



A Liquid-like Quasi-solid Polymer Electrolyte for High-performance Sodium Metal Batteries

Journal:	<i>Journal of Materials Chemistry A</i>
Manuscript ID	TA-ART-03-2025-002012.R1
Article Type:	Paper
Date Submitted by the Author:	06-May-2025
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1 A Liquid-like Quasi-solid Polymer Electrolyte for High-performance Sodium 2 Metal Batteries

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18

19 Abstract

20 Conventional liquid electrolytes cannot adequately ensure the safety of sodium metal batteries
21 (SMBs), making quasi-solid polymer electrolytes (QSPEs) attractive alternatives. Herein, we
22 introduce a QSPE that exhibits liquid-level ionic conductivity with the mechanical robustness
23 of a solid polymer electrolyte. Optimizing the ratio of poly(vinylidene fluoride-co-
24 hexafluoropropylene) and poly(ethylene glycol)-block-poly(propylene glycol)-block-
25 poly(ethylene glycol) yields a “liquid-like” electrolyte exhibiting a room-temperature ionic
26 conductivity of 1.01 mS cm⁻¹, a Na⁺ transference number of 0.78, and a glass-transition
27 temperature of 22.5°C. Raman spectroscopy shows that the electron-donating -C-O-C- units
28 promote the formation of aggregated ion pairs, enabling an inorganic-rich interphase. Density
29 functional theory calculations predict that fluoride-containing reduction products form more
30 readily than non-fluorinated counterparts, leading to the formation of a stable solid electrolyte

31 interphase and the suppression of dendritic growth. Molecular dynamics (MD) simulations give
32 insights into the solvation environment and coordination of Na⁺ ions with electron-withdrawing
33 groups. Simulations also predict high ionic conductivity and transference numbers, confirming
34 the high ion transport in the QSPE seen experimentally. Consistent with these insights, a
35 Na/Na symmetric cell cycles stably for 200 h at high current density with superior charge
36 transfer proficiency, while a Na/Prussian blue full cell delivers an initial capacity of 159 mAh
37 g⁻¹ at 0.5 C and retains outstanding performance over 500 cycles. These findings underscore
38 the importance of judicious polymer blending in advancing high-performance SMBs.

39 **Keywords:** Polymer blends; Quasi-solid state polymer electrolytes; Activation energy;
40 Solvation; Sodium metal battery

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44 1. Introduction

45 Owing to its high theoretical specific capacity and low redox potential (-2.71 V vs standard
46 hydrogen electrode), sodium metal is a compelling anode for the post-lithium-ion era ¹ Sodium-
47 metal batteries (SMBs) can surpass lithium-ion batteries in energy density and cost per kWh ².
48 Yet, SMBs that employ conventional liquid electrolytes (LEs) face major safety issues
49 electrolyte leakage, flammability, and dendritic Na growth that can short-circuit the cell ³.
50 Parasitic reactions between the Na anode and the LE also corrode the metal during cycling,
51 forming an unstable solid electrolyte interphase (SEI) ⁴. Because the physicochemical
52 properties of SEI largely dictate battery performance ⁵, many strategies have been explored to
53 stabilize it, including artificial SEI layers formed by additives, high-concentration electrolytes,
54 and solvation-structure regulation to create inorganic-rich SEI ⁶⁻¹¹. Nonetheless, these
55 techniques do not fully eliminate the intrinsic drawbacks of LE systems.

56 Recent work has focused on solid-state and, in particular, quasi-solid polymer electrolytes
57 (QSPEs), which combine superior thermo-mechanical strength with effective suppression of
58 dendrite growth ^{12,13}. Unlike glass fiber separators that merely absorb LE, QSPEs feature a
59 polymeric backbone that can be engineered into a porous network capable of retaining LE ¹⁴.
60 This solid-liquid hybrid preserves the high ionic conductivity, elevated transference number,
61 and low interfacial resistance typical of liquid systems while possessing the enhanced thermal,
62 chemical, and mechanical robustness of solid separators ^{15,16}. The interconnected porosity of
63 QSPEs also promotes electrolyte uptake and retention, facilitating rapid ion transport and
64 further mitigating dendrite formation ^{17,18}. Crucially, the performance of QSPEs can be tuned
65 by tailoring the host matrix or incorporating functional additives; excessive crystallinity in
66 the polymer, however, restricts segmental motion and thereby limits ionic transportation ¹⁹.
67 Strategies to lower the polymer crystallinity include copolymerization, the incorporation of
68 nanofillers, disruption of the chain orientation, and blending with a second polymer ²⁰. When
69 two miscible polymers are combined in an optimized ratio, cooperative interactions can deliver
70 properties superior to either constituent alone ²¹. Such interactions enhance amorphous
71 character and chain mobility, thereby boosting ionic conductivity ²². As ionic mobility directly
72 governs electrochemical kinetics, enhancing ion transport accelerates the overall battery
73 performance. Accordingly, judicious polymer blending that raises ionic conductivity and
74 transference number while tailoring solvation chemistry to promote a robust SEI can transform
75 conventional QSPEs into a “liquid-like” QSPE for next-generation SMBs.

76 Polyvinylidene fluoride (PVDF) and its copolymer poly (vinylidene fluoride-co-
77 hexafluoropropylene) (PVDF-HFP) are among the most widely utilized polymer hosts for Na⁺
78 conduction²³. Their strong affinity for LEs, robust thermo-mechanical properties, and wide
79 electrochemical stability window (ESW) make them attractive for SMBs. The abundance of
80 electron-withdrawing fluorine atoms endows these polymers with a high dielectric constant
81 (8.4), which promotes salt dissociation²⁴. However, both PVDF and PVDF-HFP are semi-
82 crystalline; amorphous domains are confined between crystalline lamellae that severely restrict
83 ion transport²⁴. Blending them with other materials has emerged as an effective strategy to
84 expand the amorphous phase and enhance ionic conductivity^{21,24}. For example, Wunder *et al.*
85 blended PVDF-HFP with pentaerythritol tetrakis (3-mercaptopropionate) and pentaerythritol
86 tetra acrylate for SMB application²⁵. The system achieved an ionic conductivity of 1.4×10^{-5}
87 mS cm⁻¹ at 20°C and an ESW of 4.5 V (*vs.* Na/Na⁺).

88 However, comprehensive studies of novel PVDF-HFP blends and their effects on crystallinity,
89 ionic mobility, and interfacial modification of SEIs are still scarce. Herein, we introduce a
90 blend of PVDF-HFP with the triblock copolymer, poly(ethylene glycol)-block-poly(propylene
91 glycol)-block-poly(ethylene glycol) (PEG-PPG-PEG). This copolymer features hydrophilic
92 PEG end blocks flanking a hydrophobic PPG mid-block. The electron-donating -C-O-C-
93 groups enhance Na-salt solubility and adjust the solvation environment through inductive and
94 resonance effects. PEG-PPG-PEG also acts as a plasticizer, lowering the crystallinity of PVDF-
95 HFP and thereby promoting ion transport. Free-standing polymer hosts have been prepared by
96 blending PVDF-HFP with PEG-PPG-PEG at various weight ratios, and their ionic mobility is
97 investigated after activation with a LE. Crystallinity decreases steadily as the triblock
98 copolymer content increases, while electrolyte uptake and porosity rise sharply. The optimized
99 blend QSPE (70 wt.% PVDF-HFP/30 wt.% PEG-PPG-PEG) exhibits an ionic conductivity of
100 1.01 mS cm⁻¹ at 25 °C, which is 405% higher than that of the pristine PVDF-HFP. Raman and
101 Fourier-transform infrared (FTIR) spectroscopy confirm liquid-like behavior, showing a larger
102 fraction of aggregated ion pairs (AGGs). Thermo-mechanical tests reveal enhanced robustness,
103 corroborated by uniform sodium deposition and stable, reversible stripping/plating in a Na//Na
104 symmetric cell. Density functional theory (DFT) calculations and molecular dynamics (MD)
105 simulations support these observations, clarifying the favorable solvation environment, high
106 ionic conductivity, and transference number of the electrolyte. A fluoride-rich, anion-derived
107 SEI boost cycling stability. Consequently, a Na//Prussian blue full cell delivers a discharge

108 capacity of 120 mAh g⁻¹ for 600 cycles at 0.5 C, retains good rate capability, and maintains an
109 average Coulombic efficiency of 98 %.

110 2. Results and discussions

111 Detailed experimental procedures, instrumentation, test parameters, and all relevant equations
112 are provided in the Supplementary information.

113 2.1 Structural and Chemical Analysis of the QSPEs

114 **Figure 1a** depicts how increasing the PEG-PPG-PEG content alters the crystallinity of the
115 parent PVDF-HFP matrix, as revealed by X-ray diffraction (XRD). Pristine PVDF-HFP
116 (denoted as Pristine_100) exhibits characteristic α -phase diffraction peaks at 17.6°, 19.8°,
117 26.3°, and 39.0°, corresponding to the (100), (020), (110), and (021) planes, respectively²⁶. As
118 the PEG-PPG-PEG fraction rises, these peaks broaden and decrease in intensity, indicating a
119 growing amorphous fraction. PEG-PPG-PEG disrupts the α -phase lamellar ordering of PVDF-
120 HFP, promoting chain mobility and enlarging the amorphous fraction. The degree of
121 crystallinity (X_{XRD} , %) was quantified using the method described by Vo et al²⁶.

$$122 \quad X_{XRD} = \frac{A}{A_o} \times 100$$

123 where A is the summed area of all crystalline peaks, and A_o is the total integrated area of all
124 peaks in the XRD pattern. The degree of crystallinity in pristine PVDF-HFP is 33.8%, whereas
125 incorporating 10, 20, 30, and 40 wt.% PEG-PPG-PEG reduces it to 29.1, 21.2, 13.2, and 11.4%,
126 respectively (**Figure S1**). This progressive loss of crystallinity upon blending likely relaxes
127 chain packing and, in turn, promotes ionic conduction.

128 FTIR of pristine_100 shows characteristic stretching vibrations of the fluorinated backbone at
129 1405, 1173, and 876 cm⁻¹ (**Figure 1b,c**). The 1173 cm⁻¹ band arises from C-F stretching
130 vibrations²⁷. Notably, the intensity of the 1100 cm⁻¹ band attributed to the -C-O-C- bond
131 increases with rising PEG-PPG-PEG content²⁸, confirming the successful incorporation of the
132 triblock copolymer into the PVDF-HFP matrix. Moreover, the 1068 cm⁻¹ band, typical of
133 crystalline PVDF-HFP²⁷, appears broader and weaker in intensity in the blend system,
134 indicating the amorphous nature of the blend. These FTIR findings corroborate the XRD
135 evidence of enhanced amorphization.

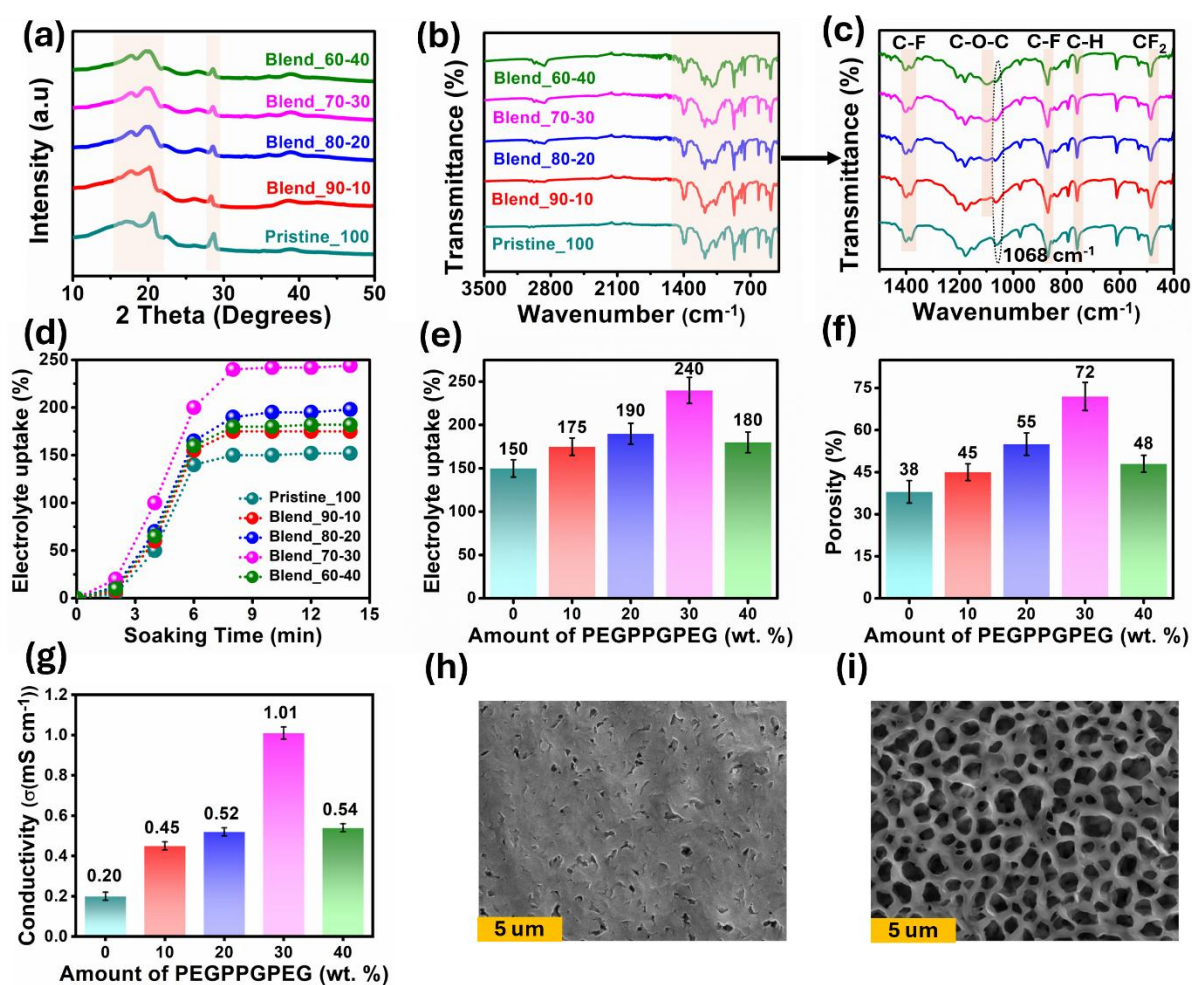
136 QSPEs were prepared by activating the polymer matrices with a LE composed of 1 M NaClO₄
137 in ethylene carbonate (EC)/dimethyl carbonate (DMC)/fluoroethylene carbonate (FEC), and

138 their physicochemical properties were subsequently evaluated. Among the polymer matrices
139 evaluated, the PVDF-HFP/PEG-PPG-PEG blend containing 30 wt.% triblock copolymers
140 (blend_70-30) shows the greatest electrolyte uptake, absorbing 240% of its own mass after 10
141 min of immersion (**Figure 1d,e**). Relative to pristine_100, which has 38% of porosity, the
142 blend_70-30 reaches 72% of porosity an increase of nearly 90% (**Figure 1f**). The trends in
143 porosity and electrolyte uptake are consistent for all samples and are likewise reflected in their
144 ionic conductivities (**Figure 1g**). Blend_70-30 QSPE records a room-temperature ionic
145 conductivity of 1.01 mS cm^{-1} , 405% higher than that of pristine_100 QSPE (0.20 mS cm^{-1}).
146 This enhanced uptake is attributed to the blend's larger amorphous fraction. Because cross-
147 sectional thickness also influences physical and electrochemical properties, we optimized the
148 membrane thickness. Ionic-conductivity and electrolyte-uptake analyses show that a $150 \mu\text{m}$
149 membrane performs best, and this thickness was adopted for subsequent experiments (**Figure**
150 **S2**).

151 Surface morphology was examined by field-emission scanning electron microscopy (FESEM)
152 for both the pristine PVDF-HFP host and blend_70-30 (**Figure 1h,i**). Unlike pristine PVDF-
153 HFP, which presents a rough surface with few pores, blend_70-30 displays an interconnected
154 porous network containing macropores $0.5\text{-}2.0 \mu\text{m}$ in diameter, accounting for its higher
155 porosity. FESEM images at various magnifications confirm that this porous structure is
156 uniform throughout the blend_70-30 matrix, whereas PVDF-HFP membranes exhibit the rough
157 morphology typical of PVDF-HFP (**Figure S3**)²¹. The macropores in blend_70-30 facilitate
158 electrolyte diffusion through the matrix, enlarge the membrane's active area, and thus increase
159 electrolyte uptake. Elemental mapping indicates that PVDF-HFP and PEG-PPG-PEG are
160 uniformly blended without noticeable agglomeration (**Figures S4 and S5**). Therefore, the
161 blend_70-30 membrane offers an architecture well-suited for QSPE development.

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164

165 **Figure 1.** (a) XRD patterns, (b,c) FTIR spectra, (d) time-dependent electrolyte uptake, (e)
 166 equilibrium electrolyte uptake, and (f) porosity of the PVDF-HFP and blend membranes. (g)
 167 Room-temperature ionic conductivity of the corresponding QSPEs. (h,i) FESEM images of (h)
 168 pristine_100 and (i) blend_70-30 membranes.

169 2.2 Temperature-dependent ionic conduction and thermo-mechanical properties

170 **Figure 2a** presents the temperature dependence of ionic conductivity for LE-activated PVDF-
 171 HFP and blend_70-30; these data are used to determine the activation energy (**Figure 2b**).
 172 Detailed electrochemical impedance spectroscopy (EIS) results for each membrane are
 173 provided in **Figure S6**. At every temperature tested, the blend_70-30 QSPE outperforms the
 174 pristine_100 QSPE; its conductivity equals or even exceeds that of conventional LEs²⁹. The
 175 improvement stems from the blend's optimized amorphous fraction: incorporation of PEG-

176 PPG-PEG disrupts PVDF-HFP crystalline domains, creating additional pathways for ion
177 transport. Blend_70-30 QSPE follows Arrhenius behavior typical of LEs³⁰ with activation
178 energy for ion conduction of 0.12 eV, whereas pristine PVDF-HFP exhibits a higher activation
179 energy (0.169 eV), reflecting slower Na⁺ kinetics in the pristine QSPE.

180 The mechanical properties of a QSPE are critical because they influence both dendrite growth
181 and its suppression³¹. Stress-strain tests were performed according to ASTM D882 (**Figure**
182 **2c**). The blend_70-30 shows a tensile modulus (E_{t-mod}) of 24.48 MPa nearly twice that of
183 pristine_100 (13.40 MPa), indicating higher resistance to deformation. Its elongation at break,
184 a measure of the ability to deform plastically before fracturing, reaches 114%, whereas the
185 pristine_100 fails at 66%. The ultimate tensile strength likewise rises from 3.55 MPa
186 (pristine_100) to 4.85 MPa (blend_70-30). Incorporating 30 wt.% PEG-PPG-PEG thus
187 enhances both flexibility and modulus, enabling the membrane to withstand the tension stresses
188 generated by dendritic growth and thereby supporting safer, longer-lived battery operation³¹.
189 Optical photographs illustrating the blend_70-30 membrane's flexibility and integrity are
190 provided in **Figure S7**.

191 Thermal stability was evaluated by thermogravimetric-differential thermogravimetric (TGA-
192 DTG) analysis. The pristine_100 shows a single, sharp weight loss down to 30% at 420 °C
193 (**Figure 2d**), consistent with the known thermal decomposition of PVDF-HFP via chain
194 scission and elimination reactions at 400-450 °C^{24,32}. By contrast, the blend_70-30 exhibits a
195 two-step degradation profile (**Figure 2e**). The first step, a 30% weight loss at 350 °C,
196 corresponds to oxidative and random scission of the ether bonds in PEG-PPG-PEG, reported
197 to commence at 300-360 °C^{33,34}. The second step, above 400 °C, marks the onset of PVDF-
198 HFP degradation. Incorporation of PEG-PPG-PEG acting as a plasticizer and reducing
199 crystallinity (as confirmed by XRD) slightly lowers the degradation temperature of PVDF-HFP
200 by disrupting its semicrystalline structure and thus reducing the activation energy for thermal
201 decomposition. DTG traces corroborate this shift. In both membranes, the 30% residue is
202 attributed to fluorinated char and other thermally stable species. Moreover, the absence of any
203 weight loss near 80-120 °C indicates negligible moisture or volatile content, confirming the
204 membranes' compatibility with sodium anode and suitability for SMB operation.

205 Thermal transitions of the polymer membranes were evaluated by differential scanning
206 calorimetry (DSC) analysis. Introducing PEG-PPG-PEG lowers the glass-transition
207 temperature (T_g) from 63.4 °C to 22.5 °C (**Figure 2f**), indicating greater chain flexibility and,

208 in turn, improved ionic transport. The blend_70-30 also exhibits a lower melting temperature
209 (T_m) than the pristine_100, signifying the disruption of crystalline domains³⁵. In addition to
210 the degree of crystallinity from the XRD patterns, we also quantified the degree of crystallinity
211 from DSC by integrating the melting endotherm to obtain the melting enthalpy (ΔH_m)³². Using
212 the ideal heat of fusion for fully crystalline PVDF-HFP ($\Delta H_m^0 = 104.7 \text{ J g}^{-1}$)³², the degree of
213 crystallinity (X_{DSC} , %) was calculated as:

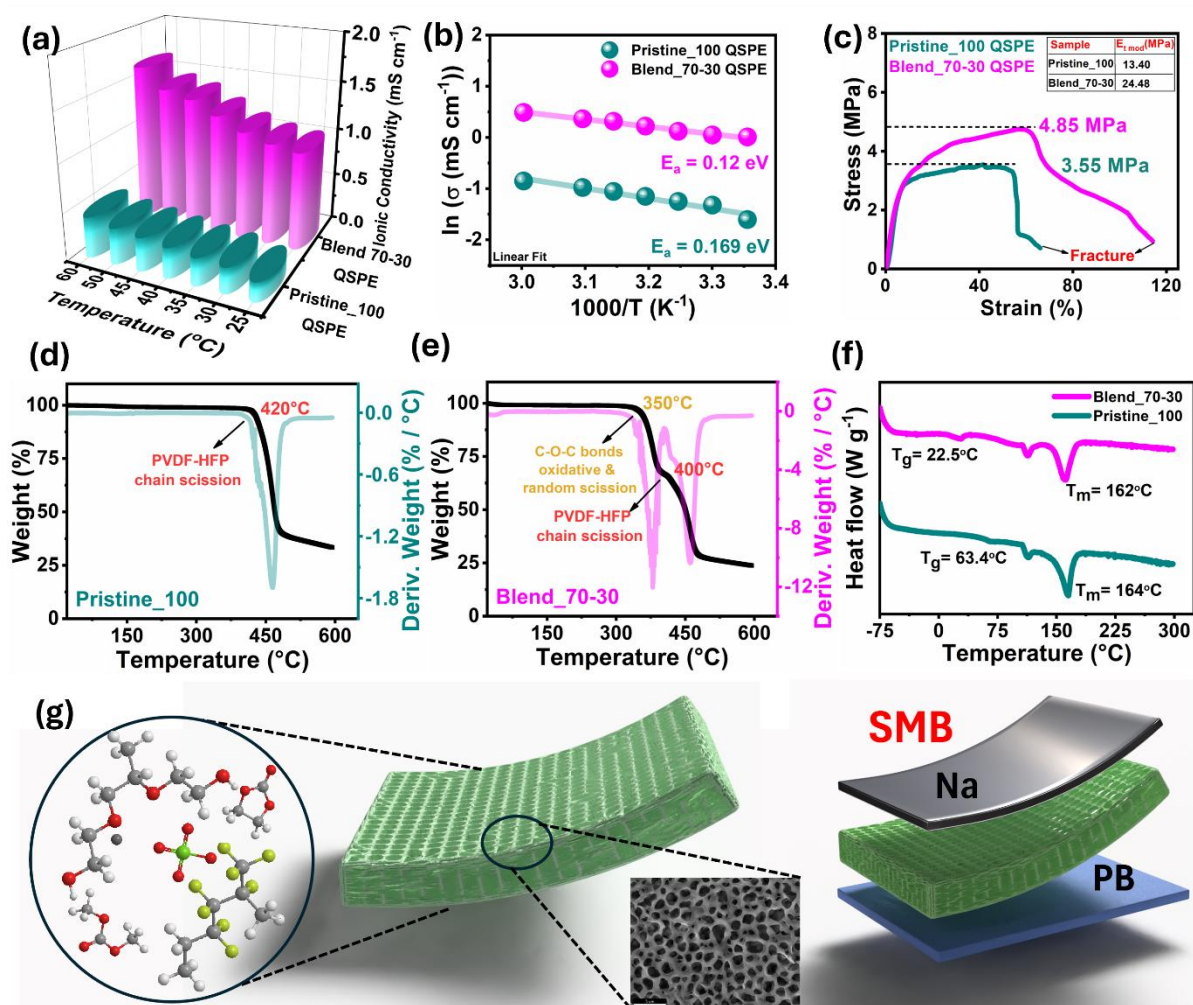
$$214 \quad X_{DSC} = \frac{\Delta H_m}{\Delta H_m^0} \times \frac{1}{W_f} \times 100$$

215 where W_f is the weight fraction of PVDF-HFP in the blend samples.

216 The pristine_100 exhibits a ΔH_m of 53.6 J g^{-1} , corresponding to a crystallinity of 51%. In
217 contrast, the blend_70-30 membrane shows a ΔH_m of 19.08 J g^{-1} ; after normalizing to the 70
218 wt.% PVDF-HFP content, its crystallinity is 26%. This pronounced reduction highlights the
219 disruptive influence of PEG-PPG-PEG on PVDF-HFP crystallization, most likely through
220 steric hindrance and plasticization by the flexible triblock chains.

221 In conclusion, the blend_70-30 system featuring robust thermo-mechanical properties, an
222 interconnected porous network, and high ionic conductivity supports a uniform, high Na^+ flux,
223 promotes even sodium deposition, and thus suppresses dendrite growth. A schematic of the
224 QSPEs and their integration into an SMB with Prussian blue (PB) cathode is shown in **Figure**
225 **2g**.

226



227

228 **Figure 2.** (a) Temperature-dependent ionic conductivities and (b) corresponding Arrhenius
 229 plots for pristine_100 and blend_70-30 QSPEs. (c) Room-temperature stress-strain curves of
 230 pristine_100 and blend_70-30. (d,e) TGA-DTG profiles of (d) pristine_100 and (e) blend_70-
 231 30. (f) DSC thermograms showing T_g and T_m for pristine_100 and blend_70-30. (g) Schematic
 232 illustration of the developed QSPE and its integration into an SMB with a PB cathode.

233 2.3 Solvation properties

234 Electron-withdrawing groups enhance the solubility of positively charged cations by inducing
 235 local dipoles that promote Na^+ dissociation and lower the energy barrier for ion migration³⁶.
 236 The strong electron-withdrawing $-\text{CF}_2$ moieties in PVDF-HFP is further activated by the ester
 237 group $(-\text{C}-\text{O}-\text{C}-)$ of PEG-PPG-PEG³⁷, improving Na-salt solubility in the blend_70-30 QSPE.
 238 FTIR spectra of blend_70-30 and pristine_100 QSPEs, together with the NaClO_4 -based LE,
 239 are compared in **Figure 3a**. In the blend_70-30 QSPE, the carbonyl stretching band $(-\text{C}=\text{O}-)$

240 shifts to lower wavenumbers, whereas the -C-O- band moves to higher wavenumbers,
241 indicating specific host-electrolyte interactions¹⁸. In contrast, the pristine_100 QSPE lacks
242 the carbonyl band and shows a much weaker -C-O- band, signifying minimal interaction with
243 the LE. Owing to the high electronegativity of the -CF and ester groups illustrated
244 schematically in **Figure 3b** the blend_70-30 QSPE becomes transparent after LE activation
245 (**Figure 3c**).

246 Raman spectroscopy was employed to verify the chemical interactions between the blend_70-
247 30 matrix and the LE (**Figure 3d**). The carbonyl-stretching band (-C=O-) at 715 cm⁻¹¹⁸
248 prominent in the neat LE remains visible in the blend_70-30 QSPE but is absent in pristine_100
249 QSPE, confirming that the blend_70-30 QSPE retains the electrolyte's local chemistry.
250 Spectral deconvolution of the 715 cm⁻¹ band in the blend_70-30 QSPE reveals that AGGs
251 constitute 54% of the species a substantial increase relative to the LE (**Figure 3e,f**). Conversely,
252 the proportion of contact ion pairs (CIPs) is lower than in the LE. A larger AGG population
253 signifies lower local polarity, which can widen the ESW and improve voltage tolerance^{18,38,39}.
254 Moreover, the accompanying increase in anion concentration favors the formation of an
255 inorganic-rich, stable SEI^{38,40}.

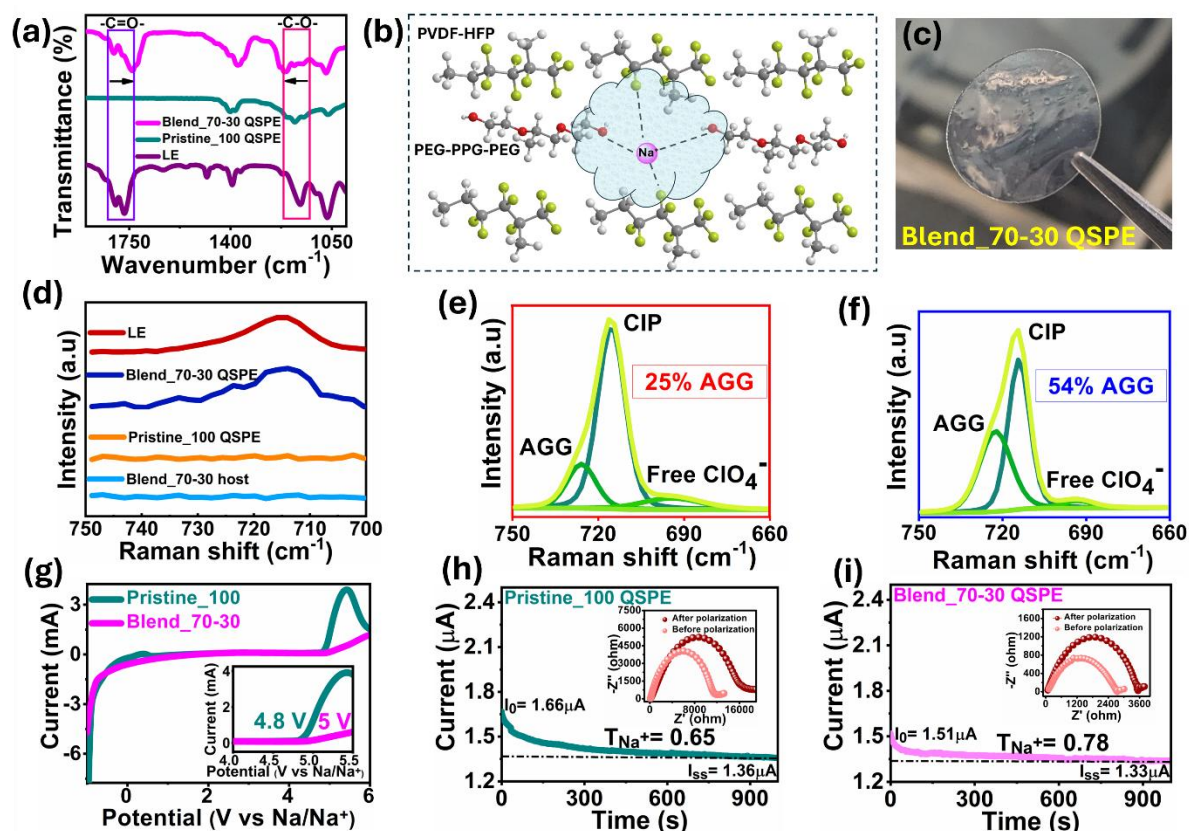
256 QSPEs combine high ionic conductivity with a broader ESW, giving them a clear advantage
257 over conventional LEs and offering scalability. In this study, pristine_100 and blend_70-30
258 QSPEs display comparable reduction stability, but the blend_70-30 QSPE shows superior
259 oxidative stability, sustaining an ESW of about 5 V (**Figure 3g**). Electron-withdrawing groups
260 typically enhance oxidative resistance by lowering the electron density of the polymer
261 backbone^{18,23}. Accordingly, the pristine_100 matrix, which contains more electron-
262 withdrawing segments, exhibits a higher oxidation current, whereas the -C-O-C- groups in
263 PEG-PPG-PEG moderate the local electronic environment, improving the oxidation stability
264 of blend_70-30. The wider ESW also aligns with solvation effects: the higher content of AGG
265 in blend_70-30 increases anion concentration and reduces local polarity, both of which are
266 known to extend the ESW^{18,39,40}. Consequently, the QSPEs containing -C-O-C- groups exhibit
267 ESW above 4.8 V (**Figure S8**).

268 Chronoamperometry was employed to determine the Na⁺ transference number, which was
269 calculated with the Bruce-Vincent method^{14,31}. As shown in **Figure 3i**, the blend_70-30 QSPE
270 displaying a room-temperature ionic conductivity of 1.01 mS cm⁻¹ achieves a Na⁺ transference
271 number of 0.78, essentially matching that of the LE^{15,41}. By contrast, pristine_100 QSPE shows

272 a lower transference number of 0.65 (**Figure 3h**). The high value confirms efficient salt
 273 dissociation within the blend_70-30 matrix.

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276

277 **Figure 3.** (a) FTIR spectra of the LE and QSPEs. (b) Schematic illustration of sodium-ion
 278 interaction with the blend_70-30 matrix. (c) Photograph of the blend_70-30 QSPE. (d) Raman
 279 spectra of the blend_70-30 host, pristine_100 QSPE, blend_70-30 QSPE, and LE. (e,f)
 280 Deconvoluted Raman spectra of (e) LE and (f) blend_70-30 QSPE. (g) Linear sweep
 281 voltammetry showing the ESW of pristine_100 and blend_70-30 QSPEs (inset: magnified
 282 curve from 4.0 to 5.5 V). (h,i) Chronoamperometry of Na/pristine_100 QSPE//Na and
 283 Na/blend_70-30 QSPE//Na cells (inset: AC impedance spectra before and after polarization).

284 2.4 Computational

285 2.4.1 DFT Calculations

286 Theoretical calculations were performed to elucidate the contributions of solvent molecules,
 287 polymeric macromolecules, and Na salt to the formation of the SEI. The electronic structures
 288 of EC, FEC, DMC, PVDF-HFP, PEG-PPG-PEG, and NaClO₄ were calculated using DFT as

289 implemented in the ONETEP program^{42,43}. A kinetic energy cutoff of 1000.0 eV was used for
290 the basis set, which consists of psinc functions equivalent to plane waves⁴⁴. The orbitals are
291 represented using non-orthogonal generalized Wannier functions with a localization radius of
292 $10.0 a_0$ ⁴⁵. The Perdew-Burke-Ernzerhof (PBE) generalized gradient approximation was used
293 for the exchange-correlation functional. The shapes and energy levels of the highest occupied
294 molecular orbital (HOMO) and the lowest unoccupied molecular orbital are shown in **Figure**
295 **4a**. The presence of fluorinated groups in FEC lowers its LUMO energy compared to EC.
296 Similarly, the fluorine groups in PVDF-HFP reduce its LUMO energy level. A lower LUMO
297 energy increases the likelihood of reduction at the Na metal anode. The reduction of these
298 fluorinated species is expected to produce fluoride-rich products, passivating further reactions,
299 stabilizing the SEI, and suppressing dendrite growth. Thus, combining solvation structure
300 analysis with theoretical calculations suggests that the SEI will be predominantly composed of
301 inorganic species, which should contribute to longer cycle life in SMBs.

302 Overall, DFT calculations reveal that the electron-withdrawing fluorine atoms in FEC and
303 PVDF-HFP lower the LUMO levels compared to their non-fluorinated counterparts. This
304 lowering of the LUMO promotes the reductive decomposition of FEC and PVDF-HFP at the
305 sodium metal surface, facilitating the formation of a robust, stable, fluoride-rich SEI that
306 passivates further electrolyte degradation and mitigates dendrite formation. Moreover, the
307 increased concentration of AGGs induced by PEG-PPG-PEG widens the ESW and contributes
308 additional inorganic components to the SEI through the decomposition of salt anions³⁸.

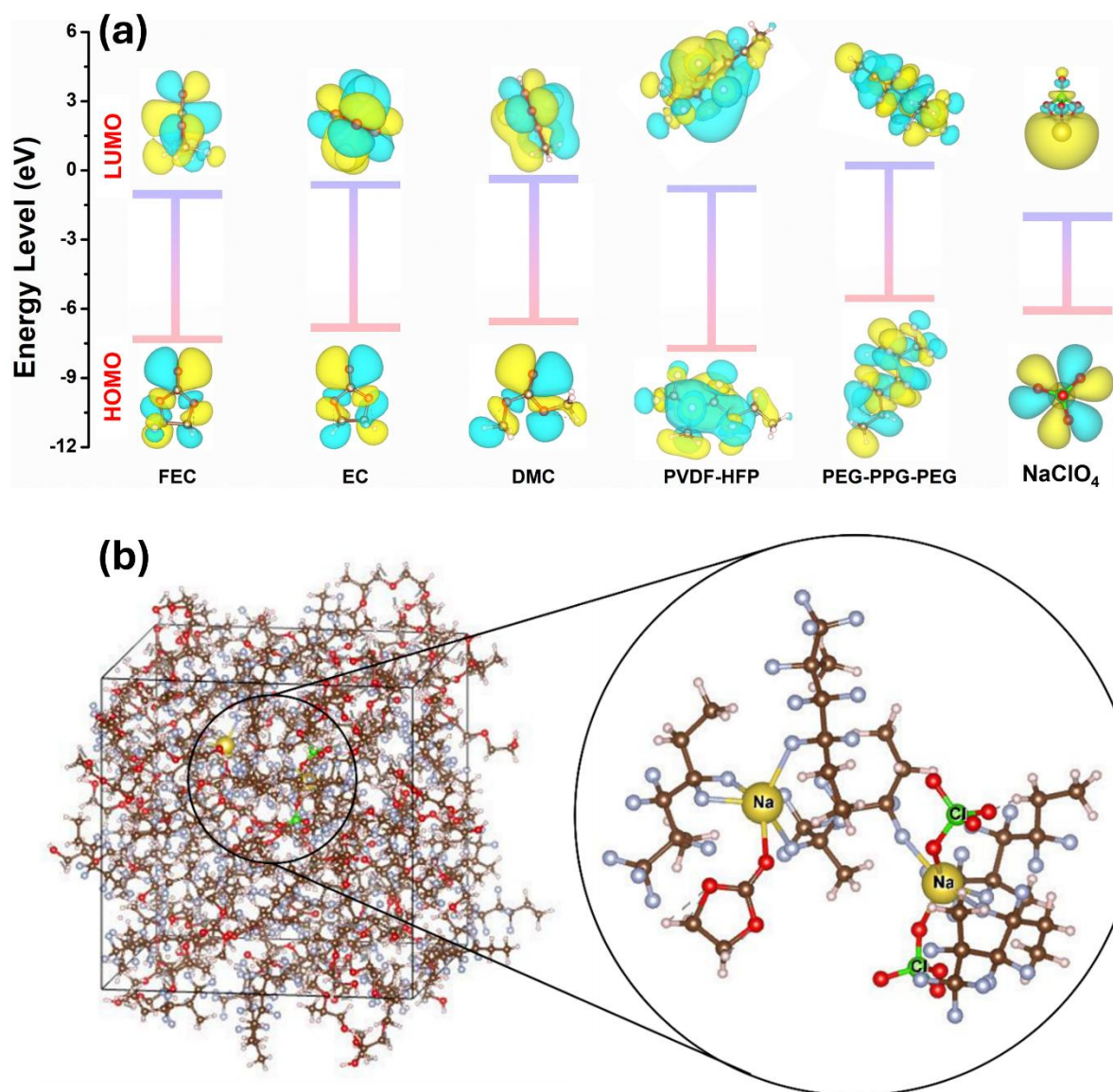
309 **2.4.2 MD simulations**

310 To gain further insights into the solvation structure, MD simulations of the electrolyte system
311 were performed using the Multi-Atomic Cluster Expansion (MACE) force field⁴⁶. To replicate
312 the experimental composition of blend_70-30 QSPE, a periodic simulation cell (25.0 \AA) was
313 constructed using PACKMOL software⁴⁷, containing 7 EC, 2 FEC, 5 DMC, 44 PVDF-HFP,
314 20 PEG-PPG-PEG, and 2 NaClO_4 , totaling 1714 atoms. Geometry optimization was first
315 carried out until all forces fell below 0.05 eV \AA^{-1} . MD simulations were then performed in the
316 NVT ensemble (number of particles (N), volume (V), and temperature (T) were kept constant)
317 using a Langevin thermostat at 300 K. The temperature and total energy profiles during the
318 MD simulation are shown in **Figure S9**, indicating that the system reaches equilibrium after
319 100 ps. A snapshot of the equilibrated structure at 100 ps is shown in **Figure 4b**, along with a
320 zoomed-in view of the salt coordination environment. Na^+ cations are found to coordinate
321 predominantly with the fluorine atoms of the PVDF-HFP polymer chains, while one Na^+ cation

322 also coordinates with the carbonyl oxygen of an EC molecule in the solvent. Another Na⁺ cation
323 is surrounded by ClO₄⁻ anions within its solvation shell, forming an AGG.

324 Transport properties of complex polymeric electrolytes can be calculated from the Onsager
325 transport coefficients, which generally decrease with increasing polymer chain length in
326 simulations⁴⁸. Here, monomeric units of PVDF-HFP and PEG-PPG-PEG were used in MD
327 simulations. As a result, the computed transport properties may represent an upper bound
328 relative to those achievable in practical polymeric systems. The methodology for calculating
329 diffusion coefficients, ionic conductivity, and transference numbers is detailed in the
330 Supplementary Information (Section 2.1). Diffusion coefficients were obtained from the slopes
331 of the mean squared displacement plots for Na⁺ and ClO₄⁻ ions, as shown in **Figure S10**.
332 Theoretical calculations yield diffusion coefficients of $2.57 \times 10^{-6} \text{ cm}^2 \text{ s}^{-1}$ for Na⁺ and 3.41×10^{-7}
333 $\text{ cm}^2 \text{ s}^{-1}$ for ClO₄⁻, along with a total ionic conductivity of 2.10 mS cm^{-1} . These values support
334 the experimentally observed high performance of the blend_70-30 QSPE. The computed Na⁺
335 transference number of 0.90 further underscores the capability for efficient ion transport in the
336 blend_70-30 QSPE. These predictions are consistent with the typical overestimations
337 associated with MD simulations using short-chain polymers. Collectively, these multiscale
338 computational and experimental insights highlight the pivotal role of electron-withdrawing
339 groups and fluorinated components in modeling solvation characteristics, stabilizing
340 interphases, and promoting efficient ion transport in SMBs.

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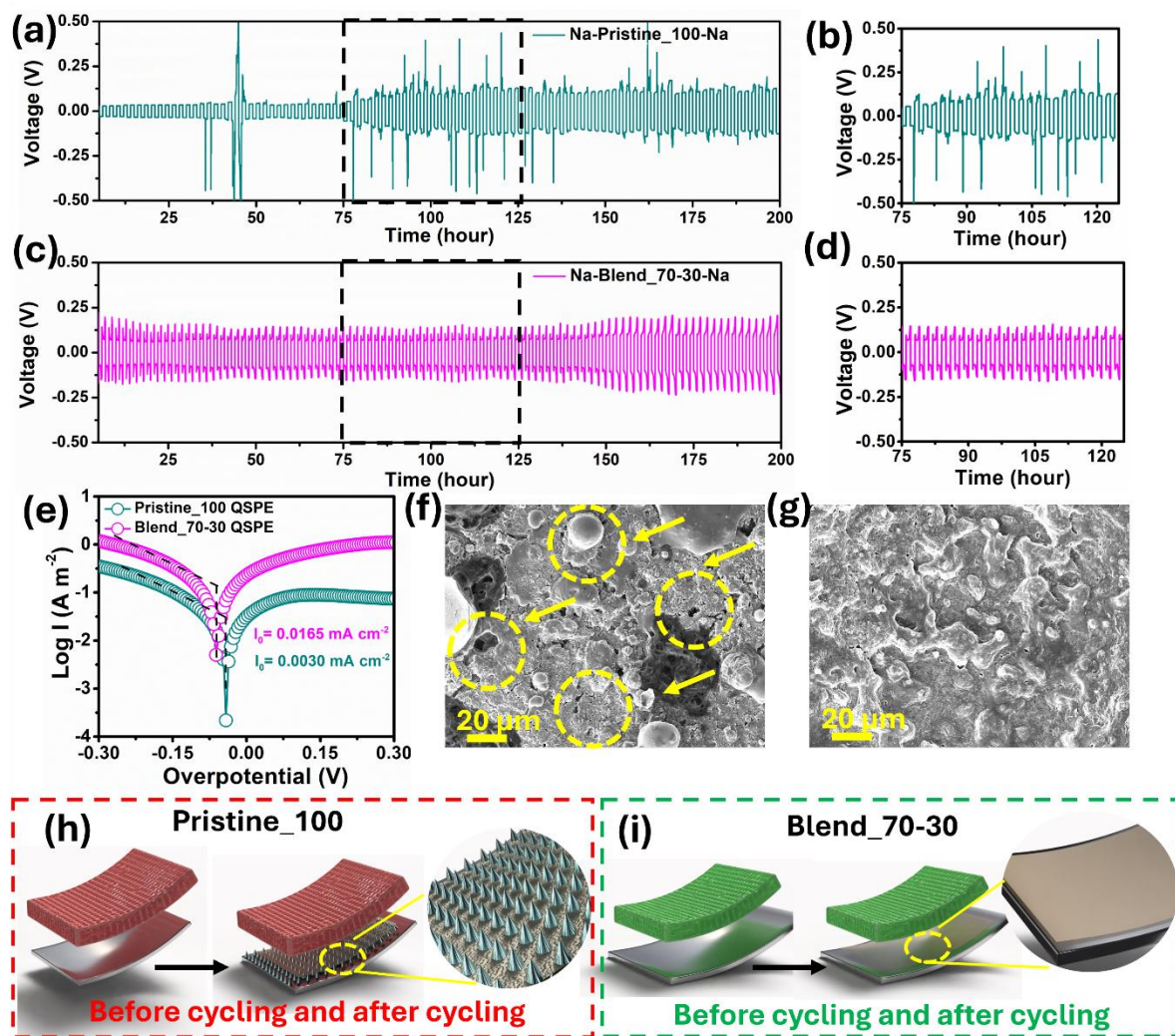
343 **Figure 4.** (a) Molecular orbital shapes and energy levels of the HOMO and LUMO for FEC,
 344 EC, DMC, PVDF-HFP, PEG-PPG-PEG, and NaClO₄. (b) Snapshot of the electrolyte system
 345 from MD simulations after 100 ps.

346 2.5 Electrochemical properties

347 Since solvation properties directly influence electrochemical behavior, further investigations
 348 were carried out in this regard. Galvanostatic stripping/plating of Na was evaluated using
 349 Na//Na symmetric cells assembled with the blend_70-30 QSPE, with a symmetric cell based
 350 on the pristine_100 QSPE also tested for comparison. The cell with the blend_70-30 QSPE,
 351 benefitting from the electron-donating -C-O-C- groups of PEG-PPG-PEG, exhibits lower local
 352 polarity and superior solvation effects, resulting in a lower deposition overpotential compared

353 to the cell with the pristine_100 QSPE (**Figure 5a-d**). The stripping/plating overpotential for
354 blend_70-30 QSPE cell is approximately 250 mV with a uniform and stable profile (**Figure 5c,**
355 **d**), significantly lower than that of the pristine_100 QSPE cell (~350 mV). While the
356 pristine_100 QSPE cell initially shows a lower overpotential, it suffers from short-circuiting
357 within 75 hours, likely due to the non-uniform deposition of Na leading to dendrite formation
358 ^{38,49}. Furthermore, the lower AGG concentration in the pristine_100 cell likely results in the
359 formation of an organic-rich SEI ¹⁸, accelerating dendrite growth and correlating with
360 the unstable stripping/plating behavior (**Figure 5a,b**). Overall, galvanostatic stripping/plating
361 analyses indicate that the blend_70-30 QSPE cell more effectively suppresses Na dendrite
362 formation compared to the pristine_100 QSPE cell.

363 To investigate the kinetics of Na⁺ stripping/plating, Tafel plots were obtained using Na//Na
364 symmetric cells assembled with pristine_100 and blend_70-30 QSPEs. As shown in **Figure 5e**,
365 the blend QSPE exhibits an exchange current density of 0.0165 mA cm⁻², whereas the
366 pristine_100 QSPE shows a significantly lower value of 0.003 mA cm⁻². Notably, a higher
367 exchange current density indicates reduced Na⁺ nucleation barriers during the electrodeposition
368 process ⁵⁰. The fivefold enhancement in exchange current density for the blend_70-30 QSPE
369 reflects improved charge-transfer kinetics at the Na electrode-electrolyte interface, which can
370 be correlated with the formation of a highly conductive and stable inorganic-rich SEI ⁵¹. Post-
371 mortem morphological analysis by FESEM was further conducted to correlate the observations
372 from overpotential measurements, exchange current densities, and Na deposition behavior after
373 10 galvanostatic cycles. As anticipated from the solvation characteristics and the galvanostatic
374 plating/stripping profiles, the pristine_100 QSPE exhibits non-uniform Na deposition, with
375 visible fractures and roughness (**Figure 5f**). Such porous and irregular Na surfaces can degrade
376 electrochemical performance and pose serious safety risks during battery operation ⁵². In
377 contrast, the blend_70-30 QSPE exhibits a smoother, denser Na deposition morphology
378 (**Figure 5g**). Schematic representations of the interfacial structures formed on Na metal are
379 shown in **Figure 5h, i**. As ionic transport across the QSPE-electrode interface is governed by
380 the functional groups of the polymer host, the synergistic effects of the fluorine groups from
381 PVDF-HFP and -C-O-C- groups from PEG-PPG-PEG promote enhanced ionic conductivity
382 and enable uniform Na deposition, thereby ensuring a stable and robust interface.



383

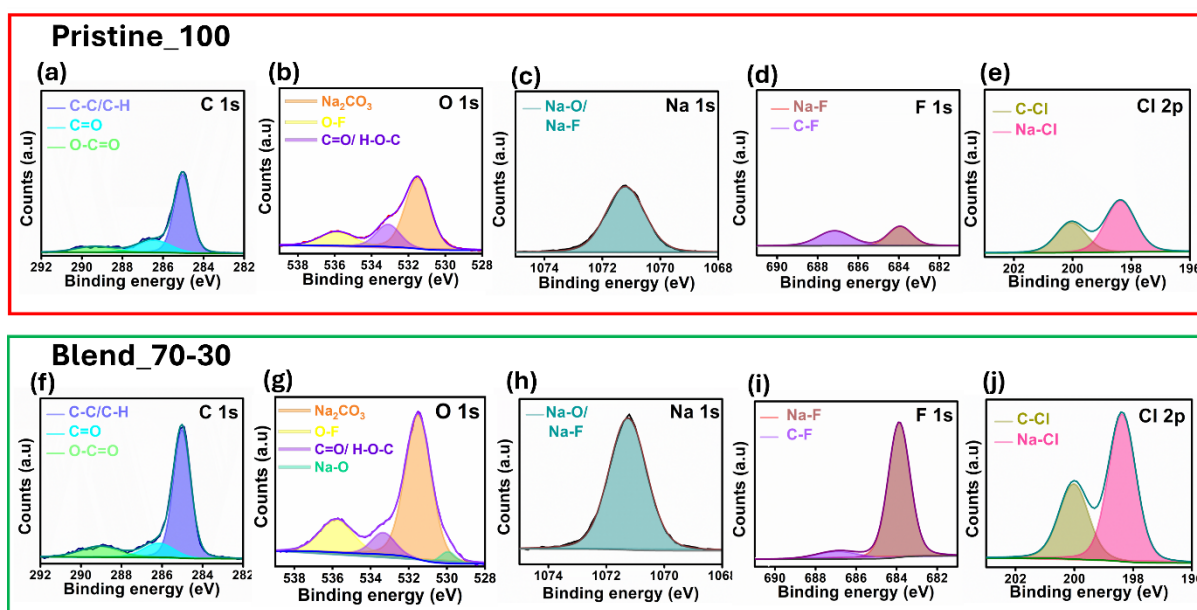
384 **Figure 5.** (a-d) Galvanostatic cycling performance of Na symmetric cells using (a,b)
 385 pristine_100 and (c,d) blend_70-30 QSPes at 1 mA cm⁻² (e) Overlaid Tafel curves of Na
 386 symmetric cells with pristine_100 and blend_70-30 QSPes. (f,g) SEM images of post-cycled
 387 sodium metal electrodes after 10 cycles at 1 mA cm⁻² for cells with (f) pristine_100 and (g)
 388 blend_70-30 QSPes. (h,i) Schematic representations of the Na metal interface before and after
 389 cycling with the respective QSPes.

390 To experimentally validate the implications of the solvation analysis and theoretical results, the
 391 chemical nature of the Na metal anode interface was investigated by X-ray photoelectron
 392 spectroscopy (XPS)^{53,54}. XPS measurements were conducted on the surface of cycled sodium
 393 after 10 cycles at 1 mA cm⁻² in Na//Na symmetric cells employing pristine_100 and blend_70-
 394 30 QSPes to assess the SEI composition. For the pristine_100 QSPe cell, the high-resolution
 395 C1s spectrum reveals typical electrolyte decomposition products, with peaks at 284.8 eV (–C–
 396 C–), 286.2 eV (C=O), and broad bands at 288.0 and 290.0 eV (O–C=O) generated during

397 cycling (**Figure 6a**)^{38,55}. The weak oxyfluoride (-O-F) peak observed in the O 1s spectrum
398 suggests the decomposition of the FEC additive (**Figure 6b**). Deconvolution of the Na 1s, F
399 1s, and Cl 2p peaks further confirms the presence of inorganic components within the SEI
400 (**Figure 6c-e**). In contrast, the blend_70-30 QSPE cell exhibits significantly higher relative
401 intensities for NaF, Na₂CO₃, NaO, and NaCl, indicating the formation of an inorganic-rich SEI
402 (**Figure 6f-j**).

403 It is well established that a stable, inorganic-rich SEI serves as a protective barrier, inhibiting
404 parasitic reactions and suppressing dendritic growth⁵⁶. This is further corroborated by the Cl
405 2p spectra observed for both the pristine_100 and the blend_70-30 QSPEs. The anionic species,
406 perchlorate (ClO₄⁻), preferentially deposits on the Na metal surface, forming a NaCl-rich
407 interphase that protects the electrode and suppresses side reactions. Overall, the formation of
408 an inorganic-rich SEI characterized by high concentrations of NaF, Na₂CO₃, and NaCl
409 correlates with the reduced overpotentials and stable voltage profiles observed during
410 galvanostatic cycling of the blend_70-30 QSPE cell. These XPS results validate the
411 mechanistic insights gained from solvation analysis and theoretical calculations, revealing the
412 origin of the improved electrochemical performance of cells cycled with the blend_70-30
413 QSPE. Moreover, these findings highlight the synergistic effect of fluorinated groups in PVDF-
414 HFP and the electron-donating -C-O-C- groups in PEG-PPG-PEG in enhancing the interfacial
415 stability and overall performance of Na metal anodes.

416



417

418 **Figure 6.** High-resolution XPS spectra of (a,f) C 1s, (b,g) O 1s, (c,h) Na 1s, (d,i) F 1s, and (e,j)
 419 Cl 2p for sodium metal electrodes in the stripped state, using QSPEs based on (a-e)
 420 pristine_100 and (f-j) blend_70-30, respectively.

421 Based on fundamental studies of ionic conductivity, solvation characteristics, transference
 422 number, exchange current density, and overall electrochemical performance, the blend_70-30
 423 QSPE exhibits properties comparable to those of a LE. Accordingly, it is hereafter referred to
 424 as a liquid-like QSPE (L-QSPE). To evaluate the practical applicability of the developed L-
 425 QSPE, a full cell comprising a Prussian blue analogue (PB) cathode and a Na metal anode was
 426 assembled. The detailed PB synthesis procedure, along with its material characterization and
 427 electrode fabrication, is provided in the Supplementary Information (**Figure S11**)^{31,57}.

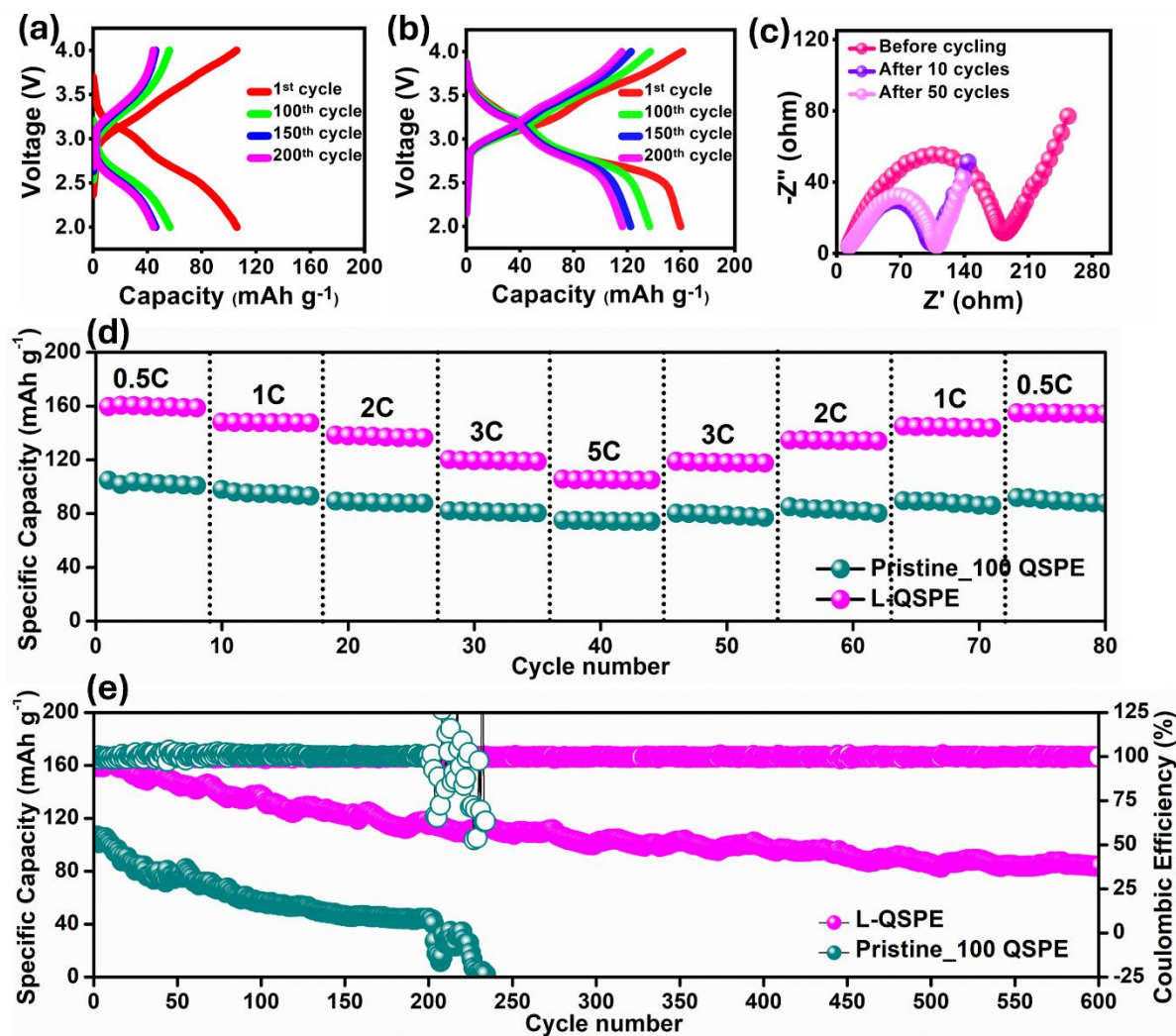
428 The Na//L-QSPE//PB cells deliver an initial capacity of 159 mAh g⁻¹ at 0.5 C (**Figure 7b**). For
 429 comparison, a full cell using the pristine_100 QSPE was also tested (**Figure 7a**). Notably, the
 430 charge-discharge plateaus observed for the PB cathode align well with the cyclic voltammetry
 431 (CV) curves, showing corresponding oxidation and reduction peaks (**Figure S12**). To further
 432 examine the evolution of interfacial resistance during cycling, EIS was conducted on the Na//L-
 433 QSPE//PB cell at various stages (**Figure 7c**). Prior to cycling, the interfacial resistance is
 434 approximately 185 Ω, which decreases to 105 Ω after 10 cycles and further to ~5 Ω after 50
 435 cycles. This progressive decrease in interfacial resistance suggests interfacial activation,

436 consistent with the formation of a stable, inorganic-rich SEI as predicted by theoretical
437 calculation and confirmed by XPS analysis.

438 Rate performance and capacity recovery at various C-rates were also evaluated for both cells
439 (**Figure 7d**). Compared to the pristine_100 QSPE cell, the L-QSPE cell exhibits superior
440 reversible capacity retention. In contrast, the pristine_100 QSPE cell fails to recover its initial
441 capacity and displays a steadily declining profile. Long-term cycling performance at 0.5 C
442 further highlights this difference (**Figure 7e**): the pristine_100 QSPE cell completely fails after
443 200 cycles, whereas the L-QSPE cell sustains stable operation for over 500 cycles, maintaining
444 an average Coulombic efficiency (CE) of ~ 98%.

445 To assess safety, a flame test was performed, with the corresponding optical images presented
446 in **Figure S13**. Compared to commercial LE-soaked Celgard separators, the L-QSPE exhibits
447 delayed fire propagation and self-extinguishing behavior. This improved flame retardancy is
448 attributed to the presence of halogenated compounds, particularly fluorine atoms embedded
449 within the polymer matrix, which suppress combustion. Additionally, the immobilization of
450 LE within the QSPE matrix reduces the concentration of low-flash-point volatile solvents⁵⁸,
451 thereby mitigating flammability risks. This effect is further amplified by the inclusion of the
452 fluorinated FEC additive. A comparison table summarizing the performance of the developed
453 L-QSPE relative to reported systems (**Table S1**) demonstrates its superior electrochemical and
454 safety characteristics. These findings emphasize the effectiveness of optimizing polymer blend
455 compositions, engineering solvation environments, and tailoring SEI formation to achieve
456 high-performance solid polymer batteries.

457



458

459 **Figure 7.** (a,b) Galvanostatic charge-discharge curves of Na//QSPE//PB cells using (a)
 460 pristine_100 QSPE and (b) L-QSPE, cycled at 0.5 C. (c) EIS spectra of the Na//L-QSPE//PB
 461 cell recorded after various cycles at 0.5 C. (d) Reversible rate performance of the cells cycled
 462 from 0.5 C to 5 C and vice-versa. (e) Long-term cycling performance at 0.5 C for cells based
 463 on pristine_100 QSPE and L-QSPE. All tests were performed under ambient conditions.

464 3. Conclusions

465 In summary, a highly ionically conductive and thermomechanically stable QSPE mimicking a
 466 “liquid-like” system has been successfully fabricated for high-performance SMBs. The
 467 optimized L-QSPE exhibits an ionic conductivity of 1.01 mS cm^{-1} and an activation energy of
 468 0.12 eV, comparable to that of liquid electrolytes. Incorporation of the PEG-PPG-PEG
 469 molecule enhances the amorphous nature and promotes the formation of an interconnected
 470 porous network, enabling high electrolyte uptake (240 %) and porosity (72 %). The presence

471 of -C-O-C- groups facilitates a favorable solvation environment, supporting the formation of
472 AGGs. Coupled with excellent mechanical properties, the L-QSPE delivers a stable Na
473 plating/stripping profile for over 200 h with a low overpotential (250 mV), and a high exchange
474 current density of $0.0165 \text{ mA cm}^{-2}$, indicating improved Na nucleation and growth kinetics. A
475 high Na^+ transference number of 0.78 and the elevated AGG content correlate with an
476 expanded ESW, attributed to reduced local polarity via the solvation effect. DFT calculations
477 reveal that fluorinated groups in PVDF-HFP lower the LUMO energy level, which enhances
478 reduction propensity at the Na metal surface. The resulting fluoride-based SEI products
479 passivate further reactions, stabilizing the interface and mitigating degradation. MD
480 simulations further highlight the role of electron-withdrawing groups in engineering solvation
481 structures and enhancing ionic transport of L-QSPE, predicting an ionic conductivity of 2.10
482 mS cm^{-1} and a transference number of 0.90 consistent with experimental observations. Finally,
483 a Na/L-QSPE/PB full cell demonstrates excellent cycling stability, maintaining an average
484 CE of 98% over 500 cycles at 0.5 C. These results underscore the potential of L-QSPE to drive
485 the development of next-generation QSPE-based high-performance SMB systems.

486 **4. Acknowledgement**

487 We would like to thank IIT-Delhi, India, and UQ, Australia, for the collaborative program,
488 UQIDAR, for the support throughout this work. The authors acknowledge the central research
489 facility (CRF), IIT-Delhi, India, for the usage of various analytical facilities. The authors thank
490 IIT Delhi HPC facility for computational resources. A.B. acknowledges seed grant from IIT
491 Delhi (SGNF148). This work was partially supported by the UQ-Yonsei International Research
492 Program, the JST-ERATO Yamauchi Materials Space Tectonics Project (JPMJER2003), and
493 the ARC Laureate Fellowship (FL230100095). M. H thanks the support from JSPS
494 Postdoctoral Fellowships for Research in Japan. This work used the Queensland node of the
495 NCRIS-enabled Australian National Fabrication Facility (ANFF).

496 During the preparation of this work, the authors used ChatGPT to check English grammar.
497 After using this tool, the authors reviewed and edited the content as needed and take full
498 responsibility for the content of the publication.

499

500 **5. Declaration of interest**

501 The authors declare no conflict of interest.

502 **6. Reference**

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The data supporting this article have been included as part of the ESI.