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Promoting Alkali and Alkali-Earth Metals on MgO for Enhancing CO2 Capture by First-Principles Calculation

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Abstract

Developing next-generation solid sorbents to improve the economy of pre- and post-combustion carbon capture processes has been challenging for many researchers. Magnesium oxide (MgO) is a promising sorbent because of its moderate sorption-desorption temperature and low heat of sorption. However, its low sorption capacity and thermal instability need to be improved. Various metal-promoted MgO sorbents have been experimentally developed to enhance the CO_2 sorption capacities. Nevertheless, rigorous computational studies to screen an optimal metal promoter have been limited to date. We conducted first-principles calculations to select metal promoters of MgO sorbents. Five alkali (Li-, Na-, K-, Rb-, Cs-) and 4 alkaline earth metals (Be-, Ca-, Sr-, Ba-) were chosen as a set of promoters. Compared with the CO_2 adsorption energy on pure MgO, the adsorption energy on the metal-promoted MgO sorbents is higher, except that for the Na-promoter, which indicates that metal promoting on MgO is an efficient approach to enhance the sorption capacities. Based on the stabilized binding of promoters on the MgO surface and the regenerability of sorbents, Li, Ca, and Sr were identified as adequate promoters among the 9 metals on the basis of PW91/GGA augmented with DFT+D2. The adsorption energies of CO₂ on metal-promoted MgO sorbents for Li, Ca, and Sr atoms are -1.13, -1.68, and -1.48 eV, respectively.

Introduction

To stop the progression of the greenhouse effect, the general consensus is that anthropogenic global CO₂ emission must be reduced over the next few decades. This CO₂ reduction has been mandated by worldwide associations, including the IPCC (Inter-governmental Panel on Climate Change) summit, since the first initiation of the Kyoto protocol. Therefore, capturing CO₂ from large stationary point sources, such as flue gas and syngas, has attracted the attention of many researchers.^{1,2}

⁸ CCS (Carbon Capture and Sequestration) techniques have been considered a viable method to
 ⁹ reduce the CO₂ level in the atmosphere. In CCS, chemical scrubbing with an aqueous amine-based

¹⁰ solvent a conventional carbon capture technique. However, recovering CO₂ from the solvent via ¹¹ a distillation process requires a large amount of energy for the re-boiler, where the solvent is va-¹² porized with a large amount of water. Due to the energy-intensive regeneration step, an alternative ¹³ carbon capture processes using solid sorbents has received considerable attention. ^{1–3} In the carbon ¹⁴ capture process based on solid sorbents, the heat of water vaporization may be avoided by replac-¹⁵ ing the liquid solution with solid particles. Moreover, the heat capacity of the solid particles is ¹⁶ lower than that of water.

Because of their low cost, abundance, and low toxicity, various alkali and alkaline earth metal oxides have been used as absorbents.⁴ Among these absorbents, MgO is preferred due to its low heat of absorption⁵ and moderate regeneration temperature (400-500 °C).^{6,7} However, the practical application of MgO has been limited because of a low CO₂ sorption capacity and thermal instability during regeneration.⁶ The CO₂ sorption capacity of MgO is half that of CaO.⁸

To enhance the sorption capacity, alkali metal-promoted MgO sorbents have been investigated 22 for a decade. Lee et al.⁹ developed a K₂CO₃-promoted MgO sorbent that has a CO₂ sorption ca-23 pacity of 12 wt% in the presence of 9 vol% H₂O and 1 vol% CO₂ with a fast and complete regen-24 eration. Alkali metal carbonate double salts supported on MgO, $(M_2CO_3)_n(MgCO_3)_p(MgO)_{1-p}$, 25 where M is Li, Na, K, and Cs, were reported.¹⁰ The maximum sorption capacity was 56 wt% in the 26 case of Na-double salts at 375 °C and 0.7 atm CO2 during PSA (Pressure Swing Adsorption). Xiao 27 et al.¹¹ reported that a K-promoted double salt MgO sorbent had the highest sorption capacity, 8.6 28 wt% in a 100 % CO₂ environment. Zhang et al.¹² synthesized a Na-promoted double salt MgO 29 sorbent, including NaNO₃, for CO₂ capture in the syngas of a pre-combustion process. During 30 multiple cycle tests, the CO₂ sorption capacity was maintained at 15 wt% in a 100 % CO₂ environ-31 ment. Yang et al.¹³ investigated the role of NaNO₃ in Ca-promoted double salt and reported that 32 NaNO₃ enhances the absorbent activity by facilitating ion diffusion. NaNO₃ on metal oxide has 33 also been shown to act as a phase transfer catalyst in the gas-solid reaction, which increases the 34 reaction rate and sorption capacity.¹⁴ Liu et al.¹⁵ developed a Cs-doped MgO based sorbent with 35 the wet impregnation method with a maximum sorption capacity of 8.3 wt% at 300 °C. Duan et 36

al. ¹⁶ conducted a computational study for Na-, K-, and Ca-promoted MgO sorbents using density
 functional theory (DFT) and phonon dynamics. They evaluated the adequate turnover temperature
 of each sorbent.

Many researchers have experimentally developed metal-promoted MgO sorbents. However, 40 to the best of our knowledge, only a few computational investigations of metal-promoted MgO 41 sorbents for CO₂ capture have been performed. Metal promoters are also limited to a few alkali 42 metals, such as potassium carbonate and sodium carbonate. In this study, we aimed to screen for an 43 optimal promoter for MgO sorbents that can be used as a CO₂ absorbent based on first-principles 44 calculations. We selected 9 metals as a set of potential promoters, including 5 alkali metals (Li-, 45 Na-, K-, Rb-, Cs-) and 4 alkaline earth (Be-, Ca-, Sr-, Ba-) metals. The effects of the 9 metal 46 promoters on MgO for CO₂ capture were evaluated via DFT calculations. 47

48 Computational details

Our DFT calculations were carried out with a periodic supercell model using the Vienna ab ini-49 tio simulation package (VASP)¹⁷⁻²⁰ with the PW91 exchange-correlation functional.^{21,22} A PAW 50 (projector augmented wave) method 23,24 was used as a plane wave basis set with an energy cutoff 51 of 400 eV. The long-range dispersion (van der Waals) contribution using the DFT + D2 approach of 52 Grimme²⁵ was applied to all calculations. The default dispersion parameters in VASP were used, 53 except for Cs and Ba, whose parameters were taken from Zhang et al.'s work.²⁶ In Venkataramanan 54 et al's work,²⁷ they validated PW91/GGA provides accurate results for alkali metals over a hybrid 55 exchange-correlation functional of MPW1PW91/6-311G(d,p). Thus, we expanded PW91/GGA 56 augmented with DFT+D2 for alkali and alkaline earth metals. We obtained an additional set of 57 results using an increased energy cutoff of 600 eV for Li and verified that the difference of energy 58 cutoff of 400 and 600 eV is unaffected, which implies that the energy cutoff of 400 eV is sufficient 59 to compare the promoters. 60



The defect-free MgO crystalline structure was cleaved in the (100) direction with a vacuum

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region of 15 Å. Each repeated slab is composed of 5 MgO layers. The adsorbate and upper 3 layers

- ⁶³ were allowed to be relaxed, whereas the lower 2 layers were to be fixed in their bulk positions.
- ⁶⁴ The adsorption energy, E_{ad} , of the metal promoter on bare MgO is defined as

$$E_{ad} = E_{P/host} - (E_P + E_{host}) \tag{1}$$

where $E_{P/host}$, E_{host} , and E_P represent the energies of the adsorption composites, host materials, and metal promoters, respectively. E_P is on the basis of the isolated atom. Lower values of E_{ad} represent a stronger adsorption of a promoter to MgO.

⁶⁸ A Bader charge analysis was conducted using a grid-based algorithm.²⁸ The charge in an atom ⁶⁹ was defined as the difference between the valence charge and the Bader charge.

70 Results and discussion

⁷¹ We conducted first-principles calculations to screen candidate metal promoters (alkali metals: Li-,
⁷² Na-, K-, Rb-, Cs- and alkaline earth metals: Be-, Ca-, Sr-, Ba-) for an optimal metal promoter on
⁷³ a MgO sorbent. First, the adsorption energies of 9 promoters on the MgO surface were calculated.
⁷⁴ CO₂ was loaded on the geometry-optimized metal-promoted MgO, and its adsorption energy was
⁷⁵ calculated and compared with the adsorption energy of CO₂ on MgO without the promoters.

⁷⁶ Adsorption of CO₂ in Non-promoted MgO

One CO₂ molecule was adsorbed to the (3×3) surface unit cell of MgO. The adsorption energy of CO₂ on the top of the lattice oxygen was the highest among the four adsorption potential sites, i.e., the twofold bridge, fourfold hollow, on top of oxygen, and on top of magnesium.

On the top of the lattice oxygen site, the CO_2 molecule was rotated every 15° in the vertical and horizontal direction to explore the ground state energy. Figure 1 shows the geometry-optimized structure of CO_2 adsorption on MgO. Table 1 provides the distances between the CO_2 and MgO surface atoms, CO_2 bending angle, and adsorption energy of CO_2 . These structural data for the



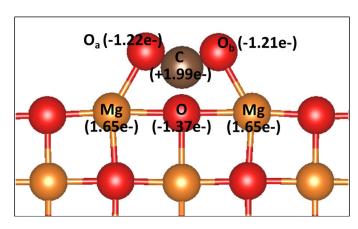


Figure 1: The optimized adsorption geometry of CO_2 on MgO surface with corresponding charge distributions; orange: magnesium, red: oxygen, brown color: carbon atoms.

⁸⁴ fourfold hollow, twofold bridge, and the top of the lattice magnesium sites are given in the Ap-

⁸⁵ pendix.

Table 1: The structural data of CO₂ adsorption on MgO for the top of the lattice oxygen site.

d(C-O) / Å	$d(O_a-Mg) / Å$	$d(O_b-Mg) / Å$	$\angle O_a$ -C-O _b /deg	E _{ads} / eV
1.45	2.20	2.18	133.6	-0.71

0.43e was transferred from the MgO surface to the CO₂ molecule. In this electron transfer, the largest charge transfer, 0.27e, was attributed to the lattice oxygen atom beneath the carbon atom.

⁸⁹ Promotion of Alkali and Alkaline Earth Metals on MgO

The alkali and alkaline earth metals were promoted on MgO. Initially, each promoter was placed on MgO at a distance of 1.2 Å. DFT energy optimization was utilized to obtain optimized configurations of promoters on MgO, as depicted in Fig. 2.

The energy of all promoters was minimized when they are bound on top of the lattice oxygen among the MgO adsorption sites. A single promoter was adsorbed on the MgO surface unit cells of (1×1) , (2×2) , (3×3) , and (4×4) , which corresponds to an adsorption coverage of 1/2, 1/8, 1/18, and 1/32 ML (monolayer). In Fig. 3, the adsorption energies of the promoters are

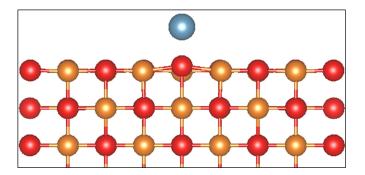


Figure 2: A side view of the relaxed structure for the promoter adsorbed on top of the lattice oxygen of MgO (3×3 surface unit cell); orange: magnesium, red: oxygen.

shown for different surface coverages. Except for the Be-promoter, 8 promoters show a similar 97 trend: the adsorption energy negatively correlates with the surface coverage due to the repulsive 98 force between the promoters.²⁹ However, at much higher coverage rates, the adsorption energies of 99 the promoters increase again. These stabilizations were attributed to an additional cluster binding 100 energy between the promoters, as described by Alfonso et al.³⁰ and Snyder et al.³¹ Unlike the 101 behaviors of the other promoters, the adsorption energy of Be continuously decreased until 1/2 102 ML. At a higher coverage of 1 ML, the adsorption energy of Be drastically increased to -4.39 eV. 103 This tendency is the result of a low cohesive energy of Be, which is approximately one-third that 104 of Ca.³² 105

The distances between repeated promoters are 12.7 Åfor 1/18 ML and 17.0 Åfor 1/32 ML. To exclude horizontal interactions between adjacent promoters, we selected a surface coverage of 1/18 ML because 12.7 Åis a sufficiently long distance between promoters and less computationally taxing than 1/32 ML.

Figure 4 represents the adsorption energies of promoters at 1/18 ML with electron transfers from promoters to MgO. Because alkaline earth metals are more electronegative than alkali metals in the same row of the periodic table of the elements (PTE), alkaline earth metals more strongly adsorb to MgO than do alkali metals.

Finazzi et al.³³ adsorbed alkali metals to the MgO surface using electron paramagnetic resonance (EPR) spectroscopy and density functional theory. They concluded that the adsorption en-

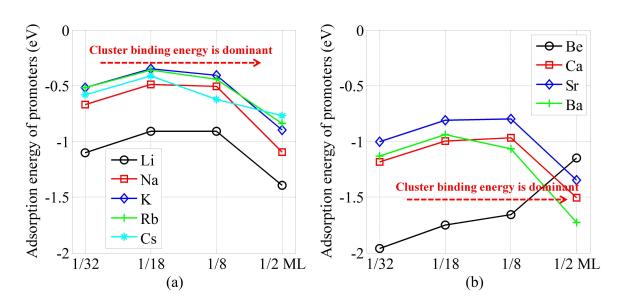


Figure 3: The adsorption energy of promoters on the MgO surface: (a) for alkali metals and (b) for alkaline earth metals.

ergies of alkali metals on MgO decrease in the following order on terrace sites: Li>Na>K. These patterns can also be observed in Fig. 4 because the electronegativity increases from the bottom to the top in PTE. Among the possible promoters the adsorption energies of Li and Be are the highest of the promoters in alkali and alkaline earth metals, whose binding is attributed to both polarization and covalent bonding with the largest charge transfer to MgO.

In general, the heat of chemisorption is greater than 0.52 eV (\approx 50 kJ/mol), which indicates that the cationization of alkali metals except for Li is contributed by mixed nature of physisorption and chemisorption. However, Li and alkaline earth metals are promoted on MgO via chemisorption, which more strongly stabilizes promoters.

Adsorption of CO₂ on Alkali- and Alkaline Earth Metal-Promoted MgO

¹²⁶ CO₂ was adsorbed on alkali- and alkaline earth metal-promoted MgO to investigate effects of ¹²⁷ promoters. Figure 5 represents the adsorption energies of CO₂ of alkali- and alkaline earth metal-¹²⁸ promoted MgO sorbents. The corresponding optimized structures and charge distributions are

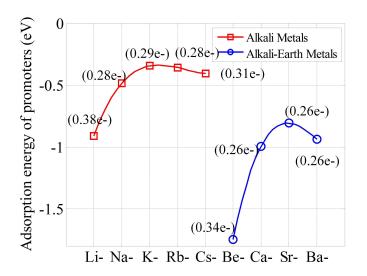


Figure 4: Adsorption energies of 9 promoters on MgO for the surface coverage, 1/18 ML. The values in parenthesis represent charge transfers from promoter to MgO.

presented in Table 2. Compared with the bending angles of CO_2 and distances of O_b -Mg and C-P for alkali metal promoters, both these angles and distances are too small for alkaline earth metal-promoted MgO. Except for the Na-promoter, the adsorption energies of CO_2 on the metal promoted MgO are higher than those on bare MgO. Similar to the highest adsorption energy found for the Li- and Be-promoter on MgO in alkali and alkaline earth metals, the adsorption energy of CO_2 was highest on Li- and Be-promoted MgO sorbents because of the high electronegativity and small Van der Waals radius, which easily transfer charge to the CO_2 molecule.

The amount of charge transferred from the MgO surface to the CO_2 molecule is 0.43e – in the absence of promoters, and more charge is transferred in the presence of promoters. The adsorbed CO_2 molecule becomes more negatively charged because both the promoters and the MgO in the vicinity of CO_2 donate electrons, thereby increasing the adsorption energy of CO_2 . These charge transfers are very drastic for alkaline earth metal promoters due to their stronger electronegativity.



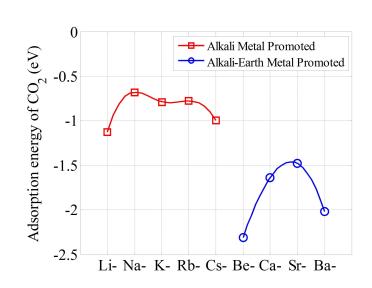


Figure 5: The adsorption energy of CO₂ on the metal-promoted MgO.

Table 2: The structural data and charge distribution of CO_2 adsorption on the metal-promoted MgO.

	Р	$\angle O_a$ -C- O_b	$d(O_b-Mg)$	d(C-P)	Charge distribution $(e-)$				CO ₂ Ads. En.	
	Г	(deg)	(Å)	(Å)	O _a	O_b	С	CO ₂	Р	(eV)
Akali Metals	Li-	136.8	2.21	2.34	-1.08	-1.23	1.43	-0.88	0.87	-1.13
	Na-	137.1	2.18	2.7	-1.11	-1.21	1.46	-0.86	0.83	-0.68
	K-	136.6	2.13	3.34	-1.00	-1.21	1.35	-0.86	0.84	-0.79
	Rb-	135.8	2.17	3.27	-1.10	-1.23	1.46	-0.87	0.84	-0.78
	Cs-	135.2	2.15	3.44	-1.14	-1.2	1.45	-0.89	0.84	-1.00
Akali- Earth Metals	Be-	122.9	2.11	1.68	-1.14	-1.24	0.78	-1.60	1.60	-2.31
	Ca-	120.9	2.10	2.36	-1.19	-1.19	0.98	-1.40	1.33	-1.68
	Sr-	121.5	2.08	2.52	-1.18	-1.22	1.00	-1.40	1.36	-1.48
	Ba-	119.3	2.09	2.69	-1.25	-1.25	1.03	-1.47	1.39	-2.02

 O_b is oxygen atom that has a shortest distance from MgO surface.

¹⁴¹ Impact of Metal Promoter on CO₂ capture

As noted in the section entitled **Promotion of Alkali and Alkaline Earth Metals on MgO**, the promoters in the top of row of PTE are more strongly adsorbed to the MgO because of their high electronegativity. However, for a metal with a large atomic radius, such as Cs and Ba, the adsorption strength increased as shown in Fig. 6, which is attributed to the attractive electrostatic interaction between Cs (or Ba) and neighboring four Mg.³⁴

On the contrary, the adsorption of CO₂ is enhanced when substrates with promoters are strongly 147 electropositive and basic, which suggests that the metals on the bottom of row of PTE are the 148 preferred promoters for a high sorption capacity. Reddy et al.³⁵ reported TGA experimental results 149 in which the CO₂ adsorption capacity was ranked as a function of the atomic radius and the basicity 150 of the alkali metals doped on CaO, i.e., Li<Na<K<Rb<Cs. Similarly, for sodium-, potassium-, and 151 cesium carbonate- doped MgO, the CO₂ sorption capacities were experimentally found to rank 152 as follows: Na<K<Cs.³⁶ The results presented in Fig. 6 also provide the same tendency for the 153 sorption capacities. Exceptional behaviors of Li and Be are attributed to the high cationizations 154 of these metals, which provide a high partial charge to CO₂. Lan et al.³⁷ calculated the binding 155 energy of CO₂ molecules to alkali and alkaline earth metals, and Li and Be showed much higher 156 binding energies than did the remaining metals. These effect can be observed in Table 2, such that 157 Li and Be are high positively charged as 0.87 and 1.60, respectively. 158

The complex correlations mentioned above generate the curves shown in Fig. 6. Hence, the 159 selection of the most adequate promoter is based on two aspects: i) the stabilization of promoter 160 binding on MgO and ii) the regenerability of CO₂. The adsorption energies of promoters must 161 exceed 0.52 eV for stable binding on MgO to ensure thermal stability. The adsorption energy of 162 CO₂ should be lower than 1.86 eV, which corresponds to the adsorption energy of CO₂ on CaO 163 (CaO + CO₂ \leftrightarrow CaCO₃). When the adsorption energy of CO₂ exceeds 1.86 eV, the desorption 164 would be difficult. Thus, an energy-intensive regeneration must be included, which results in a 165 high expenditure of the process. In terms of these two aspects, we conclude that the optimal 166 promoters are Li, Ca, and Sr on the basis of PW91/GGA augmented with DFT+D2. 167



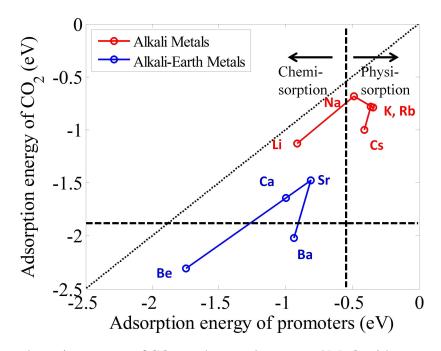


Figure 6: The adsorption energy of CO_2 on the metal-promoted MgO with respect to the adsorption energy of promoters.

To the best of the author's knowledge, Li_4SiO_4 and CaO have been utilized as high-temperature absorbents for CO₂ capture,⁷ although not as a promoter. These screened metal materials (Li, Ca, and Sr) have not been used as promoters on MgO, which allows for the development of possibly improved medium temperature sorbents.

172 Conclusions

Overcoming the energy penalty of carbon capture processes to develop improved solid-sorbents has been a major challenge for most material-related researchers. Therefore, we screened 5 alkali metals and 4 alkaline earth metal-promoted MgO sorbents using first-principles calculations in this work. In the set of 9 alkali metal promoters, most of alkali metals, except for Li, exhibited unstable binding on MgO via mixed chemisorption and physisorption, while the other promoters, i.e., alkali earth metals and Li, showed stable binding on MgO via chemisorption. Except for the ¹⁷⁹ Na-promoter, the adsorption energies of CO₂ increased compared with that on pure MgO due to ¹⁸⁰ promoter effects. Based on the stable promoter binding on MgO and the CO₂ regenerability, we ¹⁸¹ suggest that Li-, Ca-, and Sr-promoted MgO sorbents are the most appropriate CO₂ absorbents.

The metal-promoted MgO sorbents newly proposed in this study can be connected with further MD (Molecular Dynamics) and MC (Monte Carlo) studies to investigate the dynamic diffusion and reaction behaviors and the equilibrium, as conducted by Kim et al.³ These thermodynamic properties can be utilized as key parameters in process modeling studies to predict the bulk process performance.^{1,2}

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Appendix

Table 3: The structural data of CO_2 adsorption on MgO for the twofold bridge, fourfold bridge, and on top of the lattice magnesium sites.

	d(C-O) / Å	$d(O_a-Mg) / Å$	$d(O_b-Mg) / Å$	$\angle O_a$ -C-O _b /deg	E _{ads} / eV
Twofold bridge	2.30	2.73	2.64	163.8	-0.20
Fourfold hollow	2.86	2.58	2.66	176.6	-0.34
On top-Mg	3.55	3.24	3.33	179.3	-0.08

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