



**Stable High Current Density Operation of
La_{0.6}Sr_{0.4}Co_{0.2}Fe_{0.8}O_{3-δ} Oxygen Electrodes**

Journal:	<i>Journal of Materials Chemistry A</i>
Manuscript ID	TA-ART-04-2019-004020.R1
Article Type:	Paper
Date Submitted by the Author:	07-May-2019
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1 **Stable High Current Density Operation of $\text{La}_{0.6}\text{Sr}_{0.4}\text{Co}_{0.2}\text{Fe}_{0.8}\text{O}_{3-\delta}$ Oxygen Electrodes**

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10 **Abstract**

11 Solid oxide cells operated reversibly between fuel cell and electrolysis modes are
12 promising for energy storage with extremely high capacity. $\text{La}_{0.6}\text{Sr}_{0.4}\text{Co}_{0.2}\text{Fe}_{0.8}\text{O}_{3-\delta}$ (LSCF) has
13 become the dominant oxygen electrode material in electrolysis and reversible operation.
14 However, LSCF has been widely reported to degrade due to Sr surface segregation. The present
15 understanding is that the segregation rate and hence the degradation rate increases with
16 increasing temperature and current density. Here we present a study of LSCF electrode
17 performance and stability carried out with a series of extended life tests (1000 hours) over a
18 range of temperatures and reversing current densities. Although the results at lower temperatures
19 (650 – 700 °C) show the expected increase in segregation-induced degradation with increasing
20 current density, at higher temperature (750 °C) stability is improved and the electrodes become
21 fully stable at the highest current density of 1.5 A cm⁻², maintaining a stable polarization
22 resistance of 0.08 Ω·cm². This unexpected result is explained by the increased electrochemical

23 activity of LSCF at the higher temperature and a very rapid development of a stable surface
24 segregated Sr layer.

25 **Main Text**

26 The rapid increase in utilization of intermittent renewable energy sources, as needed to
27 mitigate global warming,¹ will give rise to an increasing need for electricity storage.^{2,3} The time
28 frame for storage is over days or longer, requiring clean technologies with large energy storage
29 capacities. Solid oxide cells (SOCs) operated as electrolyzers provide a promising and scalable
30 method for efficiently converting electricity into renewable fuels for direct utilization, e.g., for
31 transportation. The fuels can also be stored and converted back to electricity by reversing SOC
32 operation to fuel cell mode, completing an electricity storage cycle with the requisite very high
33 energy storage capacity along with relatively low cost and high efficiency.⁴⁻⁶ Although SOCs
34 have been extensively developed for fuel cell applications and proven to provide good stability,
35 much higher degradation rates are often observed during electrolysis and reversible operation,
36 particularly at higher current densities.⁷⁻⁹ Voltage degradation rates (at constant current) are
37 often well above 1 %/kilohour, much higher than that needed for the device to operate effectively
38 over economically-viable operational lifetimes of ≥ 5 years.^{4,10}

39 Early studies of solid oxide electrolysis utilized cells with the $(\text{La}_{0.8}\text{Sr}_{0.2})_{0.98}\text{MnO}_3$ (LSM)
40 -YSZ oxygen electrode; however, these electrodes were shown to fail at relatively large current
41 densities ($\geq 0.5 \text{ A} \cdot \text{cm}^{-2}$) via oxygen bubble formation, crack formation, and delamination at or
42 near the electrode-electrolyte interface.¹¹⁻¹⁵ More recent electrolysis studies have focused on
43 SOCs with mixed ionic and electronic conducting (MIEC) oxygen electrodes such as
44 $\text{La}_{0.6}\text{Sr}_{0.4}\text{Co}_{0.2}\text{Fe}_{0.8}\text{O}_{3-\delta}$ (LSCF) that yield better performance and electrolysis stability.^{16,17} While
45 LSCF and other similar ABO_3 perovskite MIEC electrodes typically do not degrade by the

46 aforementioned mechanisms, they can degrade via a different mechanism—surface segregation of
47 an A-site cation (typically Sr) that blocks electrochemically active sites for oxygen adsorption
48 and electron transfer.^{9,18–21} The rate of Sr segregation generally increases with increasing
49 temperature, and the current/overpotential during cell operation can also impact segregation,
50 although there are sometimes conflicting results on the effects of anodic versus cathodic
51 polarization.^{21–29}

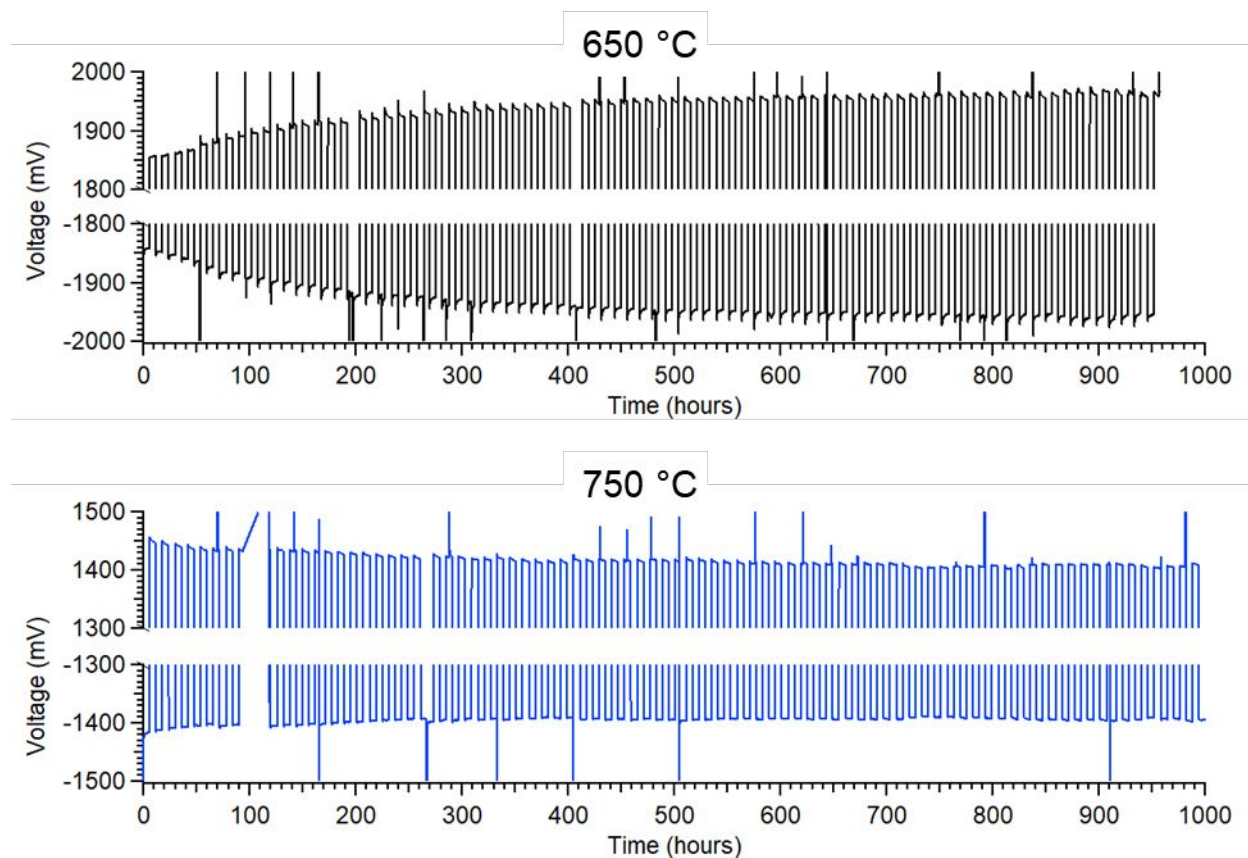
52 In contrast to the above mentioned findings, that typically show substantial degradation,
53 many of which were obtained with model thin film electrodes, porous LSCF electrodes used in
54 long-term SOC lab-scale and stack tests have generally shown little electrode degradation.^{16,30–34}
55 This disconnect may be related to the different operating conditions (temperature, current
56 density, and overpotential) or electrode geometries (thin film versus porous). These conflicting
57 results suggest that a comprehensive study, focusing on porous electrodes over a range of
58 operating temperatures and current densities, is needed to understand LSCF degradation and find
59 operating conditions that yield stable operation.

60 Here we describe life test results detailing the effects of reversing current density (j) and
61 temperature on the electrochemical stability of porous LSCF electrodes. The study directly
62 correlates the evolution of electrochemical performance, measured using impedance
63 spectroscopy, with quantitative 3D tomographic microstructure observations and Sr segregation
64 measurements. A novel surface cleaning experiment is used to prove the direct correlation
65 between Sr segregation and electrochemical performance degradation. A key finding is the
66 unexpected observation of stable operation at relatively high current density ($j = 1.5 \text{ A} \cdot \text{cm}^{-2}$) and
67 temperature (750 °C). The results show how LSCF electrodes can be operated reversibly at

68 desirably high current density without significant degradation; the results may also be applicable
69 to electrolysis operation, since the degradation mechanisms are typically similar.^{11,35,36}

70 Electrochemical Characterization

71 Figure 1 shows voltage versus time during life tests carried out at 650 and 750 °C, both
72 with $j = 1.5 \text{ A} \cdot \text{cm}^{-2}$. The cycle used in these experiments, with 6 hours in electrolysis mode and 6
73 hours in fuel cell mode, simulates the conditions at the SOC oxygen electrode during a reversible
74 energy storage application. As expected, the cell voltage is higher at the lower temperature.
75 During the 650 °C test, the voltage increases rapidly initially but then more slowly later in the
76 life test. The voltage evolution over time trends differently in the 750 °C test, with an initial
77 decrease early in the test followed by stable operation.

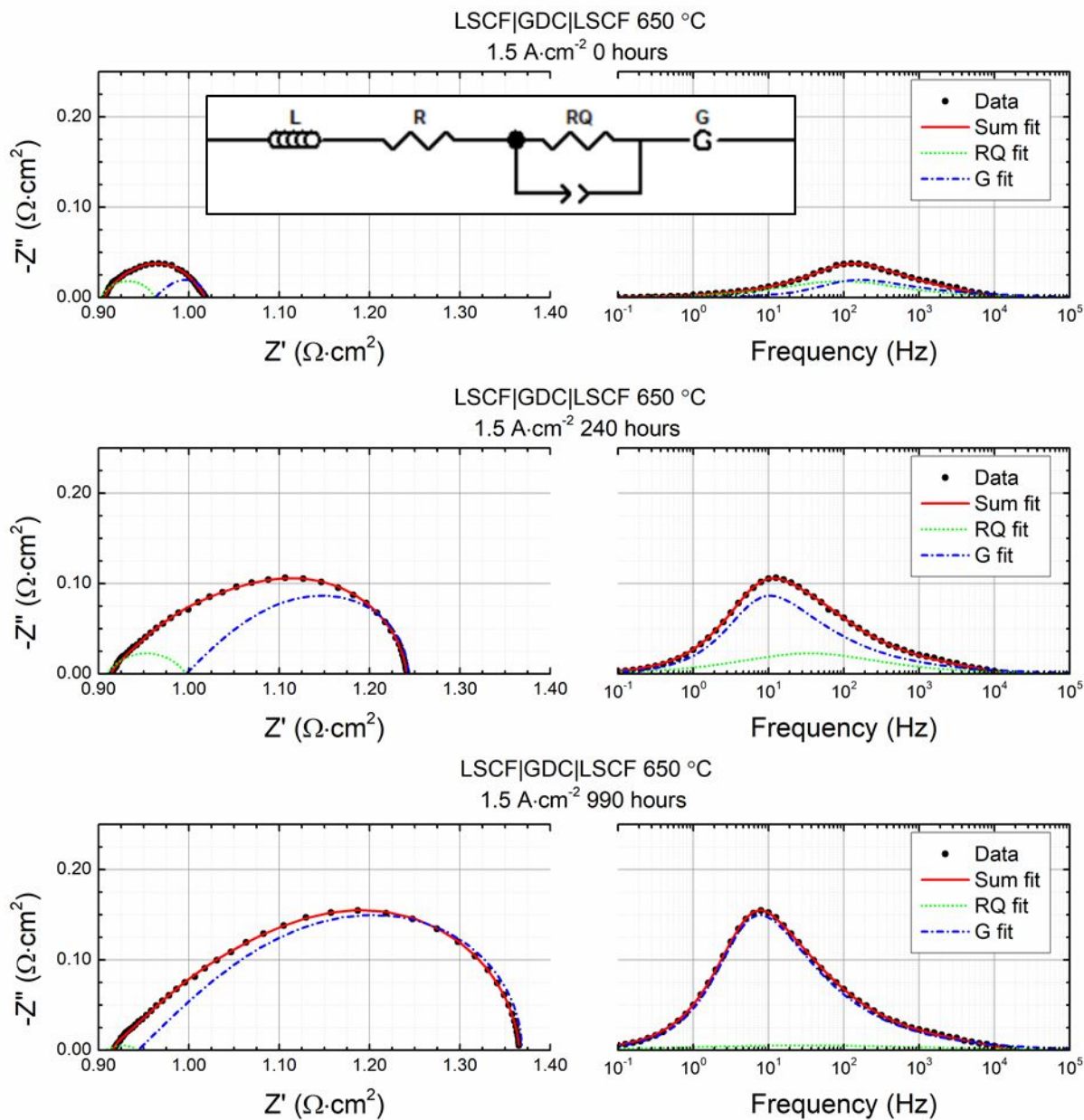


78

79 **Fig. 1 | Voltage data for LSCF |GDC|LSCF life tests.** Cells are operated for ~ 1000 hours at j
 80 $= 1.5 \text{ A} \cdot \text{cm}^{-2}$ at $650 \text{ }^\circ\text{C}$ and $750 \text{ }^\circ\text{C}$

81 Figure 2 shows typical impedance spectra taken at 0, 240, and 990 hours during the life
 82 test at $650 \text{ }^\circ\text{C}$ with $j = 1.5 \text{ A} \cdot \text{cm}^{-2}$. The spectra are fit with an L - R - RQ - G equivalent circuit that is
 83 widely used to fit data for mixed ionic and electronic conducting electrodes such as LSCF.^{37–39}
 84 The RQ element is attributed to charge transfer resistance at the electrode-electrolyte interface
 85 whereas the Gerischer element (G) is attributed to co-limiting oxygen surface exchange and
 86 diffusion in LSCF, and the sum of the two is the total polarization resistance, R_p .^{19,29,40–43} The L
 87 element accounts for measurement circuit inductance, and R corresponds to the ohmic resistance,
 88 or effectively the electrolyte resistance. The high frequency intercept shifts very little, indicating
 89 no significant change in R . On the other hand, the increase in the magnitude of the impedance

90 response demonstrates that there is substantial electrode degradation. From the evolution of the
91 impedance spectra, the increase in the cell resistance is primarily associated with the low-
92 frequency Gerischer response. Note that the impedance spectra taken at 750 °C (Supplementary
93 Fig. 1) have the same basic form as those at 650 °C and are fit well using the same equivalent
94 circuit; however, the resistance values are smaller and the spectra change little during the life
95 test.

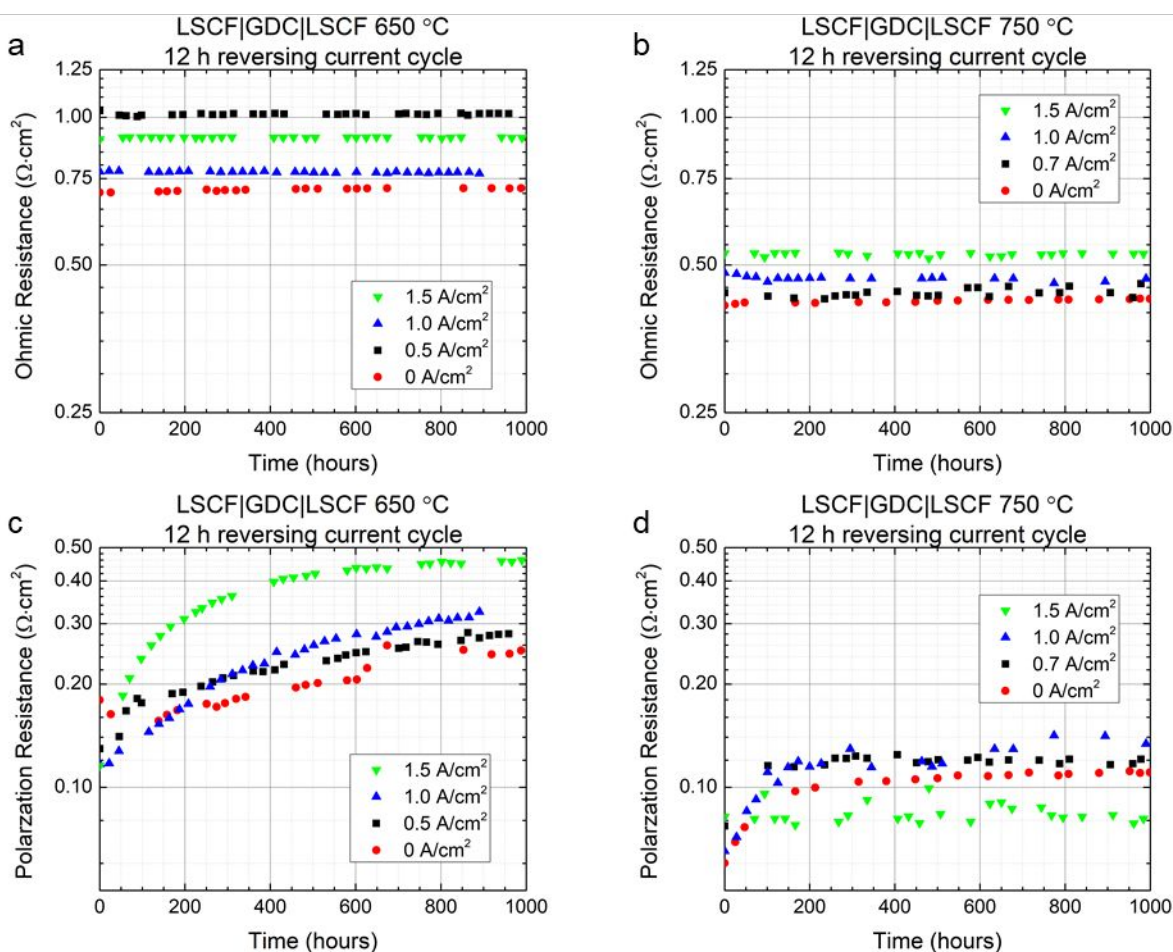


96
97 **Fig. 2 | Evolution of Nyquist and Bode plots for LSCF|GDC|LSCF cells.** Impedance spectra
98 are shown at 0, 240, and 990 hours during operation at 650 °C and $j = 1.5 \text{ A} \cdot \text{cm}^{-2}$. An inset of the
99 L-R-RQ-G equivalent circuit model used for fitting is shown.

100 The equivalent circuit fits are used to obtain R and R_P values that are plotted in Figure 3.
101 At both 650 °C (Figure 3a) and 750 °C (Figure 3b), R is stable at all j . Several cells exhibit slight
102 improvements in R , but the magnitudes of these changes are relatively insignificant, ~ 0.01

103 $\Omega \cdot \text{cm}^2$, similar to prior results for LSCF-based cells.^{9,19} The cell-to-cell variations in ohmic
 104 resistance result from differing electrolyte thicknesses.

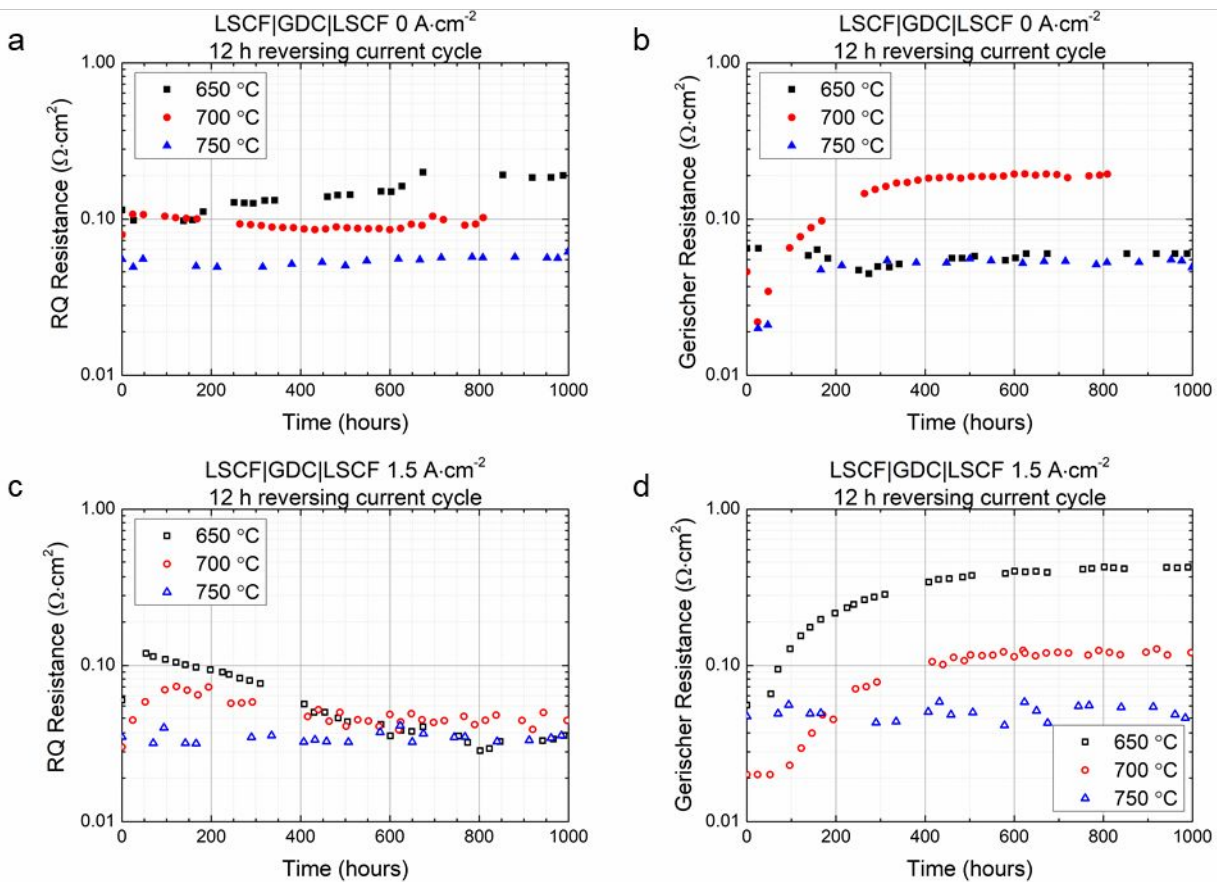
105 At 650 °C (Figure 3c), the degradation rate of R_p increases with increasing j up to 1.0
 106 $\text{A} \cdot \text{cm}^{-2}$. At $j = 1.5 \text{ A} \cdot \text{cm}^{-2}$, R_p degrades rapidly at the start, but the degradation rate slows
 107 throughout the 1000 hour test. These results are similar to those reported previously for similar
 108 LSCF electrodes tested at 700 °C.⁹ The significant R_p increases at both 650 and 700 °C can be
 109 explained by Sr surface segregation.^{9,19,44,45} At 750 °C (Figure 3d) and $j = 0, 0.7, \text{ and } 1.0 \text{ A} \cdot \text{cm}^{-2}$,
 110 R_p again increases rapidly over the first ~ 150 hours, and increases very slowly thereafter.
 111 However, when $j = 1.5 \text{ A} \cdot \text{cm}^{-2}$, R_p becomes remarkably stable throughout the life test.



112

113 **Fig. 3 | Ohmic and polarization resistances for LSCF|GDC|LSCF cells during ~ 1000 hour**
114 **life tests.** Current densities range from $j = 0$ to $1.5 \text{ A}\cdot\text{cm}^{-2}$ with $650 \text{ }^\circ\text{C}$ plotted on the left (**a,c**),
115 $750 \text{ }^\circ\text{C}$ (**b,d**) on the right.

116 Figure 4 shows the effect of temperature on R_p separated into its two components: the
117 interfacial RQ resistance (R_I) and the Gerischer resistance (R_G). Note that the $700 \text{ }^\circ\text{C}$ data is from
118 previous work and refitted using ravidav software to deconvolute the contributions from the RQ
119 and Gerischer resistances.^{9,46} R_I remains stable or decreases slightly with time in almost all cases,
120 whereas R_G is either stable or saturates after an initial increase.¹⁹ At $j = 0$ (Figure 4b), R_G remains
121 stable at $650 \text{ }^\circ\text{C}$, but increases with time at the higher temperatures. At $j = 1.5 \text{ A}\cdot\text{cm}^{-2}$ (Figure
122 4d), R_G remains constant at $750 \text{ }^\circ\text{C}$, but increases substantially at lower temperatures. These
123 opposing temperature dependences at different j are explained below based on structural and
124 chemical characterization.

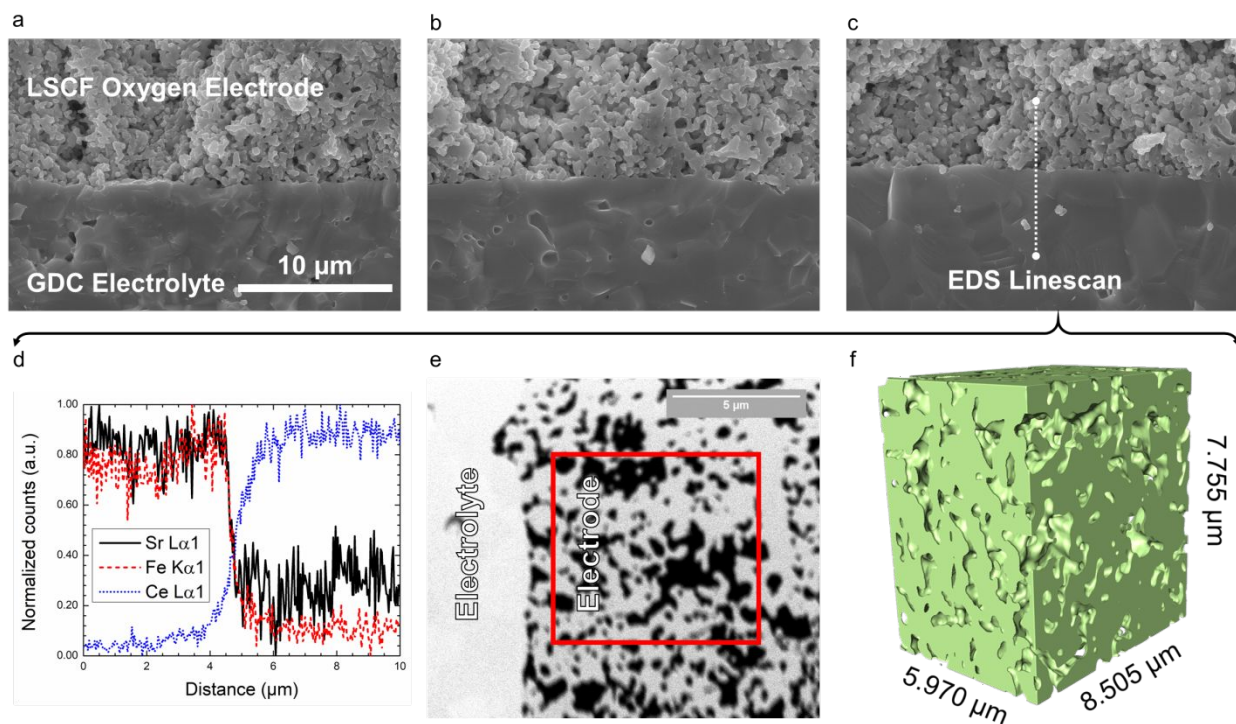


125
 126 **Fig. 4 | RQ and Gerischer resistances for LSCF|GDC|LSCF cells. a,c, RQ resistance and b,d,**
 127 Gerischer resistance during life tests at various temperatures in ambient air. The top row (a,b)
 128 shows life tests with no current ($j = 0 \text{ A}\cdot\text{cm}^{-2}$) and the bottom row (c,d) shows reversing current
 129 life tests with $j = 1.5 \text{ A}\cdot\text{cm}^{-2}$.

130 Microstructural Characterization

131 Figure 5 shows scanning electron microscope (SEM) images of the region near the
 132 electrode-electrolyte interface of the untested control cell (Figure 5a) compared with cells after
 133 life testing at $j = 1.5 \text{ A}\cdot\text{cm}^{-2}$ at 650 °C (Figure 5b) and at 750 °C (Figure 5c). There is no
 134 discernable difference between the microstructures; that is, life testing at high current density
 135 yielded no significant microstructures changes either for the highest degradation case (650 °C) or

136 the stable operation case (750 °C). Figure 5d shows an energy dispersive X-ray spectroscopy
 137 (EDS) linescan of the electrode-electrolyte interface for the 750 °C and $j = 1.5 \text{ A} \cdot \text{cm}^{-2}$ cell.
 138 Although there is apparent interfacial broadening of $\sim 1 \mu\text{m}$, a similar width is observed in all
 139 cells (not shown here) that can be attributed to the limited spatial resolution of the EDS
 140 measurement.⁴¹ Thus, no elemental migration is detected at the spatial resolution of SEM-EDS.



141
 142 **Fig. 5 | Microstructural characterization of LSCF electrodes and GDC electrolytes. a-c,**
 143 SEM images of the electrode-electrolyte interface for samples: (a) untested control, (b) 650 °C
 144 with $j = 1.5 \text{ A} \cdot \text{cm}^{-2}$ for 990 hours, (c) 750 °C with $j = 1.5 \text{ A} \cdot \text{cm}^{-2}$ for 1013 hours. d, EDS result
 145 from c. e, FIB-SEM 2-D cross-section used to reconstruct f, a 3-D microstructure of c.

146 FIB-SEM is used to image an LSCF electrode after 1013 hours at 750 °C and $j = 1.5$
 147 $\text{A} \cdot \text{cm}^{-2}$. Figure 5f shows a typical FIB-SEM two-dimensional (2-D) cross-section from a series
 148 of images used to obtain the three-dimensional (3-D) tomographic image shown in Figure 5f.
 149 Only LSCF and pore phases are observed, with no evidence of Sr-rich clusters in the LSCF

150 electrode in Figures 5, which are sometimes observed after LSCF life testing at higher
 151 temperatures.⁴⁵ These results can be compared directly with microstructural data from identically
 152 prepared cells reported previously.^{9,45} Table 1 compares porosity, surface area, and tortuosity
 153 values obtained from the 3-D data sets for the present cell and prior cells, including a control cell
 154 and cells tested for ~ 1000 hours at 700 °C with different current densities. The porosities fall in
 155 the range between 35 to 40% and the tortuosities are in the expected range for such porosity
 156 values. The variations between these values are small enough to be explained by cell-to-cell
 157 differences and 3-D tomography measurement errors.^{47,48} The specific surface area reductions
 158 after the $j = 1.5 \text{ A}\cdot\text{cm}^{-2}$ life tests are too small to draw a conclusion based on these results alone.
 159 However, the results are consistent with a prior report showing coarsening at 700 °C and $j = 1.5$
 160 $\text{A}\cdot\text{cm}^{-2}$.⁹ In any case, the observed amount of coarsening is not sufficient to significantly impact
 161 R_p .^{45,47}

162 Table 1 – **FIB-SEM results for LSCF|GDC|LSCF cells.** Porosity, tortuosity, and specific
 163 surface areas calculated from the 3-D reconstruction and compared with prior literature results.

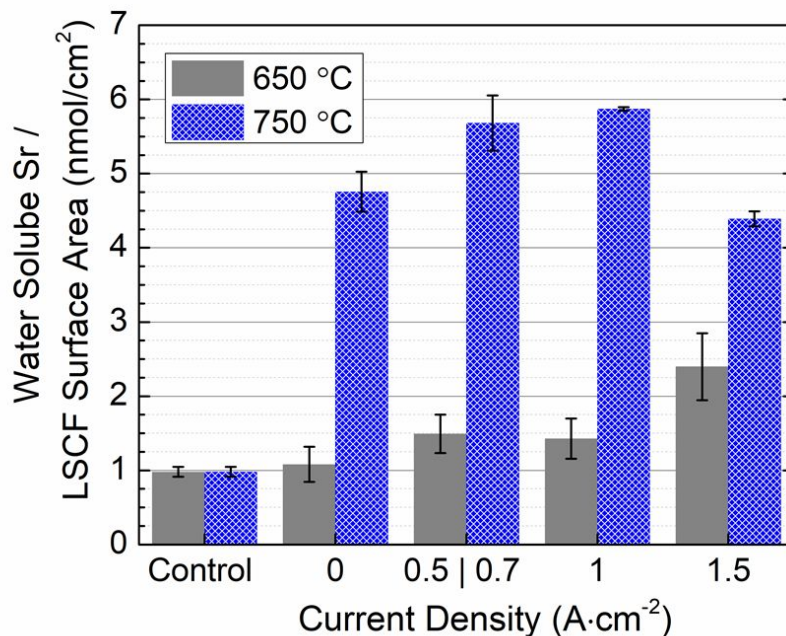
	Control ⁽⁴⁵⁾	700 °C 0 A·cm⁻² ⁽⁹⁾	700 °C 0.7 A·cm⁻² ⁽⁹⁾	700 °C 1.5 A·cm⁻² ⁽⁹⁾	750°C 1.5 A·cm⁻²
Porosity (%)	33.1%	39.69%	39.59%	34.03%	35.33%
LSCF Tortuosity	1.10	1.12	1.12	1.10	1.35
Specific Surface Area (μm⁻¹)	4.95	5.62	5.96	4.47	4.41

164

165 Sr Segregation

166 Figure 6 presents the amounts of excess Sr, normalized to the FIB-SEM-measured LSCF
 167 surface areas, measured after various life tests compared with an untested control electrode. The
 168 Sr amount does not increase after thermal annealing at 650 °C for 990 hours. However, Sr

169 coverages generally increase with increasing j at 650 °C, in agreement with prior reports that
170 current accelerates Sr out-diffusion.^{9,19,45} At $j = 1.5 \text{ A}\cdot\text{cm}^{-2}$ the segregation is fast enough that R_p
171 has increased substantially and then nearly stabilized by the end of the 650 °C life test.
172 Previously-reported results for similar LSCF electrodes at 700 °C show that the surface Sr
173 amount also increases with increasing j , but the amounts are larger than at 650 °C because of the
174 faster Sr segregation at the higher temperature.⁹ At 750 °C, there is a substantial increase in
175 surface Sr after annealing for 1000 hours; as expected, Sr out-diffusion is faster at the higher
176 temperature. Increasing to j at 750 °C further increases the amount of surface Sr, except at $j = 1.5$
177 $\text{A}\cdot\text{cm}^{-2}$ where the surface Sr declines. However, this slight decrease in segregation does not
178 appear to be significant enough to explain the stable performance. The correlation between Sr
179 segregation and the electrochemical performance is discussed further below.

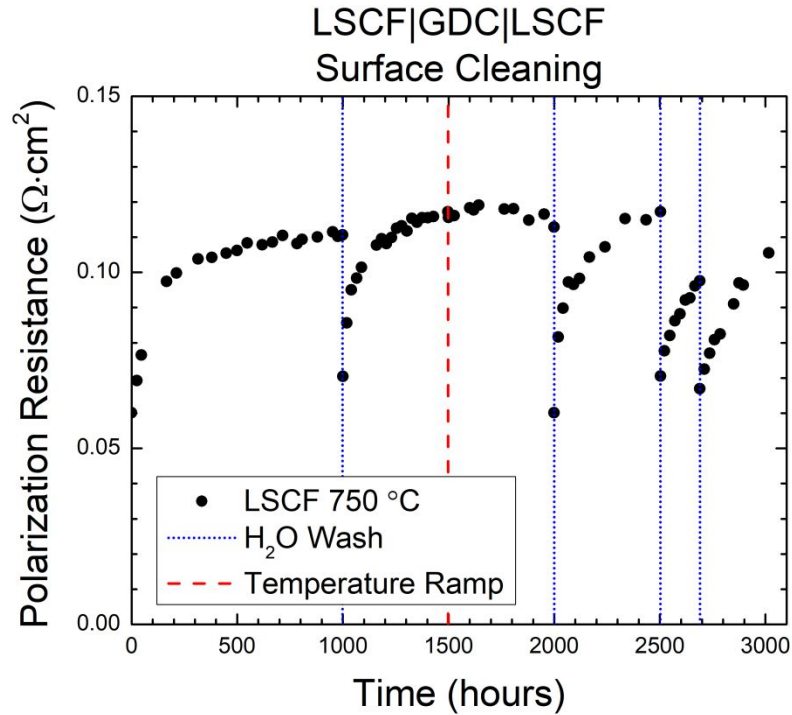


180

181 **Fig. 6 | ICP-OES analysis of water soluble Sr in LSCF electrodes.** The amount of segregated
182 Sr species is normalized to the LSCF electrode surface area at 650 and 750 °C after testing for ~
183 1000 hours with $j = 0, 0.5, 0.7, 1.0, \text{ or } 1.5 \text{ A}\cdot\text{cm}^{-2}$.

184 Surface Cleaning

185 Figure 7 shows the resistance versus time for a cell that was first maintained without
186 current for 999 hours at 750 °C, yielding a substantial increase in R_p over the first ~ 500 hours, in
187 accord with the above results. The cell was then cooled to ambient temperature and rinsed in
188 ultrapure H₂O. While this method is applicable to lab-scale symmetric electrodes that can be
189 easily submersed in H₂O, there would likely be engineering challenges to introduce this cleaning
190 step in a fuel cell stack. After drying and reheating the cell to 750 °C, the life test is resumed –
191 the R_p value has reset to its initial un-degraded value, but then increases similar to the first ~ 500
192 hours of the test. Four separate cleaning steps are carried out using this procedure. After each
193 wash, the R_p returns to its initial low value followed by degradation. The reset in R_p is also well
194 represented as a reset of the Nyquist and Bode plots shown in Supplementary Fig. 2, where each
195 wash effectively reverses the degradation in the Gerischer element. To ensure that the thermal
196 cycling carried out as part of these measurements did not affect the results, the cell was removed
197 at 1497 hours and subsequently ramped back to temperature without a washing step and no
198 change in cell performance is seen. Given that the ultrapure H₂O wash is known to remove
199 excess Sr, but not other cations,^{19,45} these results clearly links the increases in R_p with Sr
200 segregation. That is, the electrochemical degradation in Figures 1-4 results from Sr segregation.



201

202 **Fig. 7 | Polarization resistance over time for LSCF|GDC|LSCF cells using H₂O to remove**203 **surface segregated Sr.** Cells are annealed at 750 °C with $j = 0 \text{ A}\cdot\text{cm}^{-2}$ and washed with

204 ultrapure water after 999, 2000, 2503, and 2690 hours.

205 **Discussion**

206 The results above show no evidence of interface microstructural degradation such as

207 fracture, nor any increase ohmic resistance during the life tests. Such degradation, which has

208 been widely observed in LSM-electrode SOCs operated in electrolysis and reversible

209 modes,^{11,49,50} is attributed to an oxygen pressure buildup at the interface associated with the210 electrode overpotential η .^{51,52} These LSCF results agree with prior reports for LSCF-electrode211 cells reversibly-operated at 700 C and 1.0 A cm^{-2} , where the lack of interfacial degradation was212 explained by relatively low η values resulting from the low R_P values of LSCF electrodes.⁹ The

213 present results extend this observation to lower temperature and higher current density. They also

214 more strongly confirm the conclusion from that study,⁹ that electrochemical degradation is

215 associated with a Sr-enriched surface layer that impedes the oxygen surface exchange reaction,
216 appearing in the EIS data as an increased Gerischer resistance.^{9,44,45} This conclusion is consistent
217 with prior surface spectroscopy studies on model $\text{La}_{0.6}\text{Sr}_{0.4}\text{CoO}_{3-\delta}$ and $\text{La}_{0.6}\text{Sr}_{0.4}\text{Co}_{0.2}\text{Fe}_{0.8}\text{O}_{3-\delta}$
218 thin film electrodes that show the development of a Sr-enriched perovskite surface at lower
219 temperatures (400 to 650 °C). At higher temperatures, the Sr layer thickness covering the LSCF
220 surface saturates while larger Sr islands nucleate.^{53–57}

221 The above arguments, by themselves, do not explain the results in Figures 3 and 4,
222 particularly the stable electrode operation at 750 C and 1.5 A cm⁻². These figures can be
223 explained by noting (1) that increasing j increases the rate of surface segregation and (2) that the
224 LSCF electrode exists in different states with different R_G depending on its history.^{53–57} A
225 cleaner electrode surface has a lower R_G , whereas the Sr segregated surface has a higher R_G . For
226 example, in Figure 4b ($j = 0 \text{ A} \cdot \text{cm}^{-2}$), the initial R_G values are lower at higher temperature, as
227 expected for activated electrode processes, because the LSCF surfaces are all in the clean state.
228 Later in the life test, the 650 °C surface has clearly remained in the clean low R_G state due to
229 slow Sr segregation, whereas at 700 and 750 °C R_G has increased due to accelerated Sr
230 segregation.¹⁹ This yields an unusual case where R_G at 650 °C is similar to that at 750 °C. The
231 situation is reversed in Figure 4d ($j = 1.5 \text{ A} \cdot \text{cm}^{-2}$) because the current accelerates segregation. At
232 750 °C and 1.5 A · cm⁻², segregation is apparently so fast that a saturation Sr coverage has already
233 been reached by the initial EIS measurement. Thus, the initial R_G is relatively high compared to
234 the initial values at 650 and 700 °C where the surfaces are still clean. Later in the test, current-
235 enhanced Sr segregation also increases R_G at 650 and 700 °C, such that the R_G values follow the
236 temperature dependence expected for Sr-covered LSCF.

237 The present results on reversible operation do not provide direct information on stability
238 during electrolysis or fuel cell operation. However, the present trend of improved stability at
239 higher temperature seems consistent with prior electrolysis results – in higher temperature (> 750
240 $^{\circ}\text{C}$) electrolysis tests with up to $j = 1 \text{ A}\cdot\text{cm}^{-2}$ where the LSCF electrode appears to be reasonably
241 stable,^{16,30–34} whereas in lower temperature ($\leq 700 \text{ }^{\circ}\text{C}$) electrolysis with $j = 0$ to $1.5 \text{ A}\cdot\text{cm}^{-2}$,
242 where cation segregation causes serious degradation.^{9,37,43,58,59} The present results suggest that at
243 higher temperatures, Sr segregation occurs relatively quickly, and even with surface Sr present
244 R_p values are low enough for good cell performance. In this case, the segregation-induced
245 resistance increases may be viewed as an initial break-in process rather than degradation. At
246 lower temperatures, Sr segregation is slower with relatively long times to reach saturation
247 coverage,^{19,45} causing gradual R_p increases. The saturation R_p values for Sr-covered LSCF may
248 be too high to achieve desired power densities at these lower operating temperatures. It is unclear
249 if a specific part of the reversing current cycle – fuel cell or electrolysis mode – is responsible for
250 the observed acceleration of Sr segregation and associated degradation in LSCF electrodes.^{9,11} A
251 number of studies have shown that anodic polarization of ABO_3 oxygen electrodes during
252 electrolysis operation exacerbates segregation by promoting the diffusion of cations towards the
253 surface,^{21–23,29} while a cathodic bias during fuel cell operation enhances cation diffusion away
254 from the surfaces and into the bulk.^{23,24,29} However, other studies have reported the opposite
255 trend where extensive cation segregation is seen under cathodic polarization conditions.^{25–28}
256 Thus, it is unclear whether increasing the fraction of the cycle in fuel cell versus electrolysis
257 mode would reduce electrode degradation, as reported in one prior study.¹¹

258 In summary, degradation of LSCF electrode performance during reversing current
259 operation is dominated by Sr segregation. Higher current densities accelerate Sr segregation,

260 increasing the rate of electrochemical performance degradation for lower operating temperatures
261 (≤ 700 °C) where segregation is normally slow. At 750 °C, Sr segregation kinetics are faster such
262 that Sr surface coverage saturates rapidly, especially with the accelerating effects of current.
263 There is no degradation after a stable Sr surface layer is achieved, which occurs almost
264 immediately at $j = 1.5 \text{ A} \cdot \text{cm}^{-2}$, and the electrochemical activity of LSCF at 750 °C is high enough
265 to yield excellent performance. Cleaning the LSCF surface to remove segregated surface Sr
266 effectively reduces the polarization resistance, but only temporarily until Sr resurfaces.

267 **Methods**

268 Symmetric oxygen electrode cells were prepared by dry pressing GDC powder (Rhodia)
269 and sintering at 1450 °C for 6 hours. LSCF (Praxair) electrodes were screen printed (Heraeus V-
270 737) on either side and fired at 1100 °C for 2 hours to achieve $\sim 15 \mu\text{m}$ thick porous electrodes.
271 LSM (Praxair) pellets and ink (Heraeus V-737) were used as electrical contacts rather than
272 precious metal contacts to avoid possible contamination in the electrode.^{60,61} Current direction
273 was switched every 6 hours, giving a 12 hour period using a LabView controlled Keithley
274 sourcemeter; current density (j) values indicated below denote the reversing current density.
275 Some life tests were repeated to ensure their reproducibility.

276 Potentiostatic electrochemical impedance spectroscopy (EIS) measurements were taken
277 in air at the operational temperature with no applied potential and a 20 mV perturbation using a
278 Zahner IM6 Electrochemical Workstation. Prior to the impedance measurement, the current was
279 stopped and the EIS measurement taken after ~ 15 minutes to allow the cell to stabilize. The
280 impedance spectra were fit to an equivalent circuit model with an inductor, resistor, RQ element
281 (high frequency), and Gerischer element (low frequency) in series. The Gerischer follows a form
282 used by Railsback et al.³⁸ The complex nonlinear least squares fitting was performed using

283 ravedav software.⁴⁶ Scanning electron microscopy and energy dispersive X-ray spectroscopy were
284 conducted using a Hitachi SU8030 field emission SEM. Samples were fractured and coated in 15
285 nm of Osmium to reduce charging.

286 Samples were infiltrated with epoxy and polished for focused-ion beam scanning electron
287 microscopy (FIB-SEM). An FEI Helios and dual-beam Zeiss 1540XB with an accelerating
288 voltage of 2 kV and a backscattered electron detector was used to take serial cross-sectional
289 images. Segmentation and 3D reconstruction methods are described elsewhere.⁶²

290 Inductively coupled plasma-optical emission spectroscopy (ICP-OES) analysis was used
291 to measure segregated Sr-rich species. Three fragments from each cell were measured to improve
292 the statistical accuracy of the results. The cells were stirred in ultrapure water for 30 minutes,
293 which selectively dissolves Sr containing species allowing a measurement of the amount of Sr
294 segregation.^{19,44,45} The same electrodes were then dissolved in HCl overnight, providing a
295 measure of the total amount of electrode material. The solutions are mixed with appropriate
296 amounts of water, HCl, and HNO₃ for ICP-OES analysis using a Thermo iCAP 7600.

297 Since segregated Sr species (SrO, Sr(OH)₂, SrCO₃, etc.) are water soluble and LSCF is
298 not,⁵⁵ H₂O is used to clean the LSCF surfaces rather than HCl, HNO₃, or HF. Previous studies
299 have used these strong acids to etch the top surface of the perovskite electrode to expose a clean
300 surface from deeper in the electrode, thereby improving electrochemical performance.^{63–66} This
301 technique is effective, but it is destructive and highly sensitive to time and the quantity of acid
302 used. To clean the surface, cells ramp slowly from operating temperature to room temperature,
303 rinsed in ultrapure H₂O for one minute, dried at 150 °C, and finally ramped back to temperature
304 for annealing and electrochemical testing.

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419 **Acknowledgements**

420 This material is based upon work supported by the National Science Foundation under grant no.
421 OISE-1545907 and DMR-1506925. Shan-Lin Zhang gratefully acknowledges the scholarship
422 from the State Scholarship Fund of China Scholarship Council (201606285002). This work made
423 use of the EPIC facility of Northwestern University's NUANCE Center, which has received
424 support from the Soft and Hybrid Nanotechnology Experimental (SHyNE) Resource (NSF
425 ECCS-1542205); the MRSEC program (NSF DMR-1121262) at the Materials Research Center;
426 the International Institute for Nanotechnology (IIN); the Keck Foundation; and the State of
427 Illinois, through the IIN. This work made use of the MatCI Facility which receives support from
428 the MRSEC Program (NSF DMR-1720139) of the Materials Research Center at Northwestern
429 University. Metal analysis was performed at the Northwestern University Quantitative Bio-
430 element Imaging Center. The authors would like to thank Roberto Scipioni with assistance using
431 ravidav software and Travis A. Schmauss, David Lam, Alessandra DiCorato, and Cesar Villa for
432 assistance with ICP-OES sample preparation.

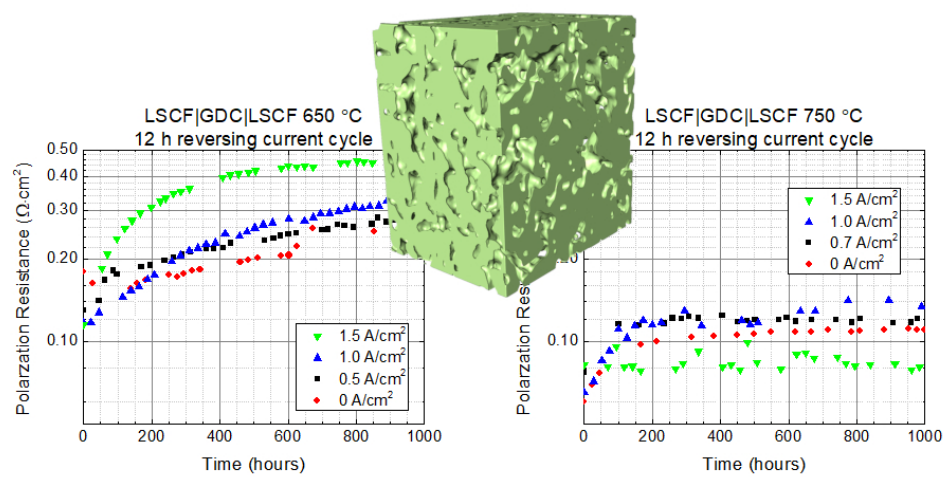
433 **Author contributions**

434 M.Y.L., J.G.R., and S.A.B. planned the experiments and analyzed the data. M.Y.L., J.G.R.,
435 H.W., and Y.A.C. fabricated samples. M.Y.L., J.G.R., H.W., Y.A.C., and S.Z. performed
436 electrochemical measurements. M.Y.L., H.W., and Q.L. contributed to ICP-OES and FIB-SEM.
437 M.Y.L. and Y.A.C. took SEM images. M.Y.L. and S.A.B. wrote the manuscript. S.A.B.
438 developed and supervised the project.

439 **Competing interests**

440 The authors declare no competing interests.

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80x39mm (300 x 300 DPI)

Stable operation of LSCF oxygen electrodes with high current densities at high temperatures for solid oxide electrochemical cells