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Non-Equilibrium Interaction Between Catalytic Colloids: Boundary Conditions and Penetration Depth[†]

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Spherical colloids that catalyze the interconversion reaction $A \leftrightharpoons B$ between solute molecules A and B whose concentration at infinity is maintained away from equilibrium effectively interact due to the non-uniform fields of solute concentrations. We show that this long range 1/r interaction is suppressed via a mechanism that is superficially reminiscent but qualitatively very different from electrostatic screening: catalytic activity drives the concentrations of solute molecules towards their equilibrium values and reduces the chemical imbalance that drives the interaction between the colloids. The imposed non-equilibrium boundary conditions give rise to a variety of geometry-dependent scenarios; while long-range interactions are suppressed (except for a finite penetration depth) in the bulk of the colloid solution in 3D, they can persist in quasi-2D geometry in which the colloids but not the solutes are confined to a surface, resulting in the formation of clusters or Wigner crystals, depending on the sign of the interaction between colloids.

1 Introduction

To build a macroscopic machine capable of directly utilizing chemical energy to perform mechanical work, bypassing heat, is a long standing and unresolved engineering challenge. At the same time, on the macromolecular or colloidal scale, this is routinely done by molecular motors moving on a solid substrate 1 or by colloidal swimmers moving through a fluid². In the latter case, mechanical motion is usually achieved by diffusiophoresis, i.e., the drift of a colloidal particle (or a liquid droplet) in a solvent, induced by gradients in the concentration of chemical species (solute)^{3–6}. The phenomenon is driven by short-range interactions between the surface of the particle and the solute molecules which result in different energies of a solute molecule close to the surface of the particle and away from it and, depending on the sign of the interaction, it leads to the motion of the particle along or opposite to the direction of the concentration gradient. Recently, diffusiophoresis has been proposed as a non-equilibrium, non-motor protein mechanism for metabolism-dependent transport of protein filaments, plasmids, storage granules, and foreign particles of different sizes in cells ^{7,8}. Related cross-diffusion and chemotaxis effects 9 have been also implicated in the aggregation of enzymes and the formation of metabolons in regions of high substrate concentrations ¹⁰. Under the name "chemically

One simple way to create solute concentration gradients is to have colloidal particles catalyzing the reaction $A \leftrightharpoons B$ between substrate A and product B molecules, provided that substrates are supplied to the system, while products are washed away. An interesting observation about such a system is that concentration gradients typically decay as 1/r with distance, thus leading to effective interactions which are long-ranged and reminiscent of electrostatics or gravity 13,20,21 . This realization leads to prediction of a plethora of beautiful and unusual states of this "phoretically active matter" 13 .

We here want to revisit that same system in order to clarify one aspect of it, which is the following. Whenever there is a catalyst that accelerates chemical transformation of A ("fuel") to B ("exhaust") molecules, $A \rightarrow B$, it accelerates also the reverse reaction, $A \leftarrow B$; in other words, it accelerates relaxation to equilibrium. This fact has interesting consequences for the analog of Debye-Hückel electrostatic screening in systems of catalytic colloids. Specifically, in electrostatics, the field that is being screened is, of course, the electric field, or potential. What is screened in our chemical system? We shall show that it is the field of chemical imbalance that measures the deviation from chemical equilibrium, $\psi(\mathbf{r}) \equiv k_{\rightarrow} c_A(\mathbf{r}) - k_{\leftarrow} c_B(\mathbf{r})$, where $c_A(\mathbf{r})$ and $c_B(\mathbf{r})$ are local concentrations of solute components, while k_{\rightarrow} and k_{\leftarrow} are corresponding catalytic rate constants. For instance, in a canonical example,

⁽or phoretically) active matter" these systems attracted much attention from theorists in recent years. A far reaching phenomenological theory was developed by Ramin Golestanian with co-authors ^{11–18} and in a number of other works ^{19–21} (reviewed in ¹⁷).

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when there is a large crowd of catalytic particles confined in an osmotic bag permeable for fuel A and exhaust B molecules, but not permeable for catalytic particles, and even if chemical imbalance is maintained outside by supplying A and removing B, the chemical imbalance field $\psi(\mathbf{r})$ penetrates into the crowd only by a finite distance and decays exponentially beyond that distance. Deep inside the crowd of catalysts both A and B are present, but in chemical equilibrium. This main point of our work has some important consequences which we will discuss at the end.

The plan of this article is as follows. To make the work self-contained and to establish the notations, we rederive some of the well-known results ¹³ about concentration profiles around single catalyst and about interactions between two catalysts in section 2. This section contains no new results and serves mostly pedagogical purposes, except that unlike previous authors, we never omit the fundamentally important reverse catalytic reaction. The crowd of catalysts, screening ²², Wigner crystals ²³, and clusters of catalytic colloids, are considered in section 3.

2 The 1/r interaction between catalytic colloids

Let c_A^∞ and c_B^∞ be the respective concentrations (molecules per unit volume) far away from the catalysts. We will assume that the energy barrier for the interconversion reaction $A \leftrightharpoons B$ is sufficiently high so that, in the absence of catalysts, the system can be maintained indefinitely out of equilibrium and therefore c_A^∞ and c_B^∞ are externally controlled parameters.

Consider first a single spherical particle of radius R which can catalyze the reaction A = B on its surface by reducing the energy barrier to a value comparable to k_BT . Assuming for simplicity that concentrations are sufficiently small, the steady state rate (current) of catalytic reaction can be written as

$$J = vk_{\rightarrow}c_A(R) - vk_{\leftarrow}c_B(R) , \qquad (1)$$

with k_{\rightarrow} and k_{\leftarrow} forward and backward rate constants, $c_A(R)$ and $c_B(R)$ the concentrations of A and B species at the surface of the catalyst, and v the volume where reaction takes place (for instance, if catalysis occurs uniformly along the spherical surface, then $v = 4\pi R^2 d$, with d a molecular length scale). As we stated, Eq. (1) is valid only for sufficiently small concentrations of A and B, otherwise the catalyst gets "clogged" and a non-linear Michaelis-Menten reaction rate has to be used, as it was done in 13. However, for our purpose, it is important to have both forward and backward reaction taken into consideration, which at large concentrations would require using the so-called reversible Michaelis-Menten kinetics ^{24,25} which was not done in ¹³. Because of the dramatic simplification, we stay with the linear relation (1). Since solute particles A and B have to be delivered to and from the catalyst surface by diffusion, their steady state concentration profiles must be found from the appropriate diffusion equation. For a spherically symmetric catalyst, the concentration fields of all solutes *A* and *B* are spherically symmetric as well:

$$c_A(r) = c_A^{\infty} - \frac{J}{4\pi D_A r} \; ; \; c_B(r) = c_B^{\infty} + \frac{J}{4\pi D_B r} \; ,$$
 (2)

where D_A and D_B are the corresponding diffusion coefficients. Plugging these expressions (at r = R) back to Eq. (1) which serves as a boundary condition for the diffusion equation, produces an equation for the current J with the solution

$$\frac{J}{v} = \frac{k_{\to} c_A^{\infty} - k_{\leftarrow} c_B^{\infty}}{1 + \frac{v}{4\pi R} \left[\frac{k_{\to}}{D_A} + \frac{k_{\leftarrow}}{D_B} \right]} . \tag{3}$$

This result is easily generalized for the case when several species of A_i and B_j are present.

Current J (3) vanishes in thermal equilibrium, since the equilibrium concentrations $c_A^{\rm eq}$ and $c_B^{\rm eq}$ obey the detailed balance condition, $k_\to c_A^{\rm eq} = k_\leftarrow c_B^{\rm eq}$. In this sense, the quantity in the numerator of formula (3) characterizes the degree of chemical imbalance which drives the process, and which can be governed by energy (if energy of a fuel molecule is larger than that of exhaust), or by entropy (if $c_A^\infty > c_B^\infty$), or by any combination of the two.

We now consider two catalytic spheres, some distance r apart, such that $r \gg R$; the catalyst spherical symmetry assumption will be relaxed later on. Because of the short-range interactions between solute molecules A and B and the catalyst, and because steady state concentrations of A and B are non-uniform in space, the energies of these two spheres depend on the distance r between them, i.e., there is an interaction force between them. This problem can be treated, in the first approximation (see Supplemental Material ²⁶), by imagining one particle located in the origin, while the other particle, positioned at distance r away, interacts with unperturbed concentration fields $c_A(r)$, $c_B(r)$ Eq. (2) created by the first. Expanding the surface energy of a sphere in small concentrations c_A and c_B at the sphere surface, as $\sigma \simeq \sigma_0 + c_A(r)\sigma_A' + c_B(r)\sigma_B'$ (where prime signs indicate partial derivatives of surface tension with respect to the corresponding concentration), we write distance-dependent part of energy for two spheres as follows:

$$\frac{E}{4\pi R^2} = \sigma_A' \left[c_A(r) - c_A^{\infty} \right] + \sigma_B' \left[c_B(r) - c_B^{\infty} \right] . \tag{4}$$

For brevity, we again drop the generalization for the case of several species A_i and B_j . The constant (r-independent) c_A^{∞} and c_B^{∞} terms are subtracted such that this energy vanishes when two droplets are infinitely far. Plugging in the concentration profiles Eq. (2), the force on each sphere is

$$\frac{f}{4\pi R^2} = \frac{J}{4\pi r^2} \left[\frac{\sigma_B'}{D_B} - \frac{\sigma_A'}{D_A} \right] . \tag{5}$$

where the current J is given by Eq. (3) (we have neglected the hydrodynamic interaction contribution to the force, $f = -\nabla E$; see ¹⁸). This force depends on the distance as $1/r^2$ i.e., it is a longrange interaction similar to gravitational and Coulomb forces, as it was pointed out in ^{11–13},16,20,21. Furthermore, the force is proportional to J – the chemical rate (or current) of interconversion of A to B, which emphasizes that the entire phenomenon is of nonequilibrium nature. It is driven by the supply of fuel A molecules as well as removal of exhaust B molecules at infinity.

A word of caution is in order about our usage of equilibrium surface tension σ and its derivatives σ'_A and σ'_B in this decidedly

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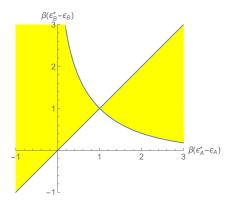


Fig. 1 Diagram of regimes for two catalytic spheres in terms of energies $\tilde{\epsilon}_A$ and $\tilde{\epsilon}_B$, according to Eq. 6c. Yellow marks the region where interaction force is repulsive, in other areas it is attractive. The plot is constructed for $D_A = D_B$; the only modification required in the case $D_A \neq D_B$ is change of scales along axes.

non-equilibrium context. In fact, it is well justified by the assumption that colloidal catalytic particles are much larger and move much slower than the solute molecules *A* and *B*.

The interaction force (5) between catalytic colloids can be either attractive or repulsive. To see this, consider the following simple model. Imagine that catalysis takes place in a narrow layer of thickness d around the catalyst surface, then

$$k_{\rightarrow} = \frac{1}{\tau} e^{\beta \left(\varepsilon_{A} - \varepsilon^{\dagger} \right)} \quad k_{\leftarrow} = \frac{1}{\tau} e^{\beta \left(\varepsilon_{B} - \varepsilon^{\dagger} \right)} ,$$
 (6a)

where $1/\tau$ is the attempt rate, $\beta=1/k_BT$, while ε_A and ε_B are the bulk free energies of A and B, and ε^\dagger is the free energy of the transition state of the catalytic surface reaction (for reasons of brevity, we will refer to these free energies as energies in the following). Furthermore, if energies of A and B molecules inside surface layer of a colloid are ε_A^* and ε_B^* , different from their bulk values ε_A and ε_B , then $\sigma_A' = d\tilde{\varepsilon}_A e^{-\beta\tilde{\varepsilon}_A}$ and $\sigma_B' = d\tilde{\varepsilon}_B e^{-\beta\tilde{\varepsilon}_B}$, with $\tilde{\varepsilon}_A = \varepsilon_A^* - \varepsilon_A$ and $\tilde{\varepsilon}_B = \varepsilon_B^* - \varepsilon_B$. In this approximation,

$$\frac{J}{4\pi R^2 d} = \frac{c_A^{\infty} e^{\beta \varepsilon_A} - c_B^{\infty} e^{\beta \varepsilon_B}}{\frac{Rd}{D_A} e^{\beta \varepsilon_A} + e^{\beta \varepsilon^{\dagger}} \tau + \frac{Rd}{D_a} e^{\beta \varepsilon_B}}$$
(6b)

$$\frac{f}{4\pi R^2} = \frac{Jd}{4\pi r^2} \left[\frac{\tilde{\varepsilon}_B}{D_B} e^{-\beta \tilde{\varepsilon}_B} - \frac{\tilde{\varepsilon}_A}{D_A} e^{-\beta \tilde{\varepsilon}_A} \right] . \tag{6c}$$

Inspection of Eq. (6c) confirms that the force between catalysts can be attractive or repulsive, depending on the energies ε_A , ε_B , ε_A^* and ε_B^* , as shown in the Fig. 1 (see also ¹⁹). For instance, if both A and B molecules are attracted to the surfaces of catalytic particles, $\varepsilon_A^* < \varepsilon_A$ and $\varepsilon_B^* < \varepsilon_B$, then the resulting long range interaction between catalysts is a competition: interaction with A pushes each sphere away from the other, towards greater supply of A, but interaction with B pulls catalysts towards one another, towards where new B is produced. Therefore, overall attraction between spheres occurs if $\varepsilon_B^* - \varepsilon_B < \varepsilon_A^* - \varepsilon_A$, and overall repulsion takes place in the opposite case.

In equations (6), we expressed phenomenological quantities σ'_A and σ'_B , as well as rate constants k_{\rightarrow} and k_{\leftarrow} in terms of energies such as ε^*_B , ε_B , ε^*_A , ε_A ; these mechanical quantities are easy to

imagine for a theorist, but virtually impossible to measure. Furthermore, we consider only the force acting on catalytic colloidal particles, which is, in principle, measurable in an optical tweezers experiment, but we do not consider their motion under this force. Translating force into velocity requires the knowledge of mobility, and simple minded assumption of Stokes friction is known to be only qualitatively and not quantitatively right. More systematic phenomenological treatments ^{11,12} operate with directly measurable surface tensions, Onsager coefficients, and other phenomenological parameters. We present the somewhat more naive approach based on equations (6) only because of its simplicity and pedagogical value.

Our consideration so far was restricted to spherically symmetric catalytic particles. This idealization is perhaps rarely realized. A catalytic particle without spherical symmetry creates non-isotropic concentration fields of reagents, which can result in auto-diffusiophoretic motion of the catalyst 4,19,27-37. Such selfdiffusiophoretic particles are of considerable current interest and considered an important example of the so-called active swimmers ^{34–36,38}. Speaking about concentration field mediated interactions between catalysts, we should think of multipole expansion of the concentration fields (see also ³⁷). Then, exactly as in the familiar electrostatics context, the dominant long range contribution is that from a monopole, $\sim 1/r^2$, which is what we considered above, while dipole (like for Janus particles), quadrupole, and higher order multipoles are important for the near field. Thus, we will continue working in the monopole approximation which is only justified when distance between catalysts is large. Accordingly, we do not consider self-diffusiophresis, simply because it was already studied in detail 11-13,16,19,27,28,35

3 A crowd of catalysts

We now turn from considering the force between two catalytic particles to the case when there are many catalysts. Since catalysts reduce free energy barriers, thus paving the way for the system to approach chemical equilibrium, in order to maintain the system away from equilibrium in the presence of a finite concentration of catalysts, it is necessary (though maybe not sufficient) to confine the catalysts to a region of space that is surrounded by a "bath" in which non-equilibrium concentrations of *A* and *B* molecules are enforced and maintained from outside. Our goal now is to explore implications of such boundary conditions.

Consider a crowd of catalytic particles, with density of $\rho(\mathbf{r})$ catalysts per unit volume. On the mean field level, overall behavior should be described by the volume fraction of catalytic centers in space, $\phi(\mathbf{r}) = v\rho(\mathbf{r})$, where v (exactly as before) is the volume of the region in which catalysis takes place on the surface of one catalytic particle. Now, let $c_A(\mathbf{r})$ and $c_B(\mathbf{r})$ be the concentration fields of "fuel" and "exhaust" molecules A and B, coarse grained over distances large compared to the typical distance between catalysts, ℓ ($\ell^{-3} \sim \rho$). Then mean field equations for concentrations of A and B read

$$\dot{c}_{A}(\mathbf{r}) = D_{A} \nabla^{2} c_{A}(\mathbf{r}) - \phi(\mathbf{r}) \left[k_{\rightarrow} c_{A}(\mathbf{r}) - k_{\leftarrow} c_{B}(\mathbf{r}) \right]$$

$$\dot{c}_{B}(\mathbf{r}) = D_{B} \nabla^{2} c_{B}(\mathbf{r}) + \phi(\mathbf{r}) \left[k_{\rightarrow} c_{A}(\mathbf{r}) - k_{\leftarrow} c_{B}(\mathbf{r}) \right]$$
(7)

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To analyze these equations, we introduce the "field of chemical imbalance"

$$\psi(\mathbf{r}) \equiv k_{\rightarrow} c_A(\mathbf{r}) - k_{\leftarrow} c_B(\mathbf{r})$$
 (8)

The meaning of $\psi(\mathbf{r})$ field (8) is clarified by noticing that, up to a constant factor $1/\nu$, $\psi(\mathbf{r})$ is equal to $J(\mathbf{r})$ – the rate of chemical reaction (1) in the vicinity of point \mathbf{r} , coarse grained over the scale ℓ in the same way as concentrations and ψ . Therefore, according to Eq. (5), it also follows that $\psi(\mathbf{r})$ determines the strength of interactions between catalytic colloids around \mathbf{r} .

In steady state, time derivatives vanish and, combining Eqs. (7) with proper weights, we find that $\psi(\mathbf{r})$ satisfies

$$\nabla^2 \psi(\mathbf{r}) - \xi^{-2}(\mathbf{r})\psi(\mathbf{r}) = 0 , \qquad (9)$$

where

$$\xi^{-2}(\mathbf{r}) = \left[\frac{k_{\rightarrow}}{D_A} + \frac{k_{\leftarrow}}{D_B}\right] \phi(\mathbf{r}) . \tag{10}$$

At first glance, Eq. (9) is identical to the celebrated Debye-Hückel equation 22 for the electrostatic potential around a point charge in an ionic solution, implying that $\xi(\mathbf{r})$ can be interpreted as the screening length (see equation (8) in reference 13). Upon further inspection one notices significant differences. First and foremost, electrostatic potential is defined up to an additive constant, while field of chemical imbalance does not have this gauge freedom, because $\psi = 0$ is the special state of chemical equilibrium. Because of that, the boundary conditions on our chemical imbalance field $\psi(\mathbf{r})$ are quite different from those on the potential in a typical electrostatics problem: while the electric potential diverges at the point charge and decays to a constant, usually identified as zero, at large distance from it, ψ is maintained at some fixed non-equilibrium value away from the catalysts where $\phi(\mathbf{r}) = 0$. Depending on the geometry, ψ vanishes or reaches some lower value inside the colloid-occupied region ($\phi(\mathbf{r}) \neq 0$) because catalysis always tends to reduce the degree of chemical imbalance and drive the system towards equilibrium at which detailed balance is obeyed and $\psi(r) = 0$. This effect has not been noticed in previous works, in which the reverse reaction (the second term in Eq. (8)) that drives the system to equilibrium, was omitted.

In order to understand the physical meaning of the length ξ let us consider the 3D situation shown in Fig. 2: catalytic colloids are confined inside a spherical osmotic bag of radius L which is permeable to solute molecules A and B but not to the colloids. Substrate molecules A are delivered by diffusion from infinity, and product molecules B are also absorbed at infinity such that their concentrations at infinity are fixed at some non-equilibrium values c_A^∞ and c_B^∞ , respectively (note that since chemical reactions take place only inside the bag, these bulk concentrations can be arbitrarily far from equilibrium). As shown in Fig. 2, the chemical imbalance field $\psi(x)$ penetrates up to a penetration depth ξ into the catalysts-occupied domain. Deeper into the bulk of the catalysts-occupied region $\psi(x) \to 0$, the concentrations of A and B approach equilibrium values. More specifically, assuming the concentrations to be c_A^∞ and c_B^∞ at infinity, concentration profiles

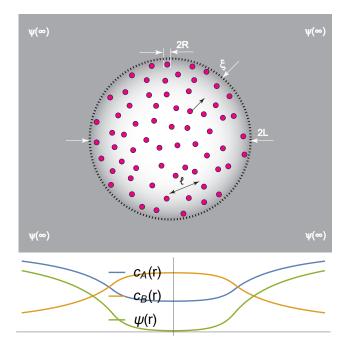


Fig. 2 Catalytic particles, of diameter 2R each, are distributed in an osmotic bag of diameter 2L (shown by thick dashed circle), while substrate molecules A diffuse from outside, and product molecules B diffuse out to infinity. The chemical imbalance function $k_{\rightarrow}c_A(r)-k_{\leftarrow}c_B(r)=\psi(r)$ is shown in shades of gray. Deep in the crowd of catalysts, there is no chemical imbalance between A and B, $\psi(x) \rightarrow 0$. For plotting, we assumed $c_B^{\infty}=0$, $\xi=L/5$, $\frac{k_{\leftarrow}}{k_{\rightarrow}}=\frac{1}{2}$ and $\frac{D_B}{D_A}=1$.

are expressed in terms of chemical imbalance function $\psi(r)$

$$c_A(r) = c_A^{\infty} + \frac{\psi(r) - \psi(\infty)}{D_A \left(\frac{k_{\rightarrow}}{D_A} + \frac{k_{\leftarrow}}{D_B}\right)}$$
(11a)

$$c_B(r) = c_B^{\infty} - \frac{\psi(r) - \psi(\infty)}{D_B \left(\frac{k_{\rightarrow}}{D_A} + \frac{k_{\leftarrow}}{D_B}\right)} , \qquad (11b)$$

while $\psi(r)$ itself is found for this spherical geometry, based on the Eq. (9), along with boundary conditions of continuous function and its derivative and no singularity at the origin:

$$\frac{\psi(r)}{\psi(\infty)} = \begin{cases} 1 - \frac{L}{r} + \frac{\xi}{r} \tanh \frac{L}{\xi} & \text{at} \quad r > L \\ \frac{\xi}{r} \frac{\sinh r/\xi}{\cosh L/\xi} & \text{at} \quad r < L \end{cases}$$
 (11c)

These results are plotted, for specific values of parameters, in Fig. 2. As expected, the current J vanishes inside the crowd of catalysts along with ψ , and the forces between colloids vanish as well. These forces (attractive or repulsive) will be significant only inside the boundary layer of thickness ξ . If the size of the osmotic bag L is smaller or comparable to the penetration depth ξ , depending on the sign of the force in Eq. (6c), catalysts will attract one another and form an aggregate (which could be smaller than the available volume of the osmotic bag) or repel each other and form a Wigner crystal 23 (occupying the whole accessible volume)

A more subtle and experimentally relevant case is a quasi-2D system, where the container has a finite depth H, while catalytic

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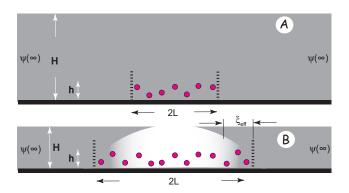


Fig. 3 Catalytic colloids are located within a gravitational height h from the bottom of the container of depth H. As before, the chemical imbalance field is approximately shown by shades of gray. Barriers or osmotic bag are shown by thick dashed lines. In case of a deep container (figure A), diffusion in 3D is sufficient to supply fuel and remove exhaust for all colloids, and chemical imbalance field ψ penetrates to all colloids. In case of a shallow container (figure B), the middle part of the "pancake" of colloids is not accessible to chemical imbalance field.

colloids are confined due to gravity within a short distance h, sometimes called gravitational height, from the bottom (or from the top if they float) of a container, as shown in a cartoon, Fig. 3. Boundary conditions, in addition to fixed value of $\psi(\infty)$ at $r \to \infty$, require zero normal (vertical) flux of either A or B particles, thus vanishing normal derivative of ψ on both top and bottom surfaces (we note in passing that this does not have simple electrostatic analogy). The situation, as it turns out, depends sensitively on the relations between several relevant length scales.

If the depth of the container is infinite or very large, as in Fig. 3A, then although colloidal spheres are confined in 2D by barriers or osmotic bag to the interior of a circle of radius L, the fuel A and exhaust B molecules are diffusing in 3D. Formally, in this case, equation (9) gets reduced simply to $\nabla^2 \psi = 0$ everywhere except a very thin pancake-shaped region of thickness h and radius L, and finite penetration depth ξ (10) exists only inside the pancake. If h is very small and $\xi \gg h$, then delivery of A and removal of B by diffusion in 3D is unhindered and reaches every point of the pancake from the top. Therefore, the force of interaction between catalytic colloids still obeys the $1/r^2$ law everywhere inside the pancake, unlike the 3D case where colloids in the bulk of the confined region essentially do not interact. In the attractive case, we expect catalysts in 2D to form a large aggregate whose growth may be stopped only when its diameter becomes comparable to H. For repulsive forces we expect formation of a 2D Wigner crystal whose size is not limited by ξ and is controlled by the confining boundaries or an osmotic bag only.

Consider now the opposite limit of a shallow container, as in Fig. 3B. Clearly, on horizontal length scales larger than H the problem becomes essentially two dimensional. Averaging Eq. (9) along the vertical direction, we obtain 2D equation of the same form, except with effective penetration depth given by $\xi_{\rm eff}^{-2} = \xi^{-2}h/H$. The solution of the corresponding 2D problem is qualitatively similar to Eqs. (11), which means that the field of chemical imbalance penetrates into the pancake of catalysts only to horizontal distance about $\xi_{\rm eff} = \xi \, (H/h)^{1/2}$. Closer to the mid-

dle of the pancake the local imbalance field is reduced by catalysis and long-range interactions between colloids are suppressed. In this case we expect attractive catalysts to assemble in 2D aggregates of size no larger than $\sim \xi_{\rm eff}$. Repulsive catalysts will form 2D Wigner crystals only for $L \leq \xi_{\rm eff}$.

This conclusion is reminiscent of the fact that "live" colloids in the experiments by Pallaci et al ³⁴, by Buttioni et al ³⁵, and by Theurkauff et al ³⁸ formed 2D aggregates of limited size that did not grow further. These colloids were not spherically-symmetric and exhibited self-diffusiophoretic swimming. Moreover, they were shown ³⁴ to form the so-called "living crystals", a finding which was interpreted as an experimental confirmation of the theoretically predicted activity-driven condensation ^{39–48}. We speculate that the limited size of the aggregates could be due to screening (screening does not require catalysts to be spherically symmetric and is expected to take place even for self-diffusiophoretically driven swimmers).

4 Conclusion

To summarize, we have presented a very simple schematic theory demonstrating that spherical colloids capable of catalyzing a reversible chemical reaction between solutes, experience a peculiar interaction which exists only as long as the concentrations of the solutes are maintained out of equilibrium by constant supply of high free energy "fuel" and removal of "exhaust" molecules at the boundaries of the colloid solution. The long range (1/r) interaction between colloids is driven by the chemical imbalance field that measures the deviation from chemical equilibrium. We have shown that, despite the apparent similarity of the underlying equations, the origin of this effect is very different from the Debve-Huckel electrolyte polarization mechanism in electrostatics: catalytic activity drives the concentrations of solute molecules towards their equilibrium values and therefore reduces the chemical imbalance that controls the strength of the diffusiophoretic interaction between the colloids.

We demonstrated that the combination of boundary conditions and finite penetration depth has a profound effect on the interaction between catalytic colloids. Thus, in a realistic 3D geometry of a colloid solution enclosed in an osmotic bag (permeable to solute molecules but not to colloids) and surrounded by a "bath" that fixes the concentrations of solutes at some arbitrary values, non-equilibrium concentrations of solutes can be maintained in steady state only within a penetration depth (screening length) from the boundary, and therefore interactions between colloids vanish in the bulk of the colloid solution. The effects of finite penetration depth can be overcome in quasi-2D geometry (with colloids confined to a surface and solute molecules free to move in 3D) where unscreened 1/r attractions between colloids can lead to macroscopic aggregates or to Wigner crystals, depending on the sign of the diffusiophoretic interaction between colloids. In the attractive case, we predict that finite 2D clusters of colloids will form if the depth of the 3D container is finite and that the diameter of these clusters will be proportional to the effective correlation length that increases as the square root of the depth H. In the repulsive case one expects Wigner crystals to form if the separtion between the barriers that confine the colloids in 2D is smaller than the effective penetration length. These theoretical predictions await experimental verification.

Conflicts of interest

There are no conflicts to declare.

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