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# **Promoting Alkali and Alkali-Earth Metals on MgO for Enhancing CO2 Capture by First-Principles Calculation**

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### Abstract

Developing next-generation solid sorbents to improve the economy of pre- and post-combustion carbon capture processes has been challenging for many researchers. Magnesium oxide (MgO) is a promising sorbent because of its moderate sorption-desorption temperature and low heat of sorption. However, its low sorption capacity and thermal instability need to be improved. Various metal-promoted MgO sorbents have been experimentally developed to enhance the  $CO<sub>2</sub>$ sorption capacities. Nevertheless, rigorous computational studies to screen an optimal metal promoter have been limited to date. We conducted first-principles calculations to select metal promoters of MgO sorbents. Five alkali (Li-, Na-, K-, Rb-, Cs-) and 4 alkaline earth metals (Be-, Ca-, Sr-, Ba-) were chosen as a set of promoters. Compared with the  $CO<sub>2</sub>$  adsorption energy on pure MgO, the adsorption energy on the metal-promoted MgO sorbents is higher, except that for the Na-promoter, which indicates that metal promoting on MgO is an efficient approach to enhance the sorption capacities. Based on the stabilized binding of promoters on the MgO surface and the regenerability of sorbents, Li, Ca, and Sr were identified as adequate promoters among the 9 metals on the basis of PW91/GGA augmented with DFT+D2. The adsorption energies of  $CO<sub>2</sub>$  on metal-promoted MgO sorbents for Li, Ca, and Sr atoms are -1.13, -1.68, and -1.48 eV, respectively.

# <sup>1</sup> Introduction

<sup>2</sup> To stop the progression of the greenhouse effect, the general consensus is that anthropogenic  $3$  global CO<sub>2</sub> emission must be reduced over the next few decades. This CO<sub>2</sub> reduction has been 4 mandated by worldwide associations, including the IPCC (Inter-governmental Panel on Climate  $5$  Change) summit, since the first initiation of the Kyoto protocol. Therefore, capturing  $CO<sub>2</sub>$  from <sup>6</sup> large stationary point sources, such as flue gas and syngas, has attracted the attention of many researchers.<sup>1,2</sup> 7

<sup>8</sup> CCS (Carbon Capture and Sequestration) techniques have been considered a viable method to  $9$  reduce the CO<sub>2</sub> level in the atmosphere. In CCS, chemical scrubbing with an aqueous amine-based

 solvent a conventional carbon capture technique. However, recovering  $CO<sub>2</sub>$  from the solvent via a distillation process requires a large amount of energy for the re-boiler, where the solvent is va- porized with a large amount of water. Due to the energy-intensive regeneration step, an alternative carbon capture processes using solid sorbents has received considerable attention.  $1-3$  In the carbon capture process based on solid sorbents, the heat of water vaporization may be avoided by replac- ing the liquid solution with solid particles. Moreover, the heat capacity of the solid particles is lower than that of water.

17 Because of their low cost, abundance, and low toxicity, various alkali and alkaline earth metal <sup>18</sup> oxides have been used as absorbents.<sup>4</sup> Among these absorbents, MgO is preferred due to its low <sup>19</sup> heat of absorption<sup>5</sup> and moderate regeneration temperature (400-500 °C).<sup>6,7</sup> However, the practical <sup>20</sup> application of MgO has been limited because of a low  $CO_2$  sorption capacity and thermal instability during regeneration.<sup>6</sup> The CO<sub>2</sub> sorption capacity of MgO is half that of CaO.<sup>8</sup> 21

<sup>22</sup> To enhance the sorption capacity, alkali metal-promoted MgO sorbents have been investigated <sup>23</sup> for a decade. Lee et al.<sup>9</sup> developed a  $K_2CO_3$ -promoted MgO sorbent that has a  $CO_2$  sorption ca-<sup>24</sup> pacity of 12 wt% in the presence of 9 vol%  $H_2O$  and 1 vol%  $CO_2$  with a fast and complete regen-<sup>25</sup> eration. Alkali metal carbonate double salts supported on MgO, (M2CO3)*n*(MgCO3)*p*(MgO)1−*p*, <sup>26</sup> where M is Li, Na, K, and Cs, were reported.<sup>10</sup> The maximum sorption capacity was 56 wt% in the  $_{27}$  case of Na-double salts at 375 °C and 0.7 atm CO<sub>2</sub> during PSA (Pressure Swing Adsorption). Xiao <sup>28</sup> et al.<sup>11</sup> reported that a K-promoted double salt MgO sorbent had the highest sorption capacity, 8.6 29 wt% in a 100 % CO<sub>2</sub> environment. Zhang et al.<sup>12</sup> synthesized a Na-promoted double salt MgO 30 sorbent, including NaNO<sub>3</sub>, for  $CO<sub>2</sub>$  capture in the syngas of a pre-combustion process. During 31 multiple cycle tests, the  $CO_2$  sorption capacity was maintained at 15 wt% in a 100 %  $CO_2$  environ- $_{32}$  ment. Yang et al.<sup>13</sup> investigated the role of NaNO<sub>3</sub> in Ca-promoted double salt and reported that 33 NaNO<sub>3</sub> enhances the absorbent activity by facilitating ion diffusion. NaNO<sub>3</sub> on metal oxide has <sup>34</sup> also been shown to act as a phase transfer catalyst in the gas-solid reaction, which increases the <sup>35</sup> reaction rate and sorption capacity.<sup>14</sup> Liu et al.<sup>15</sup> developed a Cs-doped MgO based sorbent with <sup>36</sup> the wet impregnation method with a maximum sorption capacity of 8.3 wt% at 300 °C. Duan et

 $37$  al.<sup>16</sup> conducted a computational study for Na-, K-, and Ca-promoted MgO sorbents using density <sup>38</sup> functional theory (DFT) and phonon dynamics. They evaluated the adequate turnover temperature <sup>39</sup> of each sorbent.

<sup>40</sup> Many researchers have experimentally developed metal-promoted MgO sorbents. However, <sup>41</sup> to the best of our knowledge, only a few computational investigations of metal-promoted MgO 42 sorbents for  $CO_2$  capture have been performed. Metal promoters are also limited to a few alkali metals, such as potassium carbonate and sodium carbonate. In this study, we aimed to screen for an optimal promoter for MgO sorbents that can be used as a  $CO<sub>2</sub>$  absorbent based on first-principles calculations. We selected 9 metals as a set of potential promoters, including 5 alkali metals (Li-, Na-, K-, Rb-, Cs-) and 4 alkaline earth (Be-, Ca-, Sr-, Ba-) metals. The effects of the 9 metal promoters on MgO for CO<sub>2</sub> capture were evaluated via DFT calculations.

## <sup>48</sup> Computational details

<sup>49</sup> Our DFT calculations were carried out with a periodic supercell model using the Vienna ab ini-<sup>50</sup> tio simulation package (VASP)<sup>17–20</sup> with the PW91 exchange-correlation functional.<sup>21,22</sup> A PAW  $_{51}$  (projector augmented wave) method  $^{23,24}$  was used as a plane wave basis set with an energy cutoff  $52 \text{ of } 400 \text{ eV}$ . The long-range dispersion (van der Waals) contribution using the DFT + D2 approach of  $53$  Grimme<sup>25</sup> was applied to all calculations. The default dispersion parameters in VASP were used,  $_{54}$  except for Cs and Ba, whose parameters were taken from Zhang et al.'s work.  $^{26}$  In Venkataramanan <sup>55</sup> et al's work,<sup>27</sup> they validated PW91/GGA provides accurate results for alkali metals over a hybrid  $56$  exchange-correlation functional of MPW1PW91/6-311G(d,p). Thus, we expanded PW91/GGA <sup>57</sup> augmented with DFT+D2 for alkali and alkaline earth metals. We obtained an additional set of <sup>58</sup> results using an increased energy cutoff of 600 eV for Li and verified that the difference of energy  $59$  cutoff of 400 and 600 eV is unaffected, which implies that the energy cutoff of 400 eV is sufficient <sup>60</sup> to compare the promoters.



<sup>61</sup> The defect-free MgO crystalline structure was cleaved in the (100) direction with a vacuum

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- $62$  region of 15 Å. Each repeated slab is composed of 5 MgO layers. The adsorbate and upper 3 layers
- <sup>63</sup> were allowed to be relaxed, whereas the lower 2 layers were to be fixed in their bulk positions.
- <sup>64</sup> The adsorption energy,  $E_{ad}$ , of the metal promoter on bare MgO is defined as

$$
E_{ad} = E_{P/host} - (E_P + E_{host})
$$
\n<sup>(1)</sup>

<sup>65</sup> where  $E_{P/host}$ ,  $E_{host}$ , and  $E_P$  represent the energies of the adsorption composites, host materials, <sup>66</sup> and metal promoters, respectively. *E<sup>P</sup>* is on the basis of the isolated atom. Lower values of *Ead* <sup>67</sup> represent a stronger adsorption of a promoter to MgO.

 $\epsilon$ <sup>8</sup> A Bader charge analysis was conducted using a grid-based algorithm.<sup>28</sup> The charge in an atom <sup>69</sup> was defined as the difference between the valence charge and the Bader charge.

# <sup>70</sup> Results and discussion

<sup>71</sup> We conducted first-principles calculations to screen candidate metal promoters (alkali metals: Li-, Na-, K-, Rb-, Cs- and alkaline earth metals: Be-, Ca-, Sr-, Ba-) for an optimal metal promoter on a MgO sorbent. First, the adsorption energies of 9 promoters on the MgO surface were calculated. CO<sub>2</sub> was loaded on the geometry-optimized metal-promoted MgO, and its adsorption energy was calculated and compared with the adsorption energy of  $CO<sub>2</sub>$  on MgO without the promoters.

### $76$  Adsorption of  $CO<sub>2</sub>$  in Non-promoted MgO

 $77$  One CO<sub>2</sub> molecule was adsorbed to the  $(3 \times 3)$  surface unit cell of MgO. The adsorption energy  $78$  of  $CO<sub>2</sub>$  on the top of the lattice oxygen was the highest among the four adsorption potential sites,  $\bar{z}_1$  i.e., the twofold bridge, fourfold hollow, on top of oxygen, and on top of magnesium.

 $\delta$ <sup>80</sup> On the top of the lattice oxygen site, the CO<sub>2</sub> molecule was rotated every 15<sup>o</sup> in the vertical and 81 horizontal direction to explore the ground state energy. Figure 1 shows the geometry-optimized <sup>82</sup> structure of  $CO_2$  adsorption on MgO. Table 1 provides the distances between the  $CO_2$  and MgO  $83$  surface atoms,  $CO_2$  bending angle, and adsorption energy of  $CO_2$ . These structural data for the



84 fourfold hollow, twofold bridge, and the top of the lattice magnesium sites are given in the Ap-

85 pendix.

Table 1: The structural data of  $CO<sub>2</sub>$  adsorption on MgO for the top of the lattice oxygen site.

			$d(C-O)/\mathring{A}$ $d(O_a-Mg)/\mathring{A}$ $d(O_b-Mg)/\mathring{A}$ $\angle$ $O_a-C-O_b$ /deg $E_{ads}/eV$	
1.45	2.20	2.18	133.6	$-0.71$

<sup>86</sup> 0.43*e*− was transferred from the MgO surface to the CO<sup>2</sup> molecule. In this electron transfer, <sup>87</sup> the largest charge transfer, 0.27*e*−, was attributed to the lattice oxygen atom beneath the carbon <sup>88</sup> atom.

# 89 Promotion of Alkali and Alkaline Earth Metals on MgO

<sup>90</sup> The alkali and alkaline earth metals were promoted on MgO. Initially, each promoter was placed 91 on MgO at a distance of 1.2 Å. DFT energy optimization was utilized to obtain optimized config-<sup>92</sup> urations of promoters on MgO, as depicted in Fig. 2.

<sup>93</sup> The energy of all promoters was minimized when they are bound on top of the lattice oxygen <sup>94</sup> among the MgO adsorption sites. A single promoter was adsorbed on the MgO surface unit cells 95 of  $(1 \times 1)$ ,  $(2 \times 2)$ ,  $(3 \times 3)$ , and  $(4 \times 4)$ , which corresponds to an adsorption coverage of 1/2, 1/8, 1/18, and 1/32 ML (monolayer). In Fig. 3, the adsorption energies of the promoters are



Figure 2: A side view of the relaxed structure for the promoter adsorbed on top of the lattice oxygen of MgO ( $3 \times 3$  surface unit cell); orange: magnesium, red: oxygen.

97 shown for different surface coverages. Except for the Be-promoter, 8 promoters show a similar <sup>98</sup> trend: the adsorption energy negatively correlates with the surface coverage due to the repulsive <sup>99</sup> force between the promoters.<sup>29</sup> However, at much higher coverage rates, the adsorption energies of <sup>100</sup> the promoters increase again. These stabilizations were attributed to an additional cluster binding  $_{101}$  energy between the promoters, as described by Alfonso et al.<sup>30</sup> and Snyder et al.<sup>31</sup> Unlike the 102 behaviors of the other promoters, the adsorption energy of Be continuously decreased until  $1/2$ 103 ML. At a higher coverage of 1 ML, the adsorption energy of Be drastically increased to -4.39 eV. <sup>104</sup> This tendency is the result of a low cohesive energy of Be, which is approximately one-third that of Ca.<sup>32</sup> 105

 The distances between repeated promoters are 12.7 Åfor 1/18 ML and 17.0 Åfor 1/32 ML. To exclude horizontal interactions between adjacent promoters, we selected a surface coverage of  $1/18$  ML because 12.7 Åis a sufficiently long distance between promoters and less computationally taxing than 1/32 ML.

 Figure 4 represents the adsorption energies of promoters at 1/18 ML with electron transfers from promoters to MgO. Because alkaline earth metals are more electronegative than alkali metals in the same row of the periodic table of the elements (PTE), alkaline earth metals more strongly adsorb to MgO than do alkali metals.

 $114$  Finazzi et al.<sup>33</sup> adsorbed alkali metals to the MgO surface using electron paramagnetic reso-<sup>115</sup> nance (EPR) spectroscopy and density functional theory. They concluded that the adsorption en-



Figure 3: The adsorption energy of promoters on the MgO surface: (a) for alkali metals and (b) for alkaline earth metals.

 ergies of alkali metals on MgO decrease in the following order on terrace sites: Li>Na>K. These patterns can also be observed in Fig. 4 because the electronegativity increases from the bottom to the top in PTE. Among the possible promoters the adsorption energies of Li and Be are the highest of the promoters in alkali and alkaline earth metals, whose binding is attributed to both polarization and covalent bonding with the largest charge transfer to MgO.

121 In general, the heat of chemisorption is greater than  $0.52 \text{ eV} \approx 50 \text{ kJ/mol}$ , which indicates that the cationization of alkali metals except for Li is contributed by mixed nature of physisorption and chemisorption. However, Li and alkaline earth metals are promoted on MgO via chemisorption, which more strongly stabilizes promoters.

### Adsorption of  $CO<sub>2</sub>$  on Alkali- and Alkaline Earth Metal-Promoted MgO

 CO<sub>2</sub> was adsorbed on alkali- and alkaline earth metal-promoted MgO to investigate effects of promoters. Figure 5 represents the adsorption energies of  $CO<sub>2</sub>$  of alkali- and alkaline earth metal-promoted MgO sorbents. The corresponding optimized structures and charge distributions are



Figure 4: Adsorption energies of 9 promoters on MgO for the surface coverage, 1/18 ML. The values in parenthesis represent charge transfers from promoter to MgO.

129 presented in Table 2. Compared with the bending angles of  $CO_2$  and distances of  $O_b$ -Mg and C-P for alkali metal promoters, both these angles and distances are too small for alkaline earth metal-promoted MgO. Except for the Na-promoter, the adsorption energies of  $CO<sub>2</sub>$  on the metal promoted MgO are higher than those on bare MgO. Similar to the highest adsorption energy found for the Li- and Be-promoter on MgO in alkali and alkaline earth metals, the adsorption energy of CO<sub>2</sub> was highest on Li- and Be-promoted MgO sorbents because of the high electronegativity and small Van der Waals radius, which easily transfer charge to the  $CO<sub>2</sub>$  molecule.

 The amount of charge transferred from the MgO surface to the CO<sup>2</sup> molecule is 0.43*e*− in the absence of promoters, and more charge is transferred in the presence of promoters. The adsorbed CO<sub>2</sub> molecule becomes more negatively charged because both the promoters and the MgO in the 139 vicinity of  $CO_2$  donate electrons, thereby increasing the adsorption energy of  $CO_2$ . These charge transfers are very drastic for alkaline earth metal promoters due to their stronger electronegativity.





Figure 5: The adsorption energy of  $CO<sub>2</sub>$  on the metal-promoted MgO.

Table 2: The structural data and charge distribution of  $CO<sub>2</sub>$  adsorption on the metalpromoted MgO.

	$\mathbf{P}$	$\angle$ O <sub>a</sub> -C-O <sub>b</sub>	$d(O_h-Mg)$	$d(C-P)$	Charge distribution $(e-)$				$CO2$ Ads. En.	
		$(\text{deg})$	A)	(Å)	$O_a$	$O_h$	C	CO <sub>2</sub>	P	(eV)
Akali Metals	Li-	136.8	2.21	2.34	$-1.08$	$-1.23$	1.43	$-0.88$	0.87	$-1.13$
	Na-	137.1	2.18	2.7	$-1.11$	$-1.21$	1.46	$-0.86$	0.83	$-0.68$
	$K-$	136.6	2.13	3.34	$-1.00$	$-1.21$	1.35	$-0.86$	0.84	$-0.79$
	$Rb-$	135.8	2.17	3.27	$-1.10$	$-1.23$	1.46	$-0.87$	0.84	$-0.78$
	$Cs-$	135.2	2.15	3.44	$-1.14$	$-1.2$	1.45	$-0.89$	0.84	$-1.00$
Akali- Earth Metals	Be-	122.9	2.11	1.68	$-1.14$	$-1.24$	0.78	$-1.60$	1.60	$-2.31$
	$Ca-$	120.9	2.10	2.36	$-1.19$	$-1.19$	0.98	$-1.40$	1.33	$-1.68$
	$Sr-$	121.5	2.08	2.52	$-1.18$	$-1.22$	1.00	$-1.40$	1.36	$-1.48$
	Ba-	119.3	2.09	2.69	$-1.25$	$-1.25$	1.03	$-1.47$	1.39	$-2.02$

 $*O<sub>b</sub>$  is oxygen atom that has a shortest distance from MgO surface.

### 141 Impact of Metal Promoter on  $CO_2$  capture

 As noted in the section entitled **Promotion of Alkali and Alkaline Earth Metals on MgO**, the promoters in the top of row of PTE are more strongly adsorbed to the MgO because of their high electronegativity. However, for a metal with a large atomic radius, such as Cs and Ba, the adsorption strength increased as shown in Fig. 6, which is attributed to the attractive electrostatic interaction between Cs (or Ba) and neighboring four Mg.<sup>34</sup> 146

147 On the contrary, the adsorption of  $CO<sub>2</sub>$  is enhanced when substrates with promoters are strongly <sup>148</sup> electropositive and basic, which suggests that the metals on the bottom of row of PTE are the 149 preferred promoters for a high sorption capacity. Reddy et al.<sup>35</sup> reported TGA experimental results  $_{150}$  in which the CO<sub>2</sub> adsorption capacity was ranked as a function of the atomic radius and the basicity <sup>151</sup> of the alkali metals doped on CaO, i.e., Li<Na<K<Rb<Cs. Similarly, for sodium-, potassium-, and  $152$  cesium carbonate- doped MgO, the CO<sub>2</sub> sorption capacities were experimentally found to rank  $153$  as follows: Na<K<Cs.<sup>36</sup> The results presented in Fig. 6 also provide the same tendency for the <sup>154</sup> sorption capacities. Exceptional behaviors of Li and Be are attributed to the high cationizations <sup>155</sup> of these metals, which provide a high partial charge to  $CO_2$ . Lan et al.<sup>37</sup> calculated the binding 156 energy of CO<sub>2</sub> molecules to alkali and alkaline earth metals, and Li and Be showed much higher <sup>157</sup> binding energies than did the remaining metals. These effect can be observed in Table 2, such that <sup>158</sup> Li and Be are high positively charged as 0.87 and 1.60, respectively.

 The complex correlations mentioned above generate the curves shown in Fig. 6. Hence, the selection of the most adequate promoter is based on two aspects: i) the stabilization of promoter  $_{161}$  binding on MgO and ii) the regenerability of CO<sub>2</sub>. The adsorption energies of promoters must exceed 0.52 eV for stable binding on MgO to ensure thermal stability. The adsorption energy of  $CO_2$  should be lower than 1.86 eV, which corresponds to the adsorption energy of  $CO_2$  on CaO 164 (CaO + CO<sub>2</sub>  $\leftrightarrow$  CaCO<sub>3</sub>). When the adsorption energy of CO<sub>2</sub> exceeds 1.86 eV, the desorption would be difficult. Thus, an energy-intensive regeneration must be included, which results in a high expenditure of the process. In terms of these two aspects, we conclude that the optimal promoters are Li, Ca, and Sr on the basis of PW91/GGA augmented with DFT+D2.



Figure 6: The adsorption energy of  $CO<sub>2</sub>$  on the metal-promoted MgO with respect to the adsorption energy of promoters.

168 To the best of the author's knowledge,  $Li_4SiO_4$  and CaO have been utilized as high-temperature 169 absorbents for  $CO_2$  capture,<sup>7</sup> although not as a promoter. These screened metal materials (Li, Ca, 170 and Sr) have not been used as promoters on MgO, which allows for the development of possibly <sup>171</sup> improved medium temperature sorbents.

# 172 Conclusions

173 Overcoming the energy penalty of carbon capture processes to develop improved solid-sorbents has been a major challenge for most material-related researchers. Therefore, we screened 5 alkali metals and 4 alkaline earth metal-promoted MgO sorbents using first-principles calculations in this work. In the set of 9 alkali metal promoters, most of alkali metals, except for Li, exhibited unstable binding on MgO via mixed chemisorption and physisorption, while the other promoters, i.e., alkali earth metals and Li, showed stable binding on MgO via chemisorption. Except for the

 $179$  Na-promoter, the adsorption energies of  $CO<sub>2</sub>$  increased compared with that on pure MgO due to 180 promoter effects. Based on the stable promoter binding on MgO and the  $CO<sub>2</sub>$  regenerability, we  $181$  suggest that Li-, Ca-, and Sr-promoted MgO sorbents are the most appropriate CO<sub>2</sub> absorbents.

<sup>182</sup> The metal-promoted MgO sorbents newly proposed in this study can be connected with further <sup>183</sup> MD (Molecular Dynamics) and MC (Monte Carlo) studies to investigate the dynamic diffusion <sup>184</sup> and reaction behaviors and the equilibrium, as conducted by Kim et al.<sup>3</sup> These thermodynamic <sup>185</sup> properties can be utilized as key parameters in process modeling studies to predict the bulk process performance.1,2 186

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# 193 Appendix

Table 3: The structural data of  $CO<sub>2</sub>$  adsorption on MgO for the twofold bridge, fourfold bridge, and on top of the lattice magnesium sites.

	$d(C-O)/A$	$d(O_a-Mg)/A$	$d(O_h-Mg)/A$	$\angle$ O <sub>a</sub> -C-O <sub>b</sub> /deg	$E_{ads}$ / eV
Twofold bridge	2.30	2.73	2.64	163.8	$-0.20$
Fourfold hollow	2.86	2.58	2.66	176.6	$-0.34$
On top- $Mg$	3.55	3.24	3.33	179.3	$-0.08$

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