

This is an *Accepted Manuscript*, which has been through the Royal Society of Chemistry peer review process and has been accepted for publication.

Accepted Manuscripts are published online shortly after acceptance, before technical editing, formatting and proof reading. Using this free service, authors can make their results available to the community, in citable form, before we publish the edited article. This Accepted Manuscript will be replaced by the edited, formatted and paginated article as soon as this is available.

You can find more information about *Accepted Manuscripts* in the **Information for Authors**.

Please note that technical editing may introduce minor changes to the text and/or graphics, which may alter content. The journal's standard <u>Terms & Conditions</u> and the <u>Ethical guidelines</u> still apply. In no event shall the Royal Society of Chemistry be held responsible for any errors or omissions in this *Accepted Manuscript* or any consequences arising from the use of any information it contains.



www.rsc.org/advances

- 1 Ammonium retention by oxidized biochars produced at different
- 2 pyrolysis temperatures and residence times
- Bing Wang^{a, b, *}, Johannes Lehmann^{b,c}, Kelly Hanley^b, Rachel Hestrin^b, Akio
- 4 Enders^b
- 5 ^a State Key Laboratory of Environmental Geochemistry, Institute of Geochemistry, Chinese Academy of
- 6 Sciences, Guiyang 550002, China
- 7 ^b Department of Crop and Soil Sciences, Cornell University, 909 Bradfield Hall, Ithaca, NY 14853, USA
- 8 ^cAtkinson Center for a Sustainable Future, Cornell University, Ithaca, NY, USA

^{*}Corresponding author. Tel.: +86 851 85891611

E-mail addresses: wangbing@vip.gyig.ac.cn (Bing Wang), cl273@cornell.edu (J. Lehmann), klh54@cornell.edu (K. Hanley), rh482@cornell.edu (R. Hestrin), ae55@cornell.edu (A. Enders).

9 Abstract

In order to investigate the effects of pyrolysis conditions and oxidation on the 10 retention potential of ammonium by biochar in aqueous solution, biochars were produced 11 from mixed maple wood at different pyrolysis temperatures (300, 400, 500, 600, 700°C) 12 and residence times (5, 60, 120, 400, 800 min) and adsorption and desorption was 13 determined. Hydrogen peroxide was used to oxidize the biochars to pH values ranging 14 from 7.6 to 2.7, with one set being adjusted to a pH of 7 afterwards. Without oxidation, 15 varying either pyrolysis temperatures or residence times did not have a relevant effect on 16 ammonium adsorption. When oxidized, however, ammonium adsorption was up to 3.6 17 and 1.6 times greater at lower than higher pyrolysis temperatures and shorter than longer 18 residence times, respectively. Neutralizing the oxygen-containing surface functional 19 20 groups on oxidized biochar to pH 7 further increased ammonium adsorption three to fourfold for biochars originally at a temperature of 500°C and residence time of 5 min, but 21 did not change adsorption of biochars pyrolyzed at 600°C and above and residence time 22 at 400 min and above. Adjusting the pH of unoxidized biochars had no effect on 23 ammonium adsorption. Both pyrolysis temperature and residence time significantly 24 influence the way oxidation changes charge properties with respect to ammonium 25 adsorption by woody biochar. 26

Keywords: Biochar; Biomass; Slow pyrolysis; Adsorption; Ammonium nitrogen

28 1. Introduction

Agricultural non-point source pollution caused by large amounts of nitrogen 29 fertilizers being used with low use efficiency has become a prominent problem which 30 constrains sustainable agricultural development, since a significant portion of fertilizer N 31 is lost from agricultural fields by leaching.¹ Such a loss is not only of economic concern 32 for the farmer, but also bears an environmental consequence of pollution of ground and 33 surface waters including marine ecosystems.² In addition to improved timing and dosing 34 of N applications, also an improved retention of N in the soil will help in enhancing the 35 use efficiency of applied fertilizers.^{3,4} 36

Recently, interest in biochar as a soil amendment has steadily increased and biochar 37 has attracted wide research interest. Biochar has been touted as a soil amendment to 38 improve degraded soils and increase agronomic yield by potentially changing the soil pH. 39 cation exchange capacity (CEC), reducing leaching of nutrients, and supplying nutrients 40 to plants. ⁵⁻⁸ Various pyrolysis conditions can result in biochars with different physical 41 and chemical properties, nutritional and agricultural value. Among all these factors, 42 biochar pyrolysis temperature and residence time have been considered to be the greatest 43 overall factors that influence the final characteristics of biochar, such as porous structure, 44 specific surface area and adsorption capacity as well as the retention of nutrients.⁹⁻¹² 45

A lot of research has been carried out to study the effects of pyrolysis condition on the quality and properties of biochar. ^{10, 13-17} Although several studies have investigated the adsorption of ammonium, phosphate and nitrate of different biochars, ¹⁸⁻²⁰ few research has been conducted with regard to the oxidation effect on ammonium adsorption of biochar having different properties. Some studies found that biochar can be used for

recovering excess nitrogen²⁰ and slowly release essential nutrients to soil in order to 51 improve agricultural properties, ¹⁹ improve N use efficiency, ²¹ and reduce leaching losses 52 of N.²² Key chemical and physical properties of biochar are greatly affected both by 53 choice of feedstock and process conditions (mainly temperature, residence time, heating 54 rate and feedstock preparation). These properties affect the interactions of biochar with 55 the soil as well as its fate in the environment. This underlines the importance of 56 evaluating the effect of pyrolysis conditions on the nitrogen retention potential before 57 land application. 58

Biochar is expected to be highly oxidized after long-term exposure to natural 59 oxidation processes through the formation of oxygen-containing functional groups which 60 can increase the surface acidity and CEC, ²³⁻²⁶ which influences the nutrient retention 61 capacity of biochar. Ammonium retention by biochar may be readily explained by 62 electrostatic adsorption to negatively charged surface functional groups.^{19, 24} However, 63 there has been little experimental evidence that this oxidation can be replicated by short-64 term abiotic oxidation in the laboratory under different pyrolysis conditions, which may 65 inform post-production manipulation of biochars. In addition, it is unclear whether the 66 adsorption found with aged biochars in soil is influenced by pyrolysis conditions. 67 Therefore, in order to develop a framework for the selection of biochars, the effects of 68 pyrolysis temperature and residence time on ammonium nitrogen retention by oxidized 69 70 biochar from aqueous solution need to be better understood.

The objectives of this study were to: (1) examine the retention potential of ammonium by biochars that have been oxidized to different extents; (2) establish the optimum pyrolysis temperature and residence time at which oxidized biochars adsorb the

- 74 most ammonium in aqueous solution.
- 75

76 2. Experimental methods and materials

77 2.1 Preparation of biochar

Maple wood biochars (20% sugar maple, 80% red maple) which were pyrolyzed at 78 300, 400, 500, 600, 700°C using a modified muffle furnace (Thermo Scientific, Waltham, 79 MA, USA) under argon atmosphere (sweep of 1 L min⁻¹), were ground and sieved to 80 between 149 and 850 µm to obtain a uniform particle size. The residence time in the 81 reactor was 30 min and the heating rate was 2.5°C min⁻¹. Another batch of maple wood 82 biochars was pyrolyzed at 500°C with residence times of 5 min, 30 min, 60 min, 120 min, 83 84 400 min and 800 min. The physical and chemical properties of biochars are shown in Table 1. ²⁷ All feedstocks were dried at 60°C to ca. 10% moisture (w/w) prior to 85 pyrolysis. The glassware and PE centrifuge tubes were acid washed in a hydrochloric 86 87 acid bath (10%) and rinsed with deionized (DI) water before use. The biochars were oxidized by using H_2O_2 (30% v/v) for two weeks at 30°C, all using a solid-to-liquid ratio 88 of 1:10 (w/v), which we found to result in significant changes in surface charge of 89 biochar produced at 500°C for 30 min (Wang et al., 2015). H₂O₂ was chosen in order to 90 91 minimize precipitation, complexation or analytical interference which have been observed with other oxidants (e.g., H₂SO₄, HNO₃). ²⁸ After oxidation, the H₂O₂ was 92 removed by filtration under suction using a Büchner funnel, fitted with Whatman No.1 93 filter paper, attached to a Büchner flask connected to a Welch Duo-Seal 1400 vacuum 94 pump and the oxidized biochars were rinsed with DI water. The pH values of biochars 95 were determined using a glass electrode (detection limit is 0.01 pH units) with a biochar-96

to-water ratio of 1:20 (w/v) (Orion 3-Star pH Benchtop; Thermo Electron Corporation, Beverly, MA, USA). After determining the initial pH values of the oxidized biochar samples, the biochars were dried under 60°C for 48 h, and then separated into two identical batches. One batch was utilized as it remained after oxidation and drying; for the other, hydrochloric acid (1.0 M) or sodium hydroxide solution (1.0 M) was used to

adjust the pH values to 7.00±0.01, respectively. The pH values were adjusted every 24 h
until they reached equilibrium, then suspensions were filtered through Whatman No.1
filter paper.

The specific surface area (SSA) and pore size distribution of the biochars were evaluated using the ASAP 2020 - Physisorption Analyzer (BET) CO₂ adsorption technique at 273.15 K. Determination of the CEC of biochar is based on the method by Page. ²⁹ Elemental H, O, C of biochars were determined on a Temperature Conversion Elemental Analyzer (TC/EA). Proximate analysis was conducted using ASTM D1762-84 Chemical Analysis of Wood Charcoal after modification to accommodate biochar reactivity. ¹⁶

112

97

98

99

100

101

113 2.2 Adsorption experiments

Batch adsorption experiments were conducted in PE centrifuge tubes at room temperature. All adsorption experiments were performed in triplicate. 0.5 g of biochar was added into 50-mL centrifuge tubes containing 40 mL of ammonium sulfate solution with 100 mg NH_4 – $N L^{-1}$. The tubes were shaken at 400 rpm in a mechanical shaker for 16 h and then centrifuged at 2500rpm for 10 min, and the supernatant was carefully aspirated using a Pasteur pipette. Ammonium N concentrations in the supernatant were

120	determined immediately using a continuous flow analyzer (Bran and Luebbe									
121	Autoanalyzer, SPX, Charlotte, NC).									
122										
123	2.3 Desorption experiments									
124	After the adsorption, the solution remaining in the tubes was decanted and 40 mL of									
125	ultrapure water (> 18.2 MQ·cm) which was prepared by a Barnstead E-pure water									
126	purifier was added as described for the adsorption experiment described above. This									
127	procedure was repeated twice, generating two desorption steps. Ammonium N									
128	concentrations in the supernatant were determined within 24 h by using a continuous flow									
129	analyzer (Bran and Luebbe Autoanalyzer, SPX, Charlotte, NC).									
130										
131	2.4 Statistical analysis									
132	The results of adsorption and desorption experiments were the average of three									
133	replications. The statistical software package SPSS 13.0 (Chicago, IL, USA) was used for									
134	descriptive statistics, ANOVA testing (post-hoc LSD analysis at $p < 0.05$) of ammonium									
135	adsorption and desorption at different pyrolysis temperatures and residence times. In									
136	order clarify the data present in Table 1, we performed regression analyses and added p									
137	values into the table.									
138										
139	3. Results									
140	3.1 Biochar properties									
141	Increasing the pyrolysis temperature had great effects on proton activity due to									

142 decreases in acid functional groups with greater pyrolysis temperature. Fresh biochar pH

values ranged from 6.94 at 300°C to 10.20 at 700°C. Biochars produced at higher 143 144 temperature had high alkalinity, and those at lower temperature had lower alkalinity. After oxidation, the pH dropped to 2.87 and 2.69 for biochars produced at 300°C and 145 146 400°C, respectively (Fig. 1a). During pH adjustment using NaOH, all of the oxidized biochars produced at these low temperatures dissolved, and no adsorption and desorption 147 data could be obtained. This may be explained by the reaction between sodium hydroxide 148 and acidic functional groups, such as phenolic hydroxyl and carboxyl groups. In contrast 149 to the low-temperature biochars, oxidation had lower effects on pH decrease for biochar 150 produced at higher temperature. After oxidation of biochar produced at 700°C, pH values 151 dropped from 10.2 to only 7.63. 152

In contrast to pyrolysis temperature, increasing the residence time from 5 min to 800 153 154 min at 500°C had no significant effect on pH values of the unoxidized biochar, which ranged from 8.82 at 5 min to 9.08 at 800 min (Fig. 1f). Interestingly, oxidation 155 significantly reduced the pH of biochars with short residence times, but had little effect 156 157 on pH of biochar pyrolyzed for 400 min or longer. When oxidized, varying the residence time from 5 min to 80 min at a pyrolysis temperature of 500°C had almost identical 158 effects on pH as varying the pyrolysis temperature from 300°C to 700°C at a residence 159 time of 30 min. This may be explained by the aromatization level of biochar. The high 160 temperature and long residence time makes the carbon highly aromatic. 161

Ash contents significantly increased with higher pyrolysis temperature and residence time. In contrast to ash, volatile contents decreased significantly with higher pyrolysis temperature, when the residence time increased from 60 min to 800 min, the change of volatile contents was not obvious. Fixed carbon contents of biochars significantly

increased with increasing pyrolysis temperature, but no significant increase was observed
when prolonging pyrolysis. The surface area also increased significantly with increasing
pyrolysis temperatures, but there was no alteration when pyrolyzed continuously at
500°C. Both pyrolysis temperature and residence time had significant effects on the CEC
of biochar. With the increase in pyrolysis temperature, the CEC of biochar decreased
from 117.15 cmol kg⁻¹ to 47.11 cmol kg⁻¹. Total C contents increased while total H and O
decreased with increasing temperature (Table 1).

Biochar yields decreased with increasing pyrolysis temperatures and residence times 173 Increasing the pyrolysis temperature resulted in a significant decrease in biochar yield, 174 and the highest yield was obtained at a temperature of 300°C. For instance, the yield of 175 biochar at 300°C was 62% of the dry feedstock, while at 400°C, the yield decreased to 32% 176 of the dry feedstock. At temperatures of 500, 600 and 700°C, the yield of biochar was 177 reduced to 27%, 26% and 24% of the initial weight, respectively (Fig. 1b). The largest 178 yield loss occurs within the first 120 min of residence time during pyrolysis. Increasing 179 180 the residence time from 120 min to 800 min decreased the biochar yield only slightly (Fig. 1g). 181

182

183 3.2 Ammonium adsorption

In general, fresh biochars had lower ammonium adsorption capacity than oxidized biochars; when oxidized, pH-adjusted biochars had higher adsorption capacity than not pH-adjusted biochars; and oxidized and pH-adjusted biochars pyrolyzed at lower temperatures or for shorter period of residence times had higher adsorption capacity than those pyrolyzed at higher temperatures or for longer period of times. For the fresh

biochars, there was no relevant difference among different pyrolysis temperatures. The 189 adsorbed ammonium for the fresh biochars at 300°C and 400°C was 0.87 mg g⁻¹ and 0.58 190 mg g⁻¹, respectively, and for those pyrolyzed at 500°C, 600°C, 700°C 0.52 mg g⁻¹, 0.46 191 mg g^{-1} , and 0.46 mg g^{-1} , respectively (Fig. 1c). When oxidized, biochars pyrolyzed at 192 lower temperatures (300°C, 400°C) had higher adsorption capacity than those at higher 193 pyrolysis temperatures (500°C, 600°C, 700°C). After the pH adjustment, ammonium 194 195 adsorption significantly increased at lower pyrolysis temperatures (\leq 500°C), but did not change for higher pyrolysis temperatures ($\geq 600^{\circ}$ C). 196

There was no significant difference in ammonium adsorption for fresh biochars among different residence times. However, neutralizing the oxygen-containing surface functional groups on oxidized biochars to pH 7 increased ammonium adsorption two to three-fold for biochars pyrolyzed from 5 min to 120 min (Fig. 1h).

201

202 3.3 Ammonium desorption

In general, ammonium desorption with lower pyrolysis temperature and shorter pyrolysis times was higher than with higher temperature and longer times (Fig. 1d and i). pH adjustment significantly affected the recovery: non-desorbed ammonium remained near 100% if the pH was adjusted, but decreased to 80% if the pH was not adjusted, irrespective of oxidation (Fig.1e and j). Oxidation did not have a discernable effect on the proportion of desorbed ammonium.

209

210 **4. Discussion**

4.1 Effect of oxidation and pH on ammonium retention

Freshly produced biochars typically have very low ability to adsorb ammonium, 212 showing low cation exchange capacity.³⁰ The increase in ammonium adsorption through 213 oxidation by H_2O_2 corroborate the observations from naturally aged charcoals ²³ and 214 incubation studies.²⁴ The unchanged ammonium adsorption despite greater oxidation 215 without pH adjustment may be explained by protons and possibly aluminum and reduced 216 iron or other metals that dominate the exchange sites at very low pH values.²⁰ Even 217 carbon-rich wood-based biochars as those investigated here, possess appreciable amounts 218 of ash (1.7%) which contain metals.¹⁶ On the other hand, adjusting the pH to a common 219 pH of 7, significantly increased adsorption with increasing oxidation which corroborate 220 the observations from our previous work.³¹ The reason for this is that after the pH 221 adjustment, the carboxyl and phenolic groups were deprotonated as well as free 222 aluminum and iron may have precipitated as oxides and the negatively charged organic 223 224 functional groups became the main adsorption sites for ammonium.

Abiotic oxidation with peroxide generated oxygen-containing functional groups, 225 226 which largely improve ammonium adsorption capacity. Another reason for the enhancemed ammonium adsorption capacity is the increase of negative charges on the 227 surface of the biochar. ³¹ Higher pyrolysis temperatures and longer residence times result 228 229 in higher degrees of biochar aromaticity. Elemental H/C and O/C ratios can be used to estimate the degree of aromaticity of the carbon structure. Biochars produced at low 230 temperatures had higher H/C ratios, and biochars produced at high temperatures had 231 lower H/C ratios. Previous studies have shown that biochar amendment can increase CEC 232 in soil ³² and that when aging and weathering of the biochar occurs the CEC can be 233 further increased. ³³ Therefore, the oxygen-containing functional groups and negative 234

Tage 12 01

charges in the oxidized biochar pyrolyzed under low temperatures and short residence times are higher than those pyrolyzed under high temperatures and long residence times. Previous studies have also pointed out that, initially, biochars produced at high pyrolysis temperatures (800°C) had greater exchangeable cations and CEC than those produced at lower temperatures. However, after 8 weeks of oxidation the CEC of low temperature biochars was significantly higher, ³⁴ which is consistent with the results of this study.

4.2 Pyrolysis conditions and ammonium nitrogen retention

Without oxidation, varying the pyrolysis residence time beyond 5 min had no effects on ammonium adsorption, corollary with a lack of change in pH, elemental ratios, or surface area. The lack of an increase in surface area may be explained by the observation that prolonging heat treatment at 500°C may lead to increased softening of some volatile fractions, forming an intermediate melt which closes and seals off some of the pores, compensating for any creation of pores with longer pyrolysis times.

However, the lack of change in ammonium adsorption to unoxidized biochars as a function of pyrolysis temperature is more difficult to explain, as pH, O/C ratios, and surface areas suggested a change in biochar properties. It is possible that the decrease in acid functional groups with increasing pyrolysis temperatures is compensated by an increase in surface area, canceling any temperature effects for the biochars studied here. Increases in surface area with higher pyrolysis temperature are typically observed, ¹⁴ as are lower O/C ratios.¹⁶

Interestingly, when biochars were oxidized, both residence time and pyrolysis temperature affected ammonium adsorption, and did so to a much greater extent than if they were not oxidized. The much greater adsorption to oxidized biochars produced at

lower temperatures and shorter residence times may be the result of greater oxidation, 258 shown by a greater pH drop and increases in the O/C ratios. Greater oxidation with 259 shorter pyrolysis times and lower temperatures upon exposure to H_2O_2 may be explained 260 261 by the lower degree of fused aromatic C structures typically found under those conditions, ^{35, 36} also indicated by the higher H/C ratios found in our study. This probably 262 also means that those biochars produced at lower temperatures and shorter residence 263 times will develop cation retention capacity more quickly when added to soil. This may 264 pose a tradeoff with an intent to produce biochars with long turnover times in soil, which 265 are typically produced at higher pyrolysis temperatures.³⁷ 266

267

268 5. Conclusions

Freshly produced biochars have low ability to adsorb ammonium. Only pyrolysis 269 temperature but not residence times affected oxidation, pH, surface area, and yield of 270 fresh biochar, but none of the two affected the adsorption capacity of fresh biochar. 271 Short-term abiotic oxidation significantly increased ammonium retention of biochars, and 272 under these oxidized conditions, also pyrolysis residence times had significant effects. 273 274 The greater ammonium adsorption for less pyrolyzed biochars when oxidized may 275 constitute a tradeoff with maximizing biochar persistence where both are desired. Future research should examine whether this also holds for effects of pyrolysis residence times 276 277 on biochars oxidized over time when they are added to soils.

278

279 Acknowledgements

Financial support for this work was given by the NSF-Basic Research for Enabling

RSC Advances Accepted Manuscript

281 Agricultural Development program (BREAD grant number IOS-0965336), the Fondation des Fondateurs, Towards Sustainability Foundation, the Reinvent the Toilet Challenge 282 program of the Bill and Melinda Gates Foundation, the Impact through Innovation Fund 283 of the Atkinson Center for a Sustainable Future, the International Scientific and 284 Technological Cooperation Project of Guizhou Province (grant number G[2012]7050), 285 the"Dawn of West China" Talent Training Program of the Chinese Academy of Sciences 286 (grant number [2012]179) and the State Key Laboratory of Environmental Geochemistry, 287 Geochemistry, Chinese Academy of Sciences 288 Institute of (grant number 289 SKLEG2014912). Any opinions, findings, conclusions, or recommendations expressed in this material are those of the authors and do not necessarily reflect the views of the 290 291 donors.

292

293 **References**

- 294 1. W. R. Raun and G. V. Johnson, *Agron. J*, 1999, 91, 357-363
- 295 2. S. R. Carpenter, N. F. Caraco, D. L. Correll, R. W. Howarth, A. N. Sharpley and V. H. Smith, *Ecol. Appl.*, 1998, 8, 559-568.
- 297 3. C. Steiner, B. Glaser, W. Geraldes Teixeira, J. Lehmann, W. E. Blum and W. Zech, J. Plant Nutr.
 298 Soil Sci., 2008, 171, 893-899.
- P. M. Vitousek, J. D. Aber, R. W. Howarth, G. E. Likens, P. A. Matson, D. W. Schindler, W. H.
 Schlesinger and D. G. Tilman, *Ecol. Appl.*, 1997, 7, 737-750.
- **301** 5. J. Lehmann, *Nature*, 2007, **447**, 143-144.
- K. A. Spokas, K. B. Cantrell, J. M. Novak, D. W. Archer, J. A. Ippolito, H. P. Collins, A. A.
 Boateng, I. M. Lima, M. C. Lamb and A. J. McAloon, *J. Environ. Qual*, 2012, 41, 973-989.
- 304 7. L. A. Biederman and W. S. Harpole, *Glob. Change. Biol. Bioenergy*, 2013, 5, 202-214.
- 8. C. Steiner, W. G. Teixeira, J. Lehmann, T. Nehls, J. L. V. de Macêdo, W. E. H. Blum and W. Zech, *Plant Soil*, 2007, **291**, 275-290.
- 307 9. E. Agrafioti, G. Bouras, D. Kalderis and E. Diamadopoulos, *J. Anal. Appl. Pyrol*, 2013, 101, 72 308 78.
- 309 10. F. Ronsse, S. van Hecke, D. Dickinson and W. Prins, *Glob. Change. Biol. Bioenergy*, 2013, 5, 104-115.
- 311 11. K. Gergova, N. Petrov and V. Minkova, J. Chem. Tech. Biotechnol., 1993, 56, 77-82.
- 312 12. A. Shaaban, S.-M. Se, M. F. Dimin, J. M. Juoi, M. H. Mohd Husin and N. M. M. Mitan, *J. Anal. Appl. Pyrol*, 2014, 107, 31-39.
- 314 13. K. Crombie, O. Masek, S. P. Sohi, P. Brownsort and A. Cross, *Glob. Change. Biol. Bioenergy*, 2013, 5, 122-131.
- 316 14. D. M. Mackay and P. V. Roberts, *Carbon*, 1982, **20**, 95-104.

317	15.	S. T. Shafie, M. A. Mohd Salleh, L. Lek Hang, M. M. Rahman and W. A. Wan Abdul Karim
318		Ghani, J. Purity, Utility Reaction . Environ., 2012, 1, 323-337
319	16.	A. Enders, K. Hanley, T. Whitman, S. Joseph and J. Lehmann, <i>Bioresource. Technol</i> , 2012, 114 , 644, 652
320	17	W Song and M Guo I Anal Appl Pyrol 2012 94 138-145
322	18	X Gai H Wang I Liu L Zhai S Liu T Ren and H Liu <i>PloS one</i> 2014 9 e113888
323	19	S E Hale V Alling V Martinsen J Mulder G D Breedveld and G Cornelissen <i>Chemosphere</i>
324		2013. 91 , 1612-1619.
325	20.	D. Sarkhot, T. Ghezzehei and A. Berhe, J. Environ. Oual, 2013, 42, 1545-1554.
326	21.	L. v. Zwieten, S. Kimber, A. Downie, S. Morris, S. Petty and K. Y. J. Rust, Aust. J. Soil. Res,
327		2010, 48 , 569-576.
328	22.	D. Güereña, J. Lehmann, K. Hanley, A. Enders, C. Hyland and S. Riha, Plant Soil, 2013, 365,
329		239-254.
330	23.	C. H. Cheng, J. Lehmann and M. H. Engelhard, Geochim. Cosmochim. Acta, 2008, 72, 1598-1610.
331	24.	C. H. Cheng, J. Lehmann, J. E. Thies, S. D. Burton and M. H. Engelhard, Org. Geochem., 2006,
332		37 , 1477-1488.
333	25.	C. H. Cheng and J. Lehmann, Chemosphere, 2009, 75, 1021-1027.
334	26.	C. F. Olivier, Stellenbosch: Stellenbosch University, 2011.
335	27.	ASTM, D1762-84 Standard Test Method for Chemical Analysis of Wood Charcoal, ASTM
336		International, Conshohocken, PA, 2007.
337	28.	J. P. Chen and S. Wu, <i>Langmuir</i> , 2004, 20 , 2233-2242.
338	29.	A. L. Page, Methods of Soil Analysis. Part 2. Chemical and Microbiological Properties, American
339		Society of Agronomy, Soil Science Society of America, 1982.
340	30.	S. Rajkovich, A. Enders, K. Hanley, C. Hyland, A. Zimmerman and J. Lehmann, <i>Biol. Fert. Soils</i> ,
341		2012, 48, 271-284.
342	31.	B. Wang, J. Lehmann, K. Hanley, R. Hestrin and A. Enders, <i>Chemosphere</i> , 2015, 138 , 120-126.
343	32.	B. Liang, J. Lehmann, D. Solomon, J. Kinyangi, J. Grossman, B. O'Neill, J. Skjemstad, J. Thies, F.
344	22	Luizao and J. Petersen, Soil. Sci. Soc. Am. J, 2006, $70, 179-1730$.
345	33. 24	B. Glaser, J. Lehmann and W. Zech, <i>Biol. Fert. Soils</i> , 2002, 35 , 219-230.
340 247	34. 25	C. W. Edmunds, 2012.
547 240	55.	J. Lemnann and S. Joseph, <i>Biochar for environmental management</i> . science and technology,
240 240	26	Editiscal/James & James, 2009. D. Vim A. Johnson C. W. Edmunds, M. Dadosavish, E. Vogt, T. C. Dials and N. Labhá, Engua
343	50.	Find 2011 25 $A603 A703$
251	37	I Delando I Soil Water Conserv. 2002 57 380 308
JJT	51.	3. Delgado, 5. 501 mater Conserv., 2002, 51, 507-576.

352

353

יא ר

Table	1	Phys	ical	and	chen	nical	pro	nerties	of	biocha	ars
1 4010	1.	1 Hys	icai	anu	chen	incar	pro	pernes	01	Ulocite	us.

Process conditions		ns Proximate analysis (wt.% dry)					Elem	ental conte	nts	Surface area $(m^2 g^{-1})$			
Pyrolysis temperature (°C)	Residence time (min)	рН	Volatile matter	Ash content	Fixed carbon	C _{tot} (w%)	H (w%)	O (w%)	H/C _{tot} (mol mol ⁻¹)	O/C _{tot} (mol mol ⁻¹)	BET CO ₂	CEC (cmol kg ⁻¹)	
Original biochar													
300	30	6.94	68.5	0.54	31.0	58.9	5.22	32.9	1.06	0.42	72.4±1.5	117.2±2.3	
400	30	7.60	30.3	1.75	67.9	78.8	3.53	17.0	0.54	0.16	182±1.9	98.6±1.6	
500	30	8.90	21.1	2.16	76.7	91.5	2.81	9.51	0.37	0.08	250±2.0	78.1±1.4	
600	30	9.09	13.4	2.29	84.3	88.9	2.34	5.56	0.32	0.05	298±2.0	72.5±0.9	
700	30	10.2	8.44	2.59	89.0	94.9	1.33	3.92	0.17	0.03	337±2.1	47.1±0.7	
P-value		0.003	0.034	0.029	0.034	0.042	0.005	0.023	0.027	0.049	0.004	0.002	
500	5	8.82	24.3	1.65	74.0	83.3	2.98	11.9	0.43	0.11	222±2.0	122.7±1.8	
500	60	8.84	18.5	1.93	79.6	88.8	2.89	9.18	0.39	0.08	266±2.1	114.1±1.1	
500	120	8.67	17.7	2.04	80.2	86.2	2.79	8.23	0.39	0.07	272±2.1	104.1±0.,	
500	400	8.70	14.5	2.34	83.2	91.6	2.67	7.96	0.35	0.07	294±2.1	93.0 ±0.6	
500	800	9.08	14.4	2.58	83.0	84.5	2.54	7.06	0.36	0.06	274±1.9	70.7±0.4	
P-value		0.227	0.129	0.016	0.150	1.000	0.013	0.140	0.133	0.169	0.355	0.004	
Oxidized biochar												e C	
300	30	2.87	-	-	-	49.4	5.23	44.3	1.27	0.67	61.5±1.9	143.2 ±1.5	
400	30	2.69	-	-	-	59.5	3.03	34.6	0.61	0.44	132±1.8	125.8 ±1.5	
500	30	4.01	-	-	-	73.4	2.80	19.7	0.46	0.20	243±2.0	122.7±1.	
600	30	7.00	-	-	-	84.0	2.02	8.36	0.29	0.07	287±1.9	117.8±2.1	
700	30	7.63	-	-	-	93.3	1.32	5.33	0.17	0.04	319±2.0	110.9±2.8	
P-value		0.017				0.000	0.015	0.003	0.024	0.008	0.004	0.013	
500	5	3.10	-	-	-	67.3	2.53	25.6	0.45	0.28	174±1.8	131.4±3.1	
500	60	3.94	-	-	-	76.2	2.61	18.6	0.41	0.18	246±1.9	124.6±2.9	
500	120	4.45	-	-	-	77.1	2.50	15.8	0.39	0.15	255±2.0	113.4±1.4	
500	400	7.12	-	-	-	80.5	2.47	12.6	0.37	0.12	267±1.9	96.7±1.1	
500	800	6.99	-	-	-	83.4	1.95	10.1	0.28	0.09	269±1.9	84.9±0.7	
P-value		0.046				0.089	0.021	0.074	0.007	0.104	0.251	0.011	

a Ctot is the total carbon of biochar.

b P-value for a linear regression of the effect of pyrolysis temperature and residence time.



Fig. 1. The effect of pyrolysis temperature (a-e) or residence time in the pyrolyser (g-j) on pH, biochar yield, ammonium adsorption, ammonium desorption and the proportion of non-desorbed ammonium (adsorption and desorption of oxidized and pH-adjusted biochars at low temperatures could not be studied due to their high solubility). Error bars represent standard error of triplicate samples (n = 3). Symbols may cover error

bars. 171x295mm (150 x 150 DPI)