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1	Synthesis of bentonite clay based hydroxyapatite nanocomposite cross-linked by
2	glutaraldehyde and optimization by response surface methodology for lead removal
3	from aqueous solution
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30 Abstract

A novel nanocomposite (BT-HAp) was developed by chemical synthesis of 31 32 hydroxyapatite nanoparticles and bentonite clay that further applied for toxic lead (Pb) 33 removal from aqueous solution. Three types of bentonite clay based nanocomposite were 34 prepared by varying the pH of the solution (3, 7 and 10) and addition of glutaraldehyde as 35 a cross-linking agent. The formation and performance of the prepared BT-HAps were 36 examined herein. A clear and sharp XRD peaks suggested the presence of hydroxyapatite 37 and bentonite clay compound in composite. FTIR spectrum confirmed the existence of 38 functional groups required to develop the nanocomposite. The Bt-HAp nanocomposites 39 were also characterized in terms of the BET, FESEM and TEM etc. to establish its 40 formation. The synthesized nanocomposite showed highest sorption capacity at pH 7 than 41 3 and 10. A mathematical and statistical optimizing technique (response surface 42 methodology) was applied to verify the interactive effects of various parameters on 43 sorption capacity. The analysis of variance was discussed for factors and response, that confirmed the significance of the predicted model ($R^2 = 0.9906$). Langmuir isotherm 44 model best represented the phenomenon having sorption capacity of 346 mg g^{-1} at 30° C. 45 The sorption mechanism was well described by the Pseudo 2^{nd} order kinetic model 46 47 indicating coexistence of both physisorption and chemisorption. Moreover, a 48 considerable amount of toxic Pb (~99 %) removal was observed by the synthesized 49 nanocomposite via sorption.

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Key Words: Synthesis, Nanocomposite, lead removal, optimization.

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60 **1. Introduction**

61 Application of nanoparticles for contaminated water treatment has gained remarkable 62 interest to the scientific community in recent time. The metal oxide nanoparticles like Al_2O_3 , MnO₂, MgO and TiO₂ were used for heavy metal removal from aqueous system.¹ 63 64 Similarly, silver nanoparticles also gained considerable attention for their antimicrobial activity.² Simeonidis et al. (2015) found that Fe magnetite nanoparticles (20 nm) were 65 able to remove toxic chromium from drinking water.³ The removal capacity of Cr by 66 magnetic nanoparticle was 1.8 μ g Cr (VI) mg⁻¹ for a residual concentration of 50 μ g l⁻¹ at 67 a neutral pH.³ However, these nanoparticles have some disadvantages in terms of 68 separation period and reusability of nanoparticles from treated water.⁴⁻⁷ Therefore, it is 69 70 utmost important to overcome these drawbacks to produce fresh water. The composite 71 material has gained considerable research attention in recent years for toxic contaminants 72 removal from aqueous system. These materials are easily separable from filtered water 73 due to their comparatively large size. Nanocomposite consist two or more component 74 having at least one in nano dimension with different chemical and physical properties 75 than individual. However, development of nanocomposite in combination with 76 nanoparticles (NPs) having superior property e.g. large surface area, surface reactivity and high mechanical stimuli can be a possible solution. 8,9 77

A significant threat occurs to the environment and public health due to the discharge of heavy metals especially Pb from printing, textile industries or other sources to the water body.¹⁰ It can cause structural damage in the mammalian eye, central nervous system and blood cells.¹¹ Adsorption is widely used method for heavy metal remediation due to its simple and economic operation process compared to other conventional methods. In this context, the Pb adsorption by nanocomposite could be a feasible way to remediate toxic elements from aqueous solution.¹²⁻¹⁷

Natural and synthetic nanomaterials incorporated into other functional groups for getting the desired nanocomposite with significant performance has gained attention nowadays. Several clay based nanocomposites mixed with nanoparticles are reported for the removal of water contaminants. Chao et al. (2015) reported that the adsorption characteristics are strongly influenced by bentonite clay and metal oxide nanocomposite.¹⁸ A new nanocomposite was developed by acid activated clay to study the adsorption feasibility of

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91 crystal violet dye.¹⁹ Bentonite clay composite materials are now widely applied due to 92 improved sorption time, efficiency and life cycles in water purification system including 93 heavy metal adsorption, rather than insitu application.^{19, 20-23} Bentonite clay based 94 hydroxyapatite nanocomposite has not been reported till now. Although Cynthia et al. 95 (2014) suggested that hydroxyapatite may be an alternative approach for removal of toxic 96 contaminants.²⁴ Very recently, the synthesized hydroxyapatite have been combined with 97 metal oxide nanoparticles for potential applications in water purification.²⁵⁻²⁷

It is well known that bentonite is a natural, low cost clay mineral and largely available 98 99 material. Therefore, in this study a new nanocomposite was developed combining 100 bentonite with hydroxyapatite nanomaterial (BT-HAp). Inclusions of ceramic material 101 such as bentonite clay improve the sorption capacity as well as the mechanical properties 102 of hydroxyapatite. Glutaraldehyde is used as a cross-linking agent to adhere the 103 components in composite. Additionally, it has disinfectant property with low toxicity and also enhances the mechanical property of the nanocomposite.²⁸ Reports are not available 104 105 to the best of our knowledge regarding bentonite clay based hyroxyapatite nanocomposite 106 synthesis and its application as a sorbent for Pb removal from synthetic water.

Additionaly, effect of different independent variables on Pb sorption capacity has been
optimized in this study. Central Composite Design (CCD) is considered to design the
experimental data in Response surface methodology (RSM) optimization method.
Moreover, the relationship of the response and the independent variable as pH, initial Pb
concentration, dosage is established by statistical analysis.

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113 **2. Experimental**

114 **2.1. Materials**

115 Calcium nitrate tetrahydrate (Ca $(NO_3)_2.4H_2O$) (99%); diammonium hydrogen phosphate 116 ((NH₄)₂HPO₄), (99%); ammonia (NH₃.H₂O); glutaraldehyde; lead nitrate (Pb(NO₃)₂) 117 (99%); from Merck, Germany were used. Bentonite clay was obtained from CSIR-118 CGCRI, Kolkata, used without further purification.

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120 **2.2. Synthesis of hydroxyapatite NPs**

121 The HAp nanoparticle synthesis was conducted by chemical precipitation method with some modification.²⁹ In brief, according to Ca/P ratio of 1.6:1, the Ca $(NO_3)_2$ and 122 123 $(NH_4)_2$ HPO₄ was dissolved in 100 ml Mili-Q water separately. The aqueous NH₃ was 124 used to maintain the pH of the solutions at 10. The solution of Ca (NO₃)₂ was added 125 dropwise into (NH₄)₂HPO₄ solution in rapid stirring (250 rpm) condition. Gelatin was 126 added later as an adhesion material during the precipitation. The greenish precipitate was 127 repeatedly washed to remove the impurities like ammonia and its by-products. 128 Subsequently, the green compact was washed with Mili-Q water for several times. The 129 solid product was oven dried at 50 °C for overnight and sintered at 1200 °C for 2 hrs. 130 Finally, the calcined HAp was powdered for advance applications.

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132 **2.3. Preparation of BT-HAp nanocomposite**

133 The equal ratio (1:1) of bentonite clay and synthesized hydroxyapatite NP was 134 maintained for nanocomposite preparation. Both of the solutions (50 ml) were stirred 135 (250 rpm) in a 250 ml beaker separately for 12 hrs. Hydroxyapaptite solution was then 136 poured into the bentonite clay solution in continuous stirring condition. Glutaraldehyde 137 (6ml to 100ml) was added drop wise to the solution mixture as a crosslinker. Three sets 138 of experiments were conducted at different pH range such as 3, 7 and 10. The pH was 139 adjusted by using of 0.1 (N) HCl and 0.1 (N) NaOH solutions. Finally all the solutions 140 were stirred at 250 rpm for 12 hrs at room temperature. Washing-centrifugation 141 procedure was then followed to make the neutral supernatant. Finally, prepared BT-HAp 142 nanocomposite was dried at 60 °C for 2 hrs and powdered by mortar pestle. Fig. 1 shows 143 the schematic of the nanocomposite formation process with changes of morphology. The 144 prepared samples were stored in the air tight container for further uses.

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146 **2.4. Experimental design**

147 RSM is a well known optimization approach that simultaneously considers several 148 parameters at different design levels. Moreover, this mathematical and statistical 149 modeling tool is used to achieve the desired product with less number of experiments 150 without the requirement of observing all probable combinations experimentally.³⁰⁻³⁴ 151 Central composite design was undertaken to establish the relationship between the

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152 independent variables with the response of the Pb sorption capacity. Two-level three 153 factors (2^3) were employed with a series of experiments. Design Expert software was also 154 used to express the regression model and graphical analysis of the data. Coded level (-155 1,0,+1) of variables *viz.*, nanocomposite dosage 0.5-1.5 g L⁻¹ (A), initial Pb concentration 156 50-150 (B) mg L⁻¹ and initial solution pH 4.1-6.1(C) were designed by CCD to study the 157 effects on sorption capacity (Table 1).

The quadratic model was designed by CCD and the response variables were expressed as a function of process variables. In this method, a set of twenty experiments were conducted. The quadratic model for optimum value calculation is represented below

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162
$$Y = \beta_0 + \sum_{i=1}^k \beta_i x_i + \sum_{i=1}^k \beta_{ii} x_i^2 + \sum_{i=1}^k \sum_{j=i+1}^k \beta_{ij} x_i x_j$$
(1)

163

164 where, β_0 is constant, β_i , β_{ij} , β_{ij} are regression coefficients and x_i , x_j denotes the 165 independent variables. Predicted response is represented as Y.³⁵

166 In this study, the independent given variables were considered as pH, initial Pb 167 concentration and nanocomposite dosage, whereas sorption capacity was dependent 168 experimental response.

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170 **2.5. Material characterization**

171 The X-Ray Diffraction (XRD) analysis of the BT-HAp nanocomposite was performed by 172 Philips 1710 diffractometer using Cu as anode (Netherlands). The morphology of the 173 powdered sample was investigated using field emission scanning electron microscopy (FESEM, Gemini Zeiss SupraTM, 35 VP Model, Germany). Moreover the qualitative 174 175 energy dispersive X-ray spectroscopy (EDX, Leo S430I, U.K and Carl Zeiss, ΣIGMA-176 Germany) was used to detect the elements presents in samples. Various functional groups 177 were detected by Fourier transform infrared spectroscopy (FTIR, Perkin Elmer, USA). 178 The surface area was measured by adsorption-desorption of nitrogen using multipoint 179 Braunauer-Emmett-Teller (BET) method by using Quantachrome (USA). Transmission 180 electron micrograph (TEM, Technai G2 30ST-FEI, USA), particle size distribution of 181 synthesized materials (Zetasizer, Nanoseries, Malvern) were also used to understand the

nature of the synthesized powder. The solution pH was measured by pH meter
(EUTECH, India). After adsorption processes, Pb contaminated nanocomposite was also

- 184 characterized for any changes of functional groups or morphology.
- 185

186 **2.6. Lead adsorption experiments**

187 The adsorption study was carried out in batch mode. All solutions were prepared using 188 ultrapure water from Milipore-Q (USA) system. The synthetic solutions at different concentrations were prepared by diluting the standard Pb solution (1000 mg L⁻¹) obtained 189 190 by dissolving quantitatively $Pb(NO_3)_2$ in Mili-Q water at room temperature. The sample 191 of 10 ml volume was collected at different initial concentration with nanocomposite dose 192 of 1 g L⁻¹. Adsorption studies were performed in a batch reactor at 250 rpm by magnetic 193 stirrer for 24 h. The pH, nanocomposite dosage, initial Pb concentration variations were 194 conducted for efficient Pb sorption studies. In addition, the Pb sorption was carried out at 195 different temperature to observe its effect on removal efficiency. The concentration of Pb 196 was measured by ion chromatography (881 Compact IC pro, Metrohm). The repeatability 197 study was carried out for all experiments and the errors were found minimum. The sorption capacity q_e (mg g⁻¹) and removal efficiency (R) were calculated from the 198 199 following equations:

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201	$q_e = V(C_0)$	$(-C_e)/m$		2)	
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where, *V* is the volume of solution (L), $C_0 \& C_e$ are the initial and equilibrium Pb concentration (mg L⁻¹), m (g) is the mass of the nanocomposite as adsorbent.

(3)

207

208 **2.7. Desorption study**

 $R = (C_0 - C_a)/C_0 \times 100$

209 Desorption study was accomplished in batch mode with 0.1 M Ethylene diamine tetra 210 acetic acid (EDTA), NaOH and HNO₃. The other conditions remained unchanged and 211 about 0.01 g spent nanocomposite were taken for each solution. Desorption study was

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212 carried out at 250 rpm for 180 minutes at 30° C. Desorption efficiency was estimated 213 from the following standard equation: 214 215 % Desorption = $C_d / C_a \times 100$ (4) 216 where, C_d and C_a are the amount of metal ion desorbed and adsorbed in mg L⁻¹. 217 218 219 **3. Results and Discussion** 220 3.1. Characterization of nanocomposite 221 The XRD patterns of BT-HAp nanocomposite are shown in Fig. 2(a-c). The crystal phase 222 was obtained by XRD analysis clearly shows the increase in crystalinity for BT-HAp 223 nanocomposite at pH 7 (Fig. 2b) than BT-HAp at pH 3 and 10 (Fig. 1a and 1c). This 224 result demonstrated about high crystalline structure of BT-HAp-7. The sharp and major 225 peaks related to HAp were observed as 25.94, 29.02, 31.89, 32.28, 33.0, 34.15, 39.93, 49.6, 53.3 at 20 degree. The positions and d-values were well matched with JCPDS No. 226 09-0432.²⁶ However, the peaks at $2\theta = 5.3$, 24.5, 34.7, 63.2 confirmed the presence of 227 bentonite clay in composite. The similar findings were reported previously by T. S. 228 Anirudhan et al, 2006.³⁶ Therefore, the formation of nanocomposite by BT-HAp was 229 230 justified by XRD analysis. The crystallite size was estimated by Scherrer's equation from 231 XRD pattern, $D = \kappa \lambda / \beta \cos \theta$, where constant k is 0.9-1, λ is the X-ray wavelength, β is 232 the full width half maxima and θ is the Bragg's angle. The crystallite sizes of BT-HAp-3, 233 7, 10 were 28.6 nm, 36.7 nm and 45.9 nm, respectively. 234 In Fig. 3, FTIR spectra a, b and c denotes the synthesized nanocomposite BT-HAp-3, 7, 235 and 10. The functional groups of the composite material were present in above mentioned 236 three type of nanocomposite with variation of transmittance. The absorption bands at 3627-3630 cm⁻¹ were assigned to the hydroxyl group (-OH). The broad absorption bands 237 at 3434 and 1633 cm⁻¹ may be attributed to the –OH stretching and bending, respectively 238 239 for absorption of water molecules on clay and hydroxyapatite surface. Chemical cross-240 linker glutaraldehyde helped to attach the active groups (e.g. aldehyde) of HAp particle or clay mineral with each other.³⁷ Absorption bands at 1040-1044 cm⁻¹ signifies the 241

242 presence of Si-O-Si bond in BT-HAp. Additionally, another form of silica was observed

at 522-527 cm⁻¹, respectively for the BT -HAp nanocomposite prepared at pH 3, 7 and 243 244 10. The presence of typical vibrations of 6 member rings compiled with alumina and silica-oxygen tetrahedral at 633 cm⁻¹.³⁸ The $-PO_4$ characteristic groups were assigned to 245 the absorption band at 1036-1043 cm⁻¹ which confirms the presence of hydroxyapatite in 246 247 BT-HAp nanocomposite. In addition, the occurrence of hydroxyapatite in nanocomposite 248 may be verified by the absorption band in FTIR spectra. Thus, above observation clearly 249 indicates the formation of BT-HAp nanocomposite. After sorption of Pb, the intensity was shifted and the reduced intensity of OH^{-1} group is shown in Fig. 3 (d). The change in 250 251 the FTIR spectrum after Pb sorption clearly demonstrated that the Pb ions were adsorbed 252 on BT-HAp surface due to electrostatic attraction which signifies the physical sorption process.³⁹ The FESEM images (Fig. 4 (a-e)) describes surface morphology of the 253 254 synthesized powder before and after sorption process. Fig. 4(a) signifies about the 255 formation of nearly uniform spherical HAp nanoparticles with the particle size of 35-40 256 nm. The EDX analysis associated with FESEM was very useful to detect the elemental 257 composition of the nanocomposite. The EDX analysis (inset of Fig. 4a) confirmed the 258 presence of calcium, phosphate and oxygen elements in HAp nanoparticle. On the other 259 hand, from Fig. 4(b-d) the porous surface of nanocomposite and the particle size varied 260 from 75-80 nm was observed. In Fig. 4(e), the micrograph revealed Pb sorption on the 261 nanocomposite surface that was also confirmed by EDX analysis (inset of fig. 4e).

262 The bright field TEM image confirmed the nanocomposite size ranges from 50-80 nm 263 with porous surface (Fig. 5(a-c)). The HRTEM images are presented in the inset of TEM 264 images of the particular nanocomposite. The interlayer spacing is equal to 0.294 nm of 265 BT-HAp-7 nanocomposite in the HRTEM corresponds to the (211) plane. From low 266 resolution of TEM image, the characteristic crystalline spot were obtained from SAED 267 pattern (Fig. 5 d-f). The diffraction rings and bright spots were due to polycrystalline 268 nature of the nanocomposite. A very clear rings and spots of nanoparticles suggested 269 about the formation of highly crystalline BT-HAp-7 (Fig. 5e). Similar observation was 270 also found in XRD pattern.

The surface area was measured by absorption-desorption of nitrogen by multipoint BET method. Further chemical treatment was not performed. The samples were under degassing at a temperature of 200 °C for 2 hrs followed by flushing by helium gas. The

(5)

274 moisture content and unwanted air was removed from the pores of the samples by helium 275 degassing. The relative pressure was maintained in the range of 0.05-0.3 to measure the 276 surface area. The surface area of BT-Hap was decreased as the pH of solution increases (pH 3- 21.89, pH 7- 12.4, pH 10- 11.9 m² g⁻¹) and therefore, the maximum surface area 277 278 was obtained for BT-HAp-3. However, the particle size of the nanocomposite behaves 279 inversely with the surface area and it increased with increasing solution pH. The 280 crystallite size is also observed earlier in the same pattern. The average pore diameter and 281 pore volume was determined by Barret-Joymer-Halender (BJH) method. It was observed 282 that the pore diameter and pore volume were much higher (e.g. HAp-7: 522.9Å and 0.1627 cc g^{-1}) which plays a significant role for sorption of metal ions. From intensity vs. 283 284 particle diameters plot, it was observed that the average particle size (d_{50}) of the 285 nanoparticle was obtained around 100 nm.

286

287 **3.2. Response surface optimization: ANOVA result**

According to the design matrix by CCD, ANOVA results from software are listed in Table 3. A quadratic regression model equation describing the sorption process resulted from ANOVA study can be expressed as follows:

291

Sorption Capacity

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- 293

 $= +97.72 + 1.29A - 13.87B + 0.48C - 1.04A^{2} - 11.23B^{2} - 1.2C^{2} + 0.074AB - 1.51AC - 0.14BC$

294 The above regression model shows the relation between the response and the independent variable in terms of coded factor. It can be predicted from the equation that the dosage 295 and solution pH has a positive effect on adsorption and initial Pb^{+2} concentrations have 296 297 negative effect on sorption capacity. The highest order of the significant effect by 298 different independent variable and their interactions on sorption capacity is B and lowest 299 is AB. ANOVA study was performed to justify the significance of the quadratic model. 300 The model F-value of 117.34 implies the significance of the model (Table 3). There was 301 only 0.01% possibility to make noise in the predicted model. A good correlation was 302 observed between the experimental data and predicted data. The multiple correlation coefficient (R^2) was found as 0.9906 which implies that 99.06% of the variations of 303

sorption capacity could be explained by the model. The 'Pred R^2 ' of 0.9051 was in logical conformity with the 'Adj R^2 ' of 0.9822.

306

307 3.3. Interactive effect of variables on sorption capacity

308 The effect of experimental variables and the response of sorption capacity were analyzed 309 which was designed by CCD with full factorial based on three factors. Table 4 represents 310 a comparative study on Pb sorption capacity among the nanocomposites and its basic components with 100 mg L^{-1} initial Pb solution at pH 7. The maximum sorption capacity 311 was found for BT-HAp-7 nanocomposite (97.94 mg g⁻¹) than BT-HAp-3 (95 mg g⁻¹) and 312 10 (93 mg g^{-1}) which are shown in table 4. Hence, all the sorption experiments were 313 carried out by potential BT-HAp-7 nanocomposite. Although bentonite clay (78 mg g⁻¹) 314 and HAp nanoparticles (83 mg g^{-1}) individually did not show good sorption capacity 315 316 compared to BT-HAp nanocomposite, combination of these two components were 317 explored for potential capacity. It was reported that particle sizes influenced the sorption process noticeably during in situ application of nanoparticles.⁴³ Results shows that 318 319 although BT-HAp-7 nanocomposite has less surface area than BT-HAp-3, it has got 320 better adsorption property than BT-HAp-3. Therefore, particle size was not solely 321 responsible for sorption capacity. The Pb solution was possibly able to diffuse through 322 the particles and a poor correlation might obtain by external surface, suggests that particle 323 size was not the prime parameter to control the equilibrium sorption. However, at 324 equilibrium, the sorption capacity and specific surface area were not directly proportional to each other. ¹⁷ Fig. 6(a) reveals the combine effect of dose corresponding with initial Pb 325 326 concentrations on sorption capacity of nanocomposite in contour plot. In this plot, we 327 observed that the sorption capacity was increases with increasing dosage whereas at the 328 same time under same experimental condition, sorption capacity was decreased with 329 increasing Pb concentration. The sorption capacity was reduced from 99.4 % to 75% with increasing Pb concentration from 50 mg L^{-1} to 150 mg L^{-1} with 1 mg L^{-1} dose, therefore, 330 331 metal ion uptake by the nanocomposite was reduced by decreasing driving force in form 332 of concentration gradient. On other hand the sorption capacity was enhanced with 333 increasing dosage of nanocomposite due to attachment of Pb with the higher surface area 334 of nanocomposite.

335 The combine effect of dose and the solution pH on Pb removal are shown in Fig. 6(b). It 336 was observed that the sorption capacity was increases with increasing nanocomposite 337 dosage. It was also found by quadratic model that the dose parameter have positive effect on sorption capacity however, change in sorption capacity beyond 1 g L⁻¹ dose 338 considering 100 mg L^{-1} Pb⁺² concentration was insignificant. Therefore, the optimum 339 dose was considered as 1 g L^{-1} with same experimental condition. The solution pH is an 340 341 important factor that significantly influenced the sorption capacity or removal efficiency. 342 The contour plot revealed that the sorption capacity was increases from 96% to 99.4% 343 with increasing pH from 4.5 to 5, respectively. However, the sorption capacity was decreases from 99.48 to 97.8% with changing pH from pH 5 to 5.5, respectively. At a 344 345 lower pH (<5), BT-HAp nanocomposite surfaces become positively charged due to higher H⁺ ion concentration, resulting lower sorption capacity due to repulsion between 346 positively charged nanocomposite surface and Pb⁺². The solution was favored higher 347 348 sorption capacity at pH 5 due to electrostatic attraction between negatively charged BT-HAp nanocomposite surface and the Pb⁺². Although beyond this pH, the sorption 349 experiment was unsuccessful due to precipitation of Pb as lead hydroxide.41 Hence, 350 351 selection of exact pH is very important and in this study optimum pH was found as 5 by 352 response surface methodology.

The pH has a positive effect on sorption capacity (Eqn. 5). Fig. 6(c) represents the collective effect of pH and initial Pb concentration on sorption capacity. The sorption capacity was decreases from 99.4% to 75% with increasing Pb concentration from 50 to 150 mg L^{-1} by applying 1 g L^{-1} dose at pH 5. The nanocomposite active sites were enclosed by more Pb ions and get saturated when higher Pb concentration was used and therefore, sorption capacity decreases.⁴² Similar observations were also found for other pH values.

360

361 **3.4. Validation and confirmation of model**

Validation is a technique of RSM that used to check the accuracy of the predicted model and the corresponding results are shown in Table 2. Assessment of experimental test and predicted findings confirms similar responses (Fig 7). The software was allowed to select the targeted goal for factors or responses from numerical optimization. In this study, the

factors were within the range and based on corresponding 10 optimum conditions, the sorption capacities was about 97.94 mg g⁻¹ with 0.95% deviation from experimental value. From 10 optimum conditions in numerical optimization method, the desirability as an objective function was found out 1 by considering the desired goals (Table 5). Therefore, the regression model successfully explained the process with high accuracy and reliable for predicting the sorption capacity.³²

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373 **3.5. Adsorption isotherm and kinetics**

374 Sorption capacity estimation is necessary to ascertain the amount of sorbent required for 375 potential removal of heavy metal such as Pb from aqueous solution. Adsorption isotherm 376 study was conducted by varying the Pb concentration from 50 to 150 mg L⁻¹ with dosage 377 of 1 g L⁻¹ for 24 hrs contact time. Temperature was varied as 20°, 30° and 50° C to 378 conduct the isotherm study.

379 Equilibrium data was further analyzed by Langmuir and Freundlich isotherm model to 380 understand the sorption behavior. The Langmuir model is based on monolayer coverage 381 with homogeneous surface sites whereas Freundlich model is applicable only for highly heterogeneous surfaces.^{43, 44} Table 6 represents the result of isotherm model and we 382 observed that Langmuir model fitted well with co-relation coefficient (R^2) of 0.99. The 383 384 higher n value indicates the favorable condition of adsorbate on sorbent surface. Pb 385 monolayer was bonded with functional groups of BT-HAp-7 nanocomposite during sorption. The maximum sorption capacity was found as 346 mg g^{-1} that was significantly 386 387 higher compared to other materials shown in the table 7.

Pseudo kinetic models were studied to observe the sorption mechanism. The Pseudo 1st order and 2nd order kinetic models with the empirical equations were used to determine the rate kinetics.⁴⁹ It was observed that the sorption capacity was very fast within first 15 minutes but after that the process became slower before reaching equilibrium. The pseudo 2nd order model was best fitted with linear regression correlation coefficient (R²) value of 0.999. The rate constant (k₂) value indicated the chemisorptions process of Pb ions on the nanocomposite surface.⁵⁰

395

396 3.6. Desorption study of nanocomposite

397 The adsorbents were loaded with toxic heavy metals which results an environmental 398 hazard solid spent waste. Therefore, regeneration of spent materials can make the process 399 cost-effective. Desorption study was conducted using EDTA, HNO₃ and NaOH solution. Maximum desorption about 64% from spent nanocomposites containing 97 mg g⁻¹ of Pb 400 401 was observed using EDTA solution whereas only 0.12% for and 0.01% desorption was 402 observed for HNO₃ and NaOH, respectively at 60 minutes contact time. Equilibrium was 403 reached after 120 minutes at constant stirring condition. Three consecutive sorption-404 desorption cycles were performed and sorption capacity of the nanocomposite decreases 405 about 12-16% during this period. Y. Ren et al.(2012) discussed that the sorptiondesorption process involved the complexation, physisorption and ion exchange reaction.⁵⁰ 406 407 However, the reason behind improved desorption efficiency of EDTA solutions can be explained by the reaction of loosely bound Pb⁺² with EDTA, that produced a stable lead 408

409 acetate complex and desorbed quickly. Therefore, nanocomposites were regenerated for 410 further uses.⁵¹

411

412 **4. Conclusions**

413 The nanocomposite (BT-HAp) was successfully synthesized from bentonite clay and 414 hydroxyapatite by chemical synthesis method. The novelty of this work lies on 415 development of three different nanocomposite from clay and HAp powder having 416 distinguished property. Additionally, the novel nanocomposite was potentially applied for 417 toxic heavy metal (Pb) remediation. A very simple synthesis process is discussed in this 418 report, where raw materials are of very low-cost. Hence there is a possibility to scale-up 419 the process in a cost-effective manner with a less hazardous component. BT-HAp 420 nanocomposite was synthesized at neutral pH which is very significant for application in 421 natural condition and use of minimum chemicals makes the process environment 422 friendly. The formation of BT-HAp nanocomposite was confirmed through XRD, FTIR, 423 FESEM, EDX and TEM analysis. BT-HAp-7 was established as potential sorbent having 424 less surface area than BT-HAp-3. This observation indicated that the external surface was 425 not the main parameter for sorption. The ANOVA results showed optimization of Pb 426 sorption on nanocomposite by RSM was in well agreement with experimental result under optimized condition. The multiple correlation coefficient ($R^2=0.9906$) value was 427

428 also justified the above observations. The model designed by CCD well describes the 429 sorption process where the sorbent dose and the pH have a positive effect. However, 430 initial Pb concentration had negative effect on sorption process. The Numerical 431 optimization method showed that Pb sorption capacity of nanocomposite was about 97.94 432 mg g^{-1} . The sorption process fits well with the Langmuir isotherm model signifies 433 monolayer Pb sorption on nanocomposite surface. The sorption mechanism of nanocomposite was also well explained by Pseudo 2nd order model indicated 434 435 chemisorption. In summary, the experimental and theoretical results suggest that BT-436 HAp nanocomposite could be a potential, low cost sorbent for heavy metal remediation 437 from waste water towards an environmental friendly approach.

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681	(a) dose vs. initial Pb conc., (b) dose vs. pH, (c) Initial Pb conc. vs pH.
682	
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Tables

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689	Table 1: Experimental range and levels (coded)
690	

Independent variable	Factor	Rang	ge and Level (Co	oded) 691 692
	code			693
1		-1	0	+1694
Dose, g L^{-1}	А	0.5	1	1.5695
Initial Pb	В	50	100	15696
concentration, mg L ⁻¹				69'
pН	С	4.5	5	5.569

Run	A:	B: Initial	Pb C: pH	Response:	Response: 74
	Dose	conc.		Sorption capacity,	Sorption capacity
				Actual value	Predicted value
1	0.50	50.00	4.50	98	94.78 74
2	1.00	156.00	5.00	68	68.10 74
3	1.50	50.00	5.50	99	98.46 74
4	0.50	50.00	5.50	98.5	99.05 74
5	1.50	150.00	5.50	70	70.59 74
6	1.00	100.00	5.00	97	97.72 74
7	1.50	50.00	4.50	99	100.25 75
8	1.00	100.00	5.00	96.7	97.72 75
9	1.84	100.00	5.00	98.2	96.96 75
10	1.00	100.00	5.84	96	95.15 75
11	1.00	100.00	5.00	97.5	97.72 75
12	0.20	80.00	4.00	84	86.09 75
13	0.50	150.00	4.50	68	67.16 75
14	1.50	150.00	4.00	70	70.5 75
15	1.00	100.00	5.00	98	97.72 75
16	1.00	50.00	5.00	99	100.37 76
17	1.00	100.00	5.00	97.3	97.72 76
18	1.00	100.00	5.00	97.5	97.72 76
19	1.00	100.00	4.16	95.5	93.52 76
20	0.50	150.00	5.50	71	70.88 76

739 Table 2: 2^3 factorial design matrix and experimental response as sorption capacity (mg g⁻¹)

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Source	Sum of squares	Degree of freedom (df)	Mean square	F -value	Probablity>F	Coefficient estimate
model	2973.11	9	330.35	117.34	< 0.0001	-
А	17.08	1	17.08	6.07	0.0335	1.29
В	1911.58	1	1911.58	679.01	< 0.0001	-13.87
С	3.61	1	3.61	1.28	0.2841	0.48
AB	0.041	1	0.041	0.015	0.9059	0.074
AC	30.09	1	30.09	10.69	0.0084	-1.51
BC	0.18	1	0.18	0.062	0.8082	-0.14
A^2	9.91	1	9.91	3.52	0.0900	-1.04
\mathbf{B}^2	575.49	1	575.49	204.42	< 0.0001	-11.23
C^2	30.77	1	30.77	10.93	0.0079	-1.20
$791 R^2 = 0$ 792	$0.9906, \mathrm{Adj} \mathrm{R}^2 = 0.98$	22, Pred $R^2 = 0$	0.9051			

790 Table 3: ANOVA for the quadratic model

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799	Table 4:	Comparativ	e study	of lead	sorption	capacity.

Sorbent Adsorption

Sorbent	capacity, mg
BT-HAp-3	95
BT-HAp-7	97.94
BT-HAp-10	93
Bentonite clay powder	78
HAp nanopowder	83

833 Table 5: Numerical optimization of the experiment: 10 solutions with desirability of 1

А	В	С	R1
(Dose, $g L^{-1}$)	(Initial Pb	(pH)	(Sorption capacity, mg
	concentration, mg L^{-1})		g ⁻¹)
0.80	97.33	5.13	97.9469
1.01	149.53	4.66	72.2151
0.65	99.96	4.74	95.1846
0.53	87.31	4.77	97.2562
0.76	100.15	4.83	96.2751
0.79	98.81	5.36	97.5142
0.69	128.46	5.15	85.2497
1.34	93.27	5.43	98.4342
1.10	111.00	5.50	93.3238
0.60	94.23	5.43	98.0828

	Langmuir model			Freundlich model			
	\mathbb{R}^2	$q_{\rm m}$	K_L	\mathbf{R}^2	$K_{\rm F}$	n	
		$(\operatorname{mg} g^{-1})$	$(L mg^{-1})$		$mg g^{-1} (mg L^{-1})^n$		
	0.99	346	0.015	0.97	2.6	1.39	
849							
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856							

848 Table 6: Langmuir and Freundlich isotherm model parameters for lead sorption

857	Table 7: Adsorption capacity of various nanocomposite
858	

Nanocomposite	Adsorption capacity, mg/g	Reference
AC-HAp	9-14	M.S. Fernando et al. ⁴⁵
		doi:10.1016/j.apsusc.2015.05.092
SWCNTs/WSh	185.2	S.Saadat et al. ⁴⁶
		doi:10.1016/j.jece.2014.08.024
Poly(o-phenylenediamine)	228	L. Yang et al. ⁴⁷
/reduced graphene oxide		doi:10.1016/j.apsusc.2014.04.083
Silica nanopowders/alginate	83.33	R. D. C. Soltani et al. ⁴⁸
		doi:10.1016/j.jtice.2013.09.014
BT-HAp	346	This study

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Fig. 1: Schematic of nanocomposite preparation process with changes in morphology

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