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**Effects of Pore Connectivity and Tortuosity on the Dynamics  
of Fluids Confined in Sub-nanometer Pores**

Journal:	<i>Physical Chemistry Chemical Physics</i>
Manuscript ID	CP-ART-10-2021-004955.R1
Article Type:	Paper
Date Submitted by the Author:	16-Feb-2022
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1           Effects of Pore Connectivity and Tortuosity on the Dynamics of Fluids  
2                           Confined in Sub-nanometer Pores

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8                           **Abstract**

9   Dynamical behavior of fluids under nano-pore confinement is studied extensively as  
10 it has important implications for several industrial as well as geological processes.  
11 Pore network in many porous materials exhibits a varied degree of inter connections.  
12 The extent of this pore connectivity may affect the structural and dynamical  
13 behavior of the confined fluid. However, studies of fluid confinement addressing  
14 these effects systematically are lacking. Here, we report molecular dynamics  
15 simulation studies addressing the effects of pore connectivity on the dynamics of  
16 two representative fluids – CO<sub>2</sub> and ethane in silicalite by systematically varying the  
17 degree of pore connectivity through selectively blocking some pore space with  
18 immobile methane molecules. By selectively turning off the pore spaces in the shape  
19 of straight, or tortuous zigzag channels, we also probe the effects of pore tortuosity.  
20 In general, pore connectivity is found to facilitate both the translational as well as  
21 rotational dynamics of both fluids, while the intermolecular modes of vibration in  
22 both fluids remain largely unaffected. The effects of providing connections between  
23 a set of straight or zigzag channel-like pores are however more nuanced. Pore  
24 tortuosity facilitates the rotational motion, but suppresses the translational motion of  
25 CO<sub>2</sub>, while its effects on the rotational and translational motion of ethane are less  
26 pronounced. The intermolecular vibrational modes of both fluids shift to higher  
27 energies with an increase in the number of tortuous pores. The results reported here  
28 provide a detailed molecular level understanding of the effects of pore connectivity  
29 on the dynamics of fluids and thus have implications for applications like fluid  
30 separation.

31 **Keywords:** Silicalite; CO<sub>2</sub>; Ethane; Pore-connectivity; Pore-tortuosity; MD simulation  
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## 36 1.0 INTRODUCTION

37 Migration of fluids through the lithosphere occurs through porous rocks of varying  
38 porosity and permeability [1]. A significant fraction of these pores can occur at  
39 dimensions less than 100 nm and contribute significantly to accessibly reactive  
40 surface area [2]. When fluids transport via these pores, their dynamical behavior  
41 deviates significantly from the behavior in bulk. For this reason, dynamical behavior  
42 of fluids confined in nanopores has been an important field of investigation [1,3].  
43 The scenario of fluids confined in nano-scale pores also plays out in various  
44 industrial applications including catalysis [4]. Indeed, confining reactants in nano-  
45 pores has been a useful catalysis strategy [5]. Storage of CO<sub>2</sub> and other gases is  
46 another application where understanding the behavior of fluids under nano-  
47 confinement is important [6]. Membrane-based separation of fluids also makes use  
48 of the fact that some fluids can pass through the nanopores in a membrane more  
49 efficiently than others [7].

50 Pores in natural as well as engineered materials can exhibit a varied degree of inter-  
51 connectivity [8]. Some engineered porous media may exhibit unidimensional pores  
52 isolated from each other. MCM-41 and ZSM-22 are examples of such porous media  
53 with unidimensional pores [9, 10]. Fluid dynamics in such unidimensional pores is  
54 predominantly unrestricted in the direction of pore axis and is hindered mainly by  
55 the presence of another species. For example, propane is found to be hindered by the  
56 presence of water bridges in MCM-41-S pores [11, 12]. On the other hand, the pore  
57 structure in natural media is more disordered and can have pore spaces that are  
58 blocked and isolated from other pores resulting in a variation in the degree of inter-  
59 connectivity in pores [13]. This variation in the degree of inter-connectivity of pore  
60 spaces may affect the behavior of fluids confined in them [14 – 18]. While fluid  
61 structure and dynamics under nano-confinement has been studied widely, studies  
62 addressing the effects of pore connectivity on fluid behavior under confinement are

63 mostly limited to experimental [15, 16] or theoretical [17, 18] studies that lack  
64 molecular details.

65 Molecular simulations can provide important insights on these effects at the  
66 molecular level. For example, we have recently reported a systematic study on the  
67 effects of pore connectivity on the sorption of fluids using grand canonical Monte  
68 Carlo (GCMC) simulations [19]. While pore connectivity varied between 48 and 0  
69 pore connections, was found to affect the sorption amounts, the effect of pore  
70 connectivity is expected to have a stronger effect on the dynamical properties [19]. In  
71 an earlier attempt, we used molecular dynamics (MD) simulations to address the  
72 effects of inter-connectivity of pores on the structure and dynamics of confined  
73 fluids by comparing the behavior of CO<sub>2</sub> and ethane in ZSM-22, a zeolite  
74 characterized by unidimensional pores of 0.5 nm diameter, with that in silicalite (all  
75 silica analogue of ZSM-5), a zeolite with pores of the similar size but characterized  
76 by unidimensional pores connected to each other via zig-zag channel like pores  
77 running in a perpendicular plane [14]. Connecting the one-dimensional pores with  
78 quasi one-dimensional channels was found to suppress the dynamics of both fluids  
79 while the effect of connecting the pores by artificially inserting two-dimensional  
80 inter-crystalline space was different for the two fluids [14]. The complex effects that  
81 connecting the pores may have on the dynamics of confined fluids may be difficult  
82 to capture in a simple comparative study employing two substrates with presence or  
83 absence of pore connectivity and therefore requires a systematic study probing a  
84 diverse range of heterogeneity in pore connectivity in the same substrate.

85 Silicalite is an all-silica analogue of ZSM-5 zeolite and has a network of one-  
86 dimensional channel-like pores inter-connected at regular intervals with quasi one-  
87 dimensional zigzag channels in a perpendicular plane [19]. This intricate pore  
88 network structure provides an opportunity to systematically vary the connections  
89 between pores by selectively blocking some of them, thus resulting in different  
90 scenarios of pore connectivity in the same substrate. Further, with different channel

91 geometries – straight ellipsoidal channels oriented along the crystallographic *b*-axis  
92 and sinusoidal (zigzag) channels running in a parallel plane, selectively blocking all  
93 channels of one type can also help constrain the effects of pore geometry and  
94 tortuosity. In this case, the effect of tortuosity is limited to an on-off scenario  
95 (straight channels exhibit no tortuosity while zigzag channels have a tortuous  
96 shape). It is also worth noting that because the pore size in silicalite is similar  
97 regardless of pore type (straight versus zigzag), the pore size distribution is  
98 unimodal and sharply peaked. In the previous study addressing sorption properties  
99 [19], we created 12 models of silicalite with different degrees of pore connectivity by  
100 selectively blocking some channels via loading immobile methane molecules. These  
101 12 models had pores connected via different combinations of connections ranging  
102 between 0 and 48.

103 In the present work we utilize these 12 silicalite models to study the effects of pore  
104 connectivity on the structure and dynamics of CO<sub>2</sub> and ethane confined within them  
105 using MD simulations. We begin by providing details of these models and the MD  
106 simulations in section 2, after which we present results from these studies in section  
107 3. In section 4, we discuss the implications of the results of this study and in section 5  
108 we present the salient conclusions.

109

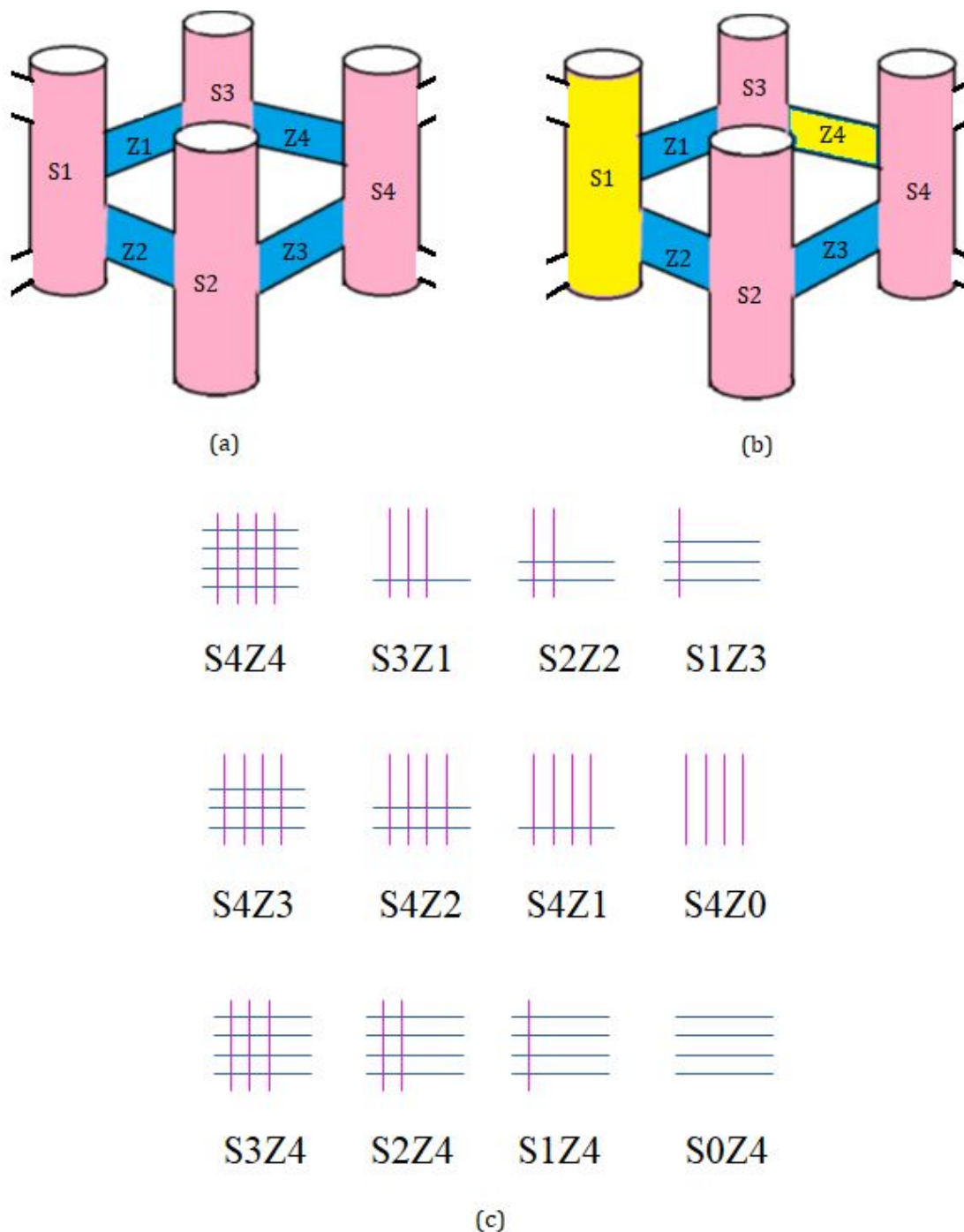
## 110 2.0 SIMULATION DETAILS

### 111 2.1 Substrate Models

112 This study employed models of silicalite with different number of pore connections  
113 generated in a previous study [19]. In brief these models were made by selectively  
114 blocking some channels of a supercell of silicalite [21] made up of 2×2×3 unit cells  
115 obtained with VESTA [22]. Methane molecules were used as blockers which were  
116 treated as an immobile part of the silicalite substrate in the MD simulations  
117 described here. Figure 1 (a) illustrates the salient features of the pore network in

118 silicalite. Straight channel-like pores are shown as pink cylinders while the zigzag  
119 channels connecting them are shown in blue. When some straight and/or zigzag  
120 channels are loaded with immobile methane molecules, they can isolate channels  
121 connected by them. This is illustrated in Figure 1 (b). Straight channels S3 and S4 are  
122 connected to each other by the zigzag channel Z4 (Figure 1(a)). When the zigzag  
123 channel Z4 is loaded with immobile methane molecules, it disrupts the connection  
124 between S3 and S4, isolating them from each other (Figure 1(b)). In the supercell of  
125 silicalite made up of  $2 \times 2 \times 3$  unit cells, there are a total of 48 connection combinations  
126 between straight and zigzag channels [19]. By selectively blocking some straight or  
127 zigzag channels, this number of pore connections can be reduced. The objective of  
128 this study is to investigate the effects of pore connectivity on the dynamics of fluids  
129 confined in a porous matrix. For this the system of pore connections were chosen so  
130 as to (i) vary the degree of pore connectivity over several values, and (ii) switch  
131 on/off pore tortuosity by selectively blocking all straight/zigzag channels  
132 respectively. This is illustrated in Figure 1 (c) which uses a cartoon schematic to  
133 represent the straight and zigzag channels by vertical magenta and horizontal blue  
134 lines, respectively. The number of intersections of these lines are proportional to the  
135 number of pore connections. A channel loaded with immobile methane is  
136 represented by an absence of the corresponding line. Thus, S4Z4 represents the  
137 unmodified silicalite where all straight and zigzag channels are open/free. When a  
138 fourth of all zigzag channels are blocked with immobile methane, it results in S4Z3  
139 with the number of pore connections reduced accordingly. In general, a model  
140 substrate with  $n$  open straight channels and  $m$  open zigzag channels is represented  
141 by  $S_nZ_m$ , where  $n$  and  $m$  represent the fraction out of a total of 4. All these  
142 substrates are illustrated in Figure 1 (c) and their pore-network details are listed in  
143 Table 1. For convenience, we classify the 12 substrates into 3 classes – S-major  
144 (substrates where more straight channels are open compared to zigzag channels;  
145 these are shown with red text color in the table), Z-major (substrates where more  
146 zigzag channels are open compared to straight channels, shown with blue text color

147 in the table) and half-volume (substrate where half-the total pore volume available is  
 148 blocked with methane, region in table 1 highlighted with yellow background). We  
 149 note that the unmodified silicalite (S4Z4) as also some other models may belong to  
 150 more than one of these 3 classes.



151

152 Figure 1. Cartoon schematics depicting (a) pore-network in unmodified silicalite. Straight channels  
 153 (S1-S4) running in the crystallographic *b*-axis are shown as pink vertical cylinders. These are  
 154 connected to each other via zigzag channels (Z1-Z4) shown in blue. Panel (b) shows the case when the

155 connection between S1 and S4 is disrupted by loading Z4 with methane (yellow). All 12 model  
 156 silicalite substrates used in the simulations are shown schematically in panel (c) representing the  
 157 straight and zigzag channels by vertical magenta and horizontal blue lines respectively. The number  
 158 of intersections of these lines are proportional to the number of pore connections. A channel loaded  
 159 with immobile methane is represented by an absence of the corresponding line.

160

161 **Table 1.** Different systems simulated and the corresponding number of pore – interconnections. S4Z4  
 162 is the unmodified silicalite. Systems with a larger number of straight channels that are free compared  
 163 to free zigzag channels are highlighted with red-colored text (S-major) while those with a larger  
 164 number of free zigzag channels compared to free straight channels are highlighted in blue-colored  
 165 text (Z-major). Systems where a half of the free space available in the unmodified silicalite is  
 166 blocked/free are highlighted with yellow background and the system S2Z2 with half each of the  
 167 straight and zigzag channels blocked/free is shown in green text color.

System name	Open straight channels (% of total)	Open sinusoidal channels (% of total)	Number of pore connections	Number of CO <sub>2</sub> molecules	Number of ethane molecules
<b>S4Z4</b>	<b>100</b>	<b>100</b>	<b>48</b>	<b>128</b>	<b>128</b>
<b>S4Z3</b>	<b>100</b>	<b>75</b>	<b>36</b>	<b>118</b>	<b>118</b>
<b>S4Z2</b>	<b>100</b>	<b>50</b>	<b>24</b>	<b>110</b>	<b>102</b>
<b>S4Z1</b>	<b>100</b>	<b>25</b>	<b>12</b>	<b>100</b>	<b>92</b>
<b>S4Z0</b>	<b>100</b>	<b>0</b>	<b>0</b>	<b>92</b>	<b>78</b>
<b>S3Z1</b>	<b>75</b>	<b>25</b>	<b>9</b>	<b>78</b>	<b>72</b>
<b>S2Z2</b>	<b>50</b>	<b>50</b>	<b>12</b>	<b>76</b>	<b>70</b>
<b>S1Z3</b>	<b>25</b>	<b>75</b>	<b>9</b>	<b>74</b>	<b>70</b>
<b>S0Z4</b>	<b>0</b>	<b>100</b>	<b>0</b>	<b>78</b>	<b>75</b>
<b>S1Z4</b>	<b>25</b>	<b>100</b>	<b>12</b>	<b>90</b>	<b>88</b>
<b>S2Z4</b>	<b>50</b>	<b>100</b>	<b>24</b>	<b>104</b>	<b>102</b>
<b>S3Z4</b>	<b>75</b>	<b>100</b>	<b>36</b>	<b>118</b>	<b>112</b>

168

## 169 2.2. MD simulations

170 CO<sub>2</sub> or ethane molecules were loaded in the model silicalite at 308.16 K and 1 bar  
 171 partial gas pressures using grand canonical Monte Carlo simulations carried out  
 172 using DL-Monte [23]. These simulations provided the appropriate number of fluid  
 173 molecules adsorbed in the supercell at the specified environmental conditions. The



174 number of fluid molecules in the supercell are also tabulated in Table 1. Note that  
175 this approach of loading molecules is consistent for a given environmental condition  
176 of temperature and partial gas pressure and results in a different number of guest  
177 molecules between the two fluids in the same type of substrate. This difference is  
178 however, less than 18% in all cases, and is unlikely to result in significant deviation  
179 in properties due to loading differences. A larger difference in the number of  
180 adsorbed molecules can be found across different substrates for the same fluid. This  
181 is required to avoid spurious crowding due to a reduced pore volume in some  
182 substrates that would result if the same number of fluid molecules were used.

183 The configuration files obtained at the end of GCMC simulations were used as the  
184 starting configurations for MD simulations. As reported in an earlier publication,  
185 simulations of adsorption of CO<sub>2</sub> and ethane were carried out at 308.16 K because  
186 both guest fluids become supercritical at the highest partial pressure (100 bar)  
187 studied at this temperature. In continuation, the simulations in the present study  
188 were also carried out at the temperature of 308.16 K. Each MD simulation was  
189 carried out at in NVT ensemble using DL-Poly-4.10 [24]. As in the previous GCMC  
190 simulations [19], TraPPE-UA [25, 26] force field was used to model the interactions  
191 of CO<sub>2</sub>, ethane, and the immobile methane molecules, while ClayFF [27] was used to  
192 represent silicalite atoms. The force-field parameters for all atoms involved are listed  
193 in Table 2. Cross-terms were calculated using the Lorentz-Berthelot mixing rules  
194 [28]. Using the same force-field for both fluids helps keep the formalism uniform.  
195 Further, as shown in a previous study [29], the set of force-fields used here (TraPPE-  
196 UA for the fluids and ClayFF for silicalite) reproduce the experimental adsorption  
197 isotherms of both fluids in silicalite. CO<sub>2</sub> and ethane were modeled as rigid  
198 molecules with translational and rotational degrees of freedom, while all atoms in  
199 the substrate including the blocker methane molecules were kept rigid throughout  
200 the simulation. For small guest molecules, the effects of using a flexible substrate are  
201 small enough to be ignored. For example, Newsome and Coppens [30] have studied

202 CO<sub>2</sub> diffusion in Na-ZSM-5 an extra-framework cation containing analogue of  
 203 silicalite using a rigid model of the substrate. They obtained diffusion coefficients of  
 204 CO<sub>2</sub> in Na-ZSM-5 at 200 K and 300 K that were in fair agreement with neutron  
 205 scattering experiments [31]. Further, the emphasis of this study is more on the  
 206 variation of diffusion coefficient with the degree of pore connectivity instead of the  
 207 absolute values of the diffusion coefficients. The gains in simplicity of the rigid  
 208 framework used in this work thus outweigh a minor loss in accuracy. All  
 209 simulations employed a calculation time step of 1 fs and lasted for 2 ns each, out of  
 210 which the first 0.5 ns were used for equilibration. 0.5 ns period was found to be long  
 211 enough for the temperature and energy to stabilize and the corresponding  
 212 fluctuations reduce to acceptable values. The remaining 1.5 ns trajectory was used to  
 213 calculate quantities with positions and velocities recorded after every 0.02 ps. For  
 214 maintaining the system temperature in the NVT simulations, Nosé-Hover  
 215 thermostat with a relaxation time of 1 ps was used.

216 Table 2: Force-field parameters used in the simulations. O<sub>c</sub> stands for the oxygen  
 217 atom belonging to CO<sub>2</sub> molecule.

Species	Atom/Pseudo-atom	Charge (q/e)	$\epsilon$ (kJ)	$\sigma$ (Å)
Silicalite	Si	+2.10	0.000008	3.301
	O	-1.05	0.650198	3.166
CO <sub>2</sub>	C	+0.70	0.224	2.80
	O <sub>c</sub>	-0.35	0.657	3.05
Ethane	CH <sub>3</sub>	0.00	0.815	3.75
Blocker Methane	CH <sub>4</sub>	0.00	1.231	3.73

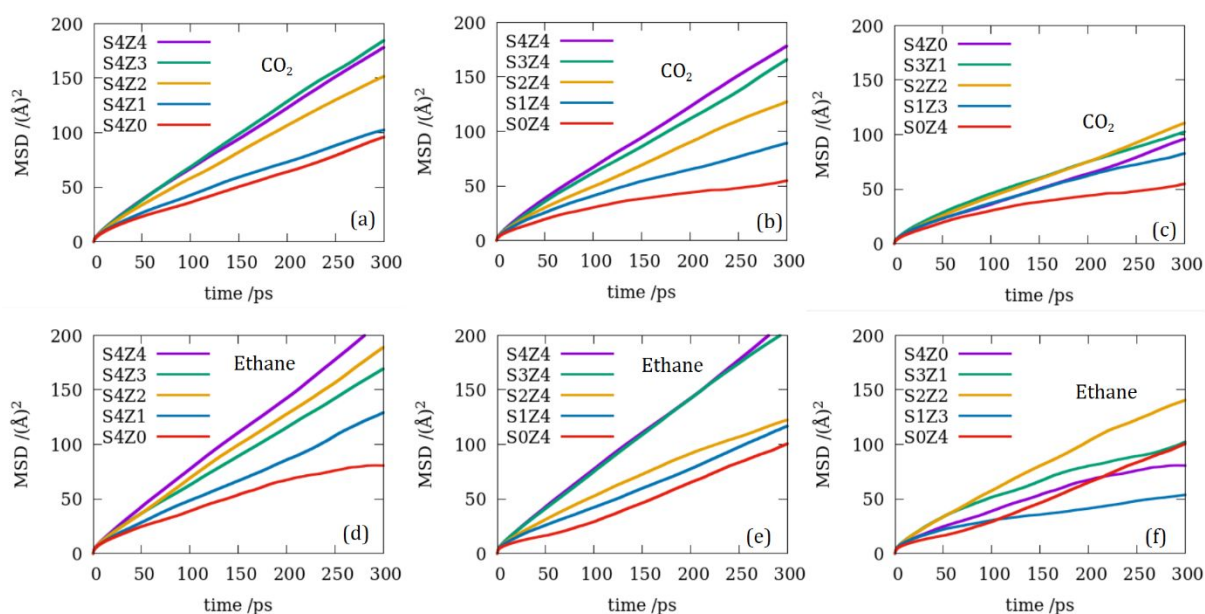
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### 219 3.0 RESULTS

220 We have already discussed the sorption and structural properties of CO<sub>2</sub> and ethane  
221 in these models in a previous publication [19]. Here we focus exclusively on the  
222 dynamical properties of the confined fluids, specifically translational, rotational and  
223 the intermolecular modes of vibration. We note that the intramolecular modes of  
224 vibration in both fluids are frozen by design due to a selection of rigid models for  
225 both fluids.

### 226 3.1 Translational motion

227 The translational motion of the confined fluids is described in terms of the mean  
228 squared displacement of the center of mass of the molecules. Figure 2 shows the  
229 MSD vs time plots for both fluids in all silicalite models investigated. In general,  
230 ethane mobility is found to be faster compared to CO<sub>2</sub> and connecting the pores is  
231 found to enhance the diffusivity of both fluids. For both fluids, a combination of  
232 straight and zigzag channels is found to facilitate diffusion. For CO<sub>2</sub> straight  
233 channels allow faster diffusion compared to zigzag channels, whereas for ethane, the  
234 distinction between the two channel types in facilitating diffusion is less clear. When  
235 the pore volume in silicalite is reduced to half, an equal distribution of the pore  
236 volume between straight and zigzag channels (S2Z2) is found to best facilitate the  
237 diffusion of both fluids.



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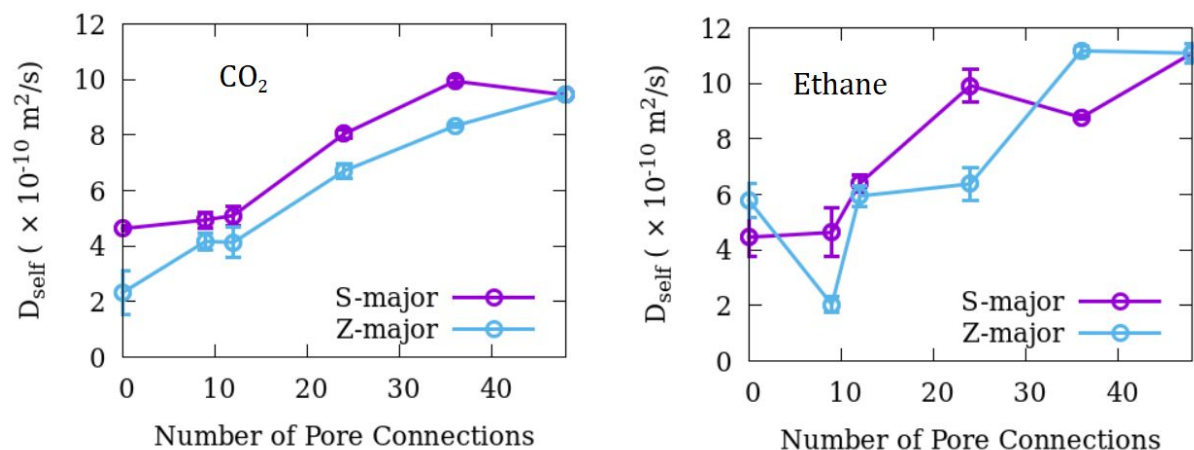
239 **Figure 2.** Mean squared displacement (MSD) as a function of time for CO<sub>2</sub> (a-c) and ethane (d-f) in  
240 silicalite. Data in (a) and (d) show S-major models of silicalite, where the number of open straight  
241 channels is equal to or greater than those of open zigzag channels. Panels (b) and (e) show the data for  
242 Z-major models where the number of zigzag channels is larger or equal to that of straight channels  
243 and (c) and (f) show the case of models with half of the unmodified silicalite (S4Z4) blocked with  
244 methane molecules. For meaning of the nomenclature SnZm refer to the text and Table 1.

245

246 Diffusivity of fluids can be quantified by calculating the self-diffusion coefficient  
247 ( $D_{\text{self}}$ ) from MD simulation data using the Einstein relation [28],

$$248 \quad D_{\text{self}} = \frac{1}{2n_d} \left( \lim_{t \rightarrow \infty} \frac{MSD}{t} \right) \quad (1),$$

249 where  $n_d$  is the number of degrees of freedom of translational motion and the  
250 quantity in the parentheses is the slope of MSD vs time plots evaluated at long times.  
251 We calculated the diffusion coefficient from the slope of MSD vs time plots in three  
252 different time ranges of 100 – 200 ps, 150 – 250 ps and 200 – 300 ps. The values of the  
253 diffusion coefficients obtained in three different time ranges thus were averaged and  
254 uncertainty obtained as the standard deviation over these averages. Values of  $D_{\text{self}}$   
255 calculated using Eq. 1 and the data in Figure 2 are shown in Figure 3 as a function of  
256 the number of pore connections. In general, the effect of connecting the pores is to  
257 enhance the diffusivity of both fluids. Further, in the case of CO<sub>2</sub>, diffusivity in the S-  
258 major substrates is higher than that in the Z-major substrate, a consequence of the  
259 simpler geometry of the straight channels. The variation in the diffusivity of ethane  
260 in different model substrate is relatively more irregular. Ethane diffusion through  
261 zigzag channels is comparable with that in the straight channels and this results in  
262 an overall higher diffusivity of ethane in the unmodified silicalite (S4Z4) also  
263 observed in an earlier study [32].

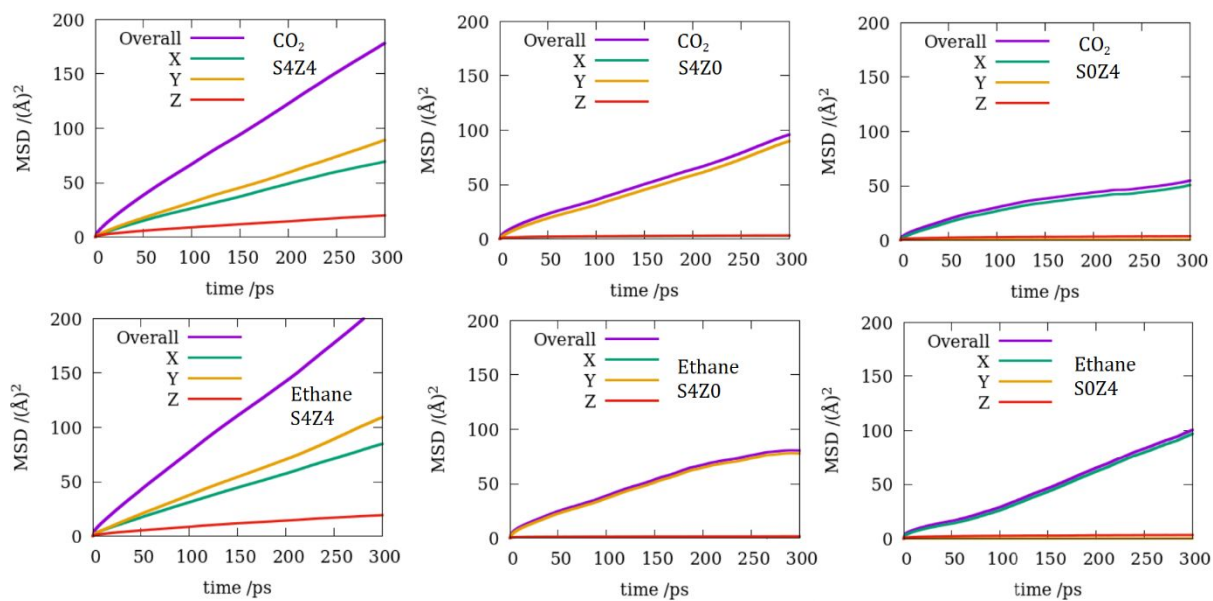


264

265 **Figure 3.** Self-diffusion coefficients ( $D_{\text{self}}$ ) as a function of the number of pore connections for CO<sub>2</sub> and  
 266 ethane confined in silicalite.

267

268 Because of the intricate pore network in silicalite, the dynamics of confined fluid is  
 269 expected to be anisotropic [32]. This results in a separation of the MSD in different  
 270 Cartesian directions. As straight channels are oriented exactly along the Y-direction,  
 271 whereas the zigzag channels lie in the X-Z plane oriented roughly, but not exactly  
 272 along the X-axis, the MSD of fluids in silicalite follows the order MSD<sub>y</sub> > MSD<sub>x</sub> >  
 273 MSD<sub>z</sub>. In case of isolated straight (S4Z0) or zigzag (S0Z4) channels, the pore network  
 274 is oriented completely in the Y direction and the X-Z plane, respectively, and the  
 275 MSD components along different directions can show significant variation. In Figure  
 276 4, we show the overall MSD resolved along the three Cartesian directions for the  
 277 three model substrates S4Z4, S4Z0 and S0Z4. As expected, the MSD along Y  
 278 direction in S4Z4 is highest for both fluids followed by that along the X direction. In  
 279 S4Z0, the motion occurs exclusively along the Y direction and the MSD in the X and  
 280 Z-directions is negligible. Conversely, in S0Z4, the motion is predominantly along X-  
 281 direction.



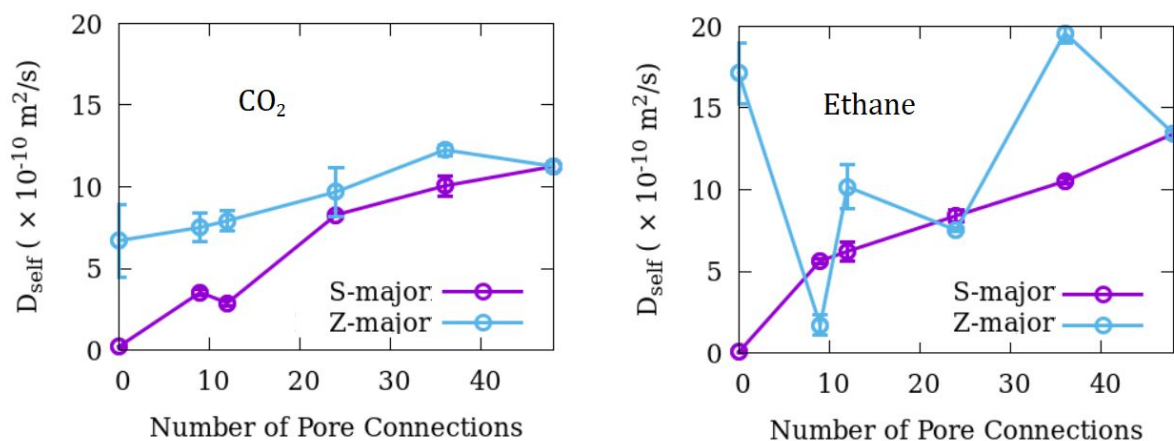
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283

284 **Figure 4.** MSD resolved in Cartesian directions compared to the overall MSD. Upper panels show  
 285 CO<sub>2</sub> while lower panels show ethane data. For clarity, data are shown for only three substrates –  
 286 S4Z4, S4Z0 and S0Z4.

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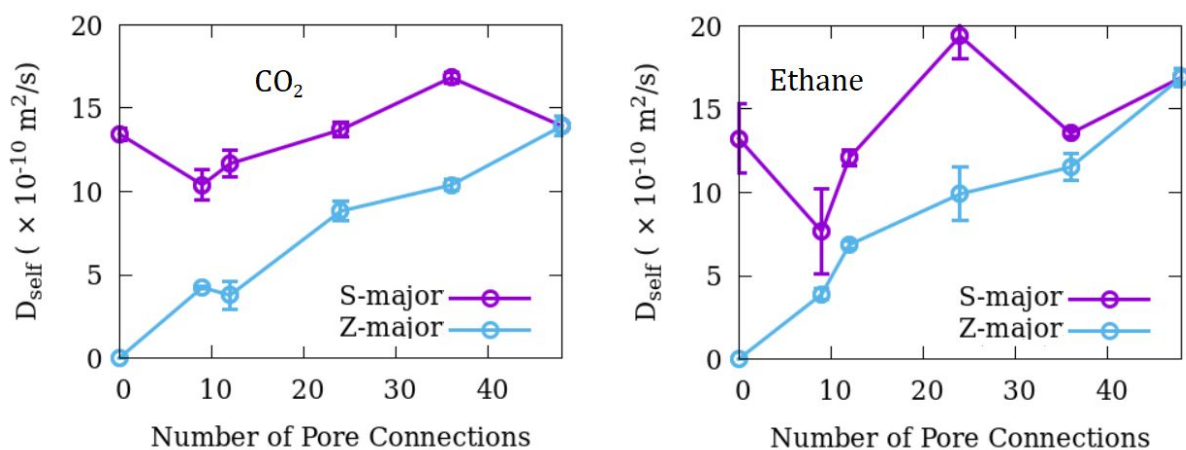
288 Figures 5 -7 show the direction specific self-diffusion coefficients of CO<sub>2</sub> and ethane  
 289 in silicalite as a function of pore connectivity. These direction specific self-diffusion  
 290 coefficients were calculated using long-time slope of the corresponding MSD vs time  
 291 plots in Eq. 1 with  $n_{d=1}$ . For CO<sub>2</sub>, the diffusion coefficients in X and Z direction  
 292 increases with increasing number of pore connections for both S-major as well as Z-  
 293 major substrates. In the Y-direction, CO<sub>2</sub> diffusivity is clearly facilitated by pore  
 294 connectivity in Z-major substrates, whereas for S-major substrates, this effect is less  
 295 clear with greater variation of  $D_{\text{self}}$  with number of pore connections. The difference  
 296 between the two extreme cases of S4Z0 (leftmost datum) and S4Z4 (rightmost  
 297 datum) is smaller than the uncertainties involved. This similarity in the diffusivity  
 298 along Y-axis in S4Z0 and S4Z4 is also true for ethane, where the difference between  
 299 the data representing the two substrates is negligible. For all other cases with ethane,  
 300 the pore connections can be seen to facilitate diffusion, except for diffusion along X-  
 301 direction in Z-major substrates where the variation is complex and the difference  
 302 between the extreme cases is negligible.



303

304 **Figure 5.** Direction-specific self-diffusion coefficients along Cartesian X-direction of CO<sub>2</sub> and  
 305 ethane in silicalite as a function of pore connectivity.

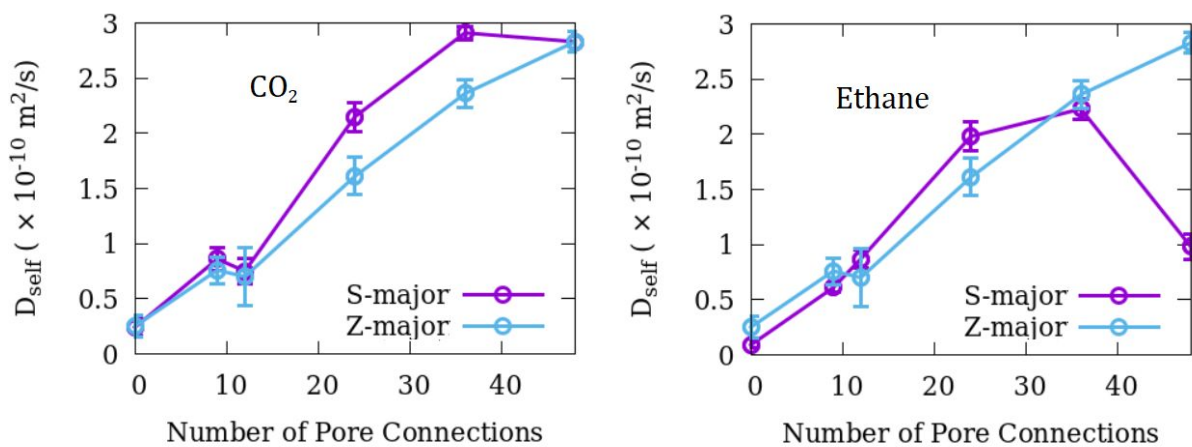
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307

308 **Figure 6.** Direction-specific self-diffusion coefficients along Cartesian Y-direction of CO<sub>2</sub> and  
 309 ethane in silicalite as a function of pore connectivity.

310

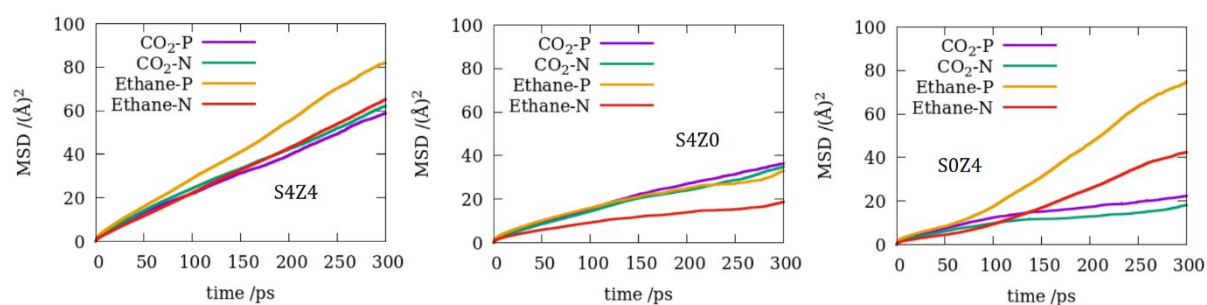


311

312 **Figure 7.** Direction specific self-diffusion coefficients along Cartesian Z-direction of CO<sub>2</sub> and  
 313 ethane in silicalite as a function of pore connectivity.

314  
 315 In the TraPPE-UA formalism, both CO<sub>2</sub> and ethane are linear dumbbell shaped  
 316 molecules. For such molecules, one can expect a difference in their dynamical  
 317 behavior along the molecular axis and in a plane perpendicular to it [33]. As the  
 318 molecules rotate, their orientation changes in time. At each time frame, we  
 319 resolve the displacement of the molecule along directions normal (N) and parallel  
 320 (P) to the instantaneous molecular axis. Since two directions can be normal to the  
 321 molecular axis, and only one is parallel to it, the MSD perpendicular to the  
 322 molecular axis is normalized via a division by 2. Figure 8 shows the MSD in the  
 323 two directions with respect to the molecular axis for CO<sub>2</sub> and ethane in 3 model  
 324 silicalite substrates. While CO<sub>2</sub> shows a little preference in the direction of motion  
 325 with respect to molecular axis, ethane clearly prefers to move parallel to the  
 326 molecular axis in all the three cases investigated.

327



328

329 **Figure 8.** MSD along the molecular axis (P) and normal to it (N) for the two fluids in three model  
 330 silicalite substrates.

331

### 332 3.2 Rotational Motion

333 Rotational motion of the two fluids in silicalite is studied via rotational  
 334 correlation function (RCF) calculated using Eq. 2 [32]

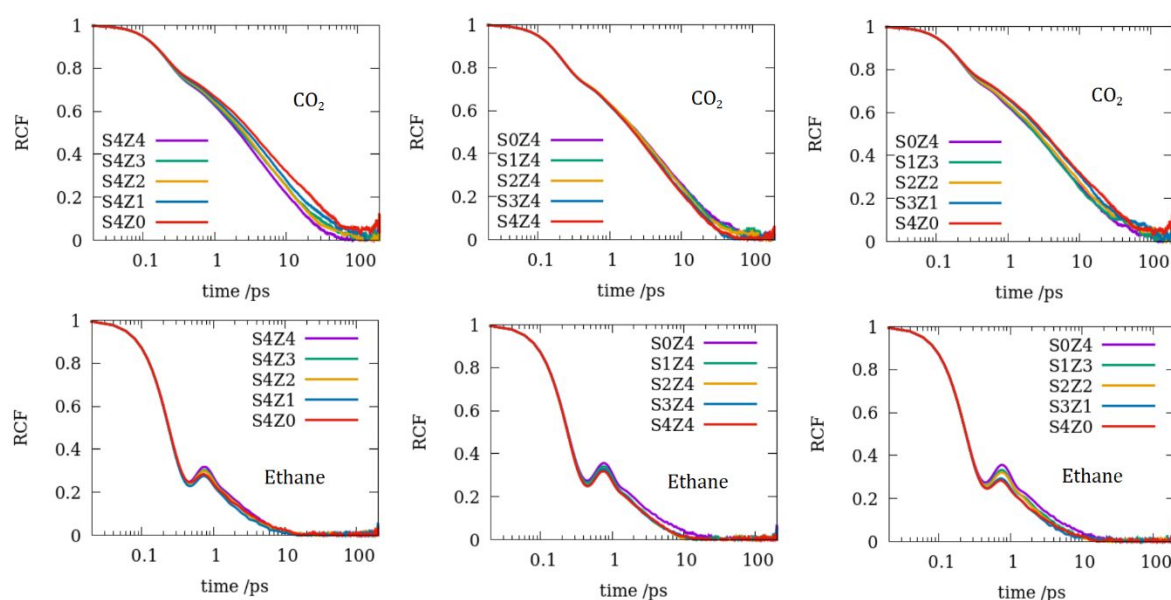
$$335 \text{RCF} = \langle \mathbf{u}(t+t_0) \cdot \mathbf{u}(t_0) \rangle \quad (2)$$

336 Here  $\mathbf{u}(t)$  is a unit vector attached to the molecular axis at time  $t$  and the angular  
 337 brackets denote an average over all molecules and the times of origin  $t_0$ . RCF of  
 338 CO<sub>2</sub> and ethane in the silicalite substrates are shown in Figure 9. As in  
 339 translational motion, ethane is found to exhibit a faster rotational motion in



340 silicalite. This is evident from a faster decay of RCF of ethane. Further, the ethane  
 341 RCF exhibits a strong wiggle at around 1 ps, - a distinct signature of restricted  
 342 librational motion at short times [32, 34]. Over a longer timescale of a few tens of  
 343 picoseconds the RCF decay completely. The RCF behavior in both fluids undergo  
 344 a transition at around 1 ps. Below this time scale, the decay is fast and  
 345 independent of the substrate. This is the initial free rotation that occurs before the  
 346 molecule can experience any hindrance to rotation due to its environment – e.g.,  
 347 substrate atoms, other fluid molecules, etc. – and is characteristic of the fluid  
 348 molecular properties alone.

349



350

351 **Figure 9.** Rotational correlation functions (RCF) of CO<sub>2</sub> (top panels) and ethane (bottom panels) in  
 352 various models of silicalite substrate.

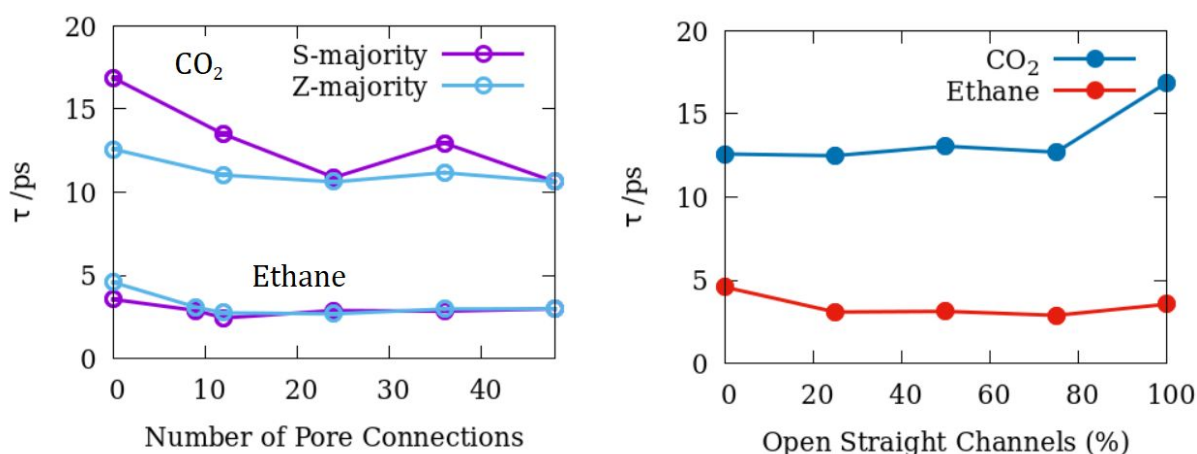
353

354 Beyond 1 ps, the RCF of both fluids decay at a relatively slower rate and also  
 355 show a dependence on the substrate. This region can therefore be used to study  
 356 the effects of pore connectivity and tortuosity on the rotational behavior of the  
 357 two fluids. In particular, the RCF of both fluids were fit with the following  
 358 exponential decay function to obtain a characteristic decay time ( $\tau$ )

359  $RCF = a \cdot \exp(-t/\tau) + b$  (3)

360 The RCF were fitted with the above model function with  $a$ ,  $b$  and  $\tau$  as the fitting  
 361 parameters. In Figure 10, we show the values of the decay time  $\tau$  obtained for all  
 362 substrates as a function of pore connectivity and tortuosity (in terms of the  
 363 percentage of open straight channels). Like translational motion, the rotational  
 364 motion of both fluids is found to be facilitated by connecting the pores, although  
 365 the effect of pore connectivity is relatively smaller on rotational motion as  
 366 compared to translational motion. By comparison, rotational motion of  $\text{CO}_2$  is  
 367 affected by pore tortuosity somewhat more than that of ethane. Further, while  
 368  $\text{CO}_2$  rotation gets faster (smaller times for zigzag channels represented by the  
 369 leftmost datum, 0 straight channels) in tortuous pores, the rotation of ethane is  
 370 slightly suppressed in them compared to straight channels.

371



372

373 **Figure 10.** Characteristic decay times  $\tau$  for rotational motion obtained by fitting the RCF with an  
 374 exponential decay function (Eq. 4), for  $\text{CO}_2$  and ethane in silicalite as a function of pore  
 375 connectivity and the percentage of open straight channels. Uncertainty in the data is smaller than  
 376 the symbols used.

377

### 378 3.3 Intermolecular Vibration

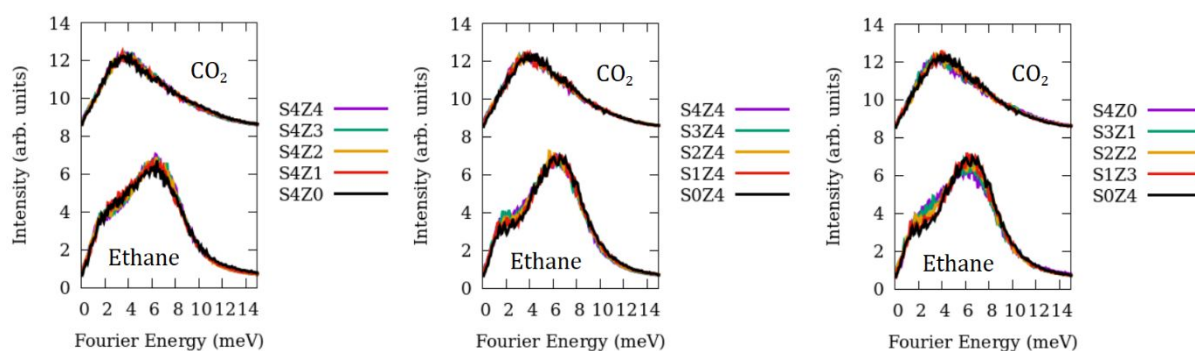
379 Intermolecular vibrational motion is studied via the power spectra  $I(\omega)$  of the  
 380 velocity autocorrelation function (VACF) using the following relations [32, 35]

$$381 \text{VACF} = \langle v(t+t_0) \cdot v(t_0) \rangle \quad (4)$$

$$382 I(\omega) = \int (\text{VACF}) \cos(\omega t) dt \quad (5)$$

383 The effect of pore connectivity on the intermolecular vibrational spectra of CO<sub>2</sub> in  
 384 silicalite is negligible (Figure 11). However, comparing the half-volume data  
 385 (rightmost panel), the peak in the CO<sub>2</sub> spectra shifts slightly to higher energies when  
 386 more zigzag channels are open. For ethane, the power spectra are bimodal for all  
 387 substrates and the higher energy mode increases at the expense of the lower energy  
 388 mode as more zigzag channels are opened. Thus, the intermolecular vibrations of  
 389 both fluids are more energetic in zigzag channels as compared to straight channels.

390



391

392 **Figure 11.** Power spectra corresponding to the intermolecular vibrational motion of CO<sub>2</sub> (top) and  
 393 ethane (bottom) in different silicalite substrates. For clarity, the intensities of the CO<sub>2</sub> spectra are  
 394 shifted upwards by 8 units.

395

## 396 4.0 DISCUSSION

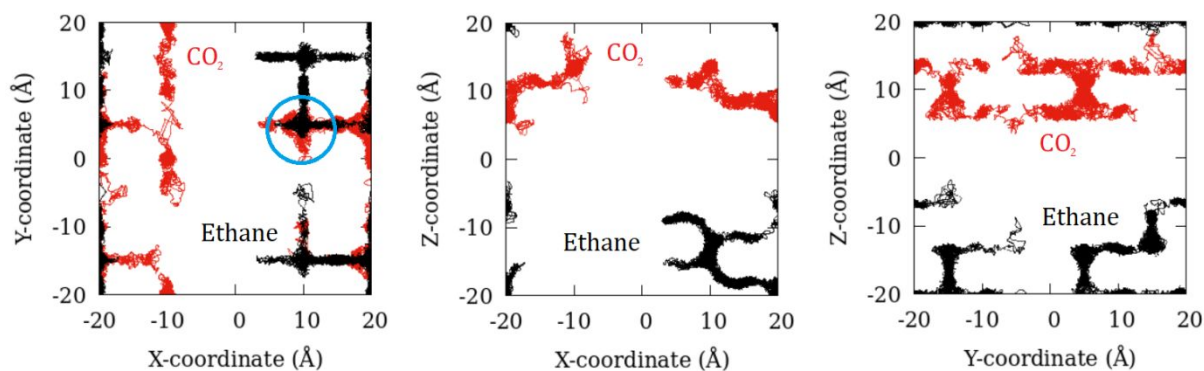
397 In what follows we discuss the effects of pore connectivity and tortuosity on the  
 398 dynamical behavior of two fluids and their implications.

### 399 4.1 Effects of Pore Connectivity

400 The overall effect of connectivity in the pore network of silicalite is to enhance both  
 401 the translational as well as the rotational motion of both fluids – CO<sub>2</sub> and ethane  
 402 (Figures 3 and 10 (a)). The effect of connecting straight or tortuous zigzag pores on  
 403 the dynamics of fluids through them is however more nuanced. As these pores are  
 404 essentially one-dimensional channels, a fair comparison between the effects of  
 405 connecting them can be made by comparing the 1-dimensional diffusivity of the  
 406 confined fluids along the direction of the channel axis. This is relatively easier to do

407 for straight channels as they are perfectly aligned along the Cartesian Y-direction  
408 whereas zigzag channels have their pore axis aligned mostly along the X-direction  
409 with a minor component along the Z-direction. Figure 6 presents diffusivity along Y-  
410 direction, where the data corresponding to S-major substrates exhibit an irregular  
411 behavior while that corresponding to Z-major substrates exhibit a relatively smooth  
412 increase with an increase in pore connections. This, along with the results shown in  
413 Figure 3 indicates that while connecting the straight channels does increase the  
414 overall diffusivity, this increase is a result of the cross-current made available by  
415 opening a cross-channel while the motion along the original direction remains  
416 largely unaffected. Note that the difference between the diffusivity along Y-direction  
417 for totally isolated straight channels and straight channels connected to maximum is  
418 negligible for both fluids. It is also noteworthy that in a previous study [14] a  
419 comparison between the 1-dimensional diffusivity of both CO<sub>2</sub> and ethane in  
420 isolated straight channels of ZSM-22 and connected straight channels of ZSM-5 led  
421 us to conclude that connecting the pores suppresses the 1-dimensional translational  
422 diffusivity of both fluids. While the previous comparative study employed two  
423 different substrates with similar shape and size of channel-like pores, the present  
424 study employing systematic blocking of the connections between straight channels  
425 in the same substrate avoids contaminating the effects seen by factors other than  
426 pore connectivity *viz.* a slight difference in pore size and shape. Like the  
427 implications of Figure 6, Figure 5 shows that while connecting straight channels  
428 progressively leads to a clear enhancement in the diffusivity along X-direction  
429 (perpendicular to the straight channel axis) for both fluids, the enhancement  
430 achieved in the diffusivity along this direction on connecting the zigzag channels is  
431 less pronounced for CO<sub>2</sub>. For ethane, the variation of diffusivity along X-direction in  
432 Z-major substrates is irregular with no significant difference between the two  
433 extreme cases of isolated zigzag channels and those connected to full extent.

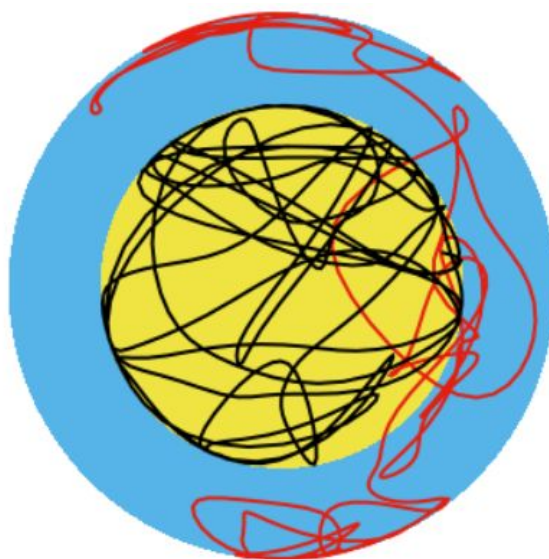
434 Examination of the variation of overall and direction-specific diffusion coefficients  
435 reveals that ethane exhibits a more complex pattern whereas data corresponding to  
436 CO<sub>2</sub> display a relatively smoother variation. In Figure 12 we show trajectories of the  
437 center of mass of one molecule each of CO<sub>2</sub> and ethane over the entire production  
438 time of 1.5 ns. Note that the shape traced by the trajectory of the CO<sub>2</sub> molecule is  
439 wider than that of ethane. This implies that CO<sub>2</sub> molecules are distributed more  
440 widely across the pore space and are in general closer to the pore surface than ethane  
441 molecules. This was also seen in the distribution observed in the previous GCMC  
442 simulations and is a result of a stronger substrate-fluid interaction in the case of CO<sub>2</sub>.  
443 This leads to an overall smaller diffusivity in CO<sub>2</sub> compared to ethane. Further, at  
444 the pore intersections (blue encircled region in the left-most panel), CO<sub>2</sub> molecules  
445 can occupy a wider region facilitating a smooth inter-channel migration whereas for  
446 ethane the inter-channel migration takes place via a relatively narrower intersection.  
447 This restricted inter-channel mobility might be responsible for the greater variation  
448 in the diffusivity of ethane as the pore connections are varied.



450 **Figure 12.** Trajectory of the center of mass of a tagged CO<sub>2</sub> (red) and ethane (black) molecule over  
451 1.5 ns in S4Z4. A pore intersection is highlighted in the left-most panel by encircling in blue.

452 Compared to translational motion, the effects of pore connectivity on the rotational  
453 motion are only marginal and are observed to be slightly stronger on rotation of CO<sub>2</sub>  
454 in the S-major substrates as compared to Z-major substrates (Figure 10). This is  
455 because, compared to translational motion, the rotational motion occurs at a much  
456 smaller length scale. Figure 13 shows the rotational motion of a tagged CO<sub>2</sub> and

457 ethane molecule each in the center of mass frame over a period of 10 ps. Over this  
458 small interval of time, while the ethane molecule has traversed the entire  
459 orientational space available (yellow sphere) the CO<sub>2</sub> molecule is restricted to only a  
460 limited part of the orientational space available to it (cyan sphere). This is consistent  
461 with the fact that the RCF for ethane decay completely within 10 ps while that of  
462 CO<sub>2</sub> have non-zero correlations left at this time (Figure 9) and indicates a stronger  
463 restriction on the rotational motion of CO<sub>2</sub> compared to ethane leading to smaller  
464 rotational time scales for the latter (Figure 10). This is a consequence of stronger  
465 substrate fluid interactions for CO<sub>2</sub> compared to ethane noted earlier. The tortuous  
466 shape of the zigzag channel can facilitate the rotational motion of CO<sub>2</sub> to a larger  
467 extent as these molecules lie relatively closer to the pore surface and therefore are  
468 affected by the pore shape to a greater extent. This results in a faster rotation as more  
469 and more zigzag channels are opened in S-major substrate leading to greater pore  
470 connectivity.



471

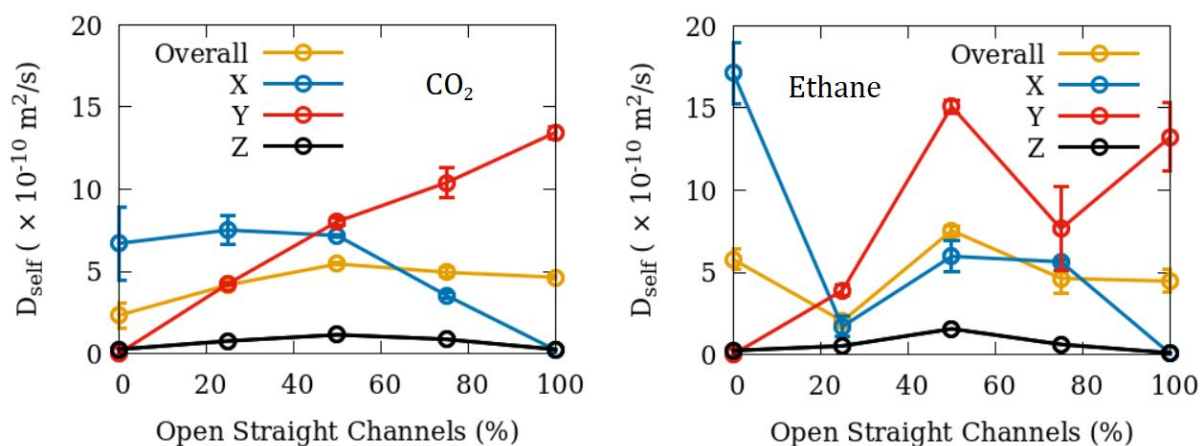
472 **Figure 13.** Trajectory of an oxygen atom belonging to a tagged CO<sub>2</sub> molecule (red) and that of a  
473 CH<sub>3</sub> pseudo atom belonging to a tagged ethane molecule (black) each in the center of mass  
474 frame of reference over a time of 10 ps in S4Z4. The entire orientational space available for ethane is  
475 shown as yellow sphere of diameter 0.154 nm while that for CO<sub>2</sub> is shown as the cyan sphere of  
476 diameter 0.232 nm containing the yellow sphere within itself.

477

478 4.2 Effects of Pore Tortuosity

479 The effects of pore tortuosity can be studied by considering the variation of  
 480 properties in the substrates characterized by 'half-volume' (yellow highlighted  
 481 region in Table 1). This is shown in Figure 10 for rotational time scales, Figure 11 for  
 482 intermolecular vibrational modes, and Figure 14 for self-diffusion coefficients  
 483 corresponding to the translational motion. While the overall translational motion of  
 484 CO<sub>2</sub> is clearly faster in straight channels and gets negatively impacted by tortuosity  
 485 of zigzag channels, for ethane, no significant difference is observed between the  
 486 diffusivity in different channel types. This is also a consequence of the stronger  
 487 fluid-substrate interaction for CO<sub>2</sub> which lies closer to the pore surface and is  
 488 therefore impacted by the pore shape to a greater extent. For the same reason, the  
 489 rotational motion of CO<sub>2</sub> is faster in the zigzag channels (Figure 10, right panel) as  
 490 the tortuous shape of these channels facilitate the rotational motion as mentioned in  
 491 the previous section. The tortuous shape of the zigzag channels also enhances the  
 492 energy of the intermolecular vibrations (Figure 11).

493



494

495 **Figure 14.** Overall and direction-specific self-diffusion coefficients corresponding to translational  
 496 motion of CO<sub>2</sub> (left) and ethane (right) in silicalite substrates characterized by 'half-volume'  
 497 (yellow highlighted region in Table 1). The left-most data points in both panels represent the  
 498 highest number of tortuous channels while the right-most data points represent the case of  
 499 straight channels with no tortuosity.

500

501

502

503

### 4.3 Implications

504 The results presented here can have important implications for applications that use  
505 fluids under confinement. While connecting several pores can enhance the overall  
506 diffusivity of the confined fluids, a judicious selection of different pore shapes in the  
507 same material can give rise to interesting effects that can be beneficial. For example,  
508 silicalite with a set of straight channels in one direction and a set of channels with a  
509 tortuous shape in the perpendicular direction can be used to separate different  
510 attributes by using well oriented samples. Further, the slowing of translational  
511 diffusivity of CO<sub>2</sub> in the zigzag channels can be used in engineered oriented silicalite  
512 membranes that let CO<sub>2</sub> pass through it more efficiently in one direction compared  
513 to a perpendicular plane.

514 In addition to the effects of pore-connectivity and tortuosity, the use of two  
515 representative fluids – one apolar and other quadrupolar also helps understand the  
516 role of fluid properties in these effects. While CO<sub>2</sub> with stronger interactions with the  
517 host due to a quadrupolar moment is affected to a greater extent by pore tortuosity,  
518 ethane remains less affected due to a weaker interaction. This suggests an important  
519 difference between apolar and polar molecules that can be utilized in separation  
520 processes. In a mixture of polar and apolar fluid, the polar fluid can be expected to  
521 be affected to a greater extent by pore tortuosity thereby enhancing the difference in  
522 the mobility of these fluids. Such a mixture can therefore be separated by making  
523 oriented membranes with tortuous pores aligned along the flow direction.

524

## 525 **5.0 CONCLUSIONS**

526 By selectively blocking some pore spaces of silicalite via immobile methane  
527 molecules, molecular dynamics simulations of silicalite substrates are used to  
528 systematically study the effects of pore connectivity and pore tortuosity on the  
529 dynamics of two representative carbon-bearing fluids – CO<sub>2</sub> and ethane. While  
530 overall diffusivity of both molecules is enhanced as more pores are connected, the  
531 trends observed in the 1-dimensional diffusivity along the channel direction are



532 more nuanced. Rotational and intermolecular vibrational motions of both fluids are  
533 found to be impacted on connecting the pores to a relatively smaller extent  
534 compared to the translational motion. Pore tortuosity is found to facilitate the  
535 rotational motion of CO<sub>2</sub> and suppress its translational motion, while its effects on  
536 the motion of ethane are less pronounced. The intermolecular vibrations of both  
537 fluids are found to be more energetic in the tortuous zigzag channels. The results of  
538 this study can be used to design oriented silicalite membranes that are more efficient  
539 in permitting CO<sub>2</sub> molecules to pass in one direction compared to a perpendicular  
540 direction. Further membranes with tortuous pores aligned along the direction of  
541 flow can be used to separate a mixture of polar and apolar fluids based on the  
542 difference in their mobilities.

543

## 544 **6.0 AUTHOR CONTRIBUTIONS**

545 S. G. Conceptualized the study, carried out the simulations, analyzed and  
546 interpreted the simulation data, and wrote the original draft. D.C. secured the  
547 funding. Both authors reviewed and revised the initial manuscript draft

548

## 549 **7.0 ACKNOWLEDGEMENT**

550 This research was funded by the U.S. Department of Basic Energy, Office of Science,  
551 Office of Basic Energy Sciences, Division of Chemical Sciences, Geosciences and  
552 Biosciences, Geosciences Program, grant number DESC0006878. We would like to  
553 acknowledge STFC's Daresbury Laboratory for providing the package DL-Poly,  
554 which was used in this work. Simulations reported in this work were carried out at  
555 the College of Arts and Sciences (ASC) Unity Cluster of the Ohio State University.  
556 The computational resources and support provided is gratefully acknowledged  
557 (Sandy Shew, Brent Curtiss, Keith Stewart and John Heimaster). Figures in this

558 manuscript were made using the freely available plotting software Gnuplot [36]  
559 (Figures 2–14).

560

## 561 **8.0 CONFLICT OF INTEREST STATEMENT**

562 The authors declare that there is no conflict of interest.

563

## 564 **9.0 DATA AVAILABILITY**

565 All data related to this study are available in this article.

566

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