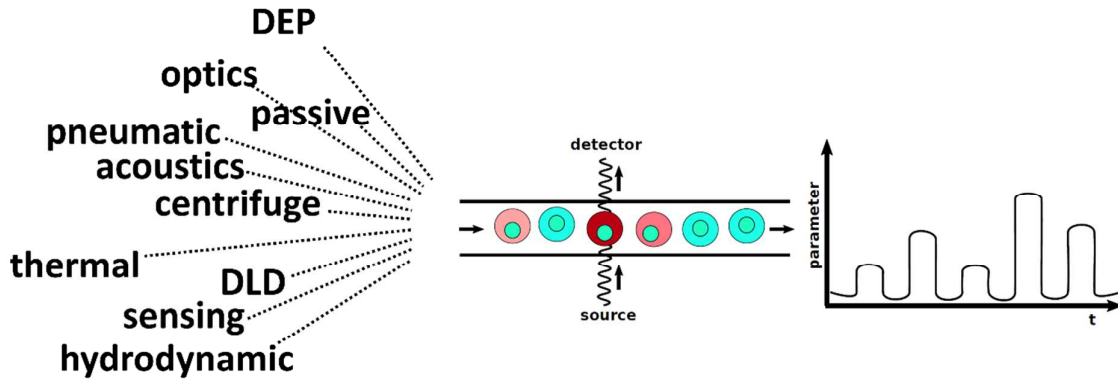




The Poisson distribution and beyond: methods for microfluidic droplet production and single cell encapsulation

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In recent years there has been an explosion of methods for encapsulating cells in droplets. This review examines the state-of-the-art, including methods for active encapsulation.

The Poisson distribution and beyond: methods for microfluidic droplet production and single cell encapsulation

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There is a recognized and growing need for rapid and efficient cell assays, where the size of microfluidic devices lend themselves to the manipulation of cellular populations down to the single cell level. An exceptional way to analyze cells independently is to encapsulate them within aqueous droplets surrounded by an immiscible fluid, so that reagents and reaction products are contained within a controlled microenvironment. Most cell encapsulation work has focused on the development and use of passive methods, where droplets are produced continuously at high rates by pumping fluids from external pressure-driven reservoirs through defined microfluidic geometries. With limited exceptions, the number of cells encapsulated per droplet in these systems is dictated by Poisson statistics, reducing the proportion of droplets that contain the desired number of cells and thus the effective rate at which single cells can be encapsulated. Nevertheless, a number of recently developed actively-controlled droplet production methods present an alternative route to the production of droplets at similar rates and with the potential to improve the efficiency of single-cell encapsulation. In this critical review, we examine both passive and active methods for droplet production and explore how these can be used to deterministically and non-deterministically encapsulate cells.

1 Introduction

Cellular analysis is a major application of microfluidic systems, whose dimensions permit the on-chip culturing and manipulation of cells using geometries and externally applied force fields with length scales comparable to the cells themselves^{1,2}. To support the controlled manipulation of cells in a high-throughput manner, a wide suite of methods have been developed to localize, lyse, electroporate, fuse, sort, concentrate, and mix cells with reagents. From a research standpoint, the predominant paradigm in which cells are suspended within a single flowing aqueous phase in a system of microchannels, has been a highly successful one, with thousands of researchers continuing to be actively engaged in this field³, producing useable devices for applications including HIV detection⁴, cancer screening^{5,2} and the organ-on-a-chip^{6,7}. However, despite the advantages conferred by operating at the microscale, many of these systems suffer from the same issues as those at larger length scales, though the physical process may differ; e.g. undesired mixing and concentration gradients can result from diffusion

instead of advective transport. Furthermore, as the dimensions of a microchannel approaches that of a cell, stiction and cell adhesion to channel walls severely limits the reusability of such devices or restricts the types of on-chip cell culturing that can be performed.

Such restrictions, especially the inability to reliably inhibit diffusive mixing over long time scales, prevent the use of single-phase systems for many applications in the growing field of single-cell analysis. Here, single cells are assayed on an individual, rather than the population basis. This is critically important as the phenotypic expression of cells can vary substantially in a cell population with identical genotypes; a good example being the somatic cell population that makes up a variety of human body tissues. Even within the same tissue cells exhibit a range of epigenetic factors, as each experiences a unique microenvironment that influences their development and function⁸. By inspecting the relevant parameters of each cell individually, whether that be via a fluorescent reporter, inferred physical dimension or electrical/mechanical property, the degree of heterogeneity in a cell population can be determined^{9–14}. Heterogeneity is known to play a key role in the development of some tumors¹⁵ in addition to applications such as the discovery of rare cells¹⁶ and high-throughput screening¹⁷, where the influence of the local microenvironment can also be assessed by altering its constituent concentrations¹⁸.

Traditionally, the study of individual cells utilizes some combination of flow cytometry and downstream processing,

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often via fluorescence activated cell sorting (FACS)^{19,20}. In flow cytometry a sample stream containing cells is hydrodynamically focused into a line of single cells, which can then be independently inspected via optical or impedance measurement^{21,22}. While flow cytometry is successful as a single-cell measurement system, where individual cells can be screened at high-throughput, as traditionally performed (in a single fluid phase) it is limited to applications where inter-cellular interaction is tolerable and poor control of the local environment is an acceptable constraint. In a single-fluid phase, the environment is controlled at a global level but uncontrolled in the immediate locality of an individual cell, meaning that any measurement of the extracellular environment is on a population rather than a single-cell basis. In a single phase system, the isolation of a cell's microenvironment can be accomplished through the use of pneumatically actuated chambers^{23,24}, although it is difficult to integrate more than a few such (independently controlled) reaction chambers on a single device.

There are a number of applications where a cell must be locally contained to control intercellular interactions and cell signalling. 3D tissue printing requires meticulous control of the cell environment in order to direct cell growth and cell fate, often through the use of hydrogel capsules and changes in the mechanical or chemical properties of the extra-cellular matrix²⁵⁻²⁷, though two-phase bioprinting presents another route to preventing cell-cell interaction^{28,29}. The artificial pancreas, for example, makes use of encapsulated islet cells to limit immune system response post-implantation³⁰⁻³². Conversely, it can be desirable to interact specific cells, such as in cell fusion for hybridoma formation, cell reprogramming, and antibiotic drug discovery, activities that require fine-grained control of a cell's position and environment³³⁻³⁵, abilities also required in studies on protein expression and antibody production^{36,37}.

An evolving methodology to control the cellular environment makes use of the principles of droplet-based microfluidics, where an aqueous flow is segmented into individual droplets within an immiscible carrier fluid (often a mineral or fluorinated oil) to encapsulate cells, organic molecules and reagents³⁷⁻⁴³. This concept for single-cell analysis is explored in Fig. 1. Here, some of the numerous advantages associated with the encapsulation of cells within droplets are evident. First, as the oil-water interface provides a natural barrier to diffusion, cellular products remain contained in its immediate vicinity, so that even significant concentration gradients between droplets can be maintained and dilution minimized⁴⁴. Second, the reaction volume is significantly reduced when compared to single-phase microfluidic systems, a significant factor when using high-value reagents such as enzymes or DNA. Third, the ability to control the location and duration of discrete fluid volumes is enhanced^{45,46} and

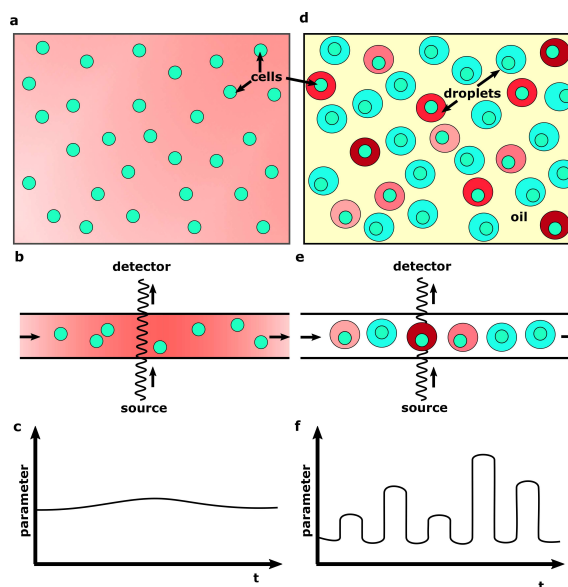


Fig. 1 Cell encapsulation enables efficient analysis of individual cells by confining them within a local microenvironment. (a-c) In conventional cell culture, ubiquitous fluid mixing only permits analysis of cells at the population level due to diffusive mixing of cellular products. (d) Encapsulation of cells within water-in-oil droplets prevents both advective and diffusive mixing. (e,f) Following encapsulation and incubation, parameters of interest can then be analyzed on an individual cell level in a high-throughput manner.

long term cell culture is simplified by preventing adhesion between encapsulated cells or to device features⁴⁷.

Two-phase systems can also be utilized with the same versatility as single-phase ones. For example, reagents and other cells can be added using a number of different micro-injection and droplet coalescence techniques^{45,48-50}. Analyte diffusion across the oil-water interface can also be controlled through interface modification to selectively control diffusion between the droplet and its environment⁵¹⁻⁵³ or between individual droplets⁵⁴⁻⁵⁷. Moreover, the ability to selectively control diffusion, and merge droplets permits long-term cell viability assessment, as noted in a range of prior studies⁵⁸⁻⁶². Leveraging these advantages has enabled the application of droplet-based encapsulation methods in high throughput drug screening¹⁷, rare cell detection⁶³, single-cell DNA amplification⁶⁴, and directed evolution⁶⁵⁻⁶⁸, in addition to non cell-based applications including the study of crystal growth^{69,70}, single-molecule detection⁷¹, protein-protein interaction⁷², nanomaterial synthesis⁷³ and drug delivery⁷⁴. For a thorough discussion of the advantages that encapsulation confers for single cell analysis, the reader is directed to a number of excellent reviews published elsewhere^{9,37,75,76}.

Cell encapsulation offers substantial benefits for microenvironmental control and sample handling, however significant questions remain regarding the optimal method(s) for encapsulation. That said, systems incorporating microfluidic methods are the most promising, where cell encapsulation is performed reliably through the use of features or force gradients on the scale of the cells themselves. By far, the most common method of encapsulating cells makes use of microfluidic channel geometries that mix co-flowing water and oil phases, where (in most cases) the water phase self-separates into discrete water droplets. Using T-junctions, flow-focusing or co-flowing intersections, droplet formation can be accurately controlled through variation of differential volumetric flow rates of the immiscible fluid phases. However, it is not straightforward to control the number of cells encapsulated on a droplet-by-droplet basis, especially important as one cell per droplet is highly desired for single-cell analysis. If the encapsulation of dispersed cells into droplets occurs passively (and randomly), this number is impossible to reliably determine on a droplet-by-droplet basis, thus limiting the utility of passive cell encapsulation for single cell analysis^{77,78}.

To this end, recent research has explored more sophisticated microfluidic techniques to control the number of cells per droplet. Indeed, a number of these have shown substantial promise for dramatically improving the efficiency by which encapsulated single cells are produced. Furthermore, there are an increasing number of active methods available for droplet production and cell encapsulation, which are able to tune droplet size or produce droplets on-demand. Examples of active methods include those incorporating electrical, acoustic, optical and magnetic fields. These approaches have the advantage that they can be arbitrarily actuated and locally focused, and show substantial promise in addressing the deficits of purely hydrodynamic cell encapsulation. Surprisingly, previous reviews of cell-based analysis in microfluidic droplets have focused almost exclusively on hydrodynamic methods and/or emphasized the applications of encapsulated cells^{9,37,62,75,76,79–81}.

Moreover, although there are a plurality of methods for encapsulating cells, on both the micro and macro scales⁷⁹, this analysis will focus specifically on microfluidic technologies used to encapsulate cells in two-phase systems, since these are better suited for en-masse, high-throughput and single-cell analysis applications. Additionally, because methods available for the encapsulation of cells are fundamentally those of droplet production, these methods are also discussed in the following sections, as future encapsulation methods are likely to be developed from the available suite of droplet production methods. These methods are also examined quantitatively in terms of their droplet production rate and potential to determine the number of cells per droplet beyond

the limitations set by Poisson statistics.

2 Microfluidic droplet production

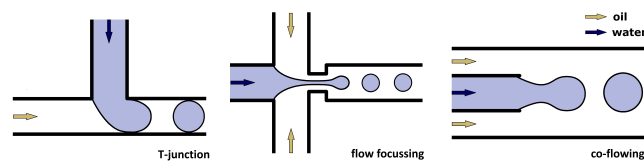


Fig. 2 Three principle microfluidic geometries are available for droplet production. In the simplest setup, oil and water are combined in a T-junction. Flow focusing and co-flowing geometries intersect the fluids in systems with both increasing degrees of symmetry and fabrication complexity from left to right, with bilateral and radial symmetry (if organized in a capillary-in-capillary setup⁸²) for co-flow and flow-focusing geometries, respectively.

Although droplet production is ubiquitous in the microfluidic literature today, the microchannel geometries required to reliably create droplets were developed little more than a decade ago^{83–86}. Because of its ubiquity, one can be forgiven for forgetting how remarkable the process is; i.e. by exploiting a number of microfluidic geometries, a fluid of arbitrary volume can be transformed into a multitude of uniformly-sized femto-nanoliter droplets at rates of up to 100 kHz⁸⁷. Moreover, given the length scale of the features used (typically between 10 and 100 μm) these channel designs can be duplicated on-chip for parallel processing. Common geometries for droplet production include T-junction, flow-focusing and co-flowing structures^{88,89} (Fig. 2), although variations on these themes have been reported, e.g. the V-junction or dual T-junctions^{90,91}. The underlying principle of operation for each of these geometries, however, is the same: an interface is created between two co-flowing immiscible fluids where one fluid self-segregates into discrete droplets that are surrounded by the second fluid. Which fluid becomes the dispersed phase (the one forming the droplets) and which forms the continuous phase (the one surrounding the droplets) is controlled by the respective surface energies of the fluid and that of the channel⁹². In most cases, such as when using hydrophobic polydimethylsiloxane channels and oil/aqueous fluids, the aqueous phase disperses, although it is possible to initiate phase inversion through hydrophilic modification of the channel walls⁹³.

Droplet production processes are fundamental to the encapsulation of cells. Because of this, an understanding of the droplet-production toolkit is essential when selecting the particular method that should be employed in a given cell-encapsulation scenario. For fluidic self-segregation to occur, a pressure source that acts either on the fluid volume

211 or the oil-water interface is required to push the dispersed
 212 phase into the continuous one. The next section explores the
 213 basic physics of fluid breakup into droplets and the different
 214 methods used to generate the required pressure gradients that
 215 give rise to this process.

216 2.1 Physics of droplet production

217 Despite the variety of methods used to drive the dispersed
 218 phase into the continuous one, the physics of droplet
 219 formation apply regardless. The physical parameters that
 220 dominate droplet formation can be determined through
 221 analysis of the capillary number $Ca = \mu U / \gamma$, where μ (Pa·s)
 222 and U ($\text{m}\cdot\text{s}^{-1}$) are the viscosity and characteristic velocity of
 223 the continuous phase and γ ($\text{N}\cdot\text{m}^{-1}$) is the surface tension
 224 of the water-oil interface, although other non-dimensional
 225 quantities are relevant to droplet breakup, including the Weber
 226 number We (reporting the relative importance of inertia with
 227 respect to interfacial tension), Bond number Bo (reporting
 228 the relative importance of gravitational forces with respect to
 229 interfacial tension) and Reynolds number Re (reporting the
 230 relative importance of inertial forces with respect to viscous
 231 forces), especially at high flow rates and when using larger
 232 dimension geometries⁹⁴. With increasing Ca , the different
 233 flow regimes are defined as the squeezing, dripping and jetting
 234 regimes^{95,96}.

235 In the surface-tension dominated squeezing regime, droplet
 236 pinch-off is driven by the pressure differential behind and in
 237 front of a confined extension of the fluid interface, where the
 238 resultant pinched-off droplet size is proportional to the flow
 239 rate ratio of the dispersed and continuous phase. At higher
 240 Ca , droplet breakup and droplet size is shear-dominated (in
 241 the dripping regime) with a smaller pressure differential on
 242 either side of the nascent droplet than in the squeezing regime,
 243 yielding droplets whose size scales inversely with increasing
 244 Ca and with a reduced dependence on the flow rate ratio.
 245 Finally, in the jetting regime, droplet breakup occurs as a
 246 result of Rayleigh-Plateau instabilities along a fluid thread
 247 in viscosity-dominated flow. These three regimes are depicted in
 248 Fig. 3. For a more thorough discussion of these regimes and
 249 parameters that determine resultant droplet size, the reader is
 250 advised to peruse one of the excellent publications or reviews
 251 on the topic^{94,95}.

252 2.2 Passive droplet production

253 Droplet generation occurs passively if the pressure source
 254 is located remotely from the droplet formation geometry.
 255 Typically, the force driving fluid flow on-chip, as in Fig. 4a,
 256 is an externally driven pressure source, such as a syringe or
 257 pressure-driven pump. Because such macroscopic pressure
 258 sources are located at distances from the device that are

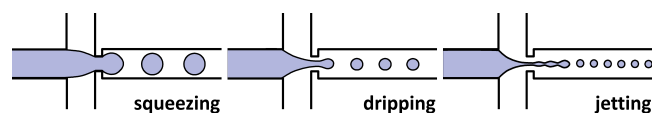


Fig. 3 Droplets are produced in the squeezing, dripping and jetting regimes with increasing capillary number, respectively. In the squeezing regime, the interface contacts both sides of the channel before breakoff. In the dripping regime droplet breakup is shear-dominated and the fluid interface is detached from the channel surface. At higher Ca (in the jetting regime) droplet breakup occurs due to Rayleigh-Plateau instabilities along an elongated fluid thread that extends into the outlet channel. In general, droplet size decreases with increasing Ca .

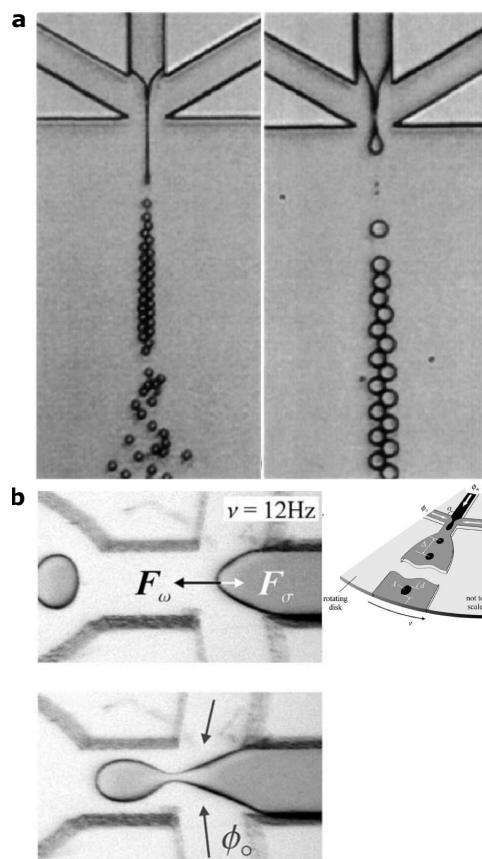


Fig. 4 (a) Droplets can be produced over a range of sizes by changing the ratio of oil and water flow rates, as controlled by external pressure sources. Reproduced with permission from reference 97, copyright 2004, AIP Publishing. (b) Alternatives exist for generating continuous droplet streams, here showing a case where centripetal forces are used to drive fluid through a droplet-forming geometry. Reproduced with permission from reference 98, copyright 2007, Springer.

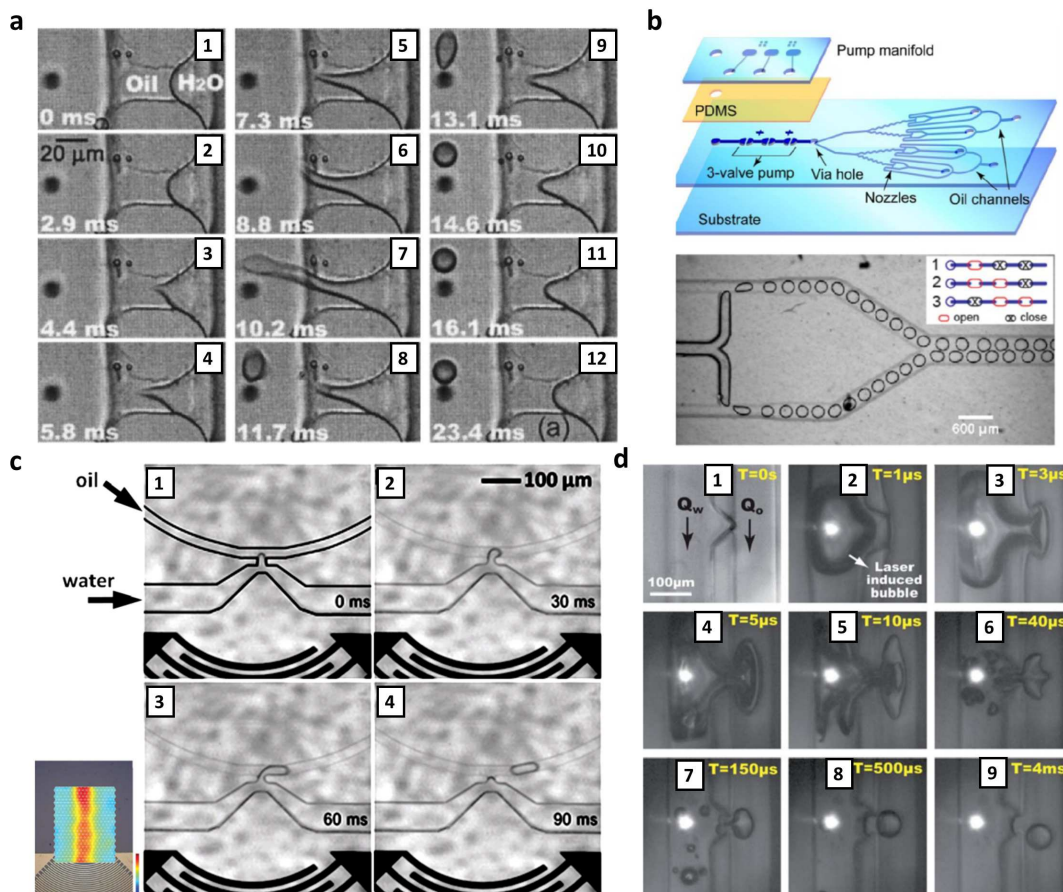


Fig. 5 A plurality of methods can be used to actively drive pressure gradients on-chip. Examples of these methods include (a) jet formation from an electrically generated Taylor cone, (b) the use of a pneumatically driven micropump, (c) acoustic force actuation and (d) laser-pulse excited cavitation. (a) Reproduced with permission from reference 99, copyright 2005, AIP publishing. (b,c) Reproduced with permission from references 100 and 101, copyright 2013, The Royal Society of Chemistry. (d) Reproduced with permission from reference 102, copyright 2011, The Royal Society of Chemistry.

orders of magnitude larger than the channel length scale, it is difficult (although not impossible) for the flow rates at the droplet forming geometry to be anything but continuous, thus resulting in continuous droplet production where the rate of individual droplets that are produced is a function of the fluid flow rates and the specific channel geometry and dimensions⁷⁴. Examples of systems used to generate continuous streams of water-in-oil droplets have been covered extensively elsewhere^{1,80,94}. However, external pumps are not the only means by which pressure gradients can be produced for continuous droplet generation. For example, Häberle *et al.* demonstrated a method whereby a rotating microfluidic device is used to generate the centripetal force necessary to create droplets in a conventional flow-focusing geometry (Fig. 4b)⁹⁸.

2.3 Active droplet production

There are other methods for producing pressure gradients, so that droplet production can occur on-demand with the application of an active, short-duration pressure source. As the timing, amplitude and duration of a pressure pulse can be arbitrarily set, such on-demand methods have the advantage of producing droplets of similarly arbitrary size and intervals. The most common active methods for droplet production are listed in Table 1. Park *et al.*, for example, used a focused pulsed laser to create a cavitating microbubble in the vicinity of a T-junction like structure, producing individual picoliter-volume water-in-oil droplets in the space of a few milliseconds and at rates up to 10 kHz¹⁰² (Fig. 5d). Interestingly, this approach has also been used to produce femtoliter-volume droplets on-demand

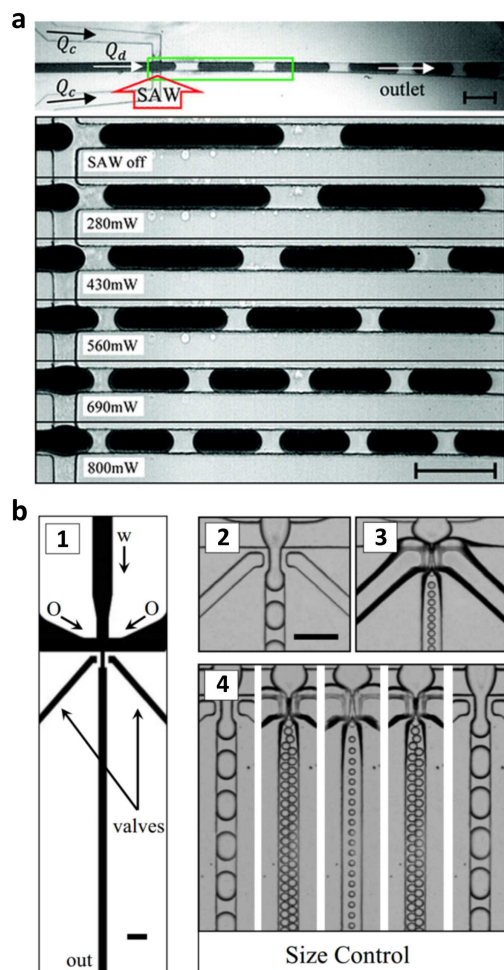


Fig. 6 Acoustic^{103,104}, electrical¹⁰⁵, mechanical^{106,107} and thermal^{107–110} forces can be locally applied to actively tune the droplet dimensions and production rates. (a) Shows the use of a surface acoustic wave (SAW) to modify the local interfacial pressure conditions at the oil-water interface, promoting the generation of smaller droplets for increasing acoustic pressure. Reproduced with permission from reference 103, copyright 2013, The Royal Society of Chemistry. In (b), integrated pneumatic valves are used to alter the droplet formation geometry, and thus local capillary number, to vary resultant droplet dimensions. Reproduced with permission from reference 106, copyright 2009, AIP Publishing. All scale bars are 100 μm .

in nanofluidic channels¹¹¹. In related work, Xu & Attinger utilized a piezoelectric actuator mounted on the chip surface, where each depression of the actuator produced an individual droplet¹¹². However, while laser-induced cavitation or external actuation have the ability to produce droplets at kHz rates, such methods require complex external equipment to produce and focus laser pulses or substantial chip components

that may be difficult to both scale down and reliably integrate. Recently, Collins *et al.* demonstrated the production of droplets using an on-chip pressure source arising from a focused surface acoustic wave (SAW), where conducting structures are patterned directly on the piezoelectric device substrate¹⁰¹ (Fig. 5c). Other methods for creating local pressure sources include integrated micropumps^{100,113} and trans-interface electric-potential generation (Fig. 5a)⁹⁹, although it should be noted that these have yet to be directly applied to on-chip encapsulation.

Alternatively, as long as external pressure sources can be controlled with sufficient precision, they can also be used to produce droplets in an on-demand fashion. Integrated pneumatic microvalves can be used for this purpose (Fig. 5b)¹¹⁶, as can manually controlled microinjectors¹¹⁷, though the rate at which the latter can accurately actuate the production of individual droplets is inherently limited by the capacitive and resistive effects of the channels and tubes through which the pressure impulses are conducted. Aside from producing individual droplets, actively controlled forces can be used in conjunction with passive droplet production methods to alter the droplet size and production rate over shorter time scales than is possible using conventional pressure-driven sources alone.

Broadly, there are three ways the droplet volume can be tuned on-chip: applying a force at the fluid interface, changing fluid properties or altering channel dimensions. In an example of the first case, Schmid *et al.* used the interfacial acoustic pressure generated by a travelling acoustic wave to act both directly on the oil-water interface during droplet formation¹⁰³ and modulate the pressure in the continuous phase¹⁰⁴, in both cases to tune the size of droplets produced continuously from an externally driven pressure source (Fig. 6a).

Interfacial forcing from an electrical source can similarly be used to modulate the size of continuously produced droplets. For example, Tan *et al.* used an electrical field to change the effective capillary number, with smaller droplets generated at higher AC voltages¹⁰⁵, where the underlying mechanisms that determine the resultant droplet size are discussed in recent work¹¹⁸. Optical sources can also be used to act on the fluid interface, where an optical beam is used to increase the residence time of a fluid-fluid interface prior to pinch-off, resulting in larger droplets for a higher applied power^{119,120}. The droplet volume can be similarly tuned by altering the fluid parameters, in effect altering the capillary number and thus the resultant droplet dimensions. For example, fluid in the vicinity of the droplet formation region can be heated, lowering the fluid viscosity and thus creating smaller droplets^{108–110}.

Finally, the channel dimensions can be modified in real-time. Here, volume tuning is achieved in one of two ways. The fluid can either be chopped, where the dispersed phase is segmented when a pneumatic pressure source is

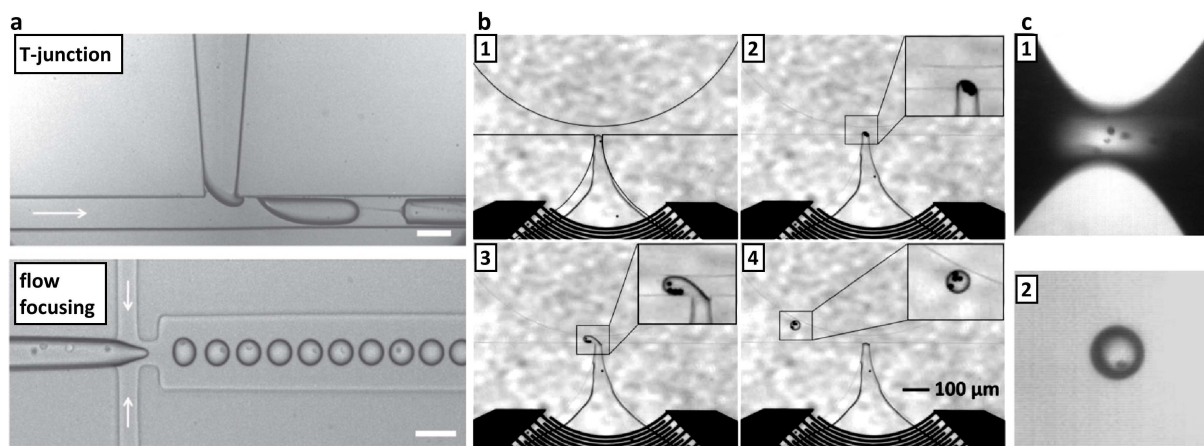


Fig. 7 There are a plurality of methods for encapsulating cells and particles in droplets. (a) In high-throughput applications, cells comprise a fraction of the aqueous volume that enters one of the droplet forming geometries presented in Fig. 2, where encapsulation occurs as a result of spontaneous droplet formation in fluids with different surface energies. Reproduced with permission from reference 114, copyright 2010, IOP publishing. Alternative methods for encapsulation include concentration and ejection using (b) focused acoustic fields and (c) using hydrodynamically thinned fluid bridges. (b) Reproduced with permission from reference 101, copyright 2013, The Royal Society of Chemistry. (c) Reproduced with permission from reference 115, copyright 2014, Elsevier.

348 pulsed to temporarily close the channel, and where each
 349 pulse creates a single droplet^{121–123}. Alternatively, the
 350 droplet forming region dimensions are constricted to increase
 351 the local fluid velocity, thus reducing droplet volume as a
 352 result of the increased capillary number (Fig. 6b)¹⁰⁶. In
 353 each of these examples, an external pneumatic source and
 354 an additional aligned elastomer layer containing air-filled
 355 channels is required, although Miralles *et al.* have reported
 356 the use of an integrated thermomechanical valve, where
 357 current flowing through a resistor heats and locally expands
 358 the PDMS channel at a T-junction, thus altering the size of
 359 droplets produced there¹⁰⁷. However, given the relatively
 360 small deflections induced, the range of droplet sizes that can
 361 be produced is also small (see Table 1).

362 Given the limited work on active droplet production
 363 methods, it is not immediately apparent which approach is
 364 best suited to on-demand droplet production or applicable
 365 to cell encapsulation, though considerations including
 366 ease of fabrication, droplet production rate and general
 367 biocompatibility are all key parameters to be assessed. For
 368 on-demand generation, none of the demonstrated methods
 369 satisfy these criteria optimally; pulsed lasers and high-voltage
 370 electrical fields have questionable biocompatibility, while the
 371 acoustic and external actuation methods have demonstrated
 372 either relatively slow generation rates or complex on-chip
 373 integration. However, the production rates listed in Table 1
 374 are indicative only of the current state of development and do
 375 not represent inherent limits, as on-demand and novel droplet
 376 generation systems remain relatively under-developed. The
 377 same applies for active droplet size tuning methods, where the

droplet production rate in principle should be able to equal
 or better than that of an equivalent passive droplet production
 platform, with the exception of pneumatically controlled
 flow chopping, which is fundamentally limited by the rate
 at which air-filled chambers can expand. With increasing
 development, miniaturization and implementation of on-chip
 actuation many of these on-demand active methods will be
 more frequently applied in applications where precise control
 of the timing and rate of droplet formation is required.

3 Non-deterministic cell encapsulation

The bulk of published work in the area of cell encapsulation
 has used passive encapsulation methods to produce droplets
 whose occupancy is statistically determined. Although
 it is not possible to strictly determine the number of
 cells per droplet with these methods, the average number
 of cells per droplet can be controlled by changing the
 concentration of the incoming cell suspension. In addition to
 conventional passive encapsulation, several novel methods for
 the on-demand production of encapsulated cells have recently
 been demonstrated. These encapsulation methods are now
 presented, with methods for deterministically encapsulating
 cells (those that can specify the number of cells per droplet)
 discussed in the next section. Recently developed methods for
 non-deterministic cell encapsulation are compared in terms of
 their encapsulation rates in Table 2.

Table 1 Comparison of active droplet production methods

Method	Production rate	Droplet volume (range)	Advantages/Disadvantages	Mechanism	Ref(s)
On-demand production					
Focused surface acoustic wave (SAW)	<10 Hz	12-30 pL	On-chip control and combined particle manipulation, limited throughput	SAW is focused at a T-junction, changing pressure conditions at the oil-water interface.	101
Bimorph actuator	2.5 kHz	25 pL to 4.5 nL	High production rate and large size range, requires bonding of actuator	An actuator compresses a chamber, displacing fluid that is ejected into an oil-filled channel.	112
Pulsed laser excitation	10 kHz	1-150 pL	High production rate and large size range, requires equipment to drive on-chip cavitation	Laser-induced cavitation displaces fluid volume into an oil phase in a modified H-filter geometry.	102
Electrical potential	<50 Hz	14 fL to 8 pL	On-chip actuation, high voltages may not be compatible with biological samples	The leading edge of a water-oil interface is directed along an electric potential gradient.	99
Tunable rate					
Surface acoustic wave droplet rate modulation	~210-1100 Hz	~80-210 pL ¹⁰³ , ~30-140 pL ¹⁰⁴	Biocompatible method for continuously altering droplet size on-chip	Acoustic pressure is applied directly to an oil-water interface or to the continuous phase, with smaller droplets produced at higher powers. Electrical potential introduces Maxwell pressure on interface, reducing droplet volume with increasing AC signals >600 V. For related work see Ref. 118 and 105.	103, 104
Electrical droplet rate modulation	10-500 Hz	~50-240pL	Unknown effects of high voltage on biological samples	Pulsed pneumatic valve temporarily closes a microfluidic channel in a flow-focusing geometry, pinching off droplets with each pressure pulse.	105
Pneumatic 'chopping'	2-20 Hz ¹²¹ , ~2-40 Hz ¹²² , ~3.4-13.8 Hz ¹²³	~0.5 - 500 pL ¹²¹ , 100-1000 pL ¹²² , ~1-500 pL ¹²³	Biocompatible, requires integration of second bonded pneumatic layer	Local temperature changes up to 50° are induced using a microheater, changing local capillary number.	121-123
Thermal viscosity change	not given	100-300 pL	Chip-integrated strategy, temperature changes will effect biocompatibility	Laser is focused at the droplet formation region, where local heating temporarily blocks interfacial movement at the leading edge.	109
Optical modulation	<i>O</i> (1) Hz	up to ~50% increase	Temperature changes will effect biocompatibility, requires optical toolkit	Local heating causes channel deformations on the order of 1 μm, changing local capillary number.	120
Thermomechanical valve	not given	up to ~50% decrease	Chip-integrated control, temperature changes will effect biocompatibility	A flow-focusing channel outlet is constricted using pneumatic actuation, changing local capillary number.	107
Pneumatic geometry control	1.2-3.4 kHz	~1-125 pL	Biocompatible, requires integration of second bonded pneumatic layer	Droplets are created in a flow-focusing geometry by spinning the entire device, causing fluid flow from the central to outer regions.	106
Lab-on-a-disk	~20-400 Hz	~5-22 nL	Can be combined with other on-disk components, total volume limited by that on-disk		98

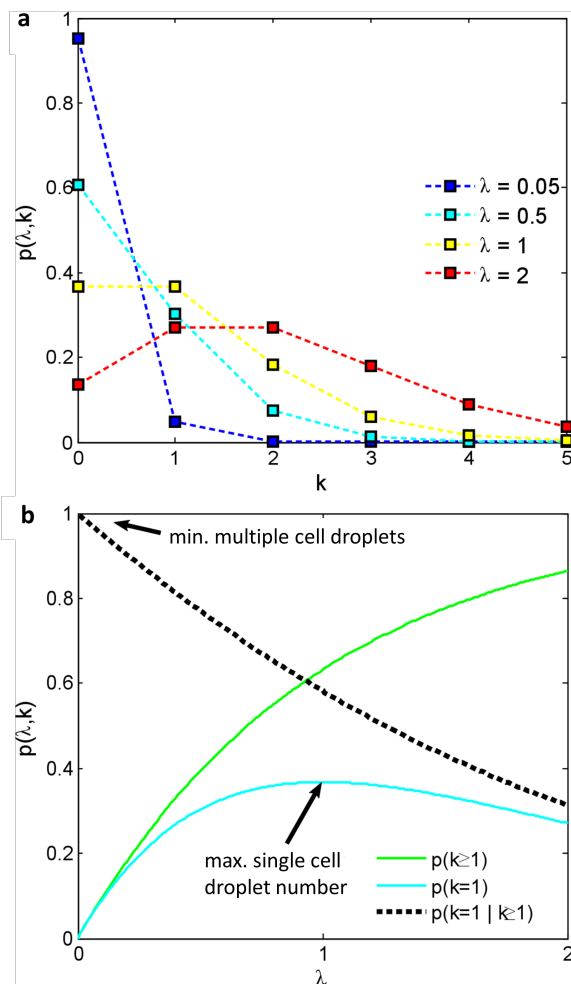


Fig. 8 The Poisson distribution is most commonly represented as in (a), where the proportion of droplets $p(\lambda, k)$ containing a given number of cells k is shown for different discrete values of λ . However, given that a defined number of cells per droplet are desired (most often one) for most applications, it makes sense to analyze the distribution according to the parameter that can be experimentally varied, λ , to determine the optimal cell concentration for given throughput and specificity requirements. (b) Shows the proportion of droplets that contain at least one cell, $p(k \geq 1)$, exactly one cell, $p(k = 1)$, and the proportion of droplets containing cells that contain exactly one, $p(k = 1 | k \geq 1)$. Single cell throughput is maximised when $\lambda = 1$, though at the cost of specificity, where only $\sim 58\%$ of droplets with cells and $\sim 36\%$ of all droplets will contain only one cell.

3.1 Passive encapsulation

A variety of cell encapsulation methods make use of either passively or actively formed droplets. Those methods using external pressure sources (syringe and pressure-driven pumps) comprise the bulk of work in the literature of cell

encapsulation, including several reviews on encapsulation and single-cell analysis^{62,79,80,124–127}. Fig. 7a shows an example of passive encapsulation as typically applied, where the physics of encapsulation are tied to those of droplet formation, such that cells are encapsulated when they comprise a portion of the fluid volume that is segmented at the droplet-producing geometry. As the number of cells per droplet volume can significantly affect the viability of a particular process – the apparent reaction kinetics could double if two, rather than one, cell were encapsulated in a droplet, for example – it is strongly desirable to have a measure of control over this parameter. In the case where encapsulated cells are both numerous and significantly smaller than the droplets (such as with encapsulated micron-sized bacteria, for example¹²⁸), the number of cells per droplet can reasonably be assumed to be representative of the volumetric concentration of cells¹²⁹. However, for single-cell analysis this is not the case, where only one cell should be contained within the droplet volume. If cells are distributed randomly in an aqueous solution, the quantity of cells per encapsulated volume is determined by Poisson statistics. As the Poisson distribution either governs cell encapsulation rates in these systems, or is addressed through the addition of system features that attempt to circumvent it, the Poisson distribution is now discussed in detail.

For suspended cells traveling through microfluidic channels, the spatial distribution and therefore the timing of their arrival at the site of droplet formation is essentially random for passive encapsulation. For high cell concentrations and large droplets, the random distribution of cells is not a significant barrier to encapsulate an approximately equal number of cells per droplet, provided it is desirable that each droplet encapsulates a large number, where the number of cells in a droplet can be approximated by a Gaussian distribution. However, for applications requiring single-cell analysis, only one cell should be encapsulated per droplet. Here, the reaction products, cell signaling and metabolic output of each cell are fully contained, and thus independently measurable. The issue at the heart of producing a large number of encapsulated single cells is that if the arrival of cells at the water-oil interface is random while the production of droplets is continuous, there is no way to guarantee that a droplet will contain only a single cell, or even any cells at all.

Although cells arrive at the droplet formation region randomly, it is still possible to probabilistically estimate the proportion of single cells that are encapsulated according to the Poisson distribution, which is applicable in the case where the average cell arrival rate is known and the arrival of individual cells occurs independently from other cells. While the arrival rate is readily measurable (from the cell concentration in the feed solution), the second assumption

460 does not strictly hold true, as two cells cannot inhabit the
 461 same volume. However, in the limiting case where the cellular
 462 volume fraction $\phi_s \ll 1$ (i.e. cells are sparsely distributed),
 463 where $\phi_s = \frac{\bar{Q}_c}{\bar{Q}_f}$, and \bar{Q}_c, \bar{Q}_f are the time-averaged volumetric
 464 flow rate of the cells and fluid flow rate, the assumption of
 465 independence is a valid one to make. Indeed, studies that
 466 have examined cell encapsulation with a randomly distributed
 467 feedstock in this limiting case have shown good agreement
 468 with Poisson statistics. Finally, the Poisson distribution is
 469 given by

$$p(k, \lambda) = \frac{\lambda^k e^{-\lambda}}{k!}, \quad (1)$$

470 where k is the number of particles in a droplet and λ is the
 471 average number of cells per droplet volume. More thoroughly,
 472 λ can be defined as the ratio between the volume fraction of
 473 cells in the pre-encapsulation solution ϕ_s and that of a droplet
 474 containing one cell, defined as $\phi_d \equiv \frac{\bar{V}_c}{\bar{V}_d}$, where the average cell
 475 and droplet volume \bar{V}_c and \bar{V}_d are constant for given oil-water
 476 flow rates and system geometry. Thus, λ can also be expressed
 477 as

$$\lambda = \frac{\phi_s}{\phi_d}. \quad (2)$$

478 The Poisson distribution is examined in Fig. 8. As is often
 479 represented in the literature, Fig. 8a shows the Poisson
 480 distribution for different cellular concentrations as measured
 481 by λ . What can be inferred from this representation is that the
 482 average number of cells per droplet will rise for increasing
 483 cellular concentrations with a maximum number fraction
 484 centered on λ – the distribution eventually approximates a
 485 Gaussian distribution with mean and variance of λ as $\lambda \rightarrow$
 486 ∞ – though for the range of cell concentrations used in
 487 single-cell encapsulation work ($\lambda < 1$), there is substantial
 488 variability in the number of cells that a given droplet might
 489 contain. A more useful representation of the distribution
 490 explicitly examines the proportion of droplets that contain a
 491 certain number of cells according to the parameter that the
 492 experimentalist can arbitrarily vary, i.e. λ . Solving $p(k, \lambda)$
 493 for the proportion of droplets that contain one cell ($k = 1$) and the
 494 proportion of cell-containing droplets that contain exactly one
 495 ($k = 1 | k \geq 1$), Fig. 8b shows the operational cell concentration
 496 range for single-cell encapsulation. Here, the choice of cell
 497 concentration in the range $\lambda = (0, 1]$ depends on the capability
 498 of downstream sorting or measuring processes to detect the
 499 number of cells per droplet. Unsurprisingly, throughput of
 500 encapsulated single cells is maximized when $\lambda = 1$, where
 501 $1/e$ ($\sim 37\%$) of droplets contain single cells, though at the
 502 expense of specificity, with 42% of droplets containing more
 503 than one cell. Towards the lower limit of concentration (and
 504 cell throughput), for example at $\lambda = 0.05$, only 5% of droplets
 505 will have cell(s), though $k = 1$ for 98% of these. It should
 506 be emphasized, however, that regardless of λ , the majority of

droplets will not contain single cells, requiring downstream
 sorting to produce an exclusively single-cell droplet emulsion.
 Having a sufficiently high percentage of single-cell droplets is
 an important factor, for example, in cell-pairing applications
 where two droplets containing individual cells are merged; in
 the case where $\lambda = 0.05$, only 0.25% of combined droplets
 will contain two cells if these droplets are merged at random.

3.2 Active encapsulation

Given the nascent stage of active methods for droplet
 production, the predominance of passive encapsulation
 methods is somewhat justified, though there are several
 methods that show promise for improving aspects of the
 cell encapsulation process. Acoustic, electrical, optical or
 magnetic forces can be used to direct cells or particles to the
 droplet-producing region and actively create droplets when
 cells or particles approach the oil-water interface. Active
 methods for droplet production have the added advantage
 that the same forcing mechanism that is used to displace the
 oil-water interface to produce droplets also has the potential
 to act on solid-liquid interfaces that direct cell motion in
 the vicinity of the interface. For example, Collins *et al.*,
 utilized a focused travelling SAW to both concentrate particles
 in solution at a water-oil interface and subsequently create
 a droplet encapsulating those particles (Fig. 7b)¹⁰¹ and to
 control the ejection of particles in a single phase¹³⁴. In an
 alternative approach, Wang *et al.* fixed a piezoelectric actuator
 to the end of a glass capillary¹³⁰. By pulsing the actuator, one
 or more droplets containing a number of cells could be ejected.
 Other novel methods for encapsulation include the formation
 of hydrodynamically-thinned bridges, which then segregate
 into droplets (some of which contain cells), as shown in Fig.
 7c¹¹⁵, the concentration and separation of magnetic particles
 in droplets^{133,135,136}, or the use of a centrifuge to eject and
 segment a cell-containing fluid from a glass capillary¹³².
 These non-deterministic encapsulation methods are compared
 in Table 2.

As currently employed, however, the encapsulation rate
 using these methods is relatively limited. In contrast to
 passively formed droplets which can be formed at kHz
 rates, the encapsulation rate using most active techniques
 is orders of magnitude lower, even if the fact that only a
 fraction of passively produced droplets will contain single
 cells is taken into account. Optical positioning and
 subsequent encapsulation has been demonstrated at only
 sub-Hz frequency, for example¹³⁷. For mass production of
 single-cell emulsions useful for high-throughput screening
 applications, encapsulation rates at least on the order of
 passively produced encapsulated droplets are required (>100
 Hz), a production rate that is typical of high-throughput
 screening platforms³⁹. Interestingly, active techniques have

Table 2 Representative non-deterministic on-demand and other novel encapsulation methods

Method	Encapsulation rate	Advantages/ Disadvantages	Mechanism	Ref(s).
On-demand methods				
Focused surface acoustic wave	<1 Hz	On-chip combined pre-concentration and droplet ejection mechanism, limited throughput	Acoustic pressure translates 10 μm particles to a water-oil interface prior to droplet formation.	101
Hydrodynamic bridges	<1 Hz	Simple to perform, limited throughput	Water droplet between two hydrophilic glass plates is expanded, forming an unstable fluid bridge that produces satellite droplets upon breakup.	115
Pulse-inertia	2-256 Hz	Effective single-cell encapsulation	An actuator expels individual droplets, some of which contain cells. Droplet size is tunable in order to maximize droplets containing a single cell.	130
Other methods				
Centrifuge	N/A	Simple method using common laboratory tools	A cell solution is forced through a nozzle at the base of a microtube insert in a lab centrifuge, producing momentarily airborne droplets that form hydrogel microbeads in a CaCl_2 solution. For related work see Ref. 131.	132
Magnetic concentration	<30 Hz	Requires bound magnetically active particles	Magnetic field is used to pre-concentrate cells bound to magnetic particles prior to droplet formation.	133

demonstrated phenomenal actuation rates in applications other than encapsulation. For example, Wu *et al.* were able to independently sort fluorescently-labelled lymphoma cells at rates of up to 20 kHz in a pure-aqueous media using pulsed-laser excitation¹³⁸. Similarly, Franke *et al.* used a fluorescence-activated, localized SAW field to sort particles, cells and droplets at kHz rates^{139,140}. Active methods have yet to achieve similar rates for cell encapsulation, though the throughput in cell sorting achieved by active methods demonstrates the potential of active methods for this application. Given the high-speed actuation that is possible using these methods, it is expected that active techniques will soon be applied to the purpose of single-cell encapsulation in two-phase systems. Indeed, if recent patents are anything to go by, a system employing pulsed laser cavitation (in a similar setup to that in Wu *et al.*¹³⁸) should demonstrate this in the near future¹⁴¹.

4 Deterministic single cell encapsulation

As discussed in Section 1, the random distribution of cells is a serious impediment to the efficient production of single-cell droplets. To circumvent the limitations posed by Poisson statistics, several approaches have been presented. These include the production of single cell emulsions by sorting droplets after they have been passively created, inertial ordering of cells prior to encapsulation and on-demand cell encapsulation. Examples of these methodologies are summarized in Table 3. It should also be noted that another deterministic method has been demonstrated, where

gel particles are closely packed prior to encapsulation so that they are released at a relatively constant rate^{152,153}. However, this method has limited applicability to cells, which are far more likely to block channels if their concentration is too high.

4.1 Single-cell emulsions by sorting

One route to obtaining high purity single-cells emulsions is to separate encapsulated cells from a stream of droplets, the vast majority of which are empty (in the case where $\lambda \ll 1$). Post-encapsulation sorting draws on the large body of work in cell, particle and droplet sorting, where cells can be sorted according to their physical dimensions, electromagnetic susceptibility, or mechanical and optical properties. Active sorting approaches, including those demonstrated in single-phase systems, make use of acoustic fields^{139,140,154–158}, optical forces^{159–161}, and electric fields^{154,162,163}, or purely hydrodynamic ones such as deterministic lateral displacement (DLD)^{144,164}, shear-induced migration¹⁴⁷ and inertial microfluidics in spiral microchannels¹⁶⁵. Many of these same hydrodynamic and active mechanisms have been utilized for high-frequency single-cell droplet sorting applied downstream of the droplet generation zone, though it is conceivable that any of them could be applied for this purpose. Active methods offer the most flexibility in sorting droplets, where any measurable quantity can be used for sorting. Using a continuously applied standing wave acoustic field, Nam *et al.* were successful in sorting alginate droplets according to the number of cells contained, where those with more cells migrate more

Table 3 Deterministic methods for single-cell encapsulation

Method	Droplet sorting/production rate (Hz)	Encapsulated cell(s) rate (Hz)	Efficiency (%)	Advantages/Disadvantages	Mechanism	Ref(s)
Post-encapsulation sorting						
Dielectrophoresis FACS	~2 kHz	~0.4 kHz (single cells)	>99% sorting efficiency	Rapid sorting, requires optical sensing apparatus	Dielectrophoretic force directs optically analyzed droplets into a separate outlet. For related work see Refs. 39 and 68.	65, 142
Travelling acoustic wave FACS	3 kHz	<3 kHz	not provided, near 100% sorting presumed	Rapid sorting, requires optical sensing apparatus	Acoustic force/streaming directs optically detected cells into a separate outlet. For related work see Ref. 139.	140
Standing acoustic wave continuous	~40 Hz	<40 Hz	97% of desired cell density beads separated	No sensing equipment required, sort on non-size parameter	Beads containing different numbers of cells exhibit differential migration in an acoustic field by virtue of their different average densities.	143
Deterministic lateral displacement	5 kHz	~2-200 Hz	~60-78% of sorted droplets contain single cells	Passive sorting, requires large chip area for DLD array	Droplets containing cells are larger, and therefore sorted from empty droplets in a DLD array. For an explanation of DLD principles, see Ref. 144, and for related work see Ref. 145.	146
Shear migration	not provided	20-160 Hz	96±3% of sorted contain single cells, 20-30% false negative (typical)	Passive sorting, optimized flow rates required	Cells initiate the formation of larger droplets in the jetting regime, which are then sorted from empty droplets via differential shear-induced migration rates.	147
Pinched flow fractionation	<200Hz	not provided	~50% of sorted contain single cells	Passive sorting, though low flow rates on the order of <i>ml/h</i> used	A large droplet containing multiple cells is broken up into smaller droplets using a microgroove structure, with smaller (empty) droplets separated from larger, cell-containing ones via pinched-flow fractionation.	148
Inertial ordering						
Straight microchannel	14.9 kHz	12 kHz	~80% contain single cells	Rapid throughput, tuned flow rates and concentrations required	Evenly-spaced cells arrive at a droplet generating geometry at a similar rate to that of droplet production due to inertial ordering.	149
Dean-flow microchannel	2.7 kHz	~2.2 kHz	~80% contain single cells	Rapid throughput, tuned flow rates and concentrations required	Similar to straight-microchannel ordering, except Dean flow biases collection into a single focused line. For related work see [33].	150
Active detection and encapsulation						
Cell sensing and pico-ejection	<1 Hz	<1 Hz	73±11% of single cells are ejected	Active single-cell droplet ejection with potential for throughput, low rate demonstrated	Suspended cells in flow are sensed using a local impedance measurement, whereafter they are dispensed with individual depressions of a piezoelectric actuator.	151
Optical trapping	<1 Hz	<1 Hz	100% of translated cells ejected	High cell selectivity, requires operator with low potential for throughput	Cells or sub-cellular components are brought to the oil-water interface using optical tweezers prior to droplet formation.	137

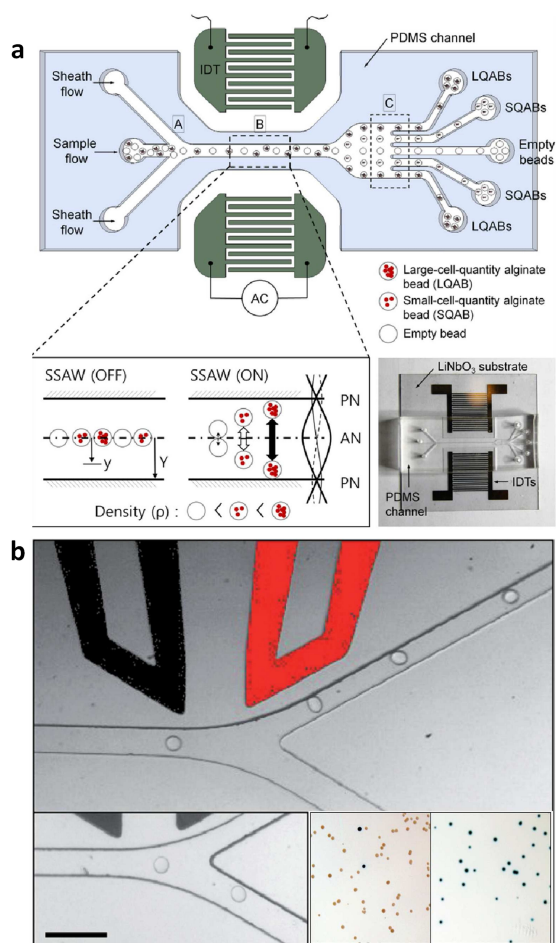


Fig. 9 Actively applied forces can be used to sort droplets on parameters other than their dimensions. (a) Using a standing SAW field, Nam *et al.* continuously sorted alginate hydrogel beads according to the number of cells contained. Reproduced with permission from reference 143, copyright 2012, AIP publishing. (b) Localized DEP can sort individual droplets according to a measured property such as fluorescence or other optically measured parameters; upper image shows droplets being actively directed upwards or passively allowed downwards (lower left), where the set of images in the lower right shows the plated cell cultures from unenriched (left) and enriched (right) droplet populations. Scale bar is 100 μm . Reproduced with permission from reference 142, copyright 2009, Royal Society of Chemistry.

613 rapidly to a standing wave nodal position by virtue of their
 614 marginally greater density and subsequent acoustic contrast
 615 factor¹⁴³ (Fig. 9a). Importantly, employing such a mechanism
 616 opens up the possibility of sorting droplets based on the
 617 quantity of cells that they contain, and not just the presence
 618 or absence of cells. On-demand sorting methods such as
 619 those using localized fluorescence-activated dielectrophoretic
 620 (DEP) forces can further expand the versatility of cell sorting

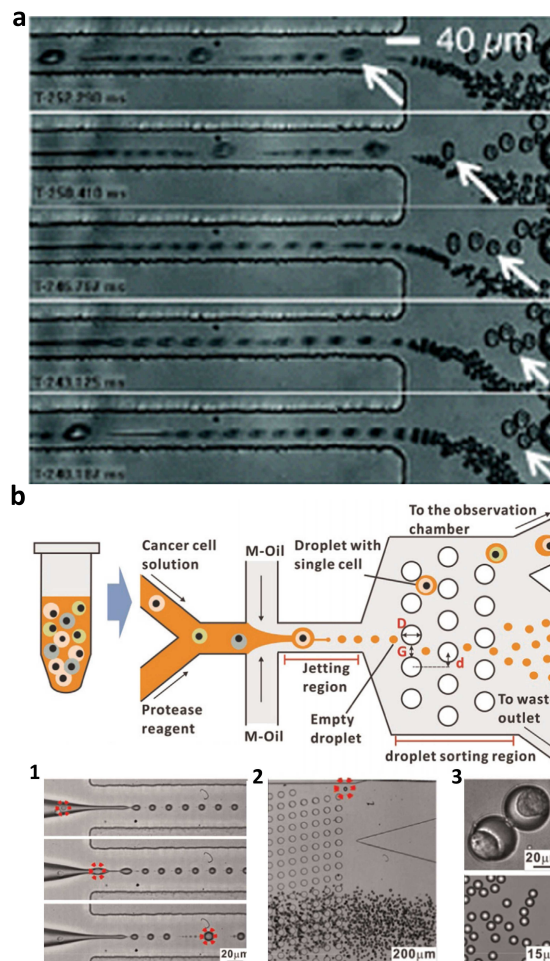


Fig. 10 Passive post-encapsulation sorting methods separate encapsulated cells from empty droplets based on the substantial size differences between the two. If produced in the jetting regime, where the width of the fluid thread is on the order of the cell dimensions, larger droplets containing cells can be sorted from the empty ones using (a) shear-induced migration and pinched-flow fractionation (PFF) or (b) mechanical-pillar deterministic lateral displacement (DLD). (b-1) In both (a) and (b), larger cell-containing droplets are produced when a cell serves as a nucleation site for Rayleigh-Plateau instabilities in the jetting regime. (b-2) shows the separation of numerous small droplets from cell-containing droplets (circled in red) in a DLD array, while (b-3) shows the substantial size differences in the sorted cell containing (top) and empty (bottom) droplets. (a) Reproduced with permission from reference 147, copyright 2008, National Academy of Sciences. (b) Reproduced with permission from reference 146, copyright 2015, Elsevier.

to include a measure of cell function. For example, Agresti *et al.* used a DEP-based sorting device to separate droplets (containing cells) expressing a threshold level of horseradish

624 peroxidase⁶⁵ (Fig. 9b). Localized acoustic fields have
625 also been used for the sorting of cells and droplets¹⁶⁶, at
626 rates of up to 3 kHz¹⁴⁰. Other excellent examples of
627 microfluidic fluorescence-activated cell sorting have been
628 reported^{54,54,142,167–169}.

629 The addition of a fluorescent or chemical reporter can
630 increase sensitivity to the detection of cells and their
631 function^{170–173}, however label-free detection is also feasible,
632 permitting the high-speed analysis of cells without the
633 requirement for added reporters. These on-chip detection
634 methods, including optical and electrical ones, are covered
635 in a recent review article¹⁷⁴. Though many have not yet
636 been utilized in conjunction with post-encapsulation sorting,
637 it is worthwhile discussing detection methods that could
638 be in future work. Kemna *et al.*, for example, were
639 able to detect 80% of encapsulated cells at >100 Hz by
640 measuring the difference in electrical impedance between
641 a droplet with and without a cell that passes above a set
642 of parallel electrodes¹⁷⁵; the addition of an active sorting
643 system post-cell detection could be a viable method for
644 the production of single cell droplets. Mass spectrometry,
645 while requiring the requisite equipment, has the ability
646 to measure fine-grained information about cells and their
647 local environment¹⁷⁶. Shigeta *et al.* were able to detect
648 femtogram amounts of trace elements (Selenium, Zinc, etc.)
649 in yeast cells at 50 Hz rates using inductively coupled
650 plasma mass spectrometry (ICP-MS), useful for the detection
651 of metals, and similar to work by Smith *et al.* where
652 protein concentrations were detected in droplets at 150 Hz
653 using electrospray ionization mass spectrometry (ESI-MS)¹⁷⁷.
654 However, the need to create an aerosol prior to detection
655 – mass spectrometry requires the input of sample ions in
656 the gas phase – with these two methods precludes the use
657 of a two-phase system wherein cells can be encapsulated
658 pre-aerosol formation. Künster *et al.* avoids the need to
659 create an aerosol while making use of two-phase encapsulated
660 cells by first depositing them on a surface-treated substrate
661 to trap individual droplets, whereupon mass spectrometry is
662 performed on a droplet-by-droplet basis after the evaporation
663 of the aqueous and volatile oil phases. Direct optical
664 detection is more readily integrated into microfluidic systems,
665 given the transparent nature of the materials typically used
666 (glass, PDMS, PMMA, etc.), which permits in-line analysis
667 to increasingly refined levels; Yu *et al.* demonstrated the
668 detection of 10 nm-scale bacteriophages in droplets containing
669 *Escherichia coli* via optical scattering¹²⁸. In a label-free
670 analogue to the work from Refs. 39, 65, 68 and 142, Zhang
671 *et al.* integrated high speed optical detection to perform
672 growth-dependent enrichment of encapsulated bacteria using
673 electrical sorting at >100 Hz¹⁷⁸.

674 Hydrodynamic methods can be used to sort droplets on
675 the basis of their size, where the presence of a cell in a

droplet alters its dimensions. In one avenue for producing
676 differently-sized droplets in this manner, a cell in a thinning
677 capillary thread (produced in the jetting regime) serves as
678 an early nucleation site for Rayleigh-plateau instabilities,
679 resulting in the production of droplets larger than those
680 that do not contain cells (Fig 101). Chabert & Viovy
681 demonstrated post-encapsulation sorting via shear-induced
682 migration of larger droplets to the channel center and a form
683 of pinched-flow fractionation (PFF)¹⁴⁷ (Fig. 10a), a sorting
684 method used similarly by Um *et al.*, though to a lower single
685 cell enrichment level¹⁴⁸ (see Table 3). Alternatively, Jing *et al.*
686 made use of a DLD pillar array for post-encapsulation
687 sorting, where larger droplets containing cells were translated
688 at an angle to the flow, and thus sorted from the smaller
689 empty droplets (Fig. 10b)¹⁴⁶. While encapsulating in the
690 jetting regime has the advantage of pre-ordering cells in the
691 thin fluid thread, a shortcoming of such an approach is that
692 the resultant droplet dimensions are limited to volumes on
693 the order of cells if the size difference is to be sufficient for
694 hydrodynamic sorting. There is, however, at least one other
695 avenue for inducing cell-dependent droplet size differences.
696 Joensson *et al.* were able to shrink droplets containing yeast
697 cells via osmosis in an lipophilic phase in which water is
698 partially soluble, whereafter the cell-containing droplets were
699 sorted using DLD¹⁴⁵. Though other methods of size-based
700 droplet sorting have been reported, including the use of
701 size-selective patterned tracks^{179,180} and a differential fluid
702 shear mechanism¹⁸¹, DLD and PFF sorting methods present
703 the best opportunity for high-throughput purely hydrodynamic
704 post-encapsulation cell sorting.
705

Active methods as employed have improved sorting
706 efficiency and speed compared to passive methods, as noted in
707 Table 3. Baret *et al.*, for example, were able to sort individual
708 droplets at rates up to 2 kHz with error rates of 0.01–1%¹⁴²,
709 comparing favourably with false positive and negative rates of
710 approximately 4% and 20%, respectively, in the shear-induced
711 migration sorting reported by Chabert *et al.*¹⁴⁷. Active sorting
712 also permits the detection of not only the presence of cells,
713 but also of cell properties, which when combined with a low
714 error rate is especially important in applications involving rare
715 cells. Efficiently performed directed evolution, for example,
716 requires that mutations in a small proportion of cells can be
717 positively selected for; active forces are used here as their
718 activation can be coupled with the optical detection of desired
719 cell traits. Active post-encapsulation cell sorting devices
720 can also make use of entirely separate droplet formation
721 geometries that can tune the droplet size to a wide range of
722 volumes – potentially on an entirely different device – without
723 the need to couple flow rates and droplet volumes between
724 droplet generation and sorting functions. On the other hand,
725 improved sorting fidelity and flexibility comes at the cost of
726 increased device complexity, where multiple structures need
727

728 to be aligned, calibrated and driven by external equipment.

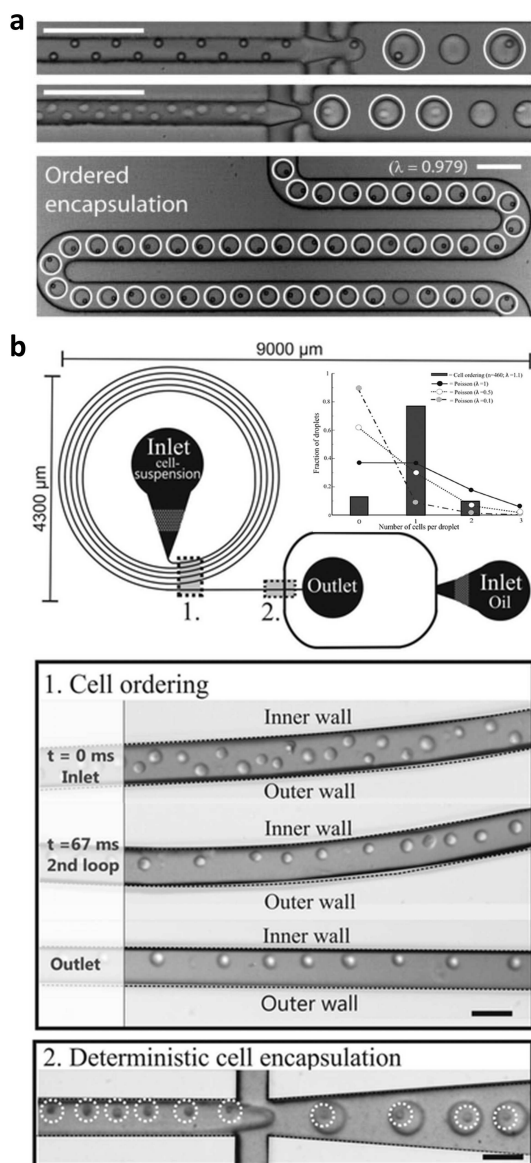


Fig. 11 Inertial ordering has the potential to drastically increase the proportion of droplets produced that contain single cells. Using (a) straight or (b) curved microchannels at suitable Reynolds numbers, particles can be focused at discrete locations laterally and ordered longitudinally. Both inertial ordering systems demonstrate significant improvement in single-cell capture efficiency as compared to what might be expected of randomly arriving cells or particles (top right of (b)). (a) Reproduced with permission from reference 149, copyright 2008, Royal Society of Chemistry. (b) Reproduced with permission from reference 150, copyright 2012, Royal Society of Chemistry. Scale bars denote (a) 100 μm and (b) 50 μm .

4.2 Inertial cell ordering

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Though sorting methods have the demonstrated ability to produce high-purity single cell emulsions, their throughput is fundamentally limited by the rate at which single cells are initially encapsulated, which itself is determined by Poisson statistics. For typical cell concentrations ($0.01 \lesssim \lambda \lesssim 0.1$), only a few percent of droplets that are produced will contain cells, with the sorted empty droplets volumes being wasted. While this waste is more often than not a secondary concern, where the total volume of wasted picoliter scale droplets might be on the order of microliters, the aggregate time spent producing them in a given droplet geometry reduces the maximum throughput by at least an order of magnitude.

A sensible solution to increase throughput is to employ a method whereby each droplet that is produced contains a single cell; if cells arrive at the formation geometry at the same rate that droplets are produced, every droplet will contain one cell. To this end, Edd *et al.* demonstrated a method they termed inertial ordering to focus particles and cells at defined positions both laterally and longitudinally in a rectangular channel prior to droplet formation (Fig. 11a)¹⁴⁹. Stable particle positions are produced laterally where the force resulting from the parabolic-profile shear gradient (pushing particles to the channel edges) is balanced by that of the wall interaction force^{124–126}, the latter analogous to the ground effect utilized by some aircraft¹⁸². Longitudinally, particles are ordered by what has been termed a hydrodynamic repulsion effect resulting from inter-particle interactions^{127,183–185}. It has been demonstrated that this hydrodynamic effect is a result of reversing fluid streamlines in the vicinity of a rotating particle, repelling nearby particles¹⁸⁵. Interestingly, this repelling effect can be manipulated, where the distance between neighboring particles is a function of the channel width¹⁸⁶, though as channel dimensions are difficult to modify in-situ, the encapsulation rate must be controlled by fine-tuning of the input flow rates.

Although Edd and co-workers produced staggered particles and cells on either side of a channel, it is also possible to focus these particles into a single line. By introducing asymmetric curve(s) in the channel geometry a secondary Dean flow is produced that reduces the number of stable equilibrium positions. A commonly employed method to produce this asymmetry and therefore inertial focusing makes use of curved channels¹⁸³. Kemna *et al.* and Schoeman *et al.* demonstrated lateral focusing and longitudinal ordering in spiral microchannels, where cells were similarly encapsulated such that the majority of droplets produced contain single cells^{33,150} (Fig. 11b). An advantage of inertial ordering is that individual cells can be encapsulated at throughputs orders of magnitude more than without ordering. Indeed, in the

780 studies by Edd, Kenma and Schoeman the cell concentration
 781 can approach the theoretical maximum single-cell output
 782 with input concentrations near $\lambda = 1$. Furthermore, being
 783 able to encapsulate cells deterministically permits activities
 784 that would be impractical without pre-ordering. Lagus
 785 & Edd and Schoeman *et al.* were able to demonstrate
 786 cell-pair co-encapsulation using two separate ordered-cell
 787 inlets that intersect at a flow-focusing geometry^{33,187}; without
 788 pre-ordering the proportion of droplets that contain one
 789 of each particle or cell would be significantly lower.
 790 Despite the advantages conferred by inertial ordering for
 791 single-cell encapsulation, in practice this method can be
 792 difficult to implement, especially for a cell population with
 793 heterogeneous characteristics. Moreover, for one cell to be
 794 encapsulated per droplet, the rate at which cells arrive at the
 795 droplet forming geometry must be equal to the rate of droplet
 796 formation, requiring finely balanced flow rates for aqueous
 797 and oil inflows. Finally, inertial ordering requires flow rates
 798 higher than typically used in microfluidic systems, with $1 < Re$
 799 < 300 and flow velocities on the order of ~ 0.1 m/s, limiting
 800 the range of other microfluidic processes this method can be
 801 coupled with.

802 4.3 On-demand encapsulation

803 An emerging methodology for the encapsulation of single
 804 cells combines the detection of cells in a constant flow with the
 805 ability to produce droplets on-demand. In this methodology,
 806 single cell droplets are produced when an automated system
 807 detects the presence of a cell and triggers the production of a
 808 droplet. This differs from the case demonstrated a decade ago,
 809 where optical trapping was used to guide an individual cell to
 810 the fluid-fluid interface, a methodology that is not inherently
 811 suited to even moderate-throughput applications¹³⁷. Though
 812 to date this detection and ejection methodology has been
 813 developed only for water-air phase systems, it could be equally
 814 successful in a water-oil one; this phase combination could
 815 be effectively be obtained by ejecting droplets through air
 816 into an oil reservoir. In an example of single-cell printing,
 817 Schoendube *et al.* used a set of electrodes to detect the local
 818 electrical impedance change induced by the presence of a cell
 819 in a continuous flow, ejecting a single cell when it arrived
 820 at the dispensing port¹⁵¹. Here, a piezoelectric actuator was
 821 pulsed after a delay period corresponding to the flow rate in the
 822 cell channel to eject a single droplet containing the detected
 823 cell. Automated optical detection permits the same activity,
 824 though in those cases demonstrated droplets are produced
 825 continuously, where waste droplets are ejected into a separate
 826 reservoir¹⁸⁹. Leibacher *et al.* and Gross *et al.* made use
 827 of a shuttered vacuum source to sort waste droplets, where
 828 Leibacher *et al.* further refined the system using an acoustic
 829 standing wave to align cells prior to ejection, thus increasing

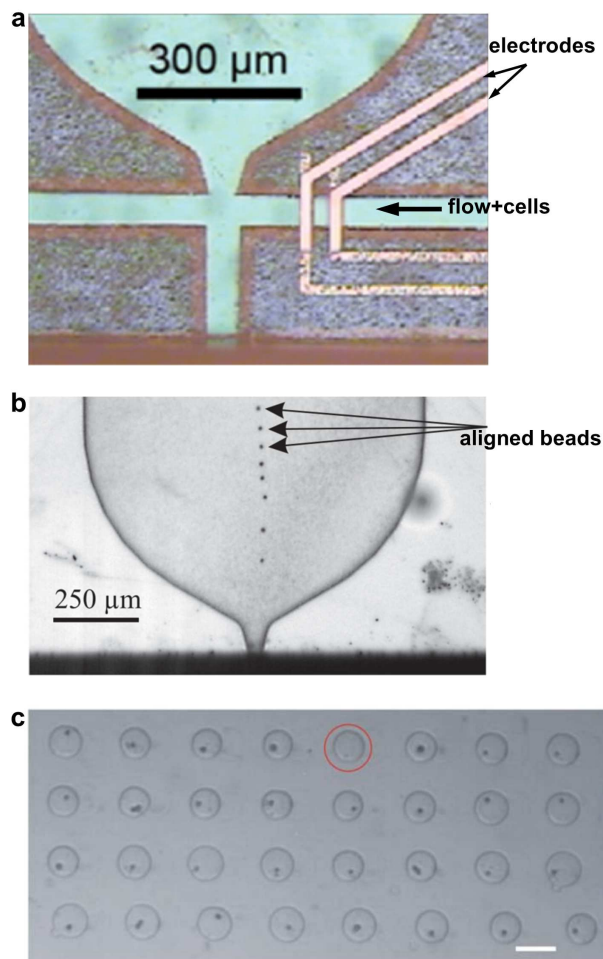


Fig. 12 Active single-cell encapsulation has been demonstrated in a limited number of cases, where detection methods are used to determine the presence of cells. In (a), the passage and velocity of a cell is measured in real-time, triggering the ejection of a single encapsulated cell after a delay. Reproduced with permission from reference 151, copyright 2015, AIP publishing. (b) Automated optical detection is also possible, and when combined with a method for aligning particles or cells, can improve the encapsulation efficiency. Reproduced with permission from reference 188, copyright 2015, AIP publishing. (c) Using these systems, single-cells can be ejected into microwell arrays. Scale bar is 200 μm. Reproduced with permission from reference 189, copyright 2011, Royal Society of Chemistry.

detection and therefore encapsulation efficiencies^{188,190}. Fig. 12 shows the geometries of the single-cell printing systems utilized in these studies.

5 Recent applications

The value of encapsulated cells is reflected in the wide range of applications where they have been used. This includes recent applications in diagnostics and therapeutics, which are briefly discussed here. A growing area for the use of encapsulated cells is in tissue engineering, where cells are encapsulated in a hydrogel matrix that effectively serves as an extracellular matrix¹⁹¹. Bulk hydrogel-cell composites have been used extensively for in-vivo tissue generation, for example being used to assist in neural regeneration after injury¹⁹². However, there is growing recognition of the value in encapsulating cells in discrete quantities, in individual hydrogel droplets rather than en-masse, permitting the preparation of non-homogeneous engineered tissues. Here, cells are encapsulated in an almost identical process to oil-water systems, except that by using a photo- or chemo-catalyzed hydrogel the bead can be stably suspended in an aqueous phase.^{79, 193–195} For example, Lin *et al.* used optical forces to direct the positions of alginate beads containing different densities of chondrocytes in order to mimic the spatial gradient of these cells in articular cartilage¹⁹⁶. Other benefits of encapsulating cells include improving the surface area-to-volume characteristics for nutrient diffusion, preventing or mediating the immune response to cells and maintaining pluripotency of stem cell culture^{197,198}. Interestingly, encapsulation also allows cells to be used effectively as therapeutic agents in their own right, where encapsulated cells hold substantial promise for delivery of cell-produced drugs. Here, a (potentially engineered) cell is used to emit the desired biopharmaceutical, where local nutrients are used to produce the drug on-site and where resulting metabolites can freely diffuse through the hydrogel matrix surrounding the cell(s). These benefits are further enhanced in a core-shell capsule, where a hydrogel bead is encased in a secondary polymer shell to prevent ingress or egress of cells¹⁹⁹. For a thorough discussion of many of these applications, the reader is advised to view an excellent review on the topic⁶¹.

Encapsulated cells are uniquely suited to applications in high-throughput screening, which leverages the ability to produce, screen and sort droplets in microfluidic systems at kHz rates to select for desired cell characteristics, often mediated by a fluorescent reporter. Distinguishing this from single-phase FACS, encapsulation enables the long-term incubation of cells in a unique microenvironment so that cells can be individually assessed on their exogenous products rather than only endogenous ones. It is then unsurprising that encapsulated cells have especially found application in the screening and enrichment of enzymes produced by cells; screening and selection of cells that produce these enzymes can be used to improve their properties, important as enzymes

are widely used in commercial applications²⁰⁰. For example, Ostafe *et al.* used two separate microfluidic devices one to encapsulate and a separate one to sort in order to select for cells expressing high cellulase activity, demonstrating a 300-fold enrichment over a single pass¹⁶⁸. This scheme can also be performed over several passes, where cells selected from one population are used to generate offspring for subsequently screened generations, in a process justly termed directed evolution. This has been used to vastly improve the enzymatic activity of horseradish peroxidase through the evolution of mutants⁶⁵ and enrich the quantity of transformed bacteria²⁰¹. Sjostrom *et al.* took the further step of, rather than relying on natural mutation rates and variations in activity, creating a library of UV-mutated yeast prior to sorting¹⁷. A potential drawback of constant throughput screening is the inability to track the life cycle of individual cells over multiple passes. However, it is not necessary to have encapsulated cells move to assay their activity. Shemesh *et al.* encapsulated individual cells in-situ to observe their metabolic activity over several hours²⁰².

6 Summary and prospects

A number of droplet production methods for the purpose of microfluidic encapsulation have been presented and discussed. As is often the case in engineering enterprises, the particular method best suited for a given application is a function of the operational parameters of that application, though naturally only methods that have reached a sufficient level of development can be considered. To date, the majority of studies employing cell encapsulation and single-cell analysis have utilized passive encapsulation methods using pressure-driven flow in droplet forming geometries, where droplet production can occur on the order of kHz. However, despite this impressive throughput, Poisson statistics fundamentally limit the rate at which a reliable number of cells can be encapsulated. Up to a point, higher input cell concentrations will increase single-cell throughput, though at most only 37% of droplets will contain only one cell, and therefore at least 67% of droplets are either wasted and/or require removal, with the result that the maximum throughput of encapsulated cells is an order of magnitude lower than the droplet production rate.

Inertial ordering methods have demonstrated the ability to vastly improve single-cell encapsulation efficiencies up to 80%, although they are limited in their range of applications due to practical constraints; high flow rates and specific cell concentrations are required to achieve the longitudinal ordering needed. These constraints strongly restrict the types of systems that this droplet production method can be directly integrated with. Additionally, even pre-ordering of cells prior to encapsulation will leave a substantial proportion of droplets

that do not contain the requisite number of cells, which may be undesirable for many applications. Passive methods have been developed for post-encapsulation sorting based on size, but they too leave a substantial proportion of droplets that are either unsorted or wrongly allocated. Similarly, for applications the cell waste resulting from lossy sorting methods may be unacceptable.

On the other hand, active sorting methods have demonstrated the ability to sort droplets according to their contents with near 100% fidelity, and can be applied for parameters other than size, including cellular activity and cell number, with sorting rates up to 10 kHz. Furthermore, though less developed for this application, active methods have the potential to address many of the shortcomings of passive droplet production and encapsulation systems. With these methods, forces are generated near fluid-fluid interfaces for on-demand droplet production, with similarly high droplet production rates realized in some systems. When coupled with systems to detect the presence of cells, these methods will have the ability to similarly encapsulate droplets on-demand to directly produce near-perfect single-cell emulsions without the need for downstream sorting. Though a truly high-throughput on-demand single-cell encapsulation system has yet to be realized, it is expected that the future development of these active methods will substantially improve the performance of applications where encapsulated single-cells are required.

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