



Surfactant-induced coagulation of agarose from aqueous extract of *Gracilaria dura* seaweed as an energy-efficient alternative to the conventional freeze-thaw process

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1 **Surfactant-induced coagulation of agarose from aqueous extract of *Gracilaria dura***
2 **seaweed as an energy-efficient alternative to the conventional freeze-thaw process**

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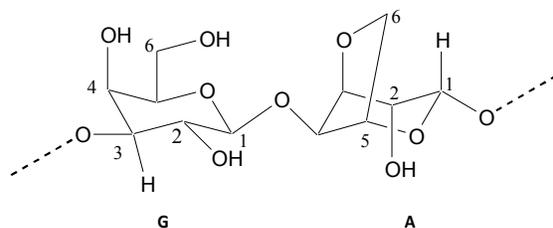
17 Surfactant-induced coagulation of agarose from alkali-treated *Gracilaria dura* seaweed extract
18 (SE) is reported. The new approach, which was suitable for linear galactans with low sulphate
19 content, dispensed with the traditional energy intensive process of “freeze-thaw” employed for
20 product isolation from extract. Only nonionic surfactants were effective and detailed studies
21 were undertaken with octyl phenol ethoxylate (Triton X-100). The coagulated product was
22 washed successively with water and water-isopropyl alcohol (IPA) to yield a fine powder of
23 agarose in 13-15% yield (with respect to dry biomass). The product exhibited excellent
24 properties (sulphate content: 0.2% w/w); degree of electro-endosmosis: 0.13; gel strength: 2200

25 g cm^{-2} (1% gel, w/v); gelling temperature: $35 \pm 1^\circ\text{C}$ essential for demanding molecular biology
26 applications, and the desired gel electrophoretic separation of DNA and RNA was
27 demonstrated. It was further confirmed that there was no degradation of the nucleic acids in the
28 gel. The agarose-depleted extract, along with water washings, was subjected to reverse osmosis
29 to recover the surfactant in concentrated form for its subsequent reuse. An assessment was
30 made of energy savings from the improved process.

31
32 **Keywords:** *Gracilaria dura*, Agarose, Surfactant, Preferential precipitation, Improved process,
33 Nucleic acid separation

35 Introduction

36 Agarose is a purified linear galactan hydrocolloid isolated from agar or agar-bearing marine
37 algae prepared by the purification of agar. Agar may be depicted by the structural formula
38 shown below. The structure comprises alternating D-galactose sub-unit (G) and 3,6-



43 anhydro-L-galactopyranose sub-unit (A) linked by α -(1 \rightarrow 3) and β -(1 \rightarrow 4) glycosidic bonds.
44 A small fraction of the hydroxyl groups at 4 position of G and/or 2 position of A is present
45 in sulphated form.^{1,2} Various grades of agarose are reported, with sulfate content ranging
46 from 0.10 to 0.35% (w/w). Agarose forms a gel matrix in aqueous medium that is ideal for
47 diffusion and electro-kinetic movement of biopolymers. This makes it suitable for

48 applications in molecular biology, electrophoresis and cell culture. Agarose is commonly
49 prepared from superior quality agar or agar-bearing marine algae, such as *Gelidium spp.*,
50 *Gracilaria spp.*, *Acanthopeltis spp.*, *Ceramium spp.*, *Pterocladia spp.*, and *Campylaeophora*
51 *spp.*¹ The red seaweed, *Gracilaria dura*, from Indian seawater has been reported recently as
52 a promising bio-resource for its preparation.¹

53 The process of agarose preparation involves (i) alkali pre-treatment of the seaweed
54 followed by autoclaving, (ii) subjecting the aqueous extract to several cycles of freeze-thaw
55 to isolate the product, and (iii) purifying the product further through solvent/chemical
56 treatment and/or chromatography to eliminate residual impurities.^{1,3-6} The energy intensive
57 nature of the process, costly purification steps and long batch time are prime reasons
58 behind the high cost of the product.

59 The present work emanated from a desire to explore alternative means of isolating
60 agarose from seaweed extract. Rheological properties of agar sol and gel in presence of
61 various cationic, anionic and nonionic surfactants have been reported previously.⁷ The gel
62 strength, viscosity, rigidity, gelling temperature and melting temperature were observed to
63 increase in presence of ionic surfactants whereas nonionic surfactants had the opposite
64 effect. The apparent weakening of gel network with nonionic surfactant prompted us to
65 exploit the phenomenon towards the development of an alternative process of product
66 isolation from seaweed extract. The present study reports the isolation of agarose from *G.*
67 *dura* seaweed extract through spontaneous coagulation mediated by nonionic surfactants.
68 Simplification of the downstream operations of purification and recycle of the surfactant
69 were additional merits of the process. The efficacy of the product obtained through the new
70 process was tested through gel electrophoresis of nucleic acids.

71 **Experimental**

72 **Materials**

73 Cultivated *G. dura* was collected from the south-east coast (Latitude: 9.28°N, and Longitude:
74 79.12°E, Mandapam, Tamil Nadu) of India. 45-days-old plants were harvested, air dried and
75 stored in plastic bags. Two cationic [cetyl trimethyl ammonium bromide (CTAB); cetyl
76 pyridinium chloride (CPC)], one anionic [sodium lauryl sulphate (SLS)] and four nonionic
77 [Triton X-100 (octyl phenol ethoxylate; $C_{14}H_{22}O(C_2H_4O)_n$]; [Synperonic 91/6 (alcohol
78 ethoxylate; $C_8/C_{10}-CH_2O-(C_2H_4O)_6$]; [Tween-80 (Polyoxyethylenesorbitan monooleate;
79 $C_{64}H_{124}O_{26}$)]; [Atplus 245 (C_9/C_{11} alcohol ethoxylate/propoxylate)] surfactants were used in the
80 present study. CTAB, CPC, SLS and Triton X-100 were procured from S. D. Fine Chemicals,
81 India and the rest of the surfactants were gifted by ICI Uniqema (presently Croda), India.
82 Agarose samples from Sigma–Aldrich, USA (Cat. No. A05066), Merck (Genei), and a sample
83 prepared from *G. dura* in our own laboratory¹ served as controls.

84

85 **Characterizations**

86 Sulphate contents analyses (ICP) were carried out on a Perkin-Elmer ICP-OES Optima
87 2000DV machine.¹ Weight average molecular weight (M_w) was estimated as per literature
88 procedure.¹ Morphology of agarose hydrogel samples before and after freeze drying was
89 studied out using optical microscope (OLYMPUS, U. TV0.63XC, T₇ Tokyo, Japan). The
90 dynamic light scattering (DLS) measurements were carried out using a Malvern instrument at a
91 scattered angle of 90° and at temperature 30°C. The incident light was the 488 nm line of a
92 argon laser GLS 3110. First, the solution was taken in a cell and the measurement was carried
93 out at 30°C. Detailed procedures of gelling property measurement, DNA and RNA gel

94 electrophoresis experiments, electroendosmosis (EEO) measurement, and recovery of
95 surfactant by reverse osmosis (RO) are provided as Electronic Supplementary Information
96 (ESI, General Experimental Section). Quantification of surfactant in concentrate stream after
97 RO was computed using the following equation:

$$98 \quad V_f \times C_f = V_p \times C_p + V_c \times C_c$$

99 wherein V_f = volume of feed; C_f = surfactant concentration in feed (w/v); V_p = volume of
100 permeate; C_p = surfactant concentration in permeate (w/v); V_c = volume of concentrate; and C_c
101 = surfactant concentration in concentrate (w/v). Absence of surfactant (Triton X-100) in
102 permeate stream was checked by HPLC (Waters Alliance 2996, USA) using C-18H column
103 and PDA detector at 220 nm, and accordingly the first term in the right hand side of the
104 equation was neglected.

105 **Preparation of agarose**

106 The alkali treated seaweed extract was prepared by modification of a previous process.¹ In the
107 laboratory process, 0.20 kg of the dry seaweed having 9 ± 1 % moisture content was taken in 2
108 L of 10 % NaOH and the reaction mixture was heated to 80°C to reduce the sulphate content of
109 the linear galactan. This was followed by several water washes (4 x 2 L) to remove the excess
110 alkali. The treated seaweed was then crushed and autoclaved (seaweed: water = 1: 35 w/w) at
111 120°C for 90 min, and the resultant hot mass was subjected directly to centrifugation at 10,000
112 rpm to obtain a clear extract. After reaching a temperature of 70-80°C, the extract was treated
113 with surfactant (4 % w/w) under continuous stirring, while allowing the mass to cool gradually
114 to room temperature. Phycocolloid precipitation was observed with the nonionic surfactants
115 and the resultant solid mass was isolated by centrifugation. The solid mass was washed with
116 water to remove excess surfactant followed by successive washing with 1: 1 (w/w) IPA: H₂O

117 (single cycle), 3: 1 (w/w) IPA: H₂O (single cycle), 17: 3 (w/w) IPA: H₂O (single cycle), and
118 finally with neat IPA (single cycle). For each washing, the solvent weight was twice the weight
119 of the solid mass taken. The product was finally subjected to vacuum drying at 50°C to obtain a
120 readily water soluble agarose powder. Experiments were subsequently conducted at bench scale
121 with 1 kg of dry biomass, yielding similar results. The procedure for recovery of surfactant
122 from agarose-depleted extract and water washings is described under supplementary material
123 (ESI, General Experimental Section). Filtrate containing surfactant left behind after the
124 recovery of agarose, along with the first water wash, was subjected to reverse osmosis (RO)
125 (Hydronautics SWC5 LD4040 low fouling seawater RO membrane module; 150 psi applied
126 pressure) for the recovery of the surfactant in concentrated form. In this process, 90 % of the
127 water was removed, leaving a concentrated surfactant which, after removal of color through
128 charcoal treatment, could be added directly into the next lot of seaweed extract to induce
129 coagulation. Similarly, the IPA-water mixtures were collected from which IPA was recovered
130 by distillation.

131

132 **Results and discussion**

133 Normally in a conventional extraction process 0.2 kg of *G. dura* gives ca. 4.5 L of extract
134 containing only 0.50-0.75 % agar/agarose. Consequently, considerable amount of energy is
135 expended in repeatedly freezing and thawing of the mass to isolate and purify the product by
136 the widely used conventional means. Precipitation through addition of alcoholic solvent is also
137 feasible but it requires twice the volume of solvent. It is therefore of interest to explore
138 alternative solutions such as incorporation of additives to induce precipitation. In line with this
139 approach, ionic and nonionic surfactants were probed in the concentration range of 2-5 % (w/w)

140 (Table 1). No effect was seen with up to 5 % (w/v) concentration of ionic surfactants added into
 141 hot seaweed extract. The lack of any coagulation with charged surfactants was consistent with
 142 literature reports that polymers bearing low charge do not interact with ionic surfactants.⁷⁻⁹
 143 When nonionic alkoxyate surfactants were evaluated, no effect was seen at 2 % (w/v)
 144 concentration. However some precipitation was observed at 3 % level while heavy precipitation
 145 was seen at 4 % concentration within 4 h upon gradual cooling of the mass to ambient
 146 temperature under continuous agitation. A study was also conducted to ascertain the relative
 147 ease of coagulation of three different seaweed extracts, namely *Gelidiella acerosa* and
 148 *Gracilaria edulis*, besides *G. dura*. No coagulation was observed with *G. edulis*, partial
 149 coagulation was seen with *G. acerosa*, and maximum coagulation with *G. dura*. This may be
 150 due to differences in the galactan charge arising from variations in the sulphate content, the
 151 value being lowest (0.2 %) in the case of *G. dura* and highest (> 1 % sulphate) in the case of *G.*
 152 *edulis*. Table 2 provides data on the properties of the product obtained upon purification

153
 154 **Table 1.** Effect of treatment of seaweed extract with cationic, anionic and nonionic surfactants.
 155

Surfactant	% w/w	Remarks
CTAB	5	No precipitation
CPC	5	No precipitation
SLS	5	No precipitation
Triton X-100	4	Precipitation observed
Synperonic 91/6	4	Precipitation observed
Tween-80	4	Precipitation observed
Atplus 245	4	Precipitation observed

156 through water wash followed by water-IPA wash. The best properties for molecular biology
 157 applications in terms of gel strength ($2200 \pm 50 \text{ g cm}^{-2}$), sulphate content and EEO were
 158 obtained with Triton X-100. Hence this surfactant was chosen for further studies although the
 159 product yield was marginally lower than in the case of Synperonic 91/6 and Atplus 245.
 160 Another important reason behind the choice was the proven applications of this surfactant in
 161 biology. Product of similar quality in 14.9 % yield was obtained when 20 L of extract (prepared
 162 at bench scale from 1 kg of dried *G. dura*) was processed similarly in a single lot. Table 3
 163 shows that the gel strength of the bench scale product was 1.5 times that of A05066 Sigma
 164 agarose employed for molecular biology applications, and the other critical properties were
 165 comparable or superior. Indeed, the gel strength was even superior to that of “exceptionally
 166 high gel strength” agarose from Sigma (A0576) employed for separation of high molecular
 167 weight nucleic acids.

168
 169 **Table 2.** Effect of nonionic surfactants on the properties of agarose.
 170

	Triton X-100	Synperonic 91/6	Tween-80	Atplus 245
Yield (%)	13.2	13.6	13.0	14.6
Moisture (%)	7.0	7.0	8.0	8.0
Ash (%)	0.8	0.9	0.9	0.9
EEO	0.13	0.13	0.14	0.14
Sulphate (%)	0.20	0.21	0.23	0.24
Gel strength (g/cm^2)	2200	2000	2000	1900
Gelling temperature ($^{\circ}\text{C}$)	35 ± 1	35 ± 1	35 ± 1	35 ± 1
$M_w/\text{g mol}^{-1}$	1.31×10^5	1.29×10^5	----	---

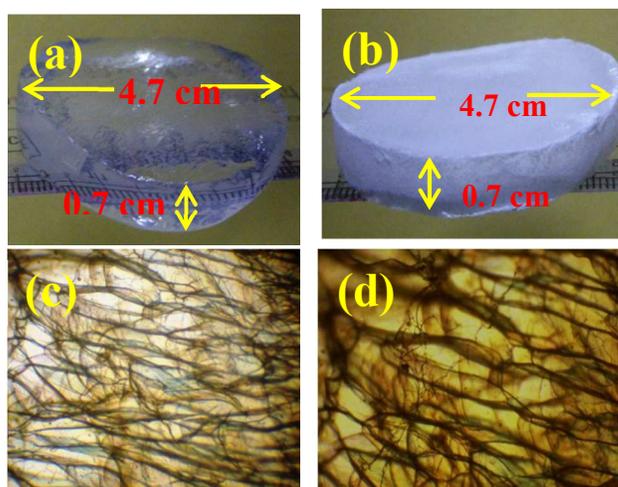
172 **Table 3.** Comparative data of agarose obtained at bench scale with Sigma agarose.

	<i>G. dura</i> agarose (present study)	Sigma agarose (A 05066) ^a	Sigma agarose (A0576) ^b
Gel strength (g cm ⁻²)	2200 ± 50 (1 % gel)	≥1500 (1.5 % gel)	≥1800 (1 % gel)
Sulphate (% w/w)	0.20	≤0.6	≤0.12
EEO ^c	0.13 (± 0.01)	0.23-0.27	0.12
Melting Temp/ °C	89 (± 1)	N/A ^d	86 (± 2)
Gelling Temp/ °C	35 (± 1)	34-37 (± 1.5)	36 (± 1.5)
DNAse, RNAse activity	ND ^e	ND ^e	ND ^e

173 ^aUsed for molecular biology; ^bHigh gel strength particularly suitable for separating high
 174 molecular weight nucleic acids at low gel concentrations; ^c≤0.13 considered as low EEO; ^dN/A
 175 = not available; ^eND = None detected.

176
 177 An experiment was undertaken to observe the gel networks after lyophilisation of the
 178 hydrogels. As can be seen from Fig. 1, agarose from *G. dura* revealed thinner strands of the
 179 linear galactan with denser network of the strands compared to A05066. The observed
 180 differences in the network properties possibly contribute to the observed variations in the gel
 181 strengths. Artifacts arising from the manner of freezing and sublimation cannot, however, be
 182 ruled out.¹⁰ It is noted that gel strength is influenced by other factors also.¹¹

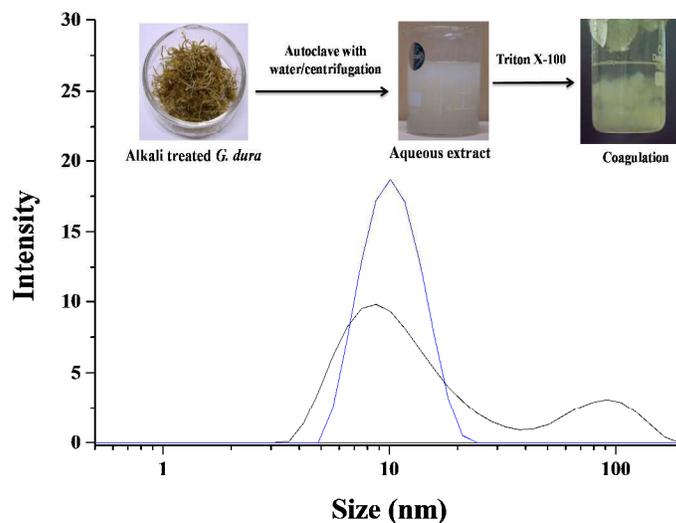
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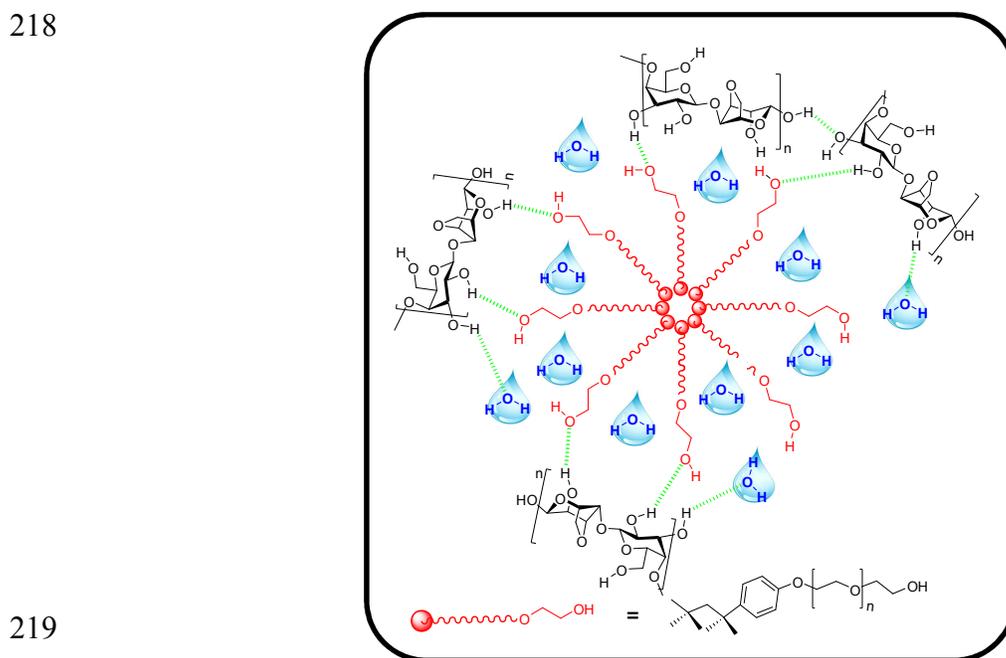
194 **Figure 1.** (a) Typical appearance (camera photo) of 0.6 % (w/v) agarose gel prepared from *G.*
195 *dura* (Table 3); (b) of solid foam after freeze drying (camera photo); optical micrographs of
196 solid foam prepared from (c) *G. dura* agarose of Table 3 and (d) A05066 Sigma agarose.

197

198 The effect of Triton X-100 was studied next. Fig. 2 shows the DLS profiles of the
199 surfactant in water and in *G. dura* extract at 4% (64 mM) concentration. The observed peak at
200 10 nm in water may be ascribed to micelle formation since the concentration of the surfactant
201 was far in excess of the critical micelle concentration (cmc) of 0.28 mM.¹² Upon addition of the
202 surfactant into seaweed extract, the intensity of the peak at 10 nm decreased markedly with
203 corresponding formation of a peak at 100 nm due to formation of a fine suspension. When the
204 agitation was stopped and the suspension maintained under ambient conditions, settled mass
205 was seen at the bottom as shown in the inset. Fig. 3 shows a possible mechanism of the
206 coagulation induced by Triton X-100. In the typical micellar structure, the hydrophobic
207 aromatic group is located in the micellar core whereas the hydrophilic ethoxylate chains
208 project outward into the bulk of the solution. It is presumed that the micelle served as a
209 template for the galactan chains, and H-bonding with water was partly substituted with H-
210 bonding with the ethoxylate chains of Triton X-100. Agarose polymer molecules may have
211 also interacted among themselves as shown in the Fig. 3. Plausibly, the above promoted
212 coagulation.



213
 214 **Figure 2.** DLS traces of solution of Triton X-100 (4% (w/v) in water (blue trace) and in
 215 seaweed extract at the same concentration (black trace). The inset shows the alkali treated
 216 seaweed, the aqueous extract prepared from the seaweed and subjected to centrifugation, and
 217 of the suspension obtained after Triton X-100-induced coagulation.



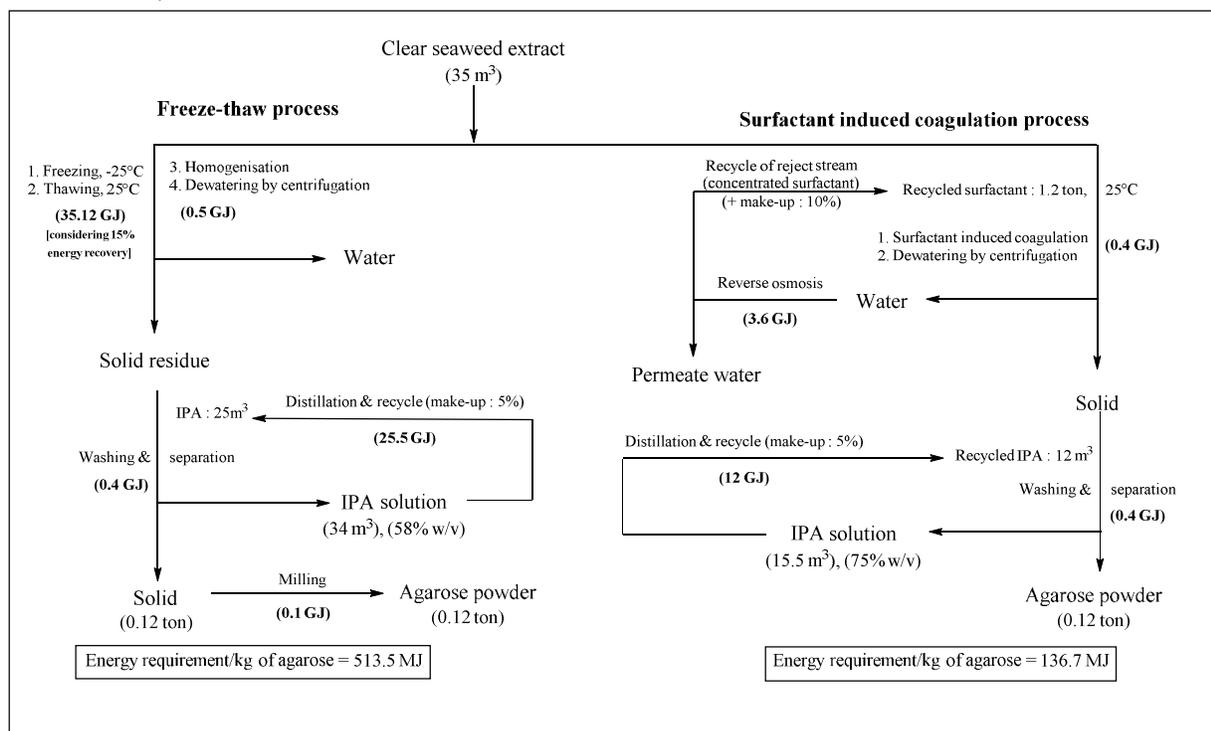
219
 220 **Figure 3.** Possible mechanism of coagulation arising from the interaction of agarose with
 221 micelles of Triton X-100.

222 Attention was focused next on the recovery and reuse of the surfactant. Although the weight
 223 percentage of the surfactant in solution was similar to that of dissolved salts in seawater, the
 224 osmotic pressure in the former case would be much lower in view of the higher molecular
 225 weight (MW = 624) of the surfactant and formation of micellar aggregates. With the above
 226 reasoning, an attempt was made to concentrate the surfactant in the supernatant seaweed extract
 227 by reverse osmosis (RO) at low-to-moderate pressure (150 psi). Table 4 provides data on
 228 processing of ca. 105 L of supernatant and water wash. Permeate stream free from surfactant
 229 ($C_p \sim 0$) was recovered in ca. 90% yield (ESI, Fig. S1) and, based on mass balance equation, C_c
 230 was estimated to be ca. 40 %. The latter was subjected to charcoal treatment to remove color
 231 and utilized thereafter in a subsequent cycle of coagulation. Product of desired quality was
 232 obtained in 12.7% yield. IPA was also recycled and reused to give the desired quality of
 233 product in 13.2% yield. Scheme 1 presents schematically the differences between the freeze-
 234 thaw (considering a single cycle) and surfactant-induced coagulation processes, along with the
 235 energy consumption in critical steps. It can be seen from the scheme that the energy savings
 236 works out to 376.8 MJ/kg of agarose. Other important advantages of the new process are (i)
 237 shorter process time and (ii) lower capital expenditure.

238 **Table 4.** Data on permeate flow rate upon concentration of spent seaweed supernatant by RO.
 239

240	Time/min	Permeate Flow/Liters per minute	Temperature/ $^{\circ}$ C
241	0	1.59	26.8
	10	1.395	27.2
242	20	1.290	27.7
	30	1.245	28.0
243	40	1.160	28.2
	50	1.04	28.6
244	60	0.940	28.9
	70	0.730	29.0
	90	0.50	29.2

Basis : 1 ton dry seaweed



245

246 **Scheme 1.** Energy computations for “freeze-thaw” and “surfactant-induced coagulation”

247 processes of agarose preparation starting from aqueous extract derived through autoclaving of 1

248 ton of dry *G. dura*.

249

250 **Biological evaluation**

251 Agarose prepared through the surfactant-mediated route was compared initially against the

252 product prepared through conventional processing. The results are presented in ESI, Fig. S2.

253 The results revealed that resolutions of DNA were identical in the two gels, confirming that

254 both the agarose products were of similar quality. Comparative evaluation was subsequently

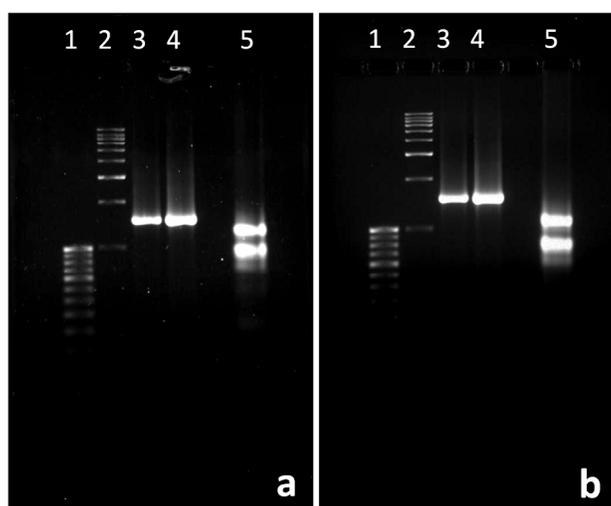
255 conducted with Sigma agarose A05066. *G. dura* agarose prepared in the present work gave

256 similar performance to that of the commercial sample when the gels were prepared with 0.7%

257 (w/v) and 1.0 % (w/v) agarose, respectively (Fig. 4a). The separation of DNA bands both in the

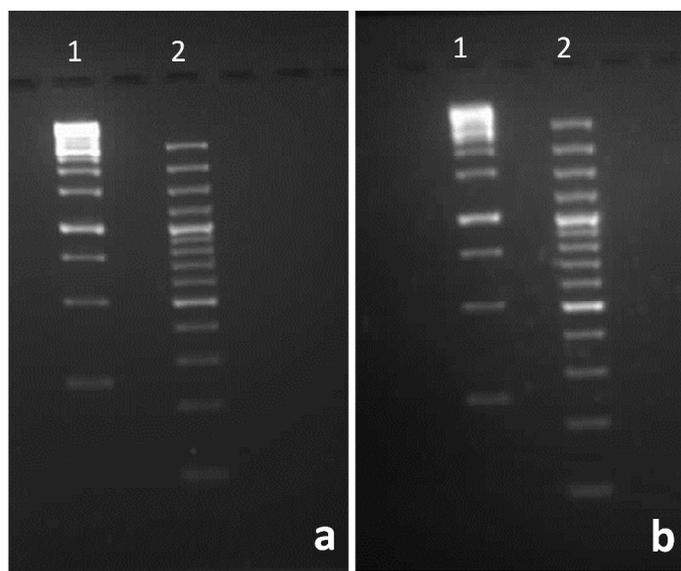
258 100 bp and 1 kb DNA ladders showed near equivalence with sharp resolution. DNA recovery
259 from the gels was >50% in both cases. PCR amplification of the extracted DNA samples
260 showed similar intensity of amplicons, confirming that the agarose obtained through surfactant-
261 induced flocculation can be used for molecular biology applications. Similarly, in the case of
262 RNA, both sub-units (28S rRNA and 18S rRNA) were clearly resolved and no smear was
263 observed in the gel, confirming the absence of degradation in the gel. Gel electrophoresis of
264 DNA and RNA was carried out several times during process development and it was
265 consistently observed that RNA and DNA do not degrade in the gel, confirming reproducible
266 absence of DNase and RNase activity. A comparison was also made of the performances at
267 higher gel concentration. 2% w/v Genei agarose from Merck was employed as benchmark.
268 1.5% w/v *G. dura* agarose of Table 3 gave equivalent DNA band resolution patterns (Fig. 4b).

269

270
271

272 **Figure 4a.** Gel electrophoresis: gel was prepared in 1x TBE buffer and DNA and RNA was
273 electrophoresed at 50 V in (a) 0.7% CSMCRI agarose gel and (b) 1.0% A05066 Sigma agarose
274 gel. Lane 1: 100 bp ladder; Lane 2: 1 Kb ladder; Lanes 3 & 4: DNA band; Lane 5: RNA [28S
275 rRNA (top); 18S rRNA (bottom)].

276



277

278

279 **Figure 4b.** DNA resolution pattern: Gel was prepared in 1x TBE buffer and DNA was
280 electrophoresed at 50 V using (a) 1.5% CSMCRI agarose gel and (b) 2 % Genei agarose
281 (Product No. 6126001, lot no. 124517) (run time: 2 h; Lane 1: 1 Kb DNA ladder; Lane 2: 100
282 bp plus DNA ladder).

283

284 **Conclusions**

285 The present study reports an alternative process of isolation of agarose from *G. dura* seaweed
286 extract that helped dispense with the energy demanding and clumsy process of “freeze-thaw.”
287 The improved process relied on spontaneous coagulation of agarose from the extract through
288 addition of a nonionic surfactant. It is presumed that the micellar aggregate of the surfactant
289 molecules above the critical micelle concentration served as template for the linear galactan
290 chains, replacing in part hydrogen-bonding to water molecules with hydrogen bonding to the
291 polar ethoxylate chain of the surfactant. This may have caused the breakdown of the gel
292 network. The micellar aggregate may also have helped to promote hydrogen bonding between
293 the agarose molecules themselves. The process could be practiced most advantageously with

294 linear galactan hydrocolloids having low sulphate content such as the product from *G. dura*.
295 Recycling of the surfactant through RO-based concentration raised the green quotient of the
296 process, although further studies are necessary to address the issue of membrane fouling upon
297 prolonged exposure. A minimum energy savings of 376.8 MJ/kg of agarose was computed for
298 the improved process but actual savings would be higher if multiple freeze-thaw cycles are to
299 be considered for the conventional process, as is normally the case in practice. Another
300 advantage was that the product was obtained directly in powder form, making it easier to
301 remove the impurities through washing and obviating the need for milling. The multiple
302 advantages of the present process, without any compromise on the quality of the product
303 essential for molecular biology applications, provide the motivation for further studies in this
304 area.

305 306 **Acknowledgement**

307
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343

Graphical abstract

