH}_4\text{OH}$ . Spectra collected after 30 min at each potential. The left hand side corresponds to the bulk of the electrolyte and the right hand side corresponds to the Pt surface.

strongly attached to the surface of Pt catalysts and cover the active sites. This could be one of the reasons why 1.3 nm Pt is less stable than 2.2 nm Pt.

## 4 Experimental

### 4.1 Synthesis of carbon-supported Pt

Carbon-supported Pt catalysts were synthesized using a polyol synthesis method described previously.<sup>61,62</sup> First, 104 mg of  $\text{PtCl}_4$  (Alfa Aesar, 99.9% metals basis) was dissolved in 12 mL of ethylene glycol (Fisher Scientific). Four reaction mixtures of  $\text{PtCl}_4$  and glycerol were prepared containing 0.25, 0.15, 0.1, and 0.08 M NaOH (ACP Chemicals Inc.). After 30 minutes of refluxing at 160 °C, the mixtures formed colloidal solutions of Pt nanoparticles. The colloids were then mixed with a corresponding amount of carbon (Vulcan XC-72, Cabot) support. The mixture was stirred for 24 hours to achieve high dispersion of nanocatalysts with a metal loading of 20 wt%. The supported catalysts were centrifuged and thoroughly washed in ultra-pure deionized water (18  $\Omega$  cm) and then dried in a freeze dryer (LABCONCO, 4.5 L cascade, benchtop freeze dry).

### 4.2 Characterization of the nanoparticles

The size and morphology of Pt/C catalysts were examined using a JEM-2100F FETEM (JEOL) transmission electron microscope (TEM). The particle size distribution was determined using ImageJ software.

All electrochemical and spectro-electrochemical measurements were carried out in an in-house built spectro-

electrochemical cell made of Teflon, as previously reported.<sup>50,63,64</sup> The cell was fitted with a calcium fluoride ( $\text{CaF}_2$ ) hemicylinder IR window (RJ Spectroscopy Co.). The working electrode consisted of a glassy carbon (GC) disk (0.197  $\text{cm}^2$  surface area) integrated in a Teflon rod equipped with a micrometer to adjust the distance between the electrode and the IR window. A Pt wire twisted around the working electrode was used as a counter electrode and Hg/HgO (Koslow Scientific) served as a reference electrode. 1 M KOH and 1 M KOH + 0.5 M  $\text{NH}_4\text{OH}$  aqueous solutions were prepared by using KOH (85% KOH basis, Sigma-Aldrich) and ammonium hydroxide,  $\text{NH}_4\text{OH}$ , 14.8 N (Fisher Scientific). All potentials were measured and reported *versus* the Hg/HgO reference electrode, unless otherwise stated.

### 4.3 In situ PM-IRRAS measurements

Polarization modulation infrared reflection absorption spectroscopy (PM-IRRAS) and electrochemical tests were carried out by integrating a Fourier transform infrared spectrometer (Bruker Tensor 37) equipped with an additional polarization modulation accessory (PMA 50 XL) located in a chamber and the spectro-electrochemical cell.<sup>45,49,63,65</sup> Cyclic voltammetry (CV) and chronoamperometry (CA) were carried out using a PARSTAT 2263 (Princeton Applied Research) potentiostat. For CV measurements, the potential was scanned from  $-0.9$  to  $0$  V *vs.* Hg/HgO at a scan rate of 20  $\text{mV s}^{-1}$  for 10 cycles. The 10th cycle is reported unless otherwise stated. For CA measurements, the potential was fixed at  $-0.3$  V for 30 minutes. A catalyst ink was prepared by adding 6 mg



of electrocatalyst powder to 1 mL of deionized water, 100  $\mu\text{L}$  of 5 wt% Nafion® and 100  $\mu\text{L}$  of isopropanol. The ink was sonicated in an ultrasonic bath for 10 minutes. After that, aliquots of 2.5  $\mu\text{L}$  of the ink were deposited onto the GC surface and dried at 60 °C for 10 minutes. The electrolyte was degassed using nitrogen gas (99.999%, Linde). Prior to the *in situ* spectroscopy analysis, a mercury cadmium telluride light detector (LN-MCT Narrow PMA50, Infrared Associates, Inc., Stuart, FL) was cooled down with liquid nitrogen to avoid potential damage due to an increase in temperature by infrared beams. Pushing the working electrode toward the calcium fluoride window, an estimated average thickness of 10  $\mu\text{m}$  of electrolyte was achieved.<sup>50</sup> All spectra were collected at a spectral resolution of 8  $\text{cm}^{-1}$  by acquiring 256 scans. The collected spectra were acquired under chronoamperometry (CA) while the potential was kept constant at different ammonia oxidation states for 5 minutes or 30 min. The infrared beam was adapted to hit the GC surface at 68° which is an optimum angle.<sup>64</sup> The surface and bulk reflectivity factors (R.F.s) were calculated using eqn (1) and (2), which are based on a previously introduced methodology:<sup>64</sup>

$$\text{Surface reflectivity factor (R.F.}_{\text{Surface}}) = \left( \frac{\text{Sample } (R_{\text{dif}})}{\text{Reference } (R_{\text{dif}})} \right) - 1 \quad (1)$$

$$\text{Bulk reflectivity factor (R.F.}_{\text{Bulk}}) = \left( \frac{\text{Sample } (R_{\text{ave}})}{\text{Reference } (R_{\text{ave}})} \right) - 1 \quad (2)$$

## Conflicts of interest

The authors declare no conflict of interest.

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