Planar Defect-Driven Electrocatalysis of CO2-to-C2H4 Conversion

<table>
<thead>
<tr>
<th>Journal:</th>
<th>Journal of Materials Chemistry A</th>
</tr>
</thead>
<tbody>
<tr>
<td>Manuscript ID</td>
<td>TA-ART-03-2021-002565.R1</td>
</tr>
<tr>
<td>Article Type:</td>
<td>Paper</td>
</tr>
<tr>
<td>Date Submitted by the Author:</td>
<td>05-Jun-2021</td>
</tr>
</tbody>
</table>
| Complete List of Authors: | Li, Zhengyuan; University of Cincinnati, Chemical and Environmental Engineering  
Fang, Yanbo; University of Cincinnati, Mechanical and Materials Engineering  
Zhang, Jianfang; Hefei University of Technology, School of Materials Science and Engineering  
Zhang, Tianyu; University of Cincinnati  
Jimenez, Juan; Brookhaven National Laboratory, Chemistry Division  
Senanayake, Sanjaya; Brookhaven National Laboratory, Chemistry  
Shanov, Vesselin; University of Cincinnati,  
Yang, Shi-ze; Arizona State University  
Wu, Jingjie; University of Cincinnati, Chemical Engineering |

SCHOLARONE™ Manuscripts
1. Introduction

The CO$_2$ electro-reduction reaction (CO$_2$RR) to value-added multi-carbon (C$_n$) products is a promising avenue to artificial carbon recycling using renewable energy sources. In particular, conversion of CO$_2$ to ethylene (C$_2$H$_4$), a major industrial feedstock with a large market size and relatively high market price, has received immense heed. The techno-economic analyses (TEAs) reveal that when (1) electricity costs fall below 4 cents/kWh; (2) C$_2$H$_4$ partial current density meets 450 mA cm$^{-2}$; and (3) energy efficiency is at least 60%, the C$_2$H$_4$ generated from CO$_2$RR becomes competitive with current market prices for that derived from fossil sources. So far, copper (Cu) and Cu-derived materials are the most efficient electrocatalysts that can convert CO$_2$ to C$_2$ products with appreciable reaction rates. However, the unsatisfactory selectivity of CO$_2$ reduction towards a specific high-order product still impedes its large-scale implementation.

It has been demonstrated that the coupling of the key intermediate (e.g., surface adsorbed *CO) is a critical step in CO$_2$-to-C$_2$$_2$ products conversion. Therefore, numerous strategies have been developed to maximize the utilization of *CO. The cascade catalysis involving tandem catalysts has been proposed to supply extra CO and thus to raise local CO concentration near Cu surface for facilitating C-C coupling. Another widely investigated approach is to properly increase concentration near Cu surface for facilitating C-C coupling.

The selectivity towards a specific C$_n$ product, such as ethylene (C$_2$H$_4$), is sensitive to the surface structure of copper (Cu) catalysts in the carbon dioxide (CO$_2$) electro-reduction. The fundamental understanding of such sensitivity can guide the development of advanced electrocatalysts, although it remains challenging at the atomic level. Here we demonstrated that the planar defects, such as stacking faults, could drive electrocatalysis of CO$_2$-to-C$_2$H$_4$ conversion with higher selectivity and productivity than Cu(100) facets at the intermediate potential region (-0.50 ~ -0.65 V vs. RHE). The unique right bipyramidal Cu nanocrystals containing a combination of (100) facets and a set of parallel planar defects delivered 67% Faradic efficiency (FE) of C$_2$H$_4$ and partial current density of 217 mA cm$^{-2}$ at -0.63 V vs. RHE. In contrast, Cu nanocubes with exclusive (100) facets exhibited only 46% FE of C$_2$H$_4$ and a partial current density of 87 mA cm$^{-2}$ at the identical potential. Both ex situ CO temperature-programmed desorption and in situ Raman spectroscopy analysis implied that the stronger *CO adsorption on planar defect sites fosters CO generation kinetics, which contributes to a higher surface coverage of *CO and in turn an enhanced reaction rate of C-C coupling towards C$_2$H$_4$ products, especially C$_2$H$_4$.
nanocubes (Cube-Cu) with exclusive Cu(100) facets exhibited only 46% FE of C\textsubscript{2}H\textsubscript{4} and partial current density of 87 mA cm\textsuperscript{-2} at the identical potential. The planar defect was discovered to show activity and selectivity towards C\textsubscript{2}H\textsubscript{4} formation superior to Cu(100) by comparing the performance between Rbp-Cu and Cube-Cu. The reaction mechanism study using CO temperature-programmed desorption and in situ Raman spectroscopy implied that the enhancement of reactivity for CO\textsubscript{2}-to-C\textsubscript{2}H\textsubscript{4} conversion originates from the stronger *CO adsorption energy on planar defects than Cu(100).

2. Experimental

2.1 Chemicals and materials

Copper(II) chloride dehydrate (CuCl\textsubscript{2}·2H\textsubscript{2}O, 99.0%), D-glucose (C\textsubscript{6}H\textsubscript{12}O\textsubscript{6}, 99.5%), hexadecylamine (HDA, 98%), sodium tetrachloropalladate(II) (Na\textsubscript{2}PdCl\textsubscript{4}, 98%), lead(II) perchlorate hydrate (Pb(ClO\textsubscript{4})\textsubscript{2}·xH\textsubscript{2}O, 99.995%), perchloric acid (HClO\textsubscript{4}, 70%), α-alumina (α-Al\textsubscript{2}O\textsubscript{3}, 99.9%) and potassium hydroxide (KOH, 99.99%) were obtained from Sigma-Aldrich and used as received.

2.2 Synthesis of Cu nanocrystals

The synthetic methods are adapted from the previous reports.\textsuperscript{26,29} In a standard synthesis of Rbp-Cu nanocrystals (NCs), 21 mg CuCl\textsubscript{2}·2H\textsubscript{2}O, 180 mg HDA, 50 mg glucose, 0.2 mg Na\textsubscript{2}PdCl\textsubscript{4} and 10 ml water were mixed and magnetically stirred in a 20-ml vial at room temperature overnight. Then Ar was slowly bubbled through the solution for 15 min. After that, the vial was tightly capped and heated at 100 °C for 6 h under magnetic stirring. The as-prepared Rbp-Cu NCs were centrifuged and washed with hexane and ethanol several times. Cube-Cu NCs were prepared following the same procedure, except that the amounts of Na\textsubscript{2}PdCl\textsubscript{4} and surfactant (HDA) were adjusted to 0 mg and 90 mg, respectively.

2.3 Characterization

The morphology of the as-prepared Cu NCs was imaged by a scanning electron microscopy (SEM, FEI Apreo LV-SEM) and a transmission electron microscope (TEM, FEI Titan ETEM). The crystalline structure was identified by X-ray diffraction (XRD, Rigaku D/MAX2500VL). The total CO generation and dimerization rates were calculated based on the measurements of three independent electrodes.

2.4 Electrochemical measurements

2.4.1 Lead underpotential deposition. The underpotential deposition of lead (Pb-UPD) was conducted in a three-electrode glass cell at ambient temperature. The Cu NCs loaded on glassy carbon electrode, Pt mesh, and Ag/AgCl (3 M KCl) were employed as working, counter, and reference electrodes, respectively. A N\textsubscript{2}-saturated 0.1 M HClO\textsubscript{4} aqueous solution with 10 mM Pb(ClO\textsubscript{4})\textsubscript{2}·xH\textsubscript{2}O was used as the electrolyte. Cyclic voltammetry (CV) with a sweep rate of 10 mV s\textsuperscript{-1} was applied for measurements.

2.4.2 Electrocatalytic measurement of CO\textsubscript{2} reduction. A customized flow cell with 1 M KOH was employed for CO\textsubscript{2}RR at ambient conditions. FAA-3-PK-75 anion exchange membrane (Fuel Cell Store) was used to separate anodic and cathodic compartments. The cathode was prepared by a spray-coating method. The as-prepared Cu NCs (4 mg) were dispersed in isopropanol (3 ml) and 6 μl Nafion solution (5 wt.%). The mixture was sonicated for 30 minutes and airbrushed onto a carbon diffusion layer (GDL, Sigracet 35BC, Fuel Cell Store). The prepared cathode gas diffusion electrode (GDE) was dried at 130 °C under vacuum for 1 h. The catalyst loadings for all samples were kept at around 0.30 mg cm\textsuperscript{-2}. Ni foam was served as the anode. The electrolyte was fed by syringe pumps (New Era Pump Systems Inc.) at 1 ml min\textsuperscript{-1} and 2 ml min\textsuperscript{-1} to the anodic and cathodic compartments, respectively. CO\textsubscript{2} gas flowed through cathode at 50 sccm via a mass flow controller (Alicat Scientific). A potentiostat (Gamry Interface 1010E) supplied a constant voltage to the flow cell and recorded the corresponding current. The cathode potential was measured relative to the Ag/AgCl (3 M KCl) reference electrode. All potentials were converted to the RHE scale using: \( E_{\text{RHE}} = E_{\text{AgAgCl}} + 0.209 V + 0.0591 \times pH \). An iR compensation was determined by potentiostatic electrochemical impedance spectroscopy (EIS).

For each applied potential, an on-line gas chromatograph (GC, SRI Instruments MultipleGas85) equipped with both the thermal conductivity detector and flame ionization detector was used to monitor the gas products. To calibrate the outlet gas flow rate of CO\textsubscript{2}, Ar, as an internal standard, was fed at 10 sccm and mixed the outlet gas stream from the flow cell before looping to the GC.\textsuperscript{11} The FE of gas products were calculated using the following equation (Eq. (1)):

\[
\text{FE}(\%) = \frac{\text{F_{j\text{total}}}}{\text{F_{j\text{total}}}} \times 100 \%
\]

where \( z \) is the number of electrons transferred for producing a target product; \( F \) is the Faraday constant; \( x \) is molar fraction of a target product determined by GC; \( V \) is the molar flow rate of gas; \( F_{j\text{total}} \) is the total current density.

Meanwhile, the catholyte was collected after electrolysis followed by quantifying the liquid products via \(^1\text{H} \) NMR (Bruker AV 400 MHz spectrometer). 500 μl of the catholyte was mixed with 100 μl internal standard of 5 mM 3-(Trimethylsilyl) propionic-2,2,3,3-d\textsubscript{4} acid sodium salt in D\textsubscript{2}O. The standard deviations were calculated based on the measurements of three independent electrodes.

The total CO generation and dimerization rates were calculated according to the following two equations (Eqs. (2) and (3)):

\[
\text{CO generation rate} = j_{\text{CO}} = \frac{f_{\text{CO}}}{\text{V}_{\text{R}} \times t} + f_{\text{CO,pr}} \times \frac{I_{\text{FAC,pr}}}{V_{\text{FAC,pr}}} + f_{\text{CO,dc}} \times \frac{I_{\text{FAC,dc}}}{V_{\text{FAC,dc}}} + f_{\text{CO,an}} \times \frac{I_{\text{FAC,an}}}{V_{\text{FAC,an}}} \tag{2}
\]

\[
\text{CO dimerization rate} = j_{\text{CO}} = \frac{f_{\text{CO}}}{\text{V}_{\text{R}} \times t} + f_{\text{CO,pr}} \times \frac{I_{\text{FAC,pr}}}{V_{\text{FAC,pr}}} + f_{\text{CO,dc}} \times \frac{I_{\text{FAC,dc}}}{V_{\text{FAC,dc}}} + f_{\text{CO,an}} \times \frac{I_{\text{FAC,an}}}{V_{\text{FAC,an}}}
\]

2.5 In situ electrochemical Raman spectroscopy measurements

In situ Raman spectroscopy measurements were carried out on a modified flow cell with a quartz window in front of the cathode GDE. Graphite and Ag/AgCl (3 M KCl) were used as counter and reference electrodes, respectively. The cathode and anode were separated by an anion exchange membrane (FAA-3-PK-75). The syringe pumps were used to pump 1 M KOH at 2 ml min\textsuperscript{-1} to both cathode and anode. CO\textsubscript{2} gas was introduced via machined flow channels to the back of the GDE at a flow rate of 50 sccm. The Raman spectra were collected...
3. Results and discussion

The Rbp-Cu NCs, which contain Cu(100) facets and abundant planar defects exposed simultaneously, were synthesized by a one-step reduction process using HDA as the capping agent. In comparison, the Cube-Cu NCs with exclusive Cu(100) facet surfaces were prepared following the same procedure except for regulating the amount of reagents. As shown in SEM images (Fig. 1a), the Rbp-Cu NCs possess a particle size of 60–80 nm with several typical projected profiles, such as triangle, rhombus, and tetragon. Additional high-magnification SEM images and schematic models of individual Rbp-Cu in different orientations are shown in the ESI (Fig. S11). TEM images unveiled the existence of parallel planar defects (e.g., stacking faults) on the Rbp-Cu surface (Fig. 1b, c and S2, ESI†). Alternating light/dark contrasts in the inset of Fig. 1b are typically a set of stacking faults. Analogous to right biyramid structures of Ag and Pd, each Rbp-Cu NC is bounded by six triangular (100) side facets (yellow in the Rbp model in the inset of Fig. 1a), and is mirror-symmetrically divided by a set of planar defects (green in the Rbp model in the inset of Fig. 1a). Benefited from the regular morphologies of Rbp-Cu, the proportion of planar defects is calculated to be 20.1% based on the geometric dimensions for a typical Rbp-Cu NC (Fig. S2e). As expected, the as-prepared Cube-Cu with a particle size of 80–120 nm, as a control sample, exhibits a regular cubic shape with (100) facets (Fig. S31).

We used Pb underpotential deposition (UPD), a surface-sensitive electrochemical technique, to further probe the surface structures of Cu NCs. Different Cu facets exhibit distinguished Pb-UPD peaks in the CV curves. As displayed in Fig. 1d, the peaks located at ca. -0.10 V and -0.08 V can be assigned to the Cu(100) and Cu(111), respectively. The peaks of Pb electrodeposition on Cu(100) are more prominent for both Rbp-Cu and Cube-Cu samples than those on Cu(111). An additional peak centered at less cathodic potential (ca. -0.06 V) is only observed for Rbp-Cu, which is ascribed to the Pb-UPD on the low-coordinated sites from surface defects. Such a kind of phenomenon that Pb over-layer on the face-centered cubic metal preferentially nucleates at the edges or steps and then expands to the terraces has been demonstrated by in situ scanning probe microscopy studies. OH electro-adsorption was also performed to verify the predominant (100) facets for both Cu NCs (Fig. S41). An additional shoulder peak at ca. 0.34 V was observed for Rbp-Cu, which is associated with surface defects. The percent of high-index surface defects on Rbp-Cu is estimated to be 17.3% according to the integral peak areas, which is close to the value obtained from TEM aforementioned. In agreement with TEM, Pb-UPD and OH electro-adsorption results confirm the presence of defect sites on Rbp-Cu, although the exact facet index is hard to identify. XRD patterns show that both types of Cu NCs exhibit a much more pronounced (100) peak and a weaker (111) peak (Fig. 1e), which is consistent with electrochemical characterization results and confirms the uniform shape of the NCs. Moreover, other than Cu peaks, no other peaks associated with copper oxide or other impurities were observed. XPS analysis reveals that Rbp-Cu and Cube-Cu both present two main peaks at 932.8 eV and 952.6 eV in Cu 2p spectrum (Fig. 1f), corresponding to Cu2 or Cu+ species. Auger Cu LMM spectrum (Fig. S51) show that both Rbp-Cu and Cube-Cu mainly consist of Cu2 (918.6 eV) at the surface, with a minimal amount of Cu+ (916.6 eV). The formation of Cu+ is caused by the rapid oxidation of Cu2 in air and would be quickly in situ reduced to metallic Cu under CO2 electrolysis. Due to the introduction of a trace amount of Pd (<0.55 at.%) as the seeds during the synthesis of Rbp-Cu, Pd 3d XPS was carried out. There is no Pd element on the Rbp-Cu surface (Fig. S61), suggesting the absence of Pd dopants or Pd-Cu bimetallic structures.

The CO2RR performance on Rbp-Cu and Cube-Cu based GDEs was measured in a customized Flow cell using 1 M KOH as the catholyte (Fig. S71 and S81). The Rbp-Cu exhibited a higher selectivity towards CH4 than Cube-Cu. The maximum FE of CH4 for Rbp-Cu achieved 67% at -0.63 V (vs. RHE, thereafter), at which the partial current density (Ipc(H2)) reached 217.1 mA cm-2 (Fig. 2a and b). The overall performance of Rbp-Cu for CO2-to-CH4 conversion is superior to most copper-based catalysts tested under identical conditions (Table S11). Combined with C2+ liquid products analyzed by 1H NMR, including ethanol (C2HOH), acetone (CH3CO), and n-propene (C3H6OH), the FE and partial current density of C2+ products (Ipc(C2+)) on Rbp-Cu reached 89% and 289 mA cm-2, respectively, at -0.63 V (Fig. 2c and d). On the contrary, the Cube-Cu showed only 46% FE of CH4 and 68% FE for C2+ products at the same overpotential. Moreover, the FE ratio of CH4 over C2H2OH was enhanced from 3.10 for Cube-Cu to 3.77 for Rbp-Cu at -0.63 V (Fig. S91). Compared to Rbp-Cu, the Cube-Cu manifested lower Ipc(H2) and Ipc(C2+) over the applied potential range (Fig. 2b and d). Interestingly, we found that the Rbp-Cu showed relatively much lower FE of CO than Cube-Cu (Fig. S101), indicating the more efficient conversion of CO to hydrocarbons and oxygenates on the Rbp-Cu. The improvement of activity and selectivity towards CH4 and C2+ products suggests that the planar defect sites on Rbp-Cu may be responsible for the enhanced C2/C coupling rate.

To exclude the possible effect of surface roughness, the electrochemical surface area (ECAS) was determined by using the double-layer capacitance (Cdl) method (Fig. S111). The ECAS normalized current density of each product followed the same trend as the geometric current density for both Rbp-Cu and Cube-Cu (Fig. S121). Under the optimal potential condition of -0.63 V for CH4 and C2+ products formation, the normalized Ipc(H2) and Ipc(C2+) for Rbp-Cu
were 1.9-fold and 1.7-fold higher than those for Cube-Cu, respectively, indicating the excellent intrinsic activity of Rbp-Cu towards CH₄ and C₂, products. Considering a lower surface-to-volume ratio of Cube-Cu related to Rbp-Cu, the loading of Cube-Cu was increased from 0.30 to 0.42 mg cm⁻², which increased the double layer capacitance (equivalent to ECSA) to 0.57 mF cm⁻² accordingly, similar to that of Rbp-Cu (0.56 mF cm⁻²) with a loading of 0.30 mg cm⁻² (Fig. S13f). Although the current density increased with catalyst loading, a similar product distribution was obtained for Cube-Cu with two different loadings. Especially, the FE of CH₄ were almost identical at the investigated overpotential range (Fig. S13e-f). Therefore, we infer that higher ECSA is not the main factor for promoting selectivity towards CH₄.

![Comparison of CO₂RR performance for Rbp-Cu and Cube-Cu](image)

**Fig. 2** Comparison of CO₂RR performance for the Rbp-Cu and Cube-Cu. (a-d) The potential-dependent (a) FE of CH₄, (b) Jₑ, (c) FE of C₂, products, and (d) Jₑ... The error bars represent standard deviation based on the measurements of three independent electrodes. (e) The stability of the Rbp-Cu operated at -0.63 V vs. RHE.

Notably, the Rbp-Cu exhibited activity towards CH₄ and C₂-products similar to Cube-Cu at potentials between -0.35 and -0.50 V (Fig. 2 and S12†), likely owing to the Cu(100) facet on both Cu NCSs that facilitates the *COCO* dimerization at such a low overpotential region.⁷ At the potential region of -0.50 ~ -0.65 V, the planar defects sites on the Rbp-Cu surface play a more critical role in CO₂-to-C₂-products conversion. The possible dimerization pathways at this overpotential range may involve the coupling between *CO* and reduced *CO* species (i.e., *CHO* and/or *COH*),⁸⁻¹² the reaction barrier of which could be decreased on low-coordinated defects.⁷,¹² However, the selectivity towards C₂H₄ for Rbp-Cu decreased dramatically at higher cathodic potentials (-0.65 ~ -0.70 V). Simultaneously, the activity and selectivity towards hydrogen (H₂) and methane (CH₄) rose accordingly (Fig. S10f and S12f). The upsurge of reactivity towards H₂ arises from the stronger competitive hydrogen evolution reaction (HER) occurring on low-coordinated sites at the high cathodic potential region.⁵,¹³ To verify this, the HER was performed under Ar atmosphere in the flow cell. Linear sweep voltammetry (LSV) showed higher electrocatalytic activity of HER for Rbp-Cu than Cube-Cu as the potential swept beyond -0.50 V (Fig. S14f), demonstrating that planar defects are more active for HER as well as CO₂RR at the high cathodic potential region. At higher overpotentials, increased adsorption of hydrogen would suppress CO₂-to-C₂ products conversion.⁴⁴

To demonstrate a stable CO₂-to-C₂ products conversion, the durability test for Rbp-Cu was operated at -0.63 V, where the optimal selectivity towards C₂H₂ and C₂ products was achieved. By using polytetrafluoroethylene-treated GDL to improve the hydrophobicity, relatively stable FE of (61 ± 5)% for C₂H₂ was recorded while FE of C₂ products was maintained at (82 ± 4)% with a total current density of (330 ± 30) mA cm⁻² during a 50-hour continuous test (Fig. 2e). As examined by TEM, the post-electrolysis Rbp-Cu retained the planar defects (Fig. S15f) although the corners or edges of well-defined morphology were degraded to some extent.⁵,⁴⁰ Surface adsorbed *CO*, the key intermediate for CO₂ reduction to hydrocarbons and oxygenates, may stabilize Cu defects in line with prior density function theory (DFT) calculations.²²

Given that the same Cu(100) facets exposed for both Rbp-Cu and Cube-Cu samples, we envisioned that the superior CO₂-to-C₂ conversion is attributed to the introduction of the planar defects on Rbp-Cu surface. These planar defects with low coordination number enable stronger *CO* adsorption that assists in building a sufficiently high surface coverage of *CO* to direct the C-C coupling.⁶,²³ To prove this hypothesis, *ex situ* CO₂-TPD experiment and *in situ* electrochemical Raman spectroscopy measurement were conducted.

![CO₂-TPD profiles of the Rbp-Cu and Cube-Cu](image)

**Fig. 3** (a) CO₂-TPD profiles of the Rbp-Cu and Cube-Cu. The desorption compound is monitored with a m/z ratio of 28 for CO. Inset is the zoom-in region from 50 to 150 °C. (b) Schematic of *in situ* Raman spectroscopy flow cell. (c-f) *In situ* Raman spectroscopy of (c) Rbp-Cu and (d) Cube-Cu during CO₂RR under different applied potentials. All given potentials are referred to RHE. (e-f) Comparison of *in situ* Raman spectra for Rbp-Cu and Cube-Cu at (e) low-frequency range and (f) high-frequency range under -0.63 V vs. RHE.
The monitored CO-TPD traces, which can give the amount and strength of \*CO adsorption, are shown in Fig. 3a and S16T. For both types of Cu NCs, the onset CO desorption began at approximately 60 °C. The observation of a later CO desorption peak at 90 °C for Rbp-Cu indicates a stronger adsorption affinity for CO and CO-related intermediates, resulting from the presence of planar defects.36,47 Additionally, the larger CO desorption peak area for Rbp-Cu implies a larger surface coverage of \*CO on Rbp-Cu than Cube-Cu.48 These CO-TPD results preliminarily support that both adsorption energy and surface coverage of \*CO are boosted on Rbp-Cu, benefiting from planar defect sites.

To evaluate the \*CO adsorption behaviors under the CO2 electrocatalysis conditions, in situ Raman spectroscopy measurements were further carried out in a modified flow cell with a quartz window in front of the cathode GDH (Fig. 3b). The Raman spectra were recorded at a range of applied potentials from the open circuit potential (OCP) to -0.70 V for both types of Cu NCs (Fig. 3c and d). For the Rbp-Cu, the low-frequency bands of the \*CO at ca. 282 and 371 cm^-1 are characteristic for the Cu-CO frustrated rotation and Cu-CO stretch, respectively (Fig. 3c).49 The high-frequency bands are associated with \( \text{C} = \text{O} \) stretching vibrations with different adsorption configurations, including bridge-bound CO (COO bridge, 1850-1880 cm^-1) and atop-bound CO (COO atop, 2000-2090 cm^-1).46,50 Notably, the asymmetric broad band for the COO atop is likely due to the \*CO adsorption on various Cu surface sites, which, in turn, may affect the activity and selectivity of CO2RR.49,51 The difference in \*CO adsorption behaviors between Rbp-Cu and Cube-Cu was assessed by comparing the in situ Raman spectra collected at the same applied potential of -0.63 V. First, a blue shift of COO atop sharp band suggests the stronger binding of \*CO at low-coordinated defect sites for the Rbp-Cu (2084 cm^-1) relative to Cube-Cu (2067 cm^-1) (Fig. 3f).49 Meanwhile, the band for the Cu-CO stretch also exhibited a blue shift on the Rbp-Cu (371 cm^-1) compared to that on the Cube-Cu (365 cm^-1) (Fig. 3e), confirming a stronger binding of \*CO to the Rbp-Cu surface.52 Second, the integrated areas of bands (e.g., Cu-CO and COO atop bands), which are proportional to the \*CO surface coverage,49 increase for Rbp-Cu compared with Cube-Cu (Fig. 3e and f). Taken together, ex situ CO-TPD and the in situ Raman spectroscopy results unravel that the Rbp-Cu promotes the adsorption and surface coverage of \*CO, which could enhance the subsequent C-C coupling kinetics and thus the production of C2 products.

To further explore the impact of the enhancement of \*CO adsorption energy on the C-C coupling kinetics, we analyzed and compared the CO generation and dimerization rates (Fig. 4 and S17f).21 The CO generation rate was referred to as the summary of the normalized production rates of CO, \( \text{CH}_4 \), and \( \text{C}_2 \) products (Eq. (2) in the Experimental section). According to the scaling relations of adsorption energy between intermediates and BEP relations between intermediate adsorption energy and activation barrier,21 the enhancement of \*CO binding indicates stronger \*COOH binding and lower activation barrier in the elementary step of \( \text{CO}_2 \text{to-} \text{COOH} \) conversion, which leads to an accelerated CO generation rate. Fig. 4a shows that the Rbp-Cu indeed provided more CO than Cube-Cu, manifesting planar defects facilitate the CO generation rate compared to terraces such as (100) facets in our case. Meanwhile, the CO dimerization rate was derived based on normalized production rates of \( \text{C}_2 \) products (Eq. (3) in the Experimental section). Again, the Rbp-Cu exhibited a much faster CO dimerization rate than Cube-Cu due partly to the increased surface coverage of \*CO (Fig. 4b). For example, the CO dimerization rate of Rbp-Cu achieved > 2.2-times as high as that of Cube-Cu at around -0.65 V. It is also reasonable to propose that C-C coupling intermediates, such as \*COCO, \*COCHO, or \*COOH, can be efficiently stabilized on defect sites, which further facilitates dimerization reaction.40,41 In short, compared to (100) facets, the stronger \*CO adsorption on planar defect sites fosters CO generation kinetics at the intermediate overpotential region, which contributes to a higher surface coverage of \*CO and in turn an enhanced reaction rate of C-C coupling towards \( \text{C}_2 \) products, especially \( \text{C}_2\text{H}_4 \).

4. Conclusions

In summary, compared to a regular Cube-Cu NC with exclusive (100) facets, the Rbp-Cu, containing a combination of planar defects (e.g., stacking faults) and (100) facets, exhibits a higher selectivity to \( \text{C}_2\text{H}_4 \) (FE = 67%), and \( \text{C}_2 \) products (FE = 89%) with the corresponding \( \text{FE} \) of 217 mA cm^-2 at -0.63 V. Using CO-TPD and in situ Raman spectroscopy, the introduction of the planar defects on Rbp-Cu surface are found to contribute to the increasing of \*CO adsorption energy and \*CO surface coverage. Based on CO generation and dimerization rates analysis, a stronger \*CO binding facilitates the \*CO surface coverage and promotes the C-C coupling kinetics. Additionally, the durability test illustrates that defects are stabilized by \*CO under CO2RR conditions. Further DFT investigations are expected to explore the relationship between specific active sites and favorable reaction pathways to either \( \text{C}_2\text{H}_4 \) or \( \text{C}_2\text{H}_2\text{OH} \) at the atomic level. Nevertheless, this work provides an in-depth insight into the reactivity comparison between planar defects and Cu(100) facets, which guides in designing advanced catalysts for efficient CO2-to-C2H4 conversion.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

This work was financially supported by NSF CBET-2033343. S.Y. acknowledges the use of facilities within the Eyring Materials Center at Arizona State University supported in part by NNCI-ECCS-1542160. J.J. and S.S. acknowledge that the research carried out at Brookhaven National Laboratory (BNL) was supported by the division of Chemical Science, Geoscience, and Bioscience, Office of Basic Energy Science of the US Department of Energy (DOE), under contract no. DE-SC0012704.

Notes and references