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## Digital quantification and selection of high-lipid-producing microalgae through a lateral dielectrophoresis-based microfluidic platform

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# 6 Digital quantification and selection of high-lipid-producing 7 microalgae through a lateral dielectrophoresis-based microfluidic 8 platform

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12 Microalgae are promising alternatives to petroleum as renewable biofuel sources, however not sufficiently economically 13 competitive yet. Here, a label-free lateral dielectrophoresis-based microfluidic sorting platform that can digitally quantify 14 and separate microalgae into six outlets based on the degree of their intracellular lipid content is presented. In this 15 microfluidic system, the degree of cellular lateral displacement is inversely proportional to the intracellular lipid level, which 16 was successfully demonstrated using Chlamydomonas reinhardtii cells. Using this functionality, a quick digital quantification 17 of sub-populations that contain different intracellular lipid level in a given population was achieved. In addition, the degree 18 of lateral displacement of microalgae could be readily controlled by simply changing the applied DEP voltage, where the 19 level of gating in the intracellular lipid-based sorting decision could be easily adjusted. This allowed for selecting only a very 20 small percentage of a given population that showed the highest degree of intracellular lipid content. In addition, this 21 approach was utilized through an iterative selection process on natural and chemically mutated microalgal populations. 22 successfully resulting in enrichment of high-lipid-accumulating microalgae. In summary, the developed platform can be 23 exploited to quickly quantify microalgae lipid distribution in a given population in real-time and label-free, as well as to 24 enrich a cell population with high-lipid-producing cells, or to select high-lipid-accumulating microalgal variants from a 25 microalgal library. 26

## 28 1. Introduction

Microalgae, photosynthetic microorganisms that convert 29 sunlight, water, and CO2 into biomass and lipids, have been widely 30 cultivated to produce various high-value products such  $\frac{51}{25}$ 31 pharmaceuticals, cosmetics, pigments, animal feed, bioplastics, and 32 functional foods  $^{1\text{-}3}$  . Moreover, microalgae have been highlighted  $\frac{53}{2}$ 33 promising resources for renewable biofuel due to increasing concerns over limited fossil fuel reserves as well as CO2 emission 34 35 Compared to other biofuel feedstock (e.g., oil crops), microalgae 36 hold several advantages such as higher photosynthetic efficiency 37 8 38 faster growth rate, higher lipid productivity, higher CO<sub>2</sub> fixatio capacity, and less competition with food sources and land usage 39 60 40 Despite these promising potentials, the production cost microalgae-based biofuels is still not economically competitive, and 41 thus, significant improvements are necessary throughout the entipe 42 algal biofuel development pipeline, including strain selection and 43 and 65 44 development, cultivation, harvesting, lipid extraction, 45 conversion<sup>8,9</sup>.

46 Monitoring and quantification of intracellular lipid level during 47 microalgal cultivation, which can provide essential information of 68 achieve precise process control and productivity improvement, have been achieved based on fluorometry, infrared (IR) radiation including mid-IR, near-IR, and Fourier transform IR, and flow cytometry <sup>10</sup>. Even though high-throughput and label-free quantification of lipid level can be achieved by these systems, these methods typically require additional sample preparation steps or complicated instrumentations. These challenges have so far limited the widespread use of these technology development to be exploited for realtime onsite monitoring and quantification of lipid level of microalgae.

Selection of microalgal strains with high lipid level through screening from natural habitats or from microalgal libraries generated through metabolic engineering and/or mutagenesis is one of the promising strategies to develop and obtain strains with higher lipid productivity <sup>11, 12</sup>. This strain selection process typically requires single-cell resolution analysis of lipid content from a large number of sample populations, since each microalgal cell in a given library is a potential variant that has different attributes. However, conventional screening and selection methods utilizing dilutionbased multi-well plate culture are labor-intensive and timeconsuming, and thus limited in throughput as well as the library size that can be screened <sup>13, 14</sup>. Other methods such as fluorescenceactivated cell sorting (FACS) and imaging flow cytometry have been successfully used to screen and select high-lipid-producing mutants <sup>15-17</sup>, as these instruments can provide orders of magnitude higher throughput compared to conventional well-plate assays. However, in all of these methods, cells have to be first fluorescently stained for examining their intracellular lipid content, thus adding additional assay steps, time, and cost is needed.

Recently, several microfluidic approaches have been developed and applied to speed up the microalgal strain development processes, cultivation condition testing steps <sup>18-22</sup>, and label-free lipid

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79 quantification <sup>23</sup>. As an example of microfluidic systems as stiland 80 development tools, a simple microfluidic device that can separate 81 cells having faster phototactic response was successfully utilized an 82 find mutants having faster growth rate and higher lipid level 20, 24 another example, a high-throughput droplet microfluidics-based 83 84 screening platform has been developed and successfully utilized 85 screen and isolate fast-growing and/or high-lipid-producing muta 86 <sup>25-27</sup>. In that droplet microfluidics platform, large numbers of o 48 87 encapsulated water-in-oil emulsion droplets were utilized, e <u>4</u>9 88 droplet functioning as individual pico-liter-scale bioreactors, analyzing the cellular attributes (e.g., growth rate and lipid content) 89 90 of each microalgal variant encapsulated within. Although the 91 microfluidics-based technologies are extremely efficient 92 powerful for selecting microalgal strains with higher lipid conte 93 they still require an intracellular lipid staining step that can eit negatively affect the cells or add additional processing steps, as well 94 <u>5</u>6 95 as somewhat difficult to utilize without expertise in microfluidics. ideal system should be able to rapidly screen, select, and sort 96 97 individual cells based on their intracellular lipid quantity in a lat 159 98 free manner.

Dielectrophoresis (DEP) is a label-free, real-time, and electing 99 field-based cell manipulation technique, which can be readily 100 101 realized in a microfluidic format, since only a simple microfluidic 102 channel integrated with electrodes is required. Thus, DEP-based cell 103 manipulation methods have been extensively utilized in various cell 104 manipulation applications <sup>28, 29</sup>. When cells pass through an electrode 105 pair where a non-uniform alternating current (AC) electric field is 106 generated, cells either experience a positive DEP (pDEP) force (1.6.3) towards the electrodes) or a negative DEP (nDEP) force (i.e., away 107 from the electrodes). The polarity and magnitude of DEP force page 108 109 determined by the dielectric properties of cells and surrounding 110 solution, the size of cell, as well as the applied voltage and frequend  $\frac{1}{9}$ This difference in DEP force depending on cell properties can 111 112 utilized to change the trajectories of cells flowing inside 67 113 microfluidic channel, enabling cell manipulation and cell separation 114 Although DEP has been demonstrated as an effective tool in cell 115 separation, most applications have been focused on mammalian 116 cells <sup>30-32</sup> and bacteria <sup>33</sup>, and only few works have been reported that 117 examine the separation of microalgae <sup>34-36</sup>, particularly based on their intracellular lipid content <sup>34, 35</sup>. Microalgal cells can experience 118 119 different magnitudes of nDEP or pDEP force depending on their lipid 120 content <sup>37, 38</sup>, resulting in different flow trajectories and thus, 121 separation. Although DEP-based microfluidic devices have been 122 successfully used to separate microalgal cells based on their intrinsic 123 properties, only simple operations and applications such as 124 separating two known microalgal strains with known lipid contents 125 have been shown so far, and no real library screening work has been 126 reported. In addition, no DEP-based microfluidic device exist that can 127 accurately determine the intracellular lipid quantity beyond simple 128 binary determination and separation (i.e., lipid vs no lipid, or high-129 lipid vs low-lipid). Last, these devices require relatively complicated 130 and rather expensive experimental setups to generate the pDEP 131 force at high-frequency (~50 MHz) and high-voltage (~30 V peak to 132 peak (V<sub>PP</sub>)) <sup>34, 35</sup>.

In this report, we present a lateral DEP-based microfluidic 133 134 platform capable of separating cells based on their intracellular l 135 content, which was exploited to monitor and quantify 136 heterogeneous distribution of intracellular lipid level of a give 137 microalgal cell population, all label-free and at single-cell resolution 138 In addition, for the first time, real library screening was conducted 139 using the platform, which was successfully demonstrated obtaining high-lipid-producing microalgal populations and strains 140

through multiple rounds of cell population enrichment steps, with and without chemical mutations in between each round.

## 2. Working principle

When electric field is induced with a planar interdigitated electrode array in a microchannel, the electric field gradient is strongest at the edge of the electrode, which can generate pDEP force acting on microalgal cells. Here, the electric field was calculated based on a line charge model <sup>30</sup>. When the interdigitated electrode array is positioned at an angle of  $\theta$  to the flow direction (instead of the typical 90-degree angle, i.e., perpendicular to the flow direction), pDEP force is created around the electrode edges and attracts cells. Since the electrodes are angled, the attracted cells move along the flow direction while remaining attracted to the electrodes, and thus move not only along the flow direction but also laterally (Fig. 1). Due to the hydrodynamic force, the x-directional pDEP force ( $F_{DEP}$ ) cannot hold onto the cells for too long, thus the cells are eventually released from the electrodes and move along the flow direction again, where they are caught by the next angled electrodes and continue the lateral movement. This lateral displacement of cells,  $\Delta y'$ , can be calculated by using the numerical simulation <sup>31, 39</sup> of:

$$\frac{d(\Delta y')}{dt} = \frac{F_{DEP} \cos \theta}{12\eta(S/l)} = \frac{\varepsilon_m V_c \cos \theta \operatorname{Re}[f_{CM}] v_a^2}{32\eta \left(\frac{S}{l}\right) [\ln(8d/\pi a)]^2} \frac{\partial \left|\vec{A}\right|^2}{\partial x}, \quad (1)$$
$$\vec{A} = \sum_{n=1}^{\infty} \left\{ (-1)^{n+1} \frac{[x + (-1)^n (2n-1)d] \overline{a_x} + z \overline{a_z}}{[x + (-1)^n (2n-1)d]^2 + z^2} + (-1)^{n+1} \frac{[x - (-1)^n (2n-1)d] \overline{a_x} + z \overline{a_z}}{[x - (-1)^n (2n-1)d]^2 + z^2} \right\}$$

The symbols used in equation (1) are described in Appendix I. Here, the lateral displacement of microalgal cells strongly depends on the magnitude of pDEP force, which is proportional to the real part of the



**Fig. 1.** Illustration of the lateral DEP microfluidic platform with a planar interdigitated electrode array is placed at an angle (5.7°) to the direction of the flow. The inset shows an enlarged view of the illustrative lateral movement of microalgal cells having different lipid level when passing over the electrode array where the pDEP force is generated. The channel width of the outlet #1-#5 is 300  $\mu$ m, except for the outlet #6 (500  $\mu$ m).

Clausius-Mossotti factor (  $Re[f_{CM}], f_{CM} = \frac{\varepsilon_c^*(\omega) - \varepsilon_m^*(\omega)}{\varepsilon_c^*(\omega) + 2\varepsilon_m^*(\omega)}, \varepsilon^* = \frac{237}{238}$  $j\frac{\sigma}{\omega}$ )) determined by the dielectric properties of cells and  $\frac{1}{299}$ 176 177 178 surrounding media. In the case of microalgal cells produad 179 intracellular lipid, their dielectric properties, which correlate with 244 180 cytoplasm conductivity ( $\sigma$ ), are mostly affected by the cell's **L**AQ 181 level, as lipid has vastly different conductivity compared to the 24B 182 of the cytoplasm (mostly conductive saline solution). The cytoplash4 183 conductivity of microalgal cells without lipid was previously reporzed 184 to be around 0.5 S/m 34. We hypothesized that the cytopla246 185 conductivity can be altered based on the volume fraction247 186 intracellular lipid in cell's entire cytoplasm. Thus, this cytopla248 187 conductivity is expected to decrease from 0.5 to 0.4, 0.25, 249 188 0.1 S/m as intracellular lipid level increases from 0 to 20, 50, 250 189 80% of cell volume, respectively. Simulation using equation2(5)1 190 shows that the real part of the Clausius-Mossotti factor decre252 191 from 0.39 to 0.37, 0.32, and 0.17, respectively (surrounding metals) 192 conductivity set to 0.04 S/m), at 3 MHz frequency (Fig. S1). Th254 193 when intracellular lipid level of a microalgal cell increases, pDEP for 55 194 decreases. In this simulation, the diameter of microalgal cells was256 195 to 7.6 µm (7.6 ± 0.6 µm, measured from 1,000 Chlamydomo263 196 reinhardtii (C. reinhardtii) cells. 258

197 The x-directional pDEP force and lateral displacements w259 198 calculated using equation (1) with the different cytopl2560 199 conductivities of 0.5, 0.4, 0.25, and 0.1 S/m when a microalgal 261 200 passes over a single electrode (Fig. S2). If the cell has no intracell262 201 lipid ( $\sigma$ =0.5), the pDEP force is larger than the hydrodynamic  $\Phi_{63}$ 202 force, and the lateral displacement becomes infinite (i.e., displaced 203 all the way to the end wall of the microfluidic channel). When 265 204 cytoplasm conductivities changed to 0.4, 0.25, and 0.1, where 266 205 magnitude of pDEP force at the edge of the electrodes decreased7 206 the calculated lateral displacements per single electrode were 2268 207 24, and 4 µm, respectively. In other words, more lipid-producing 2819 208 have reduced cytoplasm conductivity, thus resulting in decreas 270 209 their lateral displacement. This allows microalgal cells to 274 210 separated using the presented lateral DEP design purely based 2972 211 their lipid level without any labelling requirement. 273

212 From the above equation (1), the size of microalgal cell274 213 another factor that can affect the pDEP force applied to cells. 225 214 S3(a-b) show that in the case of microalgal cells without lipid or with 215 only small amount of lipid, the lateral displacement is dominate  $2\pi$ 216 the size of the cells. However, since their lateral displacement 278 217 single electrode is over 50 µm, most cells eventually reach 279 218 microfluidic channel wall and nowhere to move further. These 219 microalgal cells with very low intracellular lipid content can284 220 pushed to one side of the microchannel regardless of their 282 221 variation. On the other hand, Fig. S3(c-d) show that when 288 222 cytoplasm conductivities changed from 0.25 to 0.1, the calcular of the calcula 223 lateral displacements were  $24 \pm 3$  and  $3.6 \pm 0.1 \,\mu$ m, respectively. 285 means that as the amount of intracellular lipid increase, the late 224 225 displacement is dominated by cytoplasm conductivity rather that 226 size, which allows microalgal cells to be separated depending on tDBB 227 lipid level. In this work, we utilized this principle to design 289 228 fabricate a lateral DEP-based microfluidic platform, and utilized i290 229 both digital quantification of algal lipid in a given population as 291 230 as conducting an iterative high-lipid-producing cell enrichment 2902 231 separation assay. 293 232 294

## 233 3. Materials and methods

## 234 3.1 Design

The lateral DEP-based microfluidic sorting platform was designed to have three inlets, one for sample and the other two for buffer solutions, six outlets for collecting separated cells, and a planar interdigitated electrode array placed at an angle of 5.7° to the flow direction (Fig. 1). The width and spacing of the electrode array are both 30  $\mu$ m. The height of the microchannel is set to 30  $\mu$ m to minimize the variation of the pDEP force acting on microalgal cells along their vertical position. When microalgal cells are injected into the platform, they are focused into a 50  $\mu$ m wide streamline by sheath flow from the two side buffer inlets. The focused cell streamline is formed around 300  $\mu$ m away from the right-side microchannel wall. Since the channel width of the outlet #6 is 500  $\mu$ m, all cells that are not influenced by the pDEP force (i.e., cells with very high intracellular lipid) will come out of outlet #6 (green dashed line in Fig. 1). Cells with the lowest intracellular lipid level (i.e., highest pDEP force) will experience the largest lateral displacement, and thus move towards outlet #1 (blue dashed line).

## 3.2 Microfluidic device fabrication

The lateral DEP microfluidic platform was made of a polydimethylsiloxane (PDMS) microchannel on a 0.7 mm thick borosilicate glass substrate with patterned DEP planar electrodes (Fig. S4). First, the angled planar electrode array was prepared by Cr/Au (20nm/100nm) deposition on the glass substrate, followed by conventional photolithography and selective Cr/Au etching. A 30 µm thick layer of SU-8 2025 photoresist (Microchem, USA) was patterned on a 3-inch silicon wafer to create the master mold for the microchannel. The SU-8 master mold was coated with Tridecafluoro-1, 1, 2, 2-Tetrahydrooctyl-1-Trichlorosilane (United Chemical Technologies, Inc., Bristol PA) to facilitate PDMS replication, followed by PDMS microchannel replication (10:1 mixture, Sylgard 184, Dow Corning, Inc., MI). After oxygen plasma treatment of both the electrode-patterned glass substrate and the PDMS replica, they were aligned and bonded together for 24 hr at 80°C.

### 3.3 Cell preparation

*C. reinhardtii* strain CC-406 (wall-deficient mutant, no motility) was used to characterize the performance of the developed platform. Unless otherwise stated, cells were cultured in Tris-Acetate-Phosphate (TAP) media at 22°C under continuous illumination (60 µmol photons/m<sup>2</sup>·sec). CC-406 cells were collected during exponential growth phase (~10<sup>6</sup> cells/ml, typically after four days of culture), centrifuged at 600 g (1900 rpm) for 5 min, and resuspended in TAP media lacking NH<sub>4</sub>Cl (TAP-N) with a concentration of 2 × 10<sup>7</sup> cells/ml. Four different CC-406 samples with different lipid content were prepared by cultivation in TAP-N media for different incubation durations (12, 24, 36, and 48 hours).

In order to achieve DEP-based cell separation, all samples were resuspended in low conductivity media (0.04 S/m) before using the cells in the developed microfluidic platform. The low conductivity media contains 2.7 mM of potassium chloride (P9333, Sigma-Aldrich, USA), 0.3 mM of monopotassium phosphate (1551139, Sigma-Aldrich, USA), 0.85 mM of dibasic potassium phosphate (1151128, Sigma-Aldrich, USA), 280 mM of myo-Inositol (I5125, Sigma-Aldrich, USA), suspended in de-ionized (DI) water, and then filtered by using a 0.2  $\mu$ m membrane before use.

## 3.4 EMS mutagenesis

Ethyl methanesulfonate (EMS) mutagenesis was conducted as described in previous studies <sup>15, 27</sup>. Briefly, CC-406 cells were grown to an OD<sub>750</sub> of 0.6 ( $5 \times 10^6$  cells/ml), centrifuged, and resuspended in 6 ml of TAP media containing 225 mM of EMS. Sample tubes were wrapped with aluminium foil and incubated at room temperature for 80 min using a rocking table. After incubation, cells were harvested

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299 by centrifugation and the pellets were washed three times with 12 300 ml of TAP media. Cells were then resuspended in 6 ml of TAP media 301 and stored for cell recovery in dark for 15-18 hr. This procedure was 302 optimized to have an approximate killing rate of 80% from EMS 303 treatment (number of dead cells counted through Evans Blue 304 staining); a condition typically deemed to have sufficient mutation in 305 the population <sup>27</sup>. The final step prior to sample loading into the 306 lateral DEP microfluidic platform was centrifugation, resuspension in 307 TAP-N media, and dilution to a concentration of  $2 \times 10^7$  cells/ml, 308 followed by 72 hr incubation for lipid induction.

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#### 310 3.5 On-chip lateral DEP separation

311 Three syringe pumps provided controlled flow through the 312 microchannel. Two syringe pumps were used respectively to push 313 the cell sample and two buffer solutions into the microchannel. The 314 other syringe pump was used to withdraw six syringes, each 315 connected to the six outlets, and functioned as a reservoir to collect 316 the separated cells. The sample and buffer flow rate were 10 µl/hr 317 and 140 µl/hr, respectively, thus the total volumetric flow rate was 318 150 µl/hr. To match the total flow volume, the withdraw flow rate of 319 each outlet was set to 22.5 µl/hr, except for outlet #6 that was wider 320 (set at 37.5 µl/hr). Subsequently, microalgal cells were flown through 321 the device, collected from each outlet, and stained with BODIPY 322 (Boron-dipyrromethene) to quantify the intracellular lipid content <sup>40,</sup> 323  $^{41}$ . To generate pDEP force, 3 MHz, 5-9 V<sub>PP</sub> sinusoidal voltage was 324 supplied from a function generator (DG4202, Rigol Technologies 325 Inc.). For device characterization, 3 MHz, 5-6 V<sub>PP</sub> sinusoidal wave? 326 were applied to the device. The iterative screening process using 327 natural and chemically mutated populations was conducted und a 64 328 MHz, 9 and 7 V<sub>PP</sub> sinusoidal wave, respectively. A Zeiss Axio Obse**B6**5 329 Z1 microscope (Carl Zeiss Micro Imaging, LLC) was used to count 366 330 number of microalgal cells flowing through the microchannel using 331 chlorophyll autofluorescence (excitation: 460-500 nm, emission > 332 610 nm). About 1,000 cells were analyzed to obtain each lateral 333 distribution graph.

#### 335 3.6 Off-chip lipid content analysis

336 The lipid content of the separated cells collected from each 337 outlet was further analyzed through an off-chip lipid staining and 338 analysis step. Neutral lipid straining fluorescent dye BODIPY was 339 used, where 1 ml of cell sample was mixed with 10  $\mu$ l of BODIPY stock 340 solution (0.5 mg/ml in DMSO), incubated for 10 min in dark, and 341 rinsed at least 3 times with fresh TAP media. Both fluorescence 342 microscopy and flow cytometry were conducted to analyze the lipid 343 content. For fluorescence microscopy, BODIPY fluorescence 344 (excitation: 460-500 nm, emission: 500-550 nm) of retrieved cells 345 from each outlet was measured. About 50 cells were analyzed for 346 each measurement. All microscopic images were analyzed with the 347 NIH Image J software. For flow cytometry, a 488 nm laser was used 348 to excite BODIPY fluorescence and detected at 525 ± 25 nm (BD 349 FACSAria II Cell Sorter). The flow cytometer measurement was 350 considered complete when the total number of analyzed cells reached 10,000. Data was analyzed by FlowJo software (TreeStar, 351 352 San Carlos, CA, USA) and the average BODIPY fluorescence intens 168 of each mutant was analyzed and presented as a histogram (Fig. 369 369 353 354 and S6). 370 355

#### 356 4. Results

#### 372 4.1 Lateral displacement of cells based on their intracellular lipids 357 358 content 374

C. reinhardtii strain CC-406 (cw15), known to accumulates 359 360 intracellular lipid under stressed conditions such as nitrogen



Fig. 2. Fluorescence microscopy images of CC-406 cell trajectories (white line) inside the lateral DEP device. Cells cultured in TAP-N media for (a) 12 (b) 24 (c) 36, and (d) 48 hr showed different trajectories compared to the direction of the flow (red line, straight).



Fig. 3. Efficiency of separating cells based on their different intracellular lipid level using the lateral DEP microfluidic platform (applied voltage: 3 MHz, 5  $V_{\text{pp}}$  sinusoidal wave). (a) Measured average BODIPY fluorescence intensities of CC-406 cells ( $n=56, \pm$  SD) collected from each outlet. (b) Average size of cells ( $n=56, \pm$  SD) collected from each outlet. (c) Representative microscopy images of cells collected from each outlet.

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376 starvation <sup>42</sup>, was cultured in TAP-N media for 12, 24, 36, and 48B8 377 to induce intracellular lipid to a different degree <sup>43</sup>. Mage 378 intracellular lipid level was observed from longer nitrogen-stres 379 samples, analyzed through fluorescent neutral lipid BODIPY stain 444 380 and flow cytometry (Fig. S7). To confirm the operation of the lat 381 DEP microfluidic platform, CC-406 cells cultured in TAP-N media 463 382 12 hr were tested. All cells were separated into outlet #6 when 446 383 DEP voltage was applied (video 1(a)), while most cells whether 384 separated into outlet #1 when applying a DEP voltage of 6 V<sub>PP</sub> #45 385 MHz (video 1(b)). 447

386 The feasibility of the lateral DEP microfluidic platform 4448 387 separate microalgal cells that have different lipid level value 388 evaluated in two ways: comparison of trajectories of late450 389 displacement in the microfluidic channel, and comparison of li461 390 level of cells collected from each of the six outlets. When CC-40562 391 cells with no lipid passed over the planar electrode array, most45f3 392 them were trapped on the electrode edge when applying a D4E54 393 voltage of 5 V<sub>PP</sub> at 3 MHz. Trajectory analysis (Fig. 2(a)) showed that 394 CC-406 cells with small amount of lipid (12 hr incubation) had an 395 average lateral displacement of 145.9 ± 72.9 µm per single 396 electrode, and continuously moved along the edge of the electrode, 397 eventually being separated into outlet #1. Cells with higher level of 398 lipid content (24, 36, and 48 hr incubation) showed average lateral 399 displacements of 67.9  $\pm$  30.7, 36.0  $\pm$  22.2, and 8.6  $\pm$  3.4  $\mu$ m per single 400 electrode, respectively (Fig. 2(b-d)). This result clearly indicates that 401 the amount of lateral displacement is directly influenced by the 402 intracellular lipid level of cells.

403 Next, to further provide quantitative data on the cell separation 404 capability of the microfluidic device based on cell's intracellular lipid 405 level, the lipid content of the cells collected from each outlet were 406 analyzed through BODIPY staining. Fig. 3(a) shows the average 407 BODIPY fluorescence intensities of the cells collected from outlet #1 408 through outlet #6, which increased from  $2.2 \pm 1.7$  to  $6.0 \pm 2.8$ , 15.1 409  $\pm$  6.0, 24.6  $\pm$  6.1, 30.2  $\pm$  7.4, and 39.5  $\pm$  13.1 (×10<sup>4</sup> a.u.), respectively. 410 This means that cells with higher lipid level have less lateral 411 displacement (move towards outlet #6), while cells with lower ligid, level has larger lateral displacement (move towards outlet 446412 BODIPY fluorescence intensity of cells collected from each outlet  $\frac{1}{457}$ 413 showed statistical difference tested through independent-samples 414 t-test (n = 56,  $p < 2.7 \times 10^{-5}$ ). To check whether cell size variation may 415 have influenced the DEP lateral displacement result, average 416 sizes from each outlet were measured. However, no significant 417 differences in cell sizes between each outlet were observed Fig.  $34b_2$ 418 419 Fig. 3(c) shows representative microscopy images of cells collected 420 from each outlet. Taken together, this result confirmed that the 421 developed lateral DEP microfluidic platform can digitally quantify 422 and separate cells based on their intracellular lipid level. 423

## 424 4.2 Control of lateral distribution of cells through DEP voltage 425 control

426 Lateral distribution of cells separated through the developed 427 device (i.e. percentage of cells separated into each outlet) represents 428 the distribution of cells having different intracellular lipid level in a 429 given population. Fig. 4(a) (top row) shows such distributions when 430 a DEP voltage of 5  $V_{\mbox{\scriptsize PP}}$  was applied. It was observed that as the 431 population shifts from 12 hr (left) to 48 hr (right) incubation in N-432 limited culture (i.e., from less to more lipid-producing population? 433 more cells came out of outlet #6 rather than from outlet #1. 464 434 degree of this distribution can be altered by simply adjusting 465 435 applied voltage so that only a very small fraction of cells that show 436 the highest lipid content comes out of outlet #6. Fig. 4(b) and 46437 show how the lateral distribution of the same CC-406 cell popula

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changes under the different voltage conditions of 5, 5.5, and 6  $V_{PP}$ . Comparing the lateral distribution along each column, as the applied voltage increased, more cells were observed coming out of outlet #1 (distribution profile moving from right to left), while less cells came out of outlet #6. This simple voltage control allowed controlling the sorting threshold based on cell's intracellular lipid level. For example, when a DEP voltage of 5 V<sub>PP</sub> was applied, 83% of cells that were cultured in TAP-N media for 48 hr was collected from both outlets #5 and #6. By increasing the applied voltage to 5.5 and 6  $V_{PP}$ , this percentage dropped to 44% and 19%, respectively. When counting cells from only outlet #6 (e.g., for enrichment applications), the percentage dropped to 2 and 1.6%, respectively (from 23%, when a voltage of 5 V<sub>PP</sub> was applied). This result clearly demonstrated the capability of the platform to control the percentage of cells separated into each outlet by simply adjusting the applied voltage. This is particularly advantageous when wanting to only select the highest lipid-producing microalgal cells in a given population.



**Fig. 4.** The lateral distributions of CC-406 cells cultured in TAP-N media for 12 hr (a1, b1, c1), 24 hr (a2, b2, c2), 36 hr (a3, b3, c3), and 48 hr (a4, b4, c4) were obtained by calculating the percentage of cells separated into each outlet. The effect of different DEP voltages applied on the lateral distributions were also tested: (a1-4) 5 V<sub>pp</sub>, (b1-4) 5.5 V<sub>pp</sub>, and (c1-4) 6 V<sub>pp</sub>.



**Fig. 5.** (a) Illustration showing the iterative high-lipid-producing cell enrichment and selection process. (b1) Lateral distributions of wild-type CC-406 cells of the starting population; (b2) after round 1; (b3) after round 2; (b4) after round 3. The applied voltage was 3 MHz, 9  $V_{pp}$ .

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469 4.3 Enrichment of high-lipid-producing C. reinhardtii cells 531 470 As a first real screening application, the developed platform 5/32471 used for conducting three rounds of enrichment process from v5d3 472 type CC-406 populations to obtain a population that has a larget 473 number of high-lipid-producing cells. Fig. 5(a) shows the iterabige 474 experimental procedure of this enrichment process; 1) cell growt536 475 TAP media for 4 days to obtain enough cells, 2) cell incubation in TAB7 476 N media for 72 hr for intracellular lipid induction and accumulat 477 3) selection of high-lipid-producing cells through the develo**5** $\mathbf{6}$ 478 platform (separation and collection from only outlet #6), 4) repeato 479 steps #1 to #3. During the enrichment process, the lat541 480 distribution of cells in each round was monitored and compare 542 481 analyze how the overall cell population changed (Fig. 5(b)). From 548 482 initial population, the DEP voltage was adjusted to 9  $V_{PP}$  so that  $\frac{5}{44}$ 483 1.7% of cells from the starting population were collected from out 45 484 #6 (Fig. 5(b-1)). Cells coming out of outlets #4 to #6 are all deer**54d6** 485 to be relatively high-lipid producers, occupying 8% of the overall 486 population. Approximately 3,000 cells were collected from outle **5**#8 487 over a 3-hr period, and then re-cultured in TAP media to expand **549** 488 population. After this first round of enrichment, cells coming out 50489 outlets #4 to #6 combined together increased to 20%, and 564 490 percentage of cells coming out of outlet #6 was 6% (Fig. 5(b-2)). 552 491 For the 2<sup>nd</sup> and 3<sup>rd</sup> rounds of the microfluidic chip-based 492 enrichment process, the percentages of cells coming out of outleb 493 were 2% and 11%, respectively, while the percentages of Gens 494 coming out of outlets #4 to #6 were 70% and 98%, respectively (5 b 6 495 5(b3-4)). Overall, the lateral distribution profiles progressized 496 moved from outlet #1 to #6 where the fraction of cells separated bba 497 outlet #4 to #6 gradually increased over the rounds, from 8% (in 559 sample), to 20, 70 and 98% (3rd round), respectively. To fur 560 498 499 confirm that we are indeed enriching the cell population to hafed 500 higher lipid content, BODIPY lipid staining followed by fluoresce **562** 501 intensity analysis were carried out after each round. The average 502 BODIPY fluorescence intensities of the starting population 56d 503 samples from each round of enrichments were 37 ± 10.9, 40.4 ± 11.8, 504  $43.4 \pm 10.5$  and  $56.1 \pm 9.8$  (×  $10^4$  a.u.), respectively, meaning that the 505 overall population indeed shifted to have higher number of high-506 lipid-producing cells. Here, the average BODIPY intensity of the 3rd 507 round enrichment population is about 1.5 times higher than that of 508 the starting population.

510 4.4 Screening of EMS-mutagenized *C. reinhardtii* library for 511 selecting high-lipid-producing mutants 565

Following the success in enriching a starting population 566 512 contain higher percentage of high-lipid-producing cells, we next 513 applied the platform to iteratively select high-lipid-producing 514 515 mutants from a chemically mutated C. reinhardtii library. 569 motivation for conducting such an assay is because enrichment of 516 517 population may not necessary result in stable strains that show high lipid production, as the natural mutation rates of cells are quite row 518 <sup>13, 14</sup>. Thus, here a random mutagenesis strategy was applied to  $\frac{522}{2}$ 519 406 cells through EMS treatment to generate a mutant library.  $\frac{573}{240}$ 520 developed platform was then used to select high-lipid-producing 521 strains using a similar selection procedure described in the previous 522 576 523 section.

Fig. 6(a) shows the lateral distribution of the starting populat57,
where 8.8% of the cells came out of outlets #4 to #6 combined, 57,
only 1.8% from outlet #6. From here, cells coming out of outlet #6
were collected, diluted, and put on agar plates with dilution to form
multiple single colonies. Twelve of these single colonies were
randomly picked, each cultured in TAP media and expande82
followed by resuspension in TAP-N media for 72 hr to induce lip63.

Off-chip lipid characterization was conducted using flow cytometry combined with BODIPY staining (Fig. S5). Among the 12 mutants, mutant #5 (marked as 1<sup>st</sup>-mutant #5) showed the highest average BODIPY intensity, which was 1.4 times higher (1262  $\pm$  520 (a.u.)) compared to that of wild-type CC-406 cells (914  $\pm$  498 (a.u.)), and thus selected for another round of subsequent selection process. The characteristics of the mutant #5 was further analyzed by the lateral DEP microfluidic platform (Fig. 6(b)). When comparing the lateral distribution profiles of wild-type CC-406 and the 1<sup>st</sup>-mutant #5 cells (Fig. 6(a-b)), the proportion of cells coming out of outlets #4 to #6 combined changed from 8.8 to 41.7%, respectively, clearly showing that this can be a promising strategy in selecting high-lipid-producing mutants.

Next, another round of mutation and selection process was applied to the re-cultured mutant #5. The 1st-mutant #5 cells underwent another round of EMS treatment, and then screened through the microfluidic device. Again, cells collected from outlet #6 were plated on agar plates to form multiple single colonies. From here, 22 colonies were randomly selected, and then analyzed by flow cytometry. Based on the histogram analysis, the 2<sup>nd</sup>-mutant #2, 8, 13, 15, 16, and 17 all showed over 1.3 times higher average BODIPY intensity than that of the wild-type CC-406 cells  $(1388 \pm 716 (a.u.))$ (Fig. S6). Among them, the 2nd-mutant #16 showed the highest average BODIPY intensity, which was 1.6 times higher (2232 ± 942 (a.u.)) compared to that of wild-type CC-406, and thus was selected for further analysis. Overall, when comparing the lateral distribution profiles of the population, the portion of cells coming out of outlets #4 to #6 combined were 8.8, 41.7 and 58.9% for wild-type CC-406, 1st-mutant #5, and 2nd-mutant #16 cells, respectively (Fig. 6(a-c)). In summary, seven potentially promising high-lipid-producing microalgal strains were found through the use of the developed lateral DEP microfluidic platform, which is now undergoing further down-stream analysis.



Fig. 6. Lateral displacement of (a) wild-type CC-406 cells, (b)  $1^{st}$ -Mutant #5, and (c)  $2^{nd}$ -Mutant #16. The applied voltage was 3 MHz, 7  $V_{pp}$ .

## 5. Discussion

This paper presents a lateral DEP-based microfluidic sorting platform that allows for 1) providing digital quantification of the intracellular lipid level of a given microalgal cell population, 2) selecting cells/strains that show enhanced lipid production, and 3) enriching a given population to have more high-lipid-producing cells. The pDEP force acting on the cells is inversely proportional to their lipid level, resulting in different degree of lateral displacements (i.e., more lipid  $\rightarrow$  less pDEP force applied  $\rightarrow$  less lateral displacement). Based on this principle, the developed platform successfully separated microalgal cells with different lipid levels into the six cell collection outlets and could be employed to actually provide a profile of the intracellular lipid level of a given population in real-time.

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584 Another distinguishing feature of the developed platform is that 646 585 applied voltage can be readily adjusted to collect only the top  $64\sqrt{7}$ 586 percent of cells in terms of their intracellular lipid level in a giber 8 587 population, which was demonstrated by adjusting the voltage so 649 588 less than 2% of the top lipid producers from a given population coafed 589 be sorted and collected. This allowed an iterative enrichment process 590 to be conducted under a stringent selection condition to enhance 662 591 possibility of obtaining potential variants having high lifeb3 592 production capability. These capabilities were not available 654593 previously developed DEP-based microalgae cell separa 665 594 microfluidic systems <sup>34, 35</sup>. 656

595 The presented platform has another advantage, where 667 596 operation conditions for the DEP separation function were at a m658 597 lower frequency and voltage range (3 MHz, 5-9 V<sub>PP</sub>), compared to 659 598 previously reported DEP-based microalgae separation platfo 599 (e.g., 50 MHz, 30 V<sub>PP</sub>) <sup>34, 35</sup>. Since this low frequency and low voltage 600 signal can be easily generated using a generic low-cost function2 601 generator, the developed platform can eliminate the need 663 602 expensive high-end instruments, which enables broader utilizatio664 603 such a device. Also, this low voltage can reduce potential **Geb** 604 damages resulting from the high-intensity electric field near 666 605 electrode edges as well as joule heating 44,45. In the presented w667 606 the calculated maximum electric field in the device was 85 kV/cr668 607 9 V<sub>PP</sub>, an electric field strength known to have little effect on **669** 608 viability. This was verified through Evans blue staining of cells flow to 609 through the microfluidic system, where 98% of the cells scree 67d 610 611 to 99% for the initial cell population), indicating that the applied **67**/3 612 voltage has no negative impact on cell viability. 674

613 The optimized sample flow rate was 10  $\mu$ l/hr to effectively a  $\frac{1}{100}$ 614 the DEP force on cells (cell concentration:  $2 \times 10^7$  cells/ml), mear  $6\pi$ 615 that the throughput of the single-channel lateral DEP microflution 616 channel was 20 cells/sec. Previous DEP-based microalgae separa 678 617 study reported a maximum throughput of 10<sup>3</sup> cells/sec <sup>35</sup>. Altho**6** 618 this previous system showed higher throughput, this device sings 619 separated microalgal samples into two groups, high- and low-life 81 620 producing cells, which did not require high separation resolut 621 Although the throughput of the presented device is lower compated 622 to the previous study, the device can provide a precise and accufated 623 profile of the intracellular lipid amount of microalgal cells in a gibes 624 population. In addition, the platform allows for obtaining 686 625 accurate lipid distribution profile of 1,000 microalgal cells within 687 626 min, capable of providing rapid real-time monitoring of the lipid loss 627 of a given population. If a higher throughput is needed, a m689 628 channel approach can readily achieve any needed throughput. 690

629 Current state of the art cell identification and separation to 1 630 such as FACS have been utilized to discover high-lipid-produced 631 microalgal variants at high throughput and single-cell resolution (193 632 cells/sec) <sup>15-17</sup>. However, staining process using Nile red and BOD694 633 is required, which results in significantly lower cell viability as web 95 634 requires additional sample preparation steps. On the other hand, **696** 635 developed DEP-based platform can select microalgal cells showed 636 high-lipid production without any labelling step, thus the negatives 637 effects of cell staining can be avoided. Also, compared to the active 638 sorting method of FACS, the cell collection method where just 00 639 constant flow of samples is required makes the overall instrumzed 640 requirement very simple, making this microfluidic device potentized 641 a field-deployable system. In terms of cost burden, a FXOS 642 instrument and its maintenance are relatively expensive, typica04 housed in central user facilities. However, a DEP-based microfluighe 643 setup costs less than \$500, with material cost of a reusable single 644 chip being less than \$30, making this a highly attractive solution.707 645

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Adaptive laboratory evolution (ALE) has been carried out to improve microalgal attributes through long-term selection of serial dilution in normal TAP media <sup>46, 47</sup> and under the abiotic stresses such as high CO2 48, salt concentrations 49, 50, light intensity 51, 52, temperature <sup>53</sup>, and cooperative multi-factors <sup>54</sup>. Although useful, this process is quite time-consuming. For example, Yu et. al. 46 discovered strains having 1.5 times faster growth rate and 1.2 times higher lipid accumulation than the starting cells, however the overall process took 28 serial dilution cycles over a 84 day period. Also, populations having 1.35 times faster growth rate than the initial population were found after 1,880 generations selected over 17 months <sup>47</sup>. Compared to this, a single round of ALE process using the developed lateral DEP microfluidic platform was completed within a week, with most of the time spent to simply regrow the selected cells (3 hr of on-chip selection process, followed by 96 hr of cell re-growth to create the starting population for the next round of ALE). Through three iterative ALE processes, a population having 1.5 times higher lipid production compared to the initial sample was successfully obtained, significantly shorter than previously reported methods. Thus, we expect that this approach has the potential to significantly decrease the time required for ALE assays.

The developed lateral DEP-based microfluidic sorting platform carried out the assays using only one microalgal species, *C. reinhardtii*. However, there is no limitation on the type of unicellular microalgal cells that can be used in this platform, such as *Chlorella* sp. <sup>48</sup>, *Nannochloropsis* sp. <sup>50</sup>, *Synechocystis* sp. <sup>53</sup>, *Schizochytrium* sp. <sup>54</sup>, all being microalgae of high interest for lipid production. However, whether non-spherical cells can also be separated purely based on their intracellular lipid level remains to be seen (planned future studies), where such cell's movement could be influenced by different hydrodynamic force.

Microalgae including CC-406, *Chlorella. vulgaris, dw15*, and *pgd1*, which have been used as model samples in previously developed DEP-based sorting systems <sup>34, 35</sup>, can accumulate lipid as well as starch <sup>55</sup> which also has high dielectric constant. Regardless of starch accumulation in TAP-N cultivation, microalgae experienced different DEP force and could be separated depending on their lipid level, which was successfully demonstrated based on BODIPY fluorescence intensity. In future work, starch-less mutant, for example *C. reinhardtii* strain *star6*, can be used in this DEP-based platform to show how accumulated starch may affect microalgae separation.

As a further downstream analysis, the growth rate of the 1<sup>st</sup>mutant #5 and the 2<sup>nd</sup>-mutant #16 were analysed and showed that their growth rate was not significantly different from that of control (Fig. S8). Here, EMS chemical random mutagenesis strategy was utilized, but other physical mutagenic methods such as UV light, gamma ray, and X-ray can be used as alternative methods <sup>56</sup>. Also, instead of the fluorescent lipid staining method, lipid level of strains discovered can be further analysed through gravimetric quantification, high-performance liquid chromatography (HPLC), or near infrared (NIR) spectroscopy once a large-scare cultivation is achieved <sup>57</sup>.

In the future, the developed platform can be further improved by integrating impedance-based cell counting technology <sup>58-61</sup>, which can characterize the number of cells flowing through each outlet automatically, making the analysis process easier. Such a fully automated system will be capable of conducting real-time analysis of microalgal cell population to determine their lipid content.

## Conclusion

The developed platform has the capability to sort cells based on the degree of their intracellular lipid level, somewhat similar to using

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| 708               | fluorescence intensity of fluorescent lipid-stained cells. The platf <b>767</b>  |                 |     |
|-------------------|--|-----------------|-----|
| 709<br>710<br>711 | has broad application perspective, which not only includes obtain<br>high-lipid-producing strains or enrichment of a given population,<br>also to rapidly assess the beterogeneity of intracellular lipid leve |                 |     |
| 712<br>713        | making best harvesting decisions during algal biofuel production.<br>present setup, including the device, is relatively cheap and eas  | . 7174<br>s7762 | 7.  |
| 714               | build, thus it can be integrated also into a portable system, w  | 171213          | 8.  |
| 715               | would enable real-time onsite monitoring and screening in la   | a7g7e4          | 9.  |
| 716               | scale microalgal culture systems.  | 775             | 10  |
| /1/               |  | //6             |     |
| 718               | Conflicts of interest  | ///             | 11  |
| 719               | There are no conflicts to declare.   | 1/8             | 4.2 |
| 720               |  | 779             | 12  |
| 721               | Acknowledgements   | 700             |     |
| 722               | This work was supported by the National Science Foundation   | /o⊥<br>atjiogn) | 10  |
| 723               | (NSF) Emerging Frontiers in Research and Innovation (EFRI) g   | 702<br>17802    | 12  |
| 724               | #1240478. Any opinions, findings, and conclusions  | 78h             |     |
| 725               | recommendations expressed in this material are those of  | 70 <del>,</del> | 1/  |
| 726               | author(s) and do not necessarily reflect the views of the Nati   | onat            | 14  |
| 727               | Science Foundation.  | 787             | 15  |
| 728               |  | 788             | 10  |
| 720               | Notos  | 789             |     |
| 729               |  | 790             | 16  |
| 730               | Author contributions   | 791             |     |
| /31<br>722        | SI.H., H.S.K., and A.H. designed the experiments and co-wrote  | 7.92            | 17  |
| 732               | the theoretical analysis. A H supervised the work and wrote  | 793             |     |
| 733               | the theoretical analysis. A.H. supervised the work and wrote   | 794             |     |
| 725               | manuscript.  | 795             | 18  |
| 735               |  | 796             | -   |
| 730               | The following symbols are used in this paper:  | 797             | 19  |
| 738               | s* = complex permittivities of microalgae  | 798             |     |
| 739               | $\varepsilon_c^*$ = complex permittivities of suspension media   | 799             | 20  |
| 740               | $\varepsilon_m$ = complex permittivities of suspension media   | 800             |     |
| 741               | $\sigma$ = electrical conductivity of the material   | 801             | 21  |
| 742               | t = time   | 802             |     |
| 743               | $\eta$ = apparent viscosity of microalgal cell in a suspension media   | 803             |     |
| 744               | S = maximum cross-sectional area   | 804             | 22  |
| 745               | l = characteristic length of microalgal cell   | 805             |     |
| 746               | a = effective radius of the electrode  | 806             | 23  |
| 747               | d = half width and half spacing of a planal interdigitated electron  |                 |     |
| 748               | $F_{DEP}$ = x-directional pDEP force   | 808             |     |
| 749               | $Re[f_{CM}]$ = real part of the Clausius-mossotti factor   | 009<br>010      |     |
| 750               | $V_c$ = microalgal cell volume   | 810<br>811      |     |
| /51               | $v_a$ = applied voltage  | 812             |     |
| 752               | A = calculated electric field  | 813             |     |
| 753               | x = x-directional cell position ( $-d/2 < x < d/2$ )   | 814             | 24  |
| 754               | z = levitation height of microalgal cell from the electrode array  | 815             |     |
| /55               | $a_x = x$ -directional unit vector   | 816             | 25  |
| /56               | $a_z = z$ -directional unit vector   | 817             | -   |
| /5/               | _  | 818             |     |
| 758               | References   | 819             | 26  |
| 759               | 1. G. Markou, D. Vandamme and K. Muylaert, W   | /8/20           |     |
| 760               | Research, 2014, <b>65</b> , 186-202.   | 821             |     |
| /61               | 2. L. Zhu, <i>Renewable and Sustainable Energy Reviews</i> , 2   | 81222           | 27  |
| /62               | <b>41</b> , 1376-1384.   | 823             |     |
| /63               | 3. T. M. Mata, A. A. Martins and N. S. Caetano, <i>Renewable</i>   | 824             |     |
| 764<br>765        | Sustainable Energy Reviews, 2010, <b>14</b> , 217–232.   | 825             | 28  |
| 765               | 4. R. H. Wijttels and M. J. Barbosa, <i>Science</i> , 2010, <b>329</b> ,   | 826             | 29  |
| /00               | /99.   | 827             |     |
|                   |  | 828             |     |

ARTICLE

|            | in Biotechnology, 2015, <b>32</b> , 255-268.  |
|------------|---|
| 6.         | A. Han, H. Hou, L. Li, H. S. Kim and P. d. Figueiredo, <i>Trends</i><br><i>in Biotechnology</i> , 2013, <b>31</b> , 225-232.  |
| 7.         | X. Zeng, M. K. Danquah, X. D. Chen and Y. Lu, <i>Renewable and Sustainable Energy Reviews</i> , 2011, <b>15</b> , 3252-3260.  |
| 8.<br>9.   | D. R. Georgianna and S. P. Mayfield, 2012, <b>488</b> , 329-335.<br>Y. Chisti, <i>Journal of Biotechnology</i> , 2013, <b>167</b> , 201-214.  |
| 10.        | I. Havlik, P. Lindner, T. Scheper and K. F. Reardon, <i>Trends in Biotechnology</i> , 2013, <b>31</b> , 406-414.  |
| 11.        | M. Hlavova, Z. Turoczy and K. Bisova, <i>Biotechnology</i><br><i>Advances</i> , 2015, <b>33</b> , 1194-1203.  |
| 12.        | A. Ghosh, S. Khanra, M. Mondal, G. Halder, O. N. Tiwari, S. Saini, T. K. Bhowmick and K. Gayen, <i>Energy Conversion and Management</i> , 2016, <b>113</b> , 104-118.   |
| 13.        | X. Li, E. R. Moellering, B. Liu, C. Johnny, M. Fedewa, B. B. Sears, MH. Kuo and C. Benning, <i>The Plant Cell</i> , 2012, <b>24</b> , 4670-4686.  |
| 14.        | C. Yan, J. Fan and C. Xu, <i>Methods in Cell Biology</i> , 2013, <b>116</b> , 71-80.  |
| 15.        | B. Xie, D. Stessman, J. H. Hart, H. Dong, Y. Wang, D. A. Wright, B. J. Nikolau, M. H. Spalding and L. J. Halverson, <i>Plant Biotechnology Journal</i> , 2014, <b>12</b> , 872-882.   |
| 16.        | M. Terashima, E. S. Freeman, R. E. Jinkerson and M. C. Jonikas, <i>The Plant Journal</i> , 2015, <b>81</b> , 147-159.   |
| 17.        | K. Yamada, H. Suzuki, T. Takeuchi, Y. Kazama, S. Mitra, T. Abe, K. Goda, K. Suzuki and O. Iwata, <i>Scientific Reports</i> , 2016, <b>6</b> , 1-8.  |
| 18.        | H. S. Kim, T. L. Weiss, H. R. Thapa, T. P. Devarenne and A.<br>Han, <i>Lab on a Chip</i> , 2014, <b>14</b> , 1415-1425.   |
| 19.        | H. S. Kim, T. P. Devarenne and A. Han, <i>Lab on a Chip</i> , 2015, <b>15</b> , 2467-2475.  |
| 20.        | J. Y. H. Kim, H. S. Kwak, Y. J. Sung, H. I. Choi, M. E. Hong, H.<br>S. Lim, JH. Lee, S. Y. Lee and S. J. Sim, 2016, <b>6</b> , 21155.   |
| 21.        | B. Guo, C. Lei, H. Kobayashi, T. Ito, Y. Yalikun, Y. Jiang, Y.<br>Tanaka, Y. Ozeki and K. Goda <i>, Cytometry Part A</i> , 2017, <b>91A</b> ,<br>494-502.   |
| 22.        | H. S. Kim, T. P. Devarenne and A. Han, <i>Algal Research</i> , 2018, <b>30</b> , 149-161.   |
| 23.        | Y. Suzuki, K. Kobayashi, Y. Wakisaka, D. Deng, S. Tanaka, C<br>J. Huang, C. Lei, CW. Sun, H. Liu, Y. Fujiwaki, S. Lee, A.<br>Isozaki, Y. Kasai, T. Hayakawa, S. Sakuma, F. Arai, K.<br>Koizumi, H. Tezuka, M. Inaba, K. Hiraki, T. Ito, M. Hase, S.<br>Matsusaka, K. Shiba, K. Suga, M. Nishikawa, M. Jona, Y.<br>Yatomi, Y. Yalikun, Y. Tanaka, T. Sugimura, N. Nitta, K. Goda<br>and Y. Ozeki, <i>Proceedings of the National Academy of</i><br><i>Sciences</i> , 2019, <b>116</b> , 15842–15848. |
| 24.        | Y. J. Sung, H. S. Kwak, M. E. Hong, H. I. Choi and S. J. Sim,<br>Analytical Chemistry, 2018, <b>90</b> , 14029-14038.   |
| 25.        | S. Abalde-Cela, A. Gould, X. Liu, E. Kazamia, A. G. Smith and a. C. Abell, <i>Journal of the Royal Society Interface</i> , 2015, <b>12</b> , 106.   |
| 26.        | H. S. Kim, A. R. Guzman, H. R. Thapa, T. P. Devarenne and A. Han, <i>Biotechnology and Bioengineering</i> , 2016, <b>113</b> , 1691-1701.   |
| 27.        | H. S. Kim, SC. Hsu, SI. Han, H. R. Thapa, A. R. Guzman, D.<br>R. Browne, M. Tatli, T. P. Devarenne, D. B. Stern and A. Han,<br><i>Plant Direct</i> , 2017, 1-13.  |
| 28.<br>29. | B. Cetin and D. Li, <i>Electrophoresis</i> , 2011, <b>32</b> , 2410-2427.<br>C. Qian, H. Huang, L. Chen, X. Li, Z. Ge, T. Chen, Z. Yang and<br>L. Sun, <i>International Journal of Molecular Sciences</i> , 2014,   |

S.-F. Han, W.-B. Jin, R.-J. Tu and W.-M. Wu, Critical Reviews

8 | J. Name., 2012, 00, 1-3

This journal is  $\ensuremath{\mathbb{C}}$  The Royal Society of Chemistry 20xx

**15**, 18281-18309.

| 829<br>830        | 30. | KH. Han and A. B. Frazier, <i>Lab on a Chip</i> , 2008, <b>8</b> , 1 <b>691</b><br>1086. 892   | 59. |
|-------------------|-----|--|-----|
| 831<br>832        | 31. | SI. Han, SM. Lee, YD. Joo and KH. Han, <i>Lab on a</i> <b>(89)</b><br>2011. <b>11</b> . 3864-3872. 894   | 60. |
| 833<br>834        | 32. | J. Jung, SK. Seob, YD. Joo and KH. Han, Sensors 805<br>Actuators B: Chemical, 2011, 157, 314-320, 896  | 61. |
| 835<br>836        | 33. | T. Z. Jubery, S. K. Srivastava and P. Dutta, <i>Electrophoresis</i> , 2014, <b>35</b> , 691-713.   |     |
| 837<br>838        | 34. | YL. Deng, MY. Kuo and YJ. Juang, <i>Biomicrofluidics</i> , 2014, <b>8</b> , 064120.  |     |
| 839<br>840        | 35. | H. Hadady, D. Redelman, S. R. Hiibel and E. J. Geiger, <i>AIMS Biophysics</i> , 2016, <b>3</b> , 398-414.  |     |
| 841<br>842        | 36. | Y. Wang, J. Wang, X. Wu, Z. Jiang and W. Wang, <i>Electrophoresis</i> , 2019, <b>40</b> , 969-978.   |     |
| 843<br>844        | 37. | YL. Deng, JS. Chang and YJ. Juang, <i>Bioresource Technology</i> , 2013, <b>135</b> , 137–141.   |     |
| 845<br>846        | 38. | H. Hadady, J. J. Wong, S. R. Hiibel, D. Redelman and E. J. Geiger, <i>Electrophoresis</i> , 2014, <b>35</b> , 3533-3540.   |     |
| 847<br>848        | 39. | KH. Han, SI. Han and A. B. Frazier, <i>Lab on a Chip</i> , 2009, <b>9</b> , 2958–2964.   |     |
| 849<br>850        | 40. | T. Govender, L. Ramanna and F. B. I. Rawat, <i>Bioresource Technology</i> 2012, <b>114</b> , 507-511.  |     |
| 851<br>852        | 41. | J. Rumin, H. Bonnefond, B. Saint-Jean, C. Rouxel, A. Sciandra, O. Bernard, JP. Cadoret and G. I. Bougaran,   |     |
| 853<br>854        | 42. | <i>Biotechnology for Biofuels</i> , 2015, <b>8</b> , 42.<br>Z. T. Wang, N. Ullrich, S. Joo, S. Waffenschmidt and U.  |     |
| 855<br>856        | 43. | Goodenough, <i>Eukaryotic Cell</i> , 2009, <b>8</b> , 1856-1868.<br>H. S. Kim, S. C. Waqued, D. T. Nodurft, T. P. Devarenne, V.  |     |
| 857<br>858        | 44. | V. Yakovlevb and A. Han, <i>Analyst</i> , 2017, <b>142</b> , 1054-1060.<br>X. Xuan, <i>Electrophoresis</i> , 2008, <b>298</b> , 33-43.   |     |
| 859<br>860        | 45. | C. Church, J. Zhu, G. Huang, TR. Tzeng and X. Xuan, <i>Biomicrofluidics</i> , 2010, <b>4</b> , 044101.   |     |
| 861<br>862        | 46. | S. Yu, Q. Zhao, X. Miao and J. Shi, <i>Bioresource Technology</i> , 2013, <b>147</b> , 499–507.  |     |
| 863<br>864        | 47. | MM. Perrineau, J. Gross, E. Zelzion, D. C. Price, O. Levitan, J. Boyd and D. Bhattacharya, <i>PLOS One</i> , 2014, <b>9</b> , e92533.  |     |
| 865<br>866        | 48. | D. Li, L. Wang, Q. Zhao, W. Wei and Y. Sun, <i>Bioresource Technology</i> , 2015, <b>185</b> , 269–275.  |     |
| 867<br>868<br>869 | 49. | MM. Perrineau, E. Zelzion, J. Gross, D. C. Price, J. Boyd and D. Bhattacharya, <i>Environmental Microbiology</i> , 2014, <b>16</b> , 1755–1766.  |     |
| 870<br>871        | 50. | C. H. Ra, CH. Kang, N. K. Kim, CG. Lee and SK. Kim, <i>Renewable Energy</i> , 2015, <b>80</b> , 117-122.   |     |
| 872<br>873<br>874 | 51. | <ul> <li>W. Fu, Ó. Guðmundsson, G. Paglia, G. Herjólfsson, Ó. S.</li> <li>Andrésson, B. Ø. Palsson and S. Brynjólfsson, Applied</li> <li>Microbiology and Biotechnology. 2013. 97, 2395-2403.</li> </ul> |     |
| 875<br>876        | 52. | CH. Ra, CH. Kang, JH. Jung, GT. Jeong and SK. Kim, <i>Bioresource Technology</i> , 2016, <b>212</b> , 254–261.   |     |
| 877<br>878        | 53. | U. M. Tillich, N. Wolter, P. Franke, U. Dühring and M. Frohme, <i>BMC Biotechnology</i> , 2014, <b>14</b> , 1-15.  |     |
| 879<br>880        | 54. | X. M. Sun, L. J. Ren, Z. Q. Bi, X. J. Ji, Q. Y. Zhao, L. Jiang and<br>H. Huang, <i>Biotechnology for Biofuels</i> 2018, <b>11</b> , 1-16.  |     |
| 881<br>882<br>883 | 55. | M. Siaut, S. p. Cuiné, C. Cagnon, B. Fessler, M. Nguyen, P. Carrier, A. Beyly, F. Beisson, C. Triantaphylidès, Y. Li-  |     |
| 884<br>885        | 56. | W. Fu, A. Chaiboonchoe, B. Khraiwesh, D. R. Nelson, D. Al-<br>Khairy, A. Mystikou, A. Alzahmi and K. Salehi-Ashtiani,  |     |
| 885<br>887<br>888 | 57. | Marine drugs, 2016, <b>14</b> .<br>Y. Han, Q. Wen, Z. Chen and P. Li, <i>Energy Procedia</i> , 2011,<br><b>12</b> 944-950  |     |
| 889<br>890        | 58. | SI. Han, YD. Joo and KH. Han, <i>Sensors and Actuators B:</i><br><i>Chemical</i> , 2012, <b>171-172</b> , 1312-1320.   |     |

- S.-I. Han and K.-H. Han, *Analytical Chemistry*, 2015, **87**, 10585-10592.
- J. Kim, H. Cho, S.-I. Han and K.-H. Han, *Analytical Chemistry,* 2016, **88**, 4857-4863.
- H. Wang, N. Sobahi and A. Han, *Lab on a Chip*, 2017, **17**, 1264-1269.