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Exploring the impact of lithium halide-based redox mediators in suppressing CO₂ evolution in Li–O₂ cells†

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The realization of lithium–oxygen (Li–O₂) batteries has been impeded by parasitic reactions that cause cell component degradation, often accompanied by the release of CO₂ gas during oxidation reactions. The use of halide-based redox mediators (RMs) like LiBr and Lil has been proposed as a strategy to reduce overpotentials during oxygen evolution reactions and thus suppress the subsequent evolution of CO₂. However, there is a scarcity of research examining the effectiveness of these RMs in the direct mitigation of parasitic reactions. In this study, we investigated the evolution of CO₂ during the oxidation processes using an online electrochemical mass spectrometer. The results show that cells without RMs exhibited high overpotentials and significant CO₂ evolution from the first charging cycle. In contrast, the addition of 50 mM Lil to the electrolyte resulted in a delay in CO₂ evolution, observed only after several cycles. Notably, no CO₂ evolution was observed in cells containing 50 mM LiBr in 0.5 M LiTFSI during the cell cycling. Our findings demonstrate that while the mechanism of halide-based RMs may be similar, their chemical properties and electrochemical behaviour can greatly influence their ability to effectively mediate the oxygen evolution process.

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Introduction

Lithium–oxygen (Li–O₂) battery technology underwent a tremendous push for practical realization because of its high theoretical gravimetric energy density which is 3–5 times higher when compared with conventional lithium-ion batteries.^{1–4} However, commercialization was hindered because of poor reversible capacity, low-rate capability, poor cycle life and round-trip efficiency.^{5–8} These limitations are mainly because of unavoidable intermediate parasitic reactions occurring at electrode–electrolyte interphases during cycling.^{9–11} In non-aqueous Li–O₂ cells, the O₂ electrochemistry consists of an overall two-electron transfer (2e[−]) producing solid lithium peroxide (Li₂O₂) during discharge.^{3,12–16} Upon charging the oxygen evolution reaction (OER) occurs with oxidation of the non-conductive Li₂O₂ species.^{17,18} Parasitic chemical reactions which are accompanied with early cell failure are as follows: (1) parasitic reactions associated with the oxidation of lithium peroxide and formation of reactive intermediates during charging such as decomposition of electrolyte because of

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reactive oxygen species at the electrode electrolyte interphase. (2) Instabilities associated with carbon cathode at higher voltages. (3) Degradations associated with lithium anode.^{19–22} Several reports proposed using stationary heterogeneous catalysts coated on carbon cathode to suppress the parasitic reactions during Li–O₂ battery cycling. However, the performance of conventional stationary catalysts is limited since they are only effective for ORR products that come into direct contact with them. Furthermore, many of these catalysts can enhance additional side reactions such as carbon and electrolyte solution decomposition which negatively impacts the overall battery life.^{23,24} In this regard, soluble electrocatalysts or redox mediators (RM) can diffuse through the interphases to oxidize the insulating Li₂O₂ product layer.^{25–28} During charging, RM itself first gets oxidized at the electrode to form an oxidized species, which then chemically oxidizes the Li₂O₂ to evolve O₂.^{29–31} Liang *et al.* proposed LiBr as RM for improved electrochemical performance without necessarily changing the two electron transfer process during discharge (ORR).³¹ Nevertheless, the cells containing LiBr resulted in CO₂ evolution during OER process maybe due to formation of corrosive, free bromine (Br₂).³¹ Kwak *et al.* has conducted systematic electrochemical study using electrolyte with and without RM's specifically LiI and LiBr.^{23,31} They demonstrated improved electrochemical stability for Li–O₂ cells containing LiBr as RM. However little research was known about the influence of RM on suppressing the parasitic reactions accompanied with CO₂ evolution during OER process. Therefore, it is important to monitor the CO₂ gas evolution using online electrochemical mass spectrometer (OEMS) to decipher the role and impact of RMs in imparting interfacial stability needed for prolonged cycling.

Herein, we conducted a systematic study to examine the extent of CO₂ evolution from a diglyme based Li–O₂ cell in presence and absence of LiI and LiBr RMs. Long term monitoring of CO₂ evolution was conducted using OEMS, to follow the evolution and evolution of CO₂ over time and not only during the 1st cycle. Upon cycling the cells without RMs experienced severe electrochemical instabilities because of high overpotential behaviour. Both RMs showed initial suppression of CO₂ evolution, however on longer term cycling, the LiBr showed profound advantage over the LiI in terms of CO₂ suppression. Our results highlight the consequences of differences in chemical properties of RMs, even if they exhibit similar influence on the overpotential of the cell. We find that addition of lithium bromide RM can greatly improve the electrochemical properties and effectively mediate the oxygen evolution process.

Results and discussion

Cyclic voltammetry is conducted for neat 0.5 M LiTFSI base solution in diglyme with/without addition of 50 mM LiI or 50 mM LiBr halide based RMs. Fig. 1a shows the cyclic voltammograms observed for the proposed electrolytes under Ar atmosphere. As previously reported, 0.5 M LiTFSI in diglyme does not show any kind of redox behaviour. However the cathodic scan of the cyclic voltammogram shows low-intensity peaks at ~2 V indicating reduction of some species in the

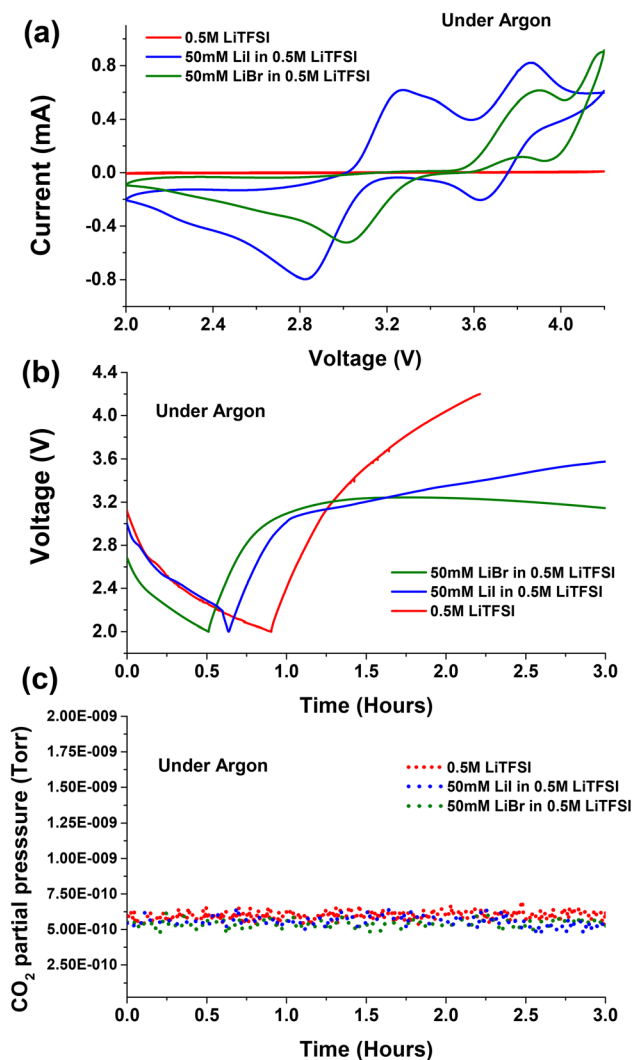


Fig. 1 (a) Cyclic voltammetry (5 mV s⁻¹) on Pt working electrode under argon atmosphere for 0.5 M LiTFSI, 50 mM LiI in 0.5 M LiTFSI, and 50 mM LiBr in 0.5 M LiTFSI in diglyme; (b) voltage profiles during galvanostatic discharge and charge under Argon for cells with lithium anode against carbon cathode separated with glass fibre separator with 0.5 M LiTFSI, 50 mM LiI in 0.5 M LiTFSI and 50 mM LiBr in 0.5 M LiTFSI in diglyme electrolytes, current density was fixed at 0.052 mA cm⁻² (OCV not shown) (c) the corresponding normalized carbon dioxide gas evolutions monitored in OEMS.

electrolyte (Fig. S1†).^{32,33} Tułodziecki *et al.* suggests that the Li⁺ cation preferentially adsorb on the carbon surface and drag the TFSI⁻ anions with them, facilitating their reduction.^{34–36} A similar electrochemical activity was observed in the galvanostatic discharge and charge profiles for neat 0.5 M LiTFSI electrolyte solution as shown in Fig. 1b. The cells with 0.5 M LiTFSI electrolyte solution discharge to 2 V very fast with negligible capacity and charged with steep raise in voltage to 4.2 V. With addition of 50 mM LiI to the 0.5 M LiTFSI base solution the cyclic voltammogram exhibited two oxidation processes during the anodic scan. The first oxidation process in the anodic scan is attribute to the conversion of iodide ion to triiodide ion (I⁻ → I₃⁻) at ~3.1 V, whereas the second oxidation process is due to



conversion of triiodide ion to iodine ($I_3^- \rightarrow I_2$) at ~ 3.8 V. This phenomenon is more evident during the galvanostatic charge profiles (Fig. 1b) where the RM undergoes two oxidation processes with two representative voltage plateaus. The first voltage plateau during charge occurs at ~ 3.1 V indicating the first oxidation process ($I^- \rightarrow I_3^-$). After steep increase in the voltage, a second voltage plateau is appearing at ~ 3.8 V, implying the second oxidation process ($I_3^- \rightarrow I_2$).

When 50 mM LiBr was added to the 0.5 M LiTFSI base solution, the cyclic voltammetry exhibited higher oxidation potentials with respect to cells containing LiI as RM. The first oxidation process of bromide ion to tribromide ion occurs at ~ 3.5 V ($Br^- \rightarrow Br_3^-$), while the second oxidation process of tribromide ion to bromine started from ~ 4 V ($Br_3^- \rightarrow Br_2$). These results are consistent with previous report for LiBr and LiI RMs.²³ Fig. 1b shows the galvanostatic discharge and charge cycle for the cells containing LiBr RM. In Ar environment the cells exhibited negligible capacity when discharged to 2 V. The subsequent charge voltage profile exhibits a voltage plateau at

~ 3.2 V indicating the oxidation of $Br^- \rightarrow Br_3^-$. As suggested by cyclic voltammogram, LiBr containing cells requires high overpotentials for the second oxidation process tribromide ion to bromine ($Br_3^- \rightarrow Br_2$) with respect to cells containing LiI as RM.

Fig. 2a–c presents the voltage profiles of 0.5 M LiTFSI, 50 mM LiI in 0.5 M LiTFSI, and 50 mM LiBr in 0.5 M LiTFSI in diglyme solutions cycled under O_2 atmosphere. The first discharge voltage profile at ~ 2.8 V is attributed to oxygen reduction reaction on the porous carbon cathode and formation of Li-peroxide species. Scanning electron microscopic imaging studies show the well reported Li_2O_2 coagulation on porous carbon cathode (Fig. S2†). Also, cells with neat 0.5 M LiTFSI electrolyte and LiBr containing additive favours the formation of Li_2O_2 which is supported by the presence of diffraction peaks at 2θ : ~ 33 , ~ 35 in the X-ray diffractograms of the discharged cathodes (Fig. 3a). Whereas cells with 50 mM LiI addition clearly exhibit LiOH phases at 2θ : ~ 32.7 and ~ 36 .^{23,37,38} Further, ATR-FTIR characterization (Fig. S3†) shows the presence of $-OH$



Fig. 2 Voltage vs. specific discharge capacity profiles of Li–O₂ cells during prolonged galvanostatic cycling under oxygen atmosphere: (a) 0.5 M LiTFSI (b) 50 mM LiBr in 0.5 M LiTFSI (c) 50 M LiI in 0.5 M LiTFSI in diglyme solutions. Current density was fixed at 0.052 mA cm⁻². (d) Overlaid time vs. voltage profiles of Li–O₂ cell for 0.5 M LiTFSI, 50 mM LiI in 0.5 M LiTFSI, 50 M LiBr in 0.5 M LiTFSI in diglyme electrolytes and (e) the corresponding CO₂ gas evolutions monitored in OEMS.





Fig. 3 X-ray diffraction spectra of Li–O₂ cells with 0.5 M LiTFSI, 50 mM LiI in 0.5 M LiTFSI and 50 mM LiBr in 0.5 M LiTFSI in diglyme solutions after (a) first cycle discharge and (b) the subsequent charge under O₂.

vibration indicating the formation LiOH in case of LiI containing cells. These results are consistent with the findings of Zhou *et al.* where they demonstrated the formation of LiOH with increasing LiI concentration in the cells.^{23,39}

Fig. 2a presents the voltage *vs.* capacity profiles of cells containing neat 0.5 M LiTFSI without any halide RMs additive. The first discharge voltage profile stabilizes at ~ 2.8 V implying the formation of Li₂O₂ deposits on the cathode side. The subsequent charge process undergoes steep rise in voltage profile till ~ 3.9 V followed by plateau in the first cycle. Upon prolonged cycling, we can clearly see the raise in overpotential cycle by cycle. This is because of clogging of the porous carbon paper by non-conductive Li₂O₂ deposits, which require additional potential to oxidize. The discharge (oxygen reduction reaction (ORR)) and charge (oxygen evolution reaction (OER)) voltage profiles indicate the instabilities of Li–O₂ cells upon prolonged cycling. These instabilities of cell components are accompanied with oxidation of etheral solvent or carbon electrode corrosion during cycling.⁴⁰ Several of these parasitic reactions are accompanied with CO₂ evolution as a main decomposition product.⁴¹ Upon monitoring CO₂ evolution during galvanostatic discharge and charge for cells with and without RM's under Ar atmosphere, no CO₂ evolution was seen (Fig. 1c). The absence of CO₂ evolution in Ar environment implies that the operation voltage is not the main cause for

degradation processes accompanied with CO₂ evolution. However, the chemical and electrochemical activity of O₂ plays a major role. Therefore, to study the parasitic reactions accompanied with CO₂ evolution, operando electrochemical gas evolutions are conducted for prolonged cycling in the presence of O₂.

Fig. 2d shows time *vs.* voltage profiles and the corresponding CO₂ evolutions measured using OEMS are shown in Fig. 2e. During the initial oxidation process, a low intensity overshoot of CO₂ evolution was observed, which continued to rise in the following three cycles. Further, in later cycles the intensity of CO₂ decreases, which may be due to passivation of discharged species on porous carbon cathode. However, the CO₂ evolution was not entirely suppressed. The evolution of CO₂ may stem from a variety of side reactions, including: (1) oxidation and degradation of electrolyte solution during OER at the electrode electrolyte interphase.^{42–45} Scheme 1a shows the oxidative decomposition of diglyme in the presence of O₂ resulting in CO₂ evolution and other side products during Li₂O₂ decomposition.^{46,47} (2) Side reactions accompanied with carbon cathode instabilities at high overpotentials Scheme 1b shows the oxidation of carbon cathode to carbon dioxide and other side products such as Li₂CO₃ beyond ~ 3.5 V.^{48–52} (3) Parasitic reactions associated with lithium anode during OER.^{19–21} In summary, the cells containing pure 0.5 M LiTFSI electrolyte exhibit consistent CO₂ evolution during OER, indicating that severe parasitic reactions are present in Li–O₂ cells without RMs.

The initial discharge (ORR) process of Li–O₂ cells containing 50 mM LiI in addition to 0.5 M LiTFSI shows a voltage plateau at around 2.8 V (Fig. 2b), similar to the cells without the RM (0.5 M LiTFSI) (Fig. 2a). The subsequent 1st cycle charging (OER) exhibits long voltage plateau between ~ 3.3 V to ~ 3.4 V indicating the oxidation of iodide ion to triiodide ion (I[–] → I₃[–]). Fig. 3b present the XRD pattern of the carbon paper after the first charging process indicating the absence of any significant peak of LiOH phases at 2θ : ~ 32.7 . This implies oxidation of LiOH species at reduced overpotential that is ~ 3.4 V with respect to neat 0.5 M LiTFSI without any RM's.^{30,53–55} In case of second discharge process, the voltage profile follows a gentle steep descent from ~ 3.4 V with a voltage plateau at ~ 3.1 V that may be due to reduction of oxidized triiodide species to iodide ion (I₃[–] → I[–]) at the cathode interface, followed by stable discharge (ORR) profile at ~ 2.8 V. The 2nd cycle charge (OER) processes exhibit two distinct oxidation processes; a first voltage plateau at around 3.4 V that is attributed to the initial conversion from iodide ion (I[–]) to triiodide ion (I₃[–]). The second



Scheme 1 Proposed parasitic chemical reactions during OER. Reaction (a) showing the oxidative decomposition of diglyme to CO₂ evolution. Reaction (b) showing the direct oxidation of carbon cathode to CO₂ gas beyond ~ 3.5 V during OER.^{46–48}



voltage plateau at around 3.8 V is assigned to the formation of the more oxidative iodine (I_2) species. Upon prolonged cycling, LiI-containing cells display instabilities in their mediating capabilities, as evidenced by changes in their OER voltage profiles. As the cycling advances, we observe a decrease in the duration of the initial voltage plateau (I^- to I_3^-), with associated increase in the duration of the second voltage plateau (I_3^- to I_2). This observation suggests that in subsequent cycles, the LiI RM requires continued oxidation of iodide ions to iodine in order to effectively oxidize the LiOH deposits.^{23,56} But as reported that corrosive iodine formed during the OER can aggressively react with the cell components which is detrimental to Li–O₂ battery life.^{56–59} In this regard, monitoring the CO₂ using OEMS is useful to justify the reported claim.

Fig. 2d shows the overlapped time vs. voltage profile of 50 mM LiI in 0.5 M LiTFSI and the corresponding CO₂ evolution in Fig. 2e. We can clearly see that during the first cycle, cells containing LiI has suppressed the CO₂ evolution with respect to the 0.5 M LiTFSI based electrolyte solution. However, after few initial cycles we see an overshoot in CO₂ evolution. We attribute the evolution of CO₂ in later cycles to the following factors: (1) the formation of corrosive iodine species that can significantly oxidize cell components. (2) Parasitic reactions at the cathode–electrolyte interface and oxidation of the electrolyte solution at high potentials. (3) Instabilities associated with the carbon cathode above ~ 3.5 V.^{1,31,48,50} In conclusion, while Li RM's can initially suppress CO₂ evolution during OER, as the cycling progresses, their mediating capabilities deteriorate, resulting in the unavoidable formation of CO₂.

Fig. 2c depicts voltage profiles of Li–O₂ cells with addition of 50 mM LiBr to the neat 0.5 M LiTFSI in diglyme. The first discharge process exhibits a plateau at ~ 2.8 V similar to neat 0.5 M LiTFSI during ORR. The subsequent first oxidation voltage profile of Li–O₂ cells with LiBr, exhibits steep voltage rise followed by a plateau at ~ 3.4 V, which is assigned to the oxidation of Br^- to Br_3^- that can diffuse and oxidize the ORR product which were deposited on the electrode surface. XRD is conducted after 1st cycle charge to evaluate the efficiency of LiBr in oxidizing the Li₂O₂ species. XRD patterns in Fig. 3b shows no crystalline phases on the carbon cathode implying efficient oxidation of Li₂O₂ species at lower charging potentials with respect to neat 0.5 M LiTFSI without any RM that otherwise requires high overpotentials for oxidizing the Li₂O₂ species.^{53,54} In the following reduction processes (discharge) of LiBr-containing cells, an additional voltage plateau is observed. This additional plateau at ~ 3.4 V is ascribed to the reduction of Br_3^- to Br^- as a result of the prior oxidation step. Unlike the LiI-containing cells, upon advanced cycling, cells with LiBr don't exhibit additional oxidation plateau at higher potentials. This phenomena is because of higher overpotential needed for the conversion of Br_3^- to Br_2 with respect to conversion of I_3^- to I_2 as suggested by cyclic voltammogram in Fig. S4.† These results are in good agreement with results published by Aurbach and Sun laboratories.^{23,31,60–62} More significantly, the LiBr containing cells exhibits stable voltage profiles upon prolonged cycling. Upon monitoring CO₂ evolution using OEMS, we can observe that LiBr containing cells has significantly suppressed CO₂

evolution during the first OER (Fig. 2e). In contrast to LiI, the LiBr RM demonstrated stable mediating capabilities during the OER process. This is likely due to the fact that tribromide species are more effective oxidizing agents than triiodide species, which facilitates oxidation of the ORR product layer without the need for higher potentials and the associated risk of forming corrosive, free bromine species. Another possibility is that the formation of tribromide species buffers the anodic voltage, and keeps us in a high enough potential to oxidize ORR products, but not too high where the degradation of cell components can occur.

To isolate the RM operation of the halide salts from potential parasitic reactions mediated by the oxygen environment during charging, such as carbon corrosion and solvent oxidation,³³ cells with and without RM agents were discharged in O₂ and charged in an Ar atmosphere. Fig. 4 depicts the electrochemical profile of Li–O₂ cells charged in the presence of Ar and the corresponding O₂ and CO₂ evolutions. While charging in Ar, the

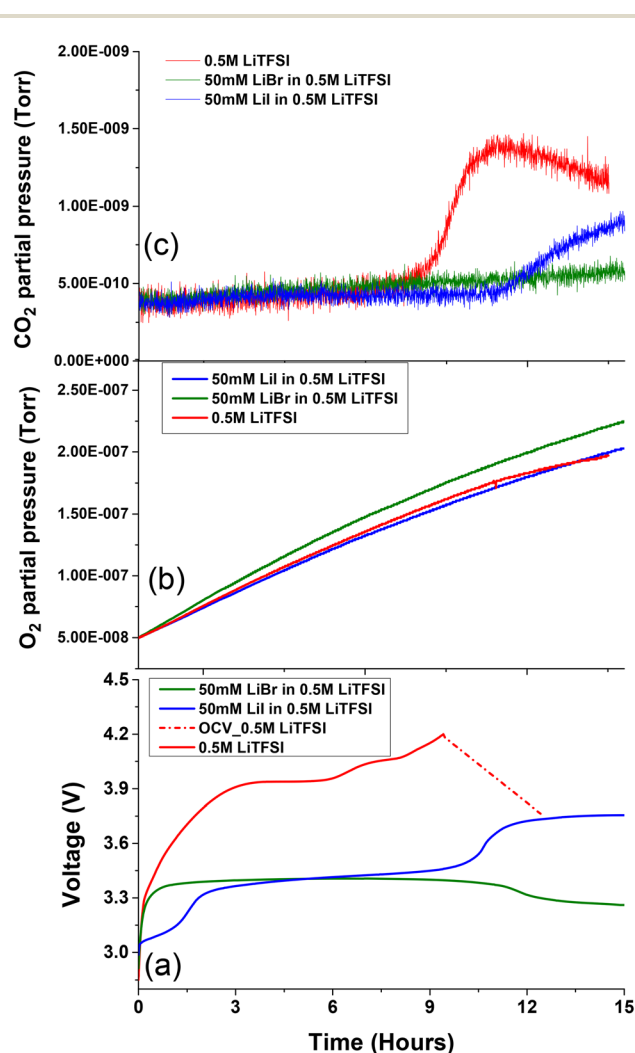


Fig. 4 (a) Voltage vs. specific discharge capacity profiles of Li–O₂ cells charged under an Ar atmosphere for pre-discharged cells in O₂. Current density was fixed at 0.052 mA cm⁻². The corresponding normalized (b) O₂ gas evolution and (c) CO₂ gas evolutions monitored in OEMS.



0.5 M LiTFSI in diglyme exhibits severe overpotential behaviour which resulted in CO₂ evolution below 4 V (Fig. 4c). These parasitic reactions are attributed to instabilities associated with carbon cathode and electrolyte decomposition at electrode electrolyte interface during oxygen evolution process at voltage potential below 4 V.^{63,64}

From the charging profile, it is evident that upon addition of 50 mM LiI to 0.5 M LiTFSI the OER takes place (Fig. 4b) at reduced overpotential with respect to cells without RMs.^{65,66} As previously discussed, the free iodine species are more reactive towards cell components than the complexed triiodide species. As can be observed (Fig. 4c), CO₂ evolution occurs at higher potentials during the formation of free iodine species.^{23,59} This implies that the main drawback of the LiI RM is the possible formation of iodine species which can lead to cell component degradation at high voltage. The formation of highly reactive iodine species at potentials lower than 4 V, makes it difficult to avoid their formation in Li–O₂ systems, where the potential can reach these values even in cells containing RM's.

Li–O₂ cells charged at Ar atmosphere were also conducted on 50 mM LiBr added to 0.5 M LiTFSI electrolyte solution (Fig. 4b). During charging process voltage increases to ~3.4 V followed stable charge profile followed by gentle decline at ~3.15 V after few hours. This indicates saturation of tribromide ion concentration from bromide ion. This behaviour is similar to OER voltage profile of the cells that were cycled in oxygen environment. Nevertheless, it is evident that cells containing LiBr have completely suppressed CO₂ evolution in the Li–O₂ cells under Ar atmosphere (Fig. 2c). This outcome also aligns with the observed increased evolution of oxygen from the oxidation of ORR products. These findings demonstrate that LiBr is a more suitable and efficient RM additive than LiI for long-term cycling of Li–O₂ cells.

Conclusions

In this study, we evaluated the effectiveness of halide-based redox mediator (RM) additives (LiI or LiBr) in suppressing side reactions during OER in Li–O₂ cells. By monitoring the evolution of CO₂ *via* OEMS, we were able to assess the effectiveness of RMs in suppressing these side reactions. We found that cells containing 0.5 M LiTFSI without RMs additives exhibited severe electrochemical instabilities from the first cycle. These instabilities were correlated to the evolution of CO₂ during OER. On the other hand, in cells where 50 mM LiI was added to 0.5 M LiTFSI solution, no CO₂ evolution was observed in the first oxidation processes. However, in the following cycles, an increase in the amount of CO₂ evolution was detected for cells containing LiI. We attribute this instability to the formation of iodine (I₂) species during the following oxidation processes. Free iodine species are more aggressive and corrosive toward the cell components than the complexed tribromide (I₃[−]) species that were prevalent in the first OER processes. Furthermore, the higher overpotential that is accompanied with the formation of I₃[−] can also lead to more side-reactions and evolution of CO₂ during the cell charging. In contrast, we found that LiBr suppressed the CO₂ evolution upon prolonged cycling.

We propose that this improved behaviour is likely due to the fact that tribromide species are more effective oxidation agents than triiodide species, which allows for oxidation of the ORR product layer without the need for higher potentials and the associated risk of forming damaging free bromine species. These results emphasize that LiBr additives are more efficient than LiI as RM additives for Li–O₂ cells. Furthermore, this study highlights the importance of thoroughly examining RM additives to ensure optimal performance and stability of Li–O₂ cells.

Experimental

Materials

Lithium bis(trifluoromethylsulphonyl)imide (LiTFSI ≥ 99.95%), lithium bromide (≥98.0%), lithium iodide (≥99.9%), lithium foil were purchased from Sigma Aldrich, high purity Diglyme purchased from Sigma (diethylene glycol dimethylether; 99.99% anhydrous), and carbon paper is purchased from MARKETECH International Inc.

Electrolyte preparation

All the salts were dried under ultra-high vacuum at ~120 °C overnight to remove any amount of moisture. 0.5 M LiTFSI, 50 mM LiI in 0.5 M LiTFSI and 50 mM LiBr in 0.5 M LiTFSI electrolytes are prepared in diglyme solutions in Argon filled atmosphere (O₂, H₂O ≤ 0.1 ppm). All the electrolyte was dried using 4 Å molecular sieves. The water content of all electrolytes was determined by Karl Fischer titration (Metrohm 756 KF) to be ≤50 ppm.

High resolution scanning electron microscopy (HRSEM)

High resolution scanning electron microscopy imaging of discharged products were taken by HR-SEM, Magellan 400 L. SEM samples were prepared by smearing the powder on carbon tape.

X-ray diffraction (XRD)

XRD is conducted for free-standing carbon cathode paper after discharge, using Bruker D8 Advanced X-ray diffractometer, using Cu K α radiation source.

Attenuated total reflectance Fourier transform infrared spectroscopy (ATR-FTIR)

ATR-FTIR was conducted using Thermo Scientific Nicolet iS10 was used for FTIR analysis to know the functional groups of discharged products formed on the porous carbon paper.

Online electrochemical mass spectroscopy

The *in situ* gas evolution during the charge–discharge cycles for Li–O₂ cells were monitored using an online electrochemical mass spectrometer (OEMS) from Hiden Analytical. OEMS is conducted in an in-house designed cell as reported previously, we monitored the O₂ and CO₂ evolution with respect to the voltage profiles for cells containing 0.5 M LiTFSI, 50 mM LiBr in 0.5 M LiTFSI and 50 mM LiI in 0.5 M LiTFSI electrolytes.²⁹ OEMS cells for Li–O₂ cells were prepared in an argon-filled glovebox by



combining Li as the anode (ϕ 14 mm) with two glass fiber separators (ϕ 29 mm), and 200 μ L of proposed electrolyte solution with binder free carbon paper is used as cathode (ϕ 11 mm). The cell outlet was connected to the OEMS capillary. The electrochemical measurements were conducted using a MPG potentiostat (BioLogic Science Instruments) within a potential window of 2.0–4.2 V at 0.052 mA cm⁻² current density charge-discharge cycles. The partial pressures of the evolved gases were plotted against time.

Conflicts of interest

There are no conflicts to declare.

References

- W.-J. Kwak, Rosy, D. Sharon, C. Xia, H. Kim, L. R. Johnson, P. G. Bruce, L. F. Nazar, Y.-K. Sun and A. A. Frimer, *Chem. Rev.*, 2020, **120**, 6626–6683.
- P. G. Bruce, S. A. Freunberger, L. J. Hardwick and J.-M. Tarascon, *Nat. Mater.*, 2012, **11**, 19–29.
- J. Lu, L. Li, J.-B. Park, Y.-K. Sun, F. Wu and K. Amine, *Chem. Rev.*, 2014, **114**, 5611–5640.
- Z. Peng, S. A. Freunberger, Y. Chen and P. G. Bruce, *Science*, 2012, **337**, 563–566.
- J.-J. Xu, Z.-L. Wang, D. Xu, L.-L. Zhang and X.-B. Zhang, *Nat. Commun.*, 2013, **4**, 1–10.
- Z. Jian, P. Liu, F. Li, P. He, X. Guo, M. Chen and H. Zhou, *Angew. Chem., Int. Ed.*, 2014, **53**, 442–446.
- Y. Wang and Y.-C. Lu, *Energy Storage Mater.*, 2020, **28**, 235–246.
- N. Mahne, O. Fontaine, M. O. Thotiyil, M. Wilkening and S. A. Freunberger, *Chem. Sci.*, 2017, **8**, 6716–6729.
- J. Højberg, B. D. McCloskey, J. Hjelm, T. Vegge, K. Johansen, P. Norby and A. C. Luntz, *ACS Appl. Mater. Interfaces*, 2015, **7**, 4039–4047.
- L. Ma, T. Yu, E. Tzoganakis, K. Amine, T. Wu, Z. Chen and J. Lu, *Adv. Energy Mater.*, 2018, **8**, 1800348.
- D. Sharon, D. Hirsberg, M. Salama, M. Afri, A. A. Frimer, M. Noked, W. Kwak, Y.-K. Sun and D. Aurbach, *ACS Appl. Mater. Interfaces*, 2016, **8**, 5300–5307.
- A. Dutta, R. A. Wong, W. Park, K. Yamanaka, T. Ohta, Y. Jung and H. R. Byon, *Nat. Commun.*, 2018, **9**, 680.
- B. D. McCloskey, R. Scheffler, A. Speidel, G. Girishkumar and A. C. Luntz, *J. Phys. Chem. C*, 2012, **116**, 23897–23905.
- Z. Lyu, Y. Zhou, W. Dai, X. Cui, M. Lai, L. Wang, F. Huo, W. Huang, Z. Hu and W. Chen, *Chem. Soc. Rev.*, 2017, **46**, 6046–6072.
- Y. Zhang, X. Zhang, J. Wang, W. C. McKee, Y. Xu and Z. Peng, *J. Phys. Chem. C*, 2016, **120**, 3690–3698.
- W.-J. Kwak, H. Kim, H.-G. Jung, D. Aurbach and Y.-K. Sun, *J. Electrochem. Soc.*, 2018, **165**, A2274.
- Y. Mo, S. P. Ong and G. Ceder, *Phys. Rev. B: Condens. Matter Mater. Phys.*, 2011, **84**, 205446.
- Y.-C. Lu, B. M. Gallant, D. G. Kwabi, J. R. Harding, R. R. Mitchell, M. S. Whittingham and Y. Shao-Horn, *Energy Environ. Sci.*, 2013, **6**, 750–768.
- X. Zhang, Z. Xie and Z. Zhou, *ChemElectroChem*, 2019, **6**, 1969–1977.
- X. Bi, K. Amine and J. Lu, *J. Mater. Chem. A*, 2020, **8**, 3563–3573.
- H. Song, H. Deng, C. Li, N. Feng, P. He and H. Zhou, *Small Methods*, 2017, **1**, 1700135.
- Z. Wu, Y. Tian, H. Chen, L. Wang, S. Qian, T. Wu, S. Zhang and J. Lu, *Chem. Soc. Rev.*, 2022, **51**, 8045–8101.
- W.-J. Kwak, D. Hirshberg, D. Sharon, M. Afri, A. A. Frimer, H.-G. Jung, D. Aurbach and Y.-K. Sun, *Energy Environ. Sci.*, 2016, **9**, 2334–2345.
- J. Wang, J. Zheng and X. Liu, *Phys. Chem. Chem. Phys.*, 2022, **24**, 17920–17940.
- Z.-F. Chen, X. Lin, H. Xia, Y. Hong, X. Liu, S. Cai, J.-N. Duan, J. Yang, Z. Zhou and J.-K. Chang, *J. Mater. Chem. A*, 2019, **7**, 14260–14270.
- T. Zhang, K. Liao, P. He and H. Zhou, *Energy Environ. Sci.*, 2016, **9**, 1024–1030.
- A. G. Tamirat, X. Guan, J. Liu, J. Luo and Y. Xia, *Chem. Soc. Rev.*, 2020, **49**, 7454–7478.
- C.-Y. Li, M.-S. Wu, W.-R. Chen, Y.-J. Rong, Q.-Y. Wang and X.-P. Zhang, *Chem. Commun.*, 2022, **58**, 13632–13635.
- Rosy, S. Akabayov, M. Leskes and M. Noked, *ACS Appl. Mater. Interfaces*, 2018, **10**, 29622–29629.
- T. Liu, M. Leskes, W. Yu, A. J. Moore, L. Zhou, P. M. Bayley, G. Kim and C. P. Grey, *Science*, 2015, **350**, 530–533.
- Z. Liang and Y.-C. Lu, *J. Am. Chem. Soc.*, 2016, **138**, 7574–7583.
- A. Tkacheva, B. Sun, J. Zhang, G. Wang and A. M. McDonagh, *J. Phys. Chem. C*, 2021, **125**, 2824–2830.
- J. Zhang, B. Sun, Y. Zhao, A. Tkacheva, Z. Liu, K. Yan, X. Guo, A. M. McDonagh, D. Shanmukaraj and C. Wang, *Nat. Commun.*, 2019, **10**, 602.
- M. Tułodziecki, J.-M. Tarascon, P.-L. Taberna and C. Guéry, *Electrochem. Commun.*, 2017, **77**, 128–132.
- V. Sharova, A. Moretti, T. Diemant, A. Varzi, R. J. Behm and S. Passerini, *J. Power Sources*, 2018, **375**, 43–52.
- L. Coustan and D. Belanger, *J. Electroanal. Chem.*, 2019, **854**, 113538.
- Z. Li, S. Ganapathy, Y. Xu, J. R. Heringa, Q. Zhu, W. Chen and M. Wagemaker, *Chem. Mater.*, 2017, **29**, 1577–1586.
- A. E. Torres, E. Ramos and P. B. Balbuena, *J. Phys. Chem. C*, 2020, **124**, 10280–10287.
- Y. Qiao, S. Wu, Y. Sun, S. Guo, J. Yi, P. He and H. Zhou, *ACS Energy Lett.*, 2017, **2**, 1869–1878.
- D. W. Kim, S. M. Ahn, J. Kang, J. Suk, H. K. Kim and Y. Kang, *J. Mater. Chem. A*, 2016, **4**, 6332–6341.
- H. Guo, W. Luo, J. Chen, S. Chou, H. Liu and J. Wang, *Adv. Sustainable Syst.*, 2018, **2**, 1700183.
- D. Sharon, D. Hirsberg, M. Afri, A. Garsuch, A. A. Frimer and D. Aurbach, *J. Phys. Chem. C*, 2014, **118**, 15207–15213.
- Y. S. Jeong, J.-B. Park, H.-G. Jung, J. Kim, X. Luo, J. Lu, L. Curtiss, K. Amine, Y.-K. Sun and B. Scrosati, *Nano Lett.*, 2015, **15**, 4261–4268.
- B. D. McCloskey, D. S. Bethune, R. M. Shelby, T. Mori, R. Scheffler, A. Speidel, M. Sherwood and A. C. Luntz, *J. Phys. Chem. Lett.*, 2012, **3**, 3043–3047.



- 45 J. Park, S. H. Lee, H. Jung, D. Aurbach and Y. Sun, *Adv. Mater.*, 2018, **30**, 1704162.
- 46 N. Tsiouvaras, S. Meini, I. Buchberger and H. A. Gasteiger, *J. Electrochem. Soc.*, 2013, **160**, A471–A477.
- 47 S. A. Freunberger, Y. Chen, N. E. Drewett, L. J. Hardwick, F. Bardé and P. G. Bruce, *Angew. Chem., Int. Ed.*, 2011, **50**, 8609–8613.
- 48 M. M. Ottakam Thotiyl, S. A. Freunberger, Z. Peng and P. G. Bruce, *J. Am. Chem. Soc.*, 2013, **135**, 494–500.
- 49 N. Mahne, B. Schafzahl, C. Leypold, M. Leypold, S. Grumm, A. Leitgeb, G. A. Strohmeier, M. Wilkening, O. Fontaine and D. Kramer, *Nat. Energy*, 2017, **2**, 1–9.
- 50 Z. Liang, Q. Zou, J. Xie and Y.-C. Lu, *Energy Environ. Sci.*, 2020, **13**, 2870–2877.
- 51 S. Meini, N. Tsiouvaras, K. U. Schwenke, M. Piana, H. Beyer, L. Lange and H. A. Gasteiger, *Phys. Chem. Chem. Phys.*, 2013, **15**, 11478–11493.
- 52 S. A. Freunberger, Y. Chen, Z. Peng, J. M. Griffin, L. J. Hardwick, F. Bardé, P. Novák and P. G. Bruce, *J. Am. Chem. Soc.*, 2011, **133**, 8040–8047.
- 53 S. Ganapathy, B. D. Adams, G. Stenou, M. S. Anastasaki, K. Goubitz, X.-F. Miao, L. F. Nazar and M. Wagemaker, *J. Am. Chem. Soc.*, 2014, **136**, 16335–16344.
- 54 H. Kim, W.-J. Kwak, H.-G. Jung and Y.-K. Sun, *Energy Storage Mater.*, 2019, **19**, 148–153.
- 55 Z. Gao, I. Temprano, J. Lei, L. Tang, J. Li, C. P. Grey and T. Liu, *Adv. Mater.*, 2023, **35**, 2201384.
- 56 W. J. Kwak, D. Hirshberg, D. Sharon, M. Afri, A. A. Frimer, H. G. Jung, D. Aurbach, Y. K. Sun, J. Kwak, D. Hirshberg, D. Sharon, H.-J. Shin, M. Afri, J.-B. Park, A. Garsuch, F. F. Chesneau, A. A. Frimer, D. Aurbach and Y.-K. Sun, *J. Mater. Chem. A*, 2015, **3**, 8855–8864.
- 57 W. K. Behl and D. Chin, *J. Electrochem. Soc.*, 1988, **135**, 16.
- 58 Y. G. Zhu, Q. Liu, Y. Rong, H. Chen, J. Yang, C. Jia, L.-J. Yu, A. Karton, Y. Ren and X. Xu, *Nat. Commun.*, 2017, **8**, 14308.
- 59 G. Leverick, M. Tułodziecki, R. Tatara, F. Bardé and Y. Shao-Horn, *Joule*, 2019, **3**, 1106–1126.
- 60 C.-Y. Li, M.-S. Wu, W.-R. Chen, Q.-Y. Wang, Y.-J. Rong and X.-P. Zhang, *J. Mater. Chem. A*, 2023, **11**, 937–942.
- 61 M. Ono and S. Matsuda, *J. Phys. Chem. C*, 2023, **127**, 6117–6124.
- 62 W. Kwak, S. Park, H. Jung and Y. Sun, *Adv. Energy Mater.*, 2018, **8**, 1702258.
- 63 S. Song, W. Xu, R. Cao, L. Luo, M. H. Engelhard, M. E. Bowden, B. Liu, L. Estevez, C.-M. Wang and J.-G. Zhang, *Nano Energy*, 2017, **33**, 195–204.
- 64 X. Yao, Q. Dong, Q. Cheng and D. Wang, *Angew. Chem., Int. Ed.*, 2016, **55**, 11344–11353.
- 65 C. M. Burke, R. Black, I. R. Kochetkov, V. Giordani, D. Addison, L. F. Nazar and B. D. McCloskey, *ACS Energy Lett.*, 2016, **1**, 747–756.
- 66 W.-J. Kwak, D. Hirshberg, D. Sharon, H.-J. Shin, M. Afri, J.-B. Park, A. Garsuch, F. F. Chesneau, A. A. Frimer and D. Aurbach, *J. Mater. Chem. A*, 2015, **3**, 8855–8864.

