



Arsenite Oxyanions Affect CeO₂ Nanoparticle Dissolution and Colloidal Stability

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Environmental significance

Due to growing industrial applications, cerium oxide nanoparticles (CeO₂ NPs) are an emerging environmental contaminant of increasing concern. In this study, we elucidated the effects of aqueous arsenite, a potential co-present contaminant, on CeO₂ NP aggregation, settling, and redox reactivity. We found that at lower arsenite concentrations, NPs remained suspended in solution while adsorbing high percentages of arsenite, allowing NPs to transport arsenite over long distances. At high arsenite concentrations, CeO₂ NPs aggregated and settled from solution. Furthermore, the effect of arsenite concentration on NP dissolution encompasses interplay between redox interactions and NP aggregation, complicating risk assessment. These findings have important implications for predicting the behavior of engineered nanomaterials in water and wastewater treatment plants and in industrial waste streams.

Arsenite Oxyanions Affect CeO₂ Nanoparticle Dissolution and Colloidal Stability[†]

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Abstract

While highly reactive cerium oxide nanoparticles (CeO₂ NPs) are widely used in industry, their transport in aquatic systems is not well understood. To fill this knowledge gap, the interactions of CeO₂ NPs with arsenite (As³⁺), a toxic metalloid and potential co-present contaminant, were investigated with respect to CeO₂ NP colloidal stability, dissolution, and surface redox reactions. Arsenite showed distictive effects at different concentrations, with a high As³⁺ concentration (10⁻ ⁴ M) inducing 90% of CeO₂ NPs to settle from solution after 8 hours, while lower As³⁺ concentrations (10⁻⁵ or 10⁻⁶ M) led to only 20% of CeO₂ NPs settling. The dissolution of NPs was most significant in the 10⁻⁵ M As³⁺ system owing to a lesser extent of aggregation, exposing more CeO_2 surface for dissolution. In the three As³⁺ concentration systems, >97% of aqueous arsenic remained as As³⁺ over 6 hours. On the NP surface, adsorbed As^{III} was oxidized to As^V, resulting in 58%–70% of the adsorbed arsenic remaining as As^{III}. Simultaneously Ce^{IV} was reduced to Ce^{III}, increasing Ce^{III} on the CeO₂ NP surface from 17% (without arsenite) to 21–25% (with arsenite). Further mechanistic analyses revealed that the adsorption of arsenite was the main contributor to neutralizing the CeO₂ NP surface potential, enhancing particle sedimentation. These findings suggest that the fate and transport of CeO₂ NPs in our experimental systems are strongly affected by arsenite concentration and its adsorption on NPs. The results also highlight the importance of the interplay between NP aggregation, oxidation, and dissolution in predicting the behaviors of CeO₂ NPs and associated toxic elements in aquatic systems.

Cerium oxide nanoparticles (CeO₂ NPs) are widely used as fuel additives and catalysts, as well as in pharmaceutical and cosmetic applications and in semiconductor production.^{1, 2} The annual production of CeO₂ NPs in the U.S. is estimated to be 35–700 tons per year,³ and global CeO₂ NP production is predicted to increase from approximately 10,000 tons/year in 2014 to 58,000 tons/year by 2020.⁴ Increasingly widespread applications of engineered CeO₂ NPs will result in their increasing presence in natural and engineered aquatic systems, posing a challenge to water and wastewater treatment as well as to risk management.⁵ Thus, a better understanding of CeO₂ NP behavior is needed, particularly in aqueous systems where interactions with other compounds can significantly alter their fate and transport.

The highly catalytic activity of CeO₂ NPs is attributed to oxygen defects in their structure, which allow for oxygen storage and reversible transformation between Ce^{IV} and Ce^{III,6,7} Because there can be multiple oxidation states of cerium in our experimental system—both in solution and in the solid phase—the oxidation states will be denoted by Roman numerals for solid phases (e.g., Ce^{IV} and Ce^{III}) and Arabic numerals for aqueous phases (e.g., Ce⁴⁺ and Ce³⁺) throughout the manuscript. Regarding these different oxidation state moieties, Ce^{IV} is less soluble than Ce^{III} (K_{sp} = 5.0 × 10⁻⁶⁰ for Ce^{IV}O₂, ⁸ and K_{sp} = 1.6 × 10⁻²⁰ for Ce^{III}(OH)₃ ⁹⁻¹¹). The redox reversibility evidenced by the multiple oxidation states co-present in CeO₂ NPs has been linked to cytotoxicity in organisms.¹ For example, the oxidative stress caused by the reduction of Ce^{IV} to Ce^{III} and the dissolution of Ce³⁺ can induce chronic toxicity to *E. coli* and adverse cell responses in human lung epithelial cells (BEAS-2B).^{12, 13} In addition, CeO₂-containing suspensions used for chemical mechanical planarization have been shown to inhibit the proliferation and viability of human cells.²

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To predict environmental risks to ecosystems and human health, it is important to improve our understanding of CeO_2 NPs' behavior and their transformation in aquatic systems.

Because CeO₂ NPs are emerging environmental contaminants, there is little data regarding CeO_2 in the environment or in water treatment facilities. One field-based measurement found that sewage sludge ash in Japan has a mean Ce element concentration of 35.4 ppm.¹⁴ It was also estimated in 2010 that 0.4–7% of the annual global production of 260,000–309,000 metric tons of engineered nanomaterials was released directly into water bodies.¹⁵ As the use of these NPs in industrial applications increases, it is becomes more likely that CeO₂ NPs will coexist with other aqueous constituents. Among such constituents of aquatic systems, arsenic is of particular interest due to its own inherent toxicity, as well as its active redox reactivity. Arsenic enters aqueous environments through both natural geochemical processes, such as the dissolution of arsenicbearing minerals,¹⁶⁻¹⁸ and anthropogenic activities, such as leaching from municipal solid waste.¹⁹ Toxic and carcinogenic, arsenic can cause acute and chronic adverse health effects such as tumors through various pathways.²⁰ Aqueous arsenic usually exists in two forms: arsenite (AsO_3^{3-} , pKa =9.23, 12.13, and 13.4, abbreviated to As^{3+} in this manuscript), which is more toxic and mobile, or arsenate (AsO₄³⁻, pKa = 2.22, 6.98, and 11.53, abbreviated to As⁵⁺), which is less toxic and adsorbs more easily on common mineral surfaces in the environment.²¹ Furthermore, As³⁺ can exist in naturally reducing environments such as anoxic lake sediments,²² and can persist during water treatment processes.²³

Physicochemical interactions between Ce^{IV}O₂(s) and arsenic are also of particular interest in the field of chemical mechanical planarization.²⁴ Along with silica (SiO₂) and alumina (Al₂O₃) NPs, CeO₂ NPs are frequently used in aqueous slurries to polish wafers during semiconductor manufacturing.^{25, 26} Gallium arsenide (GaAs), for example, is a III-V group semiconductor which is important in the manufacturing of high-efficiency solar cells.^{27, 28} Waste from polishing GaAs wafers can contain high concentrations of dissolved arsenic (1800–2400 mg/L), along with CeO₂ NPs.²⁹ Chemical reactions between arsenic and CeO₂ NPs in this waste stream can impact the efficacy of wastewater treatment processes to remove these contaminants and may also affect the polishing process by changing the NP aggregation.^{24, 30} The co-existence of high levels of arsenic and CeO₂ NPs in this waste stream has been the impetus for recent studies on interactions between CeO₂ NPs and arsenic.^{24, 30, 31}

In addition to these natural and industrial situations where arsenic and CeO₂ NPs can coexist, there is increasing interest in applying CeO₂ NPs as novel sorbents for removal of arsenic species.³²⁻³⁶ However, while these studies have proven the sorption capacity of CeO₂ NPs, little effort has been spent on understanding how sorption may affect the surface chemistry of NPs after water treatment.³⁷ This is of particular importance because separation of these NPs from solution after treatment requires a thorough knowledge of the nature of NPs. For example, the identity and aggregate size of NPs will determine the selectivity of cross-flow membrane filtration, a commonly used method for nanoparticle separation from an aqueous solution.³⁸ As CeO₂ NPs find increasing application as novel sorbents, it is even more vital to characterize how interactions with target adsorbates, such as arsenic, will affect the surface chemistry of NPs.

Adsorption isotherms of aqueous As^{5+} and As^{3+} onto CeO_2 NPs have been investigated previously, with a particular emphasis on arsenic remediation.³⁹ However, the study did not consider the possibility of redox reactions between arsenic species and CeO_2 NPs and its consequential effect on the stability and surface chemistry of CeO_2 NPs. Another recent study also reported adsorption isotherms of As^{5+} and As^{3+} on CeO_2 NPs at pH 3.6, and found that the adsorption of As^{5+} and As^{3+} onto CeO_2 NPs inhibited the NP surface reactivity.²⁴ While this study

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provided useful information on surface reactivity, a better understanding of the surface redox interactions between arsenite and CeO_2 NPs and their impacts on aggregation and dissolution of CeO_2 NPs will help to predict how these interactions affect the fate and transport of CeO_2 NPs and their associated hazards.

The fate, transport, and associated risk posed by CeO₂ NPs in aquatic systems are largely determined by their dissolution and colloidal stability. As mentioned previously, the mobilization of Ce from solid CeO₂ NPs to the aqueous phase generally results from the reduction of Ce^{IV} to Ce^{III}.⁴⁰ In addition, Ce³⁺ has been shown to have a higher toxicity than Ce^{4+,41} For risk reduction, it is vital to understand the reductive dissolution of CeO₂ NPs. To predict the environmental risk of CeO₂ NPs, their colloidal stability must also be assessed because it is an indicator of the potential quantities that can be transported downstream. A previous study on NP transport in a model wastewater treatment plant found that up to 6% of the original quantity of CeO₂ NPs were present in the secondary effluent streams.⁴² This large amount can be attributed to the high colloidal stability of these NPs in aqueous systems, owing to their surface coating with surfactants during NP preparation,⁴² as well as to surface charge alteration by the adsorption of ions (e.g., Fe²⁺)^{10, 43}, natural organic matter⁴⁴ and proteins^{45, 46} present in wastewater, which increase the electrostatic repulsive forces between NPs.

Moreover, the surface chemistry of colloidal NPs can also be altered by redox reactions, which can form additional solid coatings. With regard to the potential redox reactions between CeO_2 NPs and As^{3+} , the half reactions and overall reaction are listed below:

$$AsO_3^{3-} + H_2O \rightarrow AsO_4^{3-} + 2H^+ + 2e^-, \qquad E_{1/2}^0 = -0.56 \text{ V}$$
 (1)⁴⁷

$$CeO_2(s) + e^- + 4H^+ \rightarrow Ce^{3+} + 2H_2O,$$
 $E_{1/2}^0 = 1.66V$ (2)⁴⁸

$$2Ce^{IV} + AsO_3^{3-} + H_2O \rightarrow 2Ce^{3+} + AsO_4^{3-} + 2H^+ \qquad E_{cell}^0 = 1.10V \tag{3}$$

As shown in reaction 3, the E_{cell}^0 value is 1.10 V, indicating that the reduction of Ce^{IV}O₂ to Ce³⁺ by AsO₃³⁻ is thermodynamically favorable. However, the kinetic consideration of reductive dissolution of Ce^{IV} by As³⁺ relative to expected transport times during wastewater treatment has not yet been explored.

The purpose of this study is, therefore, to investigate the effects of As^{3+} on the colloidal stability, fate, and transport of CeO₂ NPs in a model aqueous system. First, the effects of As^{3+} on the colloidal stability of CeO₂ NPs were examined for three different As^{3+} concentrations, then the dissolution of CeO₂ NPs was compared for the same systems. Trends in dissolution and colloidal stability were next systematically investigated to delineate the mechanisms governing each system. This paper, for the first time, reports how As^{3+} adsorption and redox surface reactions on $Ce^{IV}O_2$ NPs impact CeO₂ NPs in aqueous environments. This study provides important information that can support more accurate risk assessment of CeO₂ NPs in natural and engineered aquatic systems.

EXPERIMENTAL SECTION

Materials

In this study, commercial CeO₂ NPs (<25 nm, Sigma-Aldrich, MO) were used to simulate industrially manufactured NPs. X-ray photoelectron spectroscopy (XPS) analysis of the starting CeO₂ NP material showed that the powder contained 15.5% Ce^{III} (Figure 1A), which is consistent with the Ce^{III} starting content measured by a previous study using CeO₂ NPs.⁴⁹ Reagents used included sodium nitrate (NaNO₃, ACS grade, J.T. Baker, PA), sodium arsenite (NaAsO₂, \geq 90%, Sigma Aldrich, MO), and 67–70% nitric acid (HNO₃, BDH, PA). To preclude the effect of oxygen

on redox reactions, all preparations and reaction procedures were performed in an anaerobic chamber (Coy vinyl type-B, MI). All water used to generate the reaction solutions for anaerobic experiments was degassed de-ionized (DI) water. The conductivity of the DI water was equal to or higher than 18.2 M Ω -cm. DI water was deoxygenated by boiling it in an electric kettle and cooling it overnight to room temperature in the anaerobic chamber.

Because dissolved oxygen is present in real aquatic systems, we also tested the settling trends of CeO₂ NPs under aerobic conditions for comparison (Figure S1-S3, Electronic Supplementary Information, ESI). For those experiments, DI water equilibrated with atmospheric O_2 was used, and the experiments were performed under atmospheric O_2 conditions. While these experiments helped to determine whether atmospheric oxygen affects interactions between CeO₂ NPs and As³⁺ oxyanions, they also complicated our exploration of the mechanistic interactions between CeO₂ NPs and As³⁺ oxyanions. To clearly elucidate the surface redox interactions between As³⁺ and CeO₂ NPs, we thus limited further investigations to anaerobic systems only.

Sedimentation Experiments

For anaerobic experiments, stock solutions, including CeO₂ NP dispersions, As³⁺, and NaNO₃ solutions (for ionic strength adjustment), were prepared in the anaerobic chamber. First, a 50 mg/L CeO₂ NP dispersion was created by adding commercial CeO₂ NPs to deoxygenated DI water. The suspension was sonicated for 60 minutes to break up aggregates. A 0.005 M sodium arsenite (As³⁺) stock solution and a 0.5 M NaNO₃ stock solution were also prepared in the anaerobic chamber. The 50 mg/L CeO₂ dispersion was separated into 50 mL test tubes. Aliquots of As³⁺ and NaNO₃ stock solutions were added to the dispersions to create four systems: a control system, which contained only 10 mM NaNO₃, and three different arsenite systems, which contained 10 mM NaNO₃ with 10⁻⁶, 10⁻⁵, or 10⁻⁴ M As³⁺. Arsenic concentrations as high as 10,000 ppb (1.4×10^{-4})

M) have been observed in environmental systems.⁵⁰⁻⁵² By adding dilute HNO_{3} , the As systems and control system were adjusted to pH 5, a value which is relevant to acidic aquatic systems, such as acid mine drainage sites or sites impacted by acid rain. In addition, this pH is observed in water treatment systems during coagulation with iron (pH 4.5–5.5) or aluminum (pH 5–6).⁵³ At this system pH, As³⁺ will exist primarily in H₃AsO₃ form, while As⁵⁺, if it were to form, would exist primarily as H₂AsO₄⁻.

Next, the solutions were allowed to settle in the anaerobic chamber. Starting immediately after pH adjustment (i.e., 0 hr), approximately 1 mL samples were taken at 2-hour intervals for the first 8 hours of reaction, and after 24 hrs. To avoid oxygen exposure, these samples were placed in 3-mL polyethylene cuvettes and capped before being removed from the chamber. Then, the absorbance was immediately measured at a wavelength of 305 nm using a UV-Visible spectrometer (UV-Vis, Varian Cary 50 Bio, CA). The 305 nm wavelength was chosen because the absorbance of CeO₂ NPs is at its peak there, while that of As is negligible.⁴⁰ The linear relationship between CeO₂ concentration and the 305 nm wavelength absorption was confirmed by creating a calibration curve (Figure S4 in the ESI). Samples were taken from the same vertical depth (approximately 1-2 cm below the surface) in the test tube to ensure that settling was monitored accurately. The design of these experiments was based on our previously reported colloidal stability studies^{10, 43, 44}, and all reaction systems were performed in triplicate. After 2 hours, the particle size and surface charge were measured for the particle dispersion using a Zetasizer (Malvern ZEN3600, U.K.). Because all systems came from the same 50 mg/L CeO₂ NP dispersion stock, the initial particle size and zeta potential of CeO_2 NPs were assumed to be the same for all systems. To determine the isoelectric point (pH_{iep}) of unreacted CeO₂ NPs, the solution was separated into four test tubes, the pH of each was adjusted to values between 3 and 10, and the zeta

 potential of each pH system was measured. The pH_{iep} was calculated by interpolation between the measured zeta potentials over the pH range.

Dissolution Experiments

The stock solutions for CeO₂ NP dissolution experiments were prepared following the same procedure as for the sedimentation experiments. However, rather than allowing the CeO₂ NPs to settle, 5 mL aliquots of each system were divided into test tubes. The test tubes were placed in a tube rotator (VWR 10136-084, PA) and rotated at 18 rpm for 24 hours, during which time samples were taken at 0, 2, 4, 6, 8, and 24 hours. This mixing allowed for uniform reaction between the CeO_2 NPs and solution. To remove CeO_2 NPs, samples were centrifuged at 40,000 rpm for 30 minutes using an ultracentrifuge (Thermo Scientific 46900WX80, NC). Based on a study by Tsao et al.,⁵⁴ this speed and time of the ultracentrifugation have been shown to be sufficient enough to settle 25 nm NPs from solution, and we expect most NPs in our systems to exist as > 200 nm aggregates as measured after reaction. This method has also been widely applied to separate CeO_2 NPs from solution in previous studies.⁵⁵⁻⁵⁷ The supernatant was then filtered through a 0.22 µm polypropylene syringe filter and acidified to 1% v/v HNO₃. If this ultracentrifuge/filtration method did not sufficiently remove CeO₂ NPs from solution, we would expect increased Ce concentrations at 0 hr, where the aggregate size is expected to be smallest. Instead, we found that the early time points had lower concentrations. In particular, for the control system at 0 hr, where there were no reactants to accelerate dissolution, there was negligible Ce in solution (Figure 4A). This conclusively shows that all NPs which are in the solid state are separated from solution using our ultracentrifuge/filtration method.

Concentrations of aqueous Ce and As in the supernatant were measured by inductively coupled plasma mass spectroscopy (ICP-MS, Agilent 7500 series, CA). As the solubility of Ce^{III}

is 3.2×10^{39} times higher than that of Ce^{IV}, we assumed all soluble Ce ions were Ce³⁺. It has also been shown in recent studies that dissolution of CeO₂ leads to surface depletion of Ce^{III}.⁵⁸⁻⁶⁰ All samples for settling and dissolution experiments were collected in triplicate. Reported error bars give the standard deviation between triplicate samples.

To quantify As speciation (As^{3+} or As^{5+}), additional samples containing arsenic were measured for As speciation after 6 hours and 24 hours. For this test, samples were centrifuged and filtered as described above. Next, their pH was adjusted to 3.5, and 10 mL of sample was passed through an ion-exchange column packed with resin (Dowex 1×8 in chloride form, Sigma Aldrich, MO), which allowed only As^{3+} to pass.⁶¹ The first 5 mL were discarded and the next 5 mL were collected and measured using ICP-MS. These samples gave the amount of As^{3+} in solution, while the samples which were not passed through the column gave the total As.

Characterizations of solid phases and surface complexation

Solid phase characterization was carried out using several complementary techniques. First, transmission electron microscopy (TEM, JEOL 2100F, MA) was used to image the morphologies and aggregated patterns of CeO₂ NPs. Electron diffraction patterns for selected areas were obtained to examine secondary precipitation in our reaction systems. As described above, four systems were created for settling experiments. After 2 hours of settling, approximately 50 μ L of solution from each reaction system was placed on a 300-mesh Cu Formvar-carbon grid, and the four grids were dried in a desiccator in the anaerobic chamber. After drying, the grids were placed in a storage box and taken out of the anaerobic chamber for analysis.

To determine the oxidation states of cerium and arsenic, XPS (PHI 5000 VersaProbe II, Ulvac-PHI with monochromatic Al Kα radiation (1486.6 eV)) was used. High resolution scans

were taken at 0.1 eV steps and a pass energy of 23.5 eV. For XPS sample preparation, four 1-L batches of samples were created for the same reaction conditions described above and reacted for 24 hours. The solutions were then ultra-centrifuged in small batches for 30 minutes at 40,000 rpm. After removal of the supernatant, the solids in the test tubes were collected and dried in a desiccator inside the anaerobic chamber. Ce 3d, As 3d, and O 1s spectra were analyzed and fitted using MultiPak software (Physical Electronics) with the Gaussian-Lorentzian fitting function, using the C 1s (284.8 eV) spectrum as the energy reference. In fitting of spectra of different samples, the binding energies were fixed with 0.1 eV variation. For example, 44.25 eV to 44.34 eV were considered as 44.3 eV. The full width at half maximum (FWHM) of the peaks were fixed with no variation. The peak heights and areas were variables to be fitted. The area percentage of an oxidation state was used to represent its amount percentage among different oxidation states. Note that during the fitting, small changes of peak binding energies (< 0.1 eV) would lead to a percentage error of \pm 2%. The reference binding energy peaks for Ce 3d were 884.3 and 902.6 eV for Ce^{III}, and 907.0, 900.6, 898.1, 888.7, 882.1 eV for Ce^{IV}.^{44, 62, 63} The reference binding energy peaks for As 3d were 44.3 eV for As^{III} and 45.3 eV for As^{V.64} The reference binding energy peaks for O 1s were 529.3 eV for lattice oxygen in CeO₂, 530.9 eV for As-O bond, 531.4 eV for H-O bond, and 533.4 eV for residual adsorbed H₂O.⁴⁴

To investigate how surface reactions might influence CeO_2 NP stability in the presence of arsenite, Fourier transform infrared spectroscopy (FTIR, Thermo Nicolet Nexus 470, NC) examined arsenite surface complexation with CeO_2 NPs. For these experiments, large batches were prepared identically to those for XPS experiments. Once samples were dried in the anaerobic chamber, they were mixed with KBr at a 10:1 ratio. Samples were measured immediately at a resolution of 0.1, and 1000 scans were taken.

RESULTS AND DISCUSSION

Fastest settling in the 10⁻⁴M As³⁺ system.

To identify surface chemistry changes of CeO_2 NP in the presence of arsenite, we first measured the aggregation and settling rates of CeO_2 NP under different aqueous conditions. Figure 2A shows the sedimentation trends for the As^{3+} -containing systems and the control system as a function of time. Over the first eight hours of reaction, settling trends were similar in the 10⁻⁵ M As³⁺, 10⁻⁶ M As³⁺, and control systems. On the other hand, for the 10⁻⁴ M As³⁺ system, settling occurred very quickly. By eight hours, less than 10% of the CeO₂ NPs remained in solution for the 10⁻⁴ M As system, while around 80% remained in solution for the other two As³⁺-containing systems.

To better understand these trends, the particle sizes and zeta potentials of CeO₂ NPs were measured for the four systems after 2 hours of reaction, at which point the settling differences had become defined. Aggregate sizes and zeta potentials for the four systems are shown in Figure 2B. Note that the pH_{iep} of unreacted CeO₂ NPs is 8.7 with 10 mM NaNO₃ (Figure 1B). For the 10⁻⁵ M As³⁺, 10⁻⁶ M As³⁺, and control systems, the zeta potentials were highly positive, leading to strong electrostatic repulsive forces which prevented extensive aggregation. Therefore, smaller aggregate sizes and higher colloidal stability in solutions were observed. Moreover, because the zeta potentials were similar for these systems, we speculate that the smaller size in the 10⁻⁵M and 10⁻⁶M As³⁺ systems than that in the control resulted from changes in the surface hydrophilicity by arsenite adsorption. In other words, the CeO₂ NP surface is intrinsically hydrophobic⁴⁰ due to the unique electronic structure of cerium. Thus, adsorption of arsenite that is easily solvated can make the NP surface less hydrophobic, decreasing the tendency of these NPs to aggregate, without significantly altering the zeta potential. For the 10⁻⁴ M As³⁺ system, on the other hand, the zeta potential decreased to close to zero, suggesting that electrostatic repulsive forces between NPs

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became significantly weaker. As a result, CeO_2 NPs in this system aggregated quickly, resulting in a large hydrodynamic diameter and fast settling.

The differences in NP morphology between NPs in the 10^{-4} M As³⁺ system and the other systems were examined using TEM. As shown in Figure 3, CeO₂ NPs in the 10^{-4} M As³⁺ system were more heavily aggregated than those in other systems, which was consistent with particle size and settling trends. It is noteworthy that the drying process on the TEM grid can cause aggregation, but the extent of the effect of drying on aggregation should be similar across all reaction systems. On the other hand, there was no distinct difference in the morphology of individual particles in the four systems, and we found no evidence of secondary mineral phase formation from the highresolution images and lattice fringe analyses of CeO₂ NPs (Figures S5 and S6 in the ESI).

Fastest dissolution in the $10^{-5} M As^{3+}$ system.

To obtain additional insight into the settling and size trends of CeO₂ NPs, the dissolution of CeO₂ NPs was measured over a 24-hour reaction period. As shown in Figure 4A, the greatest dissolution of CeO₂ NPs occurred in the 10^{-5} M As³⁺ system, followed by the 10^{-4} M As³⁺ system. Very little dissolution of CeO₂ NPs occurred in the 10^{-6} M As³⁺ system or in the control system. The concentrations of total aqueous arsenic in these systems were also measured, and the results can be found in Figure S2A in the ESI. Such dissolution trends are interesting because the greatest dissolution of CeO₂ NPs occurred in the median As³⁺ concentration of 10^{-5} M, rather than in the 10^{-4} M As³⁺ system, which could be expected if As³⁺ enhanced dissolution through redox interactions. This dissolution trend instead appears to be more related to aggregation. In particular, the 10^{-4} M As³⁺ system had a larger degree of aggregation than the 10^{-5} M As³⁺ system, which had an aggregate size similar to the 10^{-6} M As³⁺ system. As these systems contained the same initial quantities of CeO₂ NPs, we expect that the larger aggregates in the 10^{-4} M As³⁺ system will result

in less exposed surface area for dissolution than the 10^{-5} M As³⁺ system, and thus less Ce dissolution can occur. A discussion of aggregation effects on the nanoparticle surface area can be found in Section S4 the ESI.

Although the dissolution trend of CeO_2 NPs was interesting, it does not explain why aggregation occurred heavily with 10⁻⁴ M As³⁺, leading to fast settling in the 10⁻⁴ M As³⁺ system. Considering that dissolution of CeO₂ NPs can be indicative of redox interactions, due to the low solubility of Ce^{IV} compared to Ce^{III}, we first explored whether the oxidation state of Ce and/or adsorbed As on the CeO₂ NP surface could change the zeta potential and subsequent aggregation of CeO₂ NPs.

Redox interactions of Ce^{IV} and As^{3+} .

To test this hypothesis, we considered the oxidation states of Ce and As in the solid phase and the As speciation in the aqueous phase. In the presence of CeO₂ NPs, the percentages of aqueous As³⁺ were 99.7%, 97.7%, and 99.5% for the 10⁻⁶ M As³⁺, 10⁻⁵ M As³⁺, and 10⁻⁴ M As³⁺ systems after 6 hours, respectively, confirming that the reaction condition was anaerobic during experiments and that no significant arsenite oxidation occurred in the aqueous phase within the experimental period. Considering that the starting arsenite salt itself had an assay value of \geq 90% per the manufacturer, the slight differences among three systems could not be attributed conclusively to the extents of redox interactions between CeO₂ NPs and As³⁺.

Because the speciation of redox-active species can differ depending on the phase (i.e., in solution or on solid surfaces), we also used XPS to monitor the speciation of Ce (Figure 4B) and As (Figure 4C) on the CeO₂ NP surfaces. Ce 3d spectra showed increases in Ce^{III} content with increasing As^{3+} concentrations, with the Ce^{III} percentage increasing from 17.0% in the control

 sample to 21.0%, 23.1%, and 24.8% in the 10⁻⁶ M, 10⁻⁵ M, and 10⁻⁴ M As³⁺ systems, respectively (Figure 4B). The As 3d spectra also showed increasing extents of redox reactions with increasing As³⁺ concentrations. In particular, a clear difference can be observed between the 10⁻⁶ M As³⁺ system and 10⁻⁴ M As³⁺ system (Figure 4C). Surface arsenic in the 10⁻⁶ M As³⁺ system was 69.8% As^{III}, indicating that 30.2% of arsenite adsorbed on CeO₂ NP surfaces had been oxidized to As^V. For the 10⁻⁴ M As³⁺ systems, the percentages of As^{III} oxidized to As^V were 42.1%, 11.9% higher than that in the 10⁻⁶ M As³⁺ system, which was significant considering the fitting error (\pm 2%). Therefore, these results indicate that (1) the co-occurrence of CeO₂ NPs and As³⁺ will trigger redox interactions between Ce^{IV} and As^{III}, forming Ce^{III} and As^V, as predicted by thermodynamic calculations (Eq. 3); and (2) increasing aqueous arsenite concentrations will trigger a higher extent of arsenite oxidation on NP surfaces. The As^V percentages on CeO₂ NP surfaces were also significantly higher than the As^V percentages in solutions, indicating that the oxidation of arsenite happened predominantly on the CeO₂ NP surfaces.

Interestingly, the increased surface Ce^{III} percentages do not account for the aqueous cerium concentration trends in the different arsenite concentration systems. The Ce^{III} percentages on the NP surfaces increased with higher aqueous arsenite concentrations, whereas the dissolved cerium concentration (Ce³⁺) was the highest in the 10⁻⁵ M As³⁺ system. Although redox interactions are expected to increase Ce solubility, the higher extent of aggregation of CeO₂ NPs in the 10⁻⁴ M As³⁺ system appears to have prevented more dissolution of the formed Ce^{III} from the CeO₂ surface, contributing to the higher surface Ce^{III} percentages measured with XPS. In terms of the effects of redox interactions on the NP surface charge, redox interactions alone cannot explain the significantly lower zeta potential in the 10⁻⁴ M system. For instance, while the observed redox interaction extents from XPS were similar between the 10⁻⁵ M and 10⁻⁴ M As³⁺ systems (Figures

4B and 4C), the zeta potentials for these two systems varied greatly. We therefore further hypothesized that aqueous As^{3+} adsorption contributes to the observed change in NP surface charge. We proceeded to test this hypothesis using both XPS results and the literature, as described in the following section.

A proposed mechanism for CeO_2 -As³⁺ interactions.

To test whether As^{3+} adsorption onto CeO_2 NPs could be the underlying mechanism for the observed settling trends, we examined the XPS O1s spectra of the samples. These spectra provide additional information about the extent of arsenic adsorption onto CeO₂ NP surfaces (Figure 4D and 4E). The peak at 531.0 eV was attributed to the As–O bond, observed on the CeO₂ NP surface in the presence of arsenite.⁶⁵ With increasing arsenic concentrations, the relative intensity of this peak increases, indicating a larger arsenic sorption extent. For example, when As³⁺ concentration increased from 10⁻⁶ M to 10⁻⁴ M, the area percentage of the As-O bonds increased from 5.5% to 20.5% (Figure 4E), while the area percentage of the H–O bonds decreased from 29.0% to 13.3%. This observation suggests that the adsorption of arsenite onto CeO₂ NPs might replace the original hydroxyl groups on the surface. Previous studies have also reported ligand exchange of the hydroxyl group of metal oxides with arsenate or arsenite during arsenic adsorption.^{66, 67} Furthermore, FTIR results (Figure 4F) show a peak at ~830 cm⁻¹ for CeO₂ NP samples from arsenite-containing systems, which was attributed to the stretching of As-O bonds in arsenite.⁶⁸ The intensity of this peak increased with increasing arsenite concentrations, indicating a higher extent of arsenite adsorption on CeO₂ NP surfaces. Because the peak position did not change, arsenite in these systems are thought to be sorbed in the same fashion, and the differences in CeO_2 NP sedimentation could result from the quantity sorbed rather than changes in the sorbing mechanism.

Jian and Ali (2000) have shown that As³⁺ adsorption on Fe-containing minerals can decrease their zeta potentials²¹ owing to surface complexation between As³⁺ and mineral surfaces, which replaces surface hydroxyl groups, thus decreasing the surface charge. We propose that a similar mechanism is responsible for the lower colloidal stability of CeO₂ NPs in arsenic systems. Prior to arsenite adsorption, a high degree of surface protonation leads to a high positive zeta potential value for CeO₂ NP surfaces at pH 5, as confirmed by the $pH_{iep} = 8.7$ of CeO₂ NPs in 10 mM sodium nitrate (Figure 1B). The CeO₂ surface was also reported to be positively charged due to protonated surface hydroxyl groups, $-OH_2^+$, at pH lower than pH_{iep} .^{44, 69} After As³⁺ adsorbs onto CeO₂ NPs in the primary form of H₃AsO₃ at pH 5, it decreases the surface charge of NPs by replacing –OH₂⁺ groups from the surface with arsenite during surface complexation—which is confirmed by the XPS O 1s results (Figure 4E). With more arsenite molecules adsorbed onto the CeO_2 NP surfaces, there is a net loss of protons,²¹ further decreasing the positive surface charge and lowering the zeta potential, despite the fact that arsenite is uncharged at pH 5. The surface charge alteration of CeO₂ NPs owing to the release of surface protons has also been reported for the interaction of CeO₂ NPs with natural organic matter.⁴⁴ Moreover, the adsorbed arsenate anions $(H_2AsO_4^- \text{ at pH 5})$ could contribute partially to the more neutralized surface charge at higher As³⁺ concentrations. However, considering there was no difference in the size or zeta potential for the 10⁻⁶ M and 10⁻⁵ M As³⁺ systems, despite the 10⁻⁵ M As³⁺ system having both more sorption and significantly more oxidation to As(V), the adsorption of As^{5+} may not be a main contributor to CeO₂ NPs' colloidal stability.

To further confirm our hypothesis, we estimated the quantities of adsorbed arsenic molecules on the CeO_2 NP surface. Using the arsenic concentrations in solution measured by ICP-MS (Figure S2A, ESI)—which accounts for the net aqueous arsenic concentration after

adsorption—we calculated the number of arsenic molecules adsorbed on the NP surface by subtracting these values from the total arsenic concentrations added. For the 10^{-6} M, 10^{-5} M, and 10^{-4} M As³⁺ systems, the adsorbed arsenic amounts were 1.1×10^{19} , 6.8×10^{19} , and 6.7×10^{20} As molecules/g CeO₂, respectively. These values correspond with an As loading of 1.3 to 83.4 mg/g for 0.075 to 7.5 mg/L As³⁺, which aligns well with reported values for As³⁺ sorption by CeO₂ NPs.³³ With higher aqueous arsenite concentrations, the adsorbed arsenic molecules on CeO₂ NPs increased, further neutralizing the surface charge and decreasing the electrostatic repulsive forces between NPs. Therefore, we conclude that arsenite adsorption is the dominant mechanism responsible for the fastest aggregation and settling in the 10^{-4} M As³⁺ system.

CONCLUSIONS AND ENVIRONMENTAL IMPLICAIONS

This study describes important physicochemical interactions between As³⁺ and CeO₂ NPs, which are summarized and presented in Figure 5. First, in the 10⁻⁴ M As³⁺ system, the fastest aggregation and settling occurred due to neutralization of the surface potential of NP surfaces by arsenite adsorption. In higher As³⁺ concentration systems (10⁻⁵ M and 10⁻⁴ M As³⁺), we observed oxidation of adsorbed As^{III} to As^V, triggering the reduction of Ce^{VI} to Ce^{III} and the dissolution of Ce³⁺ from the NP surface. However, dissolution was more prominent in the 10⁻⁵ M As³⁺ system than in the 10⁻⁴ M As³⁺ system, because less CeO₂ NP aggregation led to a higher exposed surface area.

This study deepens our current understanding of the hazards posed by widely applied CeO₂ NPs. As demonstrated, in the presence of 10^{-4} M As³⁺, CeO₂ NPs aggregated and settled more quickly due to As³⁺ adsorption. Thus, less settlement time is required to remove CeO₂ NPs by sedimentation under this condition. The altered surface charge can also affect the bioaccumulation of CeO₂ NPs. A previous study found that positively charged CeO₂ NPs, which were observed in our control, 10^{-6} M, and 10^{-5} M As³⁺ systems, were significantly more toxic to *Caenorhabditis*

elegans than neutrally charged CeO₂ NPs, which were observed only in our 10^{-4} M As³⁺ system.⁷⁰ Lastly, increased aggregation of CeO₂ NPs led to less Ce³⁺ mobilization in the 10^{-4} M As³⁺ system than in the 10^{-5} M As³⁺ system, which directly affects the risk posed by CeO₂ NPs because Ce³⁺ is toxic to organisms. However, it is also important to consider how other environmentally abundant water constituents, such as natural organic matter, sulfate, phosphate, and nitrate, will influence interactions between CeO₂ NPs and arsenic species. To gain a more detailed molecular scale understanding of such dynamic systems, more studies on complexation (e.g., inner or outer-sphere complexation), and surface electron transfer between Ce^{IV} and As^{III} to cause the redox reactions can be good future research directions.

The high colloidal stability of CeO₂ NPs, which was observed in the control system and systems with lower initial As^{3+} concentrations, indicated that NPs can stay suspended for longer times, thus either more settlement time should be allowed before discharge in water treatment plants, or additional treatment may be required to remove these NPs. More importantly, this study shows that CeO₂ NPs also have a high adsorption capacity for arsenic, with 90–95% of As^{3+} adsorbed on the particle surface in the 10⁻⁶ M As^{3+} system. Therefore, in systems with low As^{3+} concentrations, As^{3+} coexisting with CeO₂ NPs may pose additional challenges, as it tends to stay on CeO₂ NP surfaces and travel for long distances, requiring more comprehensive risk assessment and waste management. These new insights into CeO₂ NPs transport and reactivity, along with their increasing industrial use, provide an impetus for future study of additional factors impacting these emerging NPs, such as the effects of pH, ionic strength, and the presence of additional redox-reactive compounds.

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Electronic supplementary information (ESI)

ESI includes 8 pages and 6 figures, which describe additional studies on the impact of dissolved oxygen on the experimental system, calibration of UV-vis sedimentation measurements, TEM investigation of secondary mineral formation, and aggregation effects on NP surface area.

References

1. Zhang, H.; He, X.; Zhang, Z.; Zhang, P.; Li, Y.; Ma, Y.; Kuang, Y.; Zhao, Y.; Chai, Z., Nano-CeO₂ Exhibits Adverse Effects at Environmental Relevant Concentrations. *Environ. Sci. Technol.* **2011**, *45* (8), 3725-3730.

2. Speed, D.; Westerhoff, P.; Sierra-Alvarez, R.; Draper, R.; Pantano, P.; Aravamudhan, S.; Chen, K. L.; Hristovski, K.; Herckes, P.; Bi, X.; Yang, Y.; Zeng, C.; Otero-Gonzalez, L.; Mikoryak, C.; Wilson, B. A.; Kosaraju, K.; Tarannum, M.; Crawford, S.; Yi, P.; Liu, X.; Babu, S. V.; Moinpour, M.; Ranville, J.; Montano, M.; Corredor, C.; Posner, J.; Shadman, F., Physical, chemical, and in vitro toxicological characterization of nanoparticles in chemical mechanical planarization suspensions used in the semiconductor industry: towards environmental health and safety assessments. *Environmental Science: Nano* **2015**, *2* (3), 227-244.

3. Piccinno, F.; Gottschalk, F.; Seeger, S.; Nowack, B., Industrial production quantities and uses of ten engineered nanomaterials in Europe and the world. *J. Nanopart. Res.* **2012**, *14* (9), 1-11.

4. Milani, Z. M.; Charbgoo, F.; Darroudi, M. J. C. I., Impact of physicochemical properties of cerium oxide nanoparticles on their toxicity effects. *Ceram. Int.* **2017**, *43* (17), 14572-14581.

5. Gomez-Rivera, F.; Field, J. A.; Brown, D.; Sierra-Alvarez, R., Fate of cerium dioxide (CeO₂) nanoparticles in municipal wastewater during activated sludge treatment. *Bioresour*. *Technol.* **2012**, *108*, 300-304.

6. Celardo, I.; De Nicola, M.; Mandoli, C.; Pedersen, J. Z.; Traversa, E.; Ghibelli, L., Ce³⁺ ions determine redox-dependent anti-apoptotic effect of cerium oxide nanoparticles. *ACS Nano* **2011**, *5* (6), 4537-4549.

7. Pirmohamed, T.; Dowding, J. M.; Singh, S.; Wasserman, B.; Heckert, E.; Karakoti, A. S.; King, J. E.; Seal, S.; Self, W. T., Nanoceria exhibit redox state-dependent catalase mimetic activity. *Chem. Commun.* **2010**, *46* (16), 2736-2738.

8. Plakhova, T. V.; Romanchuk, A. Y.; Yakunin, S. N.; Dumas, T.; Demir, S.; Wang, S.; Minasian, S. G.; Shuh, D. K.; Tyliszczak, T.; Shiryaev, A. A.; Egorov, A. V.; Ivanov, V. K.; Kalmykov, S. N., Solubility of Nanocrystalline Cerium Dioxide: Experimental Data and Thermodynamic Modeling. *J. Phys. Chem. C* **2016**, *120* (39), 22615-22626.

9. Jianjun, Z.; Bingwei, L.; Chenxuan, Y.; Xiangdong, R., Application of Ce(IV) in industrial wastewater treatment. *J. Rare Earths* **2010**, *28*, 37-39.

10. Liu, X.; Ray, J. R.; Neil, C. W.; Li, Q.; Jun, Y.-S., Enhanced colloidal stability of CeO₂ nanoparticles by ferrous ions: adsorption, redox reaction, and surface precipitation. *Environ. Sci. Technol.* **2015**, *49* (9), 5476-5483.

11. Speed, D., Environmental aspects of planarization processes. In *Advances in Chemical Mechanical Planarization (CMP)*, Elsevier: 2016; pp 229-269.

12. Thill, A.; Zeyons, O. I.; Spalla, O.; Chauvat, F.; Rose, J. m.; Auffan, M. I.; Flank, A. M., Cytotoxicity of CeO₂ nanoparticles for Escherichia coli. Physico-chemical insight of the cytotoxicity mechanism. *Environ. Sci. Technol.* **2006**, *40* (19), 6151-6156.

13. Park, E.-J.; Choi, J.; Park, Y.-K.; Park, K., Oxidative stress induced by cerium oxide nanoparticles in cultured BEAS-2B cells. *Toxicology* **2008**, *245* (1), 90-100.

14. ILS, Chemical Information Profile for Ceric Oxide [CAS No. 1306-38-3]. National Institute of Environmental Health Sciences, N. I. o. H., Ed. Research Triangle Park, NC. , 2006.

15. Keller, A. A.; McFerran, S.; Lazareva, A.; Suh, S., Global life cycle releases of engineered nanomaterials. *J. Nanopart. Res.* **2013**, *15* (6), 1-17.

16. Neil, C. W.; Yang, Y. J.; Jun, Y.-S., Arsenic mobilization and attenuation by mineralwater interactions: implications for managed aquifer recharge. *J. Environ. Monitor.* **2012**, *14* (7), 1772-1788.

17. Wu, X.; Bowers, B.; Kim, D.; Lee, B.; Jun, Y.-S., Dissolved Organic Matter Affects Arsenic Mobility and Iron (III)(hydr) oxide Formation: Implications for Managed Aquifer Recharge. *Environ. Sci. Technol.* **2019**.

18. Wu, X.; Burnell, S.; Neil, C. W.; Kim, D.; Zhang, L.; Jung, H.; Jun, Y.-S., Effects of Phosphate, Silicate, and Bicarbonate on Arsenopyrite Dissolution and Secondary Mineral Precipitation. *ACS Earth Space Chem.* **2020**, *4* (4), 515-525.

19. Ghosh, A.; Mukiibi, M.; Ela, W., TCLP underestimates leaching of arsenic from solid residuals under landfill conditions. *Environ. Sci. Technol.* **2004**, *38* (17), 4677-4682.

20. Shi, H.; Shi, X.; Liu, K. J., Oxidative mechanism of arsenic toxicity and carcinogenesis. *Mol. Cell. Biochem.* **2004**, *255* (1-2), 67-78.

21. Jain, C.; Ali, I., Arsenic: occurrence, toxicity and speciation techniques. *Water Res.* 2000, *34* (17), 4304-4312.

22. Hoeft, S. E.; Lucas, F. o.; Hollibaugh, J. T.; Oremland, R. S., Characterization of microbial arsenate reduction in the anoxic bottom waters of Mono Lake, California. *Geomicrobiol. J.* **2002**, *19* (1), 23-40.

23. Driehaus, W.; Seith, R.; Jekel, M., Oxidation of arsenate(III) with manganese oxides in water treatment. *Water Res.* **1995**, *29* (1), 297-305.

24. Bi, X.; Zeng, C.; Westerhoff, P., Adsorption of arsenic ions transforms surface reactivity of engineered cerium oxide nanoparticles. *Environ. Sci. Technol.* **2020**.

25. Speed, D.; Westerhoff, P.; Sierra-Alvarez, R.; Draper, R.; Pantano, P.; Aravamudhan, S.; Chen, K. L.; Hristovski, K.; Herckes, P.; Bi, X., Physical, chemical, and in vitro toxicological characterization of nanoparticles in chemical mechanical planarization suspensions used in the semiconductor industry: towards environmental health and safety assessments. *Environ. Sci. Nano* **2015**, *2* (3), 227-244.

26. Zantye, P. B.; Kumar, A.; Sikder, A., Chemical mechanical planarization for microelectronics applications. *Mater. Sci. Eng. Reports* **2004**, *45* (3), 89-220.

27. Torrance, K. W.; Keenan, H. E.; Hursthouse, A. S.; Stirling, D., Measurement of arsenic and gallium content of gallium arsenide semiconductor waste streams by ICP-MS. *J. Environ. Sci. Health A* **2010**, *45* (4), 471-475.

28. Guimard, D.; Morihara, R.; Bordel, D.; Tanabe, K.; Wakayama, Y.; Nishioka, M.; Arakawa, Y., Fabrication of InAs/GaAs quantum dot solar cells with enhanced photocurrent and without degradation of open circuit voltage. *Appl. Phys. Lett.* **2010**, *96* (20), 3507.

29. Torrance, K.; Keenan, H. E. In *Characterization of arsenic-rich waste slurries generated during gallium arsenide wafer lapping and polishing*, 2009 International Conference on Compound Semiconductor MANufacturing TECHnology, 2009.

30. Bi, X.; Westerhoff, P., Adsorption of iii/v ions (In(iii), Ga(iii) and As(v)) onto SiO₂, CeO₂ and Al₂O₃ nanoparticles used in the semiconductor industry. *Environ. Sci. Nano* **2016**, *3* (5), 1014-1026.

31. Zeng, C.; Nguyen, C.; Boitano, S.; Field, J. A.; Shadman, F.; Sierra-Alvarez, R. J. E. r., Cerium dioxide (CeO₂) nanoparticles decrease arsenite (As (III)) cytotoxicity to 16HBE14ohuman bronchial epithelial cells. *Environ. Res.* **2018**, *164*, 452-458.

1	
2	
3	32. Bhattacharva, S.: Saha, I.: Mukhopadhvav, A.: Chattopadhvav, D.: Chand, U., Role of
4	nanotechnology in water treatment and purification: notential applications and implications Int I
5	Cham Sci Tachnol 2013 3 (3) 50 64
6	22 Li D. Li O. Coo S. Chang, I.V. Exponetional ansamic adaptation nonformation of
7	33. LI, R.; LI, Q.; Gao, S.; Shang, J. K., Exceptional arsenic adsorption performance of
8	hydrous cerium oxide nanoparticles: Part A. Adsorption capacity and mechanism. Chem. Eng. J.
9	2012, <i>185</i> , 127-135.
10	34. Mishra, P. K.; Saxena, A.; Rawat, A. S.; Dixit, P. K.; Kumar, R.; Rai, P. K., Surfactant
11	- free one - not synthesis of low - density cerium oxide nanonarticles for adsorptive removal of
12	arrania anazian Empiren Duan Sustain Enorma 2019, 27 (1), 221, 221
13	arsenic species. Environ. Prog. Sustain. Energy 2018, 57 (1), 221-251.
14	35. Yu, L.; Ma, Y.; Ong, C. N.; Xie, J.; Liu, Y., Rapid adsorption removal of arsenate by
15	hydrous cerium oxide–graphene composite. RSC Adv. 2015, 5 (80), 64983-64990.
16	36. Yu, Y.; Zhang, C.; Yang, L.; Chen, J. P., Cerium oxide modified activated carbon as an
17	efficient and effective adsorbent for rapid uptake of arsenate and arsenite: Material development
18	and study of performance and mechanisms <i>Chem Eng. J.</i> 2017 , 315, 630-638
19	37 Lin D: Tian X: Wu E: Xing B Eate and transport of engineered panomaterials in the
20	structure of the second state of the second st
21	environment. J. Environ. Qual. 2010, 39 (6), 1890-1908.
22	38. Ali, I., New generation adsorbents for water treatment. <i>Chem. Rev.</i> 2012, <i>112</i> (10), 50/3-
23	5091.
24	39. Feng, Q.; Zhang, Z.; Ma, Y.; He, X.; Zhao, Y.; Chai, Z., Adsorption and desorption
25	characteristics of arsenic onto ceria nanoparticles. Nano. Res. lett. 2012, 7 (1), 1-8.
26	40 Liu X · Ray I R · Neil C W · Li O · Jun Y -S Enhanced Colloidal Stability of CeO2
27	Nanonarticles by Ferrous Ions: Adsorption Redox Reaction and Surface Precipitation
28	Environmental Science & Technology 2015 40(0) 5476 5492
29	Environmeniai Science & Technology 2015, 49 (9), 5470-5485.
30	41. Auffan, M. I.; Rose, J. r. m.; Wiesner, M. R.; Bottero, JY., Chemical stability of metallic
31	nanoparticles: a parameter controlling their potential cellular toxicity in vitro. <i>Environ. Poll.</i> 2009,
32	157 (4), 1127-1133.
33	42. Limbach, L. K.: Bereiter, R.: Muller, E.: Krebs, R.: Galli, R.: Stark, W. J., Removal of
34	Oxide Nanoparticles in a Model Wastewater Treatment Plant. Influence of Agglomeration and
35	Surfactants on Clearing Efficiency Environ Sci Tachnol 2008 12 (15) 5828-5833
36	A2 Day I. D. ; Wy Y. Mail C. W. ; Ing. H. Li Z. Ing. V. C. Daday shamistary of CaO
37	45. Kay, J. K., Wu, X., Nell, C. W., Jung, H., LI, Z., Jun, YS., Redox chemistry of CeO_2
38	nanoparticles in aquatic systems containing $Cr(vi)(aq)$ and Fe^{2+} ions. <i>Environ. Sci. Nano</i> 2019, 6
39	(7), 2269-2280.
40	44. Wu, X.; Neil, C. W.; Kim, D.; Jung, H.; Jun, YS., Co-effects of UV/H ₂ O ₂ and natural
41	organic matter on the surface chemistry of cerium oxide nanoparticles. <i>Environ. Sci. Nano</i> 2018,
42	5 (10) 2382-2393
43	A5 Barton I E · Auffan M · Bertrand M · Barakat M · Santaella C · Masion A ·
44	Porcohnack D: Olivi I: Dacha N: Wiegner M. D. Transformation of prioting and aitrate
45	buistinger, D., Olivi, L., Koche, N., Wieshei, N. K., Hanstormation of pristine and cliffate-
46	functionalized CeO_2 nanoparticles in a laboratory-scale activated sludge reactor. Environ. Sci.
4/	<i>Technol.</i> 2014, <i>48</i> (13), 7289-7296.
48	46. Barton, L. E.; Auffan, M.; Olivi, L.; Bottero, JY.; Wiesner, M. R., Heteroaggregation,
49	transformation and fate of CeO ₂ nanoparticles in wastewater treatment. <i>Environ. Pollut.</i> 2015. 203.
50	122-129
51	47 Dutré V : Vandecasteele C : Ondenakker S Ovidation of arsanic hearing fly ash as
52	Treatment before calidification I University Matter 1000 68 (2) 205 215
53	preureaument before solidification. J. Hazara. Mater. 1999, 08 (3), 205-215.
54	
55	
56	
5/	
50 50	24
27	

48. Yu, P.; Hayes, S. A.; O'Keefe, T. J.; O'Keefe, M. J.; Stoffer, J. O., The phase stability of cerium species in aqueous systems: II. The systems. Equilibrium considerations and pourbaix diagram calculations. *J. Electrochem. Soc.* **2005**, *153* (1), C74.

49. Dunnick, K. M.; Pillai, R.; Pisane, K. L.; Stefaniak, A. B.; Sabolsky, E. M.; Leonard, S. S., The Effect of Cerium Oxide Nanoparticle Valence State on Reactive Oxygen Species and Toxicity. *Biological Trace Element Research* **2015**, *166* (1), 96-107.

50. Hawkins, D. B. *Environmental path of arsenic in groundwater: Completion report*; University of Alaska, Institute of Water Resources: 1976.

51. Hildum, B. Arsenic speciation and groundwater chemistry at a landfill site: a case study of SHepley's Hill Landfill. Boston College, 2013.

52. NORMAN, D. I., Arsenic geochemistry and remediation using natural materials. In *Water—Pollution*, World Scientific: 2001; pp 68-87.

53. Sharp, E. L.; Parsons, S. A.; Jefferson, B., Seasonal variations in natural organic matter and its impact on coagulation in water treatment. *Sci. Total Environ.* **2006**, *363* (1–3), 183-194.

54. Tsao, T. M.; Chen, Y. M.; Wang, M. K., Origin, separation and identification of environmental nanoparticles: a review. *J. Environ. Monitor.* **2011**, *13* (5), 1156-1163.

55. Baalousha, M.; Ju - Nam, Y.; Cole, P. A.; Gaiser, B.; Fernandes, T. F.; Hriljac, J. A.; Jepson, M. A.; Stone, V.; Tyler, C. R.; Lead, J. R., Characterization of cerium oxide nanoparticles—part 1: size measurements. *Environ. Toxicol. Chem.* **2012**, *31* (5), 983-993.

56. Baalousha, M.; Le Coustumer, P.; Jones, I.; Lead, J., Characterisation of structural and surface speciation of representative commercially available cerium oxide nanoparticles. *Environ. Chem.* **2010**, *7* (4), 377-385.

57. Rogers, N. J.; Franklin, N. M.; Apte, S. C.; Batley, G. E.; Angel, B. M.; Lead, J. R.; Baalousha, M., Physico-chemical behaviour and algal toxicity of nanoparticulate CeO_2 in freshwater. *Environ. Chem.* **2010**, 7 (1), 50-60.

58. Corkhill, C. L.; Bailey, D. J.; Tocino, F. Y.; Stennett, M. C.; Miller, J. A.; Provis, J. L.; Travis, K. P.; Hyatt, N. C., Role of microstructure and surface defects on the dissolution kinetics of CeO₂, a UO₂ fuel analogue. *ACS Appl. Mater. Inter.* **2016**, *8* (16), 10562-10571.

59. Mehmood, R.; Mofarah, S. S.; Chen, W.-F.; Koshy, P.; Sorrell, C. C., Surface, Subsurface, and Bulk Oxygen Vacancies Quantified by Decoupling and Deconvolution of the Defect Structure of Redox-Active Nanoceria. *Inorg. Chem.* **2019**, *58* (9), 6016-6027.

60. Yu, J.; Wang, Z.; Wang, J.; Zhong, W.; Ju, M.; Cai, R.; Qiu, C.; Long, X.; Yang, S., The Role of Ceria in a Hybrid Catalyst toward Alkaline Water Oxidation. *ChemSusChem* **2020**, *13* (19), 5273-5279.

61. Wilkie, J. A.; Hering, J. G., Rapid Oxidation of Geothermal Arsenic(III) in Streamwaters of the Eastern Sierra Nevada. *Environ. Sci. Technol.* **1998**, *32* (5), 657-662.

62. Park, P. W.; Ledford, J. S., Effect of crystallinity on the photoreduction of cerium oxide: A study of CeO₂ and Ce/Al₂O₃ catalysts. *Langmuir* **1996**, *12* (7), 1794-1799.

63. Schierbaum, K.-D., Ordered ultra-thin cerium oxide overlayers on Pt (111) single crystal surfaces studied by LEED and XPS. *Surf. Sci.* **1998**, *399* (1), 29-38.

64. Soma, M.; Tanaka, A.; Seyama, H.; Satake, K., Characterization of arsenic in lake sediments by X-ray photoelectron spectroscopy. *Geochim. Cosmochim. Acta* **1994**, *58* (12), 2743-2745.

65. Tian, N.; Tian, X.; Liu, X.; Zhou, Z.; Yang, C.; Ma, L.; Tian, C.; Li, Y.; Wang, Y., Facile synthesis of hierarchical dendrite-like structure iron layered double hydroxide nanohybrids for effective arsenic removal. *Chem. Comm.* **2016**, *52* (80), 11955-11958.

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66. Zhang, S.; Niu, H.; Cai, Y.; Zhao, X.; Shi, Y., Arsenite and arsenate adsorption on coprecipitated bimetal oxide magnetic nanomaterials: MnFe₂O₄ and CoFe₂O₄. *Chem. Eng. J.* **2010**, *158* (3), 599-607.

67. Zhang, Y.; Yang, M.; Dou, X.-M.; He, H.; Wang, D.-S., Arsenate adsorption on an Fe–Ce bimetal oxide adsorbent: role of surface properties. *Environ. Sci. Technol.* **2005**, *39* (18), 7246-7253.

68. Rivera-Reyna, N.; Hinojosa-Reyes, L.; Guzman-Mar, J. L.; Cai, Y.; O'Shea, K.; Hernandez-Ramirez, A., Photocatalytical removal of inorganic and organic arsenic species from aqueous solution using zinc oxide semiconductor. *Photochem. Photobiol. Sci.* **2013**, *12* (4), 653-659.

69. Boehm, H., Acidic and basic properties of hydroxylated metal oxide surfaces. *Disc. Faraday Soc.* **1971**, *52*, 264-275.

70. Collin, B.; Oostveen, E.; Tsyusko, O. V.; Unrine, J. M., Influence of Natural Organic Matter and Surface Charge on the Toxicity and Bioaccumulation of Functionalized Ceria Nanoparticles in Caenorhabditis elegans. *Environ. Sci. Technol.* **2014**, *48* (2), 1280-1289.

List of Figures

- **Figure 1.** (A) XPS spectra for unreacted CeO₂ nanoparticles (NPs) and (B) Measurement of the isoelectric point pH for ceria nanoparticles in 10 mM sodium nitrate.
- Figure 2. (A) Sedimentation of CeO₂ NPs in 10 mM NaCl at pH 5 for control, 10⁻⁴ M, 10⁻⁵ M, and 10⁻⁶ M As³⁺ systems as a function of time. Absorbances of CeO₂ NPs were measured at wavelength of 305 nm, where the highest absorbance by CeO₂ NP was obtained.⁴⁰ (B) Hydrodynamic diameter and zeta potential measurements for CeO₂ NP colloids in the control, 10⁻⁴ M, 10⁻⁵ M, and 10⁻⁶ M As³⁺ systems, measured after 2 hours. Error bars are calculated from triplicate measurements.
- Figure 3. Representative TEM images of dried CeO_2 NP aggregates taken after 2 hours of reaction for the control, 10^{-4} M As³⁺, 10^{-5} M As³⁺, and 10^{-6} M As³⁺ systems.
- Figure 4. (A) Dissolved cerium concentrations for the control, 10⁻⁴ M, 10⁻⁵ M, and 10⁻⁶ M As³⁺ systems over the 24 hours reaction period measured using ICP-MS. Error bars are calculated from triplicate measurements. XPS spectra of NPs' surfaces for (B) cerium (Ce 3d), (C) adsorbed arsenic (As 3d), and (D) oxygen (O 1s) in the control, 10⁻⁴ M, 10⁻⁵ M, and 10⁻⁶ M As³⁺ systems after 24 hour reaction. (E) Area percentages (%) of each oxygen bond in four systems. (F) FTIR spectra for control CeO₂ NP samples and CeO₂ NP samples reacted with arsenite.
- Figure 5. Proposed mechanisms of As^{3+} interactions with CeO₂ NPs. Increasing As^{3+} concentrations lead to a more neutralized surface, and thus more aggregation and settling. As a result, the most dissolution occurs in the median concentration (10⁻⁵ M As^{3+}), where increased redox reactions coincide with maintained colloidal stability,

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3 4	leading to increases in reactive surface area for dissolution relative to the 10 ⁻⁴ M
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6	As ³⁺ system.
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Figure 1



В.

System	Hydrodynamic diameter (nm)	Zeta potential (mV)
Control	588.0 ± 65.1	35.5 ± 2.1
10 ⁻⁴ M As ³⁺	2,240 ± 270	2.8 ± 1.3
10 ⁻⁵ M As ³⁺	254.0 ± 10.3	34.1 ± 2.1
10 ⁻⁶ M As ³⁺	225.1 ± 9.1	36.3 ± 2.3

Figure 2







Figure 4



Figure 5

Graphical Abstract



Exposing ceria nanoparticles to high arsenite concentrations will trigger aggregation and settling, while lower concentrations promote dissolution through redox interactions.